

Supplementary materials

Algorithm of Modelling of Drinking Water Recarbonization	
1. Input data	
<ul style="list-style-type: none"> $Q(\text{H}_2\text{O}), Q(\text{CO}_2), T, S_{\text{FBRR}}, V_{\text{FBRR}}, V_{\text{VT}}, d_p, \mu, \rho_s, \rho_l$ 	
2. Hydraulic measurements	
<ul style="list-style-type: none"> $\Delta P = f(w)$ $H = f(w)$ minimum fluidization velocity w_p (Figure 1) 	
3. Saturation kinetics of water with Ca^{2+} and Mg^{2+}	
<ul style="list-style-type: none"> $\text{Ca}^{2+}, \text{Mg}^{2+}, \text{pH}, \kappa, T = f(t)$ Parameter values of recarbonization equation (Eq. 11) Mass balances – calculation of: <ul style="list-style-type: none"> Rate of HCD consumption (kg/d). Specific production of calcium / magnesium (g/kg). Specific consumption of CO_2 (g/kg). 	
4. Continuous measurements - changes of operating parameters - $Q(\text{CO}_2), Q(\text{H}_2\text{O})$	
<ul style="list-style-type: none"> $\text{Ca}^{2+}, \text{Mg}^{2+}, \text{pH}, \kappa, T = f(t)$ Multiple regression analyses: <ul style="list-style-type: none"> Values of regression coefficients (Eq. 12) 	
5. Optimization of recarbonation parameters	
<ul style="list-style-type: none"> Optimal values of independent variables $Q(\text{H}_2\text{O})$ and $Q(\text{CO}_2)$ for minimal and maximal values of dependent variables: <ul style="list-style-type: none"> Ca^{2+} Mg^{2+} $\text{Ca}^{2+} + \text{Mg}^{2+}$ $\text{Ca}^{2+}/\text{Mg}^{2+}$ 	
6. Scaling up of recarbonization system	
<ul style="list-style-type: none"> Input data for scaling up: <ul style="list-style-type: none"> $Q(\text{H}_2\text{O}), Q(\text{CO}_2), T, d_p, \mu, \rho_s, \rho_l, (\text{Ca}^{2+}, \text{Mg}^{2+})_{\text{inflow}}, (\text{Ca}^{2+}, \text{Mg}^{2+})_{\text{outflow}}$ Desing of: <ul style="list-style-type: none"> Flow rate of water concentrate of $(\text{Ca}^{2+}, \text{Mg}^{2+})_{\text{outflow}}$ Volume of water tank $V_{\text{WT}} (\text{m}^3)$ Mass rate of HCD (kg/d) Dimensions of FBRR - $V_{\text{FBRR}} (\text{m}^3), S_{\text{FBRR}} (\text{m}^2), H_{\text{FBRR}} (\text{m})$ Mass rate of CO_2 (kg/d) 	

Figure S1. Algorithm of Modelling of Drinking Water Recarbonization.

