

Supplementary material

Montmorillonite-Based Natural Adsorbent from Colombia for the Removal of Organic Pollutants from Water: Isotherms, Kinetics, Nature of Pollutants, and Matrix Effects

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Table S1. Chemical composition of fresh urine and textile wastewater.

Fresh Urine		Textile wastewater	
Concentration [mg L ⁻¹]		Concentration [mg L ⁻¹]	
Urea	16000	Dye	Required concentration
Na ₂ SO ₄	2300	NaCl	1500
NH ₄ Cl	1800	Na ₂ CO ₃	500
NaH ₂ PO ₄	2900	NaHCO ₃	500
KCl	4200	NaOH	500
MgCl ₂ •6H ₂ O	790	H ₂ SO ₄	800
CaCl ₂ •2H ₂ O	680	Starch	500
NaOH	120		

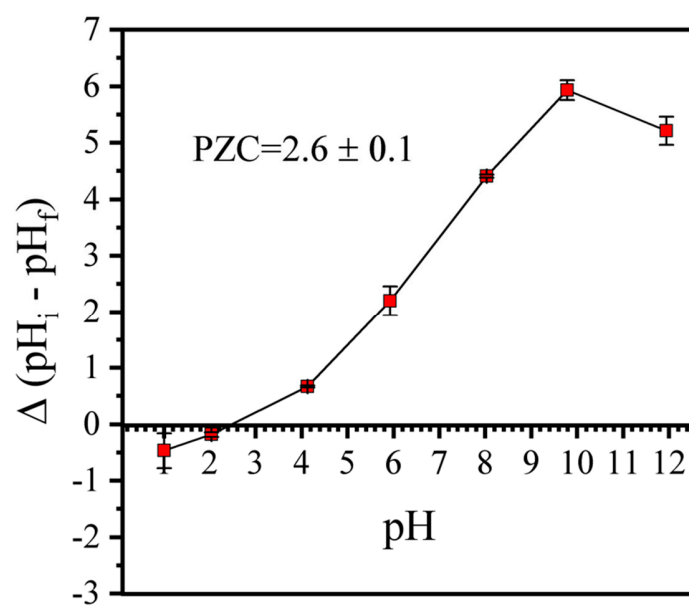


