



Optimization of Bioactive Substances in the Wastes of Some Selective Mediterranean Crops

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Abstract: Production of added products from industrial byproducts is a challenge for the current natural product industry and the extraction field more generally. Therefore, the aim of this study is to valorize the selected Mediterranean crops that can be applied as antioxidants, natural chelating agents, or even as biosolvents or biofuels after special treatment. In this study, the wastes of popular Mediterranean plants were extracted via homogenizer-assisted extraction (HAE) by applying response surface methodology (RSM) to examine the effects of process parameters on the total biophenolic contents (TBCs) of their residues. Box–Behnken design model equations calculated for each system were found significant (p < 0.0001) with an adequate value of determination coefficient (R^2). Olive leaf had the highest TBC content (58.62 mg-GAE/g-DW with 0.1 g sample, 42.5% ethanol at 6522.2 rpm for 2 min), followed by mandarin peel (27.79 mg-GAE/g-DW with 0.1 g sample, 34.24% ethanol at 8772 rpm for 1.99 min), grapefruit peel (21.12 mg-GAE/g-DW with 0.1 g sample, 42.33% ethanol at 5000 rpm for 1.125 min) and lemon peel (16.89 mg-GAE/g-DW with 0.1 g sample, 33.62% ethanol at 5007 rpm for 1.282 min). The antioxidant activities of the extracts were measured by several in vitro studies. The most prominent biophenols of the wastes were quantified by high performance liquid chromatography (HPLC). Fourier-transform infrared-attenuated total reflectance (FTIR-ATR) and atomic force microscopy (AFM) techniques were also used for characterization.

Keywords: Mediterranean crops; waste; valorization; optimization; FTIR-ATR; AFM

1. Introduction

Food waste production covers the whole food life cycle from agricultural and industrial production and processing, to retail and domestic consumptions. In developed countries, 42% of food waste is produced during domestic consumption, while 39% is from the food manufacturing industry, 14% is from the food services sector and 5% is from the retail and distribution sectors [1]. Nowadays, industrial ecology concepts have been evaluated as a leading principle of eco-innovation that targets the *zero waste economy*, where waste is used as a raw material for new products and applications. Large quantities of waste generated by food industries cause serious problems both economically and environmentally, as well as resulting in a great loss of high-added value compounds. Moreover, most of these residues have reusable potential in other production systems.

The wastes of fruit and vegetable processes are the most important resources of various types of antioxidants and dietary fibers. The reason for this is that the corresponding byproducts are made from soft tissue that is rich in both components, allowing simultaneous extraction into two separate

streams [2]. Citrus is the largest fruit crop in the world [3,4], with a global production of approximately 115 million tons per year [5]. Since their water content is less than half the total weight of the fruits, their main byproducts are their peels after processing [6]. The concerned wastes are traditionally evaluated for animal feed, pectin and fuel production [5,7]. Recent studies evaluating these wastes have suggested that some fruit or vegetable byproducts may be natural antioxidant sources. Orange peel has been used for the recovery of phenolic materials, flavonoids, essential oils and carotenoids [5,8,9]. Karsheva et al. obtained extracts from mandarin peels, and examined the level of biophenols in their extract content [6]. Singanusong et al. also found the antioxidant capacity of mandarin peels by various methods, and analyzed their total biophenolic substances [10]. Ateş et al. extracted phenolic antioxidants by various advanced separation methods (microwave-assisted extraction and supercritical-CO₂ extraction), using mandarin peel as a raw material [11]. Lemon peel was also used as raw material for pectin and flavonoid production [3,4]. Li et al. extracted lemon peels by enzyme-assisted extraction to get bioactive ingredients [12]. Furthermore, Guimarães et al. compared the water content of the lemon peel in terms of antioxidants, and observed a higher level (about eight times) of phenolic material in lemon peels compared to that of water [13]. Moreover, the same research group compared grapefruit juice and peels with respect to phenolic material. They observed that the peel had an approximately six times higher biophenol level compared to that of grapefruit water. Li et al. recycled grapefruit peels for biologically active materials by means of enzyme-assisted extraction [12].

On the other hand, olive trees are one of the most important fruit trees in Mediterranean countries, covering eight million hectares, which corresponds to about 98% of the world crop. This output demonstrates the economic and social importance of this crop [14]. Olive leaves, which are byproducts of this crop, also represent 10% of the total weight of the harvested olives, but this residue remains agricultural waste if it is not assessed [15]. Since olive leaf is a rich source of bioactive substances that have been proven many times to possess health effects, a wide variety of studies have been carried out in this regard [16]. Şahin et al. obtained extract rich in biofenol and flavonoid by using ultrasound-assisted extraction [17]. Xynos et al. [18] and Putnik et al. [19] applied pressurized liquid extraction as an environmentally friendly technology to extract olive leaf for its biophenol substances. Sahin et al. utilized solvent-free microwave extraction to attain olive leaf extract [20]. Mourtzinos et al. [21] and Athanasiadis et al. [22] obtained a rich extract of antioxidants using environmentally friendly and novel solvents, respectively. Khemakhem et al. applied novel separation methods (microfiltration, ultrafiltration and nanofiltration) to acquire extract with a high level of oleuropein (the main ingredient of the olive leaf) [23]. To our knowledge, the number of studies of citrus peels in terms of polyphenol level is quite inadequate, although there have been many studies in which olive leaf has been examined for its natural antioxidants. For this reason, evaluation of these resources, and comparison of the related wastes, is carried out in this study. On the other hand, the concerned waste samples have been extracted with homogenizer-assisted extraction (HAE), which is an extremely simple system with extremely minimal time and investment cost requirements. As the rotary blade spins at a very high speed, the texture is rapidly reduced in size by a combination of excessive shear, cavitation and scissor-like mechanical shear in the narrow gap between the rotor and the stator. Since most rotor stator homogenizers have an open configuration, the product is recirculated repeatedly. Depending on the processing speed and hardness of the tissue sample, the desired results are usually obtained in 15–120 s. The goal of the present study is to optimize the conditions of HAE for obtaining the selected raw materials, depending on their phenolic content, and to identify the richest waste byproduct with respect to bioactive properties.

