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Optimal Control of Hybrid Photovoltaic/Thermal Water System in Solar Panels Using the Linear Parameter Varying Approach

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Abstract: During photovoltaic (PV) conversion in solar panels, a part of the solar radiation is not converted to electricity by the cells, producing heat that could increase their temperature. This increase in temperature deteriorates the performance of the PV panel. In this paper, a hybrid PV/thermal (PV/T) water system is proposed to mitigate this problem. This system combines a PV panel and a thermal collector. In this paper, we focused on the modeling and control of this hybrid system in the linear parameter varying (LPV) framework. An optimal linear quadratic regulator (LQR) is proposed to control the PV cell temperature around an optimal value that maximises electricity generation. Since the system model is nonlinear, an optimal LQR gain-scheduling state-feedback control approach based on an LPV representation of the nonlinear model is designed using the Linear Matrix Inequality (LMI) method. The goal is to obtain the maximum electrical power for each solar panel. Since a reduced number of sensors is available, an LPV Kalman filter is also proposed to estimate the system states required by the state-feedback controller. The obtained results in a laboratory setup in simulation are used to assess the proposed approach, showing promise in terms of control performance of the PV/T system.

Keywords: hybrid PV/thermal (PV/T) water system; PV cell temperature; linear parameter varying (LPV); linear quadratic regulator (LQR); Linear Matrix Inequality (LMI); Kalman filter



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1. Introduction

Presently, electrical energy is necessary for almost all human activities around the world. Due to large population growth, the demand for electricity has increased tremendously in recent decades. In many countries, electricity generation still depends mainly on fossil fuel technology that requires huge financial resources in addition to contributing to climate change. With the aim of reducing the use of fossil fuel technology and avoiding environmental damage [1–3], the world is moving towards the production of electricity by using renewable energies because of their advantages, such as pollution and greenhouse gas emissions reduction and their wide availability around the world [4,5]. For this reason, renewable energies are increasingly attracting the interest of many energy utilities. This is the reason why renewable energies are becoming crucial and will play an important role in the economic development of all countries in the near future [6–8].

In order to limit global warming and reduce environmental contamination, several countries agreed to limit emissions according to the Paris convention signed at a conference on climate change held in the United States in 2015 [9,10]. Moreover, many countries are moving towards increasing the consumption of renewable energy as a solution to reduce CO₂ emissions and the production costs of using expensive fossil fuels.

Researchers and country leaders are currently focusing on harnessing green energies such as wind energy, ocean energy and solar energy [11].

Solar energy is one of the most developed clean and renewable energies today; its advantages are pollution reduction and protection of the environment. The use of this type of energy is also less costly compared to other types of energy.

Like other types of energy generation technologies, photovoltaic (PV) solar energy also has some disadvantages because solar systems are generally installed outside and will be directly exposed to climatic factors such as high temperature, wind and shading. All these factors cause a decrease in their efficiency. For this reason, several works are dedicated to studying and developing PV technology to obtain better performance. After several tests on PV systems, researchers and photovoltaic industries found that an increase in temperature could lead to a performance reduction in PV cells [12]. To mitigate this problem, many efforts have been made in order to increase their efficiency and subsequently reduce the cost of their maintenance.

Given the importance of this energy generation technology and its simplicity of use, many researchers in the PV domain are interested in improving the performance of solar panels in order to extract the maximum electrical power, e.g., by modifying the structure and design of solar panels [13]. The application of feedback control as suggested in [14] allows the design of a controller based on the prediction of DC voltage that allows the three-phase inverter to follow the maximum power despite the disturbances of climatic conditions and the variable loads. There are also other works aiming at regulating the PV cells' temperature in order to improve the performance of the panels, such as, e.g., [15], where the researchers use a phase change material for cooling the PV panels under Malaysian weather conditions. The result shows that the surface temperature of the module is reduced by 10 °C, which remains constant for a period of 4 to 6 h. In [16], two different methods were used to regulate the PV cell temperature without the interference of any other external mechanism. The first one is based on using argon gas within the concentrator element, and the second one is based on the incorporation of polymer-dispersed liquid crystal films (PDLC) on top of the module. In both cases, the power was improved by 37 mW–47 mW while temperature was reduced by 10 °C and 4 °C for the argon gas-filled module and PDLC integrated module, respectively. In [17], the cooling system uses a simple pipe which is placed on the PV module as a spiral heat exchanger in order to provide active cooling without any controller. The results show a slight decrease in the temperature of the PV module. Also, in [18], the authors of experimental and theoretical studies on the cooling of photovoltaic panels propose a solution based on the principle of evaporative cooling. The results show that the temperature of the photovoltaic panel can be reduced by 10 °C and that the improvement in power obtained is 5%. A PID controller allows the adjustment of a cooling mechanism such as a fan or heat sink to regulate the temperature of the solar panel. There are other works dedicated to the development of solar cell technologies and the mounting structures of PV modules, such as, e.g., [19–22], aiming at extracting more energy.

Due to their importance and advantages, hybrid PV/T systems have gained great attention from manufacturers in recent years. A PV/T system can produce two types of energy, electrical energy (electrical power P_e) and thermal energy (thermal power Q_t). Given the reality of global warming, it is likely that cooling and heating needs in buildings will increase. In this regard, the use of a hybrid PV/T system appears to be a very suitable solution as these systems can supply both heating and cooling depending on the specific needs of the user [22–25]. While this type of hybrid system has advantages, they can also have disadvantages related to the production and installation costs of PV-T collectors, which are still high. Moreover, certain technological improvements are necessary, including research and development of new materials, system stability improvements and the design of a supporting energy storage system [26]. There are two types of PV/T hybrid systems. The first one is a hybrid PV/T air system which is able to produce electricity and heat, where the cooling technique of the PV module is made by the circulation of air in the collector. The second one is a hybrid PV/T water system able to produce electricity and hot water, which is the subject of this paper. These systems can be covered or uncovered using different

types of PV cells (e.g., monocrystalline silicon cells, polycrystalline silicon cells, amorphous silicon cells or thin-film cells, among others).

Usually, a classic PV model absorbs between 80 and 90% of solar radiation but only 10 to 20% has been converted into electricity and the rest is transformed into heat which can be a damaging factor for PV cells [27]. The PV/T system can remedy this problem and improve the efficiency of the PV cell by producing at the same time heat or hot water for users [28].

