

Article

Effects of Surface Rotation on the Phase Change Process in a 3D Complex-Shaped Cylindrical Cavity with Ventilation Ports and Installed PCM Packed Bed System during Hybrid Nanofluid Convection

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Abstract: The combined effects of surface rotation and using binary nanoparticles on the phase change process in a 3D complex-shaped vented cavity with ventilation ports were studied during nanofluid convection. The geometry was a double T-shaped rotating vented cavity, while hybrid nanofluid contained binary Ag–MgO nano-sized particles. One of the novelties of the study was that a vented cavity was first used with the phase change–packed bed (PC–PB) system during nanofluid convection. The PC–PB system contained a spherical-shaped, encapsulated PCM paraffin wax. The Galerkin weighted residual finite element method was used as the solution method. The computations were carried out for varying values of the Reynolds numbers ($100 \leq Re \leq 500$), rotational Reynolds numbers ($100 \leq Rew \leq 500$), size of the ports ($0.1L1 \leq di \leq 0.5L1$), length of the PC–PB system ($0.4L1 \leq L0 \leq L1$), and location of the PC–PB ($0 \leq yp \leq 0.25H$). In the heat transfer fluid, the nanoparticle solid volume fraction amount was taken between 0 and 0.02%. When the fluid stream (Re) and surface rotational speed increased, the phase change process became fast. Effects of surface rotation became effective for lower values of Re while at $Re = 100$ and $Re = 500$; full phase transition time (tp) was reduced by about 39.8% and 24.5%. The port size and nanoparticle addition in the base fluid had positive impacts on the phase transition, while 34.8% reduction in tp was obtained at the largest port size, though this amount was only 9.5%, with the highest nanoparticle volume fraction. The length and vertical location of the PC–PB system have impacts on the phase transition dynamics. The reduction and increment amount in the value of tp with varying location and length of the PC–PB zone became 20% and 58%. As convection in cavities with ventilation ports are relevant in many thermal energy systems, the outcomes of this study will be helpful for the initial design and optimization of many PCM-embedded systems encountered in solar power, thermal management, refrigeration, and many other systems.

Keywords: vented cavity; complex geometry; phase change process; surface rotation; hybrid nanofluid

1. Introduction

Thermal management with phase change material (PCM) is important to consider in diverse, energy-related technologies, such as solar power, refrigeration, energy storage, electronic cooling, waste heat recovery, and many others [1–4]. This is due to the need for clean energy technologies, the cost of energy, and concerns about environmental side effects. The effectiveness of using PCMs has been improved by using metal foams and conductive fins [5,6]. Recently, nanoparticles have been used for

improving the performance of PCMs and to accelerate the phase change (Ph-C) process in diverse applications [7–9]. PCM-packed bed (PB) systems are considered in many energy applications, such as in solar, air conditioners, and many others [10]. A review for the application of PCM–PB systems and their numerical models with correlations were presented in [11]. There are a few studies that considered the application of nanofluids in PCM–PB systems [12].

Thermo-fluid applications in vented cavities arise in different areas, including air conditioning-ventilation of buildings, food technology, electronic cooling, energy storage, and many others [13]. The fluid–thermal interaction within a vented cavity is complex, due to the occurrence of multi-recirculation zones. There are many studies that considered the convective heat transfer (HT) in 2D vented cavities of simple shapes, such as squares or rectangles [14,15]. There are a few studies that considered the convection within 3D vented cavities [16–19] or complex-shaped geometries [20–23]. The opening location, size, and number of ports are important in the HT amount [24]. Many methods have been offered to improve the HT with vented cavities, such as using fins [25,26], rotating objects [27,28], flow pulsations [29,30], magnetic fields [31], and elastic walls [32]. Nanofluids have also been considered in vented cavities and in convection studies [33–38], and their effectiveness has been shown.

In the present study, the PCM–PB system is utilized with nanofluids, and Ph-C process dynamics are numerically analyzed for a complex-shaped vented cavity having one inlet and outlet port. As the HT fluid, hybrid nanofluid, which contains Ag–MgO binary particles, was used. The vented cavity is a double T-shaped complex cylindrical reactor. The present study explored the Ph-C in such a geometry with rotational surface effects. Nanoparticle loading in the base fluid was considered where experimental data for the effective nanofluid property was used. The nanofluid behavior with PCM packed bed system was considered. Non-equilibrium heat transfer is taken into account where different temperatures for fluid and solid phases in the PCM-packed bed region were utilized in a complex geometry, by using finite element method. The external flow conditions with the PCM-packed bed system are coupled together. The rotation of the system was also considered for the vented cavity. There are a few studies that considered the convection in vented cavities in 3D, and none of them included the rotational effects. One of the novelties of the configuration is that a vented cavity was used with a PCM packed bed system for the first time during nanofluid convection. Owing to many use of vented cavities in diverse energy system technologies, and considering many energy-related products with embedded PCMs, the outcomes of this study will be helpful in the design and product development of similar systems encountered in solar power, cooling applications, heat exchanger design, and many other systems.

2. Computational Details of PCM–PB Integrated System

The phase change process (Ph-C) in a complex-shaped vented cavity was examined under the effects of surface rotations during the nanofluid convection in a PCM-packed bed (PB) system. The cavity is a double T-shaped cylindrical enclosure, while hybrid nanoparticles are used in the base fluid, as shown in Figure 1. One inlet and exit port were used in the vented cavity with port sizes of d_i . The cylindrical complex-shaped cavity rotated around the mid axis with rotational speed of ω . The PCM packed bed zone was included in between the double T-shaped cavities, with a height of h_{pc} and length of L_0 , while it was located by a distance of y_{pc} above the lower T-shaped cavity. Here, H and L_1 denote the height and radius of the cylindrical double T-shaped enclosure.

