



Proceedings Synthesis of Myrtenal through Allylic Oxidation of α-Pinene over a Pd/SeO₂/SiO₂ Catalyst

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Abstract: SeO₂ based samples are tested for the oxidation of α -pinene, in liquid phase employing ethanol as the solvent. Commercial SeO₂ was tested under both reflux and under 6 atm O₂ pressure. At conversion levels of approximately 40%, the yield to myrtenal was much higher in the latter (34.4%) than in the former case (18.0%) due to the high oxidant species availability. Besides the high yield attained at relatively short reaction time. A palladium promoted selenium dioxide supported catalyst (Pd/SeO₂/SiO₂) was prepared, characterized, and submitted to the catalytic test. Selenium dioxide (14.4%) was strongly fixed to the silica support. Upon the palladium introduction (0.98%), the reducibility of SeO₂ is modified, which originates a selenium species activation towards the allylic oxidation. A 12% conversion level is attained over Pd/SeO₂/SiO₂ following 8 h of reaction time, employing ethanol as the solvent at 134 °C. The main product is myrtenal, being obtained with a selectivity of 62%. Over oxidation products are not detected. The palladium/selenium dioxide sample is easy to handle with and its recuperation following the reaction in liquid phase is possible.

Keywords: myrtenal; myrtenol; allylic oxidation; selenium dioxide; palladium

1. Introduction

Natural products oxidation plays an important role in the synthesis of new compounds, giving rise to new functional groups. In the case of allylic oxidations, the positions that are adjacent to double or triple bonds lead to the corresponding α , β -unsaturated carbonyl compounds. There are several reports on allylic oxidations methodologies, being the most know the one employing selenium dioxide (SeO₂), mainly due to its relatively high regio- and chemoselectivity, mainly leading to the corresponding allylic alcohols or α , β -unsaturated carbonyl compounds [1–3].

In spite of SeO₂ is quite simple material to handle with, it presents some disadvantages: (i) stoichiometric relations or even high SeO₂/substrate ratios are employed for carry out the oxidations [4], (ii) long reaction times are required [5], (iii) moderate yields are obtained [5], and (iv) colloidal selenium species are formed during the reaction, which are difficult to separate from the reactive mixture [3–5].

When considering the above-mentioned drawbacks, and in the context of Green Chemistry Principles that promote the employment of heterogeneous catalysis for replacing stoichiometric process [6], it is interesting to study catalytic allylic oxidation reactions.

In the present work, the allylic oxidation of α -pinene is studied, since this monoterpene is one of the most abundant in natural sources, and it is easily obtained from the essential oils of coniferous trees (pines), rosemary, lavender, and turpentine [7,8].

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A wide variety of heterogeneous catalysts have been employed for carrying out the allylic oxidation of α -pinene, employing molecular oxygen. Rauchdi et al. studied stabilized Ru nanoparticles suspensions, with water as the solvent and in tert-butyl hydroperoxide (TBHP) presence [9]. The authors have reported a relatively high yield to verbenone (39%). Platinum, palladium, ruthenium, rhodium, and iridium metal catalysts supported on activated carbon have also been studied for the oxidation of α -pinene, but the introduction of nitrogenated admixtures was employed for increasing the yields to verbenone and verbenol [10]. Kholdeeva et al. studied α -pinene oxidation over Cr- and Fe-MOF, employing TBHP. The authors reported conversion not higher than 22% at long reaction times (16 h), obtaining a mixture of several oxidation products [11]. The present work deals with the preparation and characterization of a Pd/SeO₂ supported catalyst, and its evaluation in the oxidation of α -pinene. The catalytic test is carried out in batch conditions, with O₂ as the oxidant and without employing initiators or admixtures. The activity and the selectivity to the different products are measured and the reuse of the catalyst is analyzed. The characterization is carried out by Transmission Electronic Spectroscopy (TEM), Fourier Transform Infrared Spectroscopy (FTIR), X-Ray Diffraction (XRD), and Temperature-programmed Reduction (TPR).