Figure S1. Determination of PZC value of MMT

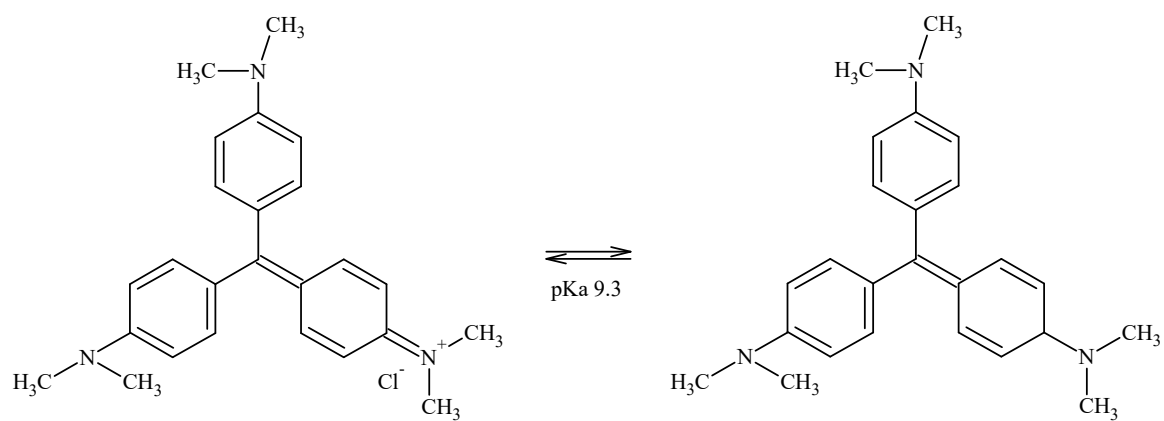


Figure S2. Structure CV

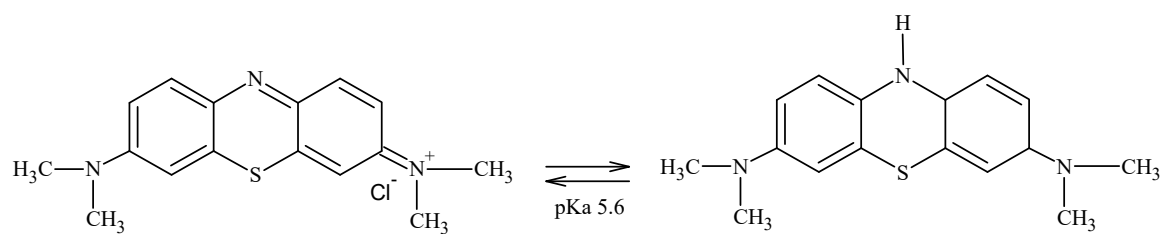


Figure S3. Structure MB

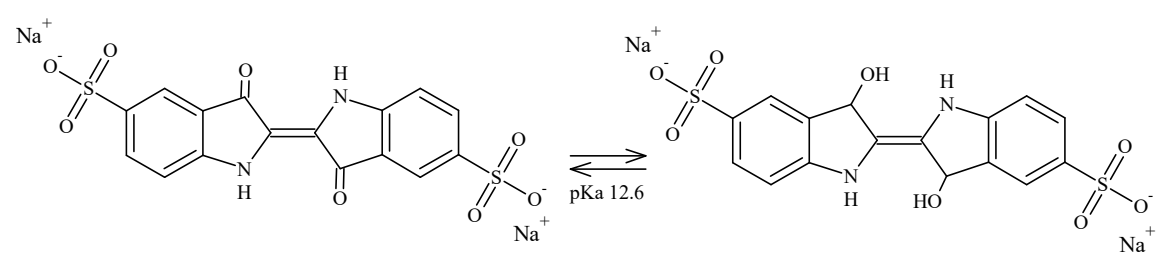


Figure S4. Structure IC

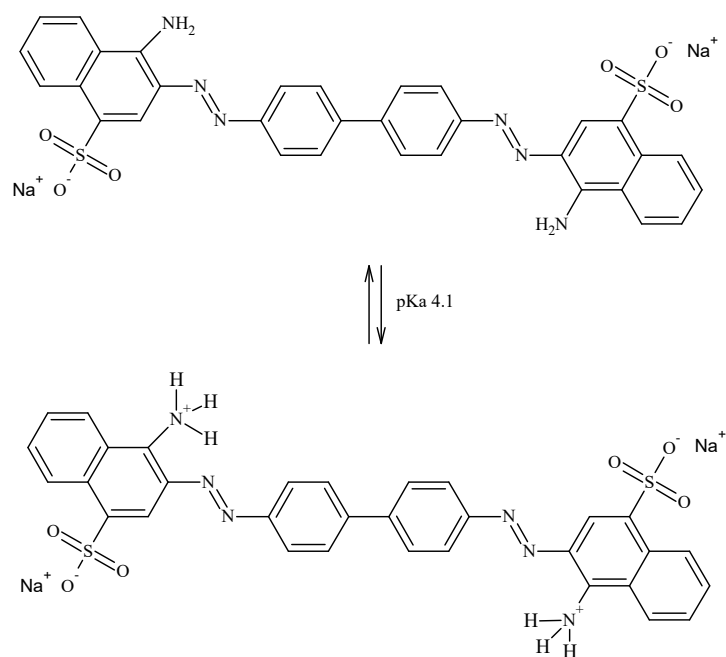


Figure S5. Structure CR

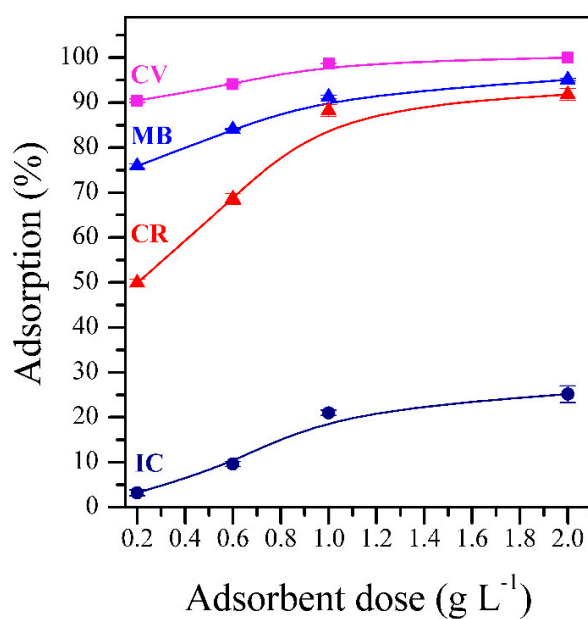


Figure S6. Effect of MMT dose in the adsorption percentage of CV, MB, CR and IC after 60 min. Conditions: Dyes concentration $1.23 \times 10^{-2} \text{ mmol L}^{-1}$, adsorbent dose $0.2 - 2 \text{ g L}^{-1}$, particle size $<200 \text{ }\mu\text{m}$, pH: IC: 5.7; CR: 6.5; MB: 5.6; CV: 7.3, temperature 25°C , stirring rate 200 rpm.

