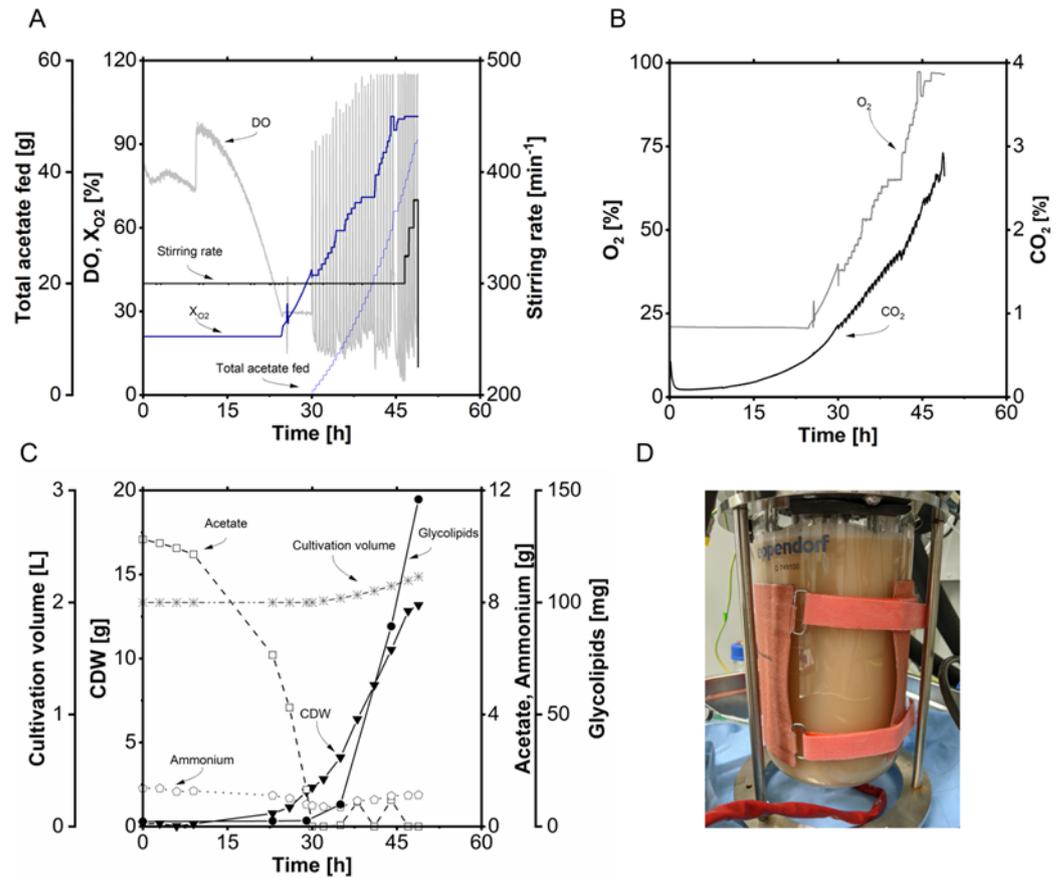
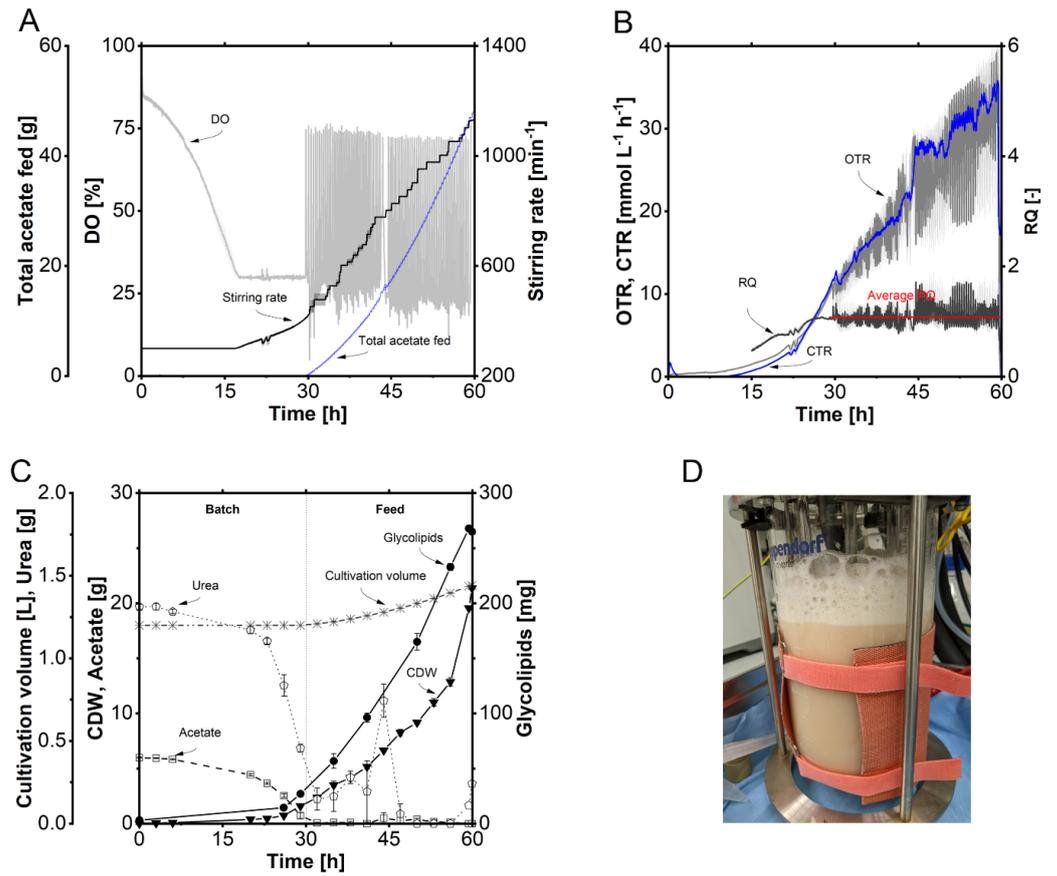


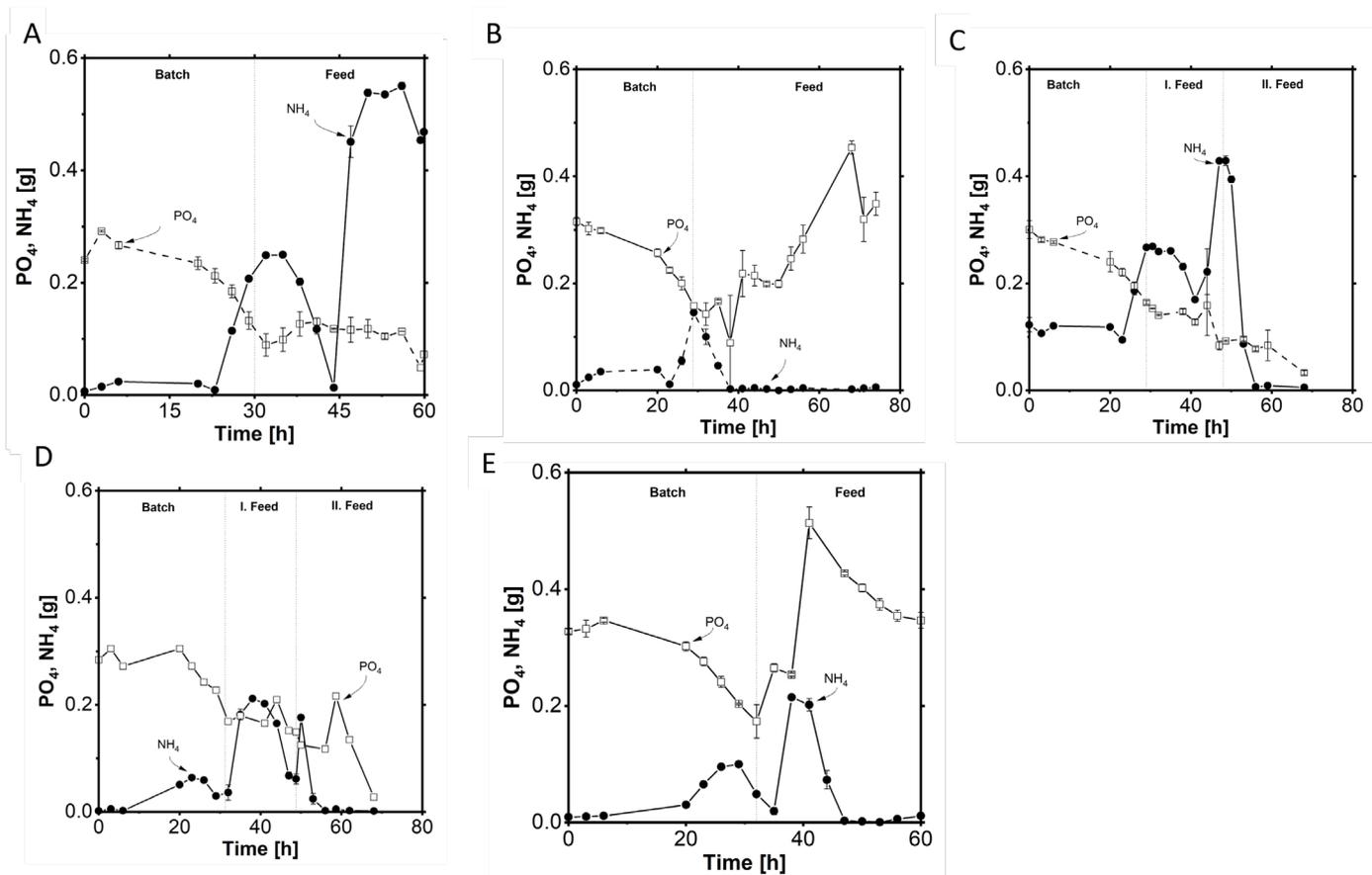
**Figure S1.** Fed-batch benchmark fermentation of *A. borkumensis* SK2 with bubble aeration and NH<sub>4</sub>Cl as nitrogen source. Time course of **(A)** total acetate fed, dissolved oxygen (DO), and stirring rate; **(B)** oxygen transfer rate (OTR), carbon dioxide transfer rate (CTR), respiratory quotient (RQ), and average RQ of fed-batch phase (red); **(C)** cultivation volume, cell dry weight (CDW), acetate, ammonium, and glycolipids amount. **(D)** Photo of the formed foam in the bioreactor after 44 h of cultivation. Error bands/bars indicate deviation from the mean (n = 2). Cultivation conditions: modified ONR7a medium, 3 L stirred-tank bioreactor, T = 30°C, pH = 7.3, N = 300 - 1,200 min<sup>-1</sup> (cascaded), DO = 30%, F<sub>Air</sub> = 0.41 L min<sup>-1</sup>, OD<sub>start</sub> = 0.2, V<sub>L</sub> = 1.2 L. DO-based feed with C/N of 8.9 Cmol Nmol<sup>-1</sup>: 200 g L<sup>-1</sup> acetate, 40 g L<sup>-1</sup> NH<sub>4</sub>Cl, 9.2 g L<sup>-1</sup> NaH<sub>2</sub>PO<sub>4</sub> 2 H<sub>2</sub>O, V<sub>Feed</sub> = 250 mL.