2. Experimental

2.1. Catalyst Synthesis and Characterization

A commercial sample of selenium dioxide (Merck, 98.0%) was employed for carrying out the reaction. This sample is named SeO₂.

A silica supported selenium dioxide catalyst (SeO₂/SiO₂) was prepared from the wet impregnation method [12]. Approximately 0.3 g of SeO₂ was dissolved in absolute ethanol (99.5%, Cicarelli), at 40 °C under magnetic stirring for 24 h. The support was silica (SiO₂) from Davison, with a specific surface area of 210 m²/g, was added to the selenium solution. Following the evaporation of ethanol, the sample was calcined at 400 °C during 60 min. The SeO₂/SiO₂ sample contains a nominal loading of 15 wt% of SeO₂.

A silica supported binary palladium/selenium dioxide catalyst was also prepared. A toluene solution of Pd(AcAc)₂ (Aldrich, 99.9%) was added to the SeO₂/SiO₂ catalyst. Following 24 h, the solid was filtered and the sample was calcined at 400 °C during 60 min. This catalyst is named Pd/SeO₂/SiO₂, and it contains a nominal Pd concentration of 1 wt%. Pd loading is determined by Atomic Absorption Spectroscopy in an A-Analyst Perkin Elmer equipment.

The samples were analyzed by X-ray diffraction (XRD) with a Panalytical Empyrean 3 diffractometer using Ni-filtered CuK α radiation and a PIXcel^{3D} detector, operating at a voltage of 45 kV and a current of 40 mA, in the 2 θ range from 10° to 80°, using a continuous scan mode with a scan angular speed of 0.02° min⁻¹.

Fourier Transform Infrared Spectroscopy (FTIR) characterized the samples in a Nicolet Nexus apparatus. The spectra were obtained with a resolution of 2 cm⁻¹ using 50 scans.

The palladium particle sizes were determined with Transmission Electronic Microscope (TEM), TEM JEOL 100 CX, at 100 kV. The Digital Micrograph software was employed for measuring crystal sizes.

2.2. Liquid Phase Oxidation of α -Pinene

Two different methodologies were followed for carrying out the oxidation of α -pinene (Riedel de Haden, 97%): (i) a methodology that is usually employed in Organic Synthesis. 1 eq of α -pinene in absolute ethanol (35 mL) was put in contact with 2.5 eq of SeO₂. The reaction mixture was placed in a round-bottomed flask and it was heated under reflux until the disappearance of the starting material. (ii) a methodology usually followed for testing heterogeneous catalysis. The allylic oxidation reaction was conducted in a 50 mL Parr Instrument, operating in batch mode, at 134 °C, and the pressure was raised to six

atmospheres of oxygen. The stirring was set in 620 rpm and the reaction was carried out over SeO₂. For this case, the reactive mixture was: 1 eq of α -pinene and 2.5 eq of SeO₂ in 35 mL of absolute ethanol (0.02 M). The stirrer was switched on and the reaction is considered to be started.

Besides, also following (ii), the allylic oxidation reaction was conducted over the SeO₂/SiO₂ (200 mg) and over the Pd/SeO₂/SiO₂ (400 mg) catalysts in an ethanolic solution of α -pinene, 35 mL, 0.1 M.

3. Results and Discussion

3.1. Preparation and Characterization

The selenium dioxide loading for both the SeO₂/SiO₂ and the Pd/SeO₂/SiO₂ was 14.4 wt%, which is a value quite similar to the target selenium dioxide concentration. In addition, it is observed that the amount of selenium dioxide remains constant following the catalytic test. This result indicates that a strong selenium dioxide/silica support interaction is developed.

The palladium loading in the Pd/SeO₂/SiO₂ sample (0.98 wt%) is also similar to the nominal concentration (1 wt%).

