

## Article

# Darcy Brinkman Equations for Hybrid Dusty Nanofluid Flow with Heat Transfer and Mass Transpiration

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**Abstract:** In the current work, we have investigated the flow past a semi-infinite porous solid media, after presenting a similarity transformation, governing equations mapped to a system of non-linear PDE. The flow of a dusty fluid and heat transfer through a porous medium have few applications, viz., the polymer processing unit of a geophysical, allied area, and chemical engineering plant. Further, we had the option to get an exact analytical solution for the velocity to the equation that is non-linear. The highlight of the current work is the flow of hybrid dusty nanofluid due to Darcy porous media through linear thermal radiation with the assistance of an analytical process. The hybrid dusty nanofluid has significant features improving the heat transfer process and is extensively developed in manufacturing industrial uses. It was found that the basic similarity equations admit two phases for both stretching/shrinking surfaces. The existence of computation on velocity and temperature profile is presented graphically for different estimations of various physical parameters.

**Keywords:** Darcy-Brinkman number; hybrid nanofluid; dusty fluid



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## 1. Introduction

The boundary layer flow is studied on continuous moving solid surfaces. Dusty fluid flows have become increasingly important in recent years. Petroleum transportation, wastewater treatment, combustion, and power plant piping are only a few examples. Furthermore, since crude oil is recovered from the pores of reservoir rocks, fluid flow through porous media has become a significant subject. The dusty fluid is a combination of micrometer-sized particles into a base fluid. The latest technical advances necessitate a different revolt in the field of a dusty fluid. The flow happens in numerous engineering and innovative processes. Applications over a wide range of science and design controls, particularly in the expulsion of a polymer in a dissolve turning measure; the expulsion from biting the dust is usually drawn and simultaneously reached out into a stretched sheet, and the boundary layer along with material behavior conveyors, the aerodynamic expulsion extrusion of glass blowing, paper manufacture, plastic sheets, and the boundary layer along with a fluid film are considered in the reduction method.

The desired fluid mechanical properties as a result of such a method would be primarily determined by two factors: the cooling fluid utilized and the rate of stretching. Fluids with non-Newtonian properties that are electrically leading can be used as cooling liquids because the flow and heat transfer can be controlled externally. The level of stretching is crucial because quick stretching induces rapid solidification. Regarding these applications, Sakiadis [1] first talked about boundary layer flow over an insistent, dense surface affected at a consistent speed. Crane [2] stretched out the Sakiadis concern to a stretching

sheet and originated a closed-form particular solution. From that point forward, several authors [3–10] generalized the stretching flow problem in different directions, resulting in numerous references. One way to develop the thermal conductivity of conventional coolants is to add nano-sized particles. Furthermore, the nanofluid is referred to as a combination of nano-sized particles, which dissipates extra heat because of its higher thermal conductivity, leading to better device thermal efficiency.

In view of these possibilities, the impact of mass transfer and energy properties concerning the air stream and water surface was investigated by Gu et al. [11]. The thermal conductivity and dynamic viscosity using hybrid nanofluid were calculated experimentally by Esfe et al. [12]. Mahabaleshwar et al. [13–16] extended his work with heat transfer within the sight of radiation and heat source/sink effects subsequently over the stretching sheet. Nanofluids across a stretching sheet with cross-diffusion impacts of hydromagnetics were investigated by Reddy and Chamkha [17]. Natural convection in a porous media saturated with nanofluid across a non-isothermal vertical plate investigated by Gorla and Chamkha [18]. Further, an extensive and substantial survey of hybrid nanofluids can be perused in the new analysis, see [19–22]. The equation is widely used in the study of porous media with high porosity. The effective viscosity is the dynamic viscosity that is related with the brinkman term. The magnitude of the viscosity ratio has been studied in the past with different results by Mahabaleshwar et al. [23,24]. The Darcy–Brinkman conditions validity has additionally been explored, especially when it derives solid–fluid interfaces in relation to boundary conditions at the Nield [25]. The research, which addresses the Navier–Stokes conditions instead of the Darcy equation, yields a connection concerning the permeability of the normal exhibit structure and the porosity, showing that the Darcy equation is effective for flow across normal construction across the entire porosity range. Linear stability analysis is used to investigate bio-thermal convection in suspension of gyrotactic microorganisms in a porous media using the Darcy–Brinkman model [26–30]

The main aim of this analysis is to use a proposed convergent analytical technique to examine the features of a hybrid nanofluid due to a Darcy porous medium using nonlinear thermal radiation. An effective resolution is different due to the non-linear nature as well as outline essence of the query. As a consequence, an analytical description of the proposed method is obtained. The governing PDEs are converted into nonlinear ODEs. As a result, the present research will look at the quantitative relationships concerning the wall impacts and the Darcy Brinkman equation in greater detail. To assess the association between flow and temperature, an inventory of equivalent coefficients among the movement aspects, as well as real proportions of the perception model, were calculated. The specifics are described using tables and graphs.

## 2. Physical Model and Solution

Consider the flow and heat transfer of an incompressible hybrid nanofluid due to a stretching/shrinking sheet in a two-dimensional boundary layer. The velocity of the sheets is assumed to be linear, i.e.,  $u_w(x) = cx$ , with  $c < 0$  for a shrinking sheet and  $c > 0$  for a stretching sheet. The stretching/shrinking sheet is parallel to the  $y = 0$  plane. The flow is produced because of the stretching/shrinking sheet affected by the concurrent utilizations of two equivalents and contrary forces along the  $x$ -plane (see Figure 1).