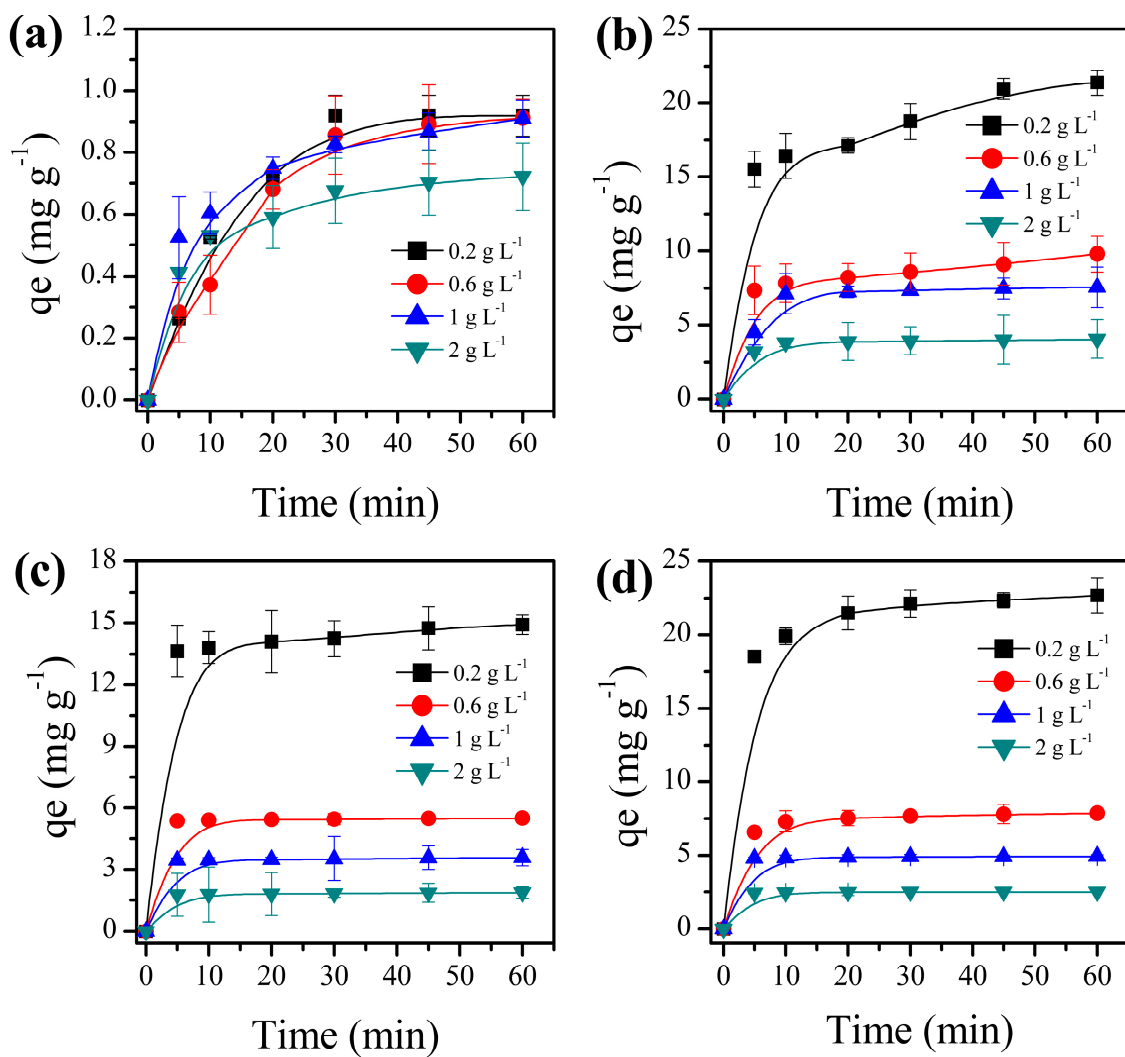


Figure S7. IC, CR, MB and CV removal in distilled water using different doses of MMT. Conditions: dyes concentration 1.23×10^{-2} mmol L⁻¹ (IC: 5.74 mg L⁻¹, CR: 8.57 mg L⁻¹, MB: 3.93 mg L⁻¹ and CV: 4.85 mg L⁻¹), adsorbent dose 0.2 - 2 g L⁻¹, particle size <200 μ m, pH: IC: 5.7; CR: 6.5; MB: 5.6; CV: 7.3, temperature 25°C, stirring rate 200 rpm.

