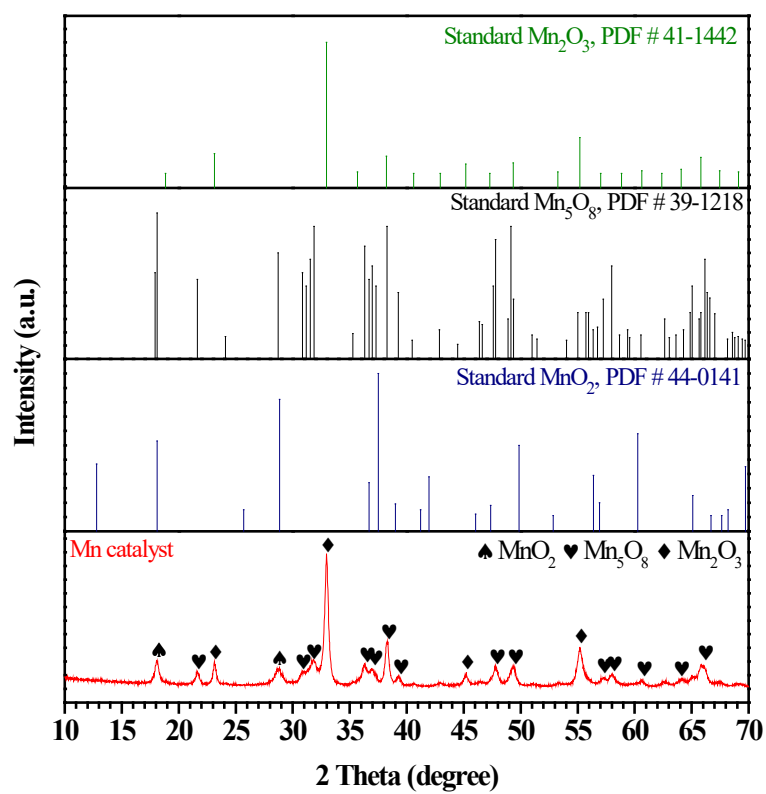
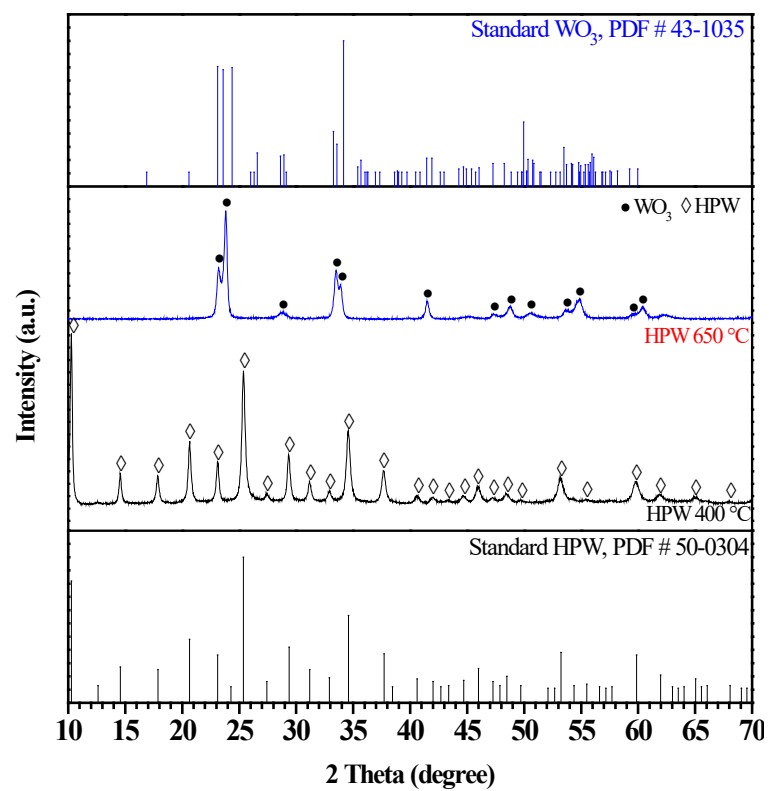