2. Materials and Methods

2.1. Plant and Chemical Materials

Olive leaf samples were supplied from Özgün Olive, Olive Oil Co in the Aegean part of Turkey (Ayvalik, Balikesir). Citrus fruits were provided by the Bati Akdeniz Agricultural Research Institute

(BATEM) in Antalya, Turkey. The samples were dried at ambient conditions. The dried leaves and peels were ground by a grinder (Moulinex Super Blender Grinder, LM209041, Paris, France), and screened through a 22-mesh sieve.

Ethanol (>99.5%) and methanol (>99.8%) were from Merck (Darmstadt, Germany), while sodium carbonate, Folin–Ciocalteu, 2,2-diphenyl-1-picrylhydrazyl (DPPH•), 2,9-dimethyl-1,10-phenanthroline (neocuproine), 6-hydroxy-2,5,7,8-tetramethylchroman-2-carboxylic acid (trolox), gallic acid, oleuropein, naringin, formic acid and acetonitrile were from Sigma-Aldrich (St. Louis, MO, USA).

2.2. Homogenizer-Assisted Extraction

Residue samples were extracted three times by an ethanol-water solution (v/v) of different concentrations by means of an IKA T25 (ULTRA-TURRAX, Staufen, Germany) brand homogenizer. The homogenization was adjusted to several conditions (Table 1). Before analysis, extracts were filtered through a syringe filter (0.45 µm) and kept in dark at -20 °C.

Table 1. Summary of the HAE-homogenizer-assisted extraction parameters with their units, symbols and levels.

Process Parameters	Units Symbol of the Parameter		Levels with the Codes		
riocess ratalleters	Units	its Symbol of the Latameters		0	1
Solvent Concentration	%, v/v	<i>X</i> ₁	20	50	80
Solid Mass	g	X2	0.1	0.175	0.25
Extraction time	min	X_3	0.5	1.25	2
Speed	rpm	X_4	5000	7000	9000

2.3. Spectrophotometric Analyzes

Total biophenolic content (TBC) determination of the extracts was carried out spectrophotometrically (PG Instruments, T60/Leicestershire, Leicester, England) depending on the Folin–Ciocalteu method at a wavelength of 765 nm [24]. The findings were expressed as a gallic acid equivalent on a dried base (mg-GAE/g-DW). Scavenging activity of the ABTS radical was measured following the procedure of Re et al. with slight modifications [25]. The wavelength was selected as 734 nm. Inhibition of ABTS was given as mg trolox equivalent antioxidant activity on a dried base (mg-TEAC/g-DW). Free-radical scavenging activity against the DPPH radical was also achieved by following the report of Yu et al. [26] with some modifications [27]. The wavelength was selected as 517 nm. Inhibition of DPPH was given as mg-TEAC/g-DW. Moreover, cupric ion reducing antioxidant capacity (CUPRAC) assay was applied to measure the antioxidant activity of the residues [28]. Maximum absorbance was observed at 450 nm. The antioxidant activity of the samples was also stated as mg-TEAC/g-DW.

2.4. Chromatographic Analysis

Individual phenolic quantification was performed by high-performance liquid chromatography (HPLC). The main ingredients of the selected wastes have been investigated in the literature. After determination of the prominent compounds of the samples, the relevant compounds were provided as standards. Then, standard solutions were prepared in several concentrations to draw a calibration curve. After measuring the absorbance of the samples, the concentrations were determined using the calibration curve. Conditions of HPLC are given in Table 2.

HPLC Conditions	Program		
Model: Agilent 1260 (Agilent, Waldbronn, Germany)	Time (min)	A (%)	B (%)
Colon: Agilent Eclipse Plus C18 RRHD 18 (3×5 mm; 1.8 μ m)	0.0	100	0
Mobile phase: A = Water + $\%$ 0.1 formic acid (v/v)	0.5	100	0
B = Acetonitrile + $\%$ 0.1 formic acid (v/v)	7.0	60	40
Detection wavelength: 276 nm	7.1	0	100
Flow rate: 1 mL/min	8.6	0	100
Column temperature: 40 °C	8.7	100	0
Injection volume: 20 µL	10	100	0

Table 2. Analyzing conditions of individual phenols along with the gradient program applied.