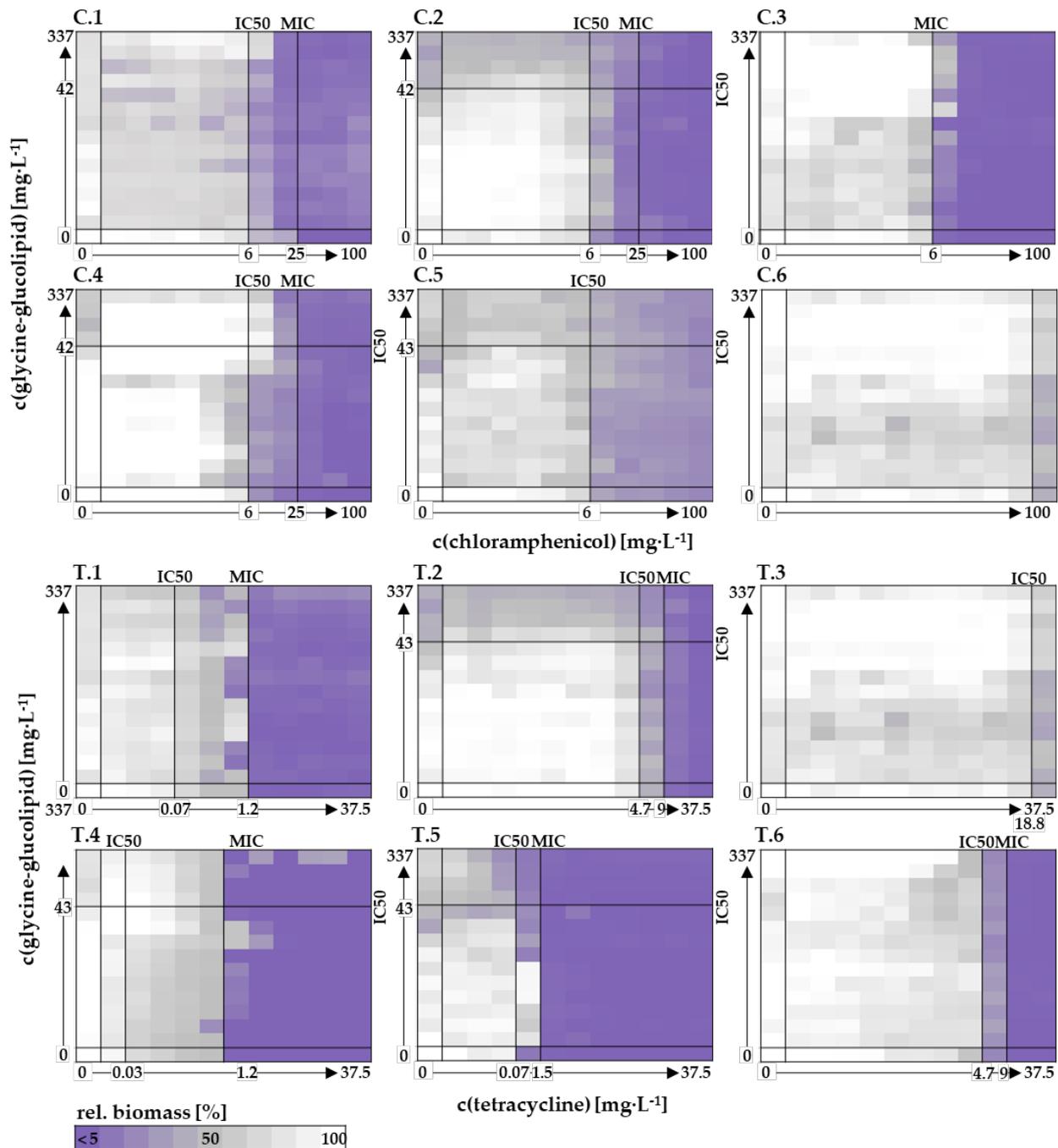
**Figure S2.** Fed-batch benchmark fermentation of *A. borkumensis* SK2 with bubble-free membrane aeration and  $NH_4Cl$  as nitrogen source. Time course of (A) total acetate fed, dissolved oxygen (DO),  $X_{O_2}$ , and stirring rate; (B)  $O_2$  and  $CO_2$  concentrations in the off-gas; (C) cultivation volume, cell dry weight (CDW), acetate, ammonium, and glycolipids amount. (D) Photo of the formed foam in the bioreactor after 47 h of cultivation. Cultivation conditions: modified ONR7a medium, 3 L stirred-tank bioreactor,  $T = 30^\circ\text{C}$ ,  $\text{pH} = 7.3$ ,  $N = 300 - 375 \text{ min}^{-1}$ ,  $\text{DO} = 30\%$ ,  $\text{TMP} = 0.3 \text{ bar}$   $X_{O_2} = 21 - 100\%$  (cascaded),  $F_{\text{Gas}} = 1.0 \text{ L min}^{-1}$ ,  $\text{OD}_{\text{start}} = 0.2$ ,  $V_L = 2.0 \text{ L}$ . DO-based feed with C/N of 8.9  $\text{Cmol Nmol}^{-1}$ :  $200 \text{ g L}^{-1}$  acetate,  $40 \text{ g L}^{-1}$   $NH_4Cl$ ,  $9.2 \text{ g L}^{-1}$   $NaH_2PO_4 \cdot 2 H_2O$ ,  $V_{\text{Feed}} = 250 \text{ mL}$ .



