

## Supporting Information

# The Role of the Anion in Imidazolium-Based Ionic Liquids for Fuel and Terpenes Processing

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## Section S1 – Chemicals and experimental details

**Table S1.** ILs chemical structures and properties (melting temperature  $T_m$ , glass transition temperature  $T_g$ , mass fraction purity as declared by the supplier  $w$ , and molecular weight  $Mw$ ).

	<u>1-butyl-3-methylimidazolium hexafluorophosphate, [C<sub>4</sub>mim][PF<sub>6</sub>]</u> Acquired from Iolitec; $w = 0.990$ ; $Mw = 284.19 \text{ g}\cdot\text{mol}^{-1}$ $T_m = 283.2 \text{ K}$ [1]; $Tg = 190.6 \text{ K}$ [1]
	<u>1-butyl-3-methylimidazolium chloride, [C<sub>4</sub>mim]Cl</u> Acquired from Iolitec; $w = 0.990$ ; $Mw = 174.67 \text{ g}\cdot\text{mol}^{-1}$ $T_m = 341.95 \text{ K}$ [2]; $Tg = 197.35 \text{ K}$ [2]

**Table S2.** Name, structure, source, boiling temperature, and mass fraction purity (as declared by the supplier) of the organic solutes used. Names in parentheses correspond to synonyms used in the text. Solutes stereochemistry is omitted in the manuscript.

Family	Name	Chemical structure	Supplier	Boiling temperature (K)	Purity (mass fraction)
	Water		- <sup>a</sup>	373.15 <sup>b</sup>	- <sup>a</sup>
Alkanes	Heptane		Aldrich	371.15 <sup>b</sup>	$\geq 0.990$
	Octane		Aldrich	398.77 <sup>b</sup>	$\geq 0.990$
	Nonane		Aldrich	423.91 <sup>b</sup>	$\geq 0.990$
	Decane		Aldrich	447.20 <sup>b</sup>	$\geq 0.990$
Cycloalkanes	Cyclohexane		Aldrich	353.90 <sup>b</sup>	$\geq 0.990$
	Methylcyclohexane		Aldrich	374.00 <sup>b</sup>	$\geq 0.990$
Ketones	Propanone (Acetone)		Aldrich	329.30 <sup>b</sup>	$\geq 0.999$
	2-Butanone		Aldrich	353.00 <sup>b</sup>	$\geq 0.990$
Ether	Ethoxyethane (Diethyl ether)		Aldrich	307.70 <sup>b</sup>	$\geq 0.999$
Cyclic Ethers	Oxolane (THF)		Aldrich	339.00 <sup>b</sup>	$\geq 0.999$
	1,4-dioxane		Aldrich	374.30 <sup>b</sup>	$\geq 0.998$
Aromatic Hydrocarbons	Benzene		Aldrich	353.22 <sup>b</sup>	$\geq 0.998$
	Toluene		Aldrich	383.75 <sup>b</sup>	$\geq 0.998$
	Ethylbenzene		Aldrich	409.35 <sup>b</sup>	$\geq 0.998$

	<i>p</i> -xylene		Aldrich	411.5 <sup>b</sup>	$\geq 0.990$
Esters	Methyl acetate		Aldrich	330.00 <sup>b</sup>	$\geq 0.998$
	Vinyl acetate		Riedel-de-Häen	345.70 <sup>b</sup>	$\geq 0.990$
	Ethyl acetate		Aldrich	350.20 <sup>b</sup>	$\geq 0.998$
Alcohols	Methanol		Aldrich	337.80 <sup>b</sup>	$\geq 0.998$
	Ethanol		Aldrich	351.50 <sup>b</sup>	$\geq 0.999$
	1-propanol		Aldrich	370.30 <sup>b</sup>	$\geq 0.999$
	2-propanol		Fluka	355.50 <sup>b</sup>	$\geq 0.995$
	2-methyl-1-propanol (Isobutanol)		Aldrich	380.80 <sup>b</sup>	$\geq 0.998$
	1-butanol		Aldrich	390.60 <sup>b</sup>	$\geq 0.995$
	2-butanol		Aldrich	372.00 <sup>b</sup>	$\geq 0.997$
	2-methyl-2-propanol ( <i>tert</i> -butanol)		Aldrich	355.50 <sup>b</sup>	$\geq 0.999$
	Acetonitrile		Fluka	355.15 <sup>b</sup>	$\geq 0.998$
	Pyridine		Aldrich	388.15 <sup>b</sup>	$\geq 0.990$
	Thiophene		Aldrich	357.15 <sup>b</sup>	$\geq 0.980$
Terpenes	$\alpha$ -pinene		Aldrich	430.00 <sup>b</sup>	$\geq 0.990$
	$\beta$ -pinene		Aldrich	439.20 <sup>b</sup>	$\geq 0.970$
	<i>R</i> -(+)-limonene		Aldrich	449.65 <sup>b</sup>	$\geq 0.990$
	<i>p</i> -cymene		Aldrich	450.28 <sup>b</sup>	$\geq 0.990$
	Myrcene		Aldrich	440.20 <sup>b</sup>	$\geq 0.990$
	$\gamma$ -terpinene		Aldrich	455.15 <sup>b</sup>	$\geq 0.970$
Terpenoid s	( <i>-</i> )-menthone		Fluka	490.79 <sup>b</sup>	$\geq 0.980$

(1 <i>R</i> )-(-)-fenchone		Aldrich	466.65 <sup>c</sup>	≥ 0.970
α-pinene oxide		Aldrich	447.15 <sup>c</sup>	≥ 0.990
Eucalyptol		Aldrich	449.55 <sup>c</sup>	≥ 0.970
Linalool		Aldrich	471.65 <sup>c</sup>	≥ 0.980
Geraniol		Aldrich	502.15 <sup>c</sup>	≈ 0.950
DL-citronellol		Aldrich	497.65 <sup>c</sup>	≥ 0.980
(1 <i>R</i> )-(+)camphor		Aldrich	480.55 <sup>c</sup>	≥ 0.980
( <i>S</i> )-(+)-carvone		Merck	503.65 <sup>c</sup>	≥ 0.997
L(-)-menthol		Acros	488.55 <sup>c</sup>	≥ 0.980
(-)isopulegol		SAFC	470.15 <sup>c</sup>	≥ 0.990
(-)borneol		Fluka	485.15 <sup>c</sup>	≥ 0.990
Citronellal		Aldrich	480.15 <sup>c</sup>	≥ 0.950
Eugenol		Aldrich	526.35 <sup>b</sup>	0.990
Carvacrol		SAFC	510.15 <sup>b</sup>	0.990
Thymol		Sigma	505.65 <sup>b</sup>	≥ 0.995

<sup>a</sup>Ultrapure water was used (resistivity of 18.2MΩ·cm, free particles ≥ 0.22 μm and total organic carbon < 5 μg·dm<sup>-3</sup>).

<sup>b</sup>The boiling temperature was obtained from Yaws [3].

<sup>c</sup>The boiling temperature was obtained from ChemSpider [4].

### Column packing and Chromatographic methodology

The column packing method follows our previous works [5–7]: the ionic liquid (IL) and the solid support (Chromosorb W/AW – DMCS, Grace, 100-120 mesh) were diluted in methanol that was then removed through vacuum-assisted rotary evaporation. The resulting solid mixture (stationary phase 45-50% in mass) was packed into an in-house glass column (length: 1 m;

internal diameter: 0.4 cm) using a vacuum pump. Before measurements, the column was pre-conditioned, *i.e.*, a stream of helium gas (carrier gas) was passed through for at least 6 h at 393.2 K to facilitate the removal of eventual impurities. The solute retention time in each IL was then measured by a Varian CP-3380 gas chromatograph equipped with a 1041 on-column injector and a thermal conductivity detector (TCD). A Swagelok S model pressure transducer with an accuracy of 0.25% BFSL was used to measure the column inlet pressure. The outlet temperature ( $\pm 0.1$  K), the atmospheric pressure ( $\pm 0.05$  atm), and the outlet flow rate (relative uncertainty of 6%) were measured with a precision gas flowmeter (Agilent, model 5067-0223). During the analyses with traditional organic solvents and water, the injector and detector temperatures were set at 503.2 K and 523.2 K, respectively. For the analyses involving terpenes and terpenoids, the injector and detector temperatures were set to 553.2 K and 573.2 K, respectively. To achieve infinite dilution conditions, the solutes were injected in the column in the volume range of (0.2-0.5)  $\mu$ L. Together with the solute, air was injected as a non-retained component. Retention times were calculated by the difference of the retention times of the solute,  $t_R$ , and air,  $t_G$ . The experiments were performed at least at three different temperatures in the range 333.2-453.2 K and each experiment was repeated at least twice. For a set of solutes (minimum 10 solutes, for each ionic liquid in the stationary phase, including compounds from different families), the retention times were measured in two independent columns at three temperatures. The  $\gamma_{13}^{\infty}$  values of the two independent columns have a repeatability with a global coefficient of variation (mean value) of 3.25%. An XP205 Mettler Toledo scale (readability  $\pm 0.01$  mg) was used to prepare the equimolar [C<sub>4</sub>mim][PF<sub>6</sub>]/[C<sub>4</sub>mim]Cl mixture (0.501:0.499 mole ratio).

## Section S2 - Thermodynamic background

### Activity Coefficient at Infinite Dilution

The retention times obtained by the inverse gas chromatography (IGC) methodology were used to calculate the activity coefficients at infinite dilution,  $\gamma_{13}^\infty$ , for a solute (1) partitioning between a carrier gas (2) and a non-volatile liquid solvent (3), using the methodologies developed by Everett [8] and Cruickshank et al. [9] in the 1960s, as presented in **Eq. (S1)**:

$$\ln \gamma_{13}^\infty = \ln \frac{n_3 RT}{V_N p_1^*} - \frac{p_1^*(B_{11} - V_1^*)}{RT} + \frac{p_0 J_2^3 (2B_{12} - V_1^\infty)}{RT} \quad (\text{S1})$$

$n_3$	number of moles of solvent packed in the column
$R$	ideal gas constant
$T$	absolute temperature of the column (regulated by the GC oven)
$V_N$	net retention volume of the solute - <b>Eq. (S2)</b>
$p_1^*$	saturated vapor pressure of the solute at the column temperature
$B_{11}$	second virial coefficient of the pure solute
$V_1^*$	molar volume of the solute
$p_0$	column outlet pressure
$J_2^3$	pressure correction factor - <b>Eq. (S3)</b>
$B_{12}$	crossed second virial coefficient of the solute and the carrier gas (helium)
$V_1^\infty$	partial molar volume of the solute at infinite dilution in the solvent

$V_N$  and  $J_2^3$  are given by:

$$V_N = (J_2^3)^{-1} U_0 (t_R - t_g) \quad (\text{S2})$$

$U_0$	outlet volumetric flow rate (at the column temperature)
$t_r$	retention times of the solute
$t_g$	retention times of air (non-retained substance)

$$J_2^3 = \frac{2(p_i/p_0)^3 - 1}{3(p_i/p_0)^2 - 1} \quad (\text{S3})$$

$p_i$	column inlet pressure
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As the flow rate,  $U$ , is measured with a flowmeter placed after the carrier gas leaves the detector, it needs to be corrected:

$$U_0 = U \frac{p_f}{p_0} \frac{T}{T_f} \quad (\text{S4})$$

- $U_f$  volumetric flow measured by the flowmeter after the carrier gas goes through the detector  
 $p_f$  pressure measured by the flowmeter after the carrier gas goes through the detector  
 $T_f$  temperature measured by the flowmeter after the carrier gas goes through the detector

To accurately estimate the column outlet pressure  $p_0$ , a linear regression between the pressure drop value ( $\Delta P$ ) and the volumetric flow rate was established at different temperatures using **Eq. (S5)**.

$$\Delta P = p_0 - p_f = A \cdot U + B \quad (\text{S5})$$

The second order virial coefficients necessary in **Eq. (S1)** were estimated using the correlation proposed by Tsnonopoulos [10] and discussed, in detail, by Poling [11]. Additional solute properties required for  $\gamma_{13}^\infty$  calculation, namely vapor pressure, density, critical properties, acentric factor, and dipole moment, were taken from previous works [5–7,12,13].