In recent years, several researchers have been interested in the control of PV/T hybrid water systems in order to improve performance [29–31]. A model predictive control is used to optimally control the operation of an HVAC system based on a hybrid PV/T system [32]. A controller based on an Artificial Neural Network (ANN) is proposed to improve performance and track optimum electrical and thermal power in [33], and in [34], where a PV/T ANN-based control algorithm was applied to detect the optimum electrical and thermal power operating point (OPOP). OPOP makes it possible to find the optimal water flow rate of a PV/T system for a given ambient temperature and solar irradiation, facilitating the extraction of maximum energy. The results showed that the application of an ANN, with one hidden layer for the thermal and electrical modeling of the PVT collector, makes it possible to improve performance using training data obtained from real experiments.

This paper investigates how to increase the performance of a hybrid PV/T water system by controlling the temperature of PV cells. The research work presented has a twofold objective: on the one hand, to implement and design an optimal LQR controller to decrease the PV cell temperature caused by the increase in ambient temperature and irradiation around an optimal value equal to 25 °C in order to extract the maximum energy, and on the other hand, to prove the effectiveness of this controller against external disturbances. Since the system model is nonlinear, an optimal LQR gain-scheduling state-feedback control approach based on an LPV representation of the nonlinear model is designed using the Linear Matrix Inequality (LMI) method. The goal is to obtain the maximum electrical power for each solar panel. Since a reduced number of temperature sensors are available, an LPV Kalman filter is also proposed to estimate the system states required for the state-feedback controller. The obtained results in simulation using a pilot-prototype installation have allowed the assessment of the proposed control method showing an improvement in electricity generation. Furthermore, the proposed approach allows us to obtain an optimal performance compared to other types of control presented in the literature [35–37].

The structure of the remainder of the paper is as follows: Section 2 describes the PV/T hybrid system used as case study. Section 3 deals with the modeling of a PV/T hybrid system using physical principles. Section 4 develops a control-oriented model in the LPV framework using the nonlinear embedding approach. Section 5 presents an optimal LQR gain-scheduling state-feedback control approach based on a polytopic representation of the LPV model. In Section 6, a state estimator based on an LPV Kalman filter is designed to estimate all the unknown system states. Finally, the main conclusions and remarks are drawn in Section 7.

2. Case Study Description

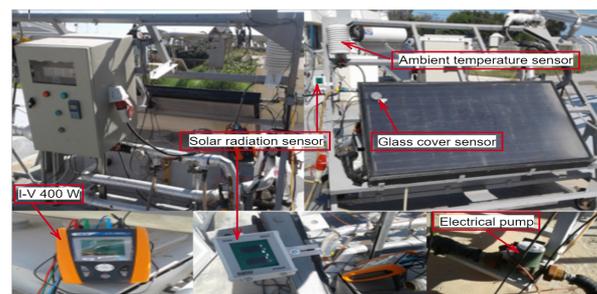
Figure 1a,b show the hybrid PV/T water system (VOLTHER PowerTherm) and its schematic diagram installed at the Research and Technology Center of Energy (CRTEn) located in the northern part of Tunisia, which was used in this paper as a case study. The considered PV/T hybrid system refrigerated with water combines two different subsystems: a photovoltaic panel (PV) and a thermal collector (T) to form the PV/T system. This system can be installed in a photovoltaic field connected to the utility grid via a smart power inverter without any effect on its operation [38]. As discussed in the introduction, the purpose of this hybrid system is to reduce the PV cell temperature (T_c) and subsequently increase the produced electrical power.

The configuration of the system is composed of a hybrid PV/T system, a water tank, a pump that allows the circulation and variation of the water flow rate in the absorber installed under the PV cells and an I-V 400 W device to measure the current, the temperature

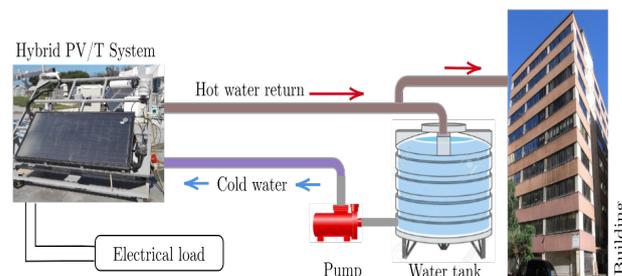
and the evolution of the electrical and thermal power in real conditions of solar radiation and ambient temperature [39].

During the operation of this system, when the ambient temperature and the solar radiation increases, the temperature of the PV cell (T_c) gradually increases and directly affects the PV performance. To solve this problem, the PV cell temperature must be decreased. As discussed in the introduction, results presented in the literature have shown that water cooling, although it could be expensive, is the most effective cooling technique. The circulation of water in the absorber is carried out by the circulation pump which allows reduction of the temperature of the PV cell. The cooling method for PV cells through the circulation of water in the absorber has limitations, as it only marginally reduces the temperature of the PV cell. This was substantiated through an experimental test conducted on the actual prototype located in the CRTEn laboratory mentioned in [40]. Despite employing water as a cooling fluid, the temperature of the PV cells persistently remains elevated. Consequently, the implementation of an optimal controller emerges as a suitable solution.

At the output of the absorber, water is recovered at a high temperature and the power delivered by the PV panel will be stored in the batteries if this system is installed in isolated sites, or injected directly into the utility grid [41]. In order to increase electricity production, PV cell temperature must be controlled, taking into account the increase or decrease in the ambient temperature.



(a)



(b)

Figure 1. (a) Hybrid PV/T system type VOLTHER PowerTherm in the CRTEn laboratory. (b) Hybrid PV/T system schematic diagram.

The evolution of the solar radiation G and the ambient temperature T_a during a day in the CRTEn laboratory, where the system is installed, is presented in Figures 2 and 3, corresponding to data collected in a real scenario.

The radiation G and the ambient temperature T_a are considered disturbances. These disturbances will directly affect the performance of the photovoltaic cells, i.e., the extracted electrical power.

Figure 4 presents a conceptual representation of the hybrid PV/T water system. The considered hybrid PV/T water system (type VOLTHER PowerTherm) consists of 72 monocrystalline cells that are covered by a glass layer. Each cell is composed of three

layers: a PV cell, an absorber layer in which the coolant circulates (in this paper, cold water) and a Tedlar layer for protection against humidity.

