

Article

# Olivine-Based Blended Compounds as Positive Electrodes for Lithium Batteries

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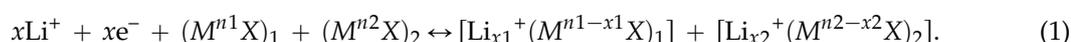
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**Abstract:** Blended cathode materials made by mixing LiFePO<sub>4</sub> (LFP) with LiMnPO<sub>4</sub> (LMP) or LiNi<sub>1/3</sub>Mn<sub>1/3</sub>Co<sub>1/3</sub>O<sub>2</sub> (NMC) that exhibit either high specific energy and high rate capability were investigated. The layered blend LMP–LFP and the physically mixed blend NMC–LFP are evaluated in terms of particle morphology and electrochemical performance. Results indicate that the LMP–LFP (66:33) blend has a better discharge rate than the LiMn<sub>1–y</sub>Fe<sub>y</sub>PO<sub>4</sub> with the same composition ( $y = 0.33$ ), and NMC–LFP (70:30) delivers a remarkable stable capacity over 125 cycles. Finally, *in situ* voltage measurement methods were applied for the evaluation of the phase evolution of blended cathodes and gradual changes in cell behavior upon cycling. We also discuss through these examples the promising development of blends as future electrodes for new generations of Li-ion batteries.

**Keywords:** blend; insertion compounds; olivine; layered materials; Li-ion batteries

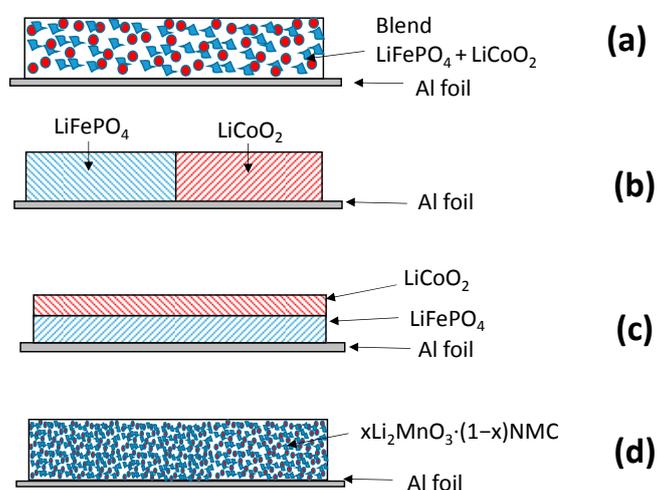
## 1. Introduction

Recent advances to develop highly effective electrode materials for Li-ion batteries (LIBs) derived from composites or blended architectures are new technological approaches to designing high-energy and high-power density storage systems [1,2]. The blend electrode is an active material formed by a mixture of two or more distinct lithium insertion compounds that possess percolating frameworks for ions and electrons to achieve better balanced electrochemical performance than that of an individual compound. We can consider four configurations: a complete physical mixture, a segregated blend, a layered-type blend and an integrated blend cathode (Figure 1). Sometimes, the notion of a blend is restricted to the case of physical mixture, but the notion in the present work is extended to all the configurations, including another one, the core-shell structure, where one of the components is the core and the other one is the shell of a particle. For materials currently used as positive electrodes in lithium batteries, the different crystal chemistries are examined from the basic reaction driven by a charge transfer from the guest Li<sup>+</sup> ions to the conduction band of the host compound. Thus, electron-donating species of a blend electrode composed of two components—(M<sup>n1</sup>X)<sub>1</sub> and (M<sup>n2</sup>X)<sub>2</sub> (where M is a transition metal with oxidation state n<sub>i</sub>, and X is an anion) host components—can give rise to a reversible reaction classically represented by the following scheme:



In the usual case,  $x_i$  is the molar lithium insertion fraction, and  $[\text{Li}_{x_i}^+(M^{n,i-x_i}X)_i]$  is the final product. The concept of using two or more electrochemically active materials in a blend matrix is not new; since 1976, Margalit suggested applying  $x\text{Ag}_3\text{PO}_4 \cdot (1-x)\text{Ag}_2\text{CrO}_4$  to a Li primary battery for pacemakers and watches [3]. This concept has been extended to numerous cathode materials to avoid their individual drawbacks [4–7]. Pynenburg *et al.* [4] patented a rechargeable lithium cell composed of a physical mixture of spinel  $\text{Li}_x\text{Mn}_2\text{O}_4$  and one of the lithiated metal oxides from the  $\text{Li}_x\text{MO}_2$  group ( $M = \text{Ni}, \text{Co}$ ), wherein  $0 < x \leq 2$ . For instance, pure  $\text{LiMn}_2\text{O}_4$  has a better rate capability than pure  $\text{LiNi}_{0.8}\text{Co}_{0.15}\text{Al}_{0.05}\text{O}_2$ , but, at a low rate, the specific energy of  $\text{LiNi}_{0.8}\text{Co}_{0.15}\text{Al}_{0.05}\text{O}_2$  is higher than that of  $\text{LiMn}_2\text{O}_4$ , so that mixing the two elements should lead to an optimized compromise [5,7]. Other effects not necessarily expected have been observed. Numata *et al.* [5] showed the advantages of blending  $\text{Li}_{1+x}\text{Mn}_{2-x}\text{O}_4 \cdot \text{LiNi}_{0.8}\text{Co}_{0.15}\text{Al}_{0.05}\text{O}_2$ , which decreased the Mn dissolution from the spinel into the electrolyte. Meanwhile, however, it increased the irreversible capacity loss in the first cycle and deteriorated the rate capability. Albertus *et al.* [7] adopted a mathematical model to multiple types of active materials in a single electrode to treat both direct (galvanostatic) and alternating (impedance) currents and concluded that combining a sloped-potential system ( $\text{LiNi}_{0.8}\text{Co}_{0.15}\text{Al}_{0.05}\text{O}_2$ ) with a flat-potential system ( $\text{LiMn}_2\text{O}_4$ ) may assist in electrode state-of-charge (SOC) determination. In 2011, LIBs (composed of 288 Li-ion cells) using a blended cathode formed by the mixture  $\text{LiMn}_2\text{O}_4 \cdot \text{LiNi}_x\text{Mn}_y\text{Co}_{1-x-y}\text{O}_2$  were developed by LG Chem. Ltd. and applied to power the GM Chevy-Volt electric vehicles [8]. In 2006, Kim *et al.* [6] studied the  $0.5\text{LiCoO}_2 \cdot 0.5\text{LiNi}_{1/3}\text{Mn}_{1/3}\text{Co}_{1/3}\text{O}_2$  (LCO–NMC)-mixed cathode exhibiting a stable cycleability maintained at *ca.* 163 mAh  $\cdot \text{g}^{-1}$ .

