

## Article

# Optimization of Cyanidin-3-O-galactoside Production from *Aronia melanocarpa* Elliot from Nonthermal Ultrasonic Extraction Process by Response Surface Methodology

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Received: 25 February 2019; Accepted: 19 March 2019; Published: 21 March 2019



**Abstract:** As a nonthermal process, ultrasonic extraction was optimized to obtain 13.21 mg/g of highly bioactive but extremely heat-sensitive cyanidin-3-O-galactoside (C3G) from *Aronia melanocarpa* Elliot under the following conditions; 75 kHz input frequency, 18.8 °C for the temperature, and 6.0 h process time. This yield was higher than 10.01 mg/g from a conventional juice extraction and was also higher than those from other reported sources. This concentration was proved to be very close to the predicted value of 13.70 mg/g from the quadratic model, with a regression coefficient of 0.969. This model also showed highly significant effects from changing frequency and time, and less significant effects from changing temperature. The extract from the optimized process showed 89.5% of higher DPPH radical scavenging activity than 71.3% from the conventional process. It was also found that the antioxidant activity of the extract was higher than that of using 13 µg/mL of C3G alone, possibly due to the synergistic effects of C3G with the other bioactive substances in the extract. Therefore, this optimized nonthermal process will be applied to obtain fairly high amounts of a thermally unstable and expensive C3G with fewer purification steps.

**Keywords:** *Aronia melanocarpa*; optimized ultrasonic extraction; cyanidine-3-O-galatoside

## 1. Introduction

Various cultivars of *Aronia melanocarpa* (Aronia), the so-called black chokeberry, have been cultivated and consumed all around the world, as this plant contains high amounts of anthocyanins, which have various biological activities such as anti-inflammation, anticancer, immunomodulation, and antiaging abilities, due to the strong antioxidant activities of these compounds [1–3]. In particular, Eastern European countries like Poland have produced substantial amounts of aronia fruits and consumed them with various types of by-products, such as aronia extract in the forms of functional juices and cordial liqueurs, fruit powders, and teas from its leaves [4,5]. Among various anthocyanins, cyanidin-3-O-galactoside (C3G) has the highest concentration in aronia, followed by cyanidin-3-O-glucoside, cyanidin-3-O-arabinoside, and other phenolic compounds, in the ranges of 0.5% (w/w) to 2.5% (w/w) depending on the varieties, culture conditions, etc. [6,7]. Aronia has been studied to utilize the efficacies of C3G and other anthocyanins in the fields of functional foods, cosmetics, medicines and other bioindustries [8–10]. However, because most anthocyanins found in nature, including C3G, are extremely unstable and particularly heat-sensitive, the application of extracting C3G from aronia has been greatly restricted. Moreover, due to the ease in damaging C3G during the purification process, this process requires several additional steps that are labor-intensive and requires many pieces of equipment for purification, the results of which lead to a high cost for obtaining pure C3G, thus limiting its industrial applications [11–13]. Most studies on C3G from aronia