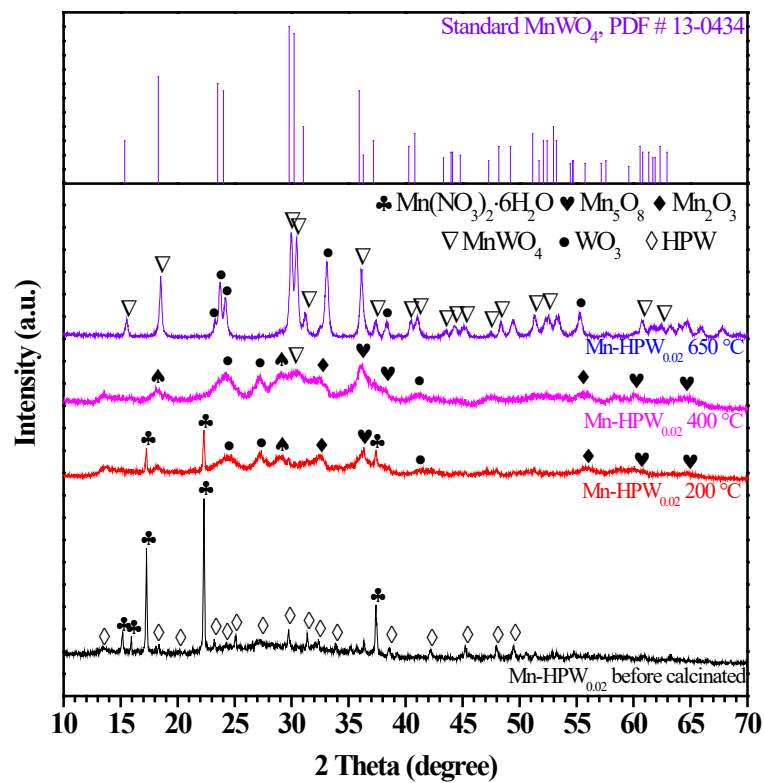
## Supporting Information



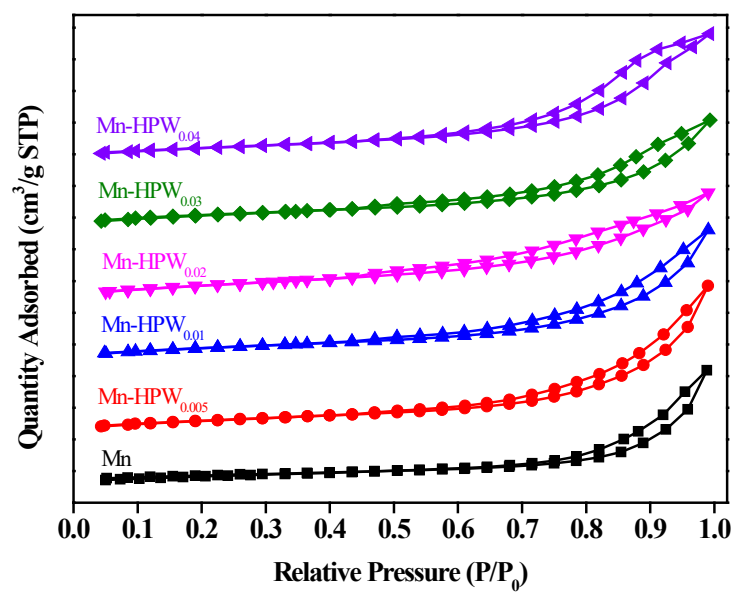
**Figure S1.** XRD patterns of the Mn samples and the standard patterns of  $\text{MnO}_2$ ,  $\text{Mn}_5\text{O}_8$ , and  $\text{Mn}_2\text{O}_3$  phases.



