

# Modelling and Cost Estimation for Conversion of Green Methanol to Renewable Liquid Transport Fuels via Olefin Oligomerisation

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The Supplementary Materials includes the input specifications and the output values of the Aspen Plus simulation model. The components selected for the system are first shown in Table S1. Next, reactions considered in each reactor are shown in Table S2-Table S5. Equipment operations are specified in Table S6. The results of the model are shown in Table S7 and Table S8 of which the former lists the purchased equipment costs calculated by APEA, and the latter shows the complete stream table.

## 1. Component specifications

**Table S1.** Component specifications of the MTO-MOGD model.

Component ID	Type	Component name	Alias
Methanol	Conventional	METHANOL	CH4O
DME	Conventional	DIMETHYL-ETHER	C2H6O-1
Water	Conventional	WATER	H2O
Methane	Conventional	METHANE	CH4
Ethane	Conventional	ETHANE	C2H6
Ethylene	Conventional	ETHYLENE	C2H4
Propane	Conventional	PROPANE	C3H8
Propylene	Conventional	PROPYLENE	C3H6-2
n-Butane	Conventional	N-BUTANE	C4H10-1
i-Butane	Conventional	ISOBUTANE	C4H10-2
Butene	Conventional	1-BUTENE	C4H8-1
n-Pentane	Conventional	N-PENTANE	C5H12-1
i-Pentane	Conventional	2-METHYL-BUTANE	C5H12-2
Cyclopentane	Conventional	CYCLOPENTANE	C5H10-1
Pentene	Conventional	1-PENTENE	C5H10-2
n-Hexane	Conventional	N-HEXANE	C6H14-1
i-Hexane	Conventional	2-METHYL-PENTANE	C6H14-2
Cyclohexane	Conventional	CYCLOHEXANE	C6H12-1
Hexene	Conventional	1-HEXENE	C6H12-3
n-Octane	Conventional	N-OCTANE	C8H18-1
i-Octane	Conventional	2,2,4-TRIMETHYLPENTANE	C8H18-13
Octene	Conventional	1-OCTENE	C8H16-16
Benzene	Conventional	BENZENE	C6H6
Durene	Conventional	1,2,4,5-TETRAMETHYLBENZENE	C10H14-9

Prehnitene	Conventional	1,2,3,4-TETRAMETHYL-BENZENE	C10H14-E7
i-Durene	Conventional	1,2,3,5-TETRAMETHYL-BENZENE	C10H14-E6
n-Dodecane	Conventional	N-DODECANE	C12H26
i-Dodecane	Conventional	2-METHYLUNDECANE	C12H26-N9
Dodecene	Conventional	1-DODECENE	C12H24-2
n-Hexadecane	Conventional	N-HEXADECANE	C16H34
i-Hexadecane	Conventional	2-METHYLPENTADECANE	C16H34-N1
Hexadecene	Conventional	1-HEXADECENE	C16H32-2
n-Octadecane	Conventional	N-OCTADECANE	C18H38
i-Octadecane	Conventional	16-METHYLHEPTADECANE	C18H38-N1
Octadecene	Conventional	1-OCTADECENE	C18H36-1
n-Eicosane	Conventional	N-EICOSANE	C20H42
i-Eicosane	Conventional	18-METHYLNONADECANE	C20H42-N3
Eicosene	Conventional	1-EICOSENE	C20H40-D1
Hydrogen	Conventional	HYDROGEN	H2

## 2. Reaction specifications

**Table S2.** Reaction specifications of the MTO reactor R-101, and standard reaction enthalpies calculated from literature values [29] and estimated by Aspen Plus.

Reaction No.	Specification type	Fractional conversion	Fractional conversion of component	Stoichiometry	$\Delta H_r^0$ , kJ/mol Calculated	$\Delta H_r^0$ , kJ/mol Aspen
1	Fractional conversion	0.99	Methanol	2 Methanol $\rightarrow$ DME + Water	-15.9	-23.9
2	Fractional conversion	0.30	DME	DME $\rightarrow$ Ethylene + Water	-5.3	-5.2
3	Fractional conversion	1	DME	3 DME $\rightarrow$ 2 Propylene + 3 Water	-132.4	-132.9
4	Fractional conversion	0.80	Ethylene	2 Ethylene $\rightarrow$ Butene	-105.6	-105.6
5	Fractional conversion	0.45	Propylene	2 Propylene $\rightarrow$ Hexene	-82.8	-82.3
6	Fractional conversion	0.45	Ethylene	Ethylene + Propylene $\rightarrow$ Pentene	-95.8	-94.5
7	Fractional conversion	0.50	Hexene	Hexene $\rightarrow$ Benzene + 3 Hydrogen	124.9	124.8
8	Fractional conversion	1	Methanol	Benzene + 4 Methanol $\rightarrow$ Durene + 4 Water	-277.3	-293.5
9	Fractional conversion	0.15	Butene	2 Butene + 2 Hydrogen $\rightarrow$ n-Butane + i-Butane	-258.5	-260.0
10	Fractional conversion	0.075	Propylene	Propylene + Hydrogen $\rightarrow$ Propane	-125.1	-125.0
11	Fractional conversion	0.15	Ethylene	Ethylene + Hydrogen $\rightarrow$ Ethane	-136.5	-136.4
12	Fractional conversion	0.50	Ethylene	Ethylene + 2 Hydrogen $\rightarrow$ 2 Methane	-202.2	-201.6
13	Fractional conversion	1	Hydrogen	Benzene + 3 Hydrogen $\rightarrow$ Cyclohexane	-207.5	-206.4