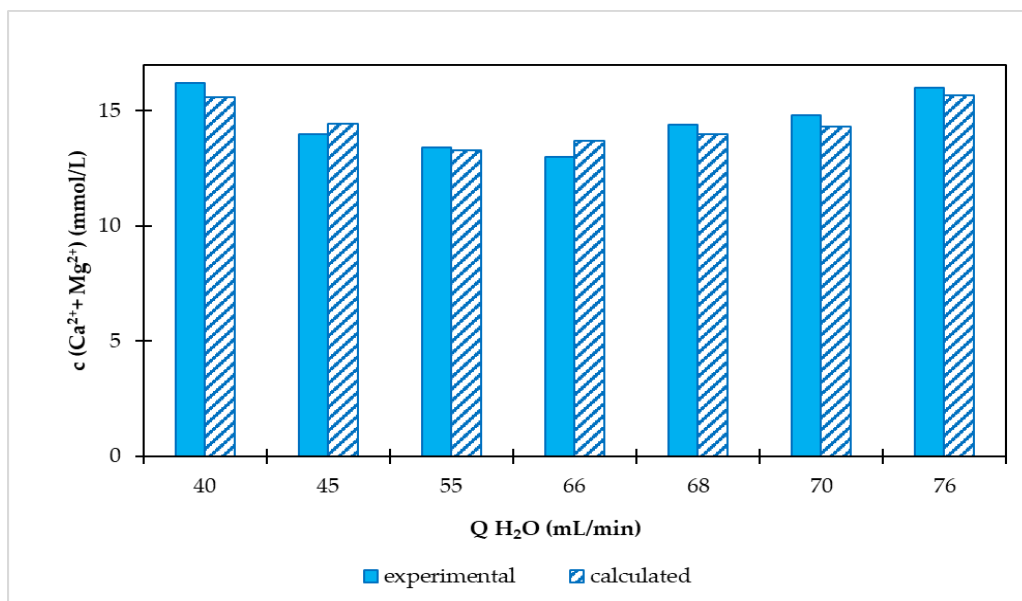


Figure S2. Calculated and measured concentrations of $\text{Ca}^{2+}+\text{Mg}^{2+}$ at different flows of treated water and CO_2 flow at the level of 0.5 L/min during operation of the laboratory FBRR.

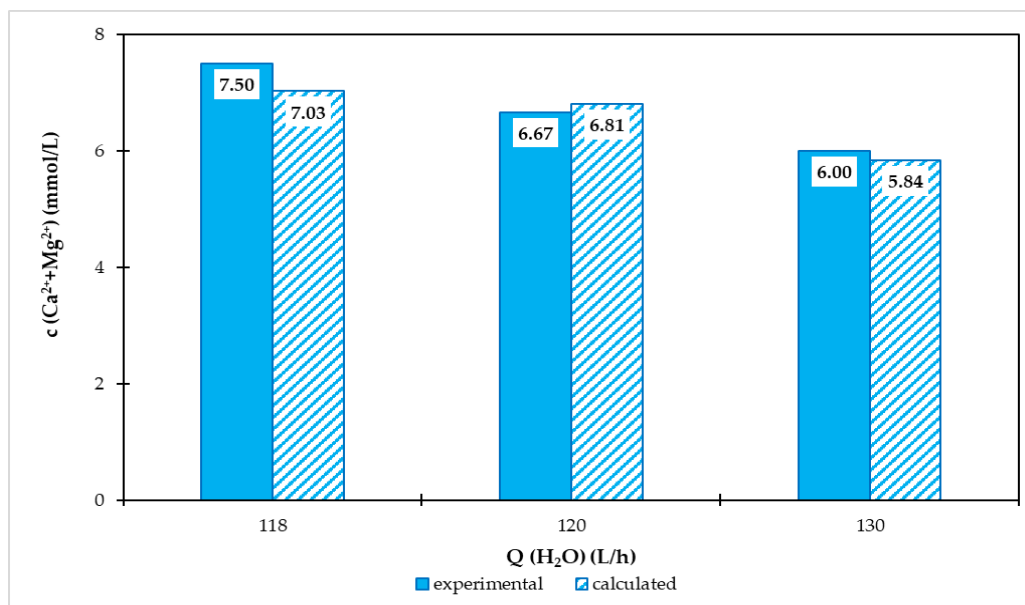


Figure S3. The total concentration of the sum of Ca^{2+} and Mg^{2+} ions in drinking water at $Q(\text{CO}_2) = 0.5$ L/min.