2.5. Atomic Force Microscopy

The nanostructural morphologies and height profiles of the lemon peels and olive leaves were examined with an atomic force microscopy (AFM) instrument, which was provided by Nanomagnetics Instruments. It was operated in tapping mode at room temperature using silicon probes coated with the aluminum (PPP–NCLR nanosensors). Samples were scanned before and after extraction processes utilizing a 10 μ m/s scanning rate and a 256 × 256 pixel resolution. The statistical parameters were evaluated from AFM images using the image analysis software NMI Viewer 2.0.7.

2.6. Fourier-Transform Infrared-Attenuated Total Reflectance

The chemical characterization of the extracts was made using a Bruker Alpha-T DRIFT spectrometer with a 528/D model through OPUS 6.5 software (Bruker Optics Inc., Coventry, UK).

2.7. Statistical Experimental Design

Box–Behnken design was applied into the selected HAE process as a three-level factorial design for the optimization of four process parameters (Table 1). Since there are relatively many independent variables, Box–Behnken design was selected in order to be more economical in a more effective way [29]. Furthermore, Box–Behnken design, along with response surface methodology (RSM) provides an evaluation of the effects of process parameters and their interactions with the relevant system. In this study, Design-Expert (Stat-Ease, Minneapolis, MN, USA) software version 10.0.4 was used.

The quadratic model of response is described the equation given below:

$$Y = \beta_0 + \sum_{i=1}^3 \beta_i X_i + \sum_{i=1}^3 \beta_{ii} X_i^2 + \sum_{i=1}^3 \sum_{j=i+1}^3 \beta_{ij} X_i X_j + e,$$
(1)

where β_0 is the constant, β_i is the linear and β_{ii} is the quadratic (i and j = 4) interaction coefficient. X_i (i = 1–4) is the non-coded factor, while Y represents the dependent parameter, known as the response.

An analysis of variance (ANOVA) test is utilized to assess the model fitting, as well as to determine the interaction between the variables using the same software. A lack of fit test was further applied to the independent and dependent variables for verification of the model fitting.

2.8. Statistical Analysis

Analysis of variance (ANOVA) statistical testing was utilized through Tukey's test of InStat software (GraphPad, San Diego, CA, USA) to analyze the means of three replicate outputs.

3. Results and Discussions

TBC findings of the olive leaf, grapefruit, lemon and mandarin peel extracts attained by HAE through Box–Behnken design are given in Table 3, which details their EtOH concentration, solid mass, extraction time and speed.

<i>X</i> ₁	Y. (g)	X_3	X_4	TBC (mg-GAE/g-DW)				
(%. <i>v/v</i>)	X ₂ (g)	(min)	(rpm)	Olive Leaf	Grapefruit Peel	Lemon Peel	Mandarin Peel	
80	0.1	1.25	7000	33.06 ± 0.000	16.06 ± 0.001	4.23 ± 0.002	24.06 ± 0.001	
20	0.175	0.5	7000	34.41 ± 0.002	12.03 ± 0.002	6.80 ± 0.001	20.70 ± 0.001	
50	0.175	0.5	5000	27.94 ± 0.001	12.03 ± 0.001	7.18 ± 0.001	18.80 ± 0.001	
50	0.175	2	9000	48.80 ± 0.000	14.13 ± 0.001	13.37 ± 0.002	22.99 ± 0.000	
50	0.1	1.25	9000	42.56 ± 0.001	15.06 ± 0.003	16.23 ± 0.003	21.90 ± 0.002	
80	0.175	1.25	9000	33.37 ± 0.000	10.70 ± 0.001	14.22 ± 0.001	17.18 ± 0.001	
50	0.175	1.25	7000	41.05 ± 0.000	12.22 ± 0.002	13.02 ± 0.001	16.89 ± 0.001	
50	0.1	0.5	7000	26.06 ± 0.001	14.06 ± 0.000	15.23 ± 0.000	15.56 ± 0.002	
50	0.175	1.25	7000	40.98 ± 0.000	13.50 ± 0.001	13.54 ± 0.001	15.63 ± 0.001	
50	0.175	1.25	7000	42.67 ± 0.000	12.65 ± 0.001	11.20 ± 0.001	15.98 ± 0.002	
50	0.1	1.25	5000	46.90 ± 0.001	22.40 ± 0.002	12.40 ± 0.001	18.90 ± 0.001	
50	0.1	2	7000	61.25 ± 0.002	15.06 ± 0.000	13.23 ± 0.002	19.73 ± 0.003	
50	0.25	0.5	7000	30.02 ± 0.000	9.36 ± 0.001	7.02 ± 0.001	1.93 ± 0.001	
50	0.25	1.25	5000	35.96 ± 0.001	11.09 ± 0.002	10.16 ± 0.001	14.62 ± 0.001	
20	0.1	1.25	7000	46.73 ± 0.001	17.06 ± 0.002	12.23 ± 0.002	24.23 ± 0.002	
20	0.175	1.25	9000	43.65 ± 0.001	12.99 ± 0.001	10.60 ± 0.001	17.65 ± 0.001	
50	0.175	1.25	7000	43.60 ± 0.001	11.36 ± 0.001	12.65 ± 0.002	17.23 ± 0.002	
80	0.175	0.5	7000	25.27 ± 0.001	9.56 ± 0.002	1.46 ± 0.001	17.18 ± 0.001	
50	0.175	0.5	9000	35.37 ± 0.001	8.41 ± 0.000	7.18 ± 0.002	25.37 ± 0.001	
50	0.175	1.25	7000	42.41 ± 0.001	10.25 ± 0.001	11.18 ± 0.000	16.32 ± 0.001	
80	0.25	1.25	7000	29.09 ± 0.000	9.62 ± 0.001	3.69 ± 0.001	13.69 ± 0.002	
20	0.175	1.25	5000	35.56 ± 0.001	13.75 ± 0.001	8.89 ± 0.001	20.13 ± 0.001	
80	0.175	2	7000	36.89 ± 0.001	9.56 ± 0.002	2.80 ± 0.001	17.56 ± 0.001	
80	0.175	1.25	5000	27.46 ± 0.002	13.56 ± 0.001	3.65 ± 0.002	15.84 ± 0.000	
50	0.25	1.25	9000	41.09 ± 0.003	14.29 ± 0.002	10.56 ± 0.001	21.62 ± 0.001	
20	0.175	2	7000	45.37 ± 0.001	13.37 ± 0.000	9.75 ± 0.001	17.75 ± 0.001	
20	0.25	1.25	7000	38.56 ± 0.001	12.02 ± 0.001	10.36 ± 0.000	7.96 ± 0.002	
50	0.175	2	5000	44.32 ± 0.002	13.18 ± 0.001	10.99 ± 0.001	25.46 ± 0.001	
50	0.25	2	7000	45.09 ± 0.001	11.49 ± 0.001	10.49 ± 0.001	20.09 ± 0.001	