In Figure 1, the XRD pattern that corresponds to commercial SeO₂ sample and to the SeO₂/SiO₂ catalyst, respectively, are shown. The commercial sample shows a diffraction peak assigned to selenium dioxide and to selenious acid (JCPDS card N° 00-041-0259 and JCPDS card N° 00-022-1314 for H₂SeO₃ and SeO₂, respectively). Both of the species are generally found together, since hydration of the oxide leads to the acid. For the supported catalysts, a wide peak, due to silica, is observed [13]. No peak corresponding to selenium species was detected, probably due to the fact that such species are highly dispersed on silica, and the corresponding peaks appear in the same region as the ones due to the support.

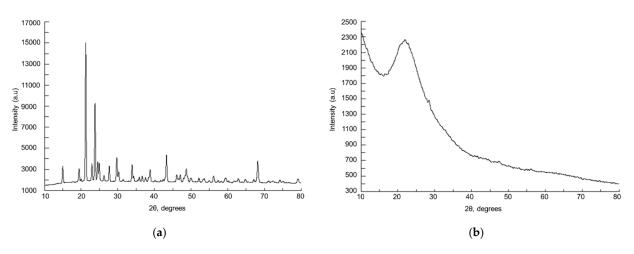


Figure 1. X-Ray Diffraction (XRD) patterns of: (a) SeO₂; (b) SeO₂/SiO₂.

The fresh and spent binary catalysts (Pd/SeO₂/SiO₂) were both also studied by XRD. Figure 2 shows the corresponding patterns. For the fresh sample, a similar spectrum as in the case of SeO₂/SiO₂ was obtained and the signals due to palladium or palladium oxide are not detected. The noble metal peaks are not observed, probably due to the high dispersion of palladium crystals developed in this sample. On the other hand, it is interesting to note that the XRD results corresponding to the used catalyst, following the catalytic test, indicate the presence of signals due to metallic palladium at 39.5 and 47.3 degrees of $2\theta^{\circ}$ and to palladium oxide (28.6 degrees of $2\theta^{\circ}$). It is likely that palladium species are highly dispersed in the fresh catalyst, and that, following the liquid phase oxidation, a sintering of the noble metal crystals occurs, which gives rise to larger palladium particles that are responsible for XRD peaks.

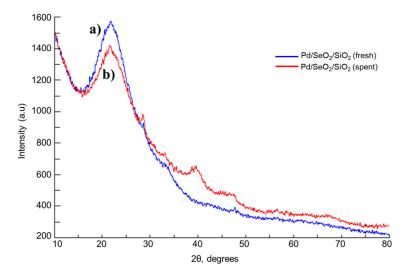
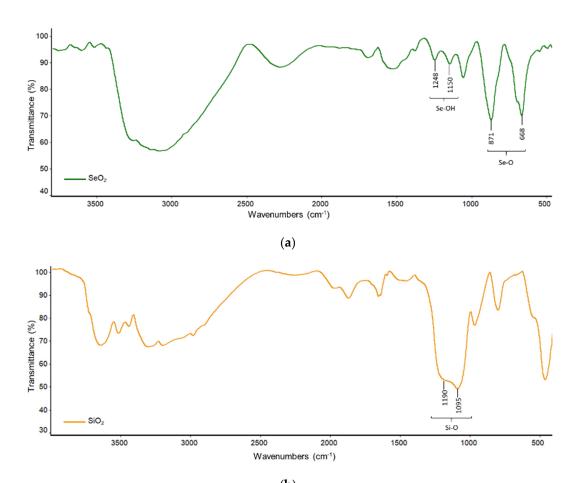
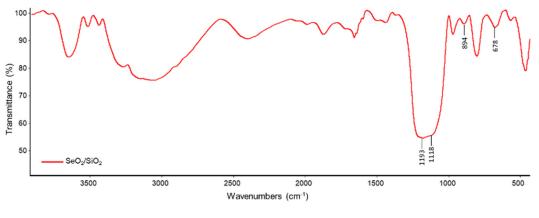


Figure 2. XRD pattern of: (a) fresh Pd/SeO₂/SiO₂ catalyst; (b) spent Pd/SeO₂/SiO₂ catalysts.