#### Excess Partial Molar Properties at Infinite Dilution

To further interpret the interactions and the measured  $\gamma_{13}^\infty$  data, the excess partial molar properties at infinite dilution, namely excess enthalpy ( $\bar{H}_m^{E,\infty}$ ) and entropy ( $\bar{S}_m^{E,\infty}$ ) which are contributions to the excess Gibbs energy ( $\bar{G}_m^{E,\infty}$ ), can be determined by using the linear dependence of  $\gamma_{13}^\infty$  with temperature (van't Hoff plot [5,14]) using the following equations:

$$\ln \gamma_{13}^\infty = \frac{\bar{H}_m^{E,\infty}}{R} \frac{1}{T} - \frac{\bar{S}_m^{E,\infty}}{R} \quad (\text{S6})$$

$$\bar{G}_m^{E,\infty} = RT \ln \gamma_{13}^\infty \quad (\text{S7})$$

And, at a reference temperature  $T_{ref}$ :

$$\bar{G}_m^{E,\infty} = \bar{H}_m^{E,\infty} - \bar{S}_m^{E,\infty} T_{ref} \quad (\text{S8})$$

### Gas-Liquid Partition Coefficient

The gas-liquid partition coefficients ( $K_L$ ) are translated as the solute partitioning between the carrier gas (helium) and the stationary phase (IL) and can be determined from the IGC experiments according to [15]:

$$\ln(K_L) = \frac{c_1^3}{c_1^2} = \ln \frac{V_N \rho_3}{m_3} - \frac{p_0 J_2^3 (2B_{12} - V_1^\infty)}{RT} \quad (\text{S9})$$

$c$	molar concentration of the solute (1)
$m_3$	mass of ionic liquid (3) in the column
$\rho_3$	density of ionic liquid (3)

### Separation Factors

To evaluate the IL performance as an entrainer in a chemical separation problem, the selectivity between the solutes pair,  $i$  and  $j$ , ( $S_{ij}^\infty$ ), and the separation capacity, ( $k_j^\infty$ ), are calculated as follows:

$$S_{ij}^\infty = \frac{\gamma_{i3}^\infty}{\gamma_{j3}^\infty} \quad (\text{S10})$$

$$k_j^\infty = \frac{1}{\gamma_{j3}^\infty} \quad (\text{S11})$$

$j$	solute with the lowest activity coefficient in each separation pair
3	refers to the ionic liquid

For an ionic liquid to be a good separation agent, high selectivities and capacities are desirable. Unfortunately, these two parameters often counteract, *i.e.*, high values for selectivity are accompanied by low capacities. Thus, it is important to have a balance between these two parameters to be able to evaluate the IL efficiency. To this end, the solvent performance index (which fairly describes this balance) was used in this work [16,17]:

$$Q_{ij}^\infty = S_{ij}^\infty k_j^\infty \quad (\text{S12})$$

## Section S3 – Results and discussion

### Activity coefficients at infinite dilution

**Table S3.** Activity coefficients at infinite dilution of the solutes in [C<sub>4</sub>mim][PF<sub>6</sub>], [C<sub>4</sub>mim][PF<sub>6</sub>]/[ C<sub>4</sub>mim]Cl equimolar mixture, and [C<sub>4</sub>mim]Cl (from the literature [5,6]).<sup>a</sup>

Solute	T / K	[C <sub>4</sub> mim][PF <sub>6</sub> ] <sup>b</sup>						[C <sub>4</sub> mim][PF <sub>6</sub> ]/[ C <sub>4</sub> mim]Cl equimolar mixture <sup>c</sup>						[C <sub>4</sub> mim]Cl <sup>d,e,f</sup>					
		333.15	343.15	353.15	363.15	373.15	383.15	333.15	343.15	353.15	363.15	373.15	383.15	333.15	343.15	353.15	363.15	373.15	383.15
Heptane	154.49	137.02	123.64	117.03	101.66	88.29	-	-	-	-	-	-	-	-	-	-	-	-	-
Octane	195.70	178.52	167.14	151.10	133.73	124.94	495.23	435.64	406.29	328.87	-	-	422.72	380.73	344.95	314.23	287.68	264.59	
Nonane	254.50	229.87	206.11	192.74	171.80	162.79	573.68	527.96	482.32	416.77	380.43	341.56	597.90	541.96	494.00	452.59	416.60	385.14	
Decane	338.66	310.84	276.48	250.87	230.93	211.51	704.16	649.55	584.53	508.29	475.14	437.91	875.50	795.82	727.31	668.00	616.33	571.06	
Cyclohexane	45.47	41.03	38.27	35.43	32.16	29.88	147.67	117.23	95.78	78.24	-	-	66.22	61.09	56.61	52.69	49.22	46.15	
Methylcyclohexane	62.95	56.98	53.96	49.19	45.48	42.32	183.48	157.92	138.15	114.31	-	-	101.50	93.88	87.21	81.35	76.17	71.56	
Benzene	1.89	1.91	1.93	1.96	1.98	2.01	3.01	2.99	2.96	2.92	2.91	2.88	4.21	4.33	4.44	4.55	4.66	4.77	
Toluene	2.92	2.95	2.97	2.99	3.02	3.04	4.83	4.82	4.80	4.65	4.56	4.55	7.23	7.44	7.65	7.85	8.04	8.23	
Ethylbenzene	5.23	5.27	5.30	5.34	5.32	5.35	8.58	8.37	8.39	8.24	8.16	8.23	12.55	12.78	13.00	13.21	13.41	13.61	
p-Xylene	4.40	4.48	4.47	4.50	4.48	4.53	7.45	7.46	7.41	7.27	7.26	7.26	12.95	13.20	13.45	13.69	13.92	14.14	
Methyl acetate	1.24	1.26	1.30	1.32	1.36	1.40	2.47	2.42	2.42	2.39	2.40	2.37	4.56	4.66	4.76	4.86	4.95	5.05	
Ethyl acetate	1.95	1.97	2.00	2.03	2.07	-	4.20	4.13	4.05	3.99	3.91	3.85	8.88	8.94	8.99	9.04	9.09	9.13	
Vinyl acetate	1.71	1.74	1.76	1.79	1.82	1.85	3.22	3.17	3.12	3.09	3.06	3.02	5.28	5.43	5.57	5.70	5.83	5.96	
THF	1.52	1.54	1.57	1.59	1.62	1.65	3.00	1.26	1.35	1.41	1.43	2.77	5.62	5.64	5.65	5.66	5.68	5.69	
1,4-dioxane	0.93	0.97	1.00	1.03	1.07	1.10	1.63	1.68	1.73	1.75	1.77	1.77	3.22	3.32	3.42	3.51	3.60	3.69	
Diethyl ether	7.89	7.93	7.92	7.90	7.76	7.62	25.82	24.48	23.27	22.24	22.68	-	20.22	19.80	19.41	19.06	18.72	18.41	
Acetonitrile	0.51	0.53	0.53	0.54	0.54	0.55	0.75	0.76	0.76	0.77	0.78	0.78	0.98	1.03	1.09	1.14	1.19	1.25	
Pyridine	0.81	0.86	0.89	0.94	0.97	1.03	1.19	1.23	1.29	1.32	1.37	1.43	1.21	1.31	1.41	1.51	1.61	1.71	
Thiophene	1.36	1.39	1.41	1.43	1.46	1.48	1.68	0.76	0.77	0.78	0.78	1.77	1.74	1.86	1.98	2.10	2.22	2.34	
Acetone	0.71	0.74	0.75	0.77	0.79	0.82	1.42	1.43	1.44	1.45	1.45	1.47	2.85	2.93	3.01	3.08	3.15	3.22	
2-Butanone	1.07	1.10	1.12	1.15	1.18	1.22	2.14	2.14	2.15	2.14	2.15	2.15	-	-	-	-	-	-	
Methanol	1.93	1.83	1.77	1.67	1.57	1.53	0.21	0.23	0.24	0.26	0.27	0.27	0.09	0.10	0.11	0.12	0.13	0.14	
Ethanol	2.58	2.35	2.20	1.99	1.80	1.71	0.36	0.37	0.38	0.38	0.39	0.39	0.18	0.20	0.22	0.23	0.25	0.27	
1-propanol	3.47	3.14	-	2.64	2.41	2.28	0.48	0.49	0.49	0.50	0.51	0.51	0.23	0.25	0.28	0.31	0.33	0.36	
2-propanol	3.18	2.88	2.65	-	2.24	2.13	0.60	0.61	0.62	0.62	0.62	0.62	0.30	0.34	0.37	0.41	0.44	0.48	
Isobutanol	4.57	4.05	3.66	3.33	3.07	2.87	0.63	0.64	0.64	0.64	0.64	0.68	0.30	0.33	0.37	0.40	0.44	0.48	
1-butanol	4.74	4.24	3.82	3.45	3.16	2.95	0.66	0.67	0.67	0.68	0.68	0.84	0.32	0.35	0.39	0.42	0.46	0.50	
2-butanol	3.96	3.62	3.31	3.05	2.88	2.73	0.79	0.81	0.82	0.83	0.84	0.64	0.41	0.45	0.50	0.55	0.61	0.66	
Tert-butanol	3.73	3.45	3.24	3.08	2.94	2.82	1.03	1.06	1.09	1.11	1.12	1.12	0.49	0.55	0.62	0.70	0.77	0.85	
Water	2.83	2.52	2.21	2.00	1.82	1.63	0.13	0.15	0.16	0.16	0.17	0.03	0.04	0.04	0.05	0.05	0.06		