Table 3. Effects of the independent variables on the TBC-total biophenolic content extraction of the relevant wastes *.

* Data are given as the mean $(n = 3) \pm$ standard deviation.

3.1. Modeling and Optimization by Box–Behnken Design

Quadratic polynomial models derived for the TBCs extracted from the relevant residues of each crop are given in Table 4. Coefficient of determination (R^2) values also indicate that the equations calculated for the four responses were adequate to explain the relationship between the dependent and independent variables ($R^2 > 0.89$).

Table 5 summarizes the statistical results of each extract system. The adequacy of the derived models obtained by Box–Behnken design were verified and found to be significant (p < 0.0001) to the experimental findings (Table 3). Regarding olive leaf, time for HAE was the most effective variable of the TBC yield, followed by solvent concentration (p < 0.0001). Time effect was also found to be statistically the most significant parameter in the extraction of anthocyanin from red raspberries by Chen et al. [30]. Amount of solid mass was the most significant parameter for the extraction of TBC from grapefruit peel (p < 0.0001). Similarly, Jeganathan et al. observed solid mass as an effective parameter for the solvent extraction of polyphenols from red grapes by applying Box–Behnken design [31]. Quadratic power of ethanol concentration was statistically (p < 0.0001) the most important parameter of all for the lemon peel extraction by HAE (p < 0.0001). Bilgin et al. also reported a second power of ethanol concentration in the HAE of TBC from *Sideritis montana* L. [32]. Second power of extraction speed was the most influential process parameter affecting the HAE of mandarin peels. This finding is in agreement with that of Şahin et al., where HAE was used for solid-liquid extraction to enrich sunflower oil with polyphenols [33].

Response		Equation	R^2	
	Olive leaf	$\begin{array}{r} 42.14 - 4.93X_1 - 3.06X_2 + 8.55X_3 + 2.23X_4 + 1.05X_1X_2 + \\ 0.17X_1X_3 - 0.55X_1X_4 - 5.03X_2X_3 + 2.37X_2X_4 - 0.74X_3X_4 \\ - 5.51X_1^2 + 0.36X_2^2 - 1.60X_3^2 - 1.31X_4^2 \end{array}$	0.9233	
TBC	Grapefruit peel	$\begin{array}{l} 12.00-1.01X_1-2.65X_2+0.94X_3-0.86X_4-0.35X_1X_2-\\ 0.33X_1X_3-0.52X_1X_4+0.28X_2X_3+2.63X_2X_4+1.14X_3X_4\\ -0.16X_1^2+2.00X_2^2-1.17X_3^2+1.25X_4^2\end{array}$	0.9219	
(mg-GAE/g-DW)	Lemon peel	$\begin{array}{r} 12.32-2.38X_1-1.77X_2+1.31X_3+1.57X_4+0.33\ X_1X_2-\\ 0.40X_1X_3+2.21X_1X_4+1.37X_2X_3-0.86X_2X_4+0.60X_3X_4\\ -4.35X_1^2+0.29X_2^2-2.25X_3^2+0.24X_4^2 \end{array}$	0.8934	
	Mandarin peel	$\begin{array}{r} 16.29 - 1.12X_1 - 1.06X_2 + 2.37X_3 + 2.49X_4 - 1.64X_1X_2 \\ + 0.45X_1X_3 + 0.52X_1X_4 - 2.82X_2X_3 + 1.00X_2X_4 + 0.46X_3X_4 \\ - 2.24X_1^2 + 1.12X_2^2 + 3.50X_3^2 + 2.33X_4^2 \end{array}$	0.9055	

Table 4. Model equations with coded factors derived by Box–Behnken design through RSM-Response

 Surface Methodology.

Table 5. Analysis of variance test using Design-Expert 10.0.4 for the HAE of TBC in the relevant wastes.