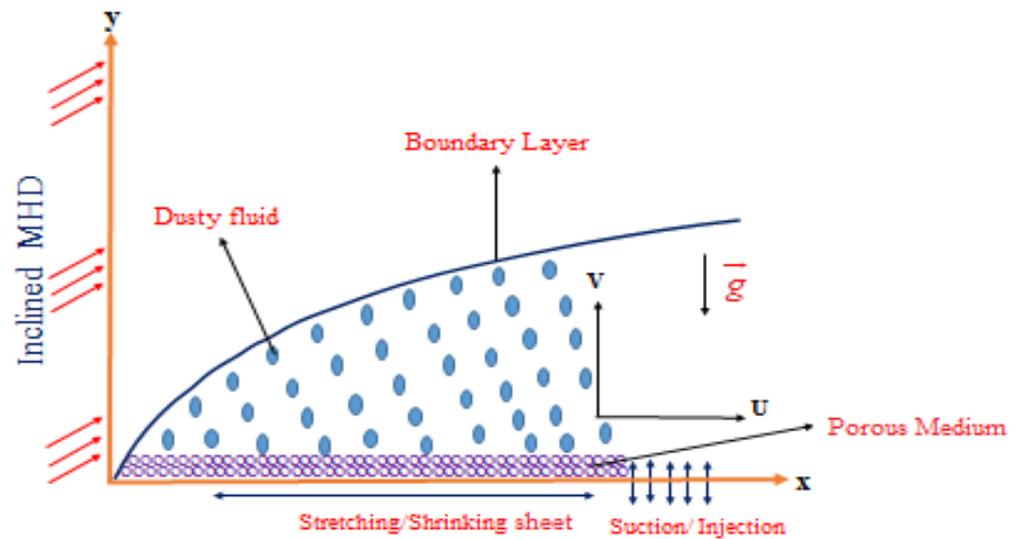


Figure 1. Physical model for stretching/shrinking boundary.

The governing equations for the boundary layer approximations are:

2.1. Fluid Phase

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \tag{1}$$

$$\frac{\rho_{hnf}}{\phi^2} \left( u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = \mu_{eff} \frac{\partial^2 u}{\partial y^2} + KN(u_p - u) - \frac{\mu_{hnf}}{k} u - \sigma_{hnf} B_0^2 \sin^2(\tau) u, \tag{2}$$

$$(\rho C_p)_{hnf} \left( u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \right) = \kappa_{hnf} \frac{\partial^2 T}{\partial y^2} + \frac{\rho_p C_m}{\tau_T} (T_p - T) + \frac{\rho_p}{\tau_v} (u_p - u)^2 - \frac{\partial q_r}{\partial y}, \tag{3}$$

2.2. Dust Phase

$$\frac{\partial u_p}{\partial x} + \frac{\partial v_p}{\partial y} = 0, \tag{4}$$

$$u_p \frac{\partial u_p}{\partial x} + v_p \frac{\partial u_p}{\partial y} = \frac{K}{m} (u - u_p), \tag{5}$$

$$\rho_p C_m \left( u_p \frac{\partial T_p}{\partial x} + v_p \frac{\partial T_p}{\partial y} \right) = \frac{\rho_p C_m}{\tau_T} (T - T_p). \tag{6}$$

where  $\mu_{eff}$  is the effective dynamic viscosity,  $K$  is the Stokes drag constant,  $N$  is the number density of dusty particle,  $B_0$  is the magnetic field,  $c_{mf}$  is the specific heat of dust particles,  $c_{pf}$  is the specific heat of fluid particles,  $l$  is the mass concentration of the particle,  $\kappa_{nf}$  is the thermal conductivity of the nanofluid,  $\mu_f$  is the limiting viscosity of fluid,  $\mu_{hnf}$  is the effective viscosity of hybrid nanofluid,  $\rho_f$  is the density of fluid fraction,  $\rho_s$  is the density of solid fraction,  $\rho_{hnf}$  is the effective density of the hybrid nanofluid, and  $\tau_v$  is the relaxation time of the dust particle.

The fluid and dust particle B.C's are given by.

$$\left. \begin{aligned} v = v_w, \quad u = u_w(x) = cx, \quad T = T_w(x) = T_\infty + bx^2 \quad \text{at } y = 0, \\ v_p \rightarrow v, \quad u \rightarrow 0, \quad u_p \rightarrow 0, \quad T_p \rightarrow T_\infty, \quad T \rightarrow T_\infty \quad \text{as } y \rightarrow \infty. \end{aligned} \right\} \tag{7}$$

The radiative heat flux is stated as follows (see Mahabaleshwar et al. [31–34]) using the Rosseland [35] approximation.

$$q_r = -\frac{4\sigma^*}{3k^*} \frac{\partial T^4}{\partial y}, \tag{8}$$

The difference of temperature expressed as linearity function in the fourth power of temperature is an assumption. The Taylor’s series expansion of the term  $T_\infty$  with the value  $T^4$  is presented as below; see Mahabaleshwar et al. [36,37]

$$T^4 = T_\infty^4 + 4T_\infty^3(T - T_\infty) + 6T_\infty^2(T - T_\infty)^2 + \dots \tag{9}$$

Ignoring higher-order terms of  $(T - T_\infty)$  in the exceeding expression absent from the first degree,  $T^4$  can be estimated by:

$$T^4 \cong -3T_\infty^4 + 4T_\infty^3 T. \tag{10}$$

By employing Equations (8) and (10) substitute in Equation (3) moderates to

$$(\rho C_p)_{hmf} \left( u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \right) = \kappa_{hmf} \left( 1 + \frac{16\sigma^* T_\infty^3}{3k^* \kappa_{nf}} \right) \frac{\partial^2 T}{\partial y^2} + \frac{\rho_p C_m}{\tau_T} (T_p - T) + \frac{\rho_p}{\tau_v} (u_p - u)^2. \tag{11}$$

Here, the Stefan–Boltzmann constant is  $\sigma^*$ , the absorption coefficient is  $k^*$ , and radiative heat flux is  $q_r$ . The following is the term for the hybrid nanofluid density, viscosity, thermal conductivity, and specific heat. Anusha et al. [26]

