

Article

Effect of Amphiphilic Polymer/Nano-Silica Composite on Shale Stability for Water-Based Muds

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Abstract: Research on using nanotechnology to solve shale instability problems in drilling engineering has been increasing. The combination of amphiphilic polymer and silica nanoparticles may be a new way to improve shale stability. Herein, an amphiphilic polymer/nano-silica composite (poly(styrene-methyl methacrylate-acrylamide)/nano-SiO₂) was introduced as a novel shale stabilizer SMA/SiO₂ for water-based muds, which possessed the advantages of both physical plugging and chemical inhibition during the drilling operations. The SMA/SiO₂ was prepared and characterized by Fourier transform infrared spectra (FT-IR), nuclear magnetic resonance (¹H-NMR), transmission electron microscope (TEM), particle size distribution (PSD) and thermogravimetric analysis (TGA) experiments, which confirmed that SMA/SiO₂ was regularly spherical with nano-scale and showed good high-temperature resistance. To evaluate the plugging capacity of SMA/SiO₂, the pressure transmission test and BET analysis were applied. The results indicated SMA/SiO₂ was capable of effectively plugging the pores and fractures in shale. To evaluate the hydration inhibition capacity of SMA/SiO₂, the rolling dispersion experiment and contact angle test were adopted. The results demonstrated that SMA/SiO₂ could reduce the tendency of shale hydration, which was better than potassium chloride (KCl) and polymeric alcohol (JHC). In addition, SMA/SiO₂ only created slight variations on the rheological parameters of the water-based muds (WBMs) and showed a significant filtration control performance. Due to the outstanding performance of physical plugging and chemical inhibition, SMA/SiO₂ was expected to be a novel shale stabilizer to solve shale instability problems.

Keywords: shale stabilizer; amphiphilic polymer; nano-SiO₂; plugging ability; hydration inhibition

1. Introduction

Drilling fluids are considered as circulating fluids in the drilling operations, which provide multiple functions. Their major functions consist of suspending/transporting drill cuttings, cooling and lubricating the drilling bits, maintaining borehole stability and reducing the formation damage [1–3]. Drilling fluids are usually grouped into three types: water-based muds (WBMs), oil-based muds, and synthetic-based muds. Due to their lower cost and lesser impact on environment, WBMs have become the most widely used drilling fluids in the world [4,5].

In recent years, the development of shale gas as an unconventional oil and gas resource has gained an increase in attention [6–12]. The technology of drilling fluids for the long well section of a horizontal well is one of the key technologies used to drill shale gas formations. Since the shale

formations develop nano-scale pores and fractures and have a strong water-sensitivity characteristic, shale instability in the drilling process is prone to occur. This restricts the process of shale gas exploration and development [13,14]. Figure 1 shows the general sketch of the shale instability problems caused by WBMs. Due to a large number of nano-scale pores and fractures developed in the shale formations, they are characterized by extremely low permeability and low porosity [15–17]. In the drilling operations, pressure transmission in WBMs will result in an increase in the pore pressure of shale formations, and thus cause wellbore instability. The best approach for solving this problem is to plug the nano-scale pores and fractures developed in the shale formations [18–20]. However, conventional agents for WBMs are too large to play an effective role of plugging. Therefore, seeking for plugging agents with a suitable size to achieve better plugging capacity is essential.

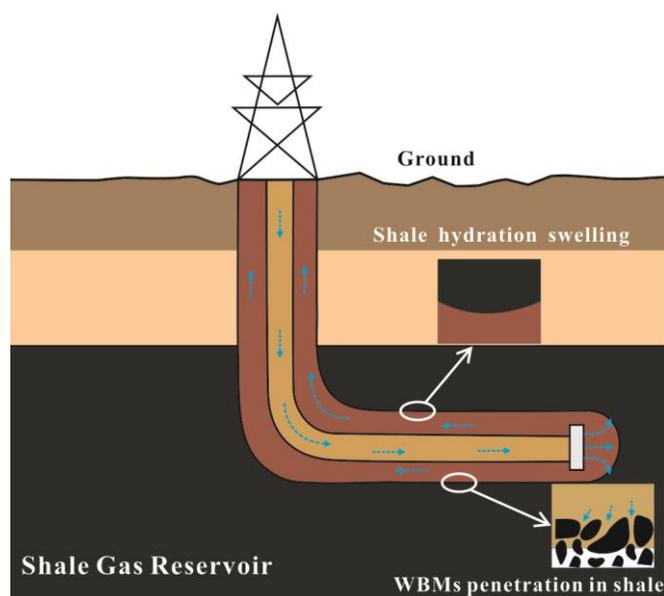


Figure 1. General sketch of the shale instability problems caused by WBMs (water-based muds).