	Source	Sum of Squares	df	Mean Square	F Value	<i>p-</i> Value Prob > l
	Model	1687.74	14	120.55	12.04	< 0.0001
	X_1 -Solvent concentration	291.40	1	291.40	29.11	< 0.0001
	X ₂ -Solid Mass	112.59	1	112.59	11.25	0.0047
	X_3 -Extraction time	877.76	1	877.76	87.69	< 0.0001
	X_4 -Speed	59.43	1	59.43	5.94	0.0288
	$X_1 X_2$	4.41	1	4.41	0.4406	0.5176
	X_1X_3	0.1111	1	0.1111	0.0111	0.9176
	X_1X_4	1.20	1	1.20	0.1198	0.7344
	$X_{2}X_{3}$	101.17	1	101.17	10.11	0.0067
Olive leaf	X_2X_4	22.40	1	22.40	2.24	0.1568
	X_3X_4	2.18	1	2.18	0.2177	0.6480
	X_1^2	196.74	1	196.74	19.65	0.0006
	$ \begin{array}{c} X_1^2 \\ X_2^2 \\ X_3^2 \end{array} $	0.8401	1	0.8401	0.0839	0.7763
	X_3^2	16.33	1	16.33	1.63	0.2223
	X_4^2	11.21	1	11.21	1.12	0.3079
	Residual	140.14	14	10.01		
	Lack of Fit	135.12	10	13.51	10.76	0.0175
	Pure Error	5.02	4	1.26		
	Cor Total	1827.88	28			
	Model	203.89	14	14.56	11.80	< 0.0001
	X_1	12.33	1	12.33	9.99	0.0069
	X2	84.48	1	84.48	68.45	< 0.0001
	X_3	10.69	1	10.69	8.66	0.0107
	X_4	9.05	1	9.05	7.33	0.0170
	X_1X_2	0.4900	1	0.4900	0.3970	0.5388
	X_1X_3	0.4444	1	0.4444	0.3601	0.5580
	X_1X_4	1.10	1	1.10	0.8893	0.3617
с <i>с</i> .,	X_2X_3	0.3211	1	0.3211	0.2602	0.6179
Grape fruit	X_2X_4	27.74	1	27.74	22.48	0.0003
	X_3X_4	5.22	1	5.22	4.23	0.0588
	X_1^2	0.1735	1	0.1735	0.1406	0.7133
	X_2^2	25.91	1	25.91	20.99	0.0004
	$ \begin{array}{c} X_1^2 \\ X_2^2 \\ X_3^2 \end{array} $	8.85	1	8.85	7.17	0.0180
	X_4^2	10.13	1	10.13	8.21	0.0125
	Residual	17.28	14	1.23		
	Lack of Fit	11.08	10	1.11	0.7153	0.6969
	Pure Error	6.20	4	1.55		
	Cor Total	221.17	28			

		Sum of		Mean		<i>p</i> -Value
	Source	Squares	df	Square	F Value	Prob > F
	Model	410.79	14	29.34	8.38	0.0001
	X_1	57.89	1	57.89	16.54	0.0012
	X_2	54.19	1	54.19	15.48	0.0015
	X_3	17.10	1	17.10	4.89	0.0442
	X_4	29.73	1	29.73	8.49	0.0113
	X_1X_2	0.3403	1	0.3403	0.0972	0.7598
	X_1X_3	0.6553	1	0.6553	0.1872	0.6718
	X_1X_4	36.00	1	36.00	10.29	0.0063
	X_2X_3	7.47	1	7.47	2.13	0.1661
Lemon peel	X_2X_4	4.35	1	4.35	1.24	0.2835
	X_3X_4	0.2268	1	0.2268	0.0648	0.8028
	X_{1}^{2}	126.78	1	126.78	36.22	< 0.0001
	X_2^2	15.87	1	15.87	4.53	0.0515
	$\bar{X_{3}^{2}}$	27.58	1	27.58	7.88	0.0140
	X_{4}^{2}	6.33	1	6.33	1.81	0.1999
	Residual	49.00	14	3.50		
	Lack of Fit	47.39	10	4.74	11.77	0.0148
	Pure Error	1.61	4	0.4025		
	Cor Total	459.79	28			
	Model	390.34	14	27.88	9.58	< 0.0001
	X_1	14.94	1	14.94	5.13	0.0399
	X_2	13.50	1	13.50	4.64	0.0492
	$\overline{X_3}$	67.65	1	67.65	23.24	0.0003
	X_4	74.42	1	74.42	25.57	0.0002
	X_1X_2	10.80	1	10.80	3.71	0.0746
	X_1X_3	0.8186	1	0.8186	0.2812	0.6042
	X_1X_4	1.09	1	1.09	0.3734	0.5509
Mandarin	$X_{2}X_{3}$	31.79	1	31.79	10.92	0.0052
peel	X_2X_4	4.00	1	4.00	1.37	0.2607
peer	X_3X_4	0.8372	1	0.8372	0.2876	0.6002
	X_{1}^{2}	32.63	1	32.63	11.21	0.0048
	X_2^{2}	8.20	1	8.20	2.82	0.1154
	X_{3}^{2}	79.47	1	79.47	27.30	0.0001
	X_{4}^{2}	35.33	1	35.33	12.14	0.0037
	Residual	40.76	14	2.91		
	Lack of Fit	39.24	10	3.92	10.37	0.0187
	Pure Error	1.51	4	0.3784		
	Cor Total	431.09	28	0.0.0.2		

Table 5. Cont.

