

Supplementary material

# Modeling and Experimental Studies on Carbon Dioxide Absorption with Sodium Hydroxide Solution in a Rotating Zigzag Bed

Zhibang Liu <sup>1</sup>, Arash Esmaeili <sup>1</sup>, Hanxiao Zhang <sup>1</sup>, Dan Wang <sup>2,3</sup>, Yuan Lu <sup>4</sup> and Lei Shao <sup>1,\*</sup>

<sup>1</sup> Research Center of the Ministry of Education for High Gravity Engineering and Technology, Beijing University of Chemical Technology, Beijing 100029, China; 2019400002@mail.buct.edu.cn (Z.L.); ar.esmaeli@mail.buct.edu.cn (A.E.); 2018200070@mail.buct.edu.cn (H.Z.)

<sup>2</sup> State Key Laboratory of Petroleum Pollution Control, Beijing 102206, China; wang-dan@cnpc.com.cn

<sup>3</sup> CNPC Research Institute of Safety and Environmental Technology, Beijing 102206, China

<sup>4</sup> CenerTech Oilfield Chemical Co., Ltd., Tianjin 300450, China; luyuan2@cnooc.com.cn

\* Correspondence: shaol@mail.buct.edu.cn; Tel.: +86-10-6442 1706

It can be calculated from  $k_L$  and  $k_G$  in Table S1 that the contribution of the gas-side mass transfer resistance to the total mass transfer resistance cannot be ignored. However, the main mass transfer resistance still lies on the liquid side. Compared with the  $k_G$  in Reference [10], the  $k_G$  in our study was smaller because the inlet gas flow rate was two orders of magnitude smaller than that in Reference [10].

The difference in the value of  $k_L$  and  $a$  between this study and Reference [10] resulted from different experimental conditions. As for  $k_L$ , the value in this study was higher than that in Reference [10] because NaOH concentration and temperature of NaOH solution used in this study were higher than those in Reference [10]. In terms of  $a$ , the value in this study was close to that in Reference [10] due to a similar structure.

It can be seen from Table S2 that the liquid-side mass-transfer coefficient and gas-liquid effective interfacial area in zone II were larger than those in zone I and III, and thus liquid-side volumetric mass-transfer coefficient in zone II was much higher than that in zone I and III, suggesting that the main contribution of liquid-side mass transfer was from zone II. The above conclusions in this study agree with those in Wang et al.'s research [2].

**Citation:** Liu, Z.; Esmaeili, A.; Zhang, H.; Wang, D.; Lu, Y.; Shao, L. Modeling and Experimental Studies on Carbon Dioxide Absorption with Sodium Hydroxide Solution in a Rotating Zigzag Bed. *Processes* **2022**, *10*, 614. <https://doi.org/10.3390/pr10030614>

Academic Editors: Elio Santacesaria, Riccardo Tesser and Vincenzo Russo

Received: 21 February 2022

Accepted: 17 March 2022

Published: 21 March 2022

**Publisher's Note:** MDPI stays neutral with regard to jurisdictional claims in published maps and institutional affiliations.



**Copyright:** © 2022 by the authors. Submitted for possible open access publication under the terms and conditions of the Creative Commons Attribution (CC BY) license (<https://creativecommons.org/licenses/by/4.0/>).

**Table S1.** Comparison of mass transfer performance between RZB in this work and that in Reference [10].

	This work	Reference [10]
Rotor volume (cm <sup>3</sup> )	665	2821
G (m <sup>3</sup> /h)	0.2-1.2	10-40
L (L/h)	25-40	80-240
N (rpm)	400-1200	600-1400
T (K)	293.15-313.15	293.15-298.15
C (kmol/m <sup>3</sup> )	0.1-0.2	0.05 or 1 (NaOH), 0.87 (ethanol)
$k_L$ (m/s)	$2.27 \times 10^{-3}$ - $4.56 \times 10^{-3}$	$1.95 \times 10^{-3}$ - $2.94 \times 10^{-3}$
$k_G$ (m/s)	$3.94 \times 10^{-3}$ - $8.84 \times 10^{-3}$	$2.09 \times 10^{-2}$ - $6.70 \times 10^{-2}$
$a$ (m <sup>2</sup> /m <sup>3</sup> )	148.72-154.88	127-338

**Table S2.** Values of individual and overall mass transfer factors in RZB.

Item	Value
Rotor volume (cm <sup>3</sup> )	665
G (m <sup>3</sup> /h)	0.2-1.2
L (L/h)	25-40
N (rpm)	400-1200
T (K)	293.15-313.15
C <sub>NaOH</sub> (kmol/m <sup>3</sup> )	0.1-0.2
$k_{L-I}$ (m/s)	$1.26 \times 10^{-3}$ - $2.97 \times 10^{-3}$
$k_{L-II}$ (m/s)	$2.60 \times 10^{-3}$ - $5.46 \times 10^{-3}$
$k_{L-III}$ (m/s)	$1.43 \times 10^{-3}$ - $3.1 \times 10^{-3}$
$k_L$ (m/s)	$2.27 \times 10^{-3}$ - $4.56 \times 10^{-3}$
$a_I$ (m <sup>2</sup> /m <sup>3</sup> )	16.69-21.33
$a_{II}$ (m <sup>2</sup> /m <sup>3</sup> )	95.32
$a_{III}$ (m <sup>2</sup> /m <sup>3</sup> )	36.68-39.4
$a$ (m <sup>2</sup> /m <sup>3</sup> )	148.72-154.88
$k_{L-I} a_I$ (1/s)	0.021-0.059
$k_{L-II} a_{II}$ (1/s)	0.25-0.52
$k_{L-III} a_{III}$ (1/s)	0.053-0.12
$k_L a$ (1/s)	0.34-0.70
$k_G$ (kmol/kPa m <sup>2</sup> s)	$1.23 \times 10^{-6}$ - $2.85 \times 10^{-6}$
$K_G a$ (kmol/kPa m <sup>3</sup> s)	$6.86 \times 10^{-5}$ - $1.04 \times 10^{-4}$