In the last few years, the interest in using nanotechnology in the oil and gas industry has been increasing [21–23]. Various kinds of nanomaterials have been introduced into WBMs as promising shale stabilizers [24–26]. The inorganic nanoparticles such as unmodified nanosilica were first introduced into WBMs as plugging agents. It was found that nanosilica could seal the shale pores and improve the filtration loss performance of WBMs [27,28]. Graphene oxide has also been investigated as another form of rigid nanoparticles, and it showed good plugging performance in WBMs [29]. However, inorganic nanoparticles are prone to aggregation, and thus the plugging ability can be weakened. Polymeric nanoparticles (such as polymer latex) possessing better dispersing performance in WBMs have also been introduced as plugging agents. The studies showed that the polymeric nanoparticles could decrease shale permeability and effectively retard pressure transmission [30,31]. However, polymer latex is usually preserved in the emulsion state and sensitive to the environmental change, which restrict its application to oilfields. Recently, polymer-inorganic nanocomposites have attracted more and more attention in the drilling fluids industry [32–35]. The benefits of nanocomposites to be applied in WBMs include excellent dispersing performance, decrease in filtration volume, and improvement of rheological properties [36,37]. Therefore, the polymer-inorganic nanocomposites may be an effective way to solve shale instability problems.

Polyacrylamide-grafted-polyethylene glycol/silica nanocomposite was reported as a potential additive for WBMs, which demonstrated good shale hydration inhibition performance [28]. But the plugging capacity was not considered in their work. Poly(AM-AMPS)/nano-SiO₂ composite was introduced into WBMs as a fluid loss agent [26]. Research showed that the composite could plug the nanopores of shale, but the shale hydration inhibition performance was not further evaluated.

Since shales mainly consist of clay minerals, shale hydration becomes another important factor causing borehole instability that cannot be ignored [38–40]. Amphiphilic polymer has been reported to be able to inhibit shale hydration [41]. The combination of amphiphilic polymer and silica nanoparticles may have the advantages of both physical plugging and chemical inhibition. In this study, a novel shale stabilizer poly(St-MMA-AM)/nano-SiO₂ composite (SMA/SiO₂) was synthesized. Poly(St-MMA-AM) was used as an amphiphilic polymer where St and MMA provided the hydrophobic segments and AM provided the hydrophilic segments.

First, materials and methods were presented. Then, the novel shale stabilizer SMA/SiO₂ was prepared and characterized. To investigate the plugging ability of SMA/SiO₂, the pressure transmission experiment and BET analysis were conducted. To evaluate the shale hydration inhibition capacity of SMA/SiO₂, the rolling dispersion experiment and contact angle test were carried out. Finally, the compatible test was conducted to evaluate the effect of SMA/SiO₂ on the rheological and filtration control properties of the WBMs.

2. Materials and Methods

2.1. Materials

Styrene (St, 99%), methyl methacrylate (MMA, 98%), acrylamide (AM, 98%), potassium chloride (KCl, 99.5%), ethanol (99.7%), sodium dodecyl sulfate (SDS), 3-methacryloxypropyltrimethoxysilane (KH570, 98%), ethylic acid (99.5%) and potassium persulfate (KPS, 99%) were obtained from Sinopharm Chemical Reagent Co., Ltd., Shanghai, China and used without further purification. KH570 was mainly used to improve the bonding properties of organic and inorganic materials. Nano-silica particles (99.8%, 7–42 nm) and octylphenol polyoxyethylene ether (OP-10, 99%) were purchased from Aladdin Reagent Co., Ltd., Shanghai, China and used as received. The TEM (JEM-2100UHR, JEOL Ltd., Akishima, Tokyo, Japan) image and the particle size distribution (PSD) curve of nano-silica particles was shown in Figure 2. The particle size of nano-silica particles was mainly distributed in the range of 7–18 nm. Due to a few nanoparticles agglomerated, the larger particles were found in 32–42 nm. Polymeric alcohol (JHC) was provided by China Oilfield Services (Sanhe, China). Sodium bentonite was provided by Weifang Huawei Bentonite Group Co., Ltd., Weifang, China. Xanthan gum and low-viscosity polyanionic celluloses were obtained from Shida Chuangxin Technology Co., Ltd., Dongying, China. Furthermore, deionized water was used during the experiments. The shale samples used in this work were provided by Turpan Hami Basin, China and the X-ray diffraction analysis results were shown in Table 1.