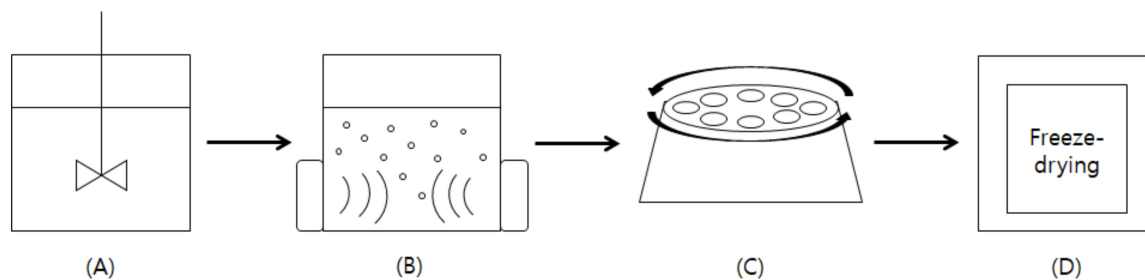
have been performed on the crude extracts, juice extracts, and/or partially purified extracts obtained by various types of pressing processes at room temperature or lower [3,14–16], so as not to break down C3G with high temperature. Especially, at higher than 60 °C for 8–10 h, 30–40% of total anthocyanins in the juice extracts were broken along with more than 50% loss of its biological activities [11,14]. However, these processes could not yield sufficient concentrations of C3G and other anthocyanins in the extracts to guarantee the efficacy of the extracts for use in applications, since pressing processes are not generally known to yield high extraction efficiencies compared to those of other solvent extraction processes [14,15,17,18]. Because of these limitations, the applications of C3G and/or extracts of aronia have been limited in industrial fields, even though various drying and production processes have been employed [11,18,19]. Therefore, several nonthermal extraction processes to obtain high amounts of C3G in the extracts from aronia have been carried out under low-temperature conditions, such as ultrasonic or ultrahigh pressure extraction processes [20–24]. Among those nonthermal processes, ultrasonic extraction processes have shown some promising results for extracting relatively higher amounts of C3G at low temperature than for those of traditional pressing processes, yielding 7–11 mg/g of relatively high amounts of C3G from various combined extraction processes [20,25]. However, ultrasonic extraction for processing aronia still has several hurdles to overcome; for example, the process must be operated under proper conditions to maintain efficiency and to obtain high yields with less input energy, which should be an important consideration for scaling up for industrial applications. Moreover, in general, low-temperature extraction has been considered to have relatively low yields, but this is a critical consideration for industrial scale-up of the production processes even though ultrasonic processes have been successfully scaled up to 5 ton of a working volume with more efficient ultrasonic generators [17]. Besides these limitations, the optimization of proper ultrasonic extraction parameters has not intensively been studied to maximize the production yields and to provide the economic feasibility of ultrasonic processes by effectively inducing cell wall crushing through high energy cavitation even at low temperatures, even though this process must have a good merit of processing aronia [17,26,27]. Moreover, detail analysis of ultrasonic extraction has not been much considered by correlating with each process parameter such as input frequency, process time, and temperature associated with its yields and also biological activities. Therefore, in this work, a more comprehensive study on optimizing the ultrasonic extraction parameters, such as process temperature, time, and input frequency, was carried out to obtain very high amounts of intact C3G from aronia, and the efficacies of the extracts obtained from the optimized process were studied to assess the superiority of the optimized ultrasonic extraction for processing aronia.

## 2. Materials and Methods

### 2.1. Preparation of the Samples

One kilograms of the dried fruits of *Aronia melanocarpa* Elliot (cultivated with organic farming method and harvested, and also dried in the shade in Danyang, a mountain area of central Korea in 2017) was mixed with 100 mL of 70% ethanol for 1 h and pressed at room temperature by a juice extractor (10 L working volume, KP-32, Shinil, Seoul, Korea) equipped with an oil pump screw type presser (DB-23, Donbo, Incheon, Korea) and a 30 µm pore size stainless steel filter for ~15 min. The filtrated cake was pressed again by a juice extractor to get more extracts from the residues, and then two filtrates from each process were mixed together to make the final control extract. After that, the filtrates were separated by a centrifuge (CF-1R, Ilshin, Dongducheon, Korea) at 4200 g for 10 min. Then, the extracts were further concentrated using a vacuum evaporator (N series, Eyela, Tokyo, Japan) at room temperature and freeze-dried using a lyophilizer (PVTFA, Ilshin, Dongducheon, Korea) to make the juice extract powder which served as a control. For the ultrasonic extraction, 1 kg of dried fruit was mixed with 10 L of 70% ethanol and placed into an ultrasonic extractor (20 L total working volume, AUG-900, Asia Ultrasonic co., Gyeonggi, Korea) with a multicontroller that can allow for the varying of the frequency and temperature, and the extraction was performed under the following