Depending on the nature and the combination of materials, the blending found different advantages (but not all of them at the same time), such as (i) the inhibition of overheating effects during overcharge conditions; (ii) a reduction in irreversible capacity decay; (iii) an improvement of cycling life; (iv) a rise of the discharge C-rate; and (v) endurance of high temperature and thermal stability [9–12].



**Figure 1.** Scheme of the four different configurations of blended cathodes: (a) completely intermixed, (b) segregated, (c) layered, and (d) integrated cathode.

The literature of olivine-based blended active cathode materials is rather sparse. The good thermal stability of olivine-structured compounds  $\text{LiMPO}_4$  ( $M = \text{Fe}, \text{Mn}$ ) makes them attractive cathode materials, but the relatively flat voltage plateau at 3.45 V *vs.*  $\text{Li}^0/\text{Li}^+$  is a limitation, which yields difficult the SOC evaluation. This drawback can be overcome using a blend of olivine with a layered material. Various mixtures have been tested such as the blend of  $\text{LiFePO}_4$  (LFP) with Li-rich NMC [13,14], which exhibits improved power capability, thermal stability, and easy SOC monitoring. In another approach, a blend of  $\text{LiFePO}_4$  with  $\text{Li}_3\text{V}_2(\text{PO}_4)_3$  (LVP) delivers lower capacity and has

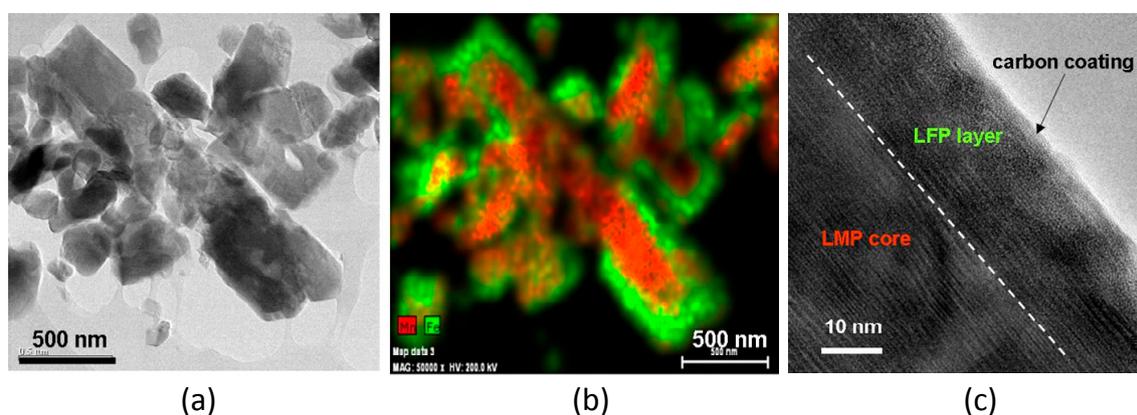
a voltage profile consisting of multiple plateaus due to the LVP component [15]. Uniform blends of micron-sized  $\text{LiMn}_2\text{O}_4$  with nano-sized  $\text{LiFePO}_4$  (1:1 mass ratio) prepared by ball milling showed that LFP powders not only cover the  $\text{LiMn}_2\text{O}_4$  particles but also effectively fill the cavity of the spinel network [16]. Recently, blend electrodes were prepared by mixing the olivine  $\text{LiFe}_{0.3}\text{Mn}_{0.7}\text{PO}_4$  (LFMP) and  $\text{LiMn}_{1.9}\text{Al}_{0.1}\text{O}_4$  spinel (LMO) in order to obtain a composite electrode, combining the high capacity of LFMP and the rate capability of the spinel [17].

In this paper, we discuss the architecture, the structural properties, and the electrochemical performance of two  $\text{LiFePO}_4$ -based blend systems as positive electrodes for lithium batteries: (i) the blend fabricated by  $\text{LiFePO}_4$  with  $\text{LiMnPO}_4$  (LMP) olivine structures, and (ii) the blend formed by the  $\text{LiFePO}_4$  olivine structure with the  $\text{LiNi}_{0.33}\text{Mn}_{0.33}\text{Co}_{0.33}\text{O}_2$ -layered compound. In both systems, the use of carbon-coated LFP results in an increase in electrode conductivity and rate capability. Thus, we show that blending may be a good solution to avoid individual drawbacks of components.