$$\left. \begin{aligned} \frac{\mu_{hmf}}{\mu_f} &= \frac{1}{(1-\varphi_1)^{2.5}(1-\varphi_2)^{2.5}} \\ \frac{\rho_{hmf}}{\rho_f} &= (1-\varphi_2) \left( 1 - \varphi_1 + \varphi_1 \frac{\rho_{s1}}{\rho_f} \right) + \varphi_2 \left( \frac{\rho_{s2}}{\rho_f} \right) \\ \frac{(\rho C_p)_{hmf}}{(\rho C_p)_f} &= (1-\varphi_2) \left( 1 - \varphi_1 + \varphi_1 \frac{(\rho C_p)_{s1}}{(\rho C_p)_f} \right) + \varphi_2 \frac{(\rho C_p)_{s2}}{(\rho C_p)_f}, \\ \frac{\sigma_{hmf}}{\sigma_f} &= \frac{\sigma_{s2} + 2\sigma_{bf} + 2\varphi_2(\sigma_{s2} - \sigma_f)}{\sigma_{s2} + 2\sigma_{bf} - \varphi_2(\sigma_{s2} - \sigma_f)} \quad \text{where } \sigma_{bf} = \sigma_f \frac{\sigma_{s1} + 2\sigma_f + 2\varphi_1(\sigma_{s1} - \sigma_f)}{\sigma_{s1} + 2\sigma_f - \varphi_1(\sigma_{s1} - \sigma_f)} \\ \frac{\kappa_{hmf}}{\kappa_f} &= \frac{\kappa_{s2} + 2\kappa_{bf} + 2\varphi_2(\kappa_{s2} - \kappa_f)}{\kappa_{s2} + 2\kappa_{bf} - \varphi_2(\kappa_{s2} - \kappa_f)} \quad \text{where } \kappa_{bf} = \kappa_f \frac{\kappa_{s1} + 2\kappa_f + 2\varphi_1(\kappa_{s1} - \kappa_f)}{\kappa_{s1} + 2\kappa_f - \varphi_1(\kappa_{s1} - \kappa_f)}. \end{aligned} \right\} \tag{12}$$

The following are the reduced equations obtained using the similarity transformation:

$$\eta = y \left[ \frac{|c|}{\nu_f} \right]^{\frac{1}{2}}, \quad u = |c| x f_\eta(\eta), \quad u_p = |c| x F_\eta(\eta), \quad v = -\sqrt{|c| \nu_f} f(\eta), \tag{13}$$

$$v_p = -\sqrt{|c| \nu_f} F(\eta), \quad \theta(\eta) = \frac{T - T_\infty}{T_w - T_\infty}, \quad \Theta(\eta) = \frac{T_p - T_\infty}{T_w - T_\infty}.$$

As a consequence,  $v_w = -\sqrt{|c| \nu_f} V_c$  is the wall mass transfer velocity. The governing equations of motion are then reduced to form.

### 2.3. Fluid Phase

$$\Delta f_{\eta\eta\eta}(\eta) + \varepsilon_2(\phi) f_{\eta\eta} f - \varepsilon_2(\phi) f_\eta^2 + l\beta(F_\eta - f_\eta) - \varepsilon_3(\phi) Q \text{Sin}^2(\tau) f_\eta - \varepsilon_1(\phi) \Omega f_\eta = 0, \tag{14}$$

$$\left( \varepsilon_5(\phi) + \frac{4}{3} Rd \right) \theta_{\eta\eta} + (Pr \varepsilon_4(\phi)) (f\theta_\eta - 2f_\eta\theta) + l\gamma Pr \beta_T (\Theta - \theta) + l\beta_v Pr Ec (F_\eta - f_\eta) = 0 \tag{15}$$

### 2.4. Dust Phase

$$F_\eta^2 - FF_\eta + \beta_v (F_\eta - f_\eta) = 0, \tag{16}$$

$$2F_\eta\Theta - F\Theta_\eta + \beta_T(\Theta - \theta) = 0. \tag{17}$$

here

$$\varepsilon_1(\phi) = \frac{\mu_{hnf}}{\mu_f} = \frac{1}{(1 - \phi_1)^{2.5}(1 - \phi_2)^{2.5}},$$

$$\varepsilon_1(\phi) = \frac{\mu_{hnf}}{\mu_f} = \frac{1}{(1 - \phi_1)^{2.5}(1 - \phi_2)^{2.5}},$$

$$\varepsilon_2(\phi) = \frac{\rho_{hnf}}{\rho_f} = (1 - \phi_2) \left( 1 - \phi_1 + \phi_1 \frac{\rho_{s1}}{\rho_f} \right) + \phi_2 \left( \frac{\rho_{s2}}{\rho_f} \right),$$

$$\varepsilon_3(\phi) = \frac{\sigma_{hnf}}{\sigma_f} = \frac{\sigma_{s2} + 2\sigma_{bf} + 2\phi_2(\sigma_{s2} - \sigma_f)}{\sigma_{s2} + 2\sigma_{bf} - \phi_2(\sigma_{s2} - \sigma_f)}$$

where

$$\sigma_{bf} = \sigma_f \frac{\sigma_{s1} + 2\sigma_f + 2\phi_1(\sigma_{s1} - \sigma_f)}{\sigma_{s1} + 2\sigma_f - \phi_1(\sigma_{s1} - \sigma_f)}$$

$$\varepsilon_4(\phi) = \frac{(\rho C_p)_{hnf}}{(\rho C_p)_f} = (1 - \phi_2) \left( 1 - \phi_1 + \phi_1 \frac{(\rho C_p)_{s1}}{(\rho C_p)_f} \right) + \phi_2 \frac{(\rho C_p)_{s2}}{(\rho C_p)_f},$$

$$\varepsilon_5(\phi) = \frac{\kappa_{hnf}}{\kappa_f} = \frac{\kappa_{s2} + 2\kappa_{bf} + 2\phi_2(\kappa_{s2} - \kappa_f)}{\kappa_{s2} + 2\kappa_{bf} - \phi_2(\kappa_{s2} - \kappa_f)}$$

where

$$\kappa_{bf} = \kappa_f \frac{\kappa_{s1} + 2\kappa_f + 2\phi_1(\kappa_{s1} - \kappa_f)}{\kappa_{s1} + 2\kappa_f - \phi_1(\kappa_{s1} - \kappa_f)}.$$

The comparative reduced boundary constraints will take the accompanying structure,

$$\left. \begin{aligned} f = V_c, \quad f_\eta = D, \quad \theta = 1 & \quad \text{at } \eta = 0, \\ f_\eta \rightarrow 0, \quad F_\eta \rightarrow 0, \quad F = f, \quad \theta \rightarrow 0, \quad \Theta \rightarrow 0 & \quad \text{as } \eta \rightarrow \infty. \end{aligned} \right\} \tag{18}$$