conditions; a frequency range of 20–100 kHz at fixed input power of 120 W, a temperature range of 15–35 °C, and an extraction time range of 2–6 h. The ranges of these parameters were determined from preliminary experiments. After ultrasonic extraction, the extracts were maintained for 6 h at room temperature to extract more C3G. Then, the extracts were filtered through filter paper and made into a powder by following the same procedures used to prepare the juice extract powder. Powders were stored at −4 °C until the experiments were performed. A schematic diagram of the ultrasonic extraction process is shown in Figure 1.



**Figure 1.** A schematic diagram of ultrasonic extraction process. (A) Mixing the aronia fruits with 70% ethanol solvent; (B) ultrasonic extraction with various variables in the range of 20 to 100 kHz of input frequency, 2–6 h of process time and 15–35 °C of process time; (C) centrifugation of the extract at 4200 g for 10 min to remove the solids; and (D) freeze-drying the supernatants.

## 2.2. Experimental Design

The extraction of C3G from aronia was optimized by the Response Surface Methodology (RSM). Table 1 shows the coded and uncoded values of the three independent variables—extraction time ( $X_1$ , 2–6 h), temperature ( $X_2$ , 15–35 °C), and ultrasonic frequency ( $X_3$ , 20–100 kHz)—defined by central composite design (CCD) at 5 levels with 20 experimental runs and three replicates. A mathematical model was designed as follows

$$Y = \beta_0 + \sum_{i=1}^k \beta_i X_i + \sum_{i=1}^k \beta_{ii} X_i^2 + \sum_{i=1}^{k-1} \sum_{j=2}^k \beta_{ij} X_i X_j \quad (1)$$

where  $Y$  is an independent variable of the C3G content in the extracts,  $\beta_0$  is the constant coefficient,  $\beta_i$  is the linear coefficient for the main effect,  $\beta_{ii}$  is the quadratic coefficient, and  $\beta_{ij}$  is the interaction coefficient. The adequacy of the proposed quadratic model was evaluated by the regression coefficient  $R^2$ , between that of the experimental and predicted data [28]. Antioxidant effects of the extracts from the optimized ethanol and conventional juice extraction processes were also compared to confirm the validity of the experimental model.

## 2.3. Determination of the C3G Contents in the Extracts

To measure the concentrations of C3G in the extracts, High-Pressure Liquid Chromatography (HPLC, Surveyor, Thermo Finnigan, San Jose, CA, USA) was used with a  $C_{18}$  column ( $4.6 \times 150$  mm, 5  $\mu$ m, Luna, Phenomenex, Torrance, CA, USA) at 25 °C and 1.0 mL/min of flow rate under the following conditions; elution solvent was 1% formic acid and mobile phase of (A) water and (B) acetonitrile with the following gradient; 0% B at 0–2 min, 0–100% B at 2–10 min, 100–70% B at 10–12 min, and 70–0% B at 12–15 min. Sample injection volume was 10  $\mu$ L after being diluted with 1:50 ( $v/v$ ) of elution solvent, only to show a main peak of C3G in the chromatograms. The absorbance was measured by a UV detector (Alts-10, Waltham, MA, USA) at 520 nm and compared with the peak areas of 100 ppm of a standard C3G (Sigma, St. Louis, MO, USA) [29].

## 2.4. Measurement of Antioxidant Activities of the Extracts

To evaluate the antioxidant activities of the extracts, the  $\alpha, \alpha$ -diphenyl- $\beta$ -picrylhydrazyl (DPPH) free-radical scavenging activity was measured by the Dietz method [30]: After mixing 150  $\mu$ L of 0.1 mM

DPPH solution prepared with methanol as the solvent with either 150  $\mu\text{L}$  of the extract or 13  $\mu\text{g/mL}$  of C3G, then the mixture was wrapped in foil to block light and left unattended for 30 min at room temperature. Thereafter, the absorbance was measured at a wavelength of 517 nm by a microplate reader (Thermo Fisher Scientific, Waltham, MA, USA). The relevant values were estimated as percent DPPH radical scavenging activity (%).