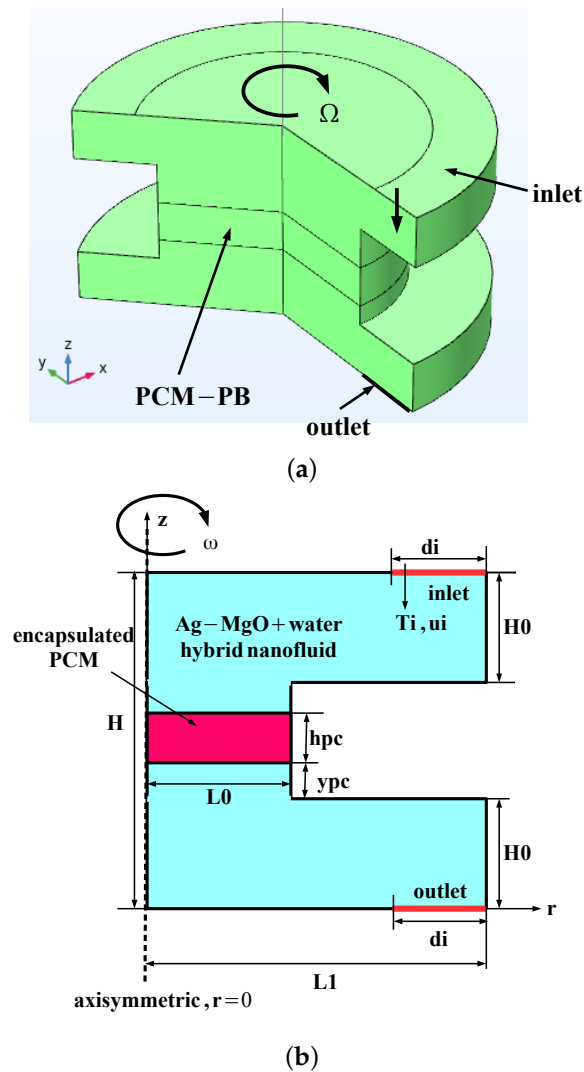


Figure 1. 3D view of the complex geometry of the vented cavity with one inlet and outlet port, as well as the (a) boundary conditions and schematic view in 2D (b).

The PCM is a spherical-shaped encapsulated paraffin wax, being 30 mm in diameter with the given thermophysical properties in [39]. The porosity of the medium for the PCM installed zone is 55. As the heat transfer (HT) fluid, water and the binary particles of Ag and MgO were considered. The solid volume fraction of the hybrid particles (NC) was taken between 0 and 0.02%. The coupled effects of surface rotation and forced convection in a vented cavity with ventilation ports were explored under the nanoparticles loading in the HT fluid. The conservation equations for the upper and lower T-shaped domains were stated as [40,41]:

$$\nabla \cdot \mathbf{u} = 0 \quad (1)$$

$$\rho(\mathbf{u} \cdot \nabla) \mathbf{u} = \nabla \cdot \left[-p\mathbf{I} + \mu(\nabla \mathbf{u} + (\nabla \mathbf{u})^T) \right] \quad (2)$$

$$\rho c_p \frac{\partial T}{\partial t} + \rho c_p \mathbf{u} \cdot \nabla T = \nabla \cdot (k \nabla T). \quad (3)$$

In the PCM packed bed zone, they were as stated in the following [42,43]:

$$\nabla \cdot \mathbf{u} = 0 \quad (4)$$

$$\frac{1}{\varepsilon_p} \rho(\mathbf{u} \cdot \nabla) \mathbf{u} \frac{1}{\varepsilon_p} = \nabla \cdot \left[-p\mathbf{I} + \mu \frac{1}{\varepsilon_p} (\nabla \mathbf{u} + (\nabla \mathbf{u})^T) \right] - (\mu \kappa^{-1} + \beta_p \rho |\mathbf{u}|) \mathbf{u} \quad (5)$$

by using the Kozeny–Carmen permeability model, as in the following [44–46]

$$\kappa = \frac{d_p^2}{180} \frac{\varepsilon_p^3}{(1 - \varepsilon_p)^2} \quad (6)$$

The following properties were used in the PCM region as [42]:

$$\begin{aligned} k &= \theta k_{f1} + (1 - \theta)k_{f2}, \quad \alpha_m = \frac{1}{2} \frac{(1 - \theta)\rho_{f2} - \theta\rho_{f1}}{\theta\rho_{f1} + (1 - \theta)\rho_{f2}}, \\ C_p &= \frac{1}{\rho} \left(\theta\rho_{f1}C_{p,f1} + (1 - \theta)\rho_{f2}C_{p,f2} \right) + L \frac{\partial \alpha_m}{\partial T}, \\ \theta &= 1 - \alpha, \quad \rho = \theta\rho_{f1} + (1 - \theta)\rho_{f2}, \end{aligned} \quad (7)$$

by using the function α , the energy equation was rewritten in the same way as in Equation (6). The α function value is 0 for $T < (T_m - \Delta T_m/2)$ and 1 for $T > (T_m + \Delta T_m/2)$.

Non-equilibrium HT interface was utilized between the phases. Two equations and additional source terms were described in the following [47]:

$$\theta_p \rho_s C_{p,s} \frac{T_s}{\partial t} + \nabla \cdot \mathbf{q}_s = q_{sf} (T_f - T_s) + \theta_p Q_s, \quad (8)$$

$$\mathbf{q}_s = -\theta_p k_s \nabla T_s, \quad \mathbf{q}_f = -(1 - \theta_p) k_f \nabla T_f. \quad (9)$$

$$\begin{aligned} (1 - \theta_p) \rho_f C_{p,f} \frac{T_f}{\partial t} + (1 - \theta_p) \rho_f C_{p,f} \mathbf{u}_f \cdot \nabla T_f + \\ + \nabla \cdot \mathbf{q}_f = q_{sf} (T_s - T_f) + (1 - \theta_p) Q_f, \end{aligned} \quad (10)$$

where the conductive heat fluxes of phases are represented by the terms \mathbf{q}_f and \mathbf{q}_s , while interstitial convective HT and source terms were given by the terms q_{sf} and Q . Description of the interstitial HT coefficient is stated as [47]:

$$\frac{1}{h_{sf}} = \frac{2r_p}{k_f \text{Nu}} + \frac{2r_p}{\beta k_s}, \quad (11)$$

where β has a value of 10 for spherical particles. The fluid-to-solid Nu number is described as [48]:

$$\text{Nu} = 2 + 1.1 \text{Pr}^{1/3} \text{Re}_p^{0.6}, \quad (12)$$

with particle Prandtl (Pr) and Reynolds numbers (Re) as:

$$\text{Pr} = \frac{\mu C_{p,f}}{k_f}, \quad \text{Re}_p = \frac{2r_p \rho_f |u_f|}{\mu}. \quad (13)$$

As the HT-fluid hybrid nanofluid (water + Ag–MgO nano-additives) is considered [49]. Effective density and specific heat of the nanofluid are given as [49]:

$$\rho_{nf} = \left[(1 - \phi_2) \left((1 - \phi_1) \rho_f + \phi_1 \rho_{s1} \right) \right] + \phi_2 \rho_{s2}, \quad (14)$$

$$(\rho c_p)_{nf} = \left[(1 - \phi_2) \left((1 - \phi_1) (\rho c_p)_f + \phi_1 (\rho c_p)_{s1} \right) \right] + \phi_2 (\rho c_p)_{s2} \quad (15)$$

As for the thermal conductivity (k_{nf}) and viscosity (μ_{nf}) description of the hybrid nanofluid, experimental data were used. The correlations depend upon the solid volume fraction of nanoparticles [50]. They are defined as [50]:

$$k_{nf} = \left(\frac{0.1747 \times 10^5 + \phi}{0.1747 \times 10^5 - 0.1498 \times 10^6 \phi + 0.1117 \times 10^7 \phi^2 + 0.1997 \times 10^8 \phi^3} \right) k_f, \quad (16)$$

$$\mu_{nf} = \left(1 + 32.795\phi - 7214\phi^2 + 714600\phi^3 - 0.1941 \times 10^8 \phi^4\right) \mu_f. \quad (17)$$

where ϕ is the sum of the solid volume fractions of binary nanoparticles in the HT-fluid as:

$$\phi = \phi_1 + \phi_2. \quad (18)$$

The Reynolds number (Re) and rotational Reynolds number (Rew) are the relevant non-dimensional parameter of interest. They are described as:

$$\text{Re} = \frac{u_i H \rho}{\mu}, \quad \text{Rew} = \frac{\omega H^2 \rho}{\mu} \quad (19)$$

The inlet temperature is T_i . An axis-symmetrical model was considered with $\frac{\partial T}{\partial r} = 0$. At the exit port, pressure outlet boundary conditions were used, while the walls of the vented cavity were considered as adiabatic $\frac{\partial T}{\partial n} = 0$. The initial temperature was taken as 303 K.

