

## Supplementary material

**Table S1.** Technical data related to different equipment used for lactic acid production.

Discrete modeling steps/ Equip- ment	Equipment param- eter	Units	Base Size	Base value (\$)	Base year	Exp*
Belt conveyor <sup>1</sup>	Length	m	30.48			
	Width	cm	60.96	70,000	2009	0.8
	Power	W/kg/s	720			
Grinder <sup>1</sup>	Throughput	t/h	28	302,000	2000	0.6
	Diameter	cm	35.56			
Screw conveyor <sup>2</sup>	Length	m	30.48	20,000	2009	0.8
	Specific power	W/((m <sup>3</sup> /s)*m)	10,800			
Bucket elevator <sup>2</sup>	Throughput	t/hr.				
	Volume	m <sup>3</sup>	20000	3,500,000	2009	0.6
Storage <sup>2</sup>	Diameter	cm	35			
	Length	m	30.48	20,000	2009	0.8
	Specific power	W/((m <sup>3</sup> /s)*m)	10,800			
Heat exchanger <sup>2</sup>	Area	m <sup>2</sup>	120	118000	2018	
Acid storage tank <sup>2</sup>	Volume	m <sup>3</sup>	48	6210	2010	0.7
Pump <sup>2</sup>						
Acid hydrolysis reactor <sup>2</sup>	Volume	m <sup>3</sup>	36.70	19,812,400	2009	0.6
Flash cooling tank <sup>2</sup>	Volume	m <sup>3</sup>	416.4	511,000	2009	0.7
Neutralization tank <sup>2</sup>	Volume	m <sup>3</sup>	446.7	236,000	2009	0.7
Cooling unit <sup>2</sup>	Area	m <sup>2</sup>	14.3	38,000		
Enzymatic hydrolysis reactor <sup>2</sup>	Volume	m <sup>3</sup>	3256	837,000	2015	0.6
Seed fermenter <sup>2</sup>	Volume	m <sup>3</sup>	900	300,000	2008	0.5
Fermentation tank <sup>2</sup>	Volume	m <sup>3</sup>	3256	837,000	2015	0.6
Storage tank <sup>2</sup>	Volume	m <sup>3</sup>	2325	165,800	1997	0.5
Dryer <sup>3</sup>	Area	m <sup>2</sup>	80.12	8,349	2002	0.6
Rotary vacuum filter <sup>4</sup>	Filter area	m <sup>2</sup>	101	254,000		
Neutralization tank <sup>2</sup>	Volume	m <sup>3</sup>	446.7	236,000	2009	0.7
Gypsum removal filter	Filter area	m <sup>2</sup>	65	195,000		
Evaporator	Area	m <sup>2</sup>	315	2068000		
Distillation column <sup>4</sup>	Volume	m <sup>3</sup>	212	879,000		
Distillation column <sup>4</sup>	Volume	m <sup>3</sup>	119	420,000		
Lignin removal <sup>4</sup>	Area	m <sup>2</sup>	342	525,000		
Anerobic digester <sup>4</sup>	Volume	m <sup>3</sup>	22463	2,989,000	2015	
Steam generator <sup>4</sup>	Throughput	t/hr.	65	696,000	2018	
Steam turbine <sup>4</sup>	Power	kW	6705	1444000	2018	

Note: \* Exponent for size factor

<sup>[1]</sup> Wright et. al., 2010

<sup>[2]</sup> Humbird et. al., 2011

<sup>[3]</sup> Jones et al., 2013

<sup>[4]</sup> Superpro Designer®

## References

1. Wright MM, Satrio J, Brown RC, Daugaard DE, et al. Techno-economic analysis of biomass fast pyrolysis to transportation fuels. Technical Report NREL/TP-6A20-46586 (2010).
2. Humbird D, Davis R, Tao L, et al. Process Design and Economics for Biochemical Conversion of Lignocellulosic Biomass to Ethanol. Technical Report NREL/LTP-5100-47764 (2011).
3. Jones S, Meyer P, Snowden-Swan L, et al. Process design and economics for the conversion of lignocellulosic biomass to hydrocarbon fuels: Fast pyrolysis and hydrotreating bio-oil pathway. Technical Report PNNL-23053 \NREL/TP-5100-61178 (2013).
4. Intelligen Inc. SuperPro Designer Software Version 10. (2023).

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