## 2. Results

### 2.1. $\text{LiMnPO}_4$ - $\text{LiFePO}_4$ (LMP-LFP) Blended Electrode

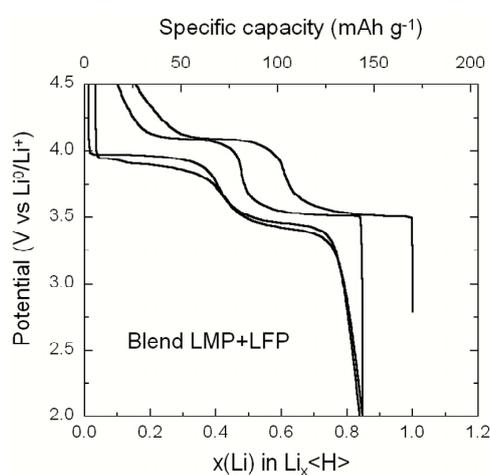
To overcome the difficulty of carbon coating on  $\text{LiMnPO}_4$  (LMP) olivine particles, it is possible to prepare a  $\text{LiMnPO}_4$ - $\text{LiFePO}_4$  (LMP-LFP) composite, in which the carbon-coated LFP component encapsulates the core of  $\text{LiMnPO}_4$  particles to take advantage of the catalytic reaction of Fe with C. The STEM images of several particles representative of the sample are shown in Figure 2. Figure 2a displays well-crystallized flaky grains several tens to 100 nm in size. Some of the grains have with many dislocations. A typical EDX map (Figure 2b) shows the two components of blended particles: LMP (in red) in the center, surrounded with a LFP layer (in green). Elemental analysis indicates the LMP-LFP (66:33) composition. The Fe content is minimal at the center and maximal at the surface, while the opposite holds true for the Mn content. The HRTEM image (Figure 2c) shows the lattice fringes with the sharp interface between  $\text{LiMnPO}_4$  and  $\text{LiFePO}_4$  and the continuous carbon-coating layer (~2–3 nm thick). To summarize the results illustrated by the structural analysis, LFP forms a continuous layer that partly covers most of the LMP particles, but it also forms few small  $\text{LiFePO}_4$  particles distributed sparsely (Figure 2). The strain at the interface between the two materials is accommodated by extended defects such as dislocations and grain boundaries; on the other hand, the LFP layer is well crystallized as evidenced by the lattice fringes in the HRTEM image (Figure 2c). This result suggests that LFP is deposited by some epitaxial effect on the well-crystallized surface of LMP, since the free surface of LFP at 600 °C is disordered [18].



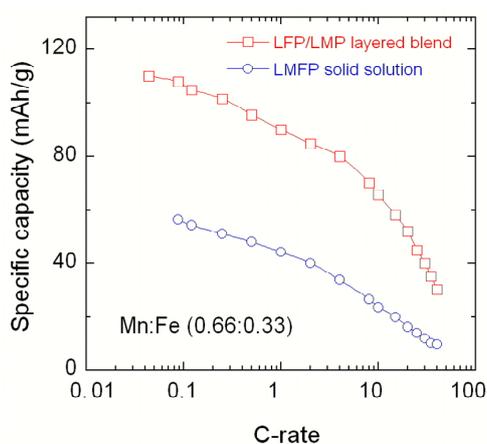
**Figure 2.** (a) STEM image of the  $\text{LiMnPO}_4$ - $\text{LiFePO}_4$  (LMP-LFP) blend particle showing the different layers; (b) The typical EDX map of LMP (in red)-LFP (in green) particle; (c) HRTEM image showing the lattice fringes with the sharp interface between  $\text{LiMnPO}_4$  and  $\text{LiFePO}_4$  and the continuous, carbon layer.

The electrochemical features of the LMP-LFP (66:33) blend is illustrated in Figure 3, showing the charge-discharge profiles *vs.* specific capacity of the Li//blend coin cell for the first two cycles.

Electrochemical tests were carried out at C/12 in the potential range 2.0–4.5 V *vs.* Li<sup>0</sup>/Li<sup>+</sup>. The upper flat part corresponds to the limit of 4.5 V imposed on the potential to protect the electrolyte. The first plateau observed at 3.5 V is characteristic of the Fe<sup>2+</sup>/Fe<sup>3+</sup> redox potential *vs.* Li in LiFePO<sub>4</sub>. The next plateau at 4.0 V is characteristic of the Mn<sup>2+</sup>/Mn<sup>3+</sup> potential in LiMnPO<sub>4</sub>, so that both components efficiently contribute to the electrochemical properties. We find that the specific capacity of the first charge is 144 mAh·g<sup>-1</sup> (charge transfer of  $x = 0.86e^-$ ) followed by the discharge/charge ratio close to unity at the second cycle. Using such a blended electrode, the electrochemical properties are improved with respect to the carbon-coated LiMn<sub>2/3</sub>Fe<sub>1/3</sub>PO<sub>4</sub> solid solution with a comparable Fe/Mn ratio, as shown in Figure 4. The Peukert plots show that, at 10C, the delivered capacity of the blend is 65.5 mAh·g<sup>-1</sup> against 23.5 mAh·g<sup>-1</sup> for LiMn<sub>2/3</sub>Fe<sub>1/3</sub>PO<sub>4</sub>. Therefore, the use of a LiFePO<sub>4</sub> as a buffer layer between the high-density cathode element (like LiMnPO<sub>4</sub>) and the carbon layer opens a new route to improve the performance of the olivine family as the active element of the cathode for Li-ion batteries. This result is attributable to the fact that the LFP shell allows for the coating of the composite, while it is difficult to deposit the carbon at the surface of LMP at a temperature small enough to avoid its decomposition ( $\approx 650$  °C).



