

Supporting Information for:

Alkali hydrolysis of sulfated cellulose nanocrystals: Optimization of reaction conditions and tailored surface charge

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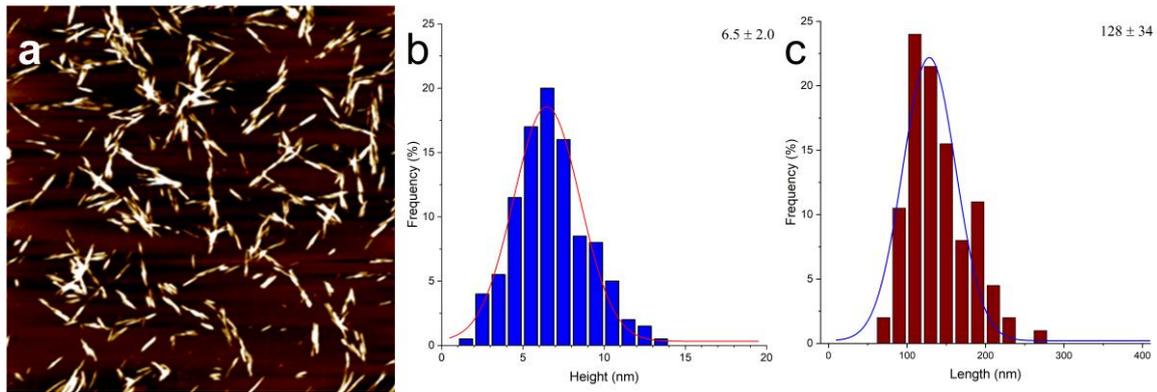


Figure S1. Characterization of CNC batch #3 used for alkali hydrolysis: (a) Representative 4 × 4 μm AFM height image of CNCs (0.01 wt%) on mica disc; (b) AFM height histogram; (c) AFM length histogram

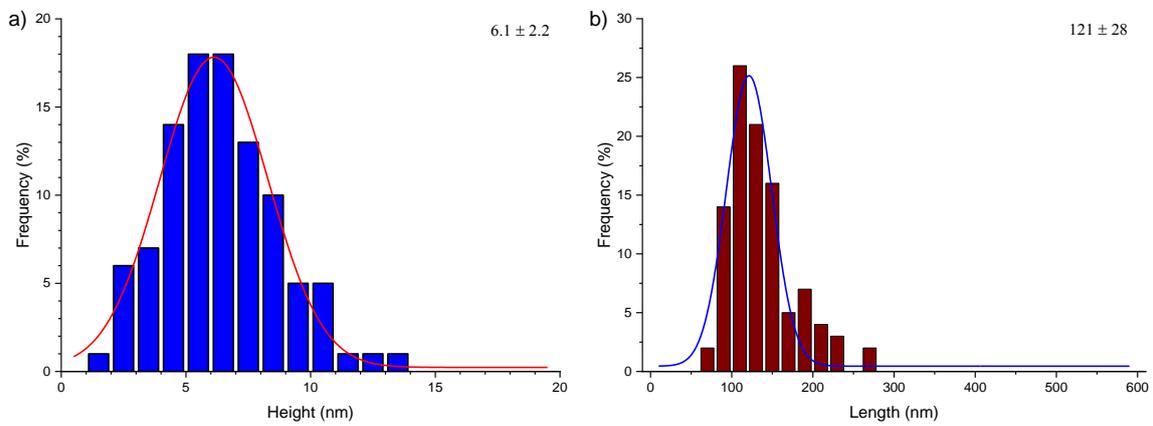


Figure S2. Characterization of CNC batch #2 used for alkali hydrolysis: (a) AFM height histogram; (b) AFM length histogram