**Table 1.** Results of estimating C3G contents in the extracts by the central composite experimental design.

| Variables                                | Level           |       |       |                   |       |       |                  |
|--|-----------------|-------|-------|-------------------|-------|-------|------------------|
|  | −2              | −1    | 0     | 1                 | 2     |       |                  |
| Extraction Time $X_1$ (h)                | 2               | 3     | 4     | 5                 | 6     |       |                  |
| Temperature $X_2$ ( $^{\circ}\text{C}$ ) | 15              | 20    | 25    | 30                | 35    |       |                  |
| Frequency $X_3$ (kHz)                    | 20              | 40    | 60    | 80                | 100   |       |                  |
| Variables                                | Coded Variables |       |       | Uncoded Variables |       |       | $Y$ (mg/g)       |
|  | $X_1$           | $X_2$ | $X_3$ | $X_1$             | $X_2$ | $X_3$ |                  |
| 1  | 1               | 1     | 0     | 5                 | 20    | 60    | $12.88 \pm 1.07$ |
| 2  | 1               | 1     | 1     | 5                 | 30    | 80    | $9.19 \pm 2.31$  |
| 3  | 1               | 2     | 2     | 5                 | 35    | 100   | $6.32 \pm 1.50$  |
| 4  | 0               | −1    | 0     | 4                 | 20    | 60    | $12.55 \pm 3.45$ |
| 5  | 0               | 1     | −1    | 4                 | 30    | 40    | $8.75 \pm 2.04$  |
| 6  | 0               | −2    | −2    | 4                 | 15    | 20    | $10.23 \pm 3.73$ |
| 7  | −1              | 1     | −1    | 3                 | 30    | 40    | $8.38 \pm 1.52$  |
| 8  | −1              | 0     | 1     | 3                 | 25    | 80    | $10.23 \pm 2.50$ |
| 9  | −1              | 2     | 2     | 3                 | 35    | 100   | $6.01 \pm 2.82$  |
| 10                                       | −2              | −2    | −2    | 2                 | 15    | 20    | $10.89 \pm 2.77$ |
| 11                                       | −2              | 1     | 2     | 2                 | 30    | 100   | $8.02 \pm 3.38$  |
| 12                                       | −2              | −1    | 0     | 2                 | 20    | 60    | $10.48 \pm 3.39$ |
| 13                                       | 2               | 2     | 2     | 6                 | 35    | 100   | $6.45 \pm 0.71$  |
| 14                                       | 2               | −2    | 2     | 6                 | 15    | 100   | $11.82 \pm 3.85$ |
| 15                                       | 2               | 0     | −1    | 6                 | 25    | 40    | $9.99 \pm 1.17$  |
| 16                                       | 1               | −2    | −2    | 5                 | 15    | 20    | $10.16 \pm 2.02$ |
| 17                                       | 0               | 2     | 2     | 4                 | 35    | 100   | $5.35 \pm 2.88$  |
| 18                                       | −1              | −2    | −2    | 3                 | 15    | 20    | $11.32 \pm 3.00$ |
| 19                                       | −2              | 2     | −1    | 2                 | 35    | 40    | $5.4 \pm 1.09$   |
| 20                                       | 2               | −1    | −2    | 6                 | 20    | 20    | $10.92 \pm 4.28$ |

### 2.5. Statistical Analysis

All experiments were performed three times and expressed as the mean  $\pm$  SD. Data were analyzed by the generalized linear model (GLM) procedure of the Statistical Analysis System (SAS, version 9.1, SAS Institute, Cary, NC). The data were also analyzed by the one-way Analysis of Variance (ANOVA) test and significant difference was set to  $p < 0.05$ .