As for the solution of the above described governing equations with appropriate initial and boundary conditions, Galerkin weighted residual FEM was used. Details of the method and implementation for heat transfer and fluid flow problems can be found in various references [51–54]. The field variables of interest (velocity components, pressure, fluid, and solid temperatures) are approximated by using the Lagrange shape functions of different orders. For any field variable of interest (S), the approximation is stated as in the following [55,56]:

$$S = \sum_{j=1}^m S_j \Phi_j \quad (20)$$

where S_j and Φ_j denote the nodal value and shape function. When the approximated field variable are inserted into the governing equations, residuals (R) are obtained. They were set to be zero in an average sense by using a weight function (W) as in the following [55]:

$$\int_V W R dV = 0. \quad (21)$$

The weight function was chosen from the same set of function as of trial. For the approximation of the velocity components and pressure, P2–P1 Lagrange finite elements were used, while temperature was approximated by using Lagrange quadratic finite elements. Artificial diffusion with the streamline upwind Petrov–Galerkin method (SUPG) was used in the solver to handle local numerical instabilities. Biconjugate gradient stabilized iterative method solver (BICGSTab) was used for fluid flow and heat transfer modules of code. The convergence criteria was defined as in the following:

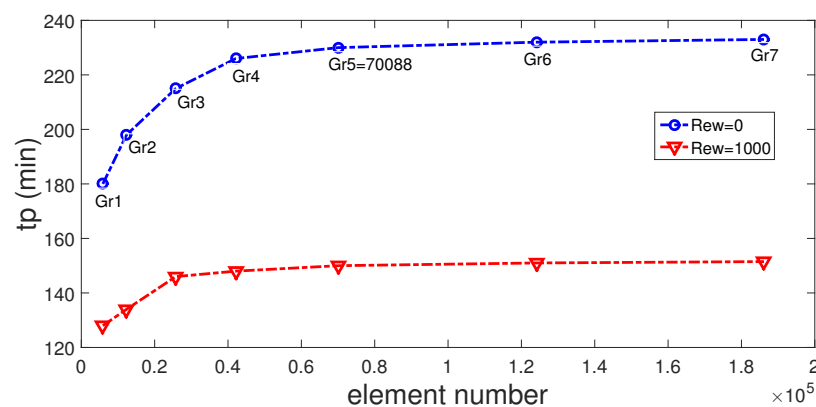
$$\left| \frac{\Gamma^{i+1} - \Gamma^i}{\Gamma^{i+1}} \right| \leq 10^{-7} \quad (22)$$

The time-dependent part was treated by using a variable-order backward differentiation formula (BDF) [57–59].

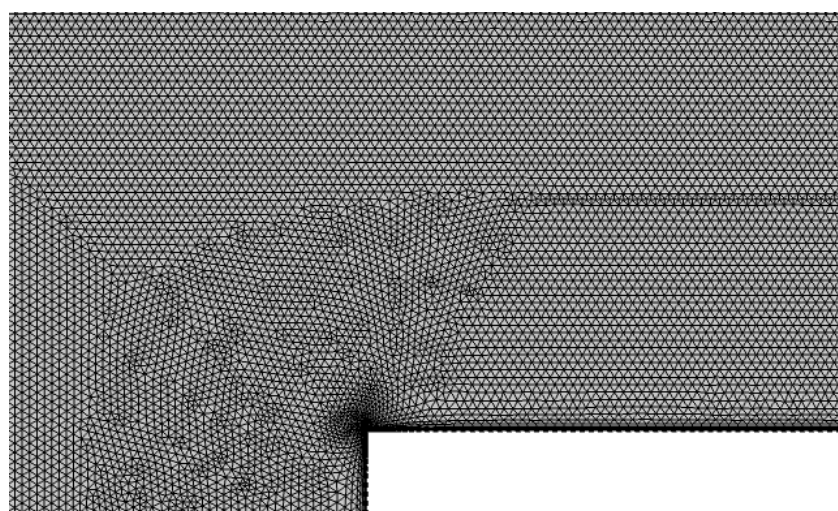
Tests for grid independence were performed by using grid types. Figure 2a shows the phase transition time (tp (min)) for different element numbers at two different rotations. Grid system 5, with 70,088 elements, was used. Grid distribution is shown in Figure 2b.

The numerical code is validated by using different available results in the literature for phase change and convection in a vented cavity. In the first study, the experimental values in [60] were used, where phase change process in a heated cavity was explored and fluid–solid interfaces were measured, along with the temperatures. The amount of solidified volume fraction was stated in terms of dimensionless time (te), cavity aspect ratio (AR) and Rayleigh number (Ra). Solidified volume fraction comparison results for $AR = 1$ at different times are shown in Figure 3, while the maximum difference of 9.3% was observed. In another validation test, convection in a vented cavity was considered, and the numerical results available in [14] were used. Figure 4 shows the comparisons of

average Nu number for different Re numbers. A maximum deviation of 3.3% was observed between the results. These results reveal that the present code was capable of capturing the effects of convective HT, with ventilation ports and phase change process dynamics, in the cavity.



(a)



(b)

Figure 2. Numerical test results for grid independence at two rotational Re numbers (a) and grid distribution for one part of the computational domain (b).