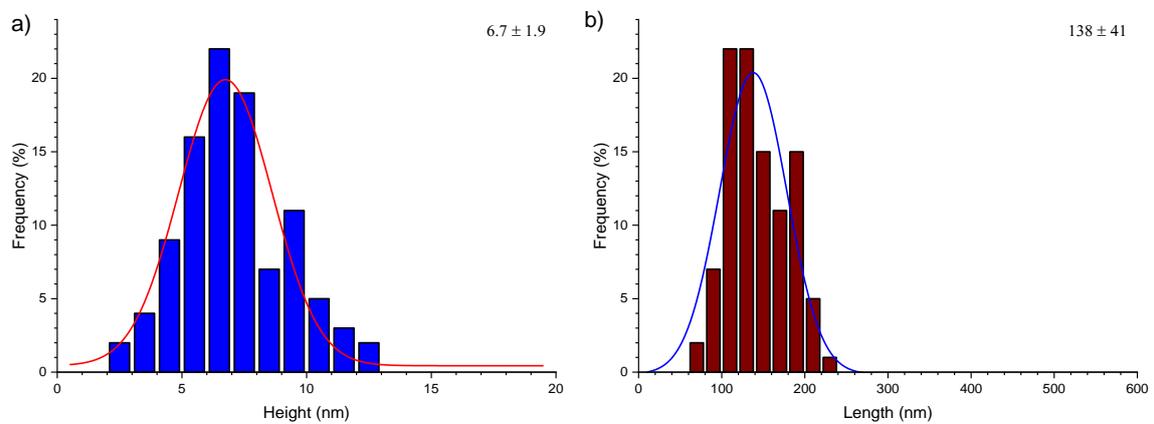


Figure S3. Characterization of CNC batch #1 used for alkali hydrolysis: (a) AFM height histogram; (b) AFM length histogram

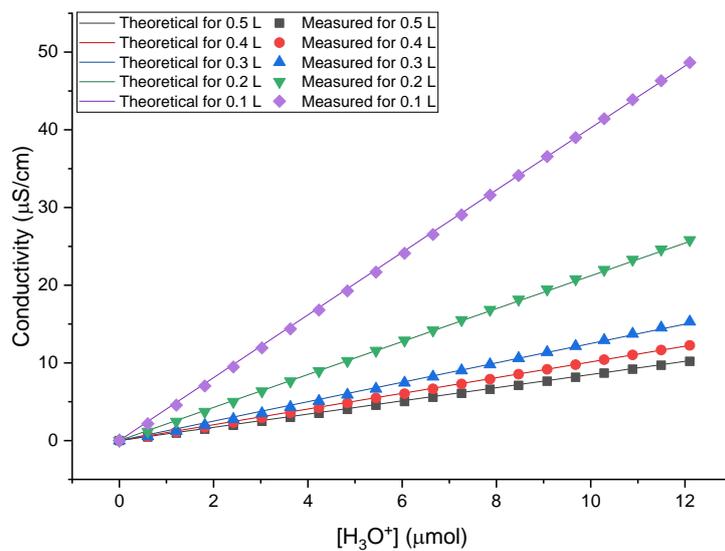


Figure S4. Effect of excess acid on measured conductivity: Measured conductivity (corrected for Cl^-) from titration of 0.01 M HCl into 0.1 (black), 0.2 (red), 0.3 (blue), 0.4 (green), or 0.5 (purple) L cells. Solid lines are the theoretical values, based on the molar conductivity of the hydronium ion (H_3O^+ , $349.6 \text{ S}\cdot\text{cm}^2\cdot\text{mol}^{-1}$)

Table S1. DOE reaction conditions and results.

exp (#)	Time (min)	Temp (°C)	[NaOH] (M)	[CNC] (wt%)	Yield (%)	-OSO ₃ ⁻ (mmol·kg ⁻¹)		Δ-OSO ₃ ⁻ (%)
						initial	final	
3	0	25	0.000	0.50	51%	211	204	3%
4	360	75	0.000	0.50	85%	197	193	2%
11	207	56	1.240	2.00	51%	211	92.8	56%
12	360	50	1.050	1.05	85%	211	61.6 [†]	69%
13	207	56	1.240	2.00	62%	211	139.5	34%
14	0	75	2.000	0.50	97%	211	203.5	4%
15	360	25	2.000	2.00	73%	211	141.4	33%
16	74	53	0.100	0.50	80%	197	130.5	34%
17	167	25	0.800	2.00	67%	197	123.0	38%
18	0	25	0.100	1.51	68%	197	186.3	5%
19	0	75	0.100	2.00	32%	197	183.0	7%
20	360	25	0.100	0.50	65%	197	142.7	28%
21	360	75	2.000	2.00	48%	211	53.3	75%
22	0	46	2.000	2.00	62%	211	156.0	26%
23	166	25	2.000	1.06	53%	211	177.7	16%
24	0	25	1.390	0.50	59%	211	206.8	2%
25	54	50	1.390	1.13	77%	211	151.8	28%
26	0	75	0.610	1.06	68%	197	148.4	25%
27	360	75	0.100	0.50	64%	197	69.7	65%
28	74	53	0.100	0.50	68%	197	131.5	33%
29	360	50	1.050	1.25	78%	197	31.2	84%
30	360	54	0.100	2.00	95%	197	85.5	57%
31	54	50	1.390	1.13	79%	211	127.4	40%
32	7	75	1.380	1.88	71%	211	109.6 [†]	48%
33	212	75	1.260	0.72	45%	211	81.5 [†]	61%
34	360	54	2.000	0.50	76%	211	59.2	72%
35	166	25	2.000	1.06	81%	211	149.6	29%
36	360	50	1.050	0.50	63%	197	80.3 [†]	62%
37	360	50	0.075	0.50	76%	197	109.1	45%
38	360	50	0.025	0.50	87%	197	170.3	14%
39	360	50	0.050	0.50	69%	197	155.6	21%
40	360	50	0.050	0.50	74%	197	147.9	25%
DOE TEST	360	60	0.130	0.78	77%	211	91.6	57%