### 3. Results and Discussion

Table 1 shows the results for estimating the content of C3G ( $Y$ ) for each experiment under the various extraction conditions as independent variables ( $X_1$ ,  $X_2$ , and  $X_3$ ), as designed by the CCD. In general, the amount of C3G in the extracts was increased the most by an increase in the ultrasonic frequency, followed by an increase in the process time, while the yield of C3G was sharply decreased as the temperature was increased. This result confirmed the susceptibility of C3G to heat, with serious destruction occurring at  $35^{\circ}\text{C}$ . The highest C3G content, 12.88 mg/g, was obtained from the extraction at 60 kHz and  $20^{\circ}\text{C}$  for 5 h, and this value was much higher than the 10.01 mg/g C3G in the juice extract powder reportedly obtained from a conventional method of processing aronia [11,13,31]. Similarly, the concentration of C3G in the extract from the optimized process was also found to be higher than 3.0–10.5 mg/g from other extraction processes with water or 70% ethanol, even though

some of the results showed exceptionally high concentrations of above 15 mg/g in their extracts, values of which were not often reproducible [32]. This result strongly implies that the ultrasonic extraction is an effective process for extracting C3G from aronia at low temperatures, and this optimized process can yield high amounts of intact C3G. Tables 2 and 3 show the results of the ANOVA and the RSM model, resulting in the following quadratic Equation (2).

$$Y = -6.19705 + 0.94378X_1 + 1.81871X_2 - 0.12436X_3 - 0.00673X_1^2 - 0.04127X_2^2 - 0.00083X_3^2 - 0.09196X_1X_2 + 0.02641X_1X_3 + 0.00522X_2X_3 \quad (2)$$

where the regression coefficient ( $R^2$ ) of this quadratic model was estimated as 0.956, which tells us this model was a good fit. The linear, quadratic, and total model regressions were also highly significant ( $p < 0.05$ ), except for the cross-products, such as  $X_1X_2$  ( $p < 0.01$ ),  $X_1X_3$  ( $p < 0.01$ ), and  $X_2X_3$  ( $p < 0.05$ ).

**Table 2.** Results of analysis of variance for C3G contents in the extracts of aronia.

| Factor <sup>1</sup> | DF <sup>2</sup> | Sum of Squares | F-Value    |
|---------------------|-----------------|----------------|------------|
| $X_1$               | 1               | 1.353          | 0.63       |
| $X_2$               | 1               | 889.08         | 51.47 **,3 |
| $X_3$               | 1               | 3691.5         | 4.07 *,3   |

<sup>1</sup>  $X_1$ , Process time (hr);  $X_2$ , Temperature (°C);  $X_3$ , Frequency (kHz). <sup>2</sup> DF: degree of freedom. <sup>3</sup>\* Significant at  $p < 0.05$ , \*\* Significant at  $p < 0.001$ .

**Table 3.** The results of estimating regression coefficients of the second order polynomials for C3G contents in the extracts.

| Parameter <sup>1</sup> | DF <sup>2</sup> | Coefficient | t-Value | p-Value |
|------------------------|-----------------|-------------|---------|---------|
| Intercept              | 1               | −6.19705    | −0.922  | 0       |
| $X_1$                  | 1               | 0.94378     | 1.061   | 0.014   |
| $X_2$                  | 1               | 1.81871     | 2.272   | 0.005   |
| $X_3$                  | 1               | −0.12436    | −0.996  | 0.009   |
| $X_1 \cdot X_1$        | 1               | −0.00673    | −0.058  | 0.001   |
| $X_2 \cdot X_2$        | 1               | −0.04127    | −2.722  | 0.087   |
| $X_3 \cdot X_3$        | 1               | −0.00083    | −1.602  | 0.370   |
| $X_1 \cdot X_2$        | 1               | −0.09196    | −1.703  | 0.819   |
| $X_1 \cdot X_3$        | 1               | 0.02641     | 1.982   | 0.126   |
| $X_2 \cdot X_3$        | 1               | 0.00522     | 1.760   | 0.109   |
| $R^2 = 0.956$          |                 |             |         |         |

