

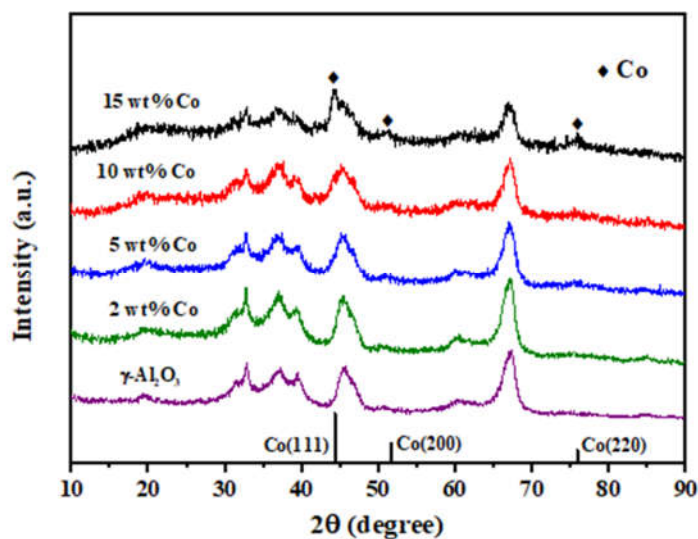
## Supporting Information

### Structural Requirements for Chemoselective Ammonolysis of Ethylene Glycol to Ethanolamine over Supported Cobalt Catalysts

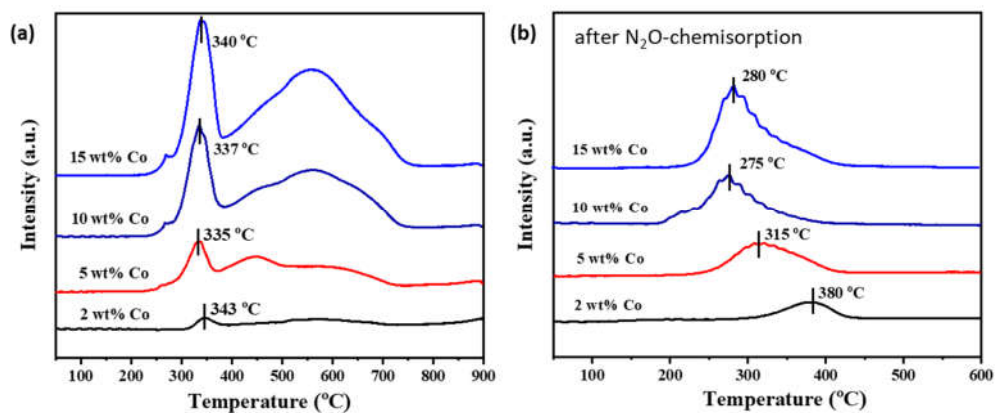
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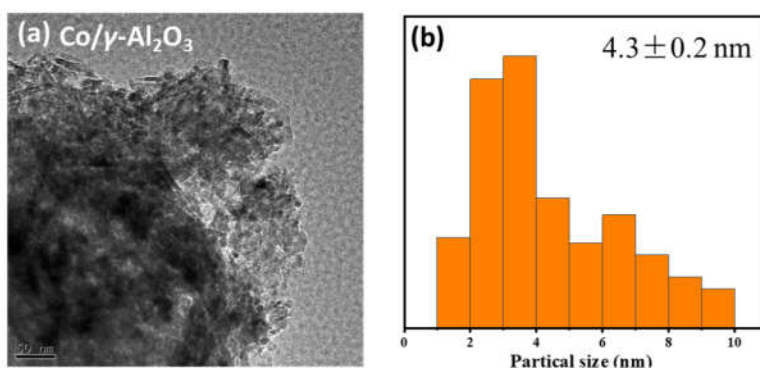
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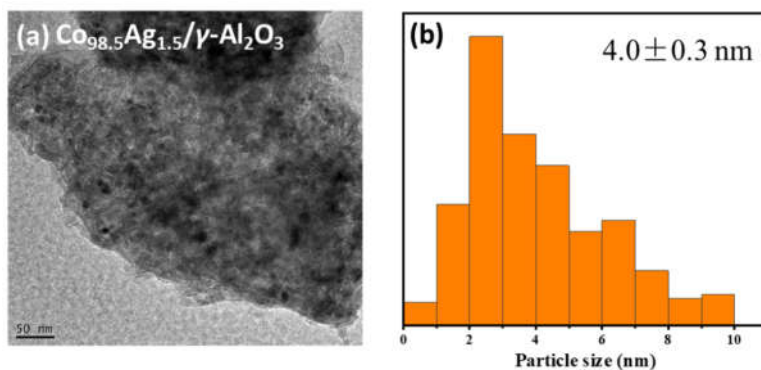
**Fig. S1.** Powder XRD patterns for Co/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> samples (Co 2 wt%-15 wt%) and the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> support with metallic Co (JCPDS 15-0806) as reference.