Chandrasekhar’s number is  $Q = \frac{\sigma_f B_0^2}{\rho_f |c|}$ ; the density of the particle phase stands for the  $\rho_p = Nm$ ; the mass concentration of the dusty particle is  $l = \frac{\rho_p}{\rho}$ ; the Prandtl number is  $Pr = \frac{v_f(\rho C_p)_f}{\kappa_f}$ ; the mass transfer strength at the sheet, as determined by the wall mass transfer parameter, is  $V_c$ ; the specific heat parameter is  $\gamma = \frac{c_m}{c_p}$ ; the velocity fluid particle interaction parameter is  $\beta_v = \frac{1}{|c|\tau_v}$ ; and the temperature’s fluid-interaction parameter is  $\beta_T = \frac{1}{|c|\tau_T}$ , the Eckert number is  $Ec = \frac{c^2}{bc_p}$ . Furthermore,  $D$  is set to such an extent that  $D = 1$  represents the stretching sheet and  $D = -1$  represents the shrinking sheet.

### 3. Fluid and Dust Phase Flow Fields

The highlights of the solution’s boundary layer estimate are recovered by the accurate solution of exponential form.

$$f(\eta) = V_c + D \frac{1 - \exp[-\lambda\eta]}{\lambda}, \quad F(\eta) = V_c + D \frac{1 - \alpha \exp[-\lambda\eta]}{\lambda}, \tag{19}$$

where  $\lambda$  must be strictly positive to match the physical boundary conditions in (18); for  $\alpha$ , which describes the stretching velocity of dust particles, no such restriction is needed. Both  $\lambda$  and  $\alpha$  are real numbers, and at this phase they are unknown. It is easy to demonstrate that the exact solutions satisfy all of the boundary conditions in (18) and (19). The following

step is to satisfy the fluid and dust momentum equations given in (14). As a consequence, the fluid phase’s momentum equation yields the following relation.

$$\begin{aligned}
 &-\Lambda V_c \lambda^3 + (\varepsilon_2(\phi) V_c^2 - \Lambda \beta - \Lambda D) \lambda^2 + \\
 &(2\varepsilon_2(\phi) V_c D + \varepsilon_2(\phi) V_c \beta + \Gamma_1(\phi) V_c \Omega + IV_c \beta + \varepsilon_3(\phi) Q \sin^2(\tau) V) \lambda \\
 &+ \varepsilon_2(\phi) D + \varepsilon_2(\phi) V_c D \beta + \varepsilon_3(\phi) Q \sin^2(\tau) + \varepsilon_3(\phi) Q \sin^2(\tau) \beta \\
 &+ \Gamma_1(\phi) D \Omega + \Gamma_1(\phi) \beta \Omega + L \beta D = 0.
 \end{aligned} \tag{20}$$

Solutions are determined by using the cubic formula

$$\lambda = -\frac{B}{3A} - \frac{2^{\frac{1}{3}}(-B - 3AC)}{(3AR)} + \frac{1}{3 \times 2^{\frac{1}{3}}A} R$$

$$\begin{aligned}
 A &= \Lambda V_c, \quad B = \varepsilon_2(\phi) V_c^2 - \Lambda \beta - \Lambda D, \\
 C &= 2\varepsilon_2(\phi) V_c D + \varepsilon_2(\phi) V_c \beta + \Gamma_1(\phi) V_c \Omega + IV_c \beta + \varepsilon_3(\phi) Q \sin^2(\tau) V_c, \\
 E &= \varepsilon_2(\phi) D + \varepsilon_2(\phi) V_c D \beta + \varepsilon_3(\phi) Q \sin^2(\tau) + \varepsilon_3(\phi) Q \sin^2(\tau) \beta \\
 &\quad + \Gamma_1(\phi) D \Omega + \Gamma_1(\phi) \beta \Omega + L \beta D,
 \end{aligned}$$

$$R = \left[ -2B^3 - 27A^2E - 9ABC - \sqrt{4(-B^2 - 3AC)^2 - (-2B^3 - 27A^2E - 9ABC)^2} \right]^{\frac{1}{3}}.$$

When substituting Equation (19) into Equation (16), the momentum equation for the dust phase is obtained, this is as follows:

$$\beta_v - (D + \beta_v + V_c \lambda) \alpha = 0. \tag{21}$$

When Equation (21) is substituted for  $\alpha$ ,

$$\alpha = \frac{\beta_v}{D + \beta_v + V_c \lambda} \tag{22}$$

Furthermore, once the values of  $\lambda$  and  $\alpha$  have been determined, the wall shears can be conveniently measured using the formulations:

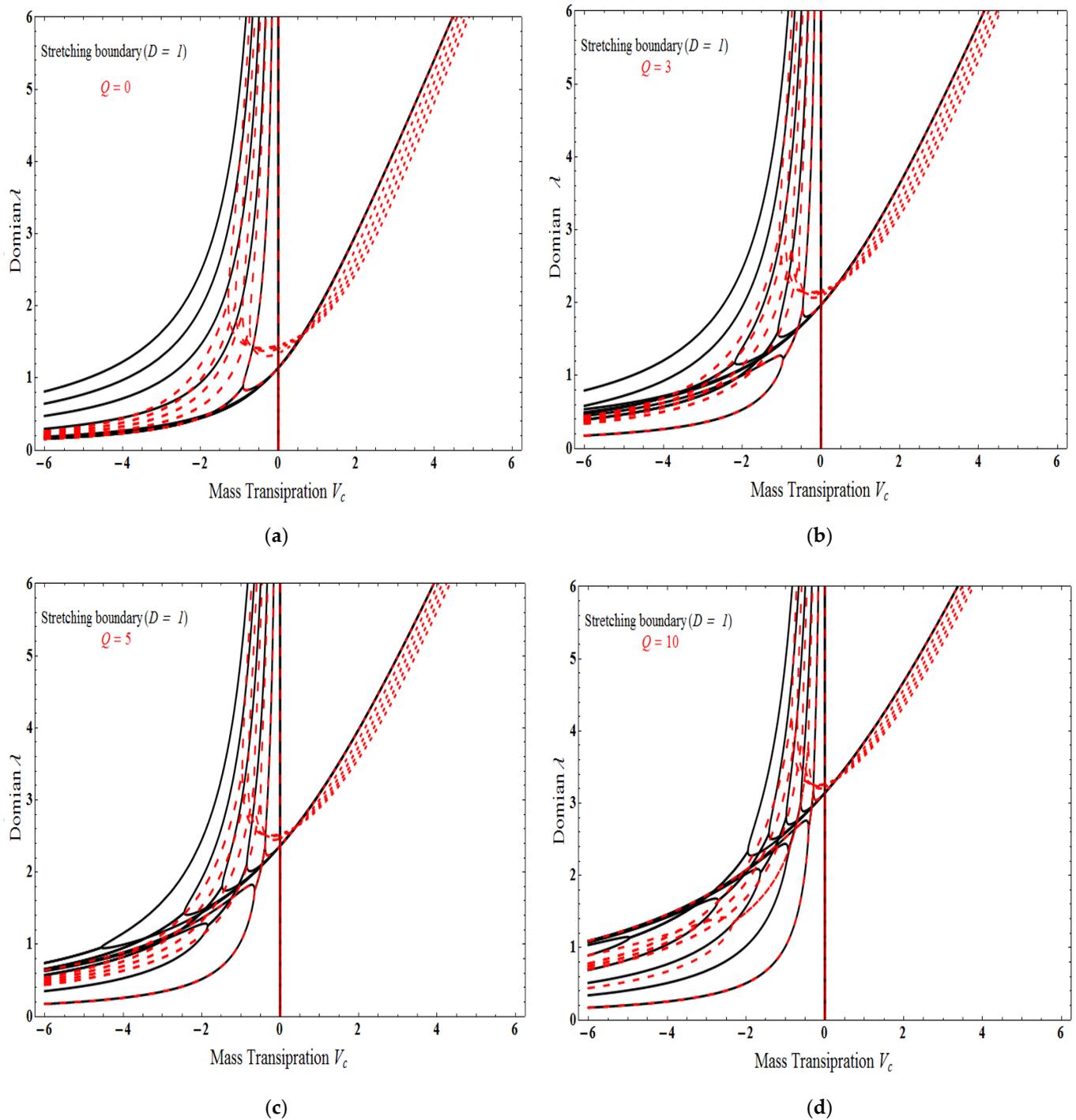
$$f_{\eta\eta}(0) = -D \lambda, \quad F_{\eta\eta}(0) = -D \alpha \lambda. \tag{23}$$

#### 4. Results and Discussion

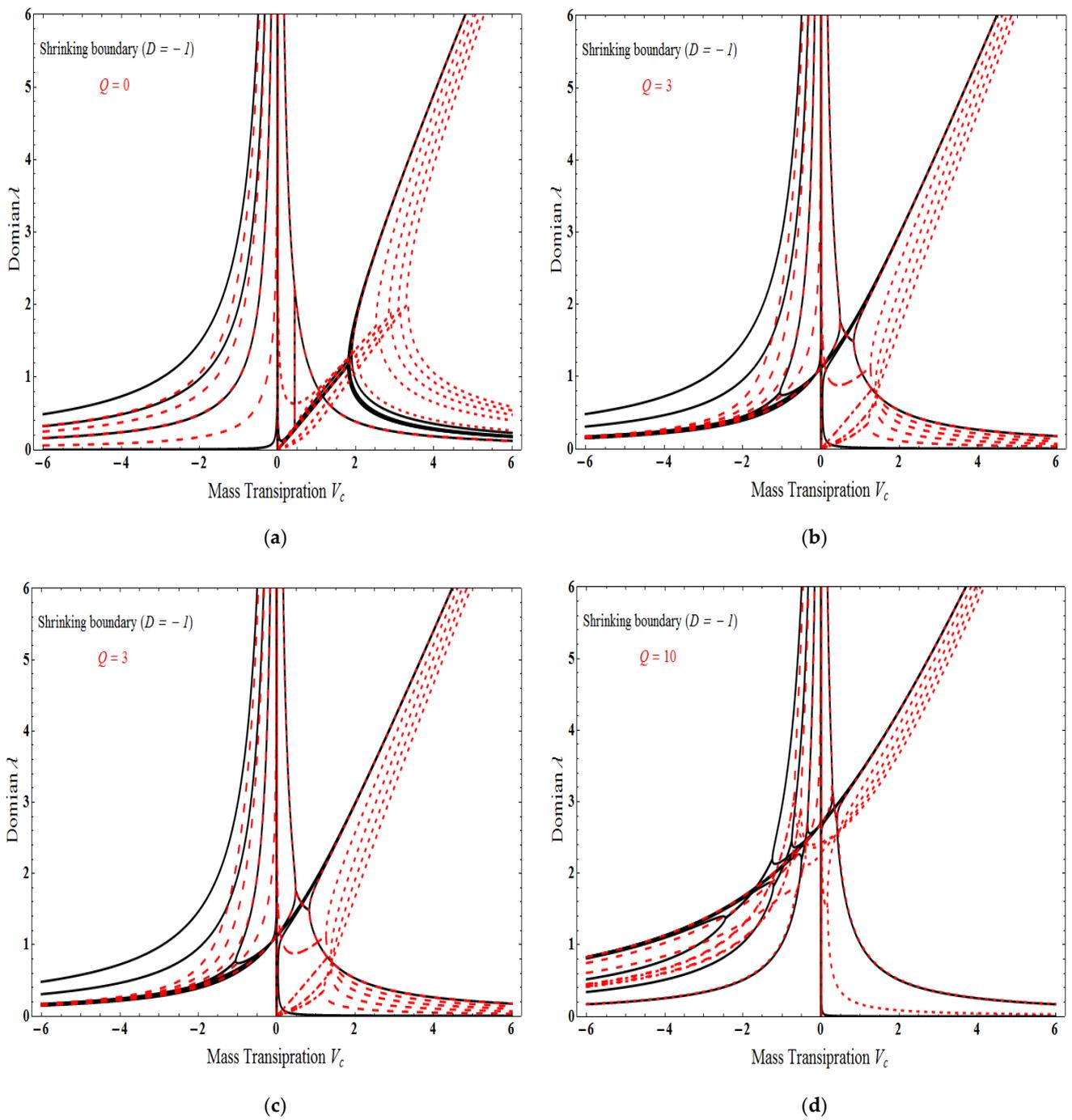
The flow of the unique/numerous two-phase dust fluid and temperature solutions due to a stretching/shrinking sheet with the effect of a heat source and heat sink is investigated in the current work. The current segment’s main aim is to investigate the graphical effects of different relevant constraints to temperature profiles and velocity for two distinctive nano fluids. The presence of mass flow transfer constraint is represented by  $V_c$ , the Eckert number is  $Ec$ , particle parameter is  $l$ ,  $\Omega$  is the Darcy porous medium,  $\beta_v$  is the interface parameter for velocity,  $Pr$  is the Prandtl number,  $\gamma$  is the specific heat parameter,  $\Lambda$  is the Brinkmann ratio, the fluid particle interaction parameter of temperature is  $\beta_T$ , and Chandrasekhar’s number is  $Q$ .