The Δ(-OSO₃⁻) standard error for (coefficient of variation, CV) in each instance is ~5%[†] indicates error was >10%; all other error was ≤10%. ¹ The stock CNC suspensions were concentrated to ~3 wt% and diluted as necessary.

The Model F-value of 6.11 implies the model is significant. There is only a 0.02% chance that an F-value this large could occur due to noise. Values of "Prob > F" less than 0.0500 indicate significant model terms: A, B, AC, C². Values >0.10 indicate model terms are not significant (Table S2). The "Lack of Fit F-value" of 1.59 implies the Lack of Fit is not significant relative to the pure error (i.e. there is a 32% chance that the lack of fit occurred due to noise). The empirical model was tested with a confirmation run (e.g. DOE TEST) to confirm the results. Expected values were 83.2 mmol·kg⁻¹ and 61%, and results gave a Δ(-OSO₃⁻) of 57% within the standard error Δ(-OSO₃⁻) of 5% and absolute error (-OSO₃⁻ mmol·kg⁻¹ ≤ 10%).

Table S2. ANOVA for response, surface reduced quadratic model.

Analysis of variance table [Partial sum of squares - Type III]						
Source	Sum of Squares	df	Mean Square	F Value	p-value Prob > F	
Model	53455.06	10	5345.51	6.11	0.0002	<i>significant</i>
<i>A-Time</i>	28160.51	1	28160.51	32.20	< 0.0001	<i>significant</i>
<i>B-Temp</i>	8763.31	1	8763.31	10.02	0.0047	<i>significant</i>
<i>C-NaOH</i>	1148.74	1	1148.74	1.31	0.2647	
<i>D-CNC wt%</i>	792.54	1	792.54	0.91	0.3520	
<i>AC</i>	9146.78	1	9146.78	10.46	0.0040	<i>significant</i>
<i>AD</i>	1286.83	1	1286.83	1.47	0.2386	
<i>BC</i>	1713.29	1	1713.29	1.96	0.1762	
<i>CD</i>	1318.04	1	1318.04	1.51	0.2332	
<i>B²</i>	1981.96	1	1981.96	2.27	0.1471	
<i>C²</i>	6331.00	1	6331.00	7.24	0.0137	<i>significant</i>
Residual	18368.35	21	874.68			
<i>Lack of Fit</i>	15343.87	16	958.99	1.59	0.3209	<i>not significant</i>
<i>Pure Error</i>	3024.48	5	604.90			
Cor Total	71823.41	31				

Results of the DOE generated the following equation (S1) in terms of coded factors:

$$107.77 - 49.07t - 35.41T + 39.37C + 24.13w - 33.13tC - 9tw - 21.85TC + 38.95Cw + 17.01T^2 + 67.35C^2 \quad (S1)$$

Where, time (*t*), Temperature (*T*), NaOH concentration (*C*), and CNC wt% (*w*) are the input factors.

Eq. S1 in turn is used to derive an equation in terms of actual factors (Table S3) based on input values.