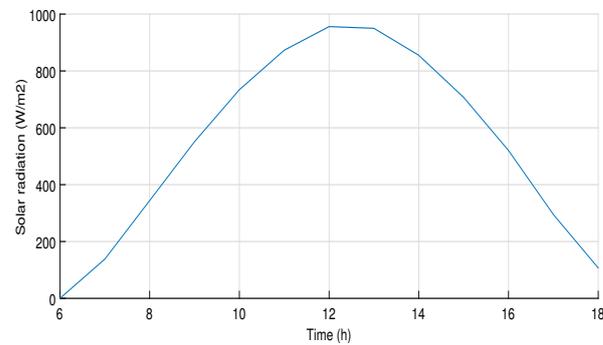


Figure 2. Real solar radiation data in CRTEn laboratory.

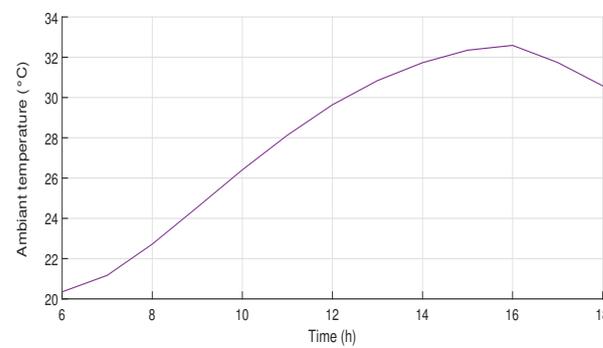


Figure 3. Real ambient temperature data in CRTEn laboratory.

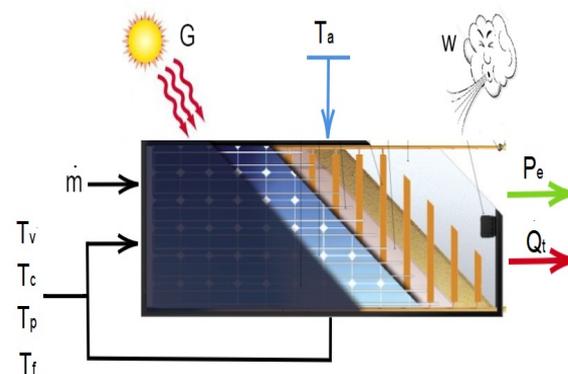


Figure 4. Conceptual representation of the covered hybrid PV/T water system.

3. PV/T Water System Control-Oriented Model

As we mentioned above, the case study system is composed of two different main systems: a covered electrical system including the photovoltaic (PV) panel and a thermal system including the thermal collector (T). Following [34], the control-oriented mathematical modeling will be described in the following.

3.1. Electrical System Modeling

Figure 5 shows the model of the monocrystalline PV cell.

By exposing the PV panels to the solar radiation, the PV cell will generate electrical power that is stored in a battery or injected directly into the electrical grid.

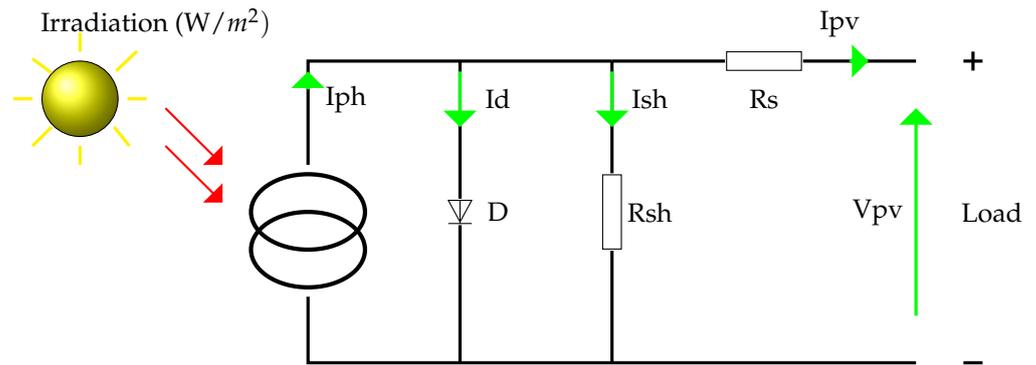


Figure 5. Electrical model of a PV cell.

The PV cell output current I_{pv} is given by

$$I_{pv} = I_{ph} - I_d - I_{sh} \quad (1)$$

where I_d is the current in the diode

$$I_d = I_{rs} e^{q \left(\frac{V_{pv} + R_s I_{pv}}{akTN_s} \right)} - 1 \quad (2)$$

and the current I_{sh} is given by

$$I_{sh} = \frac{q(V_{pv} + R_s I_{pv})}{R_{sh} R_s} \quad (3)$$

In the previous equations, I_{pv} , I_{ph} and I_{rs} are, respectively, the load current, the photoelectric current and the saturation current of the diode. V_{pv} is the load voltage. N_s and N_p are the number of cells in series and in parallel, respectively. R_s , R_{sh} are the series and shunt resistance, respectively. k is the Boltzmann constant equal to $1.38 \times 10^{-23} \text{ J/}^\circ\text{K}$, q is the electron charge equal to $1.6 \cdot 10^{-19} \text{ }^\circ\text{C}$ and a is the ideality factor of the diode. I_{ph} is the photoelectric current given by

$$I_{ph} = \frac{I_{ph}}{e^{q \left(\frac{V_{oc}}{akTN_s} \right)} - 1} \quad (4)$$

The electrical power P_{pv} of a PV cell is given by

$$P_{pv} = V_{pv} I_{pv} \quad (5)$$

where V_{pv} represents the PV voltage.

The electrical efficiency η_{elec} of the PV cell is

$$\eta_{elec} = \frac{P_{pv}}{S_{pv} G} \quad (6)$$

where P_{pv} is total electrical power, G is the solar radiation (w/m^2) and S_{pv} is the PV model surface (m^2).

This electrical efficiency can also be assessed as follows [42,43]

$$\eta_{elec} = \eta_{T_{ref}} [1 - \beta(T_{pv} - T_{ref})] \quad (7)$$

where β is the temperature coefficient of the PV module, defined by the designer and equal to $\simeq 0.0045 \text{ }^\circ\text{K}^{-1}$, T_{ref} is the reference temperature equal to $25 \text{ }^\circ\text{C}$ and $\eta_{T_{ref}}$ is the efficiency at the reference temperature.

3.2. Thermal System Modeling

The thermal modeling of the studied PV/T system is essentially based on the principle of energy conversion [13]. In order to determine the evolution of temperatures and thermal performance of each layer, the principle of energy conversion is established as

$$M_i C_i \frac{dT_i(t)}{dt} = \sum Q_i^e(t) - \sum Q_i^s(t) \quad (8)$$

where M_i is the component mass, C_i is the specific heat capacity of the component, T_i is the component temperature, and $\sum Q_i^e$ and $\sum Q_i^s$ are, respectively, the sum of the energies received/lost by i -th layer through the heat exchanges due to conduction, convection and radiation.