14	Fractional conversion	0.50	Pentene	Pentene --> Cyclopentane	-53.5	-55.4
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**Table S3.** Reaction specifications of the hydroisomerisation reactor R-102.

Reaction No.	Specification type	Molar extent	Units	Fractional conversion	Fractional conversion of component	Stoichiometry
1	Fractional conversion			0.49	Durene	2 Durene --> Prehnitene + i-Durene
2	Molar extent	0.015	kmol/h			Durene + 5 Hydrogen --> 2 n-Pentane

**Table S4.** Reaction specifications of the MOGD reactor R-103, and standard reaction enthalpies calculated from literature values [29, 30] and estimated by Aspen Plus.

Reaction No.	Specification type	Fractional conversion	Fractional conversion of component	Stoichiometry	$\Delta H_r^\theta$ , kJ/mol	Calculated	Aspen
1	Fractional conversion	1	Ethylene	2 Ethylene --> Butene	-105.6	-105.6	
2	Fractional conversion	1	Propylene	2 Propylene --> Hexene	-82.8	-82.3	
3	Fractional conversion	1	Butene	2 Butene --> Octene	-81.7	-81.3	
4	Fractional conversion	0.85	Hexene	2 Hexene --> Dodecene	-81.4	-83.3	
5	Fractional conversion	0.80	Octene	2 Octene --> Hexadecene	-82.5	-88.7	
6	Fractional conversion	0.99	Hexene	Hexene + Dodecene --> Octadecene	-82.0	-85.6	
7	Fractional conversion	0.99	Octene	Octene + Dodecene --> Eicosene	-82.4	-86.2	

**Table S5.** Reaction specifications of the hydrogenation reactor R-104.

Reaction No.	Specification type	Fractional conversion	Fractional conversion of component	Stoichiometry
1	Fractional conversion	0.90	Dodecene	2 Dodecene + 2 Hydrogen --> n-Dodecane + i-Dodecane
2	Fractional conversion	0.90	Hexadecene	2 Hexadecene + 2 Hydrogen --> n-Hexadecane + i-Hexadecane
3	Fractional conversion	0.90	Octadecene	2 Octadecene + 2 Hydrogen --> n-Octadecane + i-Octadecane
4	Fractional conversion	0.90	Eicosene	2 Eicosene + 2 Hydrogen --> n-Eicosane + i-Eicosane

### 3. Equipment specifications

**Table S6.** Equipment specifications of the MTO-MOGD model. Abbreviations used in the table: I, Isentropic; M, Mechanical; RR, Reflux ratio; and DFR, Distillate to feed ratio.

Name	Type	Specification	T, °C	P, bar	Duty, kW	No. of stages	Efficiency	Calculation type	Molar RR	Molar DFR	Condenser type	Reboiler type	Pinch, °C	Split fraction	Utility
C-101	Compr	Compressor		15		1	0.80 (I) 0.90 (M)	Isentropic							Electricity
C-102	MCompr	Multi-stage compressor		17		3	0.80 (I) 0.90 (M)	Isentropic							Electricity Cooling water
C-103	Compr	Compressor		16		1	0.80 (I) 0.90 (M)	Isentropic							Electricity
C-104	MCompr	Multi-stage compressor		40		4	0.80 (I) 0.90 (M)	Isentropic							Electricity Cooling water
C-105	Compr	Compressor		40		1	0.80 (I) 0.90 (M)	Isentropic							Electricity
D-101	Decanter	Decanter		2	0										
DIST1	RadFrac	Distillation column		15		4		Equilibrium	1.26	0.13	Partial-Vapor	Kettle			Refrigeration
DIST2	RadFrac	Distillation column		10		5		Equilibrium	0.012	0.99	Total	Kettle			LP steam Cooling water Fired heat
DIST3	RadFrac	Distillation column		5		4		Equilibrium	0.26	0.45	Partial-Vapor	Kettle			Cooling water HP steam
DIST4	RadFrac	Distillation column		1		6		Equilibrium	0.36	0.54	Partial-Vapor	Kettle			LP steam generation Fired heat
DIST5	RadFrac	Distillation column		5		7		Equilibrium	2.31	0.30	Partial-Vapor	Kettle			Refrigeration

