Special Issue

Catalysts for Water-Gas Shift Reaction

Message from the Guest Editors

The majority of industrial H2 is currently produced by methane steaming reforming (MSR) followed by watergas shift (WGS) reaction to control the H2/CO ratio and is employed in numerous applications such as ammonia synthesis, methanol synthesis, synthetic fuels, etc. Although there is much interest in developing sustainable H2 production from photocatalytic/electrocatalytic splitting of H2O and biomass reforming, production of H2 from fossil fuels (CH4, hydrocarbons and coal) will be around and expand for guite some time given its established technology and cost competitiveness. Currently, the WGS reaction is commercially performed in several stages with different catalysts to optimize the greater CO equilibrium conversion attained at lower temperatures because the reaction is exothermic and reversible. Commercially, the low-temperature WGS (LT-WGS) reaction is performed at \(\text{190} - 250 \, \text{°C} \) with a Cu/ZnO/Al2O3 catalyst, and the high-temperature WGS (HT- WGS) reaction is performed at \(\times 350 - 450 \, \times C \times it has a Cu promoted chromium-iron \) mixed oxide catalyst.

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