Terpenes/terpenoids	353.15	363.15	373.15	383.15	393.15	403.15	353.15	363.15	373.15	383.15	393.15	403.15	353.15	363.15	373.15	383.15	393.15	403.15
$\alpha$ -pinene	54.62	51.95	48.97	46.92	44.11	42.70	101.58	78.66	75.24	74.81	73.37	64.28	414.66	383.21	355.64	331.35	309.83	290.67
$\beta$ -pinene	34.09	32.72	31.36	30.78	29.21	28.67	59.82	51.01	49.25	44.38	41.78	37.97	256.84	244.63	233.60	223.61	214.52	206.23
Limonene	33.66	31.22	30.49	29.38	28.20	27.55	53.70	48.78	48.67	43.66	39.20	38.83	-	-	-	-	-	-
Myrcene	31.05	30.74	30.24	29.90	29.67	29.57	51.16	51.19	46.09	46.38	44.03	42.77	-	-	-	-	-	-
$\gamma$ -terpinene	24.67	24.42	24.11	23.85	23.79	23.55	38.04	37.16	35.64	34.90	35.01	34.62	-	-	-	-	-	-
p-cymene	13.02	12.93	12.90	12.64	12.58	12.52	22.73	21.52	20.50	21.24	20.27	20.20	-	-	-	-	-	-
Eucalyptol	17.92	17.31	17.19	16.14	15.86	15.67	35.83	32.67	29.57	30.46	28.02	26.30	189.63	182.98	176.90	171.33	166.21	161.48
Low volatile terpenoids	383.15	393.15	403.15	413.15	423.15	433.15	383.15	393.15	403.15	413.15	423.15	433.15	383.15	393.15	403.15	413.15	423.15	433.15
$\alpha$ -pinene oxide	6.25	6.51	6.67	6.83	7.07	7.21	11.55	11.69	11.94	11.99	12.12	12.92	79.52	83.01	86.45	89.86	93.23	96.55
Fenchone	5.62	5.66	5.72	5.73	5.73	5.76	10.87	10.91	11.31	10.73	10.78	11.08	67.88	66.08	64.41	62.87	61.43	60.10
Menthone	6.80	6.84	6.92	7.00	7.04	7.05	13.21	13.26	13.26	13.08	12.88	12.64	92.79	92.29	91.82	91.37	90.95	90.55
Carvone	3.41	3.49	3.57	3.68	3.75	3.85	5.64	5.65	5.86	5.90	6.13	6.40	35.70	36.16	36.62	37.05	37.47	37.87
Isopulegol	7.02	6.92	6.81	6.73	6.54	6.48	3.02	3.25	3.34	3.48	3.75	3.94	6.78	7.24	7.70	8.17	8.64	9.11
Citronellol	11.11	10.64	-	9.31	8.76	8.35	2.83	2.90	3.01	3.03	3.05	3.10	6.29	6.77	7.27	7.77	8.28	8.79
Geraniol	8.77	8.15	7.80	7.45	7.00	6.73	-	2.16	2.20	2.30	2.39	2.50	4.15	4.60	5.08	5.57	6.09	6.62
Linalool	8.23	7.98	7.96	7.89	7.88	8.01	2.86	3.05	3.31	3.49	3.67	4.15	36.17	51.90	73.11	101.26	138.05	185.47
Citronellal	8.50	8.28	8.14	8.04	7.87	7.67	15.25	14.42	13.83	12.33	12.24	-	-	-	-	-	-	
Camphor	4.38	4.43	4.54	4.64	4.73	4.85	-	8.45	8.47	8.39	8.74	8.91	51.23	51.30	51.36	51.42	51.48	51.54
Borneol	10.97	10.02	9.09	8.15	7.51	7.00	2.91	2.90	2.80	2.72	2.73	-	4.78	4.28	3.85	3.48	3.17	2.89
Menthol	11.54	10.97	10.71	10.25	9.92	9.72	3.81	3.98	4.13	4.19	4.46	4.71	8.23	8.84	9.46	10.10	10.74	11.39
Phenolic Terpenoids	413.15	423.15	433.15	443.15	453.15													
Eugenol	3.21	3.46	3.62	3.90	4.12													
Carvacrol	1.80	1.92	2.05	2.17	2.30													
Thymol	1.84	1.92	2.01	2.09	2.13													

<sup>a</sup>The estimated uncertainties in pressure, temperature, and  $\gamma_{13}^{\infty}$  are  $u(T) = 0.1$  K,  $u(p) = 0.05p$ , and  $u(\gamma_{13}^{\infty}) = 0.04$ .

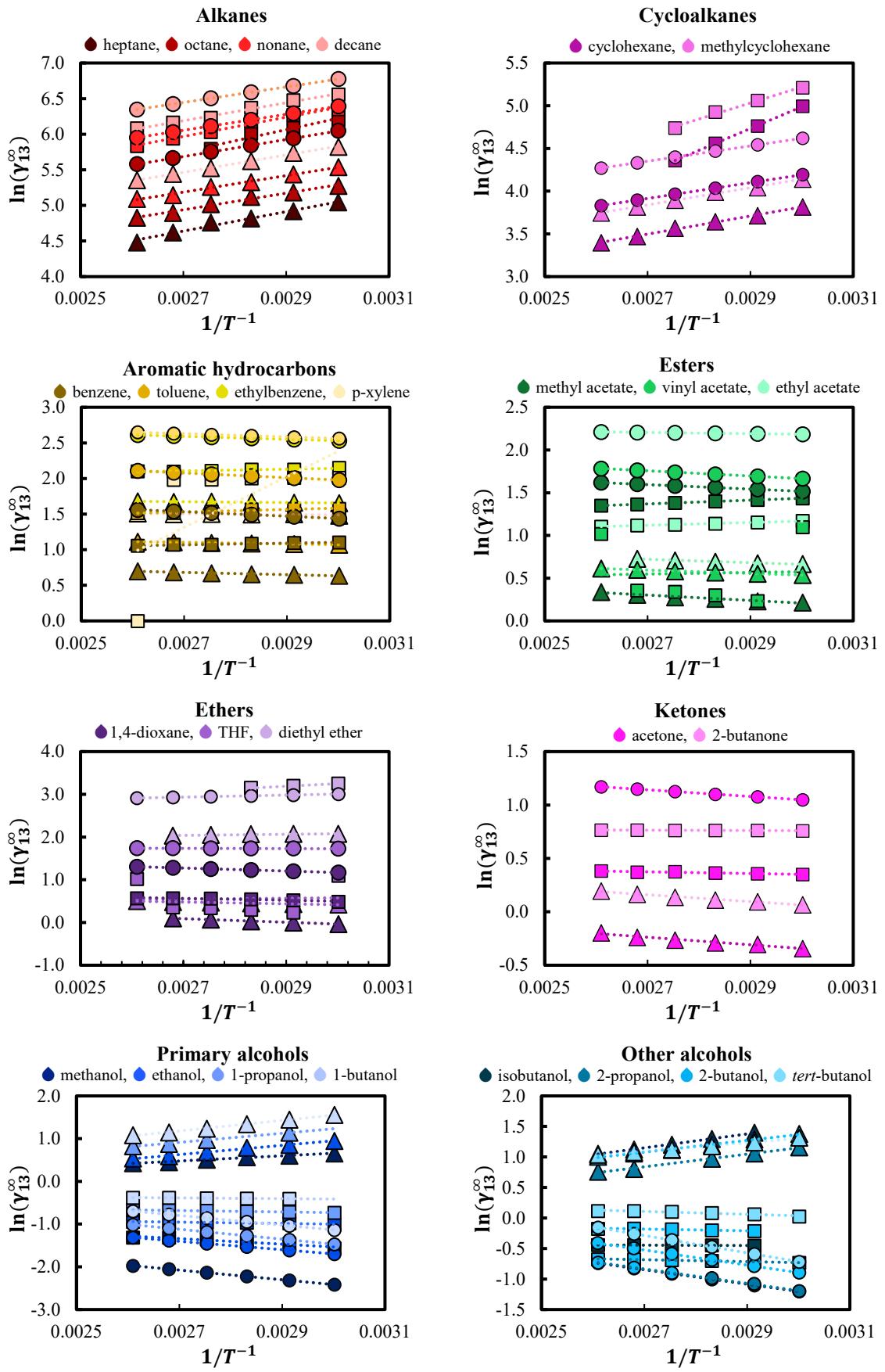
<sup>b</sup>Column Packing: 50% of IL,  $n_3 = 9.48$  mmol.

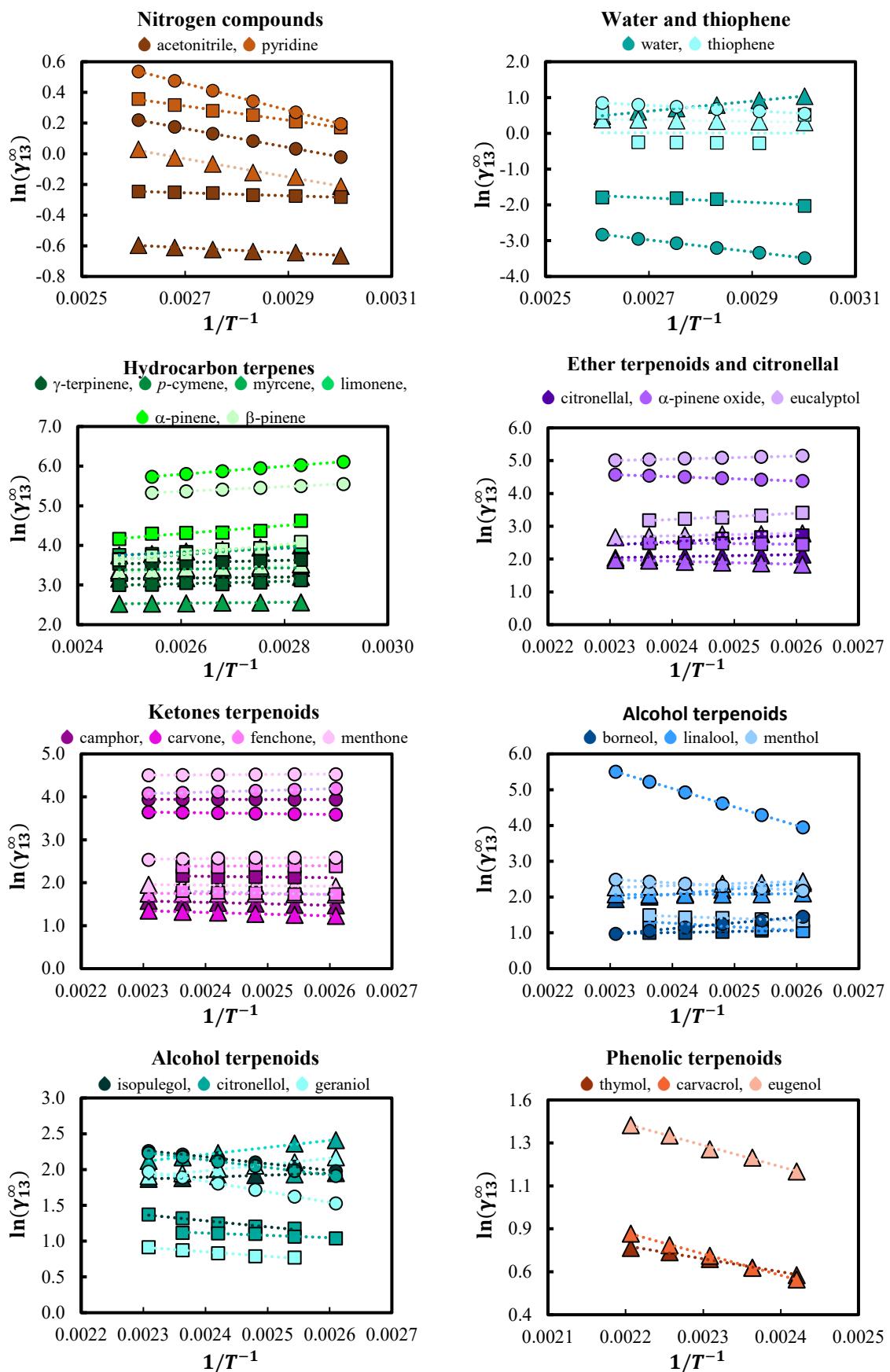
<sup>c</sup>Column Packing: 50% of IL,  $n_3 = 10.75$  mmol.