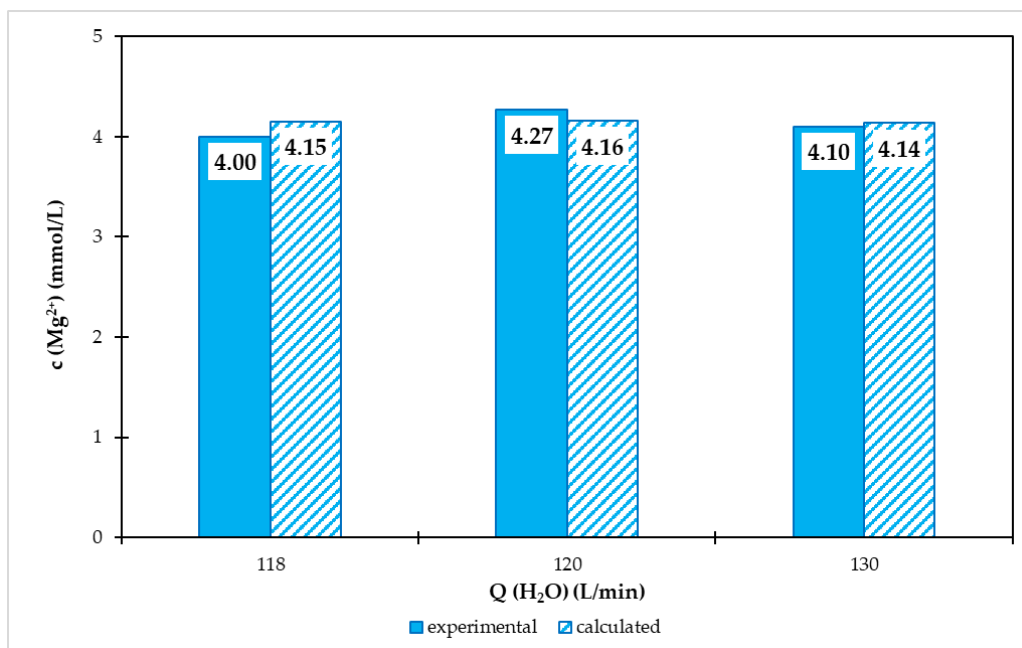


Figure S4. Molar concentration of Mg^{2+} in drinking water at $Q(\text{CO}_2) = 0.5$ L/min.

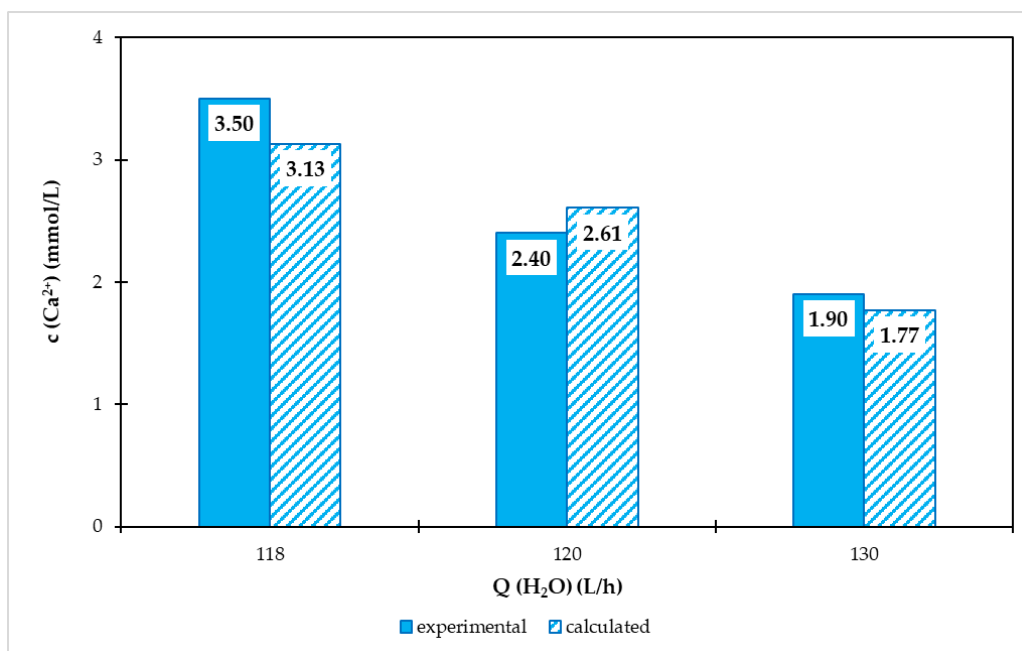


Figure S5. Molar concentration of Ca^{2+} in drinking water at $Q(\text{CO}_2) = 0.5$ L/min.