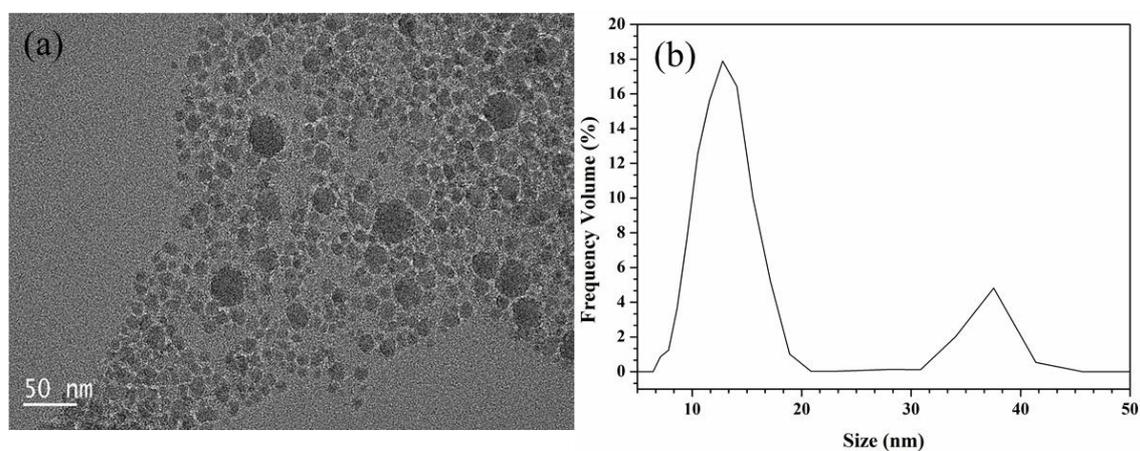


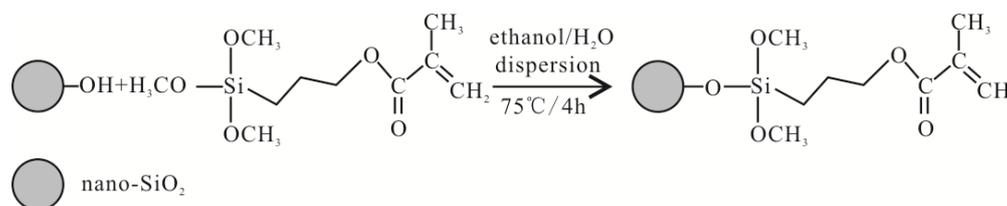
Figure 2. (a) TEM (transmission electron microscope) image and (b) PSD (particle size distribution) curve of nano-silica particles.

Table 1. Mineral content of the shale samples.

Component	Content (wt%)	Component of Clay Mineral	Content (wt%)
Quartz	20	Illite	12
Calcite	28	Chlorite	3
Plagioclase	29	Kaolinite	3
Iron dolomite	2	Illite/smectite mixed layer	82
Potassium feldspar	6		
Clay mineral	15		

2.2. Preparation of SMA/SiO₂

The novel shale stabilizer SMA/SiO₂ was prepared based on the following two stages. The first stage was to prepare KH570/SiO₂ nanoparticles. Firstly, nano-silica particles (4 g) were dispersed into ethanol (60 mL) at 25 °C under ultrasonic conditions. Then, KH570 (0.8 g) was dissolved in ethanol/H₂O dispersion and the dispersion was adjusted to pH = 4 with ethylic acid. Secondly, the above dispersions were mixed in the reactor and stirred at 75 °C for 4 h. Thirdly, the obtained KH570/SiO₂ nanoparticles were purified several times by centrifugation and washing treatment using ethanol. Figure 3 shows the schematic representation on the silane functionalization of SiO₂.

**Figure 3.** Schematic representation on the silane functionalization of SiO₂.

The second stage was to prepare the novel shale stabilizer SMA/SiO₂ with St, MMA, AM and KH570/SiO₂ nanoparticles through emulsion polymerization [42]. Firstly, KH570/SiO₂ nanoparticles (0.4 g) were added to the monomer mixture containing St (12 g), MMA (6 g) and AM (2 g), and the mixture was ultrasonically treated for 3 h. Then, the aqueous solutions consisting of deionized water (60 mL), SDS (0.1 g), and OP-10 (0.1 g) were added to the mixture, and pre-emulsified under vigorous stirring. Secondly, the pre-emulsion was transferred in a 250 mL flask and the temperature was maintained at 75 °C for 30 min. Thirdly, the aqueous solutions containing of KPS (0.12 g) was poured to the flask for inducing polymerization and the polymerization was left for 3 h. The solid product was obtained by centrifugation and washing treatment using ethanol/H₂O, and dried at 60 °C under vacuum condition for further use.