Figure 2a–d demonstrates the solution domain  $\lambda$  versus mass transpiration  $V_c$  for the varying fluid particle interaction parameter  $\beta_v$ , when considering the stretching surface with  $l = 0$  and  $l = 1$  for different values of the Chandrasekhar’s number  $Q$ . The solution domain  $\lambda$  is a monotonically increasing function of mass transpiration  $V_c$ . Figure 3a–d portrays the solution domain  $\lambda$  as function of mass transpiration  $V_c$  in the case of a shrinking surface. For different values of the Chandrasekhar’s number  $Q$ ,  $l = 0$  and  $l = 1$  for the differing interaction parameter  $\beta_v$ . The estimations of  $\lambda$  consistent with velocities are monotonically increasing, though the wall suction velocities show both increase and decrease. Figure 4 describes the impact of the stretching sheet on the velocity profile of both nanofluid and dust phases. The physical velocity field of hybrid nanofluid and dust phase will be reduced as the thickness of the momentum boundary layer is also condensed,

for the mass flow suction case; there is only a unique solution exit. Figure 5a,b displays the transverse velocity for both two levels in USB. The figure shows that in branch 1, the velocity of the hybrid nanofluid phase is more than the dusty phase, and in branch 2, the velocity of the hybrid nanofluid phase is less than the dusty phase. Chandrasekhar's number  $Q$  increases as the velocity profile decreases.



**Figure 2.** Influence of domain  $\lambda$  versus mass transpiration  $V_c$  for the varying fluid particle interaction parameter  $\beta_v = 0, 1, 2, 3, 4$ . Chandrasekhar's number is (a)  $Q = 0$ , (b)  $Q = 3$ , (c)  $Q = 5$ , and (d)  $Q = 10$  with  $\Omega = 0.1$ .



**Figure 3.** Influence of domain  $\lambda$  versus mass transpiration  $V_c$  for several values  $\beta_v = 0, 1, 2, 3, 4$ . Chandrasekhar's number is (a)  $Q = 0$ , (b)  $Q = 3$ , (c)  $Q = 5$ , and (d)  $Q = 10$  with  $\Omega = 0.1$ .

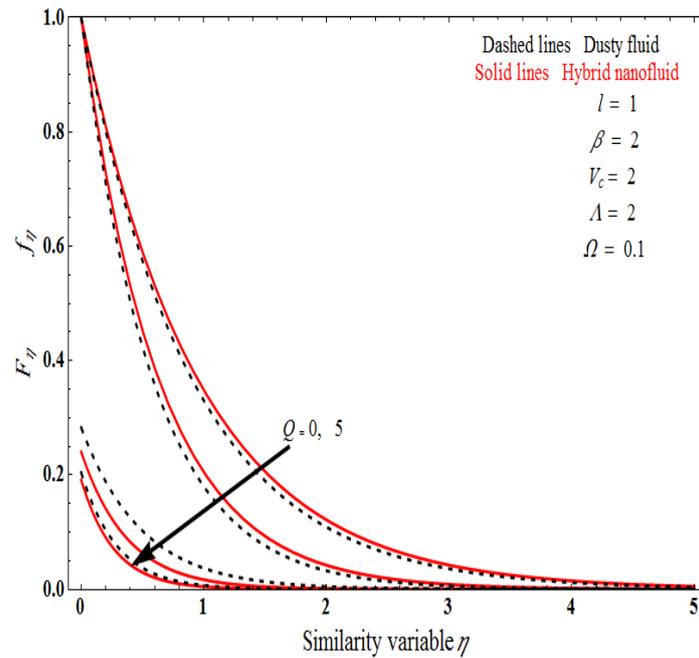


Figure 4. Influence of fluid velocity  $f_\eta$  and particle velocity  $F_\eta$  for the stretching surface.