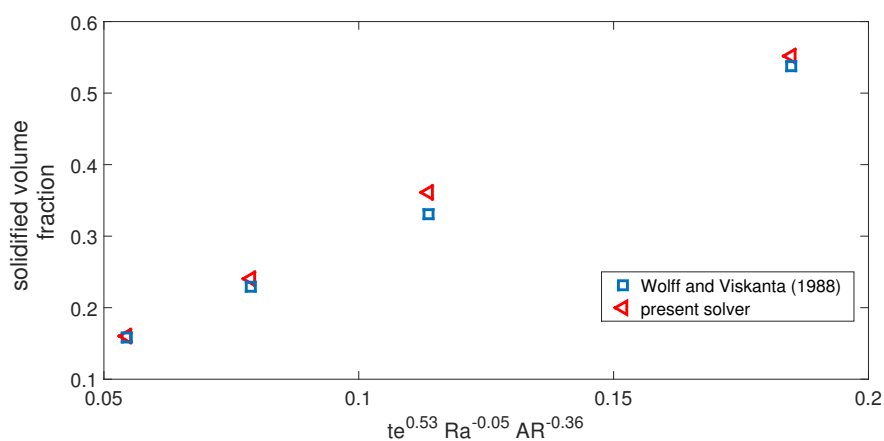


Figure 3. Comparison results (with [60]) for fraction of the solidified volume at various times for Ph-C process in a differentially heated cavity.

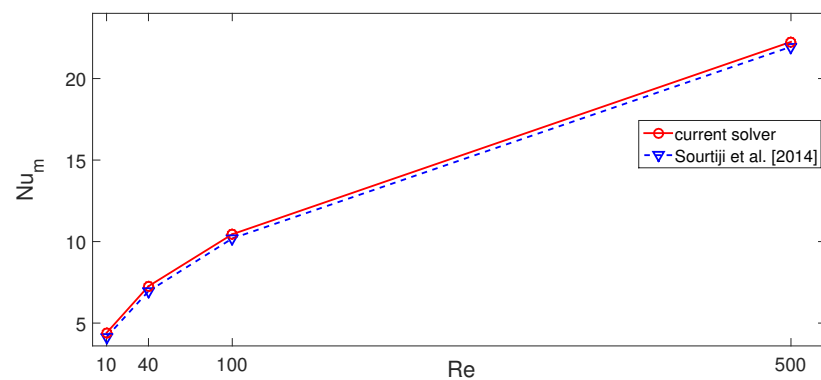


Figure 4. Average Nu number comparisons (with results of [14]) for different Re numbers, when convective HT in a vented cavity was considered.

3. Results and Discussion

The effects of geometric and operating parameters on the PhC dynamics in PCM–PB cylindrical complex-shaped cavity with ventilation ports were studied during nanofluid convection. The cavity had a double T-shape, while rotational surface effects were also considered. The nanofluid contained hybrid Ag–MgO nano-sized particles, while the PCM–PB system contains spherical-shaped, encapsulated PCM paraffin wax. The numerical tests are conducted for varying values of Re number ($100 \leq Re \leq 500$), rotational Re number ($100 \leq Rew \leq 500$), port size ($0.1L_1 \leq d_i \leq 0.5L_1$), PCM zone length ($0.4L_1 \leq L_0 \leq L_1$), location of the PCM zone ($0 \leq yp \leq 0.25H$) and nanoparticle solid volume fraction ($0 \leq NC \leq 0.5L_1$).

Figure 5 shows the flow pattern distributions within the cavity for different fluid stream Re ($Rew = 500$) and rotational Re numbers ($Re = 300$). The recirculation zones were established within the cavity, near the inlet port and above the exit port, when Re increased from $Re = 100$ to $Re = 250$. Above the PCM–PB region, toward the wall, a small vortex was also formed. As the Re further increased, the extent of those zones also modified with increased fluid stream velocity. In the absence of rotational surface effects (Figure 5d, $Rew = 0$), the upper vortex near the inlet port becomes closer to the interior of the domain. When rotational effects are considered, the vortex size near the inlet port and on the bottom corner of the upper region became larger. The fluid velocity near the walls rose, due to the rotation of the surfaces and interactions with the main fluid stream, effecting the Ph-C dynamics near the walls and in the interior of the complex-shaped cavity. The distribution of the liquid fraction (L_q), with varying fluid stream Re and rotational Re numbers, is shown in Figure 6. The Ph-C process becomes fast, especially near the walls, for higher Re number; at $t = 150$ min, a complete phase transition occurs within the cavity. However, at $Re = 100$, there are locations in the interior of the PCM–PB domain with $L_q = 0$. For the case of a higher value of fluid stream Re number, better thermal transport within the PCM–PB system was obtained, which accelerates the Ph-C process. When rotational surface effects were considered, along with the higher fluid stream velocity, it had a positive impact on the Ph-C process, especially near the wall region, due to the higher fluid velocity at those locations. The effect of Re on the distribution of L_q becomes apparent, at times, near the complete phase transition. At $t = 150$ min, a complete phase change was seen for the configuration with $Rew = 150$. The dynamics of the L_q were affected by varying the Re and Rew numbers, while the impact of the Re on the Ph-C dynamics was significant (Figure 7). The value of $L_q = 1$ was reached in a shorter time, with higher values of Re. However, the behavior of L_q (with varying Re) was different, depending upon the time interval. After $t = 70$ min, the Ph-C process becomes fast, with the highest rotational Re number, while the trend was opposite before $t = 70$ min.

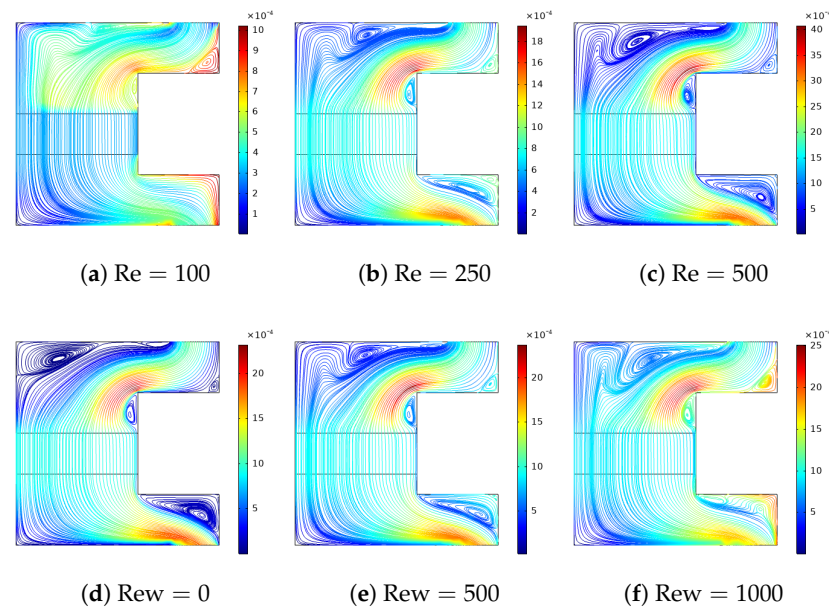


Figure 5. Impacts of fluid stream Re ($Rew = 500$, (a)–(c)) and rotational Re numbers ($Re = 300$, (d)–(f)) on the flow pattern distributions within the vented U-shaped cavity ($di = 0.25 L1$, $L0 = 0.6 L1$, $yp = 0.1 H$, and $NC = 0.02$).