2.3. Characterization of SMA/SiO₂

Fourier transform infrared spectra (FT-IR) of SiO₂, KH570/SiO₂ and SMA/SiO₂ were obtained by a FT-IR spectrometer (Nicolet 6700, Thermo Scientific, Waltham, MA, USA.). The nuclear magnetic resonance (¹H-NMR) spectrum of SMA/SiO₂ was determined by an NMR spectrometer (Bruker AV500, BRUKER OPTICS, Karlsruhe, Germany), and the sample was dissolved in CDCl₃. The particle size distribution (PSD) of SMA/SiO₂ in aqueous solution was measured with a particle size analyzer (NanoBrook Omni, Brookhaven Instruments Corporation, Holtsville, NY, USA.). The morphology of SMA/SiO₂ in aqueous solution was recorded by a transmission electron microscope (TEM, JEM-2100UHR, JEOL Ltd., Akishima, Tokyo, Japan). The thermogravimetric analysis (TGA) of SMA/SiO₂ was carried out on a TGA/DTA thermogravimetric analyzer (NETZSCH 209F3, Netzsch Group, Selb, Germany). During the experiment, the heating rate was set at 10 °C/min under a N₂ atmosphere, while the heating range was set at 25–600 °C.

2.4. Pressure Transmission Test

The pressure transmission technology provides a scientific and effective method to evaluate the plugging performance of different fluids. A shale hydra-mechanics coupling simulation test device developed by China University of Petroleum (East China) was used for the pressure transmission experiment [43]. In this test, the shale samples were cut into cylindrical cores (diameter: 2.54 cm; length: 0.75 cm). Base fluid for the test was prepared by dispersing 4 g sodium bentonite into 100 mL distilled water. Firstly, the shale core was placed into the core holder, and the axial and confining pressure were set at 5 MPa during the experiment. Then, the test fluids were pumped into the upstream entrance to contact with the shale core, while the upstream pressure was maintained at 2 MPa and the downstream's initial pressure was set at 1 MPa. The pressure transmission curve was recorded through monitoring the downstream pressure change. Furthermore, the permeability of shale cores before and after being plugged with SMA/SiO₂ could be calculated by the Equation (1) [44].

$$K = \frac{\mu\beta VL}{A} \frac{\ln\left(\frac{P_m - P_o}{P_m - P(L, t_2)}\right) - \ln\left(\frac{P_m - P_o}{P_m - P(L, t_1)}\right)}{t_2 - t_1} \quad (1)$$

The equation describes the shale permeability (K) as a function of viscosity (μ), static compression ratio (β), enclosed volume (V), length (L), cross-sectional area (A), experimental time (t), upstream pressure (P_m), initial downstream pressure (P_o) and real-time downstream pressure ($P(L, t)$).

In addition, the morphology of the shale cores before and after being plugged with SMA/SiO₂ were observed by scanning electron microscopy (SEM) to investigate the plugging mechanism.

2.5. Pore Structure Characterization of Shale

BET analysis is a widely applied method to characterize pore structure characteristics of shale [45,46]. Shale cuttings were screened and crumbled between 40 mesh and 60 mesh. Then, the shale samples were soaked in deionized water and 1% SMA/SiO₂ solutions respectively for 6 h at room temperature. After that they were removed from the solutions and dried in the air. Finally, nitrogen adsorption experiments were carried out on Quadrasorb SI equipment (Quantachrome Company, Boynton Beach, FL, USA). The surface area and pore volume of shale samples could be determined by analyzing the nitrogen adsorption data through BET analysis.

2.6. Rolling Dispersion Experiment

Rolling dispersion experiment was adopted to evaluate the hydration inhibition performance of SMA/SiO₂. In this test, shale cuttings were screened and crumbled into sizes in the range of 2.00–3.35 mm, which were dried at 105 °C for 4 h. Then, 50 g of dried shale cuttings and 350 mL of inhibitor solutions were transferred to the aging tank. The aging tanks were put into the roller furnace and hot-rolled at the temperature of 77 °C for 16 h. After cooling, shale cuttings were washed with distilled water and filtrated by a 40-mesh sieve. Finally, the recovered shale cuttings were dried and weighed to calculate the shale recovery rate.

2.7. Contact Angle Test

The contact angle test was carried out to evaluate the effect of SMA/SiO₂ on the wettability of the shale surface. In brief, the shale surface was polished using sandpaper to make it smooth. Then, the shale samples were soaked in the SMA/SiO₂ solutions at different concentrations for 6 h. After that they were removed from the solutions and dried in the air. Finally, a syringe was used to put a drop of water onto the shale surface and the images were recorded by the camera. The contact angle could be calculated by analyzing the images using built-in software. The contact angle measurement was conducted on the JC2000D5M contact angle meter (Zhongchen Company, Shanghai, China) at room temperature.