Table S3. Final equation ⁽¹⁾ in terms of actual factors:

sulfate remaining, ($-\text{OSO}_3^-$) =	
+256.71715	
$-5.67961\text{E}-003 \times (t)$	Time
$-3.26401 \times (T)$	Temperature
$-0.077399 \times (C)$	NaOH Molarity
$-0.13912 \times (w)$	⁽²⁾ sulfate half-ester (μmol)
$-2.00767\text{E}-004 \times T \times C$	
$-1.81883\text{E}-003 \times T \times w$	
$-8.73806\text{E}-004 \times T \times C$	
$+1.29817\text{E}-003 \times C \times w$	
$+0.027213 \times (T)^2$	
$+6.73481\text{E}-005 \times (C)^2$	

Notes: ¹The coefficients of each factor should not be used to determine their respective relative importance, since the units of each factor are not the same. ²sulfate half-ester = starting sulfate ($\text{mmol}\cdot\text{kg}^{-1}$) \times CNC wt% \times mass solution (kg) \times 1000 $\mu\text{mol}/\text{mmol}$. e.g. 2.0 wt% \times 200 $\text{mmol}\cdot\text{kg}^{-1}$ ($-\text{OSO}_3^-$) \times 0.020 kg H_2O \times 1000 = 80 μmol .

Design-Expert® Software
Sulfate

Lambda
Current = 1
Best = 1.16
Low C.I. = 0.38
High C.I. = 2.1

Recommend transform:
None
(Lambda = 1)

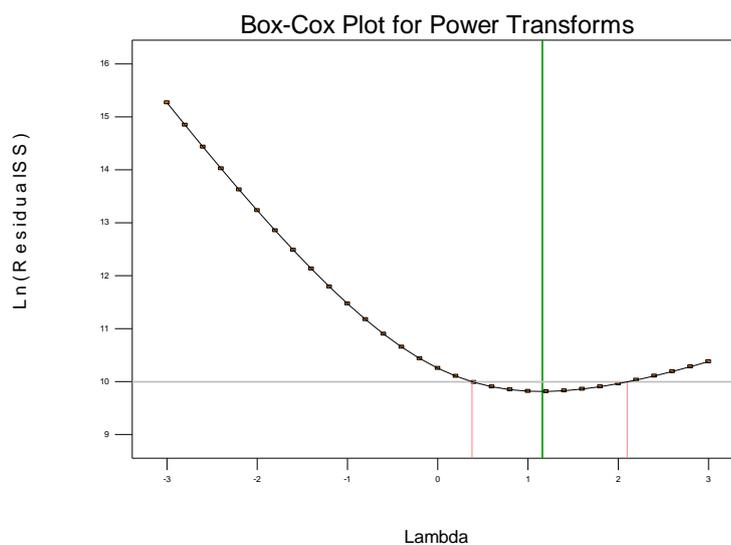


Figure S5. Box-Cox analysis of DOE results for output sulfate remaining ($\text{mmol}\cdot\text{kg}^{-1}$).

Design-Expert® Software
Sulfate

Color points by value of
Sulfate:
206.8
31.2

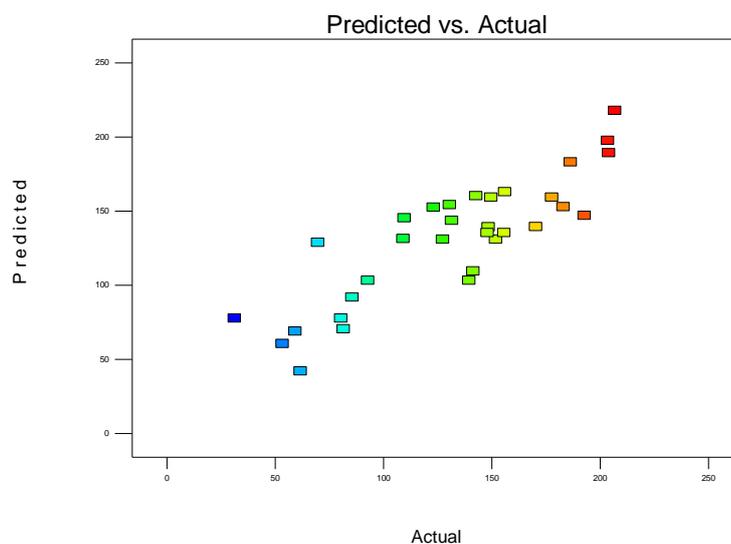


Figure S6. Predicted *vs.* experimental $-\text{OSO}_3^-$ from DOE output, sulfate remaining ($\text{mmol}\cdot\text{kg}^{-1}$).