Another statistical parameter to determine the adequacy of the proposed models for the experimental data is the value of *lack of fit*. The model proposed for grapefruit peel extraction had a non-significant lack of fit value (p > 0.05), meaning that the model is in good agreement with the experimental output. However, the remaining models had significant values for lack of fit, showing similarity with the other reports [33–38]. Kittisuban et al. declared that lack of fit with a significant value might be acceptable if there are lots of data in the relevant process system [37].

3.2. Effects of Independent Variables on the TBC Yields

Solid mass had a negative effect on each system (Figures 1a–4a). This result is to be expected from a mass transfer point of view [31]. By increasing the solid mass, the liquid extract was saturated with the target components, which unfavored the rate of mass transfer by preventing the diffusion of the biophenols into the solvent [39]. On the other hand, increasing the solvent concentration in water favored the extraction at first (Figures 1b–4b). Later, it started to decrease after the composition reached to a value of \approx 50% (v/v). Similar observations have also been attained in other reports, where

bioactive ingredients were extracted from several natural sources [40–42]. A decrease in the amount of ethanol amount in water might be hypothesized by the denaturation property of the ethanol [32]. Regarding extraction time, there was a markable increase in each system (Figures 1b–4b). Zhong and Wang [43], Silva et al. [44] and Ramić et al. [45] also had observed similar results for the time effect on the extraction of various natural products. Mixing speed had a slight effect on both olive leaf and lemon peel extraction (Figures 1c and 3c). As for grapefruit peel and mandarin peel extractions, speed of the homogenizer decreased the TBC yields up to a certain value, at which point the yield began to rise. This might be attributable to the initial degradation of the biophenol-degrading enzymes, which in turn caused these bioactive substances to precipitate [46].

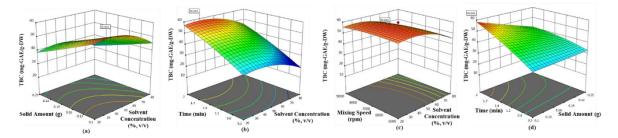


Figure 1. Response surface plot for the TBC of olive leaf extract (**a**) as a function of solvent concentration to solid mass (extraction time = 2 min and mixing speed = 6517.41 rpm); (**b**) as a function of solvent concentration to time (solid mass = 0.1 g and mixing speed = 6517.41 rpm); (**c**) as a function of solvent concentration to mixing speed (solid mass = 0.1 g and extraction time = 2 min); (**d**) as a function of solvent solid mass to extraction time (solvent concentration = 34.31 and mixing speed = 6517.41 rpm).

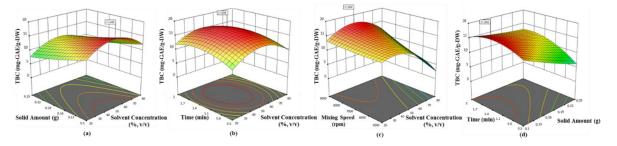


Figure 2. Response surface plot for the TBC of grapefruit peel extract (**a**) as a function of solvent concentration to solid mass (extraction time = 1.125 min and mixing speed = 5000 rpm); (**b**) as a function of solvent concentration to time (solid mass = 0.1 g and mixing speed = 5000 rpm); (**c**) as a function of solvent concentration to mixing speed (solid mass = 0.1 g and extraction time = 1.125 min); (**d**) as a function of solid mass to extraction time (solvent concentration = 42.32 and mixing speed = 5000 rpm).

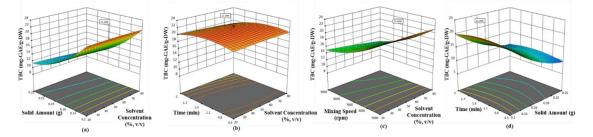


Figure 3. Response surface plot for the TBC of lemon peel extract (**a**) as a function of solvent concentration to solid mass (extraction time = 1.34 min and mixing speed = 8999.99 rpm); (**b**) as a function of solvent concentration to time (solid mass = 0.1 g and mixing speed = 8999.99 rpm); (**c**) as a function of solvent concentration to mixing speed (solid mass = 0.1 g and extraction time = 1.34 min); (**d**) as a function of solid mass to extraction time (solvent concentration = 48.09 and mixing speed = 8999.99 rpm).

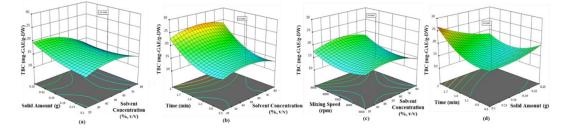


Figure 4. Response surface plot for the TBC of mandarin peel extract (**a**) as a function of solvent concentration to solid mass (extraction time = 0.70 min and mixing speed = 6372.15 rpm); (**b**) as a function of solvent concentration to time (solid mass = 0.154 g and mixing speed = 6372.15 rpm); (**c**) as a function of solvent concentration to mixing speed (solid mass = 0.154 g and extraction time = 0.70 min); (**d**) as a function of solid mass to extraction time (solvent concentration = 30.80 and mixing speed = 6372.15 rpm).

3.3. Verification of the Suggested Conditions

Table 6 summarizes the optimum HAE conditions for TBC from each residue to achieve the greatest yield with the verification results. The second-order polynomial models proposed for the relevant systems have been confirmed to be satisfactory to estimate the suggested conditions depending on the small and acceptable levels of error rate (%).