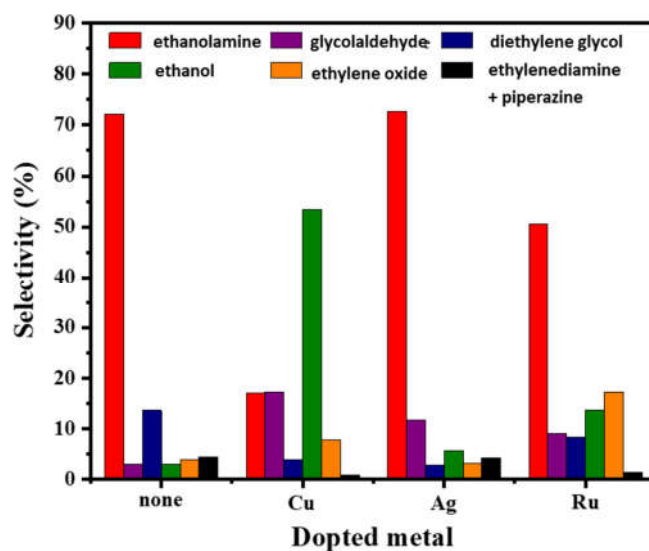
**Fig. S2.** H<sub>2</sub>-TPR profiles for (a) the oxide persursors of the Co/γ-Al<sub>2</sub>O<sub>3</sub> catalysts (Co 2 wt%-15 wt%) and (b) the Co/γ-Al<sub>2</sub>O<sub>3</sub> catalysts after treated in flowing 5% N<sub>2</sub>O/N<sub>2</sub> at 323 K for 1 h.



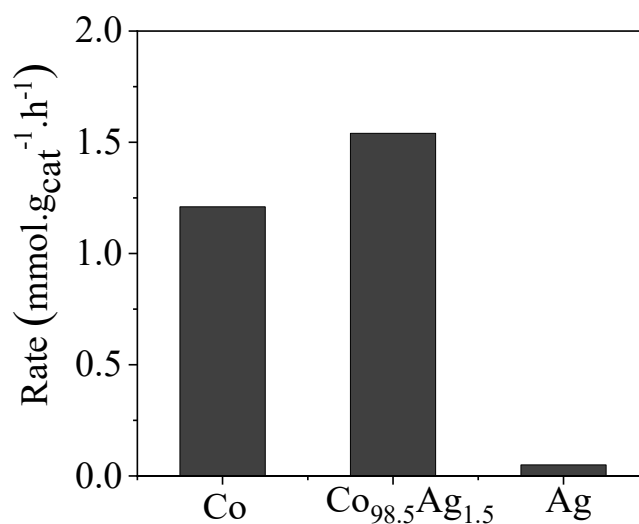
**Fig. S3.** TEM image for (a) 5 wt% Co/γ-Al<sub>2</sub>O<sub>3</sub> with (b) the corresponding statistic size distribution of the Co nanoparticles.