							LP steam
E-101	HeatX	Heat exchanger	430			5	
			Cold stream outlet				
E-102	Heater	Heater	450	2			Fired heat
E-103	HeatX	Heat exchanger	40			5	
			Cold stream outlet				
E-104	Heater	Cooler	30	2			Cooling water
E-105	HeatX	Heat exchanger	5			3	
			Hot/cold temperature approach				
E-106	Heater	Cooler	50	15			Cooling water
E-107	HeatX	Heat exchanger	5			3	
			Hot/cold temperature approach				
E-108	Heater	Heater	345	17			Fired heat
E-109	Heater	Cooler	135	16			LP steam generation
E-110	Heater	Cooler	30	16			Cooling water
E-111	Heater	Cooler	10	16			Refrigeration
E-112	Heater	Cooler	30	1			Cooling water
E-113	Heater	Heater	345	17			Fired heat
E-114	Heater	Heater	200	40			HP steam
E-115	Heater	Heater	300	40			Fired heat

E-116	Heater	Cooler	135	0		LP steam generation
E-117	Heater	Cooler	30	0		Cooling water
E-118	Heater	Cooler	135	1		LP steam generation
E-119	Heater	Cooler	30	1		Cooling water
E-120	Heater	Cooler	30	1		Cooling water
E-121	Heater	Cooler	50	5		Cooling water
E-122	Heater	Heater	300	40		Fired heat
FLASH1	Flash2	Flash column		2	0	
FLASH2	Flash2	Flash column		14.4	0	
FLASH3	Flash2	Flash column		36	0	
FLASH4	Flash2	Flash column		1	0	
P-101	Pump	Pump		2		Electricity
P-102	Pump	Pump		15		Electricity
P-103	Pump	Pump		17		Electricity
P-104	Pump	Pump		40		Electricity
P-105	Pump	Pump		40		Electricity
R-101	RStoic	Stoichiometric reactor	450	2	Vapor-Only	HP steam generation
R-102	RStoic	Stoichiometric reactor	345	16	Vapor-Liquid	Fired heat
R-103	RStoic	Stoichiometric reactor	200	39	Vapor-Liquid	LP steam generation
R-104	RStoic	Stoichiometric reactor	300	40	Vapor-Liquid	HP steam generation
V-101	Mixer	Mixing valve		0		
V-102	Mixer	Mixing valve		0		
V-103	Valve	Pressure relief valve		1	Adiabatic flash for	

				specified outlet pressure	
V-104	FSplit	Split valve			0.05
V-105	Mixer	Mixing valve	0		
V-106	Valve	Pressure relief valve	5	Adiabatic flash for specified outlet pressure	
V-107	Valve	Pressure relief valve	1	Adiabatic flash for specified outlet pressure	
V-108	Mixer	Mixing valve	0		

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**Table S7.** Equipment sizes and costs. D refers to a vessel diameter and H to height.

Equipment	Aspen model	Size		Number of items	Material factor (f <sub>m</sub> )	Equipment cost (APEA), \$ <sub>2018</sub>	Purchased cost, € <sub>2020</sub>
C-101	Compr	49	kW	1	1	782900	820730
C-102	MCompr	0.33	kW	1	1.3	1237600	1297401
C-103	Compr	0.03	kW	1	1.3	675200	707826
C-104	MCompr	15	kW	1	1.3	1498600	1571012
C-105	Compr	0.17	kW	1	1.3	741400	777224
D-101	Decanter	1.80	m <sup>3</sup>	1	1	15200	15934
DIST1-cond	RadFrac	3.95	m <sup>2</sup>	1	1	10200	10693
DIST1-cond acc		1.80	m <sup>3</sup>	1	1	14300	14991
DIST1-reb		0.57	m <sup>2</sup>	1	1	13200	13838
DIST1-reflux pump		0.37	m <sup>3</sup> /h	2	1	9600	10064
DIST1-tower		D=0.46, H=5.49	m	1	1	19400	20337
DIST2-cond	RadFrac	4.39	m <sup>2</sup>	1	1	10300	10798
DIST2-cond acc		1.80	m <sup>3</sup>	1	1	13800	14467
DIST2-reb		12	m <sup>2</sup>	1	1	18400	19289
DIST2-reflux pump		2.27	m <sup>3</sup> /h	2	1	9600	10064
DIST2-tower		D=0.46, H=6.71	m	1	1	22800	23902
DIST3-cond	RadFrac	0.26	m <sup>2</sup>	1	1	8400	8806
DIST3-cond acc		1.80	m <sup>3</sup>	1	1	13300	13943
DIST3-reb		1.23	m <sup>2</sup>	1	1	13400	14047
DIST3-reflux pump		0.16	m <sup>3</sup> /h	2	1	9600	10064
DIST3-tower		D=0.46, H=5.49	m	1	1	19300	20233
DIST4-cond	RadFrac	2.48	m <sup>2</sup>	1	1	9100	9540
DIST4-cond acc		1.80	m <sup>3</sup>	1	1	16500	17297
DIST4-reb		20	m <sup>2</sup>	1	1	20000	20966
DIST4-reflux pump		0.31	m <sup>3</sup> /h	2	1	9600	10064