The complete phase transition time (tp in minutes) reduces with higher fluid stream Re number, as shown in Figures 8a and 9a. The amount of reduction depends upon the amount of the rotation of the vented cavity. At $Rew = 500$, up to 51% reduction in the tp was obtained at the higher fluid stream Re number. In the absence of rotation ($Rew = 0$), the amount of reduction in the tp was 61%, while with the rotation of the surface at the highest speed, the amount was only 49%. Even though the tp value was lower with higher rotational surface effects (generally), the effectiveness in increasing the fluid stream velocity on the variation of tp was higher (without the rotation of the surface). As the surface rotational speed increased, the Ph-C process generally became fast and a reduction in the tp was observed. However, the impacts of rotation on the Ph-C process was significant at low fluid stream Re number. At $Re = 100$, 300, and 500, the amount of reductions in the tp were 39.8%, 34.8%, and 24.5% (when comparing cases without rotation ($Rew = 0$) and with rotations at the highest speed ($Rew = 1000$)).

The geometric variation of the 3D complex-shaped vented cavity were also influential on the fluid flow, HT, and Ph-C dynamics. One of the important geometric parameters was the port size at the inlet and outlet for the vented cavity. Their sizes were taken as di and varied during the simulations. Figure 10 shows the flow pattern variations within the vented cavity for different port sizes. When the port size increased, the upper vortex near the inlet becomes closer to the interior of the domain, while its extent increased with larger port sizes. The vortex size above the exit port also enlarged with higher values of di . The length of the PCM–PB zone effects the re-circulation zone distribution within the 3D complex-shaped vented cavity. A large vortex, occupying the most of the upper domain near the inlet port, was observed for $L0 = L1$. When the size of the PCM zone was reduced, a large vortex was established above the exit port, while near the inlet port, it disappeared. The Ph-C process was significantly influenced by the port size, as shown in Figure 11, at various time instances. In the interior of the vented cavity, the phase transition was fast for a large portion of the domain with larger port sizes. This is due to the penetration of the more fluid stream in the interior of the domain with larger port sizes and the increased effects of thermal transport within the PCM–PB zone. At $t = 150$ min, complete phase transition was seen for port size $di = 0.5 L1$.

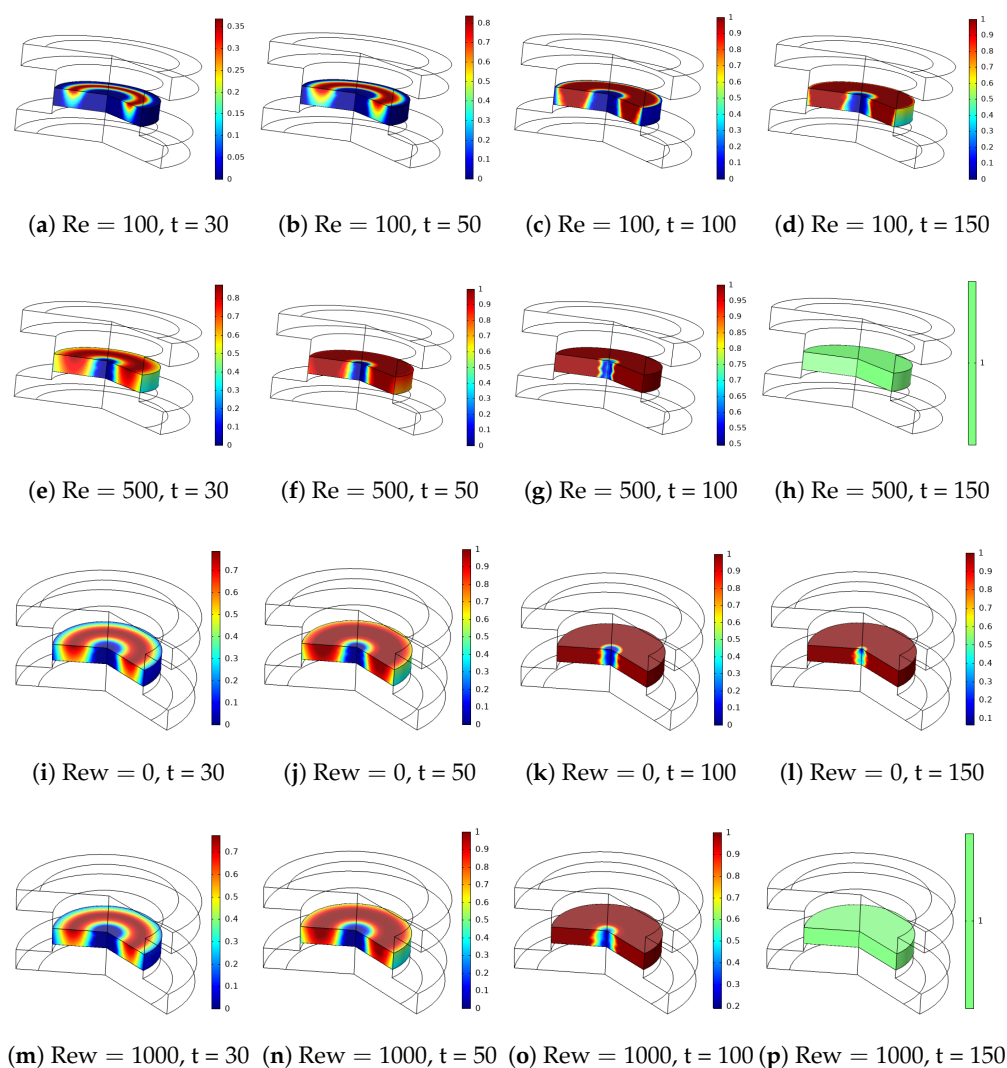


Figure 6. Distribution of liquid fraction (Lq) with varying fluid stream Re number ($Re_w = 500$, (a)–(h)) and rotational Re number ($Re = 300$, (i)–(p)) at various time instances (t in minutes) ($d_i = 0.25 L_1$, $L_0 = 0.6 L_1$, $\eta p = 0.1 H$, $NC = 0.02$).

The acceleration of the Ph-C with higher port size and its impacts on the dynamics of transition are shown in Figure 12. The phase transition time (t_p in minutes) was reduced by about 34.8%, with the highest port size. As the length of the PCM–PB region was increased, the Ph-C process became slower and the value of the t_p rose with higher L_0 . This was due to the increment of the number of spherical-shaped, encapsulated PCMs. The coupled interaction between the flow dynamics with the change in the geometry of the vented cavity and the number of spheres in the PB zone determines the amount of rise in the t_p . The increment in the t_p was about 58%, when configurations with smallest and largest L_0 were compared (Figure 13). The vertical location of the PCM–PB zone is also influential on Ph-C dynamics. When the vertical position is closer to the inlet port, it has a positive impact on the Ph-C process, as shown in Figure 14a. Complete phase transition time was reduced by about 20%, when the cases with $yp = 0.01$ H and $yp = 0.25$ H were compared. Performance improvements were further achieved by using nano-sized particles in the base HT fluid. The flow re-circulation and separated flow region near the contracted area were altered by using nanoparticles and varying their amount. The variation in the flow field affects the Ph-C dynamics. On the other hand, thermal transport within the PCM zone also positively affects nanoparticle loading in the HT fluid. The amount of reduction in t_p was obtained as 9.5%, with the highest nanoparticle volume fraction (Figure 14b).