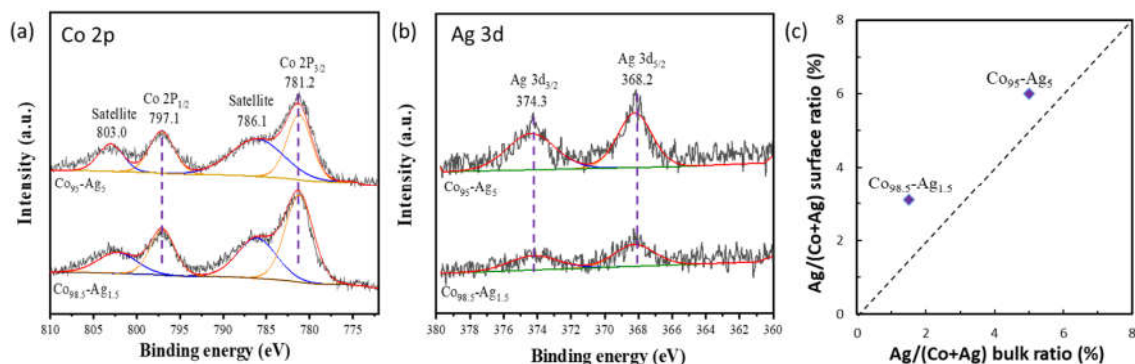
**Fig. S4.** TEM image for (a) Co<sub>98.5</sub>Ag<sub>1.5</sub>/γ-Al<sub>2</sub>O<sub>3</sub> with (b) the corresponding statistic size distribution of the Co nanoparticles.



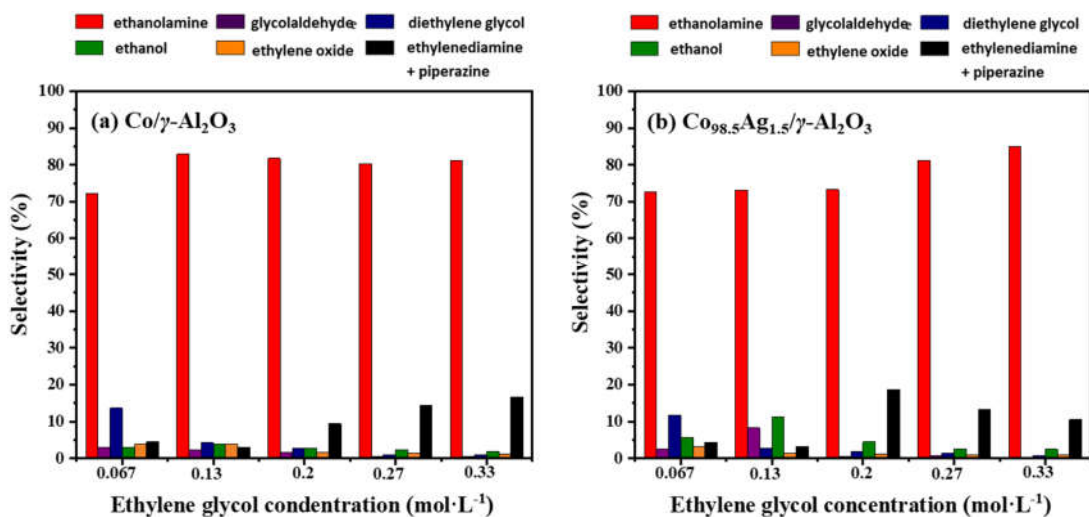
**Fig. S5.** Detailed product distribution of the ammonolysis of ethylene glycol on  $\text{Co}_{98.5}\text{M}_{1.5}/\gamma\text{-Al}_2\text{O}_3$  ( $\text{M} = \text{Cu}, \text{Ag}, \text{and Ru}$ ; 5 wt% Co) catalysts at ~20% conversion (453 K, 0.6 MPa  $\text{NH}_3$ , 3.0 MPa  $\text{H}_2$ , 0.067 mol/L ethylene glycol in tetrahydrofuran solution, 2 h).



