

Extended Abstract

# Natural Mexican Zeolite Modified with Iron to Remove Arsenic Ions from Water Sources <sup>†</sup>

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**Abstract:** In this work the elimination of arsenic ions (V) in water was investigated by adsorption with Mexican natural zeolite (clinoptilolite type) conditioned with iron, the zeolite originating in the state of Oaxaca in Mexico used as an adsorbent medium was placed in a bed zeolite fixed column system of downward and upward flow to retain arsenic ions at pH 7 and 5. The zeolite was characterized by XRD, SEM/EDS and FTIR before and after the arsenic adsorption tests, the results showed that the methods of modification used are suitable for the superficial modification of the natural zeolite since it does not modify its structure. The results showed that with an initial concentration of As of 1 ppm, at a pH of 7, at 25 °C, an elimination of 99.23% was obtained, with a capacity of 0.09 mg<sub>As</sub>·g<sup>-1</sup><sub>zeolite</sub>.

**Keywords:** adsorption; ion arsenic; natural zeolite

## 1. Introduction

The Arsenic is an element present in the earth's crust and dispersed in the environment through natural processes and some anthropic activities. It is released into the environment naturally through the weathering and erosion of mineral sulfides, some activities such as mining, the use of wood protectors potentially increase its concentration in air, water and soil. In aqueous phase is found in inorganic form, in the form of arsenate and arsenite mainly, the pollution of groundwater by salts of this element originates what is known as endemic regional hydroarsenicism. The International Agency for Research on Cancer (IARC) [1] categorizes the inorganic As within group I, as a substance with proven carcinogenic action for humans. The presence of As has been found in groundwater in several countries such as Argentina, Mexico, Bangladesh, Canada and the United States. Regarding the concentration of arsenic in drinking water, the World Health Organization (WHO) and the Environmental Protection Agency (EPA) establish maximum concentrations of 10 µg·L<sup>-1</sup>. In Mexico, in some states such as Hidalgo [2], Morelos and Michoacán concentrations of arsenic have been found in bodies of water at around 1000 µg·L<sup>-1</sup>, a concentration that is well above what is allowed by Mexican regulations with the NOM-127-SSA1-1994 which establishes a limit of 25 µg·L<sup>-1</sup>. Given this problem in Mexico, the use of a Mexican natural zeolite (clinoptilolite type) modified superficially with iron, originally from the district of Etla in the region of the central valleys of Oaxaca, is proposed as an adsorbent medium for the removal of arsenic.

## 2. Experimental

The natural zeolite used in this study was collected from Mexican tuff in a deposit of the district of Etla (latitude 17.232951, longitude -96.810989) in the region of the central valleys in the state of Oaxaca. The samples were milled and sieved to 16 mesh size, washed with deionized water to remove impurities and dried at 100 °C. The previously washed natural zeolite was subjected to an ion exchange with 100 mL of 2 M NaCl solution using 10 g of natural zeolite at room temperature for 24 h, then washed and dried at 100 °C to obtain the sodium zeolite. Then the sodium zeolite was conditioned with  $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$  solution 0.5 M, and was deposited on the zeolite by the precipitation-impregnation method using as  $\text{NH}_4\text{OH}$  precipitant agent, subsequently dried at 100 °C for 24 h and finally washed with deionized water and dry again at 100 °C. Table 1 show the adsorbent materials used in the removal of arsenic ions (V).

**Table 1.** Adsorbents materials.

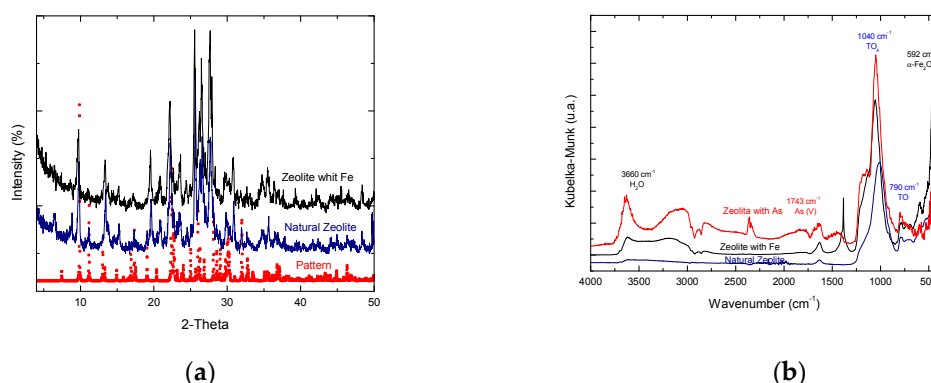
Sample	Description
ZN	Natural zeolite
ZN-Na	Zeolite sodium
ZN-Fe	Zeolite with Fe

The materials in Table 1 were characterized, before and after the adsorption process by: X-ray Diffraction (XRD) in a Philip diffractometer, X'pert model, Scanning Electron Microscopy (SEM/EDS) in a Supra 55VP microscope, Carl Zeiss. Fourier Transform Infrared Spectroscopy (FTIR), in a Varian model spectrometer Excalibur 3600. To determine the arsenic removal capacity of water contaminated with the adsorbent materials, two upflow and downflow column systems were used with a fixed bed of 10 g of adsorbent material and 100 mL of  $\text{As}^{+5}$  solution at pH 7 and modify the pH with HCl to 5, with a contact time of 24 h for the downflow column and with continuous flow 0.3 ml/min for the upflow column. All tests were performed with concentration of 1 ppm, room temperature and an output flow rate of 0.3 mL/min. The determination of arsenic was carried out by analysis of atomic absorption of the water samples treated in the Center for Applied Research in Environment and Health (CIAAS) within the Coordination for the Innovation and Application of Science and Technology (CIACYT) in the state of San Luis Potosí.