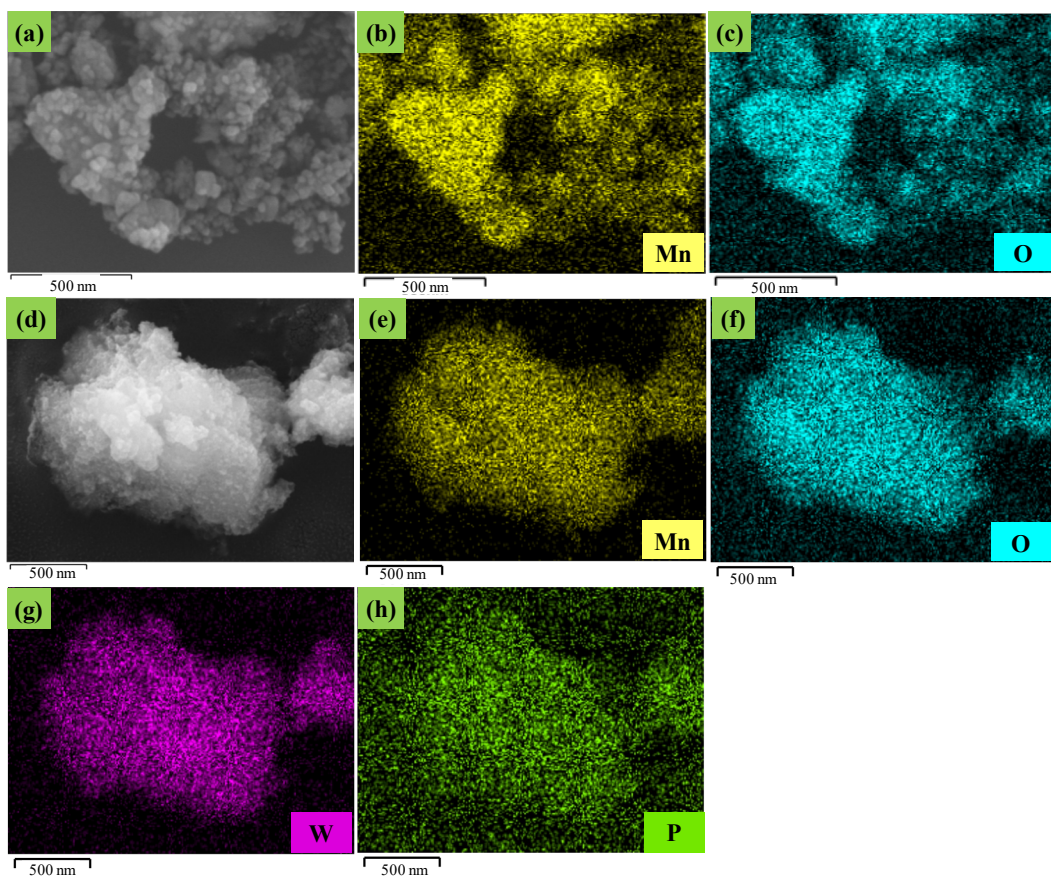
**Figure S2.** XRD patterns of HPW calcinated at 400 °C and 650 °C; the standard patterns of HPW and  $\text{WO}_3$  phases.