DIST4-tower		D=0.61, H=7.32	m	1	1	36600	38369
DIST5-cond	RadFrac	3.08	m <sup>2</sup>	1	1	9200	9645
DIST5-cond acc		1.80	m <sup>3</sup>	1	1	13300	13943
DIST5-reb		0.68	m <sup>2</sup>	1	1	13200	13838
DIST5-reflux pump		0.30	m <sup>3</sup> /h	2	1	9600	10064
DIST5-tower		D=0.46, H=8.53	m	1	1	27300	28619
E-101	HeatX	69	m <sup>2</sup>	1	1.3	21700	22749
E-102	Heater	16	m <sup>2</sup>	1	1.3	14400	15096
E-103	HeatX	0.52	m <sup>2</sup>	1	1	8400	8806
E-104	Heater	13	m <sup>2</sup>	1	1	11200	11741
E-105	HeatX	1.23	m <sup>2</sup>	1	1	9100	9540
E-106	Heater	3.06	m <sup>2</sup>	1	1	9200	9645
E-107	HeatX	0.49	m <sup>2</sup>	1	1.3	8500	8911
E-108	Heater	0.49	m <sup>2</sup>	1	1.3	8900	9330
E-109	Heater	1.06	m <sup>2</sup>	1	1.3	9100	9540
E-110	Heater	0.49	m <sup>2</sup>	1	1.3	8400	8806
E-111	Heater	0.49	m <sup>2</sup>	1	1.3	8400	8806
E-112	Heater	0.61	m <sup>2</sup>	1	1	8400	8806
E-113	Heater	0.49	m <sup>2</sup>	1	1	8900	9330
E-114	Heater	2.08	m <sup>2</sup>	1	1	9400	9854
E-115	Heater	5.46	m <sup>2</sup>	1	1	13100	13733
E-116	Heater	24	m <sup>2</sup>	1	1.3	17800	18660
E-117	Heater	2.18	m <sup>2</sup>	1	1.3	9300	9749
E-118	Heater	15	m <sup>2</sup>	1	1	11500	12056
E-119	Heater	1.70	m <sup>2</sup>	1	1	8900	9330
E-120	Heater	1.06	m <sup>2</sup>	1	1	8900	9330
E-121	Heater	0.84	m <sup>2</sup>	1	1	8900	9330
E-122	Heater	0.64	m <sup>2</sup>	1	1.3	9000	9435
FLASH1	Flash2	2.40	m <sup>3</sup>	1	1	16400	17192

FLASH2	Flash2	2.40	m <sup>3</sup>	1	1.3	17800	18660
FLASH3	Flash2	2.40	m <sup>3</sup>	1	1.3	22300	23378
FLASH4	Flash2	2.40	m <sup>3</sup>	1	1.3	16900	17717
P-101	Pump	4.16	m <sup>3</sup> /h	1	1.3	4300	4508
P-102	Pump	1E-07	m <sup>3</sup> /h	1	1	16300	17088
P-103	Pump	0.05	m <sup>3</sup> /h	1	1	16300	17088
P-104	Pump	2.25	m <sup>3</sup> /h	1	1	57100	59859
P-105	Pump	1.70	m <sup>3</sup> /h	1	1	59600	62480
R-101	RStoic	5.56	m <sup>3</sup>	2	1.3	250400	262499
R-102	RStoic	0.05	m <sup>3</sup>	2	1.3	44600	46755
R-103	RStoic	4.26	m <sup>3</sup>	2	1.3	229800	240904
R-104	RStoic	4.47	m <sup>3</sup>	2	1.3	198400	207987
V-101	Mixer						
V-102	Mixer						
V-103	Valve						
V-104	FSplit						
V-105	Mixer						
V-106	Valve						
V-107	Valve						
V-108	Mixer						
Total						6502500	6816701
Total, 10 <sup>-6</sup>						<b>6.50</b>	<b>6.82</b>