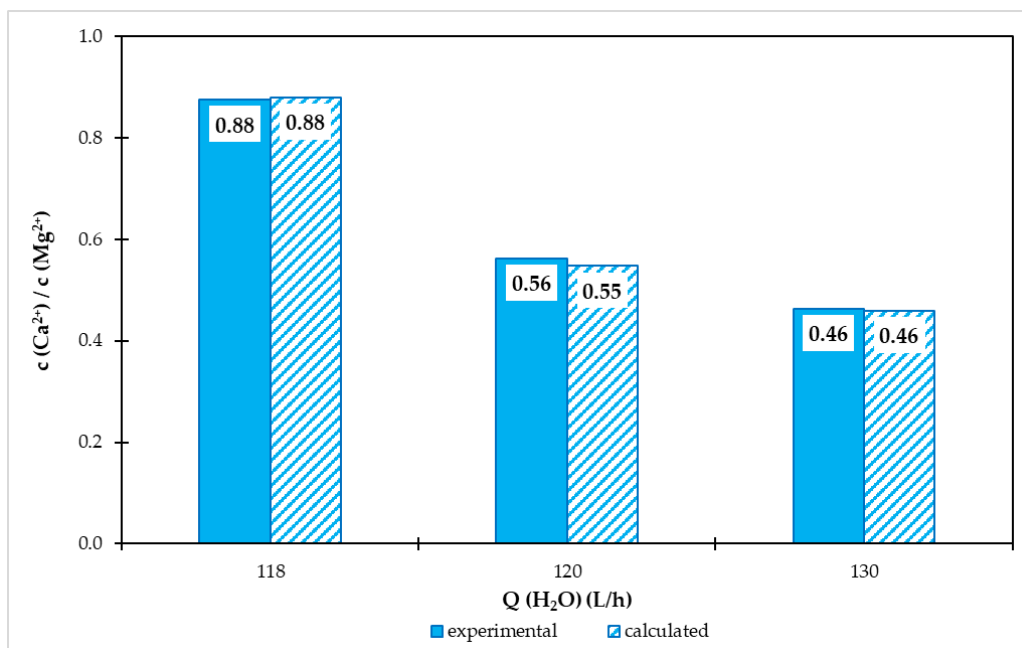


Figure S6. Molar concentration ration of Ca^{2+} and Mg^{2+} in drinking water at $Q(\text{CO}_2) = 0.5 \text{ L/min}$.