The thermal modeling of the real PV/T hybrid case study system presented in Figure 4 allows us to determine the energy balance of each layer (glass cover, PV cell, absorber and fluid circulation). The mathematical model describing the evolution of the temperature of each layer in function of the water flow (\dot{m}), the solar radiation (G) and the ambient temperature (T_a) is the following [34]

- Glass layer temperature (T_v):

$$C_v M_v \frac{dT_v(t)}{dt} = \alpha_v G(t) A_v + A_v (h_{win} + h_{rva})(T_a(t) - T_v(t)) + A_v h_{rcv}(T_c(t) - T_v(t)) + A_v h_{cv}(T_c(t) - T_v(t)) \quad (9)$$

- Cell layer temperature (T_c):

$$C_c M_c \frac{dT_c(t)}{dt} = (\alpha_c G A_c \tau_v (1 - \nu_r)) - A_v h_{rcv}(T_v(t) - T_c(t)) - A_v h_{cv}(T_c(t) - T_v(t)) - A_c h_{cp}(T_c(t) - T_p(t)) \quad (10)$$

- Absorber layer temperature (T_p):

$$C_p M_p \frac{dT_p(t)}{dt} = (A_c h_{cp}(T_c(t) - T_p(t)) - A_c h_{pa}(T_p(t) - T_a(t)) - A_f h_{fa}(T_f(t) - T_a(t)) - \dot{m} C_f \Delta T_f(t)) \quad (11)$$

- Fluid layer temperature (T_f):

$$C_f M_f \frac{dT_f(t)}{dt} = A_f h_{pf}(T_p(t) - T_f(t)) \quad (12)$$

In the previous equations, there are several heat transfer coefficients defined as follows:

- h_{rcv} is the radiation heat transfer coefficient between the glass cover and the absorber

$$h_{rcv} = \frac{\sigma(T_v^2 + T_a^2)(T_v + T_a)}{(\frac{1}{\epsilon_v} + \frac{1}{\epsilon_c}) - 1} \quad (13)$$

- h_{cv} is the convective heat transfer coefficient between the glass cover and the PV cell

$$h_{cv} = \left[\frac{\delta_v}{k_v} + \frac{\delta_c}{k_c} \right]^{-1} \quad (14)$$

- h_{win} is the convective heat transfer coefficient according to [44,45]:

$$h_{win} = 2.8 + 3w_s \quad (15)$$

- h_{rva} is the radiation heat transfer coefficient between the glass cover and the environment

$$h_{rva} = \epsilon_v \sigma (T_v^2 + T_a^2) (T_v + T_a) \quad (16)$$

The real parameters used in the simulation of the considered hybrid PV/T water system (type VOLTHER PowerTherm) available in the CRTEn laboratory are listed in Table 1.

The previous thermal mathematical model of the system can be represented in nonlinear state-space form as follows:

$$\begin{aligned} \dot{x}(t) &= f(x(t), u(t), d(t)) \\ y(t) &= h(x(t), u(t)) \end{aligned} \quad (17)$$

where $x = [T_v, T_c, T_p, T_f]^T$ is the state vector that represents, respectively, the temperature of each layer, $u = \dot{m}$ is the control input that corresponds to the water flow rate, $d = [G, T_a]^T$ is the disturbance vector that contains the solar radiation (G) and the ambient temperature (T_a), and $y = [P_e, Q_t]^T$ is the output vector that contains the measurements provided by the available sensors that provide the electrical power (P_e) and the thermal power (Q_t). f and g are vectorial functions that are obtained from the physical model.

Table 1. Real parameters of PV/T system (VOLTHER PowerTherm).

Parameters	Value
Glass cover layer	
Area of Glass (A_v)	1.64 m ²
Mass of Glass (m_v)	7.2 kg
Specific heat capacity (c_v)	790 J/kg/K
Emissivity (ϵ_v)	0.88
Transmissivity (τ_v)	0.95
Thickness (δ_v)	0.004 m
Absorber layer	
Area of Absorber (A_p)	2 m ²
Mass of Absorber (m_p)	9.03 kg
Specific heat capacity (c_p)	900 J/kg/K
PV cell layer	
Area of PV module (A_c)	0.87 m ²
Mass of PV module (m_c)	5.4 kg
Specific heat capacity (c_c)	860 J/kg/K
Emissivity (ϵ_c)	0.93
Thickness (δ_c)	0.0003 m
Water layer	
Area of fluid channel (A_f)	0.165 m ²
Specific heat capacity (c_f)	4180 J/kg/K
h_{pf}	100
h_{cp}	5.7
h_{fa}	300

4. LPV Modeling of the PV/T System

4.1. LPV Model

The thermal model (17) is nonlinear. Using the LPV approach, the nonlinearities are embedded in some varying parameters θ_{ij} in the function of the temperatures of each layer. The LPV model is obtained using the nonlinear embedding method proposed in [46] leading to a linear time-varying system, whose state-space representation depends on some varying parameters θ

$$\begin{aligned} \dot{x}(t) &= A(\theta)x(t) + Bu(t) + B_d d(t) \\ y(t) &= Cx(t) \end{aligned} \quad (18)$$

where the state vector $x \in \mathbb{R}^{n_x}$, control input $u \in \mathbb{R}^{n_u}$, output vector $y \in \mathbb{R}^{n_y}$ and disturbance vector $d \in \mathbb{R}^{n_d}$ are defined in the same manner as in the nonlinear model (17).