#### 4. Stream table

**Table S8.** Stream table of the MTO-MOGD model.

<b>Stream</b>		<b>1</b>	<b>2</b>	<b>3</b>	<b>4</b>	<b>5</b>	<b>6</b>	<b>7</b>	<b>8</b>	<b>9</b>	<b>10</b>	<b>11</b>	<b>12</b>	<b>13</b>	<b>14</b>	<b>15</b>	<b>16</b>	<b>17</b>	<b>18</b>	<b>19</b>	<b>20</b>	
Temperature	C	25	25	430	450	450	85	82	30	30	30	33	30	117	125	103	50	66	290	292	315	
Pressure	bar	1	2	2	2	2	2	2	2	2	2	15	2	15	15	15	15	15	15	10	17	17
Molar Vapor Fraction		0	0	1	1	1	0	0	0	0	0	0	1	1	1	1	0	0	0	0	0	
Molar Liquid Fraction		1	1	0	0	0	1	1	1	1	1	1	0	0	0	0	1	1	1	1	1	
<b>Mole Flows</b>	<b>kmol/h</b>	<b>94</b>	<b>94</b>	<b>94</b>	<b>94</b>	<b>118</b>	<b>118</b>	<b>118</b>	<b>118</b>	<b>93</b>	<b>0</b>	<b>0</b>	<b>25</b>	<b>25</b>	<b>25</b>	<b>25</b>	<b>25</b>	<b>22</b>	<b>0</b>	<b>0</b>	<b>0</b>	
Methanol	kmol/h	94	94	94	94	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
DME	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
Water	kmol/h	0	0	0	0	94	94	94	94	93	0	0	0	0	0	0	0	0	0	0	0	
Methane	kmol/h	0	0	0	0	1	1	1	1	0	0	0	1	1	1	1	1	0	0	0	0	
Ethane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
Ethylene	kmol/h	0	0	0	0	1	1	1	1	0	0	0	1	1	1	1	1	0	0	0	0	
Propane	kmol/h	0	0	0	0	1	1	1	1	0	0	0	1	1	1	1	1	1	0	0	0	
Propylene	kmol/h	0	0	0	0	10	10	10	10	0	0	0	10	10	10	10	10	9	0	0	0	
n-Butane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
i-Butane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
Butene	kmol/h	0	0	0	0	5	5	5	5	0	0	0	5	5	5	5	5	5	0	0	0	
n-Pentane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
i-Pentane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
Cyclopentane	kmol/h	0	0	0	0	1	1	1	1	0	0	0	1	1	1	1	1	1	0	0	0	
Pentene	kmol/h	0	0	0	0	1	1	1	1	0	0	0	1	1	1	1	1	1	0	0	0	
n-Hexane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
i-Hexane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
Cyclohexane	kmol/h	0	0	0	0	1	1	1	1	0	0	0	1	1	1	1	1	1	0	0	0	
Hexene	kmol/h	0	0	0	0	2	2	2	2	0	0	0	2	2	2	2	2	2	0	0	0	

n-Octane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
i-Octane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
Octene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
Benzene	kmol/h	0	0	0	0	1	1	1	1	0	0	0	1	1	1	1	1	0	
Durene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
Prehnitene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
Isodurene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
n-Dodecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
i-Dodecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
Dodecene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
n-Hexadecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
i-Hexadecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
Hexadecene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
n-Octadecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
i-Octadecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
Octadecene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
n-Eicosane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
i-Eicosane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
Eicosene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
Hydrogen	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
<b>Mass Flows</b>	<b>kg/h</b>	<b>3000</b>	<b>1679</b>	<b>0</b>	<b>0</b>	<b>1321</b>	<b>1321</b>	<b>1321</b>	<b>1321</b>	<b>1223</b>	<b>28</b>	<b>28</b>							
Methanol	kg/h	3000	3000	3000	3000	0	0	0	0	0	0	0	0	0	0	0	0	0	0
DME	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Water	kg/h	0	0	0	0	1687	1687	1687	1687	1679	0	0	8	8	8	8	8	0	0
Methane	kg/h	0	0	0	0	21	21	21	21	0	0	0	21	21	21	21	1	0	0
Ethane	kg/h	0	0	0	0	7	7	7	7	0	0	0	7	7	7	7	4	0	0
Ethylene	kg/h	0	0	0	0	18	18	18	18	0	0	0	18	18	18	18	7	0	0
Propane	kg/h	0	0	0	0	35	35	35	35	0	0	0	35	35	35	35	31	0	0
Propylene	kg/h	0	0	0	0	414	414	414	414	0	0	0	414	414	414	414	362	0	0
n-Butane	kg/h	0	0	0	0	24	24	24	24	0	0	0	24	24	24	24	24	0	0
i-Butane	kg/h	0	0	0	0	24	24	24	24	0	0	0	24	24	24	24	24	0	0

Butene	kg/h	0	0	0	0	265	265	265	265	0	0	0	265	265	265	265	265	265	260	0	0	0	
n-Pentane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Pentane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Cyclopentane	kg/h	0	0	0	0	44	44	44	44	0	0	0	44	44	44	44	44	44	44	0	0	0	0
Pentene	kg/h	0	0	0	0	44	44	44	44	0	0	0	44	44	44	44	44	44	44	0	0	0	0
n-Hexane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Hexane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Cyclohexane	kg/h	0	0	0	0	116	116	116	116	0	0	0	116	116	116	116	116	116	116	1	1	1	1
Hexene	kg/h	0	0	0	0	205	205	205	205	0	0	0	205	205	205	205	205	205	205	0	0	0	0
n-Octane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Octane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Octene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Benzene	kg/h	0	0	0	0	64	64	64	64	0	0	0	64	64	64	64	64	64	64	0	0	0	0
Durene	kg/h	0	0	0	0	31	31	31	31	0	0	0	31	31	31	31	31	31	31	26	26	26	26
Prehnitene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Isodurene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
n-Dodecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Dodecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Dodecene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
n-Hexadecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Hexadecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Hexadecene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
n-Octadecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Octadecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Octadecene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
n-Eicosane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Eicosane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Eicosene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Hydrogen	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Volume Flow	m <sup>3</sup> /h	4	4	2730	2809	3543	484	463	302	2	0	0	301	44	45	35	8	2	0	0	0	0	0