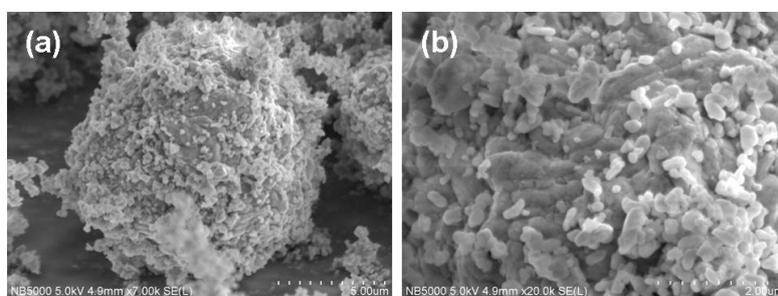
**Figure 3.** Charge-discharge profiles of Li coin cell with a LMP–LFP (66:33) blend positive electrode for the 1st and 2nd cycle. Electrochemical tests were carried out at C/12 in the potential range 2.0–4.5 V *vs.* Li<sup>0</sup>/Li<sup>+</sup>.



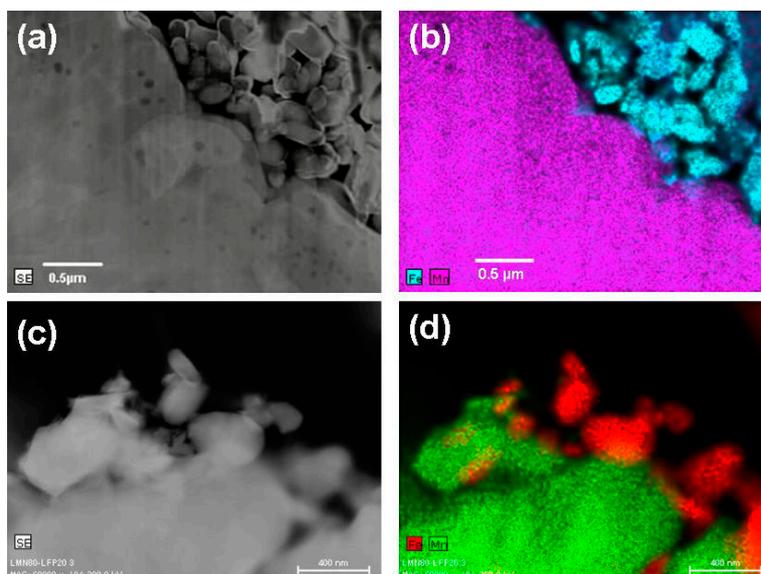
**Figure 4.** Peukert plot of the LMP–LFP blend compared with the cathode of the same composition formed by the LiMn<sub>1-y</sub>Fe<sub>y</sub>PO<sub>4</sub> ( $y = 0.33$ ) solid solution.

## 2.2. $\text{LiNi}_{1/3}\text{Mn}_{1/3}\text{Co}_{1/3}\text{O}_2\text{-LiFePO}_4$ (NMC-LFP) Blended Electrode

A blended cathode formed by the  $\text{LiNi}_{1/3}\text{Mn}_{1/3}\text{Co}_{1/3}\text{O}_2\text{-LiFePO}_4$  (NMC-LFP) mixture exhibits excellent rate capability by using nano-sized LFP particles and delivers higher capacity, *i.e.*,  $180 \text{ mAh}\cdot\text{g}^{-1}$ , due to the NMC component. Consequently, a Li-ion battery including NMC-LFP physical blending provides a good solution that achieves both energy and power capability and exhibits improved electrochemical features with thermal stability similar to LFP. In the SEM images of the NMC-LFP (70:30) blend shown in Figure 5, one discerns the two distinct components of this blend. The cathode material prepared by ultra-microtomy exhibits large spherically shaped NMC particles (secondary particles  $\sim 10 \mu\text{m}$  in size, having a very close size distribution) and small LFP nano-sized particles ( $<0.5 \mu\text{m}$ ), but no LFP coating on NMC is observed. This could be due to the mechanical force applied during the microtomy. Figure 6 shows the TEM images and EDX maps of NMC-LFP blends with different compositions: (a) (70:30) with Fe in blue, Mn in violet and (b) (80:20) with Fe in red, Mn in green. The differences in morphology and particle size between the two samples are evidenced. Higher SEM magnification confirms that the co-grounded blend sample possesses a better coverage of NMC with LFP than the (80:20) sample.



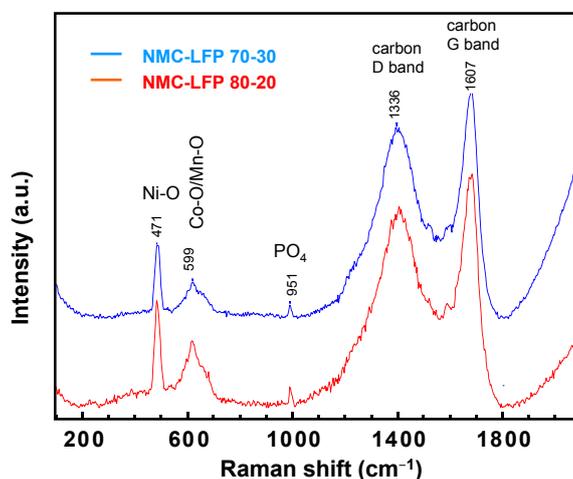
**Figure 5.** SEM images of the  $\text{LiNi}_{1/3}\text{Mn}_{1/3}\text{Co}_{1/3}\text{O}_2\text{-LiFePO}_4$  (NMC-LFP) (70:30) blend powders showing (a) big NMC particle surrounded by nano-sized LFP and (b) a detail of the blend.