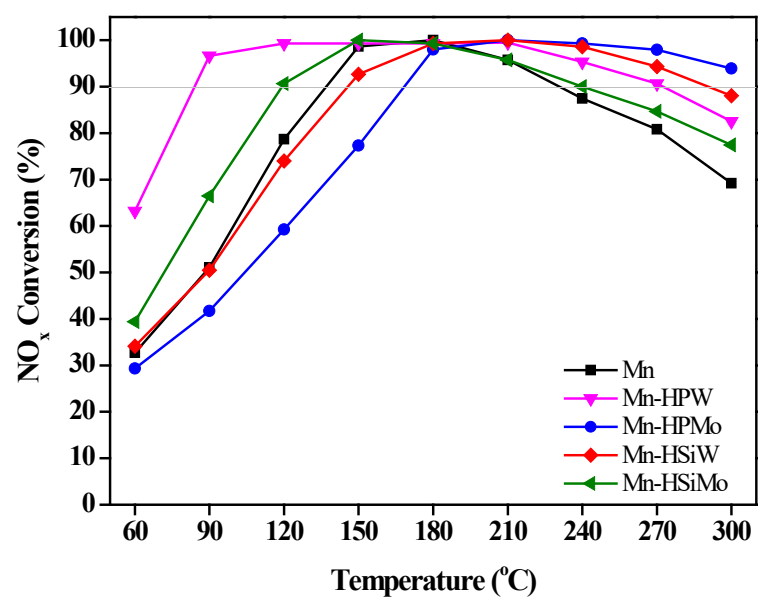
**Figure S3.** XRD patterns of Mn-HPW<sub>0.02</sub> before calcination, Mn-HPW<sub>0.02</sub> calcinated at 200 °C, 400 °C, and 650 °C; the standard patterns of MnWO<sub>4</sub> phases.



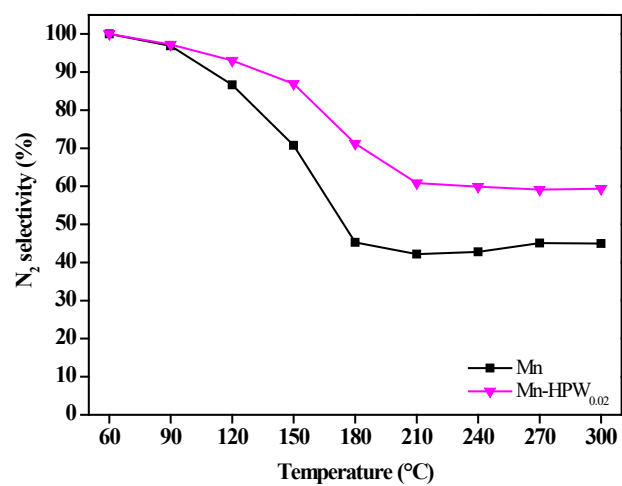
**Figure S4.** N<sub>2</sub> adsorption-desorption isotherms on the Mn and Mn-HPW<sub>x</sub> catalysts.



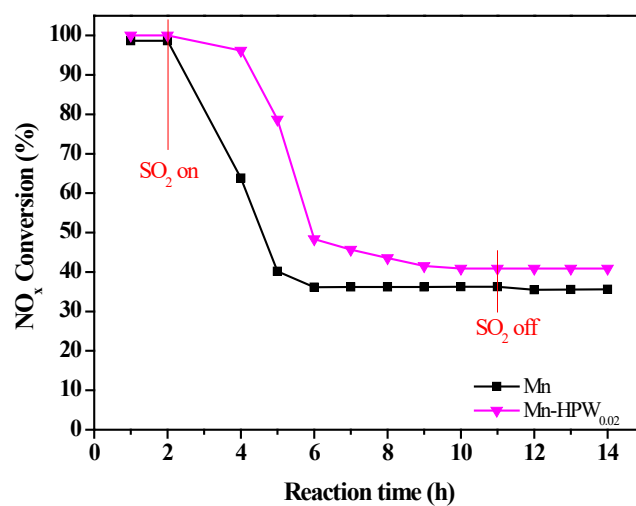
**Figure S5.** EDX mapping of Mn (a-c) and Mn-HPW<sub>0.02</sub> (d-h).