**Table S8.** (cont.).

<b>Stream</b>		<b>21</b>	<b>22</b>	<b>23</b>	<b>24</b>	<b>25</b>	<b>26</b>	<b>27</b>	<b>28</b>	<b>29</b>	<b>30</b>	<b>31</b>	<b>32</b>	<b>33</b>	<b>34</b>	<b>35</b>	<b>36</b>	<b>37</b>	<b>38</b>	<b>39</b>	<b>40</b>
Temperature	C	345	345	320	135	30	10	10	80	41	30	10	21	85	345	44	51	98	200	200	
Pressure	bar	17	16	16	16	16	16	14	5	1	1	14	14	16	16	17	10	40	40	40	39
Molar Vapor Fraction		1	1	1	1	1	1	0	0	0	0	1	1	1	1	1	0	0	0	1	0
Molar Liquid Fraction		0	0	0	0	0	0	1	1	1	1	0	0	0	0	0	1	1	1	0	1
<b>Mole Flows</b>	<b>kmol/h</b>	<b>0</b>	<b>1</b>	<b>1</b>	<b>1</b>	<b>1</b>	<b>1</b>	<b>0</b>	<b>3</b>	<b>3</b>	<b>3</b>	<b>0</b>	<b>0</b>	<b>0</b>	<b>0</b>	<b>0</b>	<b>21</b>	<b>21</b>	<b>21</b>	<b>21</b>	<b>9</b>
Methanol	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
DME	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Water	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Methane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Ethane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Ethylene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Propane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	1	1	1	1	1
Propylene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	9	9	9	9	0
n-Butane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Butane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Butene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	5	5	5	5	0
n-Pentane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Pentane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Cyclopentane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	1	1	1	1	1
Pentene	kmol/h	0	0	0	0	0	0	0	1	1	1	0	0	0	0	0	1	1	1	1	1
n-Hexane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Hexane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Cyclohexane	kmol/h	0	0	0	0	0	0	0	1	1	1	0	0	0	0	0	1	1	1	1	1
Hexene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	2	2	2	2	0
n-Octane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Octane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Octene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0

Benzene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	1	1	1	1	1
Durene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Prehnitene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Isodurene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
n-Dodecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Dodecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Dodecene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	1
n-Hexadecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Hexadecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Hexadecene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	1
n-Octadecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Octadecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Octadecene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	1
n-Eicosane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Eicosane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Eicosene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Hydrogen	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
<b>Mass Flows</b>	<b>kg/h</b>	<b>28</b>	<b>29</b>	<b>29</b>	<b>29</b>	<b>29</b>	<b>28</b>	<b>224</b>	<b>224</b>	<b>224</b>	<b>1</b>	<b>1</b>	<b>1</b>	<b>1</b>	<b>1</b>	<b>1195</b>	<b>1195</b>	<b>1195</b>	<b>1195</b>	<b>1195</b>
Methanol	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
DME	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Water	kg/h	0	0	0	0	0	0	0	7	7	7	0	0	0	0	8	8	8	8	8
Methane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	1	1	1	1	1
Ethane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	4	4	4	4	4
Ethylene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	7	7	7	7	0
Propane	kg/h	0	0	0	0	0	0	0	2	2	2	0	0	0	0	31	31	31	31	31
Propylene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	362	362	362	362	0
n-Butane	kg/h	0	0	0	0	0	0	0	14	14	14	0	0	0	0	24	24	24	24	24
i-Butane	kg/h	0	0	0	0	0	0	0	7	7	7	0	0	0	0	24	24	24	24	24
Butene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	260	260	260	260	0
n-Pentane	kg/h	0	2	2	2	2	2	2	2	2	2	0	0	0	0	0	0	0	0	0
i-Pentane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0