**Figure 6.** TEM images and EDX maps of NMC-LFP blends with different compositions. (a,b) 70:30 (Fe in blue, Mn in violet) and (c,d) 80:20 (Fe in red, Mn in green).

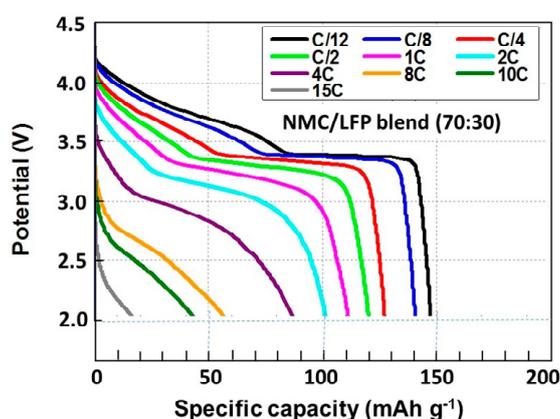
The structural properties of the NMC-LFP blends were studied by Raman spectroscopy as shown in Figure 7. A typical Raman spectrum displays three sets of bands: (i) the vibrational features of

NMC with Ni–O mode at  $471\text{ cm}^{-1}$  and the broad band at *ca.*  $600\text{ cm}^{-1}$  attributed to the Co–O/Mn–O stretching modes [19]; (ii) the symmetric stretching vibration of  $\text{PO}_4^{3-}$  molecular units of  $\text{LiFePO}_4$  at around  $950\text{ cm}^{-1}$ ; and (iii) two broad Raman bands of the carbon surrounding the LFP particles centered at  $1336$  and  $1607\text{ cm}^{-1}$  assigned to the D- and G-bands, respectively. Note that the high intensity of the latter bands is due to the strong Raman scattering efficiency of carbon [20].

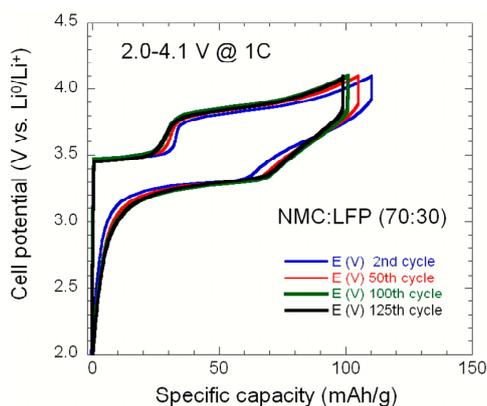


**Figure 7.** Raman spectra of NMC–LFP blends. Spectra were recorded using a 514.5 nm laser line excitation.

Figure 8 shows the discharge profiles (5th cycle) as a function of the C-rate for a Li-coin cell with the NMC–LFP (70:30) blend as positive electrode. Electrochemical tests were carried out in the potential range 2.0–4.2 V *vs.*  $\text{Li}^0/\text{Li}^+$ . The shape of the curves shows combined features of LFP with the potential plateau at 3.35 V and the sloppy profile of the NMC component from 3.4 to 4.2 V (see discussion below). This behavior suggests the independent charge–discharge profiles of the cathode constituents. The discharge capacity is  $148\text{ mAh}\cdot\text{g}^{-1}$  at C/12 rate and  $42\text{ mAh}\cdot\text{g}^{-1}$  at 10C. Note that, as some  $\text{Li}^+$  ions are not removed from NMC at 4.2-V cut-off voltages, this causes a lower specific capacity. The electrochemical performance of a Li-coin cell with the NMC–LFP (70:30) blend positive electrode as a function of the number of cycles at 1C rate (Figure 9) shows that this cathode material exhibits very stable cycleability after 125 cycles.

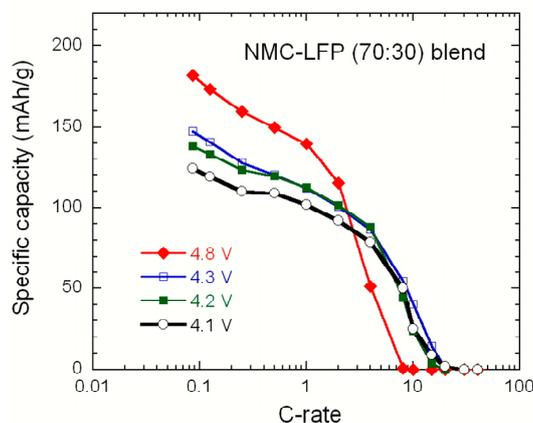


**Figure 8.** Discharge profiles (5th cycle) as a function of the C-rate of Li-coin cell with a NMC–LFP (70:30) blend positive electrode. Electrochemical tests were carried out in the potential range 2.0–4.2 V *vs.*  $\text{Li}^0/\text{Li}^+$ .



**Figure 9.** Electrochemical performance of a Li coin cell with a NMC–LFP (70:30) blend positive electrode as a function cycle.

The Peukert plots of the NMC–LFP (70:30) blended electrode cycled at different cut-off voltages are shown in Figure 10. These results indicate that (i) the 4.8-V cut-off provides the higher specific capacity of  $180 \text{ mAh} \cdot \text{g}^{-1}$  at a C/10 rate, but shows the lowest performance at high rates; (ii) higher capacity was obtained when the voltage cut-off was higher than 4.1, 4.2, and 4.3 V; and (iii) for the 4.1-V cut-off, the capacity fade is less pronounced, *i.e.*,  $0.12 \text{ mAh} \cdot \text{g}^{-1}$  per cycle. The impedance measurements, after formation cycles, show an increase in the charge transfer resistance at a voltage cut-off of 4.8 V, and a comparable result is observed with 4.1 and 4.3 V cut-off. As pointed out by Imachi *et al.* [12], who investigated a double-layered  $\text{LiCoO}_2 \cdot \text{LiFePO}_4$  blended cathode, the advantage of blending LFP consists in the creation a resistive barrier that improves the tolerance against overcharging the electrochemical cell.