2.8. Compatible Test

The compatible test was conducted to evaluate the effect of SMA/SiO₂ on the rheological and filtration control properties of the WBMs. The WBMs were prepared by mixing 4% pre-hydrated sodium bentonite muds, 1% low-viscosity polyanionic celluloses, 0.2% xanthan gum and 3% potassium chloride under high-speed (8000 rpm) stirring conditions for 20 min. Then, the WBMs were transferred into an ageing oven (Haitongda Company, Qingdao, China) and hot-rolled at the temperature of 120 °C for 16 h. After being hot-rolled, the rheological and filtration control properties of the WBMs were measured. The compatibility of SMA/SiO₂ in WBMs was evaluated by comparing the rheological and filtration control performance of WBMs with or without SMA/SiO₂.

The rheological parameters such as apparent viscosity (AV), plastic viscosity (PV), and yield point (YP) were measured based on the API-recommended standard procedure by ZNN-D6 rotating viscometers (Haitongda Company, Qingdao, China). The Equations (2)–(4) were used to calculate the rheological parameters according to the readings from the high rotational speeds (300 and 600 rpm). The fluid loss (FL_{API}) of the WBMs was tested on ZNS-2A filtration apparatus (Haitongda Company, Qingdao, China).

$$\text{Apparent Viscosity (AV)} = \Phi 600 / 2 \text{ (mPa}\cdot\text{s)} \quad (2)$$

$$\text{Plastic Viscosity (PV)} = \Phi 600 - \Phi 300 \text{ (mPa}\cdot\text{s)} \quad (3)$$

$$\text{Yield Point (YP)} = (\Phi 300 - \text{PV}) / 2 \text{ (Pa)} \quad (4)$$

3. Results and Discussion

3.1. Characterization of the SMA/SiO₂

Figure 4 depicts FT-IR spectra of SiO₂, KH570/SiO₂ and SMA/SiO₂, and the characteristic peaks were observed. As shown in Figure 4a, the stretching band of O–H (3419 cm⁻¹) in SiO₂ was significantly weakened after the surface modification of SiO₂. The new peaks at 2928 cm⁻¹ and 2844 cm⁻¹ were for the stretching vibrations of the methyl and methylene from KH570. Thus, KH570 was successfully grafted onto SiO₂. Figure 4b shows the FT-IR spectrum of SMA/SiO₂. The peaks at 3061 cm⁻¹ and 3026 cm⁻¹ were for the C–H in the benzene ring from St. The peaks at 1603 cm⁻¹, 1495 cm⁻¹ and 1452 cm⁻¹ were for the vibrations of the benzene skeleton from St. The peak at 1730 cm⁻¹ was for the stretching vibrations of C=O, while 1200 cm⁻¹ represented the stretching vibrations of C–O–C from MMA. The peak at 3429 cm⁻¹ represented the stretching vibrations of N–H from AM. In addition, the stretching vibrations of Si–O and Si–O–Si were located at 1117 cm⁻¹ and 1076 cm⁻¹ respectively. Therefore, the FT-IR spectra show that SMA/SiO₂ was successfully prepared.

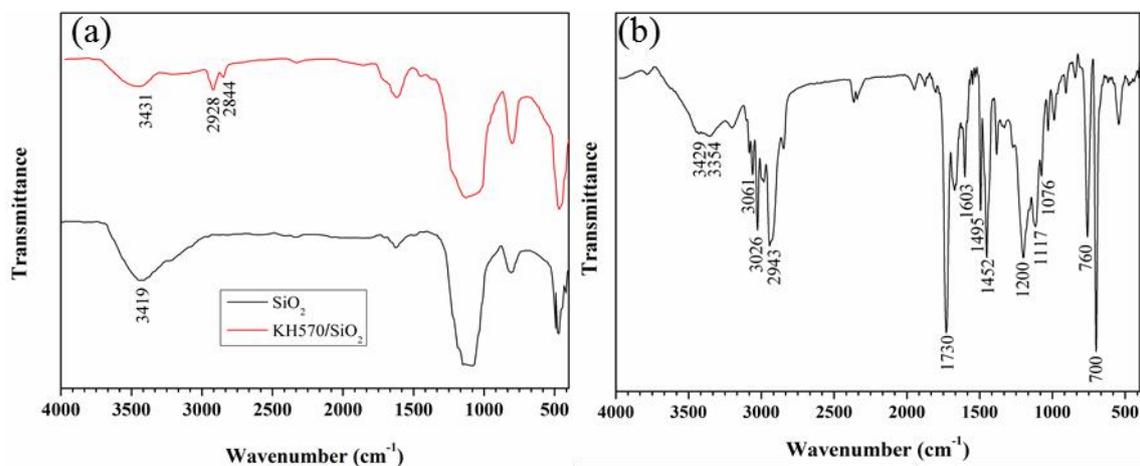


Figure 4. FT-IR spectra of (a) SiO₂, KH570/SiO₂ and (b) SMA/SiO₂.