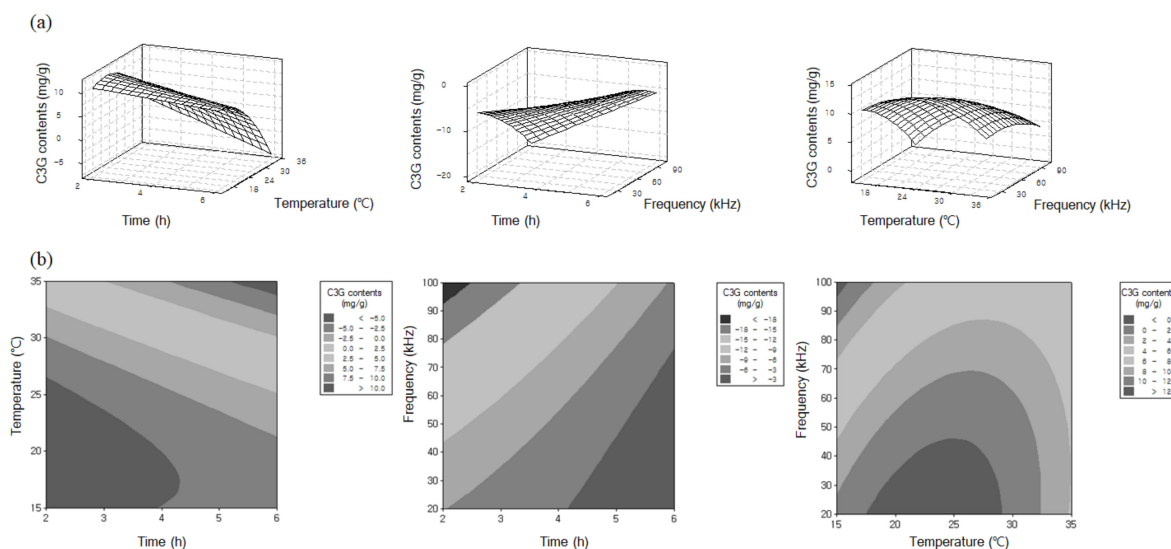
<sup>1</sup>  $X_1$ , Process time (hr);  $X_2$ , Temperature (°C);  $X_3$ , Frequency (kHz). <sup>2</sup> DF: degree of freedom

Figure 2 also illustrates the three-dimensional response surfaces and contour plots for the C3G contents as a function of the three variables ultrasonic frequency, process temperature, and extraction time. The saddle point of each plot well represented the optimal conditions that can obtain the highest concentration of C3G in the extract, considering each of two processes.

As shown in Table 1, the amount of C3G in the extracts was most significantly increased by an increase in the frequency in the range of 20 to 60 kHz, but the extraction was not much more effective at frequencies above 80 kHz. The contents of C3G were also increased as the process time increased from 3 to 6 h, which shows that longer process times can be helpful to increase the yield of C3G. However, the concentrations of C3G in the extracts were significantly decreased by an increase in the temperature from 30 to 35 °C. This result could have been due to the breakdown of C3G in the extracts at higher temperatures, as similar results have been reported elsewhere [11,14].