**Figure 10.** Specific capacity of the NMC–LFP (70:30) blended electrode as a function of C-rate in lithium cells cycled at different cut-off voltages.

### 3. Phase Evolution

*In situ* voltage measurement methods have been applied for the evaluation of the phase evolution of blended cathodes and gradual changes in cell behavior upon cycling. Using the so-called incremental capacity (IC) with respect to cell potential,  $dQ/dV = f(V)$ , and the differential voltage curve  $dV/dQ = f(Q)$  could provide such information, since voltage plateaus in the V–Q profile is identifiable by  $dQ/dV$  peaks on IC curves [21,22].

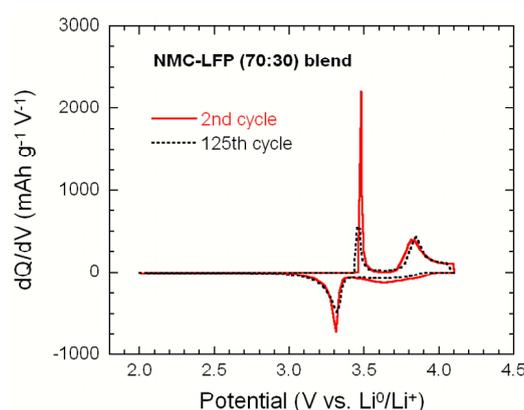
Figure 11 presents the incremental capacity *vs.* potential for the Li coin cell with the NMC–LFP (70:30) blend cathode. The peaks in Figure 11 should only relate to the positive electrode material since the negative electrode is lithium metal. The typical IC curves of the blend clearly display two sets of

redox peaks, each one related to the NMC or LFP component. The IC of the blend exhibits a sharp peak at 3.47 V corresponding to the voltage plateau of the charge profile  $Q$  vs.  $V$  due to the  $\text{Fe}^{2+}/\text{Fe}^{3+}$  oxidation in the LFP component followed by a broad feature at 3.85 V corresponding to the  $\text{Ni}^{2+}/\text{Ni}^{4+}$  oxidation in the NMC component. The reduction processes occurred at 3.65 and 3.32 V, respectively. The IC curves show that the decrease in the area of the LFP peak at 3.47 V on charge, along with the slight evolution of the peak at 3.32 V on discharge, while the redox NMC peaks are almost unchanged after 125 cycles. These results reveal the possible mechanisms involved in the blend material that could be associated with the strain–stress field interaction in the particles due to the mechanical milling preparation with the net effect of shortening the 3.47-V plateau. Thus, changes in the  $dQ/dV$  curves can help to identify ageing of electrode materials [23].

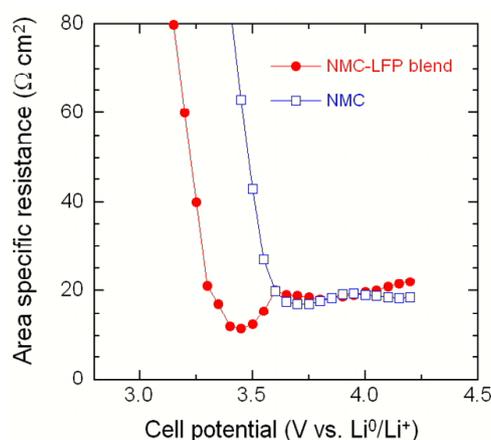
Another typical test to characterize the power capability of a cell at different state of charge (SOC) is the plot of the area specific resistance (ASR) vs. the cell potential defined by the Equation (2):

$$\text{ASR} = \frac{V_{\text{oc}} - V_{\text{cell}}}{I} A, \quad (2)$$

where  $V_{\text{oc}}$  is the open-circuit voltage,  $I$  the current, and  $A$  is the electrode area. As presented in Figure 12, the ASR of the NMC cell drops sharply for potential  $V_{\text{cell}} < 3.5$  V, which is an inherent electrochemical feature of layered oxides, while the ASR of the NMC–LFP blend increases sharply at lower potential, *ca.* 3.25 V. These results show that the blend cathode can deliver high power at low SOC due to the 3.5-V plateau of the discharge curve of LFP.