<sup>d</sup>Column Packing: 51.1% of IL,  $n_3 = 17.02$  mmol.

<sup>e</sup>The  $\gamma_{13}^{\infty}$  of water and organic solutes in [C<sub>4</sub>mim]Cl were extrapolated at 333.15-353.15 K and interpolated at 363.15-383.15 K using data obtained in a temperature range of 358.15-388.15 K reported by Martins et al. [5].

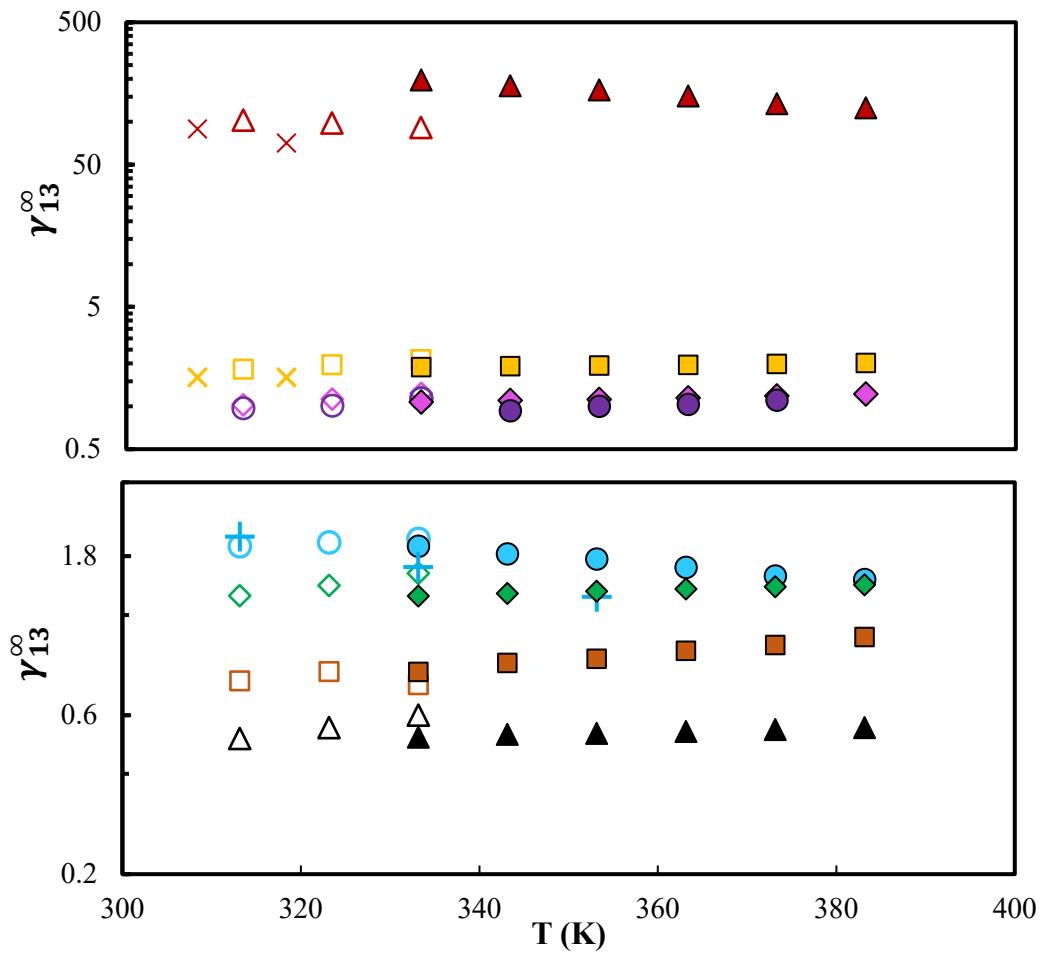
<sup>f</sup>The  $\gamma_{13}^{\infty}$  of terpenes and terpenoids in [C<sub>4</sub>mim]Cl were extrapolated at 353.15-393.15 K and interpolated at 403.15-433.15 K using data obtained in a temperature range of 398.15-448.25 K reported by Martins et al. [6].





**Figure S1.** Representation of  $\ln \gamma_{13}^{\infty}$  as function of  $1/T (K^{-1})$  of the solutes in (●),  $[C_4mim]Cl$  [5,6]; (■),  $[C_4mim][PF_6]/[C_4mim]Cl$  mixture; and (▲),  $[C_4mim][PF_6]$ .

*Comparison with literature data*



**Figure S2.** Comparison of the experimental activity coefficients at infinite dilution with values from the literature for  $[C_4mim][PF_6]$ . Colour code: ▲ octane, ■ benzene, ● 1,4-dioxane, ♦ 2-butanone, ● methanol, ■ pyridine, ▲ acetonitrile, and ♦ thiophene. Full symbols correspond to experimental data measured in this work, and empty symbols correspond to literature data from Mutelet et al. [18]; (x), Zhu et al. [19]; and (+), Dobryakov et al. [20].

*Solvatochromic parameters*

**Table S4.** Solvatochromic parameters, namely dipolarity/polarizability ( $\pi^*$ ), hydrogen bond acidity ( $\alpha$ ), and hydrogen bond basicity ( $\beta$ ) for some methylimidazolium-based ILs [21,22].

Ionic Liquid	$\pi^*$	$\alpha$	$\beta$	Source
1-butyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide, [C <sub>4</sub> mim][BETI]	0.83	0.55	0.42	[21]
1-butyl-3-methylimidazolium hexafluorophosphate, [C <sub>4</sub> mim][PF <sub>6</sub> ]	0.90	0.54	0.44	[21]
1-butyl-3-methylimidazolium tricyanomethanide, [C <sub>4</sub> mim][TCM]	0.94	0.51	0.54	[21]
1-butyl-3-methylimidazolium dicyanamide, [C <sub>4</sub> mim][DCA]	0.98	0.44	0.64	[21]
1-butyl-3-methylimidazolium chloride, [C <sub>4</sub> mim]Cl	1.13	0.32	0.95	[21]
1-butyl-3-methylimidazolium dimethylphosphate, [C <sub>4</sub> mim][(CH <sub>3</sub> ) <sub>2</sub> PO <sub>4</sub> ]	0.98	0.45	1.13	[22]
1-butyl-3-methyl-imidazolium acetate, [C <sub>4</sub> mim][OAc]	0.89	0.57	1.18	[21]

### Density measurements

Density of pure [C<sub>4</sub>mim][PF<sub>6</sub>] was calculated as an average of available literature data reported in the literature [23–25], **Table S5**. The density of the equimolar [C<sub>4</sub>mim][PF<sub>6</sub>]/[C<sub>4</sub>mim]Cl mixture (**Table S6**) was estimated assuming an ideal mixture, following the methodology proposed by Rebelo et al. [26] and previously employed by us [7,12]. For that, the density data available in the literature of pure [C<sub>4</sub>mim]Cl [5,27–35] and [C<sub>4</sub>mim][PF<sub>6</sub>] [23–25] (**Table S5**) were used.

**Table S5.** Overview of the density data of pure [C<sub>4</sub>mim]Cl and pure [C<sub>4</sub>mim][PF<sub>6</sub>] available in the literature at atmospheric pressure (NP: number of data points).

Ionic Liquid	Temperature range (K)	Density range (g · cm <sup>-3</sup> )	NP	Reference
[C <sub>4</sub> mim][PF <sub>6</sub> ]	293.5-414.9	1.370-1.270	10	[23]
	278.2-413.2	1.383-1.274	10	[24]
	293.2-363.2	1.372-1.315	15	[25]
[C <sub>4</sub> mim]Cl	308.2-373.2	1.079-1.044	14	[5]
	313.1-364.8	1.073-1.045	11	[32]
	303.1-363.1	1.080-1.047	13	[31]
	348.2-373.2	1.054-1.041	6	[34]
	348.2-373.2	1.056-1.043	6	[35]
	298.2-333.2	1.082-1.045	4	[28]
	298.2-328.2	1.074-1.056	5	[27]
	343.2-363.2	1.058-1.047	5	[33]
	298.2-318.2	1.082-1.071	3	[30]
	298.2-313.2	1.075-1.063	4	[29]

**Table S6.** Densities ( $\rho$  / g · cm<sup>-3</sup>) for the [C<sub>4</sub>mim][PF<sub>6</sub>]/[C<sub>4</sub>mim]Cl equimolar mixture (estimated).<sup>a</sup>

T / K	[C <sub>4</sub> mim][PF <sub>6</sub> ]/[C <sub>4</sub> mim]Cl
298.15	1.240
303.15	1.237
313.15	1.231
323.15	1.225
333.15	1.218
343.15	1.212
353.15	1.204
363.15	1.198

<sup>a</sup>The uncertainties in temperature and density are:  $u(T) = \pm 0.02$  K, and  $u(\rho) = \pm 5 \times 10^{-4}$  g · cm<sup>-3</sup>.