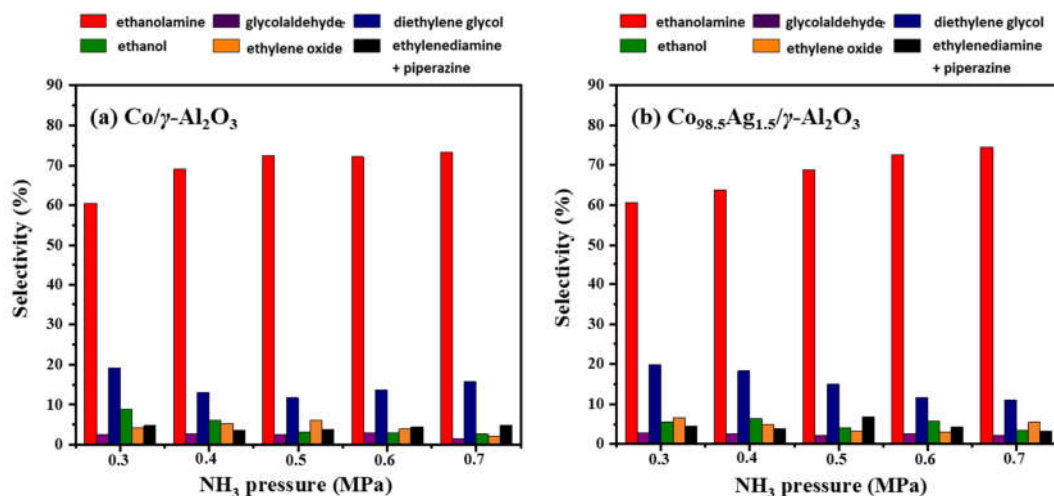
**Fig. S6.** Activity comparison among 5 wt%  $\text{Co}/\gamma\text{-Al}_2\text{O}_3$ , 5 wt%  $\text{Co}_{98.5}\text{Ag}_{1.5}/\gamma\text{-Al}_2\text{O}_3$ , and 5 wt%  $\text{Ag}/\gamma\text{-Al}_2\text{O}_3$  in catalytic ammonolysis of ethylene glycol (453 K, 0.6 MPa  $\text{NH}_3$ , 3.0 MPa  $\text{H}_2$ , 0.067 mol/L ethylene glycol in tetrahydrofuran solution, 2 h).



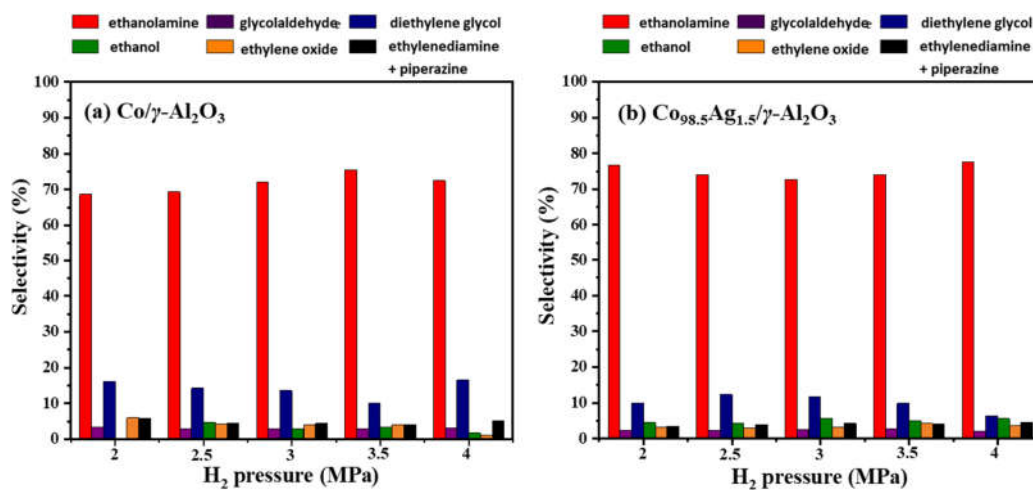
**Fig. R7.** (a) Co 2p and (b) Ag 3d XPS spectra for the Co<sub>98.5</sub>Ag<sub>1.5</sub>/γ-Al<sub>2</sub>O<sub>3</sub> and Co<sub>95</sub>Ag<sub>5</sub>/γ-Al<sub>2</sub>O<sub>3</sub> catalysts and (c) the corresponding Ag/(Co+Ag) surface ratios determined from these spectra.