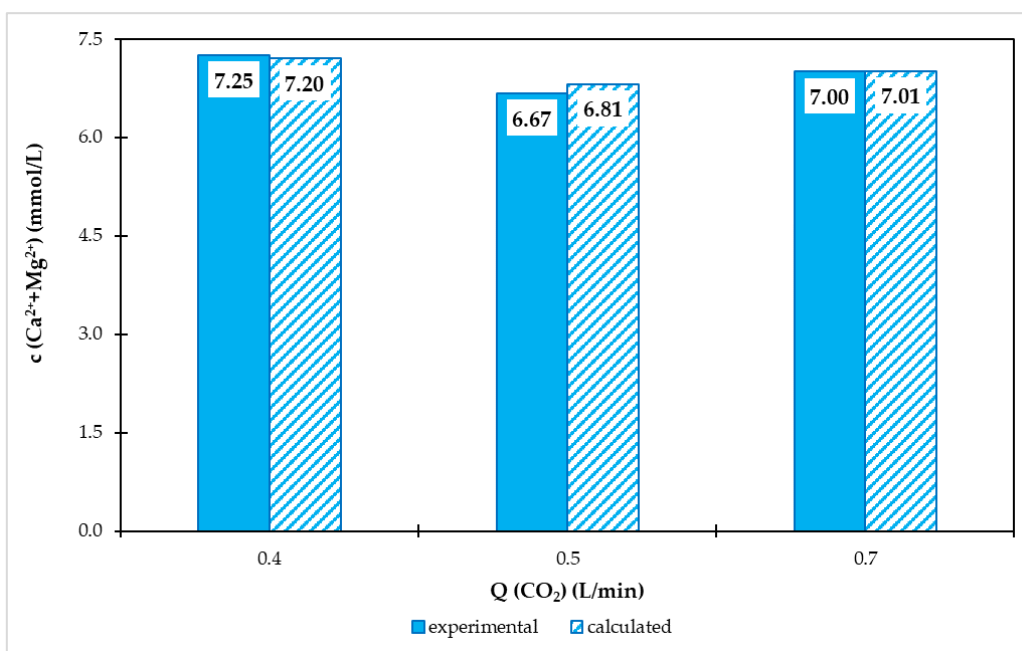


Figure S7. Molar concentration of the sum of Ca^{2+} and Mg^{2+} in drinking water at $Q(\text{H}_2\text{O}) = 120 \text{ L/h}$.

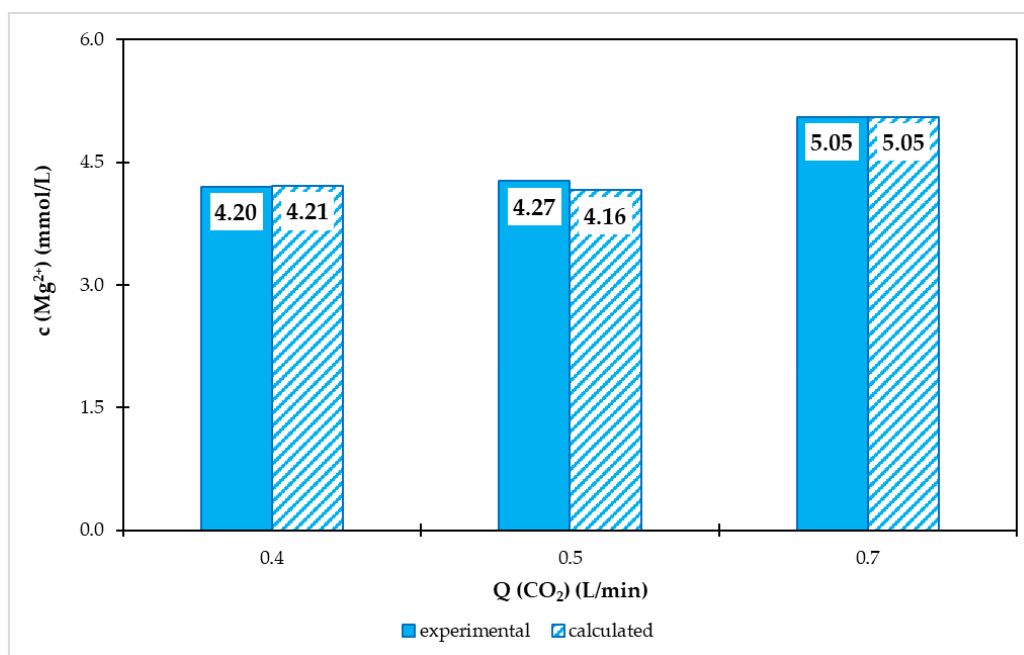


Figure S8. Molar concentration of the sum of Mg²⁺ in drinking water at Q(H₂O) = 120 L/h.