FTIR spectra that correspond to SeO₂, SiO₂ and SeO₂/SiO₂ are shown in Figure 3. For SeO₂ (Figure 3a), the bands at 871 and 668 cm⁻¹ are due to Se-O stretching, while those at 1248 and 1150 cm⁻¹ are due Se-OH [14].





(c)

Figure 3. FTIR spectra of: (a) SeO₂; (b) SiO₂; and, (c) SeO₂/SiO₂.

The FTIR spectrum corresponding to SiO₂ shows several bands (Figure 3b). Bands at 1190 and 1095 cm⁻¹ are due to Si-O stretching [13]. Both of these bands are shifted and their relative intensity is modified in SeO₂/SiO₂. This modification would be due to the high interaction between both oxides. Besides, the band at 894 and 678 cm⁻¹ due to selenium dioxide species are observed for the SeO₂/SiO₂ sample.

The FTIR analysis of the Pd/SeO₂/SiO₂ catalyst showed a similar result to the SeO₂/SiO₂ sample (Figure 4). The spent catalyst, following the catalytic test, was also studied by FTIR, and no differences with the fresh sample are detected. It is worth noting that bands due to the C-H, C=O, or C-OH groups were not detected over the sample used, which would indicate that no irreversible adsorption of reactants, intermediates, or products occurs during the reaction. Such adsorption was observed over used catalyst employed for liquid phase reactions involving aldehyde, alcohols, and acids over metal supported catalysts, and it would be responsible for catalyst deactivation [15].

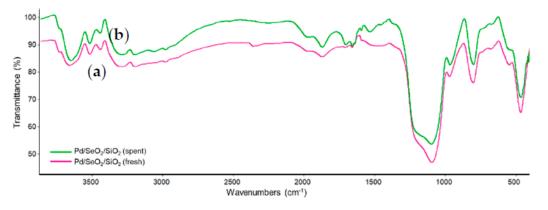
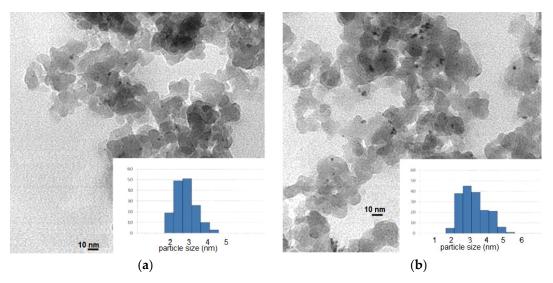


Figure 4. FTIR spectra of: (a) fresh Pd/SeO₂/SiO₂; (b) spent Pd/SeO₂/SiO₂.

Regarding TEM, characterization was carried out over SeO₂/SiO₂ sample, but is not possible to observe any difference between the silica support and the selenium species. Similar electronic densities of the samples would be the responsible for the low contrast between silica and selenium species.

TEM analysis was also carried out for the Pd/SeO₂/SiO₂ catalyst, for both the as prepared sample and the catalyst following the catalytic reaction. Figure 5 shows the results. Palladium particles in the fresh sample present a particle size of 2.9 nm, while the ones that correspond to spent catalyst show crystals with a size of 3.5 nm. It is concluded that



morphological modification takes place under reaction conditions, leading to an increase in palladium particle size. We will revert to this matter later.

Figure 5. Transmission Electronic Spectroscopy (TEM) images of: (a) fresh Pd/SeO₂/SiO₂ catalysts; (b) spent Pd/SeO₂/SiO₂ catalysts.

3.2. Catalytic Test

In the scheme, shown in Figure 6 some of the possible products from the α -pinene allylic oxidation are shown.

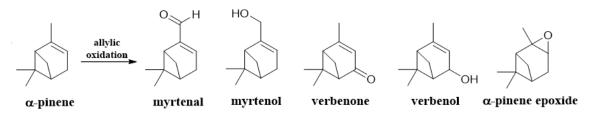


Figure 6. Some of the products from the allylic oxidation of α -pinene.