The results imply that ultrasonic treatment is an effective process to obtain heat-labile components from natural sources with a lower temperature and shorter time than those of conventional methods. To validate the model of Equation (2), Table 4 compares the contents of C3G from experimental results with the predictive model, operated under the optimal conditions determined by ridge analysis

(Minitab release ver. 14.12.1, Minitab Inc., State College, PA, USA, 2015). The model estimated a concentration of 13.70 mg/g of C3G under optimal conditions, and from the experiment with those same conditions, 13.01 mg/g of C3G was obtained, which is within ca. 95% similarity. Therefore, this result clearly confirms that the proposed quadratic model was well designed. The amount of C3G from this optimal extraction condition was also the highest concentration obtained from aronia, as compared to the concentrations estimated in Table 1. This concentration was similar to or even higher than other reported data from various extraction conditions [6,33].

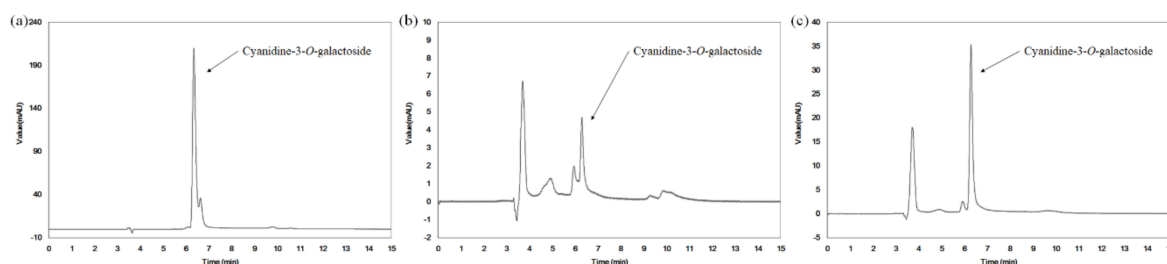


**Figure 2.** 3-D response surfaces (a) and contour plots (b) as a function of ultrasonic frequency, process temperature and time.

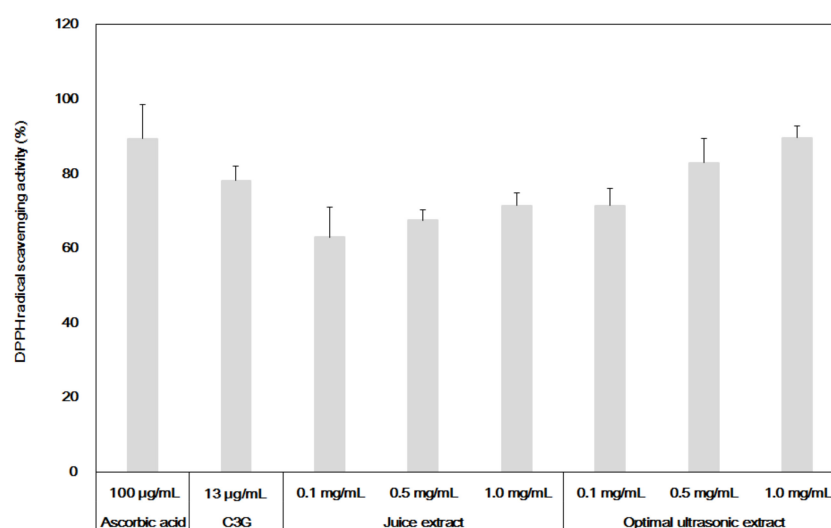
**Table 4.** Comparison of predicted and experimented values of response variables operated under an optimal extraction condition.

| Dependent Variables |                  |                 | Response Variables     |                           |
|---------------------|------------------|-----------------|------------------------|---------------------------|
| Time (h)            | Temperature (°C) | Frequency (kHz) | Predicted Value (mg/g) | Experimental Value (mg/g) |
| 6.0                 | 18.8             | 75.0            | 13.70                  | 13.01 ± 2.62              |