$A \in \mathbb{R}^{n_x \times n_x}$, $B \in \mathbb{R}^{n_x \times n_u}$, $B_d \in \mathbb{R}^{n_x \times n_d}$ and $C \in \mathbb{R}^{n_y \times n_x}$ are the system matrices. Note that $A(\theta)$ is a matrix that contains some varying parameters θ_{ij} that depend on the state vector x (temperatures of the layers) and embed all the nonlinearities of the nonlinear model (17). In particular, the obtained state matrix $A(\theta)$ contains four varying parameters θ_{ij}

$$A(\theta) = \begin{bmatrix} \theta_{11} & \theta_{12} & a_{13} & a_{14} \\ \theta_{21} & \theta_{22} & a_{23} & a_{24} \\ a_{31} & a_{32} & a_{33} & a_{34} \\ a_{41} & a_{42} & a_{43} & a_{44} \end{bmatrix} \quad (19)$$

with the following expressions

$$\theta_{11} = \frac{-A_v(h_{win} + h_{rva} + h_{rcv} + h_{cv})}{(c_v m_v)} \quad (20)$$

$$\theta_{12} = \frac{A_v(h_{rcv} + h_{cv})}{(c_v m_v)} \quad (21)$$

$$\theta_{21} = \frac{-A_v(h_{rcv} + h_{cv})}{(c_c m_c)} \quad (22)$$

$$\theta_{22} = \frac{-A_c h_{cp} - A_v h_{cv} + A_v h_{rcv}}{(c_c m_c)} \quad (23)$$

The rest of the parameters a_{ij} are constant.

4.2. Polytopic LPV Model

To design the optimal LQR gain-scheduling controller and associated state estimator, we will transform the LPV model above in a polytopic representation using the bounding box approach [47]. Analysing the expressions of the varying parameters (20)–(23), they depend on the glass cover temperature T_v and the ambient temperature T_a according to (13) and (16). Using the minimum and maximum values of these two temperatures in the considered operating range, we can derive the vertex matrices A_i of the polytopic representation of the matrix $A(\theta)$

$$\dot{x}(t) = \sum_{i=0}^N v_i(\theta)(A_i x(t) + B_i u(t)) \quad (24)$$

with $\sum_{i=0}^N v_i(\theta) = 1$, and $0 \leq v_i(\theta) \leq 1$, for $i = 1, \dots, N$ with $N = 2^{n_\theta}$ being n_θ the number of varying parameters.

As we have four varying parameters θ_{ij} , we will have $N = 16$ different matrices considering all the possible minimum/maximum values.

$$A_1 = \begin{bmatrix} \theta_{11} & \theta_{12} & a_{13} & a_{14} \\ \theta_{21} & \theta_{22} & a_{23} & a_{24} \\ a_{31} & a_{32} & a_{33} & a_{34} \\ a_{41} & a_{42} & a_{43} & a_{44} \end{bmatrix}, \dots, A_{16} = \begin{bmatrix} \overline{\theta_{11}} & \overline{\theta_{12}} & a_{13} & a_{14} \\ \overline{\theta_{21}} & \overline{\theta_{22}} & a_{23} & a_{24} \\ a_{31} & a_{32} & a_{33} & a_{34} \\ a_{41} & a_{42} & a_{43} & a_{44} \end{bmatrix}$$

To find the interpolation function $v_i(\theta)$ in the polytopic representation (24), we will derive the expression of the interpolation function of each varying parameter θ_{ij} such that these two conditions are satisfied

$$\theta_{ij} = \mu_{ij}^{\min}(\theta_{ij})\underline{\theta}_{ij} + \mu_{ij}^{\max}(\theta_{ij})\overline{\theta}_{ij} \quad (25)$$

$$\mu_{ij}^{min}(\theta_{ij}) + \mu_{ij}^{max}(\theta_{ij}) = 1 \tag{26}$$

From these two conditions, it follows that

$$\mu_{ij}^{min}(\theta_{ij}) = \frac{\bar{\theta}_{ij} - \theta_{ij}}{\theta_{ij} - \underline{\theta}_{ij}} \tag{27}$$

$$\mu_{ij}^{max}(\theta_{ij}) = 1 - \mu_{ij}^{min}(\theta_{ij}) = \frac{\theta_{ij} - \underline{\theta}_{ij}}{\bar{\theta}_{ij} - \underline{\theta}_{ij}} \tag{28}$$

Finally, the expressions of the interpolation functions $\nu_i(\theta)$ in the polytopic representation (24) are as follows:

$$\begin{aligned} \nu_1(\theta) &= \mu_{11}^{min}(\theta_{11})\mu_{12}^{min}(\theta_{12})\mu_{21}^{min}(\theta_{21})\mu_{22}^{min}(\theta_{22}) \\ &\dots \\ \nu_{16}(\theta) &= \mu_{11}^{max}(\theta_{11})\mu_{12}^{max}(\theta_{12})\mu_{21}^{max}(\theta_{21})\mu_{22}^{max}(\theta_{22}) \end{aligned}$$

Figures 6–9 present the evolution of the values of the interpolation functions $\nu_i(\theta)$ in the polytopic representation (24) around a particular operating point.

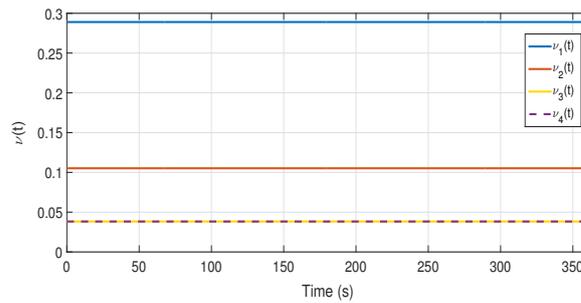


Figure 6. Interpolation functions $\nu_1, \nu_2, \nu_3, \nu_4$ of the polytopic LPV model.

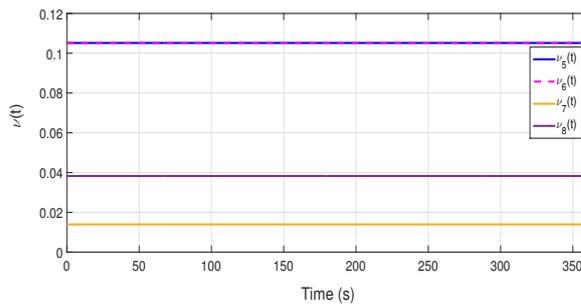


Figure 7. Interpolation functions $\nu_5, \nu_6, \nu_7, \nu_8$ of the polytopic LPV model.

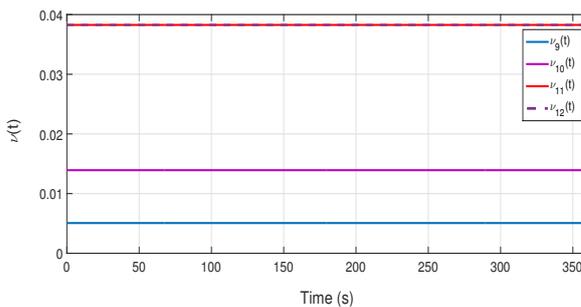


Figure 8. Interpolation functions $\nu_9, \nu_{10}, \nu_{11}, \nu_{12}$ of the polytopic LPV model.