In order to further characterize the chemical structure of SMA/SiO₂, the ¹H-NMR spectra of SMA/SiO₂ is presented in Figure 5. The peaks corresponding to the protons in the copolymer were labeled. It can be concluded that St, MMA and AM were grafted onto KH570/SiO₂. Thus, the chemical structure of SMA/SiO₂ was further confirmed.

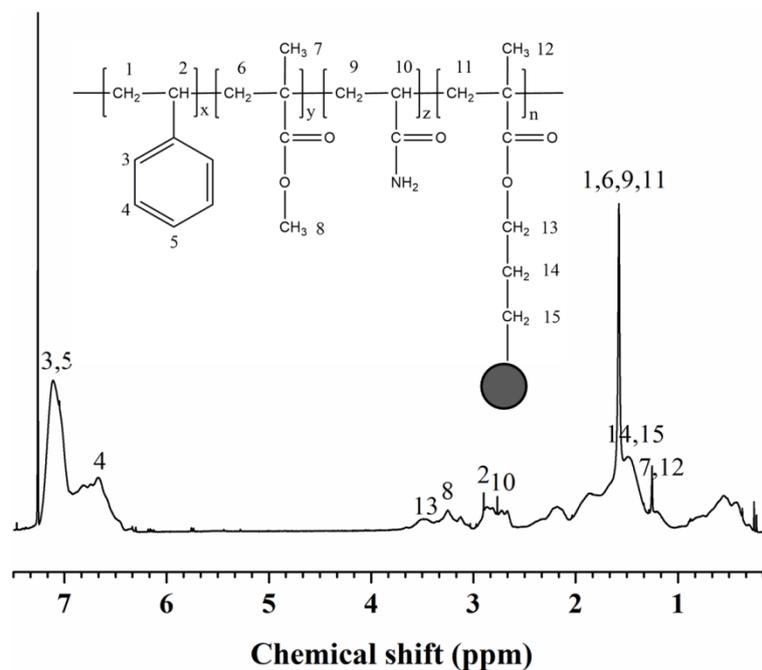


Figure 5. ¹H-NMR spectra of SMA/SiO₂.

The dispersion morphology of SMA/SiO₂ in aqueous solution was observed, and the TEM image is shown in Figure 6. The spherical nanoparticles exhibited good dispersivity in the aqueous solution. In addition, the average particle size of SMA/SiO₂ was about 75 nm, and the particle size distribution was mainly in the range of 50–90 nm.

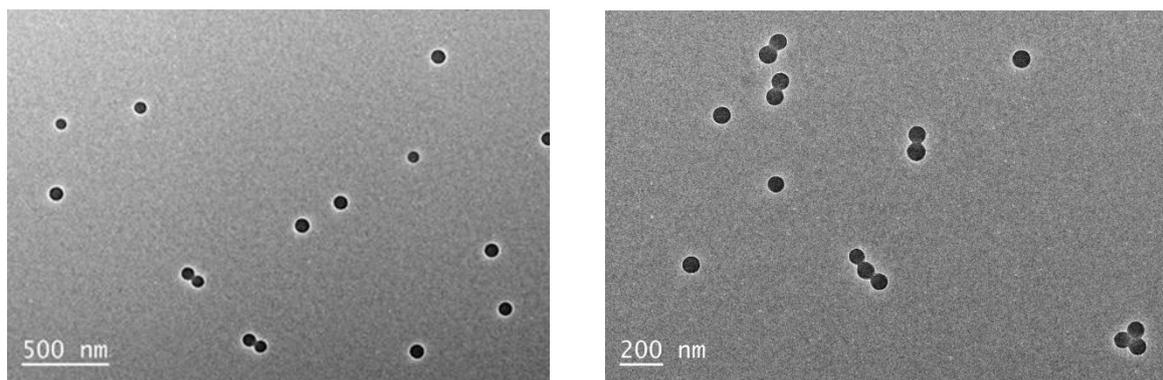


Figure 6. TEM image of SMA/SiO₂.

Figure 7 presents the PSD curves of SMA/SiO₂. The test results showed that the average particle size of SMA/SiO₂ was 72 nm, while the particle size was mainly distributed in the range of 43–122 nm. Due to a few nanoparticles in SMA/SiO₂ agglomerated, the larger particles were found in the PSD test results. Overall, the PSD test results corresponded with the TEM characterization results. The nanoscale diameter of SMA/SiO₂ was further confirmed. It could be inferred that SMA/SiO₂ was able to plug the shale pores and cracks in nano-scale.