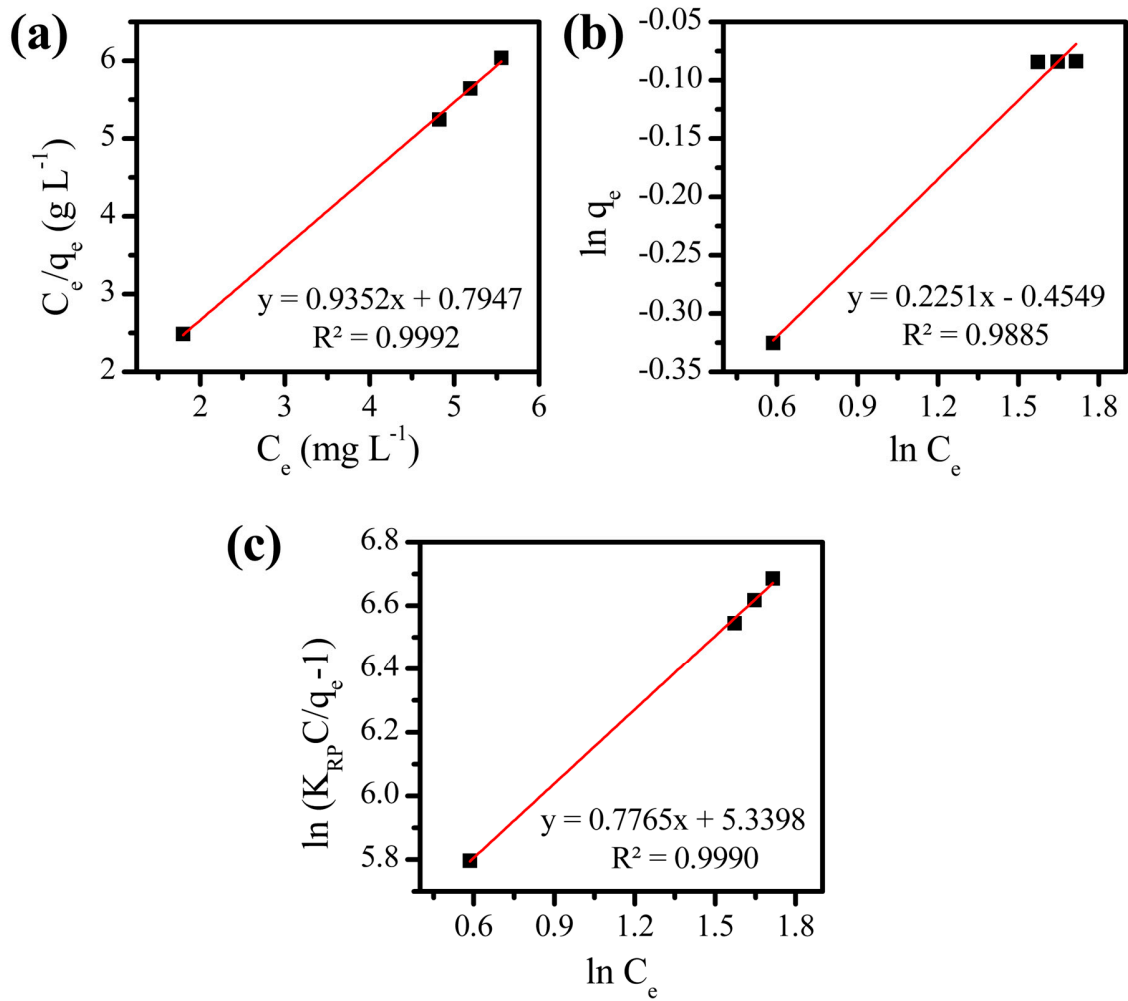


Figure S8. Adsorption isotherms for IC removal in distilled water using MMT as an adsorbent. (a) Langmuir model; (b) Freundlich model; (c) Redlich-Peterson model. Conditions: dye concentration 1.23×10^{-2} mmol L⁻¹ (5.74 mg L⁻¹), adsorbent dose 0.2 - 2 g L⁻¹, particle size <200 μ m, pH: 5.7, temperature 25°C, stirring rate 200 rpm, time 60 min.

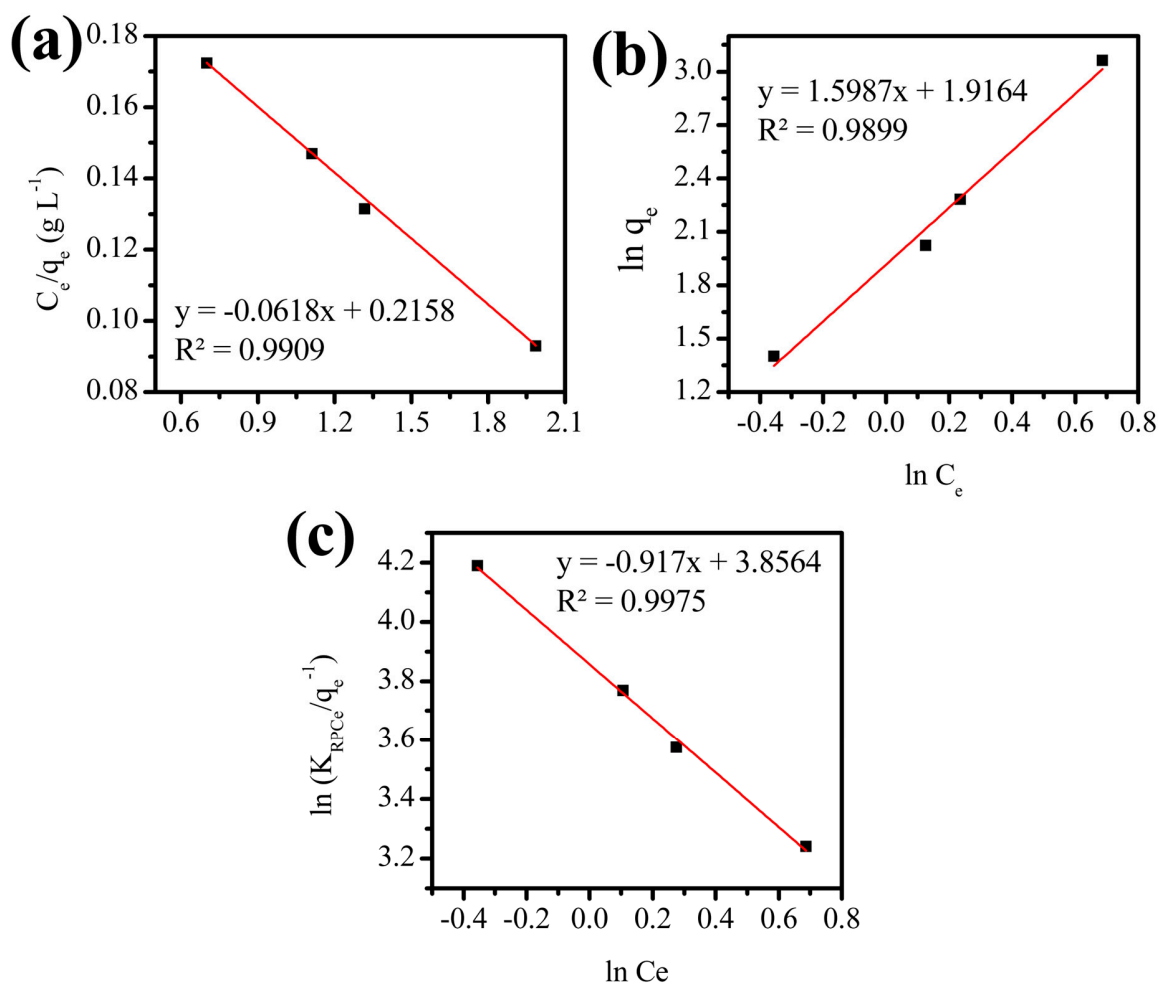


Figure S9. Adsorption isotherms for CR removal in distilled water using MMT as an adsorbent. (a) Langmuir model; (b) Freundlich model; (c) Redlich-Peterson model. Conditions: dye concentration 1.23×10^{-2} mmol L⁻¹ (8.57 mg L⁻¹), adsorbent dose 0.2 - 2 g L⁻¹, particle size <200 μ m, pH: 6.5, temperature 25°C, stirring rate 200 rpm, time 60 min.