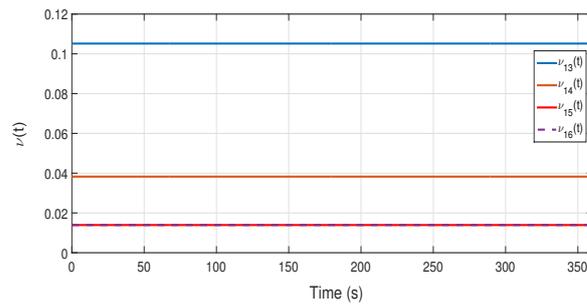


Figure 9. Interpolation functions ν_{13} , ν_{14} , ν_{15} , ν_{16} of the polytopic LPV model.

5. Control Design of the PV/T System

5.1. Problem Statement

Figure 10 shows a real evolution of cell temperature in the real setup at the CRTEN laboratory (Tunisia). This figure shows how the cell temperature varies with the hour of the day in the function of ambient temperature (T_a) and solar radiation (G) presented in Figures 2 and 3. This behaviour has also been reproduced with the thermal model (17) using the same data for T_a and G .

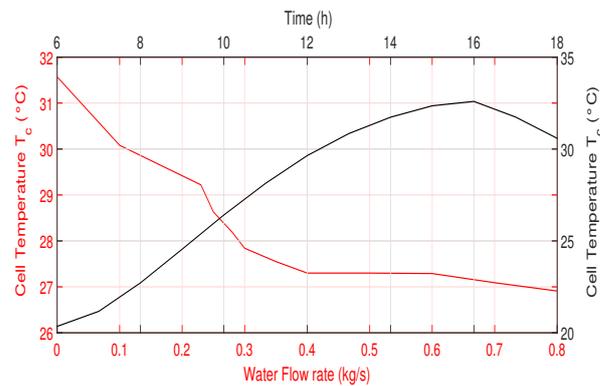


Figure 10. Real variation of cell temperature by varying time and water flow rate.

On the other hand, Figure 11 shows the variation of the electric power during the day based on the real values of the solar radiation (see Figure 2). This variation depends also on the cell temperature. When this temperature increases, the electric power will decrease. Therefore, the control of this temperature to its optimal value is a key issue in order to extract the maximum electric power P_e and to guarantee the optimal operation of PV cells. The cell temperature can be reduced by manipulating the water flow rate \dot{m} that circulates in the absorber as can be observed in Figure 6.

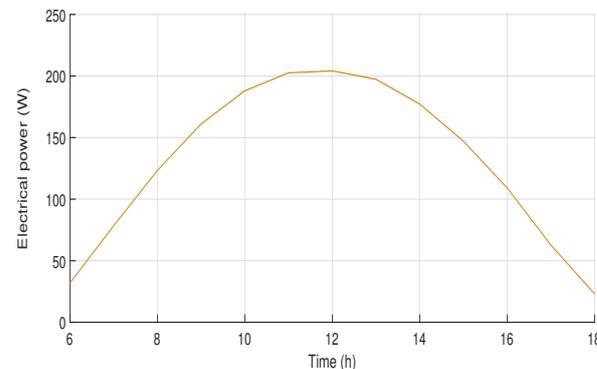


Figure 11. Variation of the electrical power.

In this section, we will propose a solution to the problem related to decreasing PV cell efficiency because of increasing cell temperature. As already discussed, as solar radiation and ambient temperature increase, the temperature of PV cells gradually increases, decreasing the efficiency of the PV cell and consequently decreasing the electrical power P_e .

The proposed solution is based on designing an optimal LQR LPV state feedback controller that maintains the cells' temperature T_c around 25 °C by manipulating the flow rate of water \dot{m} that circulates in the absorber. This temperature allows the establishment of the standard operating conditions suggested by the manufacturer to obtain the optimal efficiency of the PV cell.

The proposed LPV controller strategy is developed using the polytopic LPV thermal model (24) which takes into account the parameter variation (20)–(23) in the function of the ambient temperature T_a and the glass cover temperature T_v .

This controller is similar to a standard state feedback controller but the feedback gain $K(\theta)$ varies with the varying parameters (20)–(23) in order to guarantee maximum electrical power P for each solar radiation G and ambient temperature T_a . The LPV state feedback controller provides the following control action which corresponds to the manipulated water flow rate \dot{m} in the absorber

$$u(t) = -K(\theta)x(t) \quad (29)$$

where

$$K(\theta) = \sum_{i=1}^N v_i(\theta)K_i \quad (30)$$

such that the closed-loop system is given by

$$\dot{x}(t) = \sum_{i=1}^N v_i(\theta)(A_i - BK_i)x(t) \quad (31)$$

The design of the controller gains K_i associated with the vertices of the polytopic model (24) is based on formulating the LQR optimal control problem in LMI form as presented in the next section.

5.2. LMI Method

The optimal K_i will be obtained by rewriting the Ricatti equation associated with the LQR problem

$$(A_i - BK_i)^T P + P(A_i - BK_i) + Q + K_i^T R K_i < 0 \quad (32)$$

in LMI form.

To do so, we will right multiply (32) by $Y = P^{-1}$ and introduce the following change of variables:

$$W_i = K_i Y \quad (33)$$

$$Q = H^T H \quad (34)$$

Then, we will apply the Schur lemma and will find the following LMI for the Ricatti Equation (32).

$$\begin{bmatrix} YA_i^T + AY - BW_i - W_i^T B^T & YH^T & W_i^T \\ & -I_n & 0 \\ & & 0 & -R^{-1} \end{bmatrix} < 0 \quad (35)$$

To obtain the optimal K_i , we will need to solve the following optimization problem

$$\begin{aligned}
 & \min_{\gamma, W_i, Y \geq 0} \\
 & \text{subject to:} \\
 & \begin{bmatrix} YA_i^T + AY - BW_i - W_i^T B^T & YH^T & W_i^T \\ & HY & -I_n & 0 \\ & W_i & 0 & -R^{-1} \end{bmatrix} < 0 \quad i = 1, \dots, N \quad (36) \\
 & \begin{bmatrix} \gamma I_n & I_n \\ I_n & Y \end{bmatrix} > 0
 \end{aligned}$$

Then, after the solution of this problem, the optimal K_i will be obtained as follows:

$$K_i = W_i Y^{-1} \quad (37)$$

The tuning of the LPV LQR controller parameters Q and R is obtained by varying their values and determining the Pareto plot presented in Figure 12 which allows us to determine the parameters that provide the best trade-off between error minimisation (performance) and control effort (energy consumption). The best value for the parameters is achieved in the corner point of the plot presented in Figure 12.