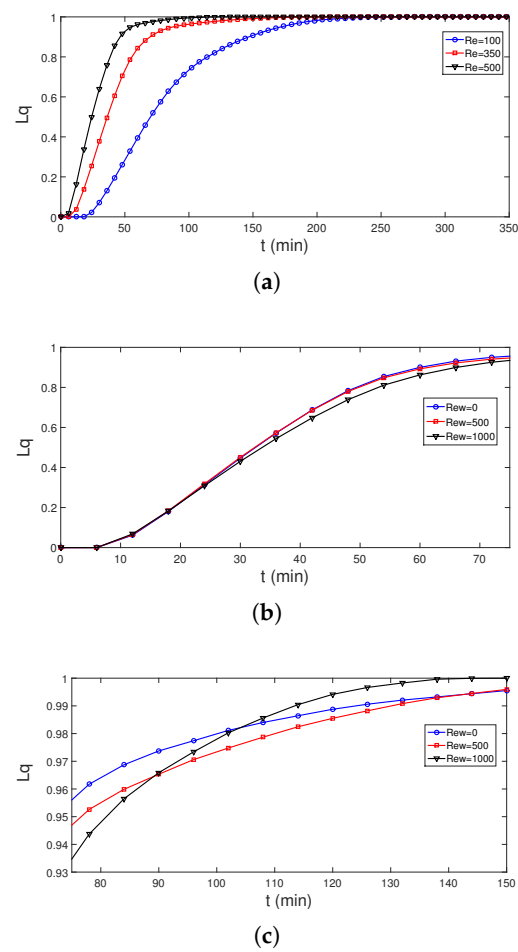


Figure 7. Time evolution of average Lq with varying Re ((a) $Re\omega = 500$) and varying $Re\omega$ ((b,c) $Re = 300$) ($di = 0.25 L1$, $L0 = 0.6 L1$, $yp = 0.1 H$, and $NC = 0.02$).

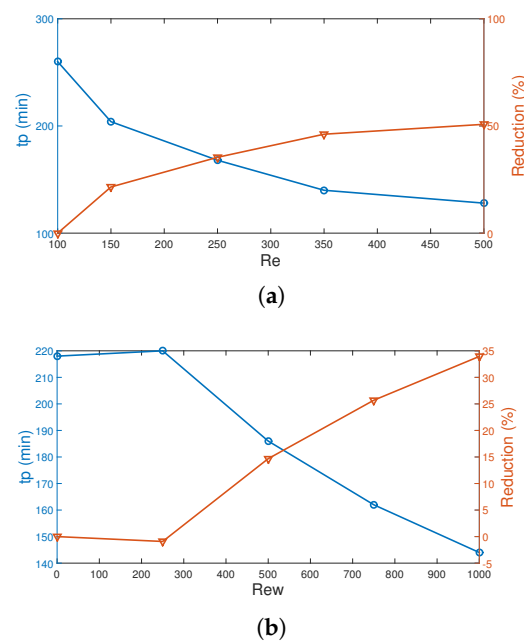


Figure 8. Complete phase transition time (tp in minutes) with varying Re (a) and rotational Re (b). The amount of reduction in the tp is also presented in the figures ($di = 0.25 L1$, $L0 = 0.6 L1$, $yp = 0.1 H$, and $NC = 0.02$).

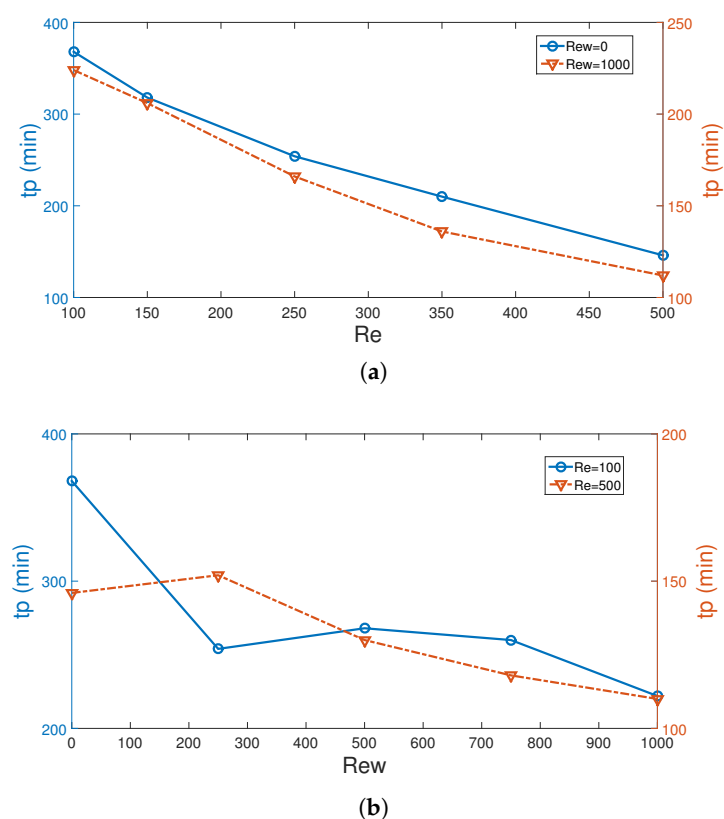


Figure 9. Complete phase transition time (tp in minutes) with varying Re at the lowest and highest Rew (a) and with varying Rew at the lowest and highest Re (b) ($di = 0.25 L1$, $L0 = 0.6 L1$, $yp = 0.1 H$, and $NC = 0.02$).