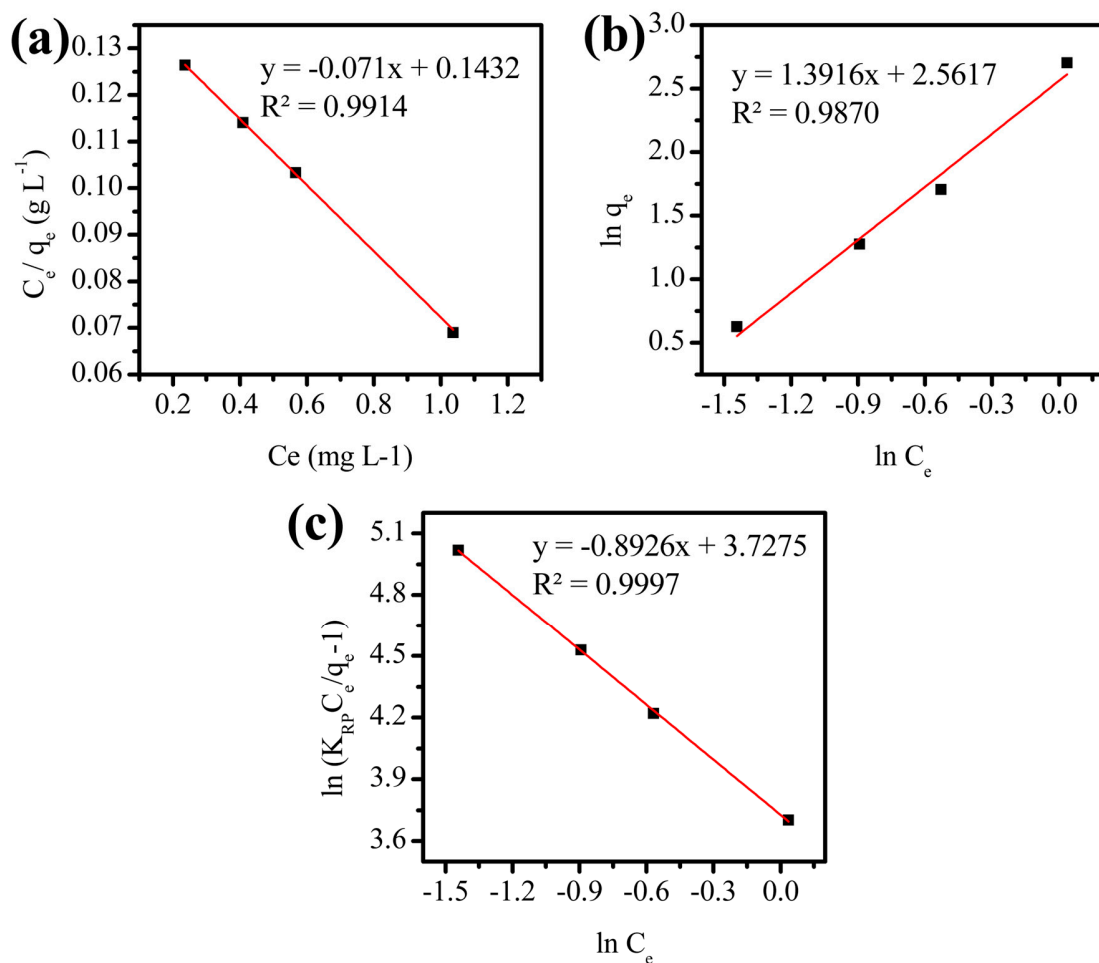


Figure S10. Adsorption isotherms for MB removal in distilled water using MMT as an adsorbent. (a) Langmuir model; (b) Freundlich model; (c) Redlich-Peterson model. Conditions: dye concentration 1.23×10^{-2} mmol L⁻¹ (3.93 mg L⁻¹), adsorbent dose 0.2-2 g L⁻¹, particle size <200 μ m, pH: 5.6, temperature 25°C, stirring rate 200 rpm, time 60 min.