Figure 3 compares the HPLC chromatograms of C3G in the extracts from the conventional juice extraction process and this optimized ultrasonic process. It was very clear that higher amounts of C3G were obtained from the optimal extraction process than from conventional juice extraction even though the minor tailing of the peaks of the standard C3G was observed in Figure 3a, which would not much affect the measurement of actual concentrations of C3G in the extracts. Therefore, it can be concluded that this optimized process can be employed to yield a high quality extract containing high amounts of intact C3G, which can possibly reduce the production costs of purifying C3G and increase the efficacy of the extract itself. To confirm this hypothesis, Figure 4 compares the antioxidant activities of the extracts from the two different processes. The activities were also compared with the data from adding 13 µg/mL of C3G alone as a positive control, whose concentration was equivalent to the amount of C3G present in 1.0 mg/mL of the extracts, based on the results of Table 4. In general, the higher the concentration of C3G used in the treatment, the better the antioxidant activity. Specifically, even at the same dose of 1.0 mg/mL, the extract from the optimal conditions had higher activity than that from a conventional juice extraction, 89.5% vs. 71.3%, respectively. This difference in antioxidant activity between the two extracts could well reflect the difference of C3G content under the same treatment concentration of the extracts, with 13.01 mg/g vs. 10.01 mg/g of C3G in the extracts from the optimal and conventional processes, respectively.



**Figure 3.** Comparison of High-Pressure Liquid Chromatography (HPLC) chromatograms of C3G in the extract from three different extraction conditions: (a) standard C3G, (b) conventional extraction by a juice extractor, and (c) optimal extraction condition.



**Figure 4.** Comparison of antioxidant activities of the extracts from optimized ultrasonic process, juice extraction, and pure C3G, along with ascorbic acid as a positive control.

Interestingly, adding 13 µg/mL of C3G alone did not show the same the antioxidant activity as that of adding 1.0 mg/mL of the extract from the optimal process, even though the extract contained the same amount of C3G. However, the antioxidant activity of adding 13 µg/mL of C3G alone was better than that of adding 1.0 mg/mL of the juice extract that contained a lower C3G concentration of 10.01 mg/g. These results clearly indicate that the antioxidant activities of the extracts from aronia were mainly due to the amount of C3G but that the higher antioxidant activity of the extract from the optimized process might have been due to synergistic effects of C3G with other biologically active substances in the extracts, since the optimized process can yield higher contents of both C3G and other components. Taken together, these results suggest that aronia extract from an optimized ultrasonic extraction process could be used as a high quality, functional food that has strong antioxidant activities and that it is not necessary to prepare a highly purified C3G from the extracts.

#### 4. Conclusions

This work was the first to show that high contents of extremely heat-labile C3G from *A. melanocarpa* Elliot can be obtained by optimizing ultrasonic process parameters such as input frequency, process time, and temperature. This process was found that the ultrasonic frequency and process time are very important for C3G extraction, and it is clearly shown that at higher process temperatures, C3G was greatly degraded. It was also confirmed that the extracts from the optimized ultrasonic process have higher C3G concentrations and show higher antioxidant activity than those from a conventional juice extractor, a common process with less efficiency so far. The antioxidant activity of C3G alone was lower than that of the extract containing the same concentration of C3G, possibly due to synergistic effects

of C3G with other biologically active components extracted from the optimized process. However, further investigation should also be carried out to confirm more detail mechanism of its synergistic effects. In this work, strong antioxidant activities of the extracts were attributed mainly to the C3G content of the extracts. In conclusion, this optimal ultrasonic extraction process can yield high-quality aronia extracts containing very high amounts of intact C3G, and fewer purification steps reduces the production cost needed to obtain high purity and yield of C3G. In conclusion, this optimal ultrasonic extraction process can yield high-quality aronia extracts containing very high amounts of intact C3G, which could also reduce purification steps to obtain high purity and yield of C3G. The results also suggest that by optimizing ultrasonic parameters at low temperatures, high extraction yields of heat-sensitive substances from many various natural sources including aronia can be expected.

**Author Contributions:** H.Y.L. designed the whole experiment and drafted the manuscript. The author read and approved the final manuscript.

**Conflicts of Interest:** The author declares no conflicts of interest.

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