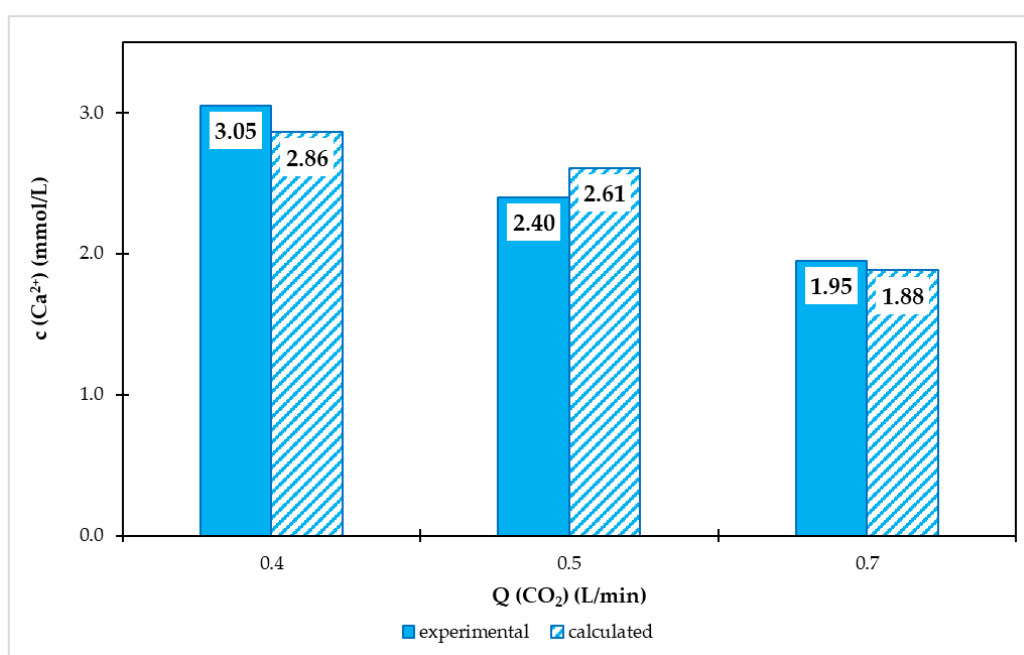


Figure S9. Molar concentration of the sum of Ca²⁺ in drinking water at Q(H₂O) = 120 L/h.

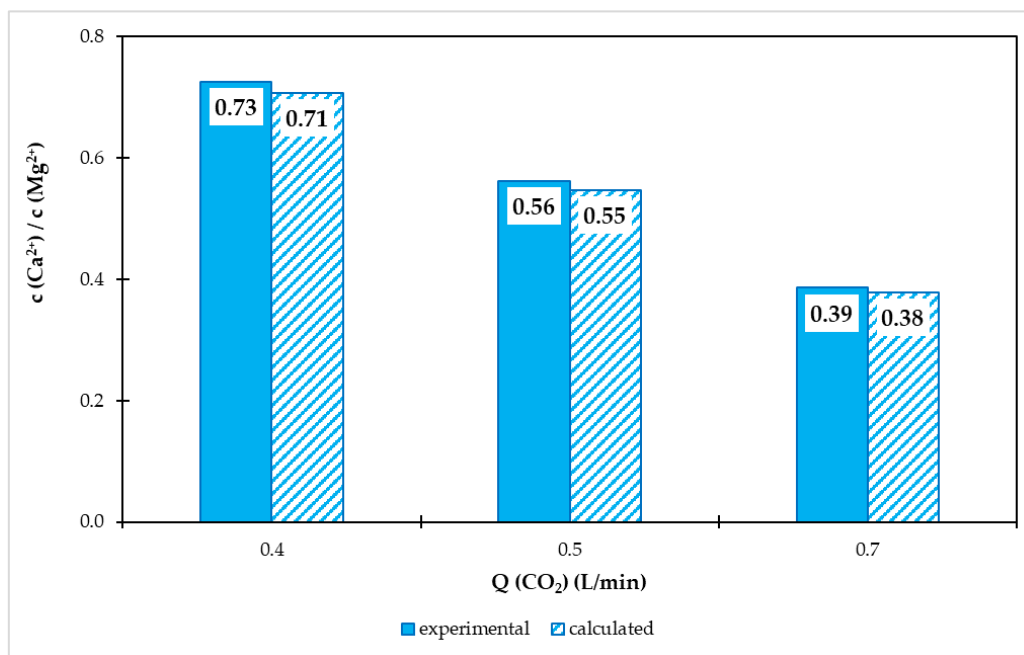


Figure S10. Molar ratio of Ca^{2+} and Mg^{2+} concentration in drinking water at $Q(\text{H}_2\text{O}) = 120 \text{ L/h}$.