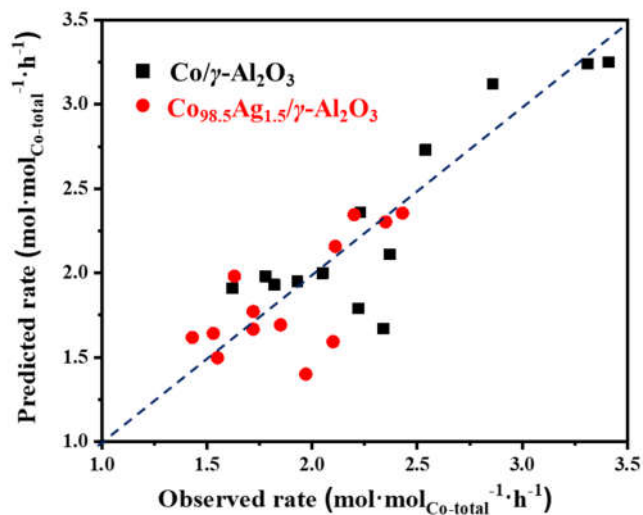
**Fig. S8.** Selectivities of ethylene glycol concentration on (a) Co/γ-Al<sub>2</sub>O<sub>3</sub> and (b) Co<sub>98.5</sub>Ag<sub>1.5</sub>/γ-Al<sub>2</sub>O<sub>3</sub> catalysts (Co 5 wt%) as a function of ethylene glycol concentration (453 K, 0.6 MPa NH<sub>3</sub>, 3.0 MPa H<sub>2</sub>, 2 h, ~20% ethylene glycol conversion obtained by varying the catalyst amount or reaction time).



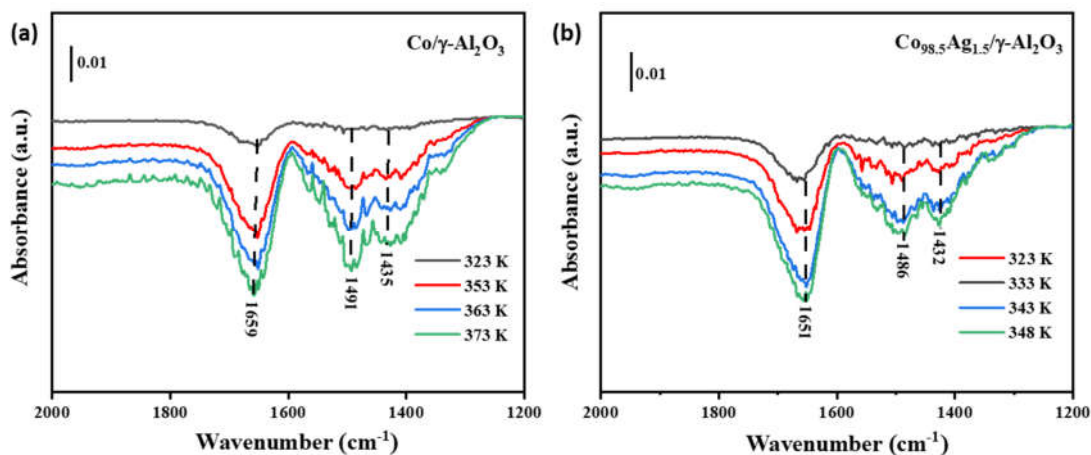
**Fig. S9.** Selectivities of ethylene glycol concentration on (a)  $\text{Co}/\gamma\text{-Al}_2\text{O}_3$  and (b)  $\text{Co}_{98.5}\text{Ag}_{1.5}/\gamma\text{-Al}_2\text{O}_3$  catalysts (Co 5 wt%) as a function of  $\text{NH}_3$  pressure (453 K, 3.0 MPa  $\text{H}_2$ , 0.067 mol/L ethylene glycol in tetrahydrofuran solution, 2 h, ~20% ethylene glycol conversion obtained by varying the catalyst amount or reaction time).