Cyclopentane	kg/h	0	0	0	0	0	0	0	33	33	33	0	0	0	0	0	44	44	44	44	44
Pentene	kg/h	0	0	0	0	0	0	0	38	38	38	0	0	0	0	0	44	44	44	44	44
n-Hexane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Hexane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Cyclohexane	kg/h	1	1	1	1	1	1	59	59	59	0	0	0	0	0	0	115	115	115	115	115
Hexene	kg/h	0	0	0	0	0	0	0	1	1	1	0	0	0	0	0	204	204	204	204	1
n-Octane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Octane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Octene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	1
Benzene	kg/h	0	0	0	0	0	0	36	36	36	0	0	0	0	0	0	64	64	64	64	64
Durene	kg/h	26	11	11	11	11	11	11	11	11	11	0	0	0	0	0	5	5	5	5	5
Prehnitene	kg/h	0	6	6	6	6	6	6	6	6	6	0	0	0	0	0	0	0	0	0	0
Isodurene	kg/h	0	6	6	6	6	6	6	6	6	6	0	0	0	0	0	0	0	0	0	0
n-Dodecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Dodecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Dodecene	kg/h	0	0	0	0	0	0	0	1	1	1	0	0	0	0	0	0	0	0	0	234
n-Hexadecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Hexadecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Hexadecene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	213
n-Octadecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Octadecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Octadecene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	252
n-Eicosane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Eicosane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Eicosene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	132
Hydrogen	kg/h	0	1	1	1	1	1	0	0	0	0	1	1	1	1	1	0	0	0	0	0
Volume Flow	m <sup>3</sup> /h	0	2	2	1	1	1	0	0	19	2	1	1	0	1	1	2	2	2	15	2

**Table S8.** (cont.).

<b>Stream</b>		<b>41</b>	<b>42</b>	<b>43</b>	<b>44</b>	<b>45</b>	<b>46</b>	<b>47</b>	<b>48</b>	<b>49</b>	<b>50</b>	<b>51</b>	<b>52</b>	<b>53</b>	<b>54</b>	<b>55</b>	<b>56</b>	<b>57</b>	<b>58</b>	<b>59</b>	<b>60</b>
Temperature	C	177	216	222	300	300	135	30	30	32	32	299	135	30	196	30	32	30	42	112	300
Pressure	bar	5	5	40	40	40	40	40	36	1	1	1	1	1	1	1	1	36	40	40	40
Molar Vapor Fraction		0	0	0	0	0	0	0	0	0	0	0	0	0	1	0	1	1	1	1	1
Molar Liquid Fraction		1	1	1	1	1	1	1	1	1	1	1	1	1	0	1	0	0	0	0	0
<b>Mole Flows</b>	<b>kmol/h</b>	<b>9</b>	<b>5</b>	<b>5</b>	<b>5</b>	<b>7</b>	<b>7</b>	<b>7</b>	<b>5</b>	<b>5</b>	<b>5</b>	<b>2</b>	<b>2</b>	<b>3</b>	<b>3</b>	<b>0</b>	<b>2</b>	<b>2</b>	<b>5</b>	<b>5</b>	<b>5</b>
Methanol	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
DME	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Water	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Methane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Ethane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Ethylene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Propane	kmol/h	1	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Propylene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
n-Butane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Butane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Butene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
n-Pentane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Pentane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Cyclopentane	kmol/h	1	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Pentene	kmol/h	1	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
n-Hexane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Hexane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Cyclohexane	kmol/h	1	1	1	1	1	1	1	1	1	1	0	0	0	1	1	0	0	0	0	0
Hexene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
n-Octane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Octane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Octene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0



Cyclopentane	kg/h	44	11	11	11	11	11	11	11	10	0	0	0	10	10	0	0	0	0	0
Pentene	kg/h	44	6	6	6	6	6	6	6	0	0	0	0	6	6	0	0	0	0	0
n-Hexane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Hexane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Cyclohexane	kg/h	115	57	57	57	58	58	58	57	57	0	0	0	57	57	0	0	0	0	0
Hexene	kg/h	1	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
n-Octane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
i-Octane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Octene	kg/h	1	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Benzene	kg/h	64	28	28	28	29	29	29	28	28	0	0	0	28	28	0	0	0	0	0
Durene	kg/h	5	5	5	5	5	5	5	5	5	0	0	0	5	5	0	0	0	0	0
Prehnitene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Isodurene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
n-Dodecane	kg/h	0	0	0	0	106	106	106	106	106	3	3	3	103	103	0	0	0	0	0
i-Dodecane	kg/h	0	0	0	0	106	106	106	106	106	2	2	2	104	104	0	0	0	0	0
Dodecene	kg/h	234	233	233	233	23	23	23	23	23	0	0	0	23	23	0	0	0	0	0
n-Hexadecane	kg/h	0	0	0	0	97	97	97	97	97	92	92	92	5	5	0	0	0	0	0
i-Hexadecane	kg/h	0	0	0	0	97	97	97	97	97	89	89	89	8	8	0	0	0	0	0
Hexadecene	kg/h	213	213	213	213	21	21	21	21	21	20	20	20	1	1	0	0	0	0	0
n-Octadecane	kg/h	0	0	0	0	114	114	114	114	114	114	114	114	0	0	0	0	0	0	0
i-Octadecane	kg/h	0	0	0	0	114	114	114	114	114	114	114	114	1	1	0	0	0	0	0
Octadecene	kg/h	252	252	252	252	25	25	25	25	25	25	25	25	0	0	0	0	0	0	0
n-Eicosane	kg/h	0	0	0	0	60	60	60	60	60	60	60	60	0	0	0	0	0	0	0
i-Eicosane	kg/h	0	0	0	0	60	60	60	60	60	60	60	60	0	0	0	0	0	0	0
Eicosene	kg/h	132	132	132	132	13	13	13	13	13	13	13	13	0	0	0	0	0	0	0
Hydrogen	kg/h	0	0	0	0	4	4	4	0	0	0	0	0	0	0	3	3	10	10	6
Volume Flow	m <sup>3</sup> /h	31	2	2	2	4	3	2	1	5	1	1	1	105	1	4	1	1	4	6