			I	Maximum		
Item	Optimum Extraction Conditions		TBC (mg-GAE/g-DW)			
			Experimental	Predicted	Error%	
	X_1 (%. v/v)	34.24				
Oliver level	X_2 (g)	0.100	E9 ()	E0.16	0.02	
Olive leaf	X_3 (min)	2.00	58.62	59.16	0.92	
	X_4 (rpm)	6522.2				
	<i>X</i> ₁	42.33		21.46		
Grapefruit peel	X_2	0.100	21.12		1 (1	
Giaperiun peer	X_3	1.125			1.61	
	X_4	5000				
	X_1	33.62		10.00		
Lemon peel	X_2	0.100	16.89		1.07	
Lemon peer	X_3	1.282	16.89	17.07	1.07	
	X_4	5007				
	X_1	42.5				
Mandarin peel	X_2	0.100	27.70	20.04	1 1 1	
	$\overline{X_3}$	1.99	27.79	28.94	4.14	
	X_4	8772				

Table 6. Verification results of the optimum conditions for the HAE of each residue.

3.4. Evaluation of the Bioactive Ingredients in the Extracts

Table 7 demonstrates the quantitative results of the most prominent phenolic compounds of each item. When the spectrophotometric analysis is assessed (Table 8), the related biophenols have proven to be the most contributing compounds to bioactive properties. A mathematical statement can be formed to confirm the concerned relationship by means of correlation coefficients between the relevant dependent variables (oleuropein/naringin and TBC; oleuropein/naringin and DPPH/CUPRAC/ABTS; TBC and DPPH/CUPRAC/ABTS). When the coefficients of correlation (0.8517) are checked, a strong relationship between the individual and total biophenols is observed. Furthermore, the relationships (>0.94) between the total biophenols and each antioxidant activity assay finding are also extremely

satisfactory for verifying the contribution of total biophenols to the antioxidant capacity of the selected waste products.

Table 7. Major bioactive compounds derived from the selected byproducts under optimal extraction conditions *.

Item	R _t (min)	Major Biophenols	Concentration (mg/g-DW)
Olive leaf	5.910	Oleuropein	79.26 ± 0.001 ^a
Grapefruit peel	5.400	Naringin	36.10 ± 0.001 ^b
Lemon peel	5.400	Naringin	10.33 ± 0.002 ^c
Mandarin peel	5.400	Naringin	25.56 ± 0.001 ^d

* Data are given as the mean (n = 3) \pm standard deviation. Lines not sharing a common (a, b, c and d) letter indicate significant differences at p < 0.001.

Item.	TBC (mg-GAE/g-DW)	DPPH (mg-TAEC/g-DW)	CUPRAC (mg-TAEC/g-DW)	ABTS (mg-TAEC/g-DW)
Olive leaf	16.86 ± 0.004 ^a	20.39 ± 0.001 ^a	64.01 ± 0.003 ^a	60.12 ± 0.001 ^a
Grapefruit peel	5.39 ± 0.002 ^b	1.78 ± 0.001 ^b	20.61 ± 0.001 ^b	555.02 ± 0.002 ^b
Lemon peel	3.44 ± 0.001 ^c	2.36 ± 0.001 ^c	24.05 ± 0.002 ^c	69.71 ± 0.002 ^c
Mandarin peel	8.96 ± 0.003 ^d	5.58 ± 0.002 ^d	32.34 ± 0.003 ^d	326.76 ± 0.004 ^d

Table 8. Antioxidant properties of the relevant residues *.

* Data are given as the mean (n = 3) \pm standard deviation. Lines not sharing a common letter (a, b, c and d) indicate significant differences at p < 0.001.

On the other hand, selected antioxidant activity methods also showed positive correlations with each other. The correlation coefficients between DPPH and CUPRAC, CUPRAC and ABTS, and DPPH and ABTS were found as 0.9955, 0.9052 and 0.8764, respectively.

3.5. Infrared Spectra of the Extracts

A large variety of samples such as powders, films, liquids and solids can be studied using this characterization technique which clarifies the functional groups in the samples studied. Figure 5 demonstrates the FTIR spectra of the selected waste extracts obtained at optimum conditions, which comprises the range between 4000 and 500 cm⁻¹. The peaks ranging from 3010 to 3670 cm⁻¹ correspond to the O–H stretch of the hydroxyl group, comprising biophenols and alcohols [47]. The sharper peaks observed between 3409 and 1733 cm⁻¹ are assigned to C=O and O–H stretchings, which are attributable to oleuropein, naringin and other phenolic compounds of the leaf and peel extracts [48]. The band located at 500–800 cm⁻¹ characterizes C–H, denoting the alkanes and aromatics [49].