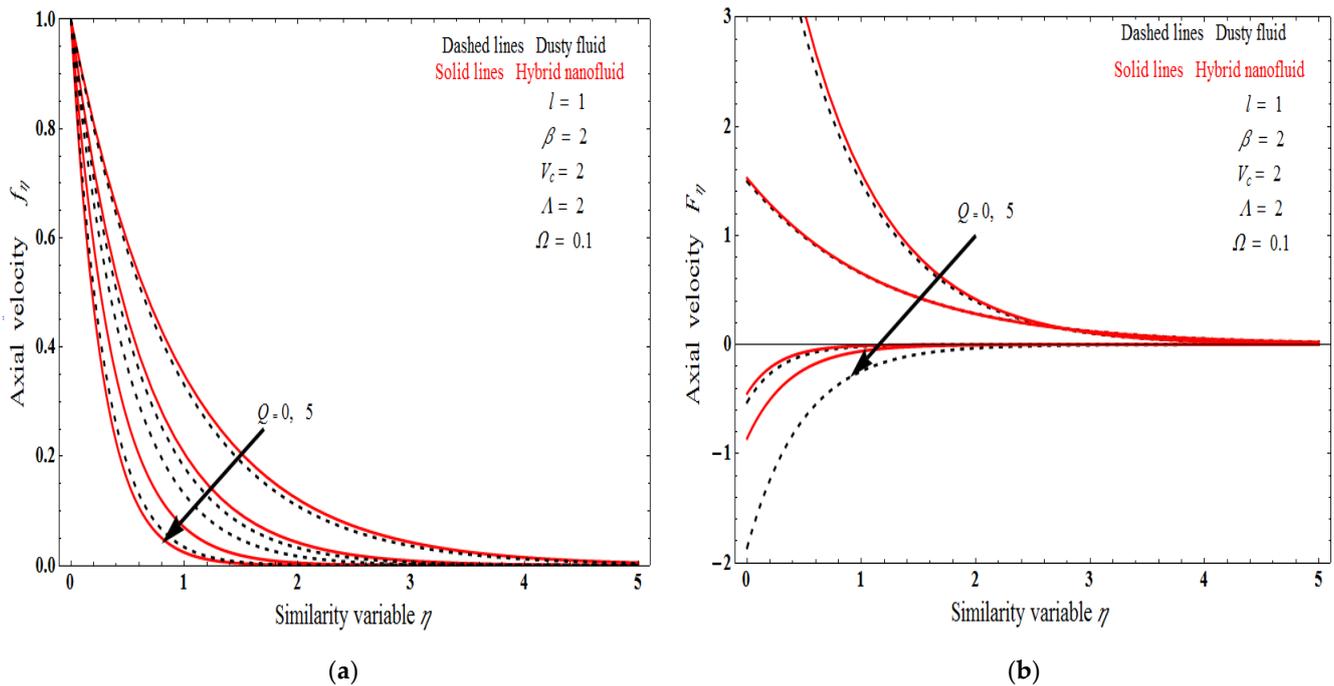
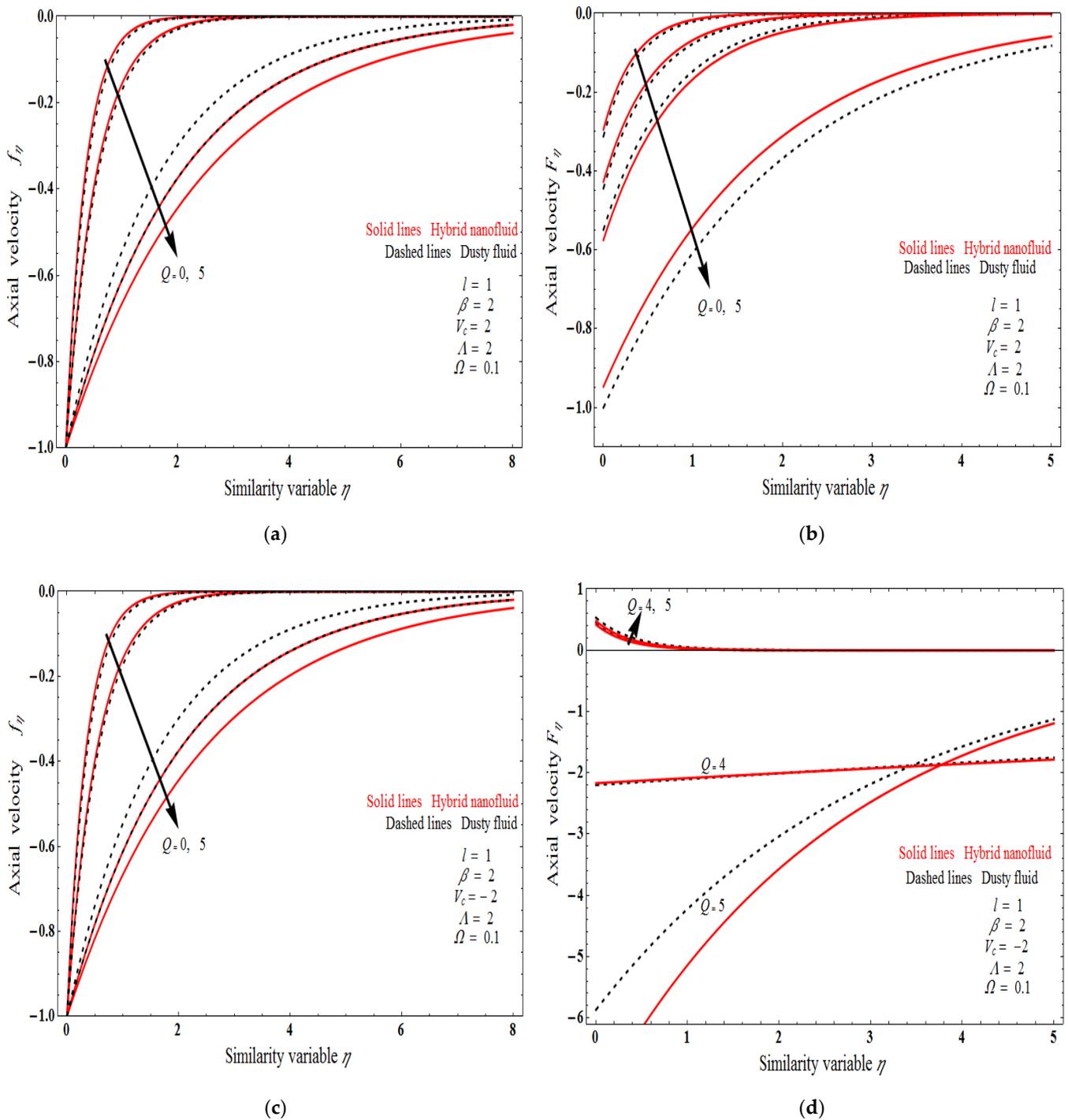


Figure 5. Influence of fluid velocity (a)  $f_\eta$  and (b)  $F_\eta$  particle velocity for the stretching surface with dual solution.

Figure 6a–d depicts the impact of the stretching sheet on the velocity profile of both fluid and dust fluid. The suction case is illustrated in Figure 6a,b; it is demonstrated that as the suction increases, the velocity profiles of fluid and dust fluid increase. The injection case is shown in Figure 7c,d; as the injection value increases the fluid and dust phases of the velocity profile increase. However, as the injection value increases, the opposite behavior occurs. Subsequently, the magnetic field performances decrease the boundary layer development because of expanding the Lorentz force; the physical validity of this behavior is disputed. Figure 7 portrays the velocity profile under different values of Brinkman numeral; it is observed that Brinkman number increments as velocity profiles are

also increased. Figure 8 represents the effect of Darcy number exhibits for both fluid and dusty nanofluids. It is revealed that as the Darcy number  $\Omega$  increases, the hybrid nanofluid decreases. Since the porosity parameter increases in velocity, as a result, the boundary layer thickness is reduced.