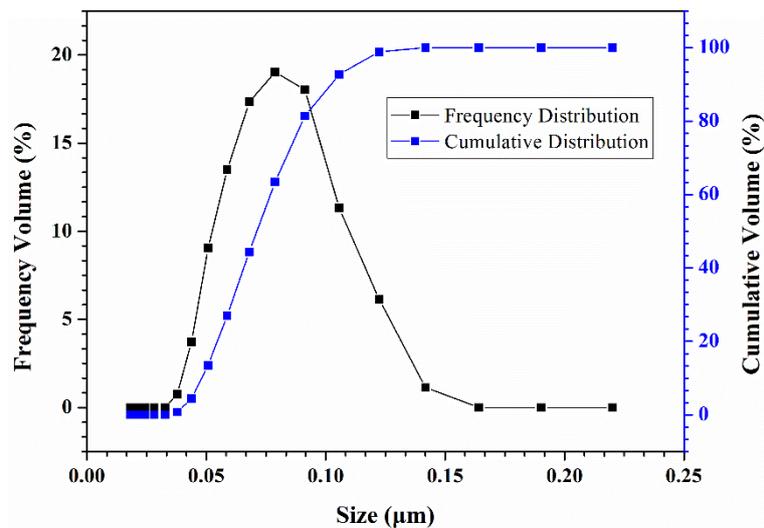


Figure 7. PSD curves of SMA/SiO₂.

Figure 8 shows the thermogravimetric curves of SMA/SiO₂. The weight loss was less than 0.3% for SMA/SiO₂ below the temperature of 120 °C due to the solvent evaporation. No significant weight loss was observed before the temperature reached 390 °C. Thermal stability is essential for plugging agents since WBMs withstand high-temperature stratum conditions. Through the results of TGA analysis, good high-temperature resistance of SMA/SiO₂ was confirmed.

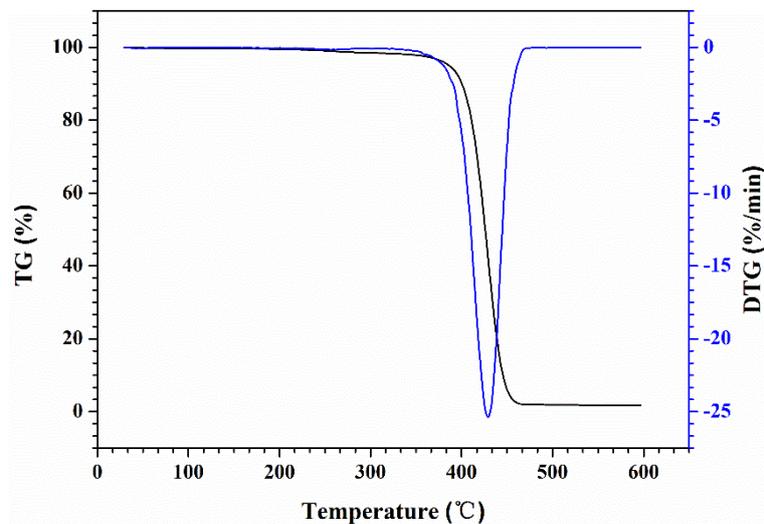


Figure 8. TGA (thermogravimetric analysis) curves of SMA/SiO₂.

3.2. Pressure Transmission Test

Figure 9 presents the downstream pressure change with time when the shale cores interacted with different test fluids. As shown in Figure 9, the pressure transmission rate of the shale cores was so fast that the downstream and upstream pressures were basically the same after 40 min. For the base fluid, a lower growth rate of the downstream pressure was observed, and it took about 128 min to achieve the equilibrium for the downstream and upstream pressures. For the base fluid containing 1% SiO₂, it took about 183 min to achieve the equilibrium for the downstream and upstream pressures. For the base fluid containing 1% SMA/SiO₂, it took about 255 min to achieve the equilibrium, which was significantly longer than the penetration times of the shale cores and the base fluid containing 1% SiO₂. Thus, SMA/SiO₂ played a notable role in slowing down the shale pressure transmission rate. The plugging capacity of SMA/SiO₂ was further evaluated through analyzing the shale permeability

change. The permeability of the shale cores before being plugged was $1.68 \times 10^{-6} \mu\text{m}^2$. After being treated by the base fluid and the base fluid containing 1% SiO_2 , the permeability was decreased to $1.09 \times 10^{-7} \mu\text{m}^2$ and $8.00 \times 10^{-8} \mu\text{m}^2$ respectively. Most noteworthy, after being plugged by the base fluid containing 1% SMA/ SiO_2 , the permeability was significantly reduced to $6.45 \times 10^{-8} \mu\text{m}^2$. Therefore, SMA/ SiO_2 possessed the capacity to seal the nano-scale pores and fractures, and a lower pressure transmission rate and shale permeability were observed after interact with SMA/ SiO_2 .