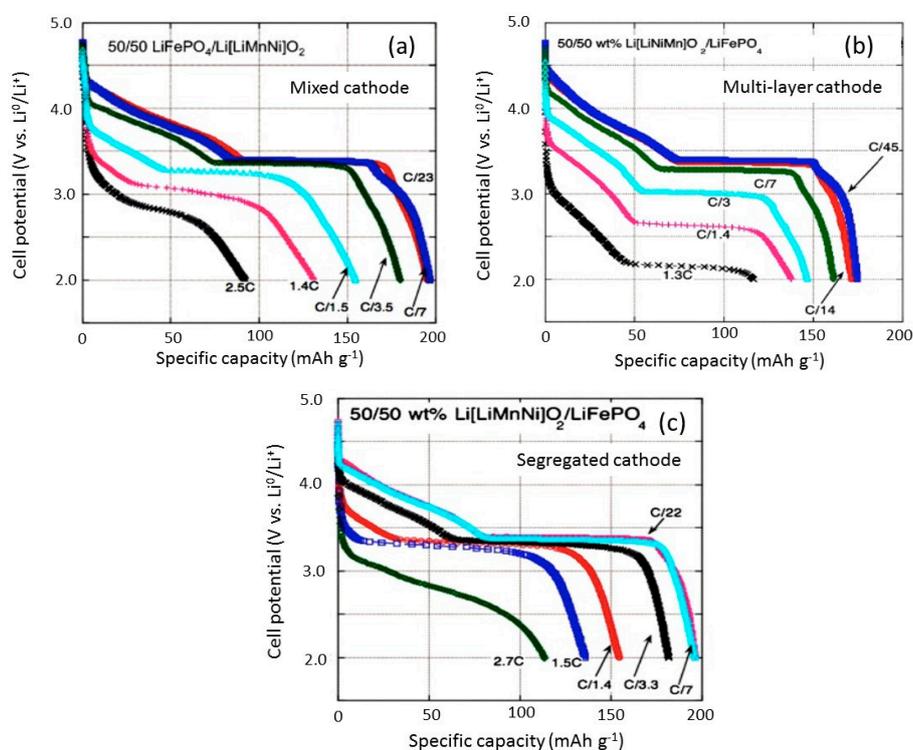
**Figure 11.** Incremental capacity  $dQ/dV$  of the NMC–LFP (70:30) blended electrode vs. potential as a function of the cycle number.



**Figure 12.** Plot of the area specific resistance of NMC and NMC–LFP blend as a function of the cell potential showing the increase in area specific resistance (ASR) at low state of charge (SOC).

#### 4. Discussion

The results we report here enable the evaluation of the blends as new cathodes in a given geometry. This remains to be determined and chosen to optimize the electrochemical performance. In the case of the LMP–LFP blend, the core-shell geometry must be chosen because the purpose is to have a conductive carbon coating layer that could be deposited more efficiently on LFP than on LMP. In the case of NMC–LFP, only the case of mixed powders was investigated. To our knowledge, the only work where the effect of the geometrical distribution of the powders has been investigated is the comparison between the electrochemical properties of cells prepared with positive electrodes made of  $\text{Li}[\text{Li}_{0.17}\text{Mn}_{0.58}\text{Ni}_{0.25}]\text{O}_2$ –LFP blend in the completely intermixed, segregated, and layered geometries (see Figure 1) [13]. The discharge profiles are reported in Figure 13 for the case of an equal ratio of the two powders at different C-rates after few initial cycles devoted to the stabilization of the cell and solid-electrolyte interface. The characteristic sloping discharge curve starting above 4 V can be attributed to the  $\text{Li}[\text{Li}_{0.17}\text{Mn}_{0.58}\text{Ni}_{0.25}]\text{O}_2$  part, and the relatively level portion of the curve occurring at less than 3.4 V can be attributed to the carbon-coated  $\text{LiFePO}_4$ . Clearly, the performance of the three electrodes is different. The low-rate capability of  $\text{Li}[\text{Li}_{0.17}\text{Mn}_{0.58}\text{Ni}_{0.25}]\text{O}_2$  lowered overall electrode specific energy when the materials were mixed intimately or layered on top of each other in a single electrode. The best geometry for this blend is thus the segregated case, because it is the only configuration where the current can be driven through the LFP part at a high discharge rate. Otherwise, the active particles of both components must be held at the same potential. On the other hand, if  $\text{Li}[\text{Li}_{0.17}\text{Mn}_{0.58}\text{Ni}_{0.25}]\text{O}_2$  is replaced by  $\text{LiCoO}_2$ , a material with a higher rate capability than  $\text{Li}[\text{Li}_{0.17}\text{Mn}_{0.58}\text{Ni}_{0.25}]\text{O}_2$ , the layered cell's performance will greatly improve. Therefore, more systematic studies of blends as a function of the different geometries should be investigated in the near future.



**Figure 13.** Discharge curves of  $\text{Li}[\text{Li}_{0.17}\text{Mn}_{0.58}\text{Ni}_{0.25}]\text{O}_2$ –LFP blended cathodes in different geometries [13]. (a) physically mixed cathode; (b) multilayer cathode and (c) segregated cathode.

Another field of investigation that should be developed is the optimization of the mixed powders. In practice, it is very difficult to mix powders. The phenomenon of de-mixing has been well-known

for a long time [24]. In practice, the sizes of the particles of the components of the blend are different, in which case “size-segregation” may occur. This phenomenon is made possible by the gaps that open up around particles when they are shaken, allowing percolation to occur. Large particles tend to move toward less dense regions of smaller particles, so that large objects can rise to the top of vertically shaken layers, a well-known effect in granular materials. In addition, the particles can also spontaneously form patterns in the process [25]. The properties of mixed powders then depend on different parameters: the shape and size of the particles of the two blend elements, the packing structure of the powder mixtures in the scale of particle contacts (coordination number of each powder, defined as the number of particles surrounding and having contact with a reference particle), and the distribution of the contact chains, which, in the present case, also determines the electrical resistance of the blend. So far, the development of powder dynamics has been investigated in the framework of vibrations and flow. In the context of blends for electrodes, the dynamics is associated with the volume change of the particles induced by the lithium insertion of or de-insertion upon cycling, which is a new area of research to be developed in the near future.