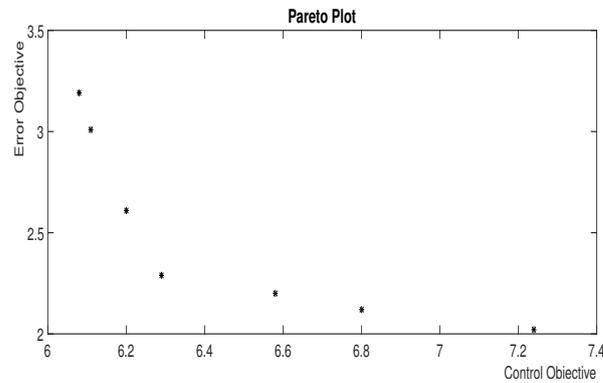


Figure 12. Tuning control parameters using the Pareto plot.

Figure 13 shows the closed-loop response of the PV cell temperature using the designed LPV LQR optimal controller (29). The PV/T system is simulated using the nonlinear model presented in Section 3. In this figure, we can observe that after the application of this controller, the PV cell temperature reaches the optimal value (25 °C) in a short time. This shows the effectiveness of this controller in terms of regulating the temperature of PV cells around the optimal value.

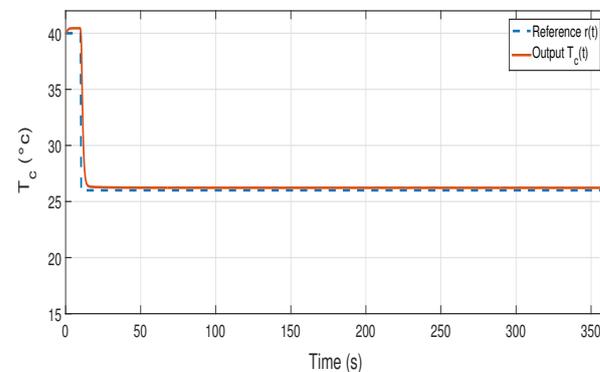


Figure 13. PV cell temperature (T_c) applying the LQR LPV controller (without disturbance).

To show the benefits of using the LPV LQR controller proposed in this paper, it is compared with the results obtained using a classical linear-time invariant (LTI) LQR optimal controller designed with the model linearised around the optimal operating point.

This controller has a single controller gain matrix K that will be applied in the whole operating range, different from the LPV LQR controller that uses a set of controllers which are scheduled with the operating point according to (29).

The simulation results obtained with the LTI LQR controller are presented in Figure 14. It can be observed that the LQR controller is not able to exactly reach the steady state value because of the variation of the system matrix A with the operating point (19). This fact motivates the use of the proposed LPV approach.

Figure 15 shows the evolution of the control action u that represents the mass flow rate of water injected by the pump from the water tank to the absorber.

The trade-off between speed of the time-response and energy consumption in the water pump can be established with the LQR weights Q and R , respectively.

Further, a disturbance was added to the PV/T system. Figure 16 shows the evolution of the PV cell temperature proving that the controller is able to adjust the PV cell temperature to the optimum value despite the disturbance.

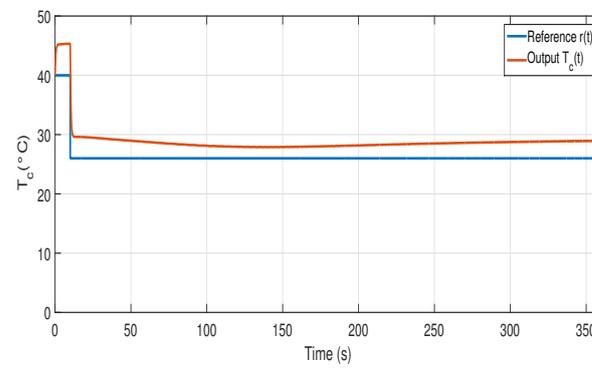


Figure 14. Evolution of the PV cell temperature (T_c) with LQR controller.

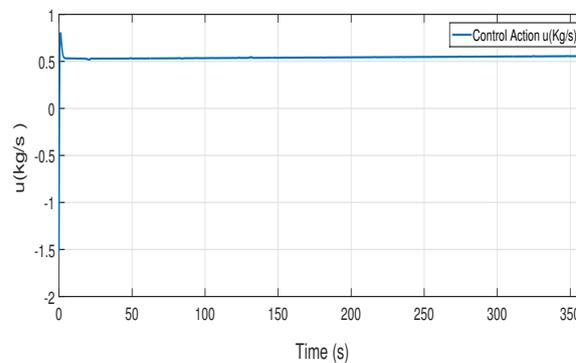


Figure 15. Control action $u(t)$.

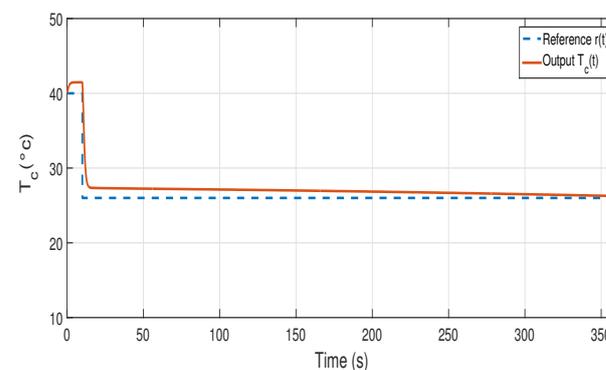


Figure 16. PV cell temperature (T_c) applying the LQR LPV controller (with disturbance).

Finally, from Equations (6) and (7), the electrical power P_e (that corresponds with P_{pv}) generated by the PV/T system is equal to

$$P_e = \eta_{elec} S_{pv} G \quad (38)$$

The evolution of this electrical power after the application of the control to adjust the PV cell temperature to its optimal value is represented in Figure 17.

Figure 17 shows the generation of electrical power when the temperature of the PV cell has been adjusted to an optimal value. According to (7), the PV cell produces the maximum electrical power in this case.