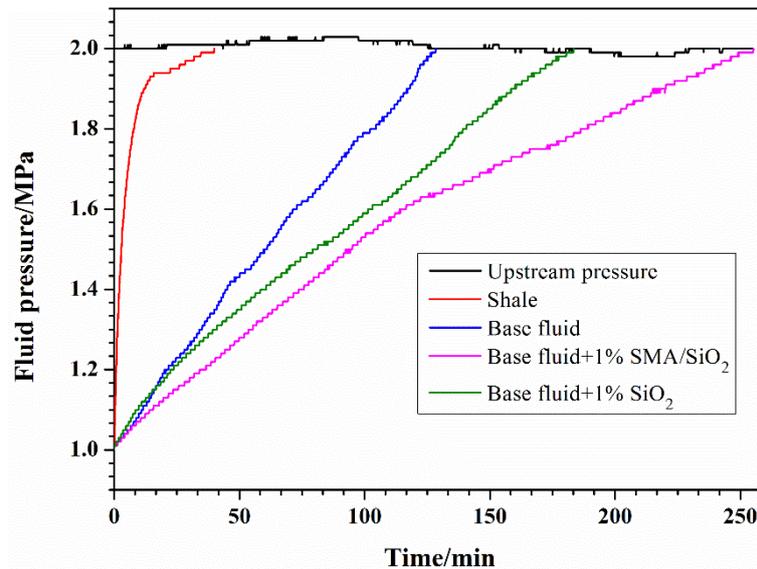


Figure 9. Pressure transmission experiment curves.

The SEM images of the shale cores after the pressure transmission experiments are shown in Figure 10. As shown in Figure 10a, a lot of pores and fractures developed in the shale cores and it can be inferred that the diameter of shale pores and the width of shale fractures were mainly distributed between 50–500 nm. These pores and fractures were effectively plugged after interaction with SMA/ SiO_2 in the base fluid (Figure 10b). After being plugged, the core surface changed to be smooth and dense, and an isolation layer was formed on it. As a result, the shale permeability was significantly reduced and the plugging capacity of SMA/ SiO_2 was excellent.

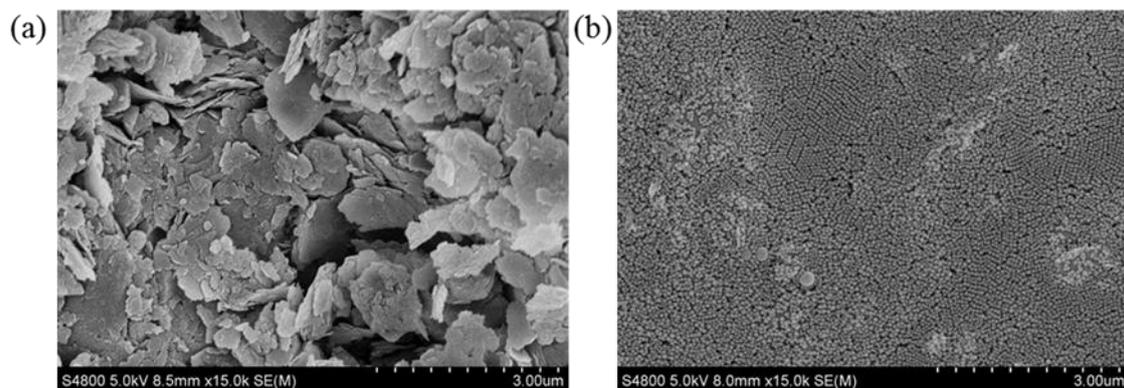


Figure 10. SEM images of the shale cores (a) before interaction and (b) after interaction with the base fluid containing 1% SMA/ SiO_2 .

3.3. Pore Structure Characterization of Shale

The plugging capacity of SMA/ SiO_2 was further determined through BET analysis, and the surface area and pore volume of shale samples were used as evaluation parameters. As presented in

Figure 11, the surface area of original shale without treatment was $15.51 \text{ m}^2/\text{g}$, with a pore volume of $0.02541 \text{ cm}^3/\text{g}$. After being soaked in deionized water, the surface area and pore volume of shale were increased to $19.64 \text{ m}^2/\text{g}$ and $0.03107 \text{ cm}^3/\text{g}$ respectively. The large increase in the surface area and pore volume indicated that water strongly interacted with shale, resulting in bigger pores and fractures in shale samples. The hydration and capillary effect are essential factors leading to the pores and fractures propagation in shale samples [47]. However, after being soaked in 1.0% SiO_2 solutions, the surface area and pore volume of shale were decreased to $13.42 \text{ m}^2/\text{g}$ and $0.02407