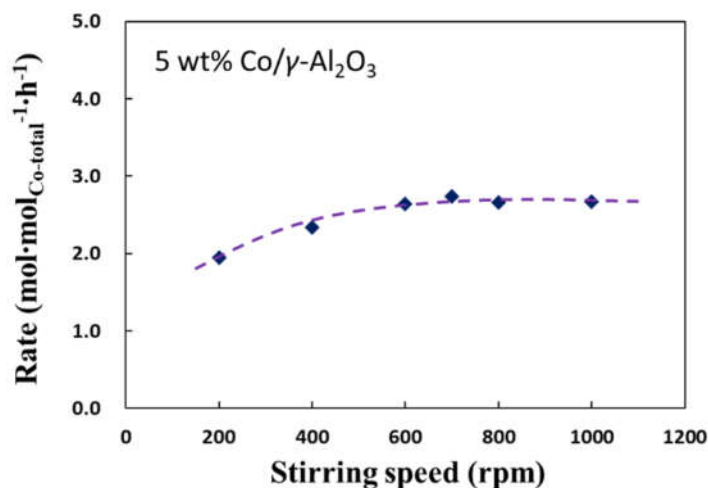
**Fig. S10.** Selectivities of ethylene glycol concentration on (a)  $\text{Co}/\gamma\text{-Al}_2\text{O}_3$  and (b)  $\text{Co}_{98.5}\text{Ag}_{1.5}/\gamma\text{-Al}_2\text{O}_3$  catalysts (Co 5 wt%) as a function of  $\text{H}_2$  pressure (453 K, 0.6 MPa  $\text{NH}_3$ , 0.067 mol/L ethylene glycol in tetrahydrofuran solution, 2 h, ~20% ethylene glycol conversion obtained by varying the catalyst amount or reaction time).



**Fig. S11.** A parity plot for the measured and predicted rates of ethylene glycol amination (Equation 2) on the  $\text{Co}/\gamma\text{-Al}_2\text{O}_3$  and  $\text{Co}_{98.5}\text{Ag}_{1.5}/\gamma\text{-Al}_2\text{O}_3$  catalysts.

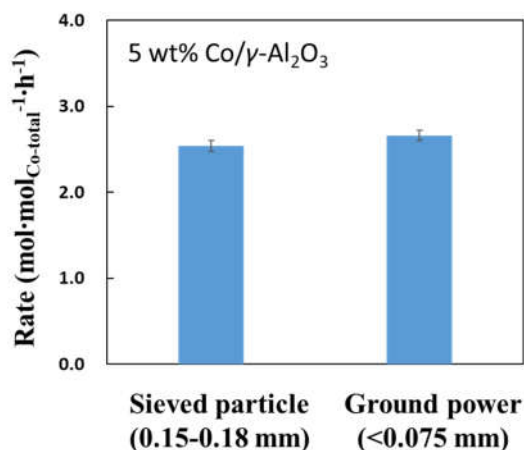


**Fig. S12.** Infrared spectra of  $\text{NH}_3$  desorption as a function of temperature for (a)  $\text{Co}/\gamma\text{-Al}_2\text{O}_3$  and (b)  $\text{Co}_{98.5}\text{Ag}_{1.5}/\gamma\text{-Al}_2\text{O}_3$  (using the respective spectra collected at ambient temperature as the background).



**Fig. S13.** Effect of stirring speed on the rate of ethylene glycol ammonolysis over 5 wt% Co/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> (453 K, 0.6 MPa NH<sub>3</sub>, 3.0 MPa H<sub>2</sub>, 0.067 mol/L ethylene glycol in tetrahydrofuran solution, 2 h).

As shown in Figure S13, the rate of ethylene glycol ammonolysis on 5 wt% Co/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> increased with the stirring speed until the speed was above 600 rpm, which reflects the threshold value to overcome the interphase diffusion limitation at the examined reaction condition. Our kinetic measurements were all conducted at a high speed of 800 rpm, ensuring that the interphase diffusion limitation was avoided in this study.



**Fig. S14.** Effect of particle size on the rate of ethylene glycol ammonolysis over 5 wt% Co/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> (453 K, 0.6 MPa NH<sub>3</sub>, 3.0 MPa H<sub>2</sub>, 0.067 mol/L ethylene glycol in tetrahydrofuran solution, 2 h).

As shown in Figure S14, the rate of ethylene glycol ammonolysis obtained on two different particle-sized Co/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> samples (0.15-0.18 vs. < 0.075 mm) were nearly identical (2.54 vs. 2.66 mol·mol<sub>Co-total</sub><sup>-1</sup>·h<sup>-1</sup>), indicating the intra-particle diffusion limitation can also be excluded.