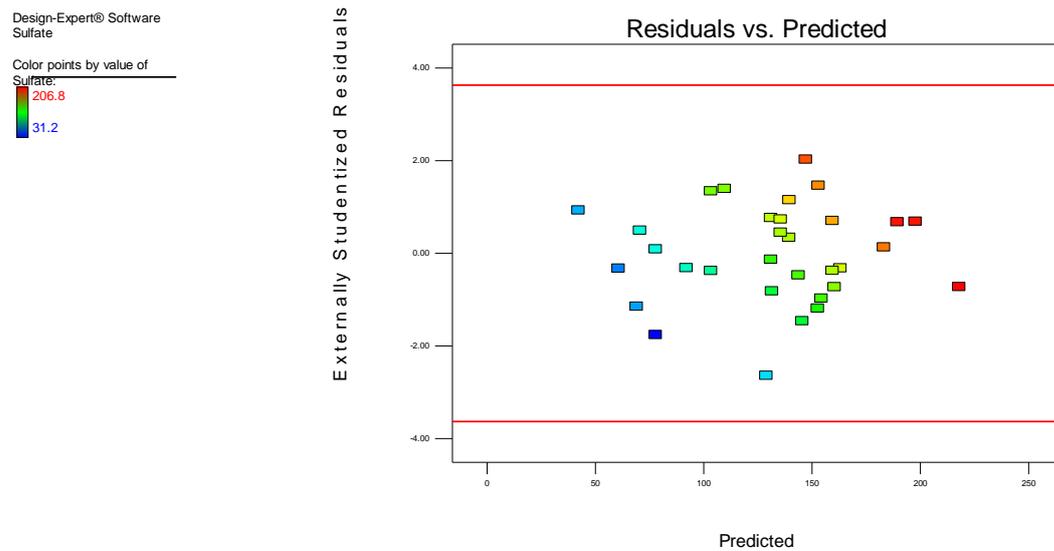


Figure S7. Residuals *vs.* predicted from DOE output, sulfate remaining ($\text{mmol}\cdot\text{kg}^{-1}$).

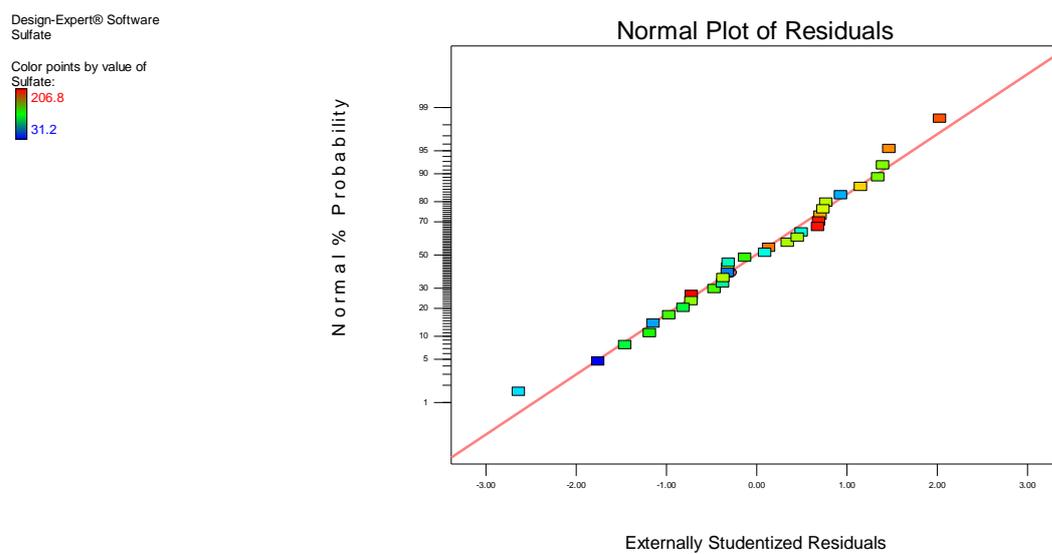


Figure S8. Normalized residuals plot showing the residuals are normally distributed