**Figure S6.** NH<sub>3</sub>-SCR activity on Mn, Mn-HPW, Mn-HPMo, Mn-HSiW, and Mn-HSiMo at 60-300 °C.



**Figure S7.** N<sub>2</sub> selectivity on the Mn and Mn-HPW<sub>0.02</sub> catalysts at 60-300 °C.

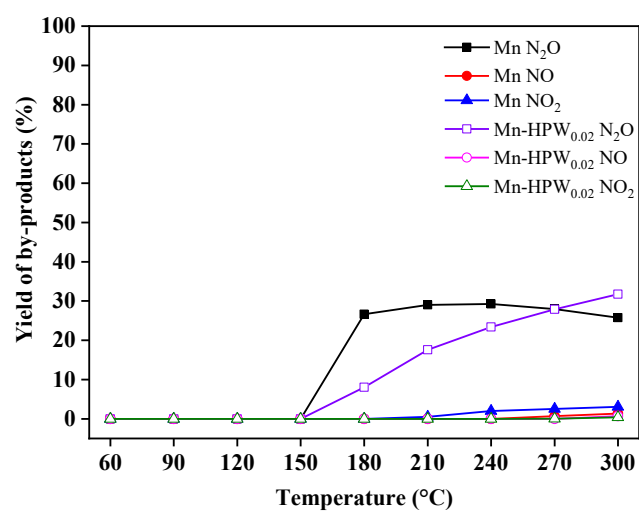


**Figure S8.** Effect of 50 ppm SO<sub>2</sub> on NH<sub>3</sub>-SCR activity over the Mn and Mn-HPW<sub>0.02</sub> catalysts at 150 °C.



**Table S1.** Representative Mn-based catalysts decorated by different assistant for NH<sub>3</sub>-SCR.

Catalyst	NO <sub>x</sub> conversion	Reaction condition							Reference
		[NO]	[NH <sub>3</sub> ]	[O <sub>2</sub> ]	Flow rate	GHSV (h <sup>-1</sup> )	WHSV (mL/g·h)	Weight (g)	
		(ppm)	(ppm)	(%)	(mL/min)				
Mn-Nb	> 90% (125-200 °C)	500	500	5	500	50,000	——	——	[58]
Mn-Co	> 90% (125-350 °C)	500	500	3	210	38,000	——	0.40	[30]
Mn-Sm	> 90% (75-200 °C)	500	500	5	——	48,600	——	0.30	[53]
Mn-Fe	~100% (120-240 °C)	500	500	5	600	36,000	——	0.47	[28]
Mn-Eu	> 90% (100-400 °C)	600	600	5	1000	108,000	——	0.28	[59]
Mn-Cu	> 90% (125-225 °C)	500	500	3	200	100,000	——	0.15	[60]
Mn-Ni	~100% (150-300 °C)	600	600	5	375	45000	——	——	[61]
Mn-Ce	> 90% (120-180°C)	500	500	2	100	11,000	30,000	0.20	[62]
Mn-Ce	> 90% (100-400 °C)	500	500	5	200	32,000	——	——	[63]
Mn-HPW <sub>0.02</sub>	> 90% (90-270 °C)	500	500	5	200	——	80,000	0.15	In this work