**Figure S3.** DO-based fed-batch benchmark fermentation of *A. borkumensis* SK2 with bubble aeration and urea as nitrogen source. Time course of (A) total acetate fed, dissolved oxygen (DO), and stirring rate; (B) oxygen transfer rate (OTR), carbon dioxide transfer rate (CTR), respiratory quotient (RQ), and average RQ of fed-batch phase (red); (C) cultivation volume, cell dry weight (CDW), acetate, urea, and glycolipids amount. (D) Photo of the formed foam in the bioreactor after 56 h cultivation. Error bands/bars indicate deviation from the mean ( $n = 2$ ). Cultivation conditions: modified ONR7a medium, 3 L stirred-tank bioreactor,  $T = 30^{\circ}\text{C}$ ,  $\text{pH} = 7.3$ ,  $N = 300 - 1,200 \text{ min}^{-1}$  (cascaded),  $\text{DO} = 30\%$ ,  $F_{\text{Air}} = 0.41 \text{ L min}^{-1}$ ,  $\text{OD}_{\text{start}} = 0.2$ ,  $V_{\text{L}} = 1.2 \text{ L}$ . DO-based feed with  $\text{C/N}$  of 8.9  $\text{Cmol Nmol}^{-1}$ :  $200 \text{ g L}^{-1}$  acetate,  $22.4 \text{ g L}^{-1}$  urea,  $9.2 \text{ g L}^{-1} \text{ NaH}_2\text{PO}_4 \cdot 2 \text{ H}_2\text{O}$ ,  $V_{\text{Feed}} = 250 \text{ mL}$ .



**Figure S4.** Ammonium and phosphate amount time course of the urea fed-batch fermentations. **(A)** DO-based fed-batch urea fermentation with a C/N ratio of 8.9  $\text{Cmol Nmol}^{-1}$ . **(B)** DO-based fed-batch urea fermentation with a C/N ratio of 17.8  $\text{Cmol Nmol}^{-1}$ . **(C)** DO-based two-stage fed-batch urea fermentation with a C/N ratio of 17.8  $\text{Cmol Nmol}^{-1}$ . **(D)** DO-based two-stage fed-batch urea fermentation with a C/N ratio of 26.7  $\text{Cmol Nmol}^{-1}$ . **(E)** pH-stat fed-batch fermentation of *A. borkumensis* SK2 with bubble aeration and glacial acetic acid with C/N of 17.8 as feed.



**Figure S5.** Combined antibacterial effect of chloramphenicol and tetracycline with glycine-glucolipid against different bacteria for MIC (<5% growth in terms of reached cell density) and IC50 (<50% growth) determination. The substances were each applied in dilution series with a dilution factor of two against each other according to a Checkerboard matrix. The color scale represents the relative biomass of the cultures after 18 h cultivation in relative percentage terms compared to the reference culture without antibiotic or surfactant. Violet: <5% defined as no growth; grey: moderately affected cell growth; white: unaffected cell growth. The MIC and IC50 values for the individual tests of chloramphenicol, tetracycline and glycine-glucolipid are specified. All values are in mg·L<sup>-1</sup>, with the individual dilution series being as follows: chloramphenicol (0-0.04-0.09-0.19-0.39-0.78-1.56-3.13-6.25-12.5-25-50-100), tetracycline (0-0.015-0.03-0.07-0.146-0.29-0.586-1.171-2.344-4.688-9.375-18.75-37.5), and glycine-glucolipid (0-0.02-0.04-0.08-0.16-0.33-0.66-1.32-2.63-5.27-10.53-21.07-42.14-84.27-168.55-337.09). The presented values represent the mean of two independently conducted experiments in triplicate (n=2). C: chloramphenicol; T: tetracycline; 1: *C. glutamicum*; 2: *S. marcescens*; 3: *S. epidermidis*; 4: *E. faecium*; 5: *S. aureus*; 6: *P. aeruginosa*.