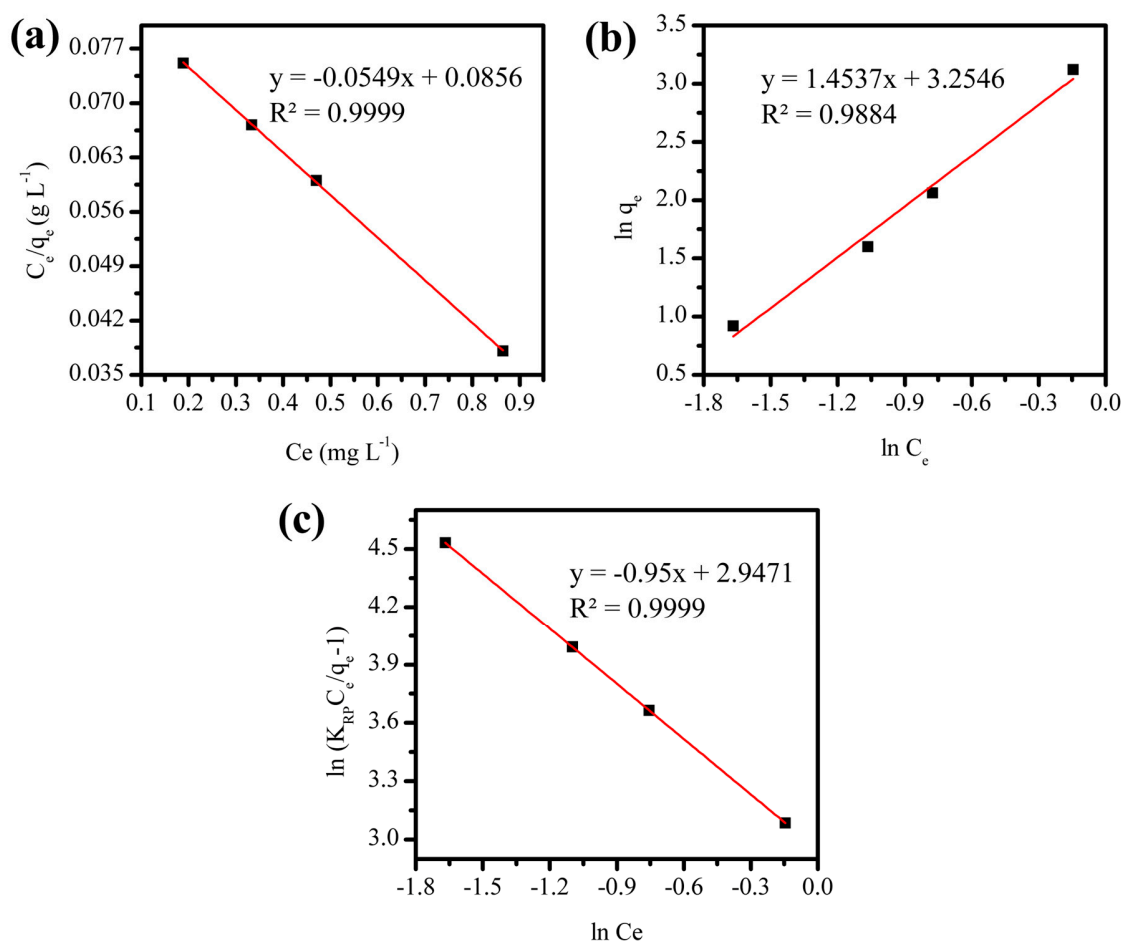


Figure S11. Adsorption isotherms for CV removal in distilled water using MMT as an adsorbent. (a) Langmuir model; (b) Freundlich model; (c) Redlich-Peterson model. Conditions: dye concentration 1.23×10^{-2} mmol L⁻¹ (4.85 mg L⁻¹), adsorbent dose 0.2 - 2 g L⁻¹, particle size <200 μ m, pH: 7.3, temperature 25°C, stirring rate 200 rpm, time 60 min.

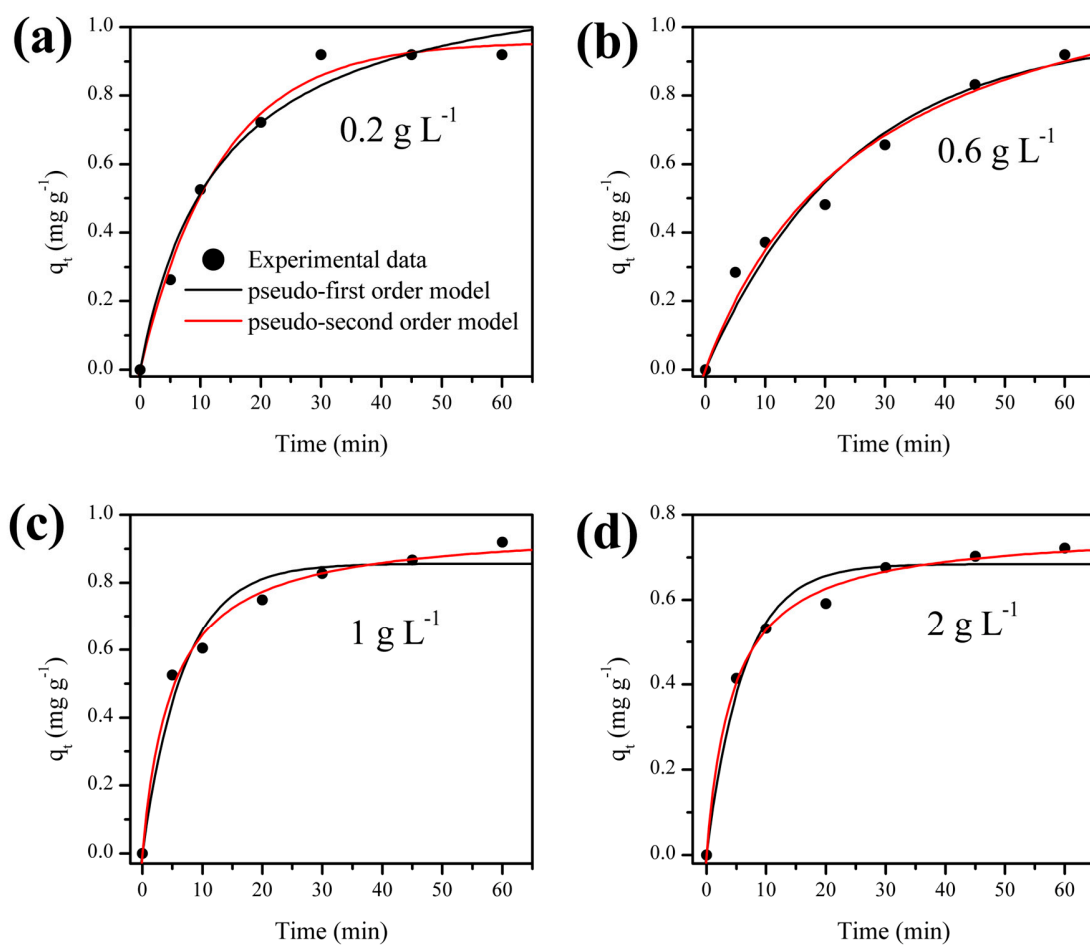


Figure S12. Kinetics of pseudo-first order model and pseudo-second order model for IC removal in distilled water using MMT as an adsorbent. (a) 0.2 g L⁻¹; (b) 0.6 g L⁻¹; (c) 1 g L⁻¹; (d) 2 g L⁻¹. Conditions: dye concentration 1.23×10^{-2} mmol L⁻¹ (5.74 mg L⁻¹), particle size <200 μ m, pH: 5.7, temperature 25°C, stirring rate 200 rpm, time 60 min.