### Gas-liquid partition coefficients

**Table S7.** Gas–liquid partition coefficients,  $K_L$ , of the solutes in [C<sub>4</sub>mim][PF<sub>6</sub>], [C<sub>4</sub>mim][PF<sub>6</sub>]/[C<sub>4</sub>mim]Cl equimolar mixture, and [C<sub>4</sub>mim]Cl [5,6].<sup>a</sup>

Solute	<i>T / K</i>	[C <sub>4</sub> mim][PF <sub>6</sub> ] <sup>b</sup>						[C <sub>4</sub> mim][PF <sub>6</sub> ]/[C <sub>4</sub> mim]Cl equimolar mixture <sup>c</sup>						[C <sub>4</sub> mim]Cl <sup>d,e</sup>					
		333.15	343.15	353.15	363.15	373.15	383.15	333.15	343.15	353.15	363.15	373.15	383.15	333.15	343.15	353.15	363.15	373.15	383.15
Heptane	3.10	2.49	2.02	1.60	1.40	1.26	-	-	-	-	-	-	-	-	-	-	-	-	-
Octane	6.45	4.80	3.59	2.84	2.36	1.89	2.87	2.19	1.66	1.48	-	-	3.70	2.86	2.24	1.78	1.43	1.16	
Nonane	12.96	9.28	6.91	5.08	4.02	3.07	6.48	4.56	3.33	2.65	2.05	1.65	8.12	5.52	3.84	2.72	1.96	1.44	
Decane	25.55	17.15	12.32	8.94	9.01	6.59	13.86	9.26	6.58	4.99	3.63	2.74	12.09	8.44	6.02	4.37	3.22	2.42	
Cyclohexane	5.68	4.64	3.75	3.12	2.69	2.31	1.97	1.83	1.69	1.60	-	-	4.88	3.97	3.27	2.73	2.30	1.95	
Methylcyclohexane	7.75	6.16	4.79	3.96	3.29	2.77	3.00	2.51	2.11	1.92	-	-	5.99	4.76	3.82	3.11	2.56	2.13	
Benzene	135.68	97.89	72.68	54.79	42.19	32.91	95.75	70.59	53.54	41.50	32.42	26.05	75.65	54.98	40.68	30.60	23.38	18.11	
Toluene	244.94	170.27	121.34	88.64	65.97	50.19	167.07	117.36	84.83	64.48	49.46	37.96	123.41	85.76	60.83	43.98	32.35	24.18	
Ethylbenzene	340.11	227.06	155.79	110.12	79.79	58.92	233.28	157.40	110.92	80.98	58.68	43.33	175.26	118.32	81.67	57.54	41.30	30.17	
p-xylene	437.29	287.67	198.67	139.80	101.72	74.47	290.86	196.04	133.82	95.92	70.85	52.53	184.36	123.89	85.15	59.75	42.72	31.09	
Methyl acetate	98.50	72.23	53.42	40.91	31.52	24.63	55.73	42.36	32.38	25.47	20.21	16.37	33.03	24.67	18.73	14.44	11.28	8.94	
Ethyl acetate	124.88	89.05	64.73	48.14	36.43	27.46	65.28	47.83	36.05	27.72	21.84	17.45	33.72	24.78	18.53	14.08	10.85	8.48	
Vinyl acetate	121.33	86.77	63.60	47.60	36.34	28.25	72.71	53.68	40.53	31.22	24.41	19.61	48.73	35.25	25.97	19.46	14.81	11.43	
THF	106.04	77.89	58.05	44.32	34.45	27.11	60.70	45.75	35.11	27.94	22.08	18.31	35.72	27.03	20.79	16.21	12.82	10.26	
1,4-dioxane	590.75	400.44	279.13	199.17	144.38	107.11	381.14	262.56	184.71	134.23	99.73	75.69	214.11	148.61	105.31	76.05	55.89	41.74	
Diethyl ether	7.74	6.03	4.82	3.93	3.29	2.81	2.67	2.22	1.92	-	-	-	3.77	3.07	2.53	2.11	1.78	1.51	
Acetonitrile	544.69	391.32	290.88	219.01	167.82	130.77	419.35	305.55	226.64	171.36	132.59	104.41	361.27	254.56	182.97	133.92	99.68	75.34	
Pyridine	1100.38	709.15	484.55	331.03	234.76	167.19	844.14	557.50	376.74	264.52	187.46	136.10	906.90	588.91	391.88	266.69	185.28	131.19	
Thiophene	215.50	153.34	112.26	83.92	63.98	49.78	198.35	142.81	104.31	78.28	60.17	46.84	54.74	74.51	103.20	74.51	54.74	40.87	
Acetone	168.65	121.65	91.73	69.87	54.11	41.92	94.87	70.84	53.96	41.69	33.25	26.61	52.36	38.95	29.46	22.63	17.63	13.91	
2-butanone	240.02	169.77	124.07	91.80	69.22	52.99	135.50	98.16	72.97	55.54	42.91	33.90	-	-	-	-	-	-	
Methanol	82.52	60.67	44.87	34.78	27.53	21.49	879.32	584.87	395.50	275.40	197.59	138.71	1955.12	1289.10	870.25	600.34	422.47	302.80	
Ethanol	110.36	80.95	59.45	46.65	37.31	29.11	887.56	582.54	396.32	277.57	201.57	145.14	1655.20	1071.79	711.32	482.86	334.65	236.42	
1-propanol	188.71	134.05	95.54	72.28	55.74	42.45	1551.15	984.73	644.35	439.55	306.23	215.63	2806.67	1750.49	1121.34	736.16	494.31	338.89	
2-propanol	108.17	78.19	57.67	-	34.23	26.53	645.72	422.55	282.05	195.55	140.33	102.92	1066.14	686.01	452.57	305.49	210.60	148.03	
Isobutanol	346.04	236.06	166.45	121.14	89.75	67.14	-	1716.71	1081.52	705.75	478.15	327.83	4868.88	2930.47	1815.24	1154.48	752.27	501.27	
1-butanol	183.22	127.22	91.56	67.90	50.50	38.64	1048.17	660.92	429.19	286.83	200.31	142.13	1625.18	1018.63	655.58	432.28	291.48	200.62	
2-butanol	235.69	163.99	116.51	85.07	63.33	47.94	-	1188.52	758.10	502.77	344.49	242.99	3228.93	1979.75	1247.94	806.89	534.05	361.17	
tert-butanol	92.64	65.78	47.60	35.29	26.86	20.91	381.97	247.50	165.82	114.24	81.52	59.38	626.49	402.73	265.44	179.02	123.31	86.61	
Water	232.15	170.92	131.36	100.53	78.26	63.57	5637.67	-	2193.85	1467.39	1009.63	697.82	23903.05	14085.83	8553.00	5338.11	3416.87	2238.64	
<b>Terpenes/terpenoids</b>	<b>353.15</b>	<b>363.15</b>	<b>373.15</b>	<b>383.15</b>	<b>393.15</b>	<b>403.15</b>	<b>353.15</b>	<b>363.15</b>	<b>373.15</b>	<b>383.15</b>	<b>393.15</b>	<b>403.15</b>	<b>353.15</b>	<b>363.15</b>	<b>373.15</b>	<b>383.15</b>	<b>393.15</b>	<b>403.15</b>	
$\alpha$ -pinene	26.97	20.23	15.40	12.04	9.59	7.75	17.02	15.50	11.71	8.71	6.70	5.89	4.44	3.41	2.66	2.1	1.68	1.35	
$\beta$ -pinene	59.84	44.56	32.08	24.53	18.25	14.32	40.41	32.61	23.83	19.08	14.94	12.34	9.81	7.25	5.44	4.15	3.2	2.51	
Limonene	102.03	71.16	51.41	37.52	28.02	21.26	74.04	54.29	37.40	29.10	23.24	17.18	-	-	-	-	-	-	
Myrcene	91.27	61.76	43.34	31.30	23.16	17.60	63.05	42.09	32.36	22.97	17.77	13.77	-	-	-	-	-	-	
$\gamma$ -terpinene	314.04	210.56	145.13	103.10	75.05	55.73	204.75	143.56	103.18	70.05	52.95	39.21	-	-	-	-	-	-	
p-cymene	140.62	96.38	67.66	48.63	35.69	26.67	103.47	71.68	51.99	37.87	27.49	20.68	-	-	-	-	-	-	

Eucalyptol	186.30	132.14	90.56	65.23	47.84	35.20	109.60	79.77	59.87	40.36	31.02	23.84	19.17	13.76	10.06	7.47	5.63	4.31
<b>Low volatile terpenoids</b>	<b>383.15</b>	<b>393.15</b>	<b>403.15</b>	<b>413.15</b>	<b>423.15</b>	<b>433.15</b>	<b>383.15</b>	<b>393.15</b>	<b>403.15</b>	<b>413.15</b>	<b>423.15</b>	<b>433.15</b>	<b>383.15</b>	<b>393.15</b>	<b>403.15</b>	<b>413.15</b>	<b>423.15</b>	<b>433.15</b>
$\alpha$ -pinene oxide	270.43	190.74	139.98	105.07	79.50	62.12	165.62	120.27	88.66	67.90	52.62	39.35	36.41	25.77	18.56	13.59	10.1	7.61
Fenchone	410.12	291.03	210.22	155.91	118.06	90.09	239.75	171.06	120.52	94.54	71.18	53.25	46.22	32.92	23.85	17.56	13.13	9.94
Menthone	507.24	352.24	249.38	180.61	134.16	101.87	295.31	205.98	147.54	109.59	83.26	64.56	63.63	43.7	30.59	21.79	15.79	11.61
Carvone	1854.64	1230.15	836.01	579.42	413.90	299.54	1270.71	860.46	577.97	409.92	287.44	204.74	372.3	242.83	161.87	110.09	76.29	53.79
Isopulegol	541.77	368.76	257.82	184.10	136.45	101.19	1422.81	889.88	596.52	403.67	270.42	188.94	977.43	597.61	374.64	240.37	157.57	105.37
Citronellol	890.40	565.37	-	263.39	186.51	133.78	3959.04	2349.61	1425.46	918.23	607.59	409.36	3192.98	1828.23	1076.92	651.24	403.53	255.76
Geraniol	1379.30	900.40	590.07	399.07	281.99	199.72	-	3845.17	2367.00	1465.05	935.95	611.33	5610.21	3158.11	1830.5	1090.09	665.66	416.07
Linalool	348.89	238.71	163.47	115.57	83.09	59.89	1136.43	706.95	445.72	296.35	202.39	131.23	845.75	503.77	308.08	193.06	123.75	81.01
Citronellal	439.90	300.53	209.29	148.95	109.58	82.7	277.42	195.44	139.69	110.21	79.98	-	-	-	-	-	-	
Camphor	768.10	537.13	380.46	275.89	204.77	153.55	-	319.26	231.06	173.15	125.68	94.98	104.4	71.6	50.05	35.62	25.77	18.93
Borneol	712.01	476.42	331.39	240.37	174.09	128.03	3041.14	1864.09	1218.97	815.52	544.07	-	2760.58	1635.77	995.42	620.85	396.19	258.24
Menthol	514.57	345.54	234.07	166.99	121.17	89.13	1761.51	1079.08	688.30	463.36	305.72	209.09	1412.22	834.49	506.49	315.12	200.61	130.47
<b>Phenolic Terpenoids</b>	<b>413.15</b>	<b>423.15</b>	<b>433.15</b>	<b>443.15</b>	<b>453.15</b>													
Eugenol	2793.29	1839.16	1276.32	876.73	624.55													
Carvacrol	2007.14	1327.99	896.86	624.45	441.41													
Thymol	1548.37	1034.42	700.96	488.02	350.61													