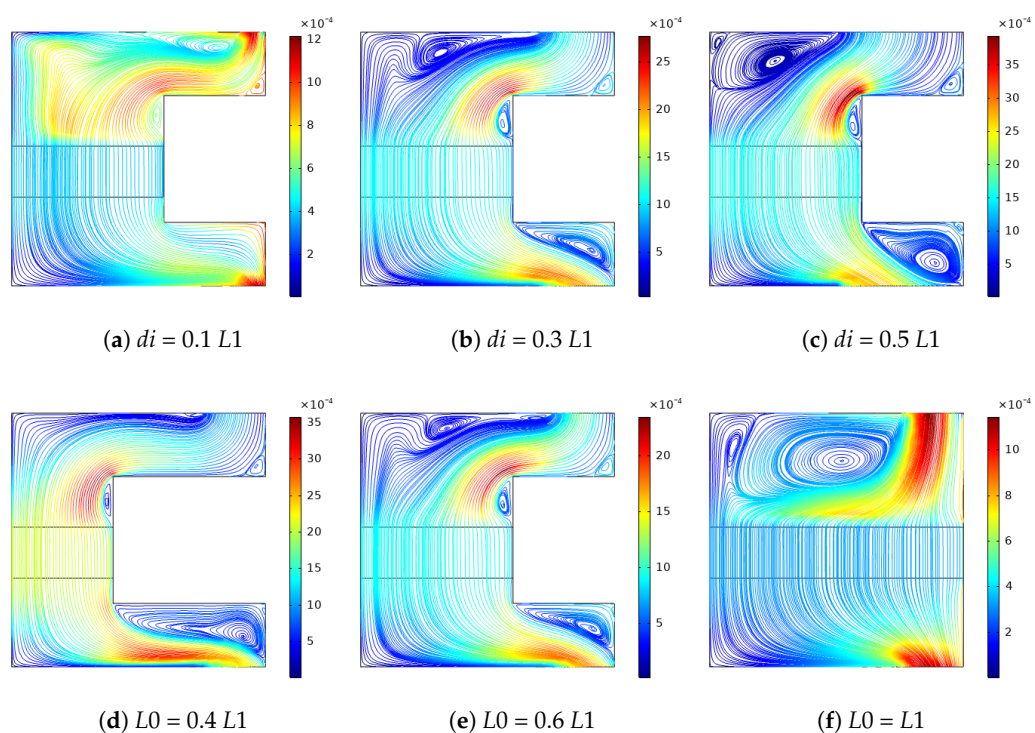


Figure 10. Effects of port size ($L0 = 0.6 L1$ (a–c)) and PCM domain length ($di = 0.25 L1$ (d–f)) on the distribution of flow patterns within the U-shaped cavity ($Re = 300$, $Rew = 500$, $yp = 0.1 H$, and $NC = 0.02$).

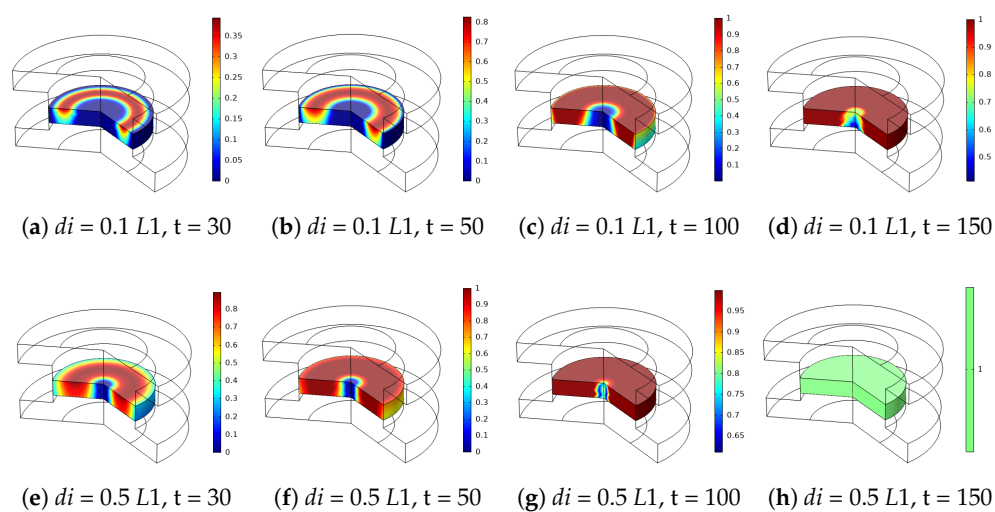


Figure 11. Distribution of time dependent liquid fraction within the cavity with varying port sizes ($Re = 300$, $Re_w = 500$, $L0 = 0.6 L1$, $yp = 0.1 H$, and $NC = 0.02$).

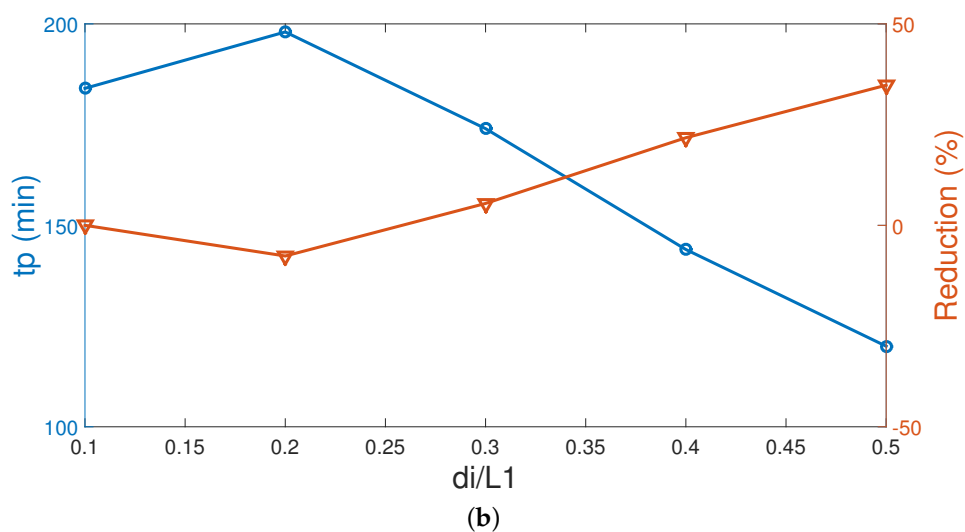
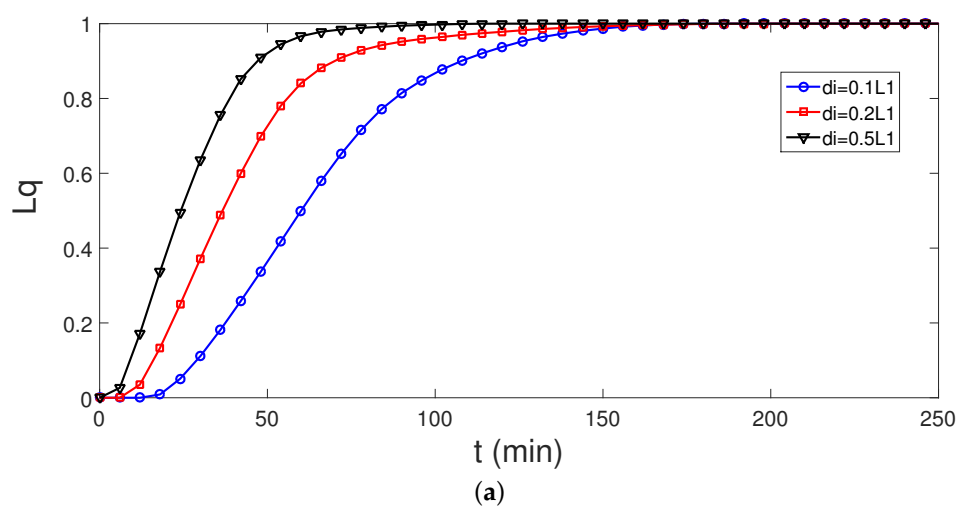


Figure 12. Impacts of port size on the time evolution of average Lq (a) and complete phase transition time (tp in minutes) (b) ($Re = 300$, $Re_w = 500$, $L0 = 0.6 L1$, $yp = 0.1 H$, and $NC = 0.02$).