Selenium dioxide mediates the allylic oxidation of alkenes with retention of the double bond position. When the double bond is inside a ring, oxidation occurs in the α -position to the more substituted carbon of the double bond with a reactivity order CH₂ > CH₃ > CH [3]. Based on this, for α -pinene, myrtenal and myrtenol should be expected when employing SeO₂. Myrtenal is a component of essential oils mainly found in medicinal plants, and it has been reported to have pharmacological activities against many diseases such as diabetes, cancer, and malaria, among others [16–18]. On the other hand, antimicrobial and antifungal activities have been also documented [19]. Myrtenol, another monoterpene isolated from essential oils of some aromatic plants, despite being used for its flavoring properties, several studies have shown that it has anti-inflammatory and antinociceptive effects [20,21].

In the present work, the allylic oxidation of α -pinene over SeO₂ was carried out following two methodologies. Firstly (methodology i) the reaction was performed in liquid phase employing ethanol as the solvent, under reflux (78 °C), and conversion and selectivities were measured along with time. As could be expected, myrtenol was the main product at early reaction times and low conversion values. Anyway, myrtenal was also produced (Table 1). Myrtenal yield increases along with time, while the one corresponding to myrtenol diminishes, which shows that the aldehyde is being formed from the oxidation of the alcohol. At 13 h, the selectivity to myrtenal does not surpass 56%, yielding 28%. This yield is lower than the one that was reported by Lin et al. [18]; however, it is important to note that these authors have carried out the reaction employing 1,4-dioxane, a solvent not friendly to the environment.

Table 1. Allylic oxidation of α -pinene over SeO₂ through conventional test (methodology (i), under reflux)^a.

Entry	Time (h)	X b (%)	S ol ° (%)	S al ^d (%)
1	5	18	72	28
2	7	23	65	35
3	9	34	59	41
4	11	41	56	44
5	13	50	44	56

^aReaction conditions: 1 eq. of α -pinene, 2.5 eq. of SeO₂, in 35 mL of ethanol (0.02 M), 78 °C. ^b Conversion of α -pinene. ^c Selectivity to myrtenol. ^d Selectivity to myrtenal.

In addition, the oxidation of α -pinene was performed over SeO₂ following methodology (ii), in batch conditions, under oxygen pressure (6 atm), and at a higher temperature than in the previous case (134 °C against 78 °C). In this case, the 41% of conversion was attained at shorter times than for the reaction being carried out under reflux (5 h against 11 h). Myrtenal and myrtenol were the only detected products, showing a notably high selectivity to the aldehyde (84%) (Table 2). Thus, the yield to myrtenal (34.4%) was higher when the reaction is carried out under oxygen pressure than under reflux (18%). The high yield to myrtenal reached in the former case would be due to both the higher reaction temperature and the improved oxygen concentration in the liquid phase.

Table 2. Allylic oxidation of α -pinene over SeO₂ (methodology (ii), batch reactor under 6 atm O₂)^a.

Entry	Time (h)	X b (%)	S ol ° (%)	S al ^d (%)
1	2	5	58	42
2	3.5	21	29	71
3	5	41	16	84

^a Reaction conditions: 1 eq. of α -pinene, 2.5 eq. of SeO₂, in 35 mL of ethanol (0.02 M), 134 °C. ^b Conversion of α -pinene. ^c Selectivity to myrtenol. ^d Selectivity to myrtenal.

In the context of developing a supported heterogeneous catalyst, SeO₂ was fixed to SiO₂; thus, the SeO₂/SiO₂ sample was obtained. This catalyst is practically inactive in the allylic oxidation of α -pinene, reaching a 3% conversion level following 18 h, at 134 °C under oxygen pressure (6 atm). It is likely that, in the SeO₂/SiO₂ sample, the active species (selenium ones) are diluted in an inert support, which results in an insufficient active phase amount. The introduction of Pd to the selenium dioxide/silica system was envisaged for increasing the activity of the SeO₂/SiO₂ catalyst. The promotion of the selenium dioxide/silica material with the noble metal was quite effective, since the Pd/SeO₂/SiO₂ catalyst is much more active than the palladium free sample, tested under the same experimental conditions. A 12% conversion was reached at 8 h, showing relatively high selectivity to myrtenal (62%), being myrtenol the other product. It is important to note that no other co-product was detected.