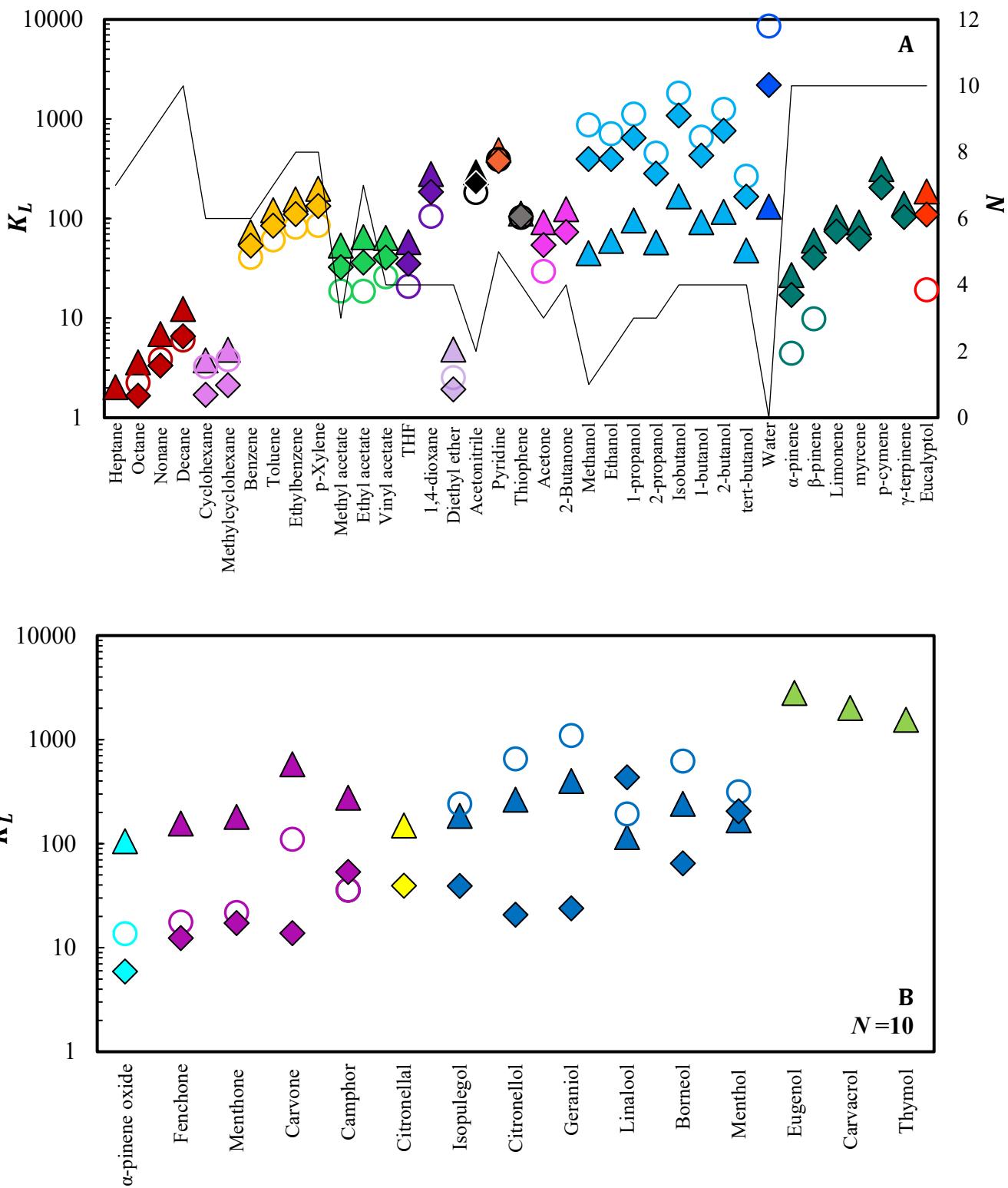
<sup>a</sup>The estimated uncertainties in the pressure and temperature are  $u(T) = 0.1$  K, and  $u(p) = 0.05$ .

<sup>b</sup>Column Packing: 50% of IL,  $n_3 = 9.48$  mmol.

<sup>c</sup>Column Packing: 50% of IL,  $n_3 = 10.75$  mmol.

<sup>d</sup>Column Packing: 51.1% of IL,  $n_3 = 17.02$  mmol.

<sup>e</sup>Extrapolated using the data reported by the authors [5,6].



Limiting partial molar excess properties

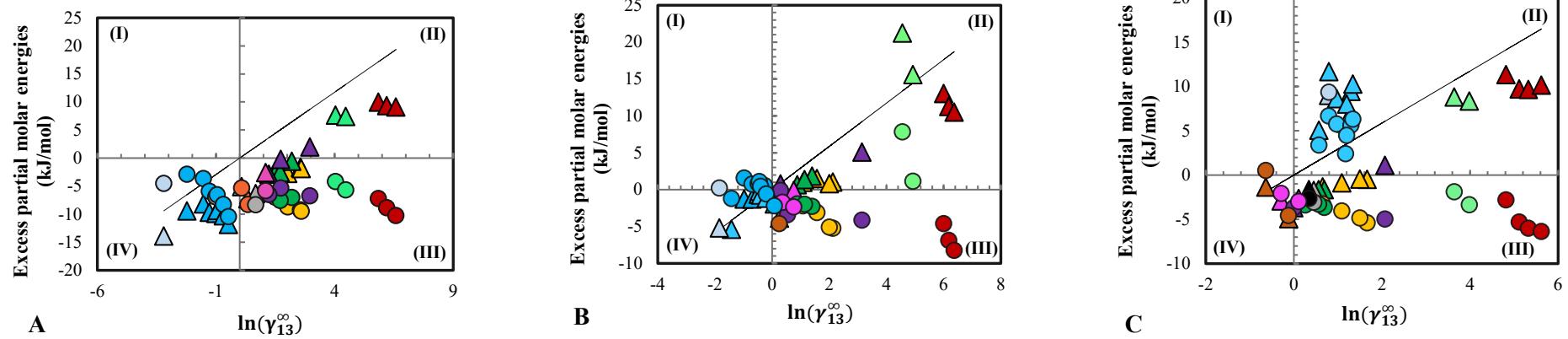
**Table S8.** Thermodynamic functions at infinite dilution: partial molar excess Gibbs free energies ( $\bar{G}_m^{E,\infty}$ /kJ·mol<sup>-1</sup>), partial molar excess enthalpies ( $\bar{H}_m^{E,\infty}$ /kJ·mol<sup>-1</sup>), and partial molar excess entropies ( $T_{ref}\bar{S}_m^{E,\infty}$ /kJ·mol<sup>-1</sup>) of several solutes in [C<sub>4</sub>mim][PF<sub>6</sub>], equimolar [C<sub>4</sub>mim][PF<sub>6</sub>]/[C<sub>4</sub>mim]Cl mixture, and [C<sub>4</sub>mim]Cl [5,6].

Solutes	[C <sub>4</sub> mim][PF <sub>6</sub> ]			[C <sub>4</sub> mim][PF <sub>6</sub> ]/[C <sub>4</sub> mim]Cl equimolar mixture			[C <sub>4</sub> mim]Cl <sup>a,b</sup>		
	$\bar{G}_m^E$	$\bar{H}_m^E$	$T_{ref}\bar{S}_m^E$	$\bar{G}_m^E$	$\bar{H}_m^E$	$T_{ref}\bar{S}_m^E$	$\bar{G}_m^E$	$\bar{H}_m^E$	$T_{ref}\bar{S}_m^E$
	<i>T<sub>ref</sub> = 353.2 K</i>								
Heptane	14.14	11.33	-2.82	-	-	-	-	-	-
Octane	15.03	9.72	-5.31	17.64	13.00	-4.64	17.16	9.94	-7.21
Nonane	15.64	9.64	-6.00	18.14	11.26	-6.88	18.21	9.34	-8.88
Decane	16.51	10.14	-6.37	18.71	10.48	-8.23	19.35	9.07	-10.28
Cyclohexane	10.70	8.81	-1.89	13.39	21.21	7.81	11.85	7.67	-4.19
Methylcyclohexane	11.71	8.35	-3.36	14.47	15.59	1.12	13.12	7.42	-5.70
Benzene	1.93	-1.34	-3.27	3.18	0.98	-2.20	4.38	-2.62	-7.00
Toluene	3.20	-0.87	-4.07	4.61	1.49	-3.12	5.97	-2.74	-8.71
Ethylbenzene	4.90	-0.49	-5.39	6.24	1.02	-5.23	7.53	-1.72	-9.25
p-xylene	4.40	-0.47	-4.87	5.88	0.78	-5.10	7.63	-1.86	-9.49
Methyl acetate	0.77	-2.61	-3.38	2.59	0.65	-1.95	4.58	-2.17	-6.75
Ethyl acetate	2.03	-1.64	-3.67	4.11	1.83	-2.27	6.45	-0.58	-7.03
Vinyl acetate	1.67	-1.64	-3.30	3.34	1.35	-1.99	5.04	-2.54	-7.58
THF	1.32	-1.75	-3.08	0.88	0.77	-0.11	5.08	-0.24	-5.33
1,4-dioxane	0.00	-3.68	-3.68	1.61	-1.79	-3.40	3.61	-2.92	-6.52
Diethyl ether	6.08	1.10	-4.98	9.24	5.09	-4.15	8.71	1.99	-6.72
Acetonitrile	-1.87	-1.37	0.50	-0.79	-0.80	-0.01	0.24	-5.10	-5.35
Pyridine	-0.35	-4.94	-4.59	0.74	-3.87	-4.61	1.01	-7.27	-8.27
Thiophene	1.01	-1.64	-2.65	-0.77	-0.22	0.54	2.00	-6.35	-8.35
Acetone	-0.85	-2.93	-2.08	1.07	-0.65	-1.72	3.23	-2.59	-5.83
2-butanone	0.33	-2.66	-2.98	2.24	-0.13	-2.37	-	-	-
Methanol	1.67	5.05	3.38	-4.17	-5.38	-1.21	-6.53	-9.42	-2.88
Ethanol	2.32	8.98	6.66	-2.85	-1.30	1.56	-4.50	-8.17	-3.67
1-propanol	0.00	8.84	8.84	-2.06	-1.31	0.76	-3.74	-9.66	-5.93
2-propanol	2.86	8.61	5.75	-1.42	-0.63	0.79	-2.90	-9.85	-6.95
Isobutanol	3.81	9.45	5.65	-1.31	-0.22	1.09	-2.95	-9.85	-6.90