**Figure 6.** Influence of fluid velocity  $f_\eta$  and particle velocity  $F_\eta$  for the Shrinking surface: (a)  $f_\eta$  for suction case, (b)  $F_\eta$  for suction case, (c)  $f_\eta$  for injection case and (d)  $F_\eta$  for injection case.

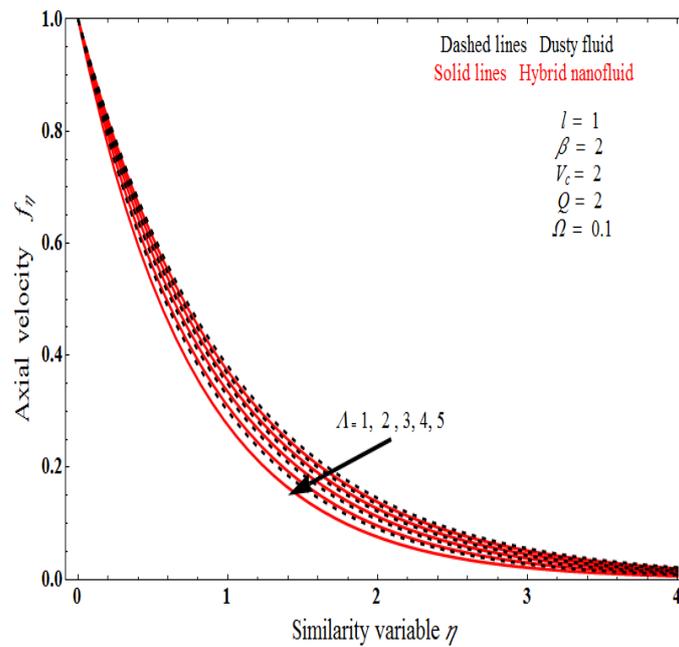


Figure 7. The impact of velocity profile on Brinkman number  $\Lambda$ .

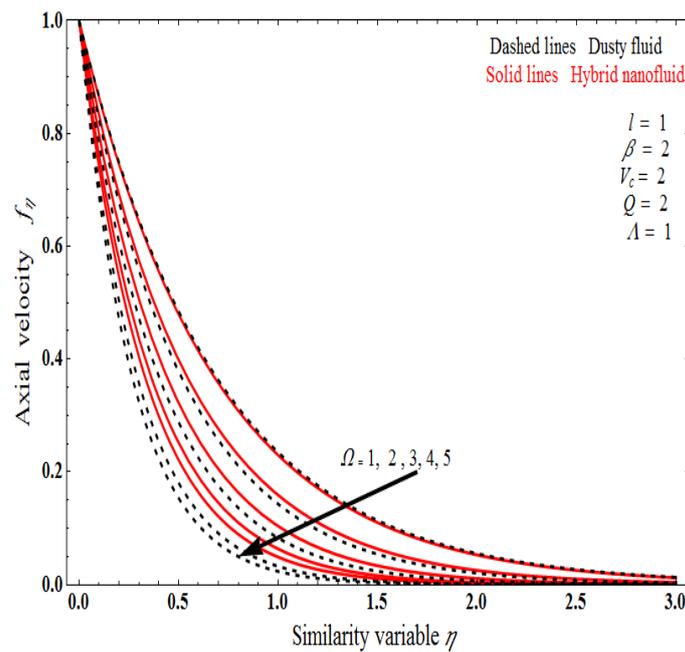


Figure 8. Impact of Darcy number  $\Omega$  on velocity profile.

### 5. Conclusions

In this analytical study, the energy and transfer of momentum of an MHD flow of a hybrid dusty fluid due to a stretching/shrinking sheet are investigated; a set of nonlinear ODEs is attained after applying the appropriate similarity transformations. Also, Darcy–Brinkman ratio and radiation were taken into account and were solved with an analytical method.

- Darcy–Brinkman ratio and radiation were taken into account and were solved by analytical method.
- The velocity profile for two phases reduces when Darcy’s number increases.
- As the Brinkman number increases, the thickness of the momentum boundary layer increases.

- The set of physical parameters under consideration determines if branch 1 or branch 2 arrangements are cooler, which would be important through the cooling method.

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### Nomenclature

Symbols	Descriptions	S. I. Units
$B_0$	Magnetic field	(Tesla)
$d$	stretching/shrinking constant	$(wm^{-2})$
$k$	thermal conductivity	$(m^2s^{-1})$
$k^*$	absorption constant	$(m^{-2})$
$M$	magnetic parameter	$(w S Kg^{-1})$
$N$	density number	(-)
$P$	pressure	(-)
$P$	dimensionless pressure	(-)
$T$	temperature	(K)
$V_w$	mass flux	$(ms^{-1})$
$V_c$	suction/injection velocity	(-)
$V_c > 0$	suction velocity	(-)
$V_c < 0$	injection velocity	(-)
$u, v$	velocities	$(m s^{-1})$
<b>Greek letters</b>		
$\alpha$	constant	(-)
$\beta_v$	interaction parameter	(-)
$\beta_T$	Fluid particle for temperature	(-)
$\Lambda$	Brinkmann ratio	(-)
$\Omega$	Darcy model	(-)
$\mu_f$	limiting viscosity of fluid	(-)
$\mu_{eff}$	effective dynamic viscosity	$(N s m^{-2})$
$\eta$	similarity variable	(-)
$\sigma$	electrical conductivity	$(S m^{-1})$
$\sigma^*$	Stefan-Boltzmann	$(Wm^{-2}K^{-4})$
$\tau$	inclined angle	(-)
$\tau_v$	relaxation time	(-)
<b>Subscript</b>		
$S_1$	density of solid fraction of hybrid nanofluid	
$S_2$	density of solid fraction of hybrid nanofluid	
$P$	solid particles	
$w$	wall temperature	
$\infty$	ambient fluid	
$f$	parameter of base fluid	
$hmf$	parameter of hybrid nanofluid	

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