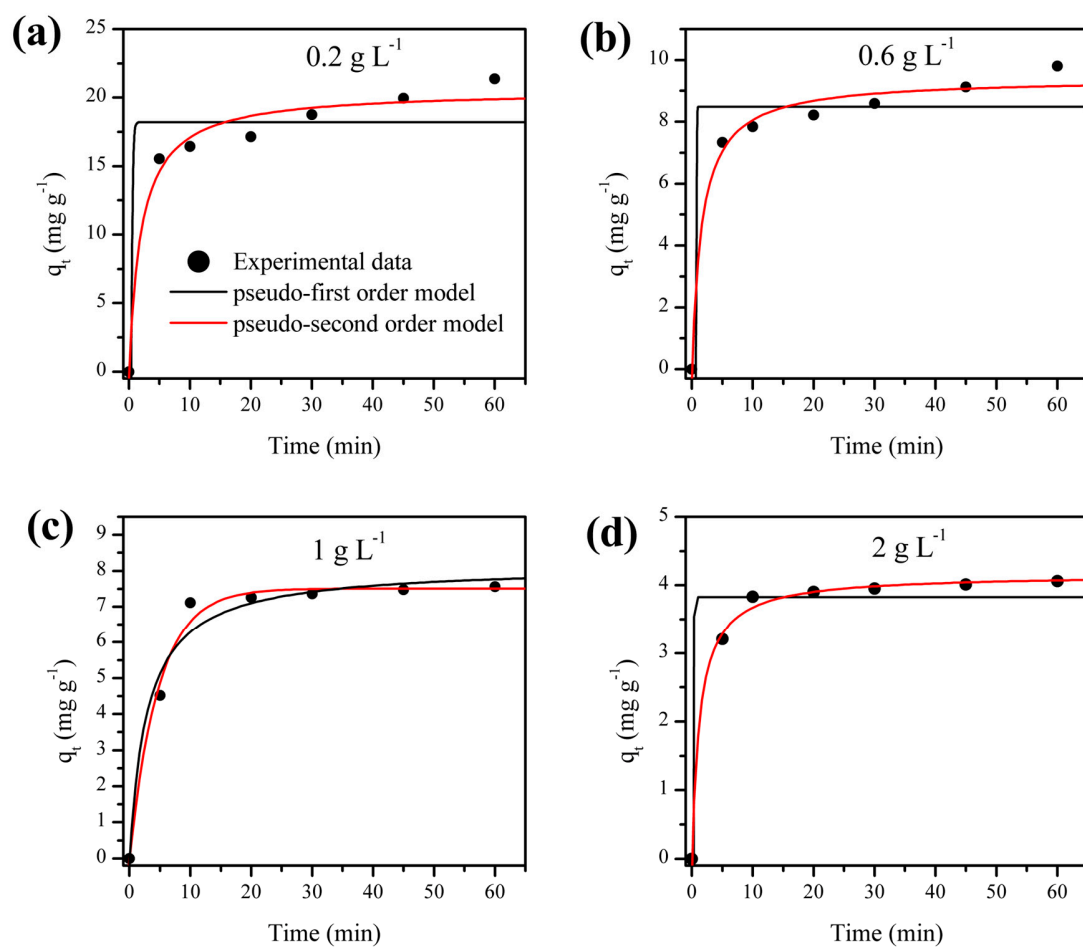


Figure S13. Kinetics of pseudo-first order model and pseudo-second order model for CR removal in distilled water using MMT as an adsorbent. (a) 0.2 g L⁻¹; (b) 0.6 g L⁻¹; (c) 1 g L⁻¹; (d) 2 g L⁻¹. Conditions: dye concentration 1.23×10^{-2} mmol L⁻¹ (8.57 mg L⁻¹), particle size <200 μ m, pH: 6.5, temperature 25°C, stirring rate 200 rpm, time 60 min.