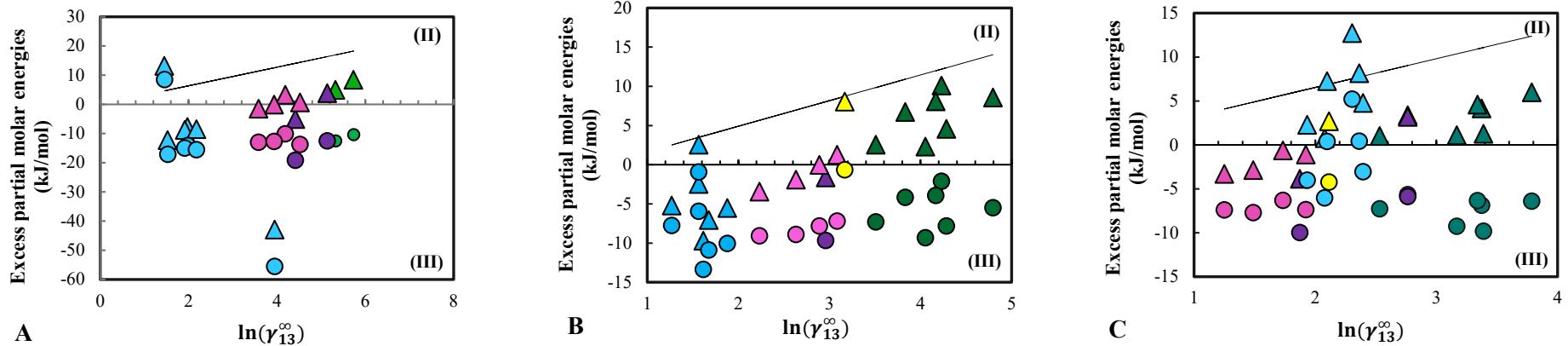
1-butanol	3.93	10.25	6.32	-1.17	-0.73	0.44	-2.78	-9.35	-6.57
2-butanol	3.52	8.00	4.48	-0.59	-1.18	-0.59	-2.02	-10.28	-8.26
<i>tert</i> -butanol	3.45	5.86	2.40	0.24	-1.95	-2.20	-1.39	-11.84	-10.45
Water	2.33	11.67	9.34	-5.40	-5.20	0.20	-9.39	-13.93	-4.53
<b>Terpenes and Terpenoids</b>									
							<b>T<sub>ref</sub> = 383.2 K</b>		
$\alpha$ -pinene	12.26	5.97	-6.29	13.75	8.55	-5.20	18.27	7.96	-10.31
$\beta$ -pinene	10.92	4.15	-6.77	12.08	10.08	-2.00	16.98	4.66	-12.32
Limonene	10.77	4.57	-6.20	12.03	8.06	-3.97	-	-	-
Myrcene	10.82	1.24	-9.59	12.22	4.54	-7.68	-	-	-
$\gamma$ -terpinene	10.10	1.09	-9.02	11.32	2.29	-9.02	-	-	-
<i>p</i> -cymene	8.08	1.00	-7.08	9.73	2.52	-7.22	-	-	-
Eucalyptol	8.86	3.37	-5.49	10.88	6.71	-4.18	16.20	3.41	-12.79
$\alpha$ -pinene oxide	5.84	3.16	-9.71	13.75	-1.64	-9.44	14.08	-5.09	-19.17
Fenchone	5.50	-3.87	-6.15	7.79	-0.03	-7.63	13.35	3.20	-10.15
Menthone	6.11	-0.66	-7.21	7.60	1.24	-6.98	14.41	0.64	-13.77
Carvone	3.91	-1.10	-7.24	8.22	-3.45	-8.96	11.43	-1.55	-12.98
Isopulegol	6.21	-3.33	-3.92	5.51	-7.09	-7.09	6.31	-7.76	-14.07
Citronellol	7.67	2.29	0.48	0.00	-2.47	-5.78	6.09	-8.80	-14.89
Geraniol	6.92	8.15	0.31	3.31	-5.24	-5.24	4.86	-12.26	-17.13
Linalool	6.71	7.23	-5.96	0.00	-9.73	-13.08	12.58	-42.92	-55.50
Citronellal	6.82	0.75	-4.15	3.35	8.04	-0.64	-	-	-
Camphor	4.70	2.67	-7.57	8.68	-1.26	-1.26	12.54	-0.16	-12.70
Borneol	7.63	-2.86	5.08	0.00	2.53	-0.87	4.63	13.18	8.55
Menthol	7.79	12.71	-3.04	3.40	-4.94	-9.21	6.94	-8.55	-15.49
<b>Phenolic Terpenoids</b>									
							<b>T<sub>ref</sub> = 413.2 K</b>		
Eugenol	4.01	-9.59	-13.60	-	-	-	-	-	-
Carvacrol	2.02	-9.55	-11.57	-	-	-	-	-	-
Thymol	2.10	-5.81	-7.92	-	-	-	-	-	-

<sup>a</sup>The partial molar thermodynamic functions of water and organic solutes in [C<sub>4</sub>mim]Cl were calculated from the  $\gamma_{13}^{\infty}$  data obtained in the temperature range of 358.15–388.15 K, reported by Martins et al. [5].

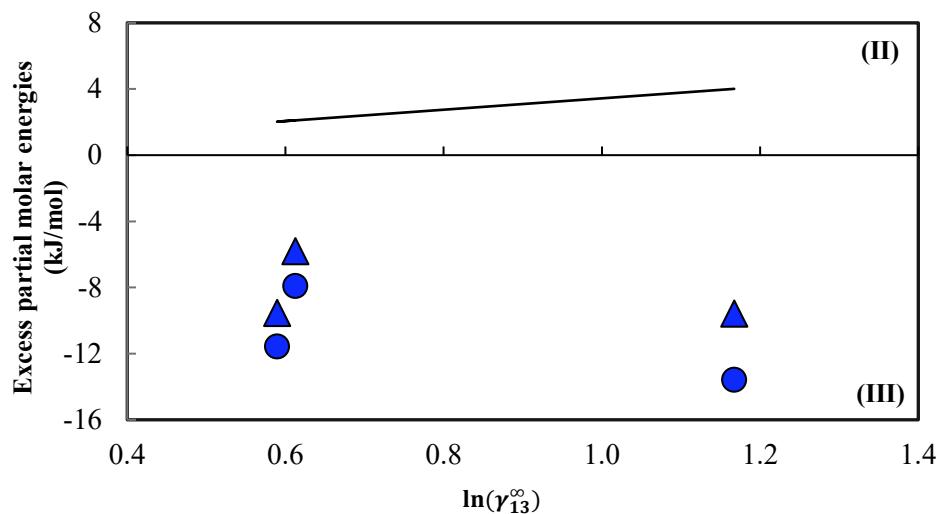
<sup>b</sup>The partial molar thermodynamic functions of terpenes and terpenoids in [C<sub>4</sub>mim]Cl were calculated from the  $\gamma_{13}^{\infty}$  data obtained in the temperature range of 398.15–448.15 K, reported by Martins et al. [6].



**Figure S4.** Partial molar excess properties at 353.15 K of the studied organic solutes as a function of  $\ln(\gamma_{13}^{\infty})$  for A,  $[\text{C}_4\text{mim}]\text{Cl}$  (interpolated values from [5]); B,  $[\text{C}_4\text{mim}]\text{Cl}/[\text{C}_4\text{mim}]\text{[PF}_6]$  equimolar mixture; and C,  $[\text{C}_4\text{mim}]\text{[PF}_6]$ . The solid line represents  $\bar{G}_m^{E,\infty}$ , the triangles correspond to  $\bar{H}_m^{E,\infty}$ , and the circles are  $T_{ref}\bar{S}_m^{E,\infty}$ . Color code: ●, alkanes; ●, cycloalkanes; ●, aromatic hydrocarbons; ●, ethers; ●, esters; ●, ketones; ●, alcohols; ●, water; ●, acetonitrile and pyridine; and ●, thiophene.



**Figure S5.** Partial molar excess properties at 393.15 K of the studied terpenes and terpenoids as a function of  $\ln(\gamma_{13}^{\infty})$  for A,  $[\text{C}_4\text{mim}]\text{Cl}$  (interpolated values from [6]); B,  $[\text{C}_4\text{mim}]\text{Cl}/[\text{C}_4\text{mim}]\text{[PF}_6]$  equimolar mixture; and C,  $[\text{C}_4\text{mim}]\text{[PF}_6]$ . The solid line represents  $\bar{G}_m^{E,\infty}$ , the triangles correspond to  $\bar{H}_m^{E,\infty}$ , and the circles are  $T_{ref}\bar{S}_m^{E,\infty}$ . Color code: ●, alcohol terpenoids; ●, ketone terpenoids; ●, ether terpenoids; ●, citronellal; ●, hydrocarbon terpenes.



**Figure S6.** Partial molar excess properties as a function of  $\ln(\gamma_{13}^\infty)$  for phenolic terpenoids in  $[\text{C}_4\text{mim}][\text{PF}_6]$  at 413.2 K. The solid line represents  $\bar{G}_m^{E,\infty}$ , the triangles correspond to  $\bar{H}_m^{E,\infty}$ , and the circles are the  $T_{ref}\bar{S}_m^{E,\infty}$ .