## 3. Results and Discussion

Figure 1a shows the XRD results of the natural and conditioned zeolites, the diffractogram of the natural zeolite corresponds to the diffraction peaks of the clinoptilolite type zeolite according to that reported by Mansouri [3] and correspond with the same peaks of the zeolite conditioned with iron so it is stated that the structure of the zeolite was not altered after the conditioning treatments. The Figure 1b shows the results of FTIR of natural zeolite and that conditioned with Fe, where the characteristic bands of a zeolite are observed. The samples modified with iron, also present the bands corresponding to the presence of water and the presence of  $\text{Fe}_2\text{O}_3$  [4].

Table 2 shows the results of the SEM/EDS analysis, for the washed natural zeolite, the sodium zeolite and the zeolite conditioned with Fe, after the ion exchange with Na, the percentage increase of the Na cation is observed. The zeolite conditioned with Fe increased its percentage 13 times more (bold letters) with respect to the content of this metal in the natural zeolite.



**Figure 1.** (a) XRD diffractograms of the natural and conditioned zeolite, (b) FTIR spectrums of the natural and conditioned zeolite.

**Table 2.** SEM/EDS analysis of natural and conditioned zeolites.

Element	wt %			
	ZN	ZN-Na	ZN-Fe	ZN-Fe/As
Si K	26.98	34.31	25.79	28.1
O K	56.40	50.38	44.81	53.78
Al K	5.91	5.64	4.72	4.57
Na K	1.55	5.22	3.67	0.9
Mg K	0.36	0.24	0	0.09
K K	3.83	1.68	1.64	2.68
Fe K	1.25	1.85	16.34	7.24
C K	3.40	0.68	3.03	2.3
Ca K	0.32	0	0	0
As L	0	0	0	0.36
<b>Total</b>	<b>100</b>	<b>100</b>	<b>100</b>	<b>100</b>

The results of the removal of As from contaminated water are presented in Table 3, these data indicate that natural clinoptilolite type zeolite is not feasible to remove As(V) ions from water. The conditioning of the natural zeolite with Fe greatly favoured the removal of the As ions in both column systems (downflow and upflow) since an average adsorption capacity of 0.09 mg<sub>As</sub>·g<sup>-1</sup><sub>zeolite</sub> was obtained for downflow and 0.35 mg<sub>As</sub>·g<sup>-1</sup><sub>zeolite</sub> for upflow, at temperature environment with neutral pH and with a particle size of 1.18 mm. In both studies equilibrium is not reached, these values are a three times larger environment in the upflow column since it is a greater volume treated of water contaminated with arsenate ion. The removal is slightly favoured when the pH of the solution is modified to 5 in both systems, however it can be suggested that the two column systems are appropriate to eliminate the arsenic ions (V).

The removal of arsenic from a real sample obtained from the state of Guanajuato with an initial content of 0.020 mg·L<sup>-1</sup> of As, presented optimal results with a percentage removal of 100% using the downflow column with the conditioned zeolite and pH of 7.5 and the 600 mL of natural water were treated.

**Table 3.** Adsorption of ions As(V) in column system with natural and modified zeolite.

Adsorbent Material	pH	Initial As (mg·L <sup>-1</sup> )	Removed As (mg·L <sup>-1</sup> )	Volume Treated (mL)	Removal (%)	Ad <sub>seq.</sub> (mg <sub>As</sub> /g <sub>zeolite</sub> )
Downflow column						
ZN	7	1	1	1000	0	0
ZN-Fe	7	1	9.92	1000	99.23	0.099
ZN-Fe	5	1	9.99	1000	99.51	0.109
Upflow column						
ZN	7	1	1	3600	0	0
ZN-Fe	7	1	0.96	3600	96.12	0.349
ZN-Fe	5	1	0.98	3680	98.25	0.357

## 4. Conclusions

It was possible to remove As from contaminated water efficiently, with an initial concentration of 1 mg·L<sup>-1</sup>, in the two column systems, using as adsorbent material a natural Mexican zeolite, conditioned with Fe, in this study it was found that iron incorporation favors the removal of As since the natural zeolite is not able to retain the As. With these results it is affirmed that the conditioned natural zeolite is apt to remove As (V) of water in the two column systems and at the two studied pH. However, the best results were obtained in the downflow column with 99.5% elimination and at pH 5. The results of XRD, SEM/EDS and FTIR have shown that the conditioning methods allowed to generate a material with adsorbent properties ideal for the removal of arsenic from contaminated water and allowed to corroborate the presence of As adsorbed in the material. This research could help the development of a prototype that combines the advantages of a conventional filter with those of a natural adsorbent medium conditioned with Fe, providing a continuous treatment, of low cost and relatively easy to operate, for its implementation in marginalized areas of Mexico.

**Author Contributions:** M.G-A. and M.T-R. conceived of and designed the experiments and analyzed the data, M.G-A. performed the experiments, J.M-S. and L.C-Y. designed the analyzes by AAS and V.M-A wrote the paper.

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**Conflicts of Interest:** The authors declare no conflict of interest.

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