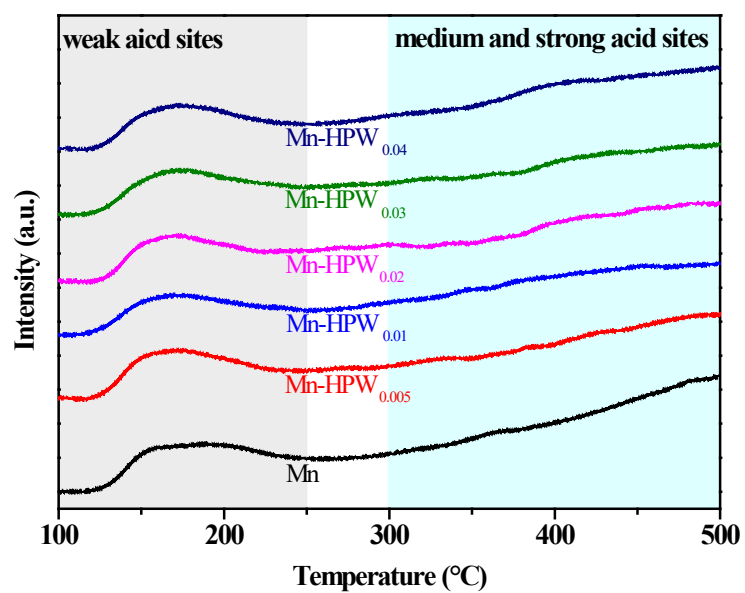


**Figure S9.** Yield of N<sub>2</sub>O, NO, and NO<sub>2</sub> on Mn and Mn-HPW<sub>0.02</sub> at 60-300 °C.

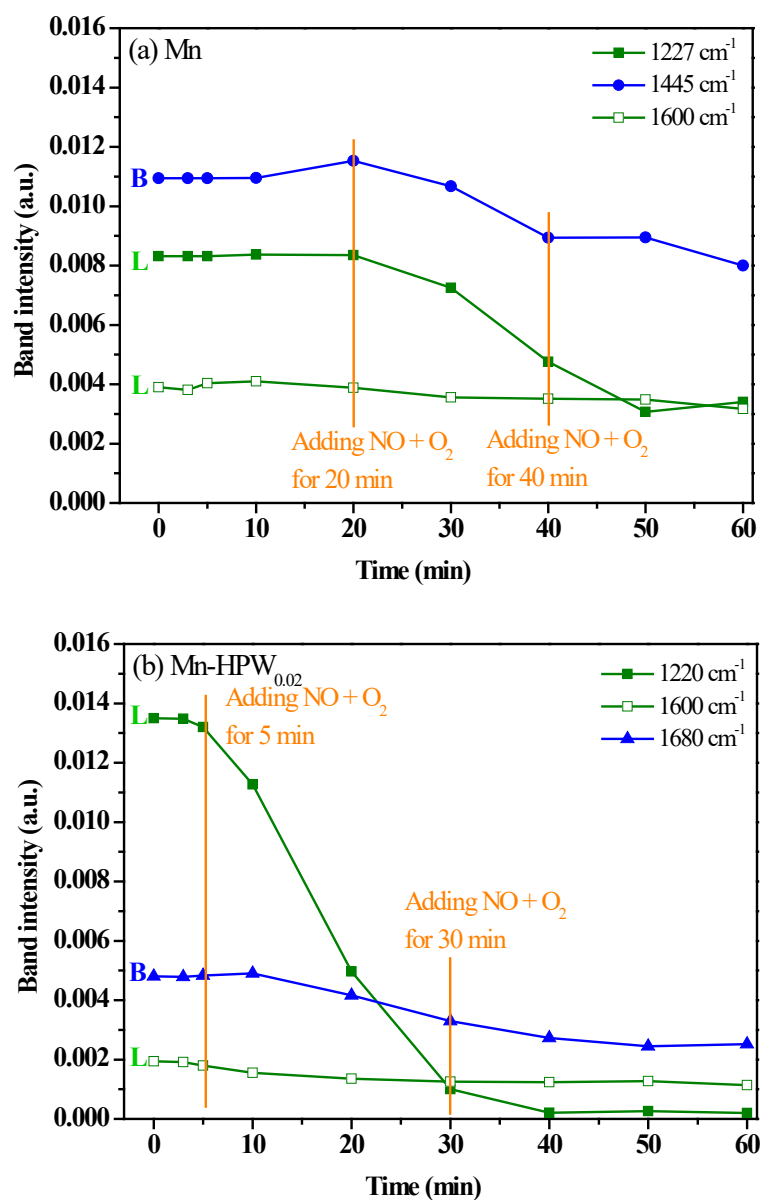
**Table S2** Reduction temperature and relative ratio in H<sub>2</sub>-TPR curves.