Fractionation factors

**Table S9.** Selectivities ( $S_{ij}^{\infty}$ ), capacities ( $k_j^{\infty}$ ), and solvent performance indexes ( $Q_{ij}^{\infty}$ ) at infinite dilution for different terpenes mixtures in ILs at 403.2 K.<sup>a</sup>

Ionic Liquid	$S_{ij}^{\infty}/k_j^{\infty}/Q_{ij}^{\infty}$							Source
	$\alpha$ -pinene/ $\beta$ -pinene	$\beta$ -pinene/limonene	$p$ -cymene/limonene	limonene/linalool	menthol/menthone	borneol/camphor	limonene/carvone	
[C <sub>4</sub> mim][PF <sub>6</sub> ]	1.49/0.03/0.05	1.04/0.04/0.04	1.25/0.08/0.10	3.46/0.13/0.43	1.55/0.14/0.22	2.00/0.22/ 0.44	7.71/0.28/2.16	This work
[C <sub>4</sub> mim][PF <sub>6</sub> ]/ [C <sub>4</sub> mim]Cl	1.69/0.03/0.04	1.02/0.03/0.03	1.93/0.05/0.10	11.73/0.30/3.54	3.21/0.24/0.78	3.02/0.36/ 1.08	6.63/0.17/1.13	This work
[C <sub>4</sub> mim]Cl	1.41/0.01/0.01	-	-	-	9.05/0.89/8.05	14.77/4.24/62.62	-	[6] <sup>b</sup>
[P <sub>6,6,6,14</sub> ]Cl	1.14/0.99/1.13	1.12/0.99/1.11	1.04/0.88/0.92	10.20/9.01/91.88	10.16/11.72/119.14	7.48/14.15/105.90	1.23/1.09/1.34	
[P <sub>6,6,6,14</sub> ][(C <sub>8</sub> H <sub>17</sub> ) <sub>2</sub> PO <sub>2</sub> ]	1.07/1.59/1.69	1.15/1.59/1.82	1.03/1.38/1.42	5.93/8.20/ 48.64	-	-	1.24/1.38/1.71	[7]
[C <sub>4</sub> mim][OAc]	1.33/0.06/0.08	1.35/0.06/0.08	1.62/0.07/0.11	-	-	-	5.38/0.23/1.21	
[C <sub>8</sub> mim]Cl	1.37/0.08/0.11	1.07/0.09/0.09	1.34/0.12/0.15	15.40/1.34/ 20.61	11.62/1.76/20.43	16.86/3.21/54.11	3.46/0.30/1.04	
[C <sub>4</sub> mim]Cl/[C <sub>12</sub> mim]Cl	1.38/0.11/0.15	1.04/0.11/0.11	1.22/0.13/0.16	14.06/1.54/21.62	11.79/1.97/23.21	18.11/3.28/59.32	3.07/0.34/1.03	[16]
[C <sub>12</sub> mim]Cl	1.24/0.24/0.29	1.01/0.24/0.29	1.06/0.25/0.27	9.65/2.27/ 21.88	8.48/2.39/20.25	12.54/4.04/ 50.64	1.81/0.43/0.77	

<sup>a</sup> $j$  = solute with the lowest activity coefficient in each separation pair.

<sup>b</sup>Interpolated using the data reported by the authors.

**Table S10.** Selectivities ( $S_{ij}^{\infty}$ ), capacities ( $k_j^{\infty}$ ), and solvent performance indexes ( $Q_{ij}^{\infty}$ ) at infinite dilution for selected mixtures involving phenolic terpenoids in [C<sub>4</sub>mim][PF<sub>6</sub>] and [C<sub>4</sub>mim][CF<sub>3</sub>SO<sub>3</sub>] at 413.2 K.

Mixture	Ionic liquid	$S_{ij}^{\infty}$	$k_j^{\infty}$	$Q_{ij}^{\infty}$	Source
linalool/thymol	[C <sub>4</sub> mim][PF <sub>6</sub> ]	4.75	0.54	2.57	This work
	[C <sub>4</sub> mim][CF <sub>3</sub> SO <sub>3</sub> ]	113.53 <sup>a</sup>	1.57 <sup>a</sup>	178.22 <sup>a</sup>	[6]
linalool/eugenol	[C <sub>4</sub> mim][PF <sub>6</sub> ]	2.73	0.31	0.85	This work
	[C <sub>4</sub> mim][CF <sub>3</sub> SO <sub>3</sub> ]	55.58 <sup>a</sup>	0.77 <sup>a</sup>	42.7 <sup>a</sup>	[6]
eucalyptol/eugenol	[C <sub>4</sub> mim][PF <sub>6</sub> ]	4.73 <sup>b</sup>	0.31	1.47 <sup>b</sup>	This work
	[C <sub>4</sub> mim][CF <sub>3</sub> SO <sub>3</sub> ]	9.47 <sup>a</sup>	0.77 <sup>a</sup>	7.28 <sup>a</sup>	[6]
$\alpha$ -pinene/carvacrol	[C <sub>4</sub> mim][PF <sub>6</sub> ]	22.82 <sup>b</sup>	0.55	12.66 <sup>b</sup>	This work
	[C <sub>4</sub> mim][CF <sub>3</sub> SO <sub>3</sub> ]	35.25 <sup>a</sup>	1.58 <sup>a</sup>	55.83 <sup>a</sup>	[6]
$\alpha$ -pinene/thymol	[C <sub>4</sub> mim][PF <sub>6</sub> ]	22.30 <sup>b</sup>	0.54	12.09 <sup>b</sup>	This work
	[C <sub>4</sub> mim][CF <sub>3</sub> SO <sub>3</sub> ]	34.94	1.57	54.85	[6]
$\beta$ -pinene/carvacrol	[C <sub>4</sub> mim][PF <sub>6</sub> ]	15.22 <sup>b</sup>	0.55	8.44 <sup>b</sup>	This work
	[C <sub>4</sub> mim][CF <sub>3</sub> SO <sub>3</sub> ]	27.38 <sup>a</sup>	1.58 <sup>a</sup>	43.36 <sup>a</sup>	[6]
$\beta$ -pinene/thymol	[C <sub>4</sub> mim][PF <sub>6</sub> ]	14.88 <sup>b</sup>	0.54	8.07 <sup>b</sup>	This work
	[C <sub>4</sub> mim][CF <sub>3</sub> SO <sub>3</sub> ]	27.14 <sup>a</sup>	1.57 <sup>a</sup>	42.60 <sup>a</sup>	[6]
$\gamma$ -terpinene/carvacrol		6.90 <sup>b</sup>	0.55	3.80 <sup>b</sup>	
$\gamma$ -terpinene/thymol		6.74 <sup>b</sup>	0.54	3.65 <sup>b</sup>	
myrcene/carvacrol		16.19 <sup>b</sup>	0.55	8.98 <sup>b</sup>	
myrcene/thymol		15.83 <sup>b</sup>	0.54	8.58 <sup>b</sup>	
limonene/carvacrol	[C <sub>4</sub> mim][PF <sub>6</sub> ]	14.74 <sup>b</sup>	0.55	8.17 <sup>b</sup>	This work
limonene/thymol		14.40 <sup>b</sup>	0.54	7.81 <sup>b</sup>	
<i>p</i> -cymene/carvacrol		13.01 <sup>b</sup>	0.55	7.21 <sup>b</sup>	
<i>p</i> -cymene/thymol		12.71 <sup>b</sup>	0.54	6.89 <sup>b</sup>	

<sup>a</sup>Interpolated values using the data reported by the authors.

<sup>b</sup>Extrapolated values using the experimental data measured in this work.

**Table S11.** Selectivities ( $S_{ij}^{\infty}$ ), capacities ( $k_j^{\infty}$ ), and solvent performance indexes ( $k_j^{\infty}$ ) at infinite dilution for selected mixtures of organic compounds relevant in fuel separation problems, in methylimidazolium-based ionic liquids, at 333.2 K.

Ionic Liquid	$S_{ij}^{\infty} / k_j^{\infty} / Q_{ij}^{\infty}$				Source
	octane/benzene	cyclohexane/benzene	octane/thiophene	octane/pyridine	
[C <sub>4</sub> mim][PF <sub>6</sub> ]	103.77/0.53/55.02	24.11/0.53/12.78	143.39/0.73/105.07	241.90/1.24/299.02	This work
	42.56/0.47/19.98	9.38/0.47/4.40	56.66/0.63/35.41	122.51/1.35/165.56	[18]
[C <sub>4</sub> mim][PF <sub>6</sub> ]/[C <sub>4</sub> mim]Cl	164.36/0.33/54.55	49.00/0.33/16.17	296.25/0.60/177.22	416.53/0.84/350.34	This work
[C <sub>4</sub> mim]Cl	100.36/0.24/23.83	15.72/0.24/3.77	243.46/0.58/140.22	347.99/0.82/286.43	[5] <sup>a</sup>
[C <sub>4</sub> mim][SCN]	93.56/0.58/54.72	16.49/0.58/9.64	156.86/0.98/153.79	-	[36] <sup>b</sup>
[C <sub>4</sub> mim][CF <sub>3</sub> SO <sub>3</sub> ]	38.36/0.63/24.13	10.18/0.63/6.41	52.58/0.86/45.33	-	[37] <sup>b</sup>
[C <sub>4</sub> mim][DCA]	63.31/0.50/31.82	12.38/0.50/6.22	100.40/0.80/80.00	137.70/0.92/126.00	[38] <sup>b</sup>
[C <sub>4</sub> mim][BETI]	18.51/0.98/18.26	6.45/0.98/6.36	19.25/1.02/19.74	46.00/2.45/112.76	[39] <sup>b</sup>
[C <sub>4</sub> mim][OAc]	33.28/0.39/12.95	7.88/0.39/3.07	69.54/0.81/56.54	67.88/0.79/53.88	[7]
[C <sub>4</sub> mim][CH <sub>3</sub> SO <sub>3</sub> ]	55.46/0.32/18.01	5.99/0.32/1.94	99.32/0.58/57.75	15.63/0.09/1.43	[5] <sup>a</sup>
[C <sub>4</sub> mim][(CH <sub>3</sub> ) <sub>2</sub> PO <sub>4</sub> ]	20.55/0.43/8.82	5.27/0.43/2.26	38.62/0.81/31.15	40.59/0.85/34.40	[5] <sup>a</sup>
[C <sub>4</sub> mim][TOS]	14.79/0.51/7.55	8.32/0.51/4.24	57.57/0.90/51.86	-	[40] <sup>b</sup>
[C <sub>4</sub> mim][TCM]	45.35/0.77/34.88	10.19/0.77/7.84	62.84/1.07/67.00	96.79/1.64/158.95	[41] <sup>b</sup>
[C <sub>4</sub> mim][DBP]	6.83/1.07/7.30	3.05/1.07/3.30	-	-	[42]
[C <sub>8</sub> mim]Cl	27.91/0.48/13.45	19.80/0.48/9.54	53.62/0.93/49.65	59.51/1.03/61.17	
[C <sub>4</sub> mim]Cl/[C <sub>12</sub> mim]Cl	13.06/0.50/6.56	10.34/0.50/5.19	23.96/0.92/22.06	23.17/0.89/20.63	[16]
[C <sub>12</sub> mim]Cl	4.91/0.82/4.04	3.27/0.82/2.70	7.38/1.24/9.13	5.77/0.97/5.59	

<sup>a</sup>Extrapolated using the data reported by the authors.

<sup>b</sup>Interpolated using the data reported by the authors.

**Table S12.** Selectivities ( $S_{ij}^{\infty}$ ) at infinite dilution for selected mixtures of organic compounds in eutectic mixtures [43] and in  $[\text{C}_4\text{mim}] \text{Cl}/[\text{C}_4\text{mim}] [\text{PF}_6]$  equimolar mixture at 298.2 K.

	decane/butanol	decane/benzene	ethyl acetate/butanol	cyclohexane/benzene	Reference
$[\text{Ch}] \text{Cl} + \text{Glycerol}$ (1:1)	90	31	3	8.4	[43]
$[\text{Ch}] \text{Cl} + \text{Glycerol}$ (1:2)	62	27	2.1	6.4	[43]
$[\text{C}_4\text{mim}] [\text{PF}_6]/[\text{C}_4\text{mim}] \text{Cl}$	1653	287	8	72	This work

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