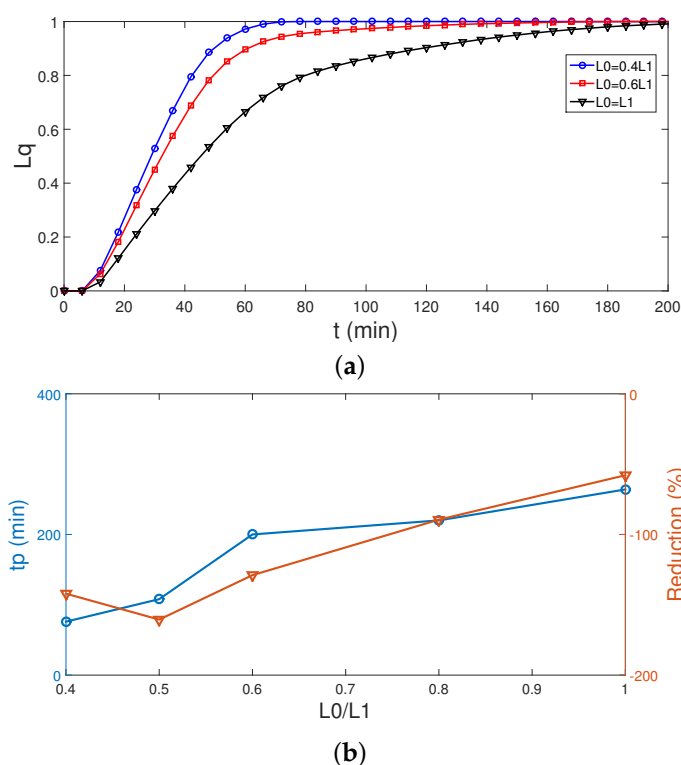


Figure 13. Effects of PCM-zone length on the time evolution of average Lq (a) and on the complete phase transition time (tp in minutes) (b) ($Re = 300$, $Re_w = 500$, $di = 0.25 L1$, $yp = 0.1 H$, and $NC = 0.02$).

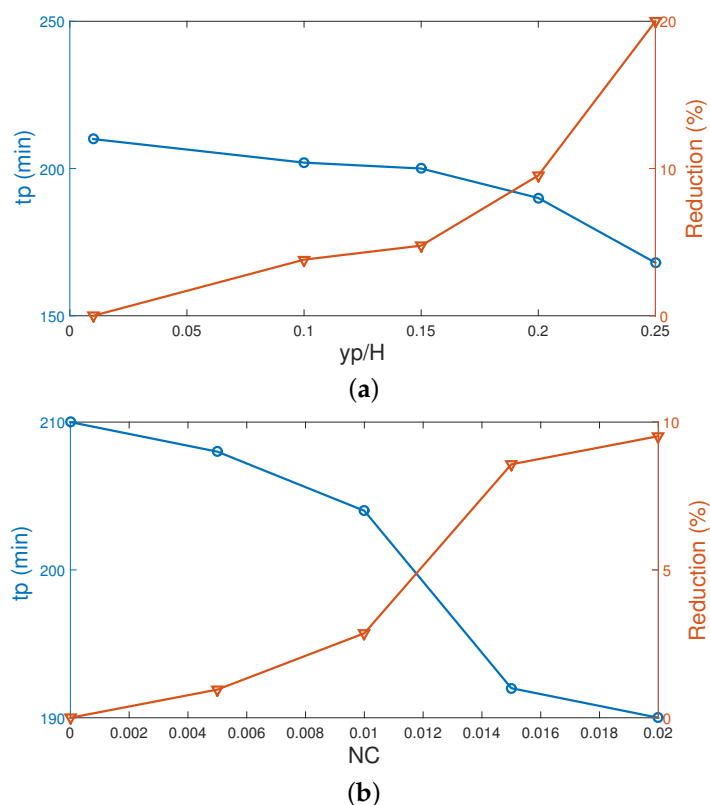


Figure 14. Impacts of PCM-zone location within the vented cavity ((a) $NC = 0.02$) and including nanoparticles in the base fluid ((b) $yp = 0.1 H$) on the complete phase transition time in minutes. Amount of reductions in the tp is also provided ($Re = 300$, $Re_w = 500$, $di = 0.25 L1$, and $L0 = 0.6 L1$).

4. Conclusions

The phase change process in a 3D complex-shaped cavity is explored under the combined effects of surface rotations and nanoparticle loading in the base fluid for a PCM-packed bed integrated system. The following conclusions are drawn as:

- The impacts of surface rotation on the phase change become effective for lower values of fluid stream Re numbers.
- At the highest rotational speed of the surface, a 39.8% and 24.5% reduction in the phase transition time (t_p) were achieved at $Re = 100$ and $Re = 500$.
- Flow recirculation, especially near the ports, are affected by the port sizes, while a larger port size accelerates the phase change process. When configurations with the smallest and largest port sizes are compared, a 34.8% reduction in t_p is obtained.
- The size and vertical location of the PCM–PB system shows opposite behavior on the phase change dynamics. When the zone is closer to the inlet port, phase change accelerates. The reduction and increment in the t_p are obtained as 20% and 58% for the largest y_p and length of the PCM zone.
- Inclusion of hybrid nanoparticles in the base HT fluid accelerates the phase transition and a t_p reduction of about 9.5% is achieved at the highest nanoparticle loading.

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Abbreviations

The following abbreviations are used in this manuscript:

d_i	port size
L_q	liquid fraction
k	thermal conductivity
H	cavity height
h_{pc}	PCM–PB height
L	radius of cylinder
L_0	PCM–PB radius
L_f	latent heat of fusion
n	unit normal vector
Nu	Nusselt number
p	pressure
Pr	Prandtl number
Re	Reynolds number
R	residual
Re_w	rotational Reynolds number
t	time
t_p	full phase transition time
T	temperature
T_m	melting temperature
u, v, w	velocity components
W	weight function
r, z	cylindrical coordinates
y_{pc}	distance of PCM–PB from lower cavity

Greek Characters

ν	kinematic viscosity
ρ	density of the fluid
κ	permeability
ε	porosity
ω	angular rotational speed

Subscripts

c	cold
h	hot
m	average
nf	nanofluid
p	solid particle

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