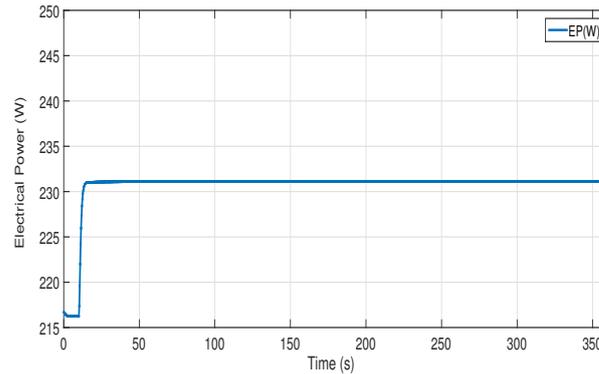


Figure 17. Electrical power obtained using the proposed LPV LQR controller.

6. State Estimator Design of the PV/T System

To implement the previous controller, we need to have access to all the temperatures of the thermal model (17). However, as discussed in Section 2, the measurements provided by the available sensors only provide the electrical power (P_e) and the thermal power (Q_i). So, we will need a state estimator that, using the available sensors and the thermal model, will be able to state the temperatures (states) of the PV/T system.

In this section, we will design an optimal state estimator based on an LPV Kalman filter with the LMI method. The considered LPV state estimator has the following structure

$$\dot{\hat{x}}(t) = A(\theta)\hat{x}(t) + Bu(t) + L(\theta)(y(t) - \hat{y}(t)) \quad (39)$$

$$\hat{y}(t) = C\hat{x}(t) \quad (40)$$

where the gain-scheduled estimator gain $L(\theta)$ is defined as

$$L(\theta) = \sum_{i=1}^N v_i(\theta)L_i \quad (41)$$

Obtaining the estimator gains L_i associated to the vertices of the polytopic model (24) is based on formulating the Kalman filter problem in LMI form as presented in the following, considering that the state observer equations can be rewritten as follows:

$$\dot{\hat{x}}(t) = (A(\theta) - L(\theta)C)\hat{x}(t) + Bu(t) + L(\theta)y(t) \quad (42)$$

Applying the duality principle between control and estimation to the LQR Riccati Equation (32) ($A_i \rightarrow A^T$, $B \rightarrow C^T$, $K_i \rightarrow L_i^T$), we arrive at

$$(A_i^T - C^T L_i^T)^T P + P(A_i^T - C^T L_i^T) + Q + L_i R L_i^T < 0 \quad (43)$$

To express this equation in LMI form, we proceed similarly to the LQR case; we will right multiply (32) by $Y = P^{-1}$ and introduce the following change of variables :

$$W_i = L_i^T Y \quad (44)$$

$$Q = H^T H \quad (45)$$

Then, we will apply the Schur lemma and find the following LMI representation for (43)

$$\begin{bmatrix} YA_i + A_i^T Y - C^T W_i - W_i^T C & YH^T & W_i^T \\ & HY & -I_n & 0 \\ & W_i & 0 & -R^{-1} \end{bmatrix} < 0 \quad (46)$$

Finally, to obtain the optimal L_i we will need to solve the following optimization problem

$$\begin{aligned} & \min_{\gamma, W_i, Y \geq 0} \\ & \text{subject to:} \\ & \begin{bmatrix} YA_i + A_i^T Y - C^T W_i - W_i^T C & YH^T & W_i^T \\ & HY & -I_n & 0 \\ & W_i & 0 & -R^{-1} \end{bmatrix} < 0 \quad i = 1, \dots, N \\ & \begin{bmatrix} \gamma I_n & I_n \\ I_n & Y \end{bmatrix} > 0 \end{aligned} \quad (47)$$

Then, after the solution of this problem, the optimal L_i will be obtained as follows:

$$L_i = Y^{-1} W_i \quad (48)$$

Figure 18 shows the response of the closed-loop system when the LPV Kalman-based state observer, designed using the previous procedure, is used to estimate the states. Comparing this response with the one presented in Figure 12, we can see that it is identical to the one obtained using the LPV state feedback controller considering all states measured. This validates the merit of the proposed state estimation scheme.

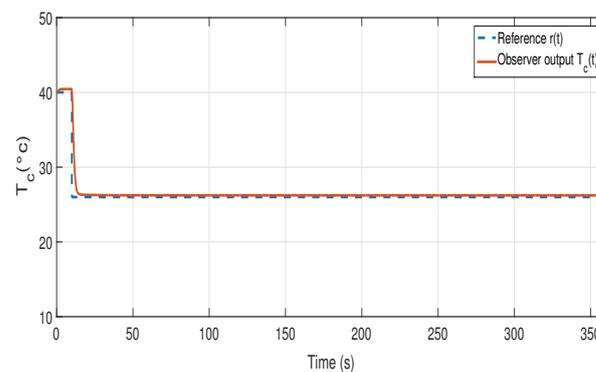


Figure 18. PV cell temperature T_c of polytopic LPV system with observer.

7. Conclusions

In this work, the modeling and control of a hybrid PV/T water system in the linear parameter varying (LPV) framework has been proposed. First, the physical model of this PV/T hybrid system was presented. Then, a control-oriented model was derived by transforming the physical nonlinear model into an LPV representation. Using this representation in polytopic form, an optimal LQR LPV state feedback controller was designed using the LMI method. The obtained controller was implemented and tested in simulation, taking into account the disturbance presented by the solar radiation and the ambient temperature during the day. The main goal of this controller is to regulate the PV cell temperature to an optimal value in order to guarantee the extraction of the maximum electrical power. Additionally, a state estimator scheme based on an LPV Kalman

filter is proposed to estimate the temperatures of the different layers from the available sensors. The obtained results prove that the optimal LQR LPV state feedback controller not only successfully avoids the problem of temperature increase in PV cells, allowing the PV/T system to extract the maximum electrical energy, but also offers better performance and improvement in higher energy production despite external disturbances. As part of future work, the proposed approach will be tested in the real setup available in the CRTEN laboratory.

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Conflicts of Interest: The authors declare no conflict of interest.

Nomenclature

Table compiles the descriptions of the main symbols used throughout the paper.

Symbol	Description
A_i	Area, m^2
M_i	Mass, kg
\dot{m}	Water flow rate, l/min
C_i	Specific heat capacity, J/kg K
G	Solar radiation, W/m^2
T_v, T_c, T_p, T_f	Layer temperature, $^{\circ}C$
T_a	Ambient temperature, $^{\circ}C$
h_i	Heat transfer coefficient, W/m^2K
h_r	Radiation heat transfer coefficient, W/m^2K
k	Insulation thermal conductivity, $W/m K$

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