3.6. Nanostructural Morphologies of the Extracts

AFM is a suitable technique to explore the parameters of average surface roughness, homogeneity and particle size distribution for biomaterials with high resolution topographic images [50]. Evaluation of the interfacial behavior of the surface is crucial to understanding the interactions of the selected systems. In this regard, AFM was conducted to realize the morphological and nanostructure changes of the extracted materials. This technique provided a visualization of the deposited materials with a nanometric resolution. Figure 6a,b demonstrates two-dimensional (2D) AFM images of the olive leaf samples obtained before and after the extraction processes, respectively. From the 2D images, cross-section profiles and histograms, it is revealed that untreated leaves have more grains and particles when compared to those of treated samples. The significant difference observed between these two structures is due to the extraction process. As can be seen in Figure 6a, the heterogeneously distributed particles of various sizes cover all of the surfaces. The chemical composition of the olive leaves, consisting of the minerals, chlorophylls, fatty acids and phenolic substances, are removed after the extraction process. The histogram plots clarified that the average size distribution was about 750 nm for the untreated samples, while it was nearly 250 nm for the treated leaves.

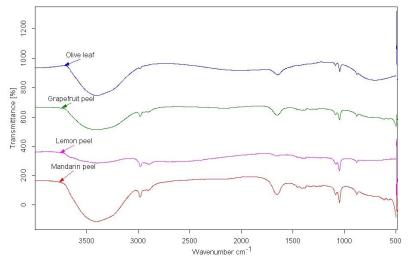


Figure 5. FTIR spectra of the relevant residues.

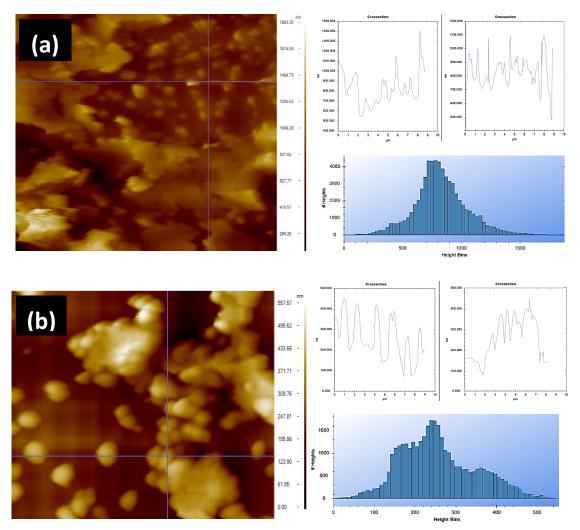


Figure 6. 2D AFM- atomic force microscopy images, cross-section profiles and histograms of the olive leaf samples (**a**) before and (**b**) after extraction.

Figure 7a,b represents the lemon peel before and after extraction processes. It is noteworthy that the lemon peel had a spikier structure after the extraction process compared with the randomly distributed particles shown in Figure 7a. The spaces and the valleys in the sample obtained after the extraction process were higher than the untreated lemon peels. According to the histogram plots, the average heights of the particles are different, while their size distributions are nearly the same. After the extraction process, compact, spiky and porous structures were observed, indicating some biophenolic substances were removed from the peel matrix.

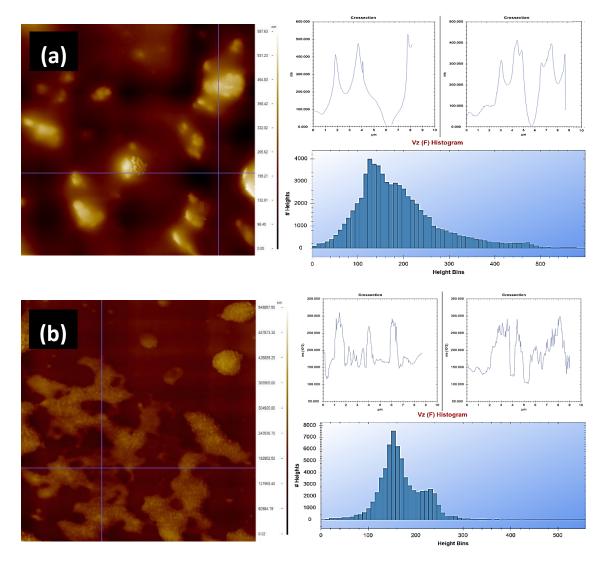


Figure 7. 2D AFM images, cross-section profiles and histograms of the lemon peel samples (**a**) before and (**b**) after extraction.

4. Conclusions

Olive leaf was found to possess the highest phenolic ingredients (58.62 mg-GAE/g-DW with 0.1 g sample, 42.5% ethanol at 6522.2 rpm for 2 min), followed by mandarin peel (27.79 mg-GAE/g-DW with 0.1 g sample, 34.24% ethanol at 8772 rpm for 1.99 min), grapefruit peel (21.12 mg-GAE/g-DW with 0.1 g sample, 42.33% ethanol at 5000 rpm for 1.125 min) and lemon peel (16.89 mg-GAE/g-DW with 0.1 g sample, 33.62% ethanol at 5007 rpm for 1.282 min). The quadratic models proposed by Box–Behnken design were found satisfactory, depending on the statistical results (p < 0.0001 and $R^2 > 0.89$). The convincing correlation coefficients (>0.94) between the phenolic ingredients and antioxidant activity tested by each assay proved that polyphenols in the selected waste products

were the most contributing substances of bioactive properties. Hereby, the present findings will be guidance for science researchers, consumers and commercial entities (cosmetic, pharmaceutical and food industries) with a green process developed for the extraction of the most popular Mediterranean crops. On the other hand, additional studies are necessary to determine whether there is a link between possible prominent compounds in the extracts related to health benefits. In short, the need for newly developed natural additives is very clear, but the most important issue is to be careful that the product is reliable.

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