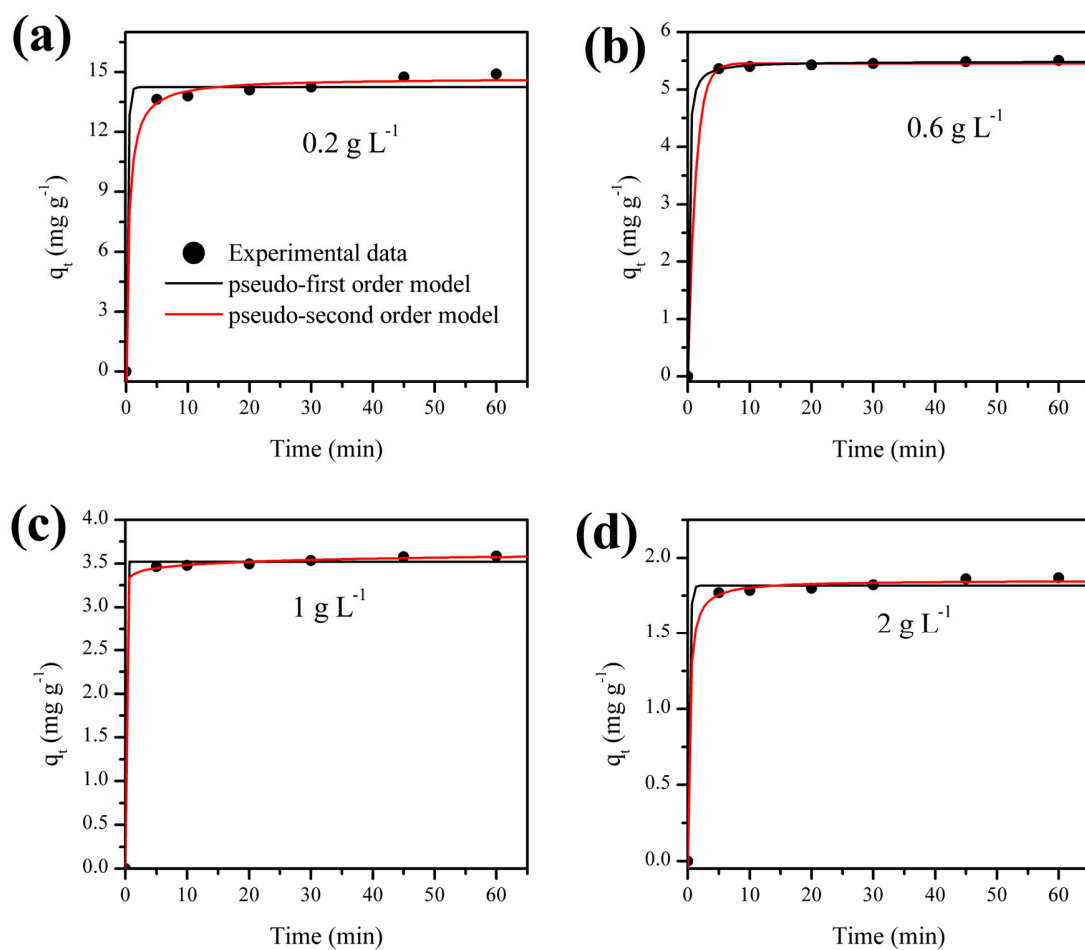


Figure S14. Kinetics of pseudo-first order model and pseudo second-order model for MB removal in distilled water using MMT as an adsorbent. (a) 0.2 g L⁻¹; (b) 0.6 g L⁻¹; (c) 1 g L⁻¹; (d) 2 g L⁻¹. Conditions: dye concentration 1.23×10^{-2} mmol L⁻¹ (3.93 mg L⁻¹), particle size <200 μ m, pH: 5.6, temperature 25°C, stirring rate 200 rpm, time 60 min.

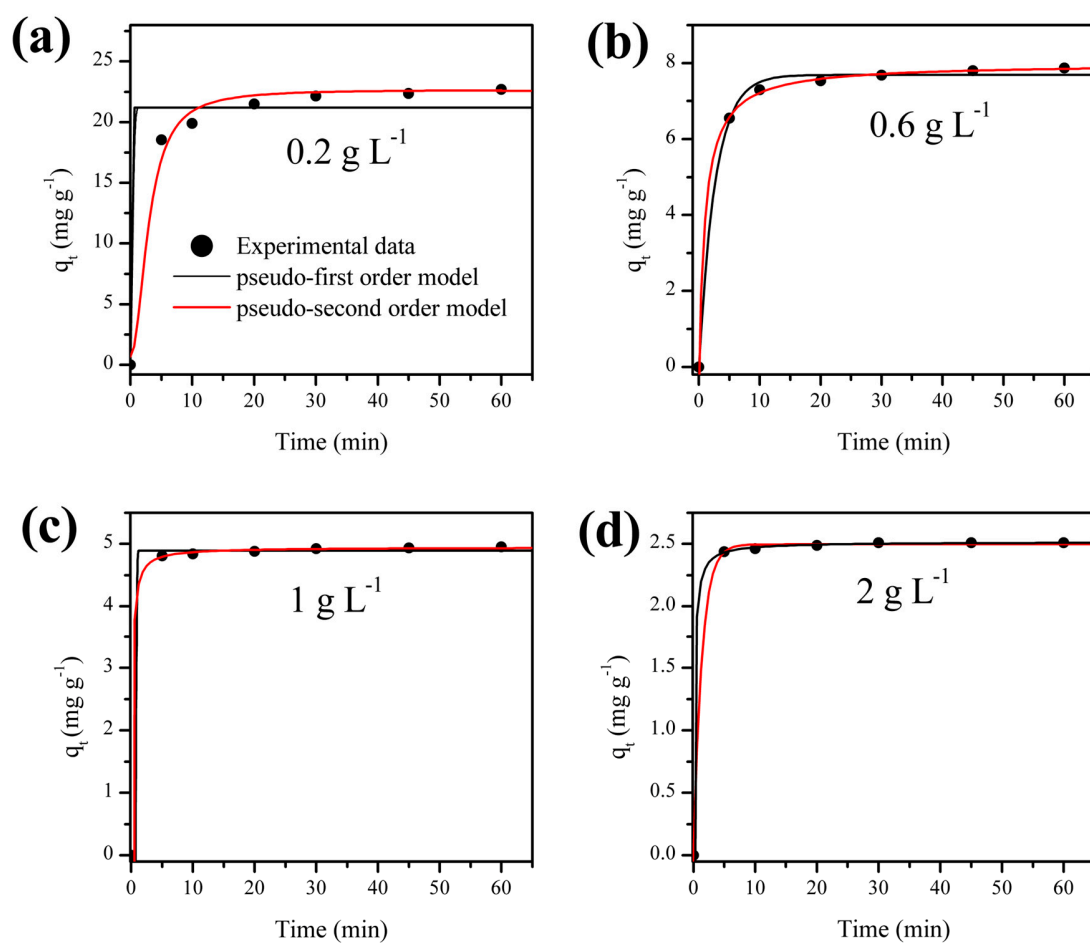


Figure S15. Kinetics of pseudo-first order model and pseudo-second order model for CV removal in distilled water using MMT as an adsorbent. (a) 0.2 g L⁻¹; (b) 0.6 g L⁻¹; (c) 1 g L⁻¹; (d) 2 g L⁻¹. Conditions: dye concentration 1.23×10^{-2} mmol L⁻¹ (4.85 mg L⁻¹), particle size <200 μ m, pH: 7.3, temperature 25°C, stirring rate 200 rpm, time 60 min.