The relatively high selectivity to myrtenal that is achieved over the Pd/SeO₂/SiO₂ catalyst is a quite interesting result, since previous reports, corresponding to Pd (or any other noble metal) based catalysts, indicated that the main products that correspond to α -pinene oxidations are verbenol and verbenone, and also that verbenoic acid is detected, originated in over oxidation of the aldehyde. It is likely that the oxidation over Pd/SeO₂/SiO₂ is governed by selenium species, leading to the allylic oxidation of the double bond in α position to the more substituted carbon of the double bond, and that palladium plays a promotional role on SeO₂. An analysis of the reducibility of the catalysts was carried out in order to throw some light on the promotional effect of Pd on selenium dioxide. The TPR results (Figure 7) indicate that palladium strongly modifies the SeO₂ redox character. A change in the reduction pattern of supported selenium dioxide upon the noble metal introduction can be observed. In the profile corresponding to SeO₂/SiO₂ (Figure 7a) a consumption peak centered at 290 °C is detected, which would be due to the reduction of selenium dioxide. In the binary Pd/SeO₂/SiO₂ catalyst, the reduction temperature is notably lower (Figure 7b), showing a reduction peak with a maximum at 270 °C. In this sense, it is proposed that the palladium promotional effect on selenium dioxide originates from a high interaction, which modifies the selenium dioxide reducibility. Taking into account that the catalytic results that indicate that the oxidation only yields myrtenal and myrtenol, it is concluded that palladium just plays a promotional role, without a direct participation in the activation of α -pinene. On the other hand, if palladium would act as the active phase, verbenone and verbenol should be produced, as usually observed over noble metal-based catalysts.

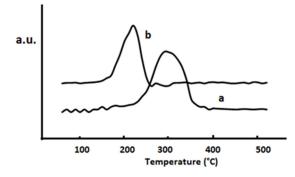


Figure 7. Temperature-programmed Reduction (TPR) profiles of: (a) SeO₂/SiO₂; (b) Pd/SeO₂/SiO₂.

It is concluded that Pd/SeO₂/SiO₂ is an active catalyst for carrying out the oxidation of α -pinene, which shows a relatively high selectivity towards myrtenal. In addition, a practical advantage arises due to the employment of a supported material, which is easy to both handle and separate from the reactive mixture by comparison with the SeO₂ sample.

Finally, a comment on the reuse of the Pd/SeO₂/SiO₂ should be carried out. The spent catalyst, following the reaction, was withdrawn from the reactor, washed with fresh solvent, a new catalytic test was performed. The activity of the catalyst was too low, showing that the reuse cannot be accomplished. The deactivation phenomena over Pd/SeO₂/SiO₂ are probably related with the larger palladium particle size, as measured from TEM analysis. It could be speculated that larger Pd crystals have no the same promotional effect on SeO₂ due to a lower contact between palladium and selenium species. In on-going studies, other catalysts, with different selenium dioxide and palladium loading, are being prepared and tested for the interest reaction, trying to obtain a sample that can be reused.

4. Conclusions

The comparisons between two different methodologies for the oxidation of α -pinene, employing SeO₂, leads to different myrtenal yields. The reaction carried out under reflux, under traditional organic synthesis conditions, yields lower myrtenal than when the reaction is performed under 6 atm of O₂. At the same conversion level, the selectivity to myrtenal is higher under oxidant overpressure than under reflux.

An effective supported catalyst for the oxidation of α -pinene was studied. The binary Pd/SeO₂ catalyst that is supported on SiO₂ leads to the oxidation in the α position to the more substituted carbon of the double bond. The binary sample is more selective to myrtenal than unsupported selenium dioxide, showing no overoxidation products. The pre-

sent results are promising regarding the substitution of the conventional oxidation methods for α -pinene by a catalytic transformation, being in line with Green Chemistry Principles.

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