## 5. Materials and Methods

### 5.1. Synthesis and Characterizations

The synthesis procedure of the LMP–LFP composite consists of three steps: (i)  $\text{LiMnPO}_4$  olivine was synthesized by the hydrothermal method assisted with ascorbic acid ( $1.3 \text{ g} \cdot \text{L}^{-1}$ ) and 3% Denka black using  $\text{LiOH} \cdot \text{H}_2\text{O}$ ,  $\text{MnSO}_4 \cdot \text{H}_2\text{O}$ , and  $\text{H}_3\text{PO}_4$  (Li:Mn:P molar ratio 3:1:1) as raw materials; (ii) As-prepared LMP powders were added to the LFP precursor solution made by the dissolution of  $\text{LiOH} \cdot \text{H}_2\text{O}$ ,  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ , and  $(\text{NH}_4)_2\text{HPO}_4$  in distilled water. The reactive medium thus obtained is poured into a polytetrafluoroethylene (PTFE) vessel, put into a stainless steel chamber (Parr, Volume = 325 mL), and heated at  $220 \text{ }^\circ\text{C}$  for 7 h. After cooling at room temperature, the powder is obtained by filtration, washed three times in distilled water, and dried at  $90 \text{ }^\circ\text{C}$  during 12 h in  $\text{N}_2$  atmosphere. At the end, 15.1 g of LMP–LFP blended material was obtained; (iii) The carbon-coating of the composite was obtained by mixing the product of step (ii) with a solution of lactose, the ratio lactose/composite being 1/10. This product was heated at  $400 \text{ }^\circ\text{C}$  for one hour, then heated at  $600 \text{ }^\circ\text{C}$  for 3 h [26].

$\text{LiNi}_{0.33}\text{Mn}_{0.33}\text{Co}_{0.33}\text{O}_2$ -layered powders were prepared using the co-precipitation method described elsewhere [27] by a hydroxide route, for which transition-metal hydroxide and lithium carbonate were starting materials. Using a lithium excess  $\eta = \text{Li}/M$  ratio of 1.05 the sample shows low cationic mixing  $\text{Ni}^{2+}(3b) < 2\%$ . The composite was obtained by physical mixing of NMC with carbon-coated LFP using a ball milling technique with different weights (70:30) and (20:80) ratios (NMC:LFP).

The characterization of the samples was done using a Hitachi HD-2700C dedicated STEM with a CEOS aberration corrector and a cold field-emission gun equipped with a newly designed silicon-drift detector (SDD) from Bruker (East Milton, ON, Canada), which offers over 10 times the solid angle of conventional energy-dispersive X-ray Si(Li) detectors. This dedicated STEM has demonstrated an image resolution of 78 pm in high angle annular dark field (HAADF).

### 5.2. Electrochemical Tests

Electrochemical tests were performed with composite electrode materials prepared by mixing 80% (*w/w*) of the active material, 10% (*w/w*) super C65 carbon (TIMCAL, Willebroek, Belgium), and 10% (*w/w*) polyvinylidene fluoride (Solef PVdF 6020 binder, Solvay, Brussels, Belgium) in *N*-methyl-2-pyrrolidone (NMP, Sigma-Aldrich, St. Louis, MO, USA) to produce a slurry. A 90- $\mu\text{m}$ -thick film was obtained by coating this slurry on aluminum foil that gives an electrode loading  $\sim 8 \text{ mg} \cdot \text{cm}^{-2}$ . This film was dried overnight at  $80 \text{ }^\circ\text{C}$ , and then punched out with a diameter of 1.4 cm. The cell was assembled as coin-type cells in an argon-filled glove box using lithium foil (Alfa Aesar, Ward Hill,

MA, USA) as an anode, LP30 (1 mol·L<sup>-1</sup> LiPF<sub>6</sub> in (1:1) ethylene carbonate (EC)—dimethyl carbonate (DMC) as an electrolyte, and glass microfiber filters (Whatmann®-GF/D 70 mm Ø, Sigma-Aldrich) as a separator. VMP3 multi-channel potentiostat (Bio-Logic, Claix, France) was used to electrochemically characterize the electrodes at 25 °C in the voltage range of 1.5–4.8 V vs. Li<sup>0</sup>/Li<sup>+</sup> in galvanostatic tests.

## 6. Conclusions

In this paper, we studied two blended cathode materials based on a mixture of nano-structured particles of LiFePO<sub>4</sub> olivine with another micro-structured insertion compounds such as LiMnPO<sub>4</sub> olivine and LiNi<sub>1/3</sub>Mn<sub>1/3</sub>Co<sub>1/3</sub>O<sub>2</sub>-layered compound. To overcome the difficulty of carbon coating on LiMnPO<sub>4</sub> olivine particles, the preparation of the LMP–LFP (66:33) composite was realized. Using such a blended electrode, the electrochemical properties are improved with respect to the carbon-coated LiMn<sub>2/3</sub>Fe<sub>1/3</sub>PO<sub>4</sub> solid solution with a comparable Fe/Mn ratio. The blended cathode formed by the NMC–LFP mixture exhibits excellent rate capability by using nano-sized LFP particles and delivers a higher capacity, *i.e.*, 180 mAh·g<sup>-1</sup>, due to the NMC component. Consequently, Li-ion batteries including NMC–LFP physical blending provide a good solution that achieves both energy and power capability and exhibits improved electrochemical features with thermal stability similar to LFP.

*In situ* voltage measurement methods were applied for the evaluation of the phase evolution of blended cathodes and gradual changes in cell behavior upon cycling using the so-called incremental capacity (IC) with respect to cell potential,  $dQ/dV = f(V)$ . Another typical test to characterize the power capability of a cell at different states of charge (SOCs) is the plot of the area specific resistance (ASR) vs. the cell potential. Both methods have demonstrated that blending cathode materials with LiFePO<sub>4</sub> nano-particles improves their electrochemical performance. We hope that the electrochemistry will lean on the progress that has been made in mathematics to model non-linear dynamics of powder mixing and will benefit from the powder technology sustained by their application in different fields of the industry in the near future, aiming to optimize the blends to be used as new electrodes of Li-ion batteries.

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