**Table S8.** (cont.).

<b>Stream</b>		<b>61</b>	<b>62</b>	<b>63</b>	<b>64</b>	<b>65</b>	<b>66</b>	<b>67</b>	<b>68</b>	<b>69</b>	<b>70</b>	<b>71</b>	<b>72</b>
Temperature	C	109	50	88	25	309	25	145	30	40	12	10	20
Pressure	bar	5	5	5	1	17	1	40	2	2	15	14	5
Molar Vapor													
Fraction		1	0	0	1	1	1	1	0	0	1	1	1
Molar Liquid													
Fraction		0	1	1	0	0	0	0	1	1	0	0	0
<b>Mole Flows</b>	<b>kmol/h</b>	<b>4</b>	<b>4</b>	<b>3</b>	<b>0</b>	<b>0</b>	<b>4</b>	<b>4</b>	<b>93</b>	<b>93</b>	<b>3</b>	<b>0</b>	<b>1</b>
Methanol	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
DME	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Water	kmol/h	0	0	0	0	0	0	0	93	93	0	0	0
Methane	kmol/h	0	0	0	0	0	0	0	0	0	1	0	0
Ethane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Ethylene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Propane	kmol/h	1	1	0	0	0	0	0	0	0	0	0	1
Propylene	kmol/h	0	0	0	0	0	0	0	0	0	1	0	0
n-Butane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
i-Butane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Butene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
n-Pentane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
i-Pentane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Cyclopentane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Pentene	kmol/h	1	1	1	0	0	0	0	0	0	0	0	0
n-Hexane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
i-Hexane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Cyclohexane	kmol/h	1	1	1	0	0	0	0	0	0	0	0	0
Hexene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
n-Octane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
i-Octane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Octene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0

Benzene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Durene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Prehnitene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Isodurene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
n-Dodecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
i-Dodecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Dodecene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
n-Hexadecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
i-Hexadecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Hexadecene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
n-Octadecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
i-Octadecane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Octadecene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
n-Eicosane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
i-Eicosane	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Eicosene	kmol/h	0	0	0	0	0	0	0	0	0	0	0	0
Hydrogen	kmol/h	0	0	0	0	0	4	4	0	0	0	0	0
<b>Mass Flows</b>	<b>kg/h</b>	<b>255</b>	<b>255</b>	<b>196</b>	<b>0</b>	<b>0</b>	<b>7</b>	<b>7</b>	<b>1679</b>	<b>1679</b>	<b>98</b>	<b>0</b>	<b>59</b>
Methanol	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
DME	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
Water	kg/h	8	8	7	0	0	0	0	1679	1679	0	0	0
Methane	kg/h	1	1	0	0	0	0	0	0	0	20	0	1
Ethane	kg/h	4	4	0	0	0	0	0	0	0	3	0	4
Ethylene	kg/h	0	0	0	0	0	0	0	0	0	12	0	0
Propane	kg/h	31	31	2	0	0	0	0	0	0	4	0	30
Propylene	kg/h	0	0	0	0	0	0	0	0	0	53	0	0
n-Butane	kg/h	23	23	14	0	0	0	0	0	0	0	0	9
i-Butane	kg/h	23	23	7	0	0	0	0	0	0	1	0	16
Butene	kg/h	0	0	0	0	0	0	0	0	0	5	0	0
n-Pentane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
i-Pentane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0

Cyclopentane	kg/h	33	33	33	0	0	0	0	0	0	0	0	0
Pentene	kg/h	38	38	38	0	0	0	0	0	0	0	0	0
n-Hexane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
i-Hexane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
Cyclohexane	kg/h	58	58	58	0	0	0	0	0	0	0	0	0
Hexene	kg/h	1	1	1	0	0	0	0	0	0	0	0	0
n-Octane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
i-Octane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
Octene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
Benzene	kg/h	35	35	35	0	0	0	0	0	0	0	0	0
Durene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
Prehnitene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
Isodurene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
n-Dodecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
i-Dodecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
Dodecene	kg/h	1	1	1	0	0	0	0	0	0	0	0	0
n-Hexadecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
i-Hexadecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
Hexadecene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
n-Octadecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
i-Octadecane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
Octadecene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
n-Eicosane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
i-Eicosane	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
Eicosene	kg/h	0	0	0	0	0	0	0	0	0	0	0	0
Hydrogen	kg/h	0	0	0	0	0	7	7	0	0	0	0	0
Volume Flow	m <sup>3</sup> /h	25	3	0	2	0	88	3	2	2	4	0	6