Catalyst	Reduction temperature (°C)		Relative ratio	
	Peak I	Peak II	Peak I	Peak II
Mn	315	470	1.00 *	1.00 *
Mn-HPW <sub>0.005</sub>	315	470	0.62	0.91
Mn-HPW <sub>0.01</sub>	315	480	0.55	0.66
Mn-HPW <sub>0.02</sub>	315	490	0.51	0.60
Mn-HPW <sub>0.03</sub>	315	470	0.34	0.31
Mn-HPW <sub>0.04</sub>	308	470	0.18	0.27

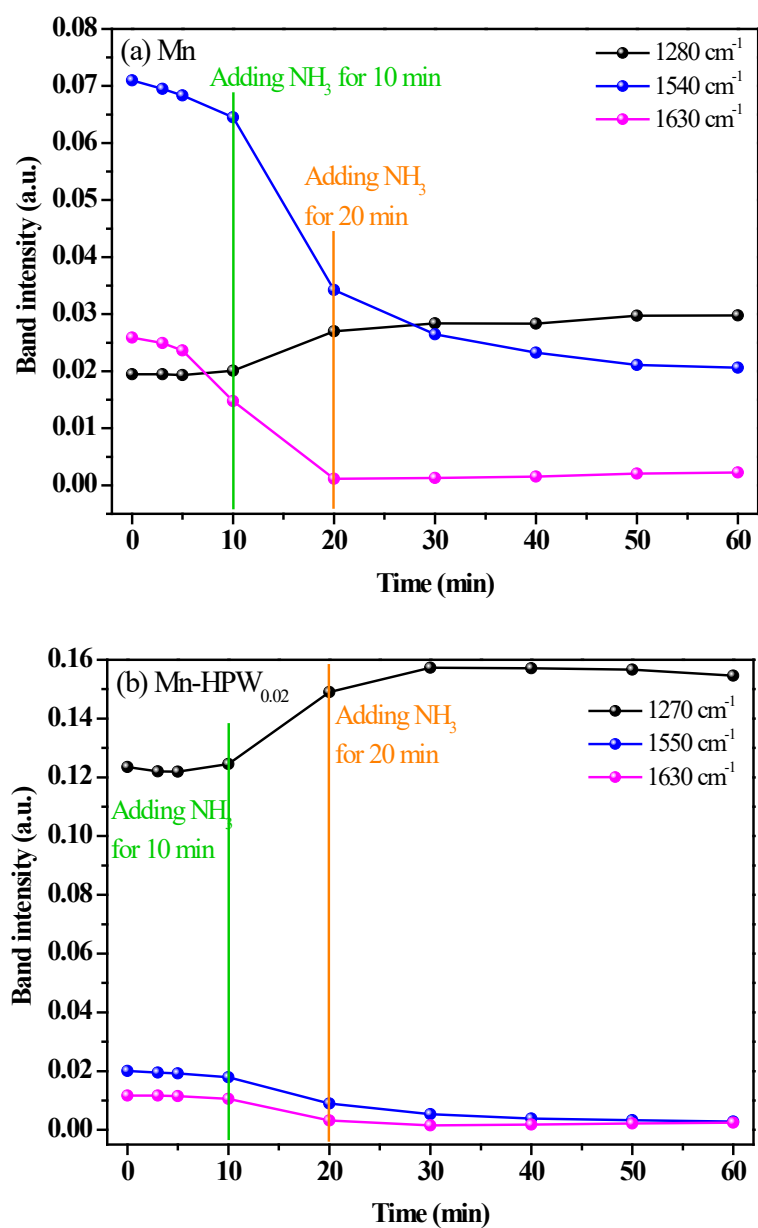
\* The area of peak I and peak II over the Mn catalyst is set as 1.00, respectively, compare with other catalysts.



**Figure S10.** NH<sub>3</sub>-TPD profiles of the Mn and Mn-HPW<sub>x</sub> catalysts.



**Figure S11.** Dependence of the band intensities of NH<sub>3</sub>-derived species on time over Mn (a) and Mn-HPW<sub>0.02</sub> (b).



**Figure S12.** Dependence of the band intensities of the NO<sub>x</sub>-derived species on time over Mn (a) and Mn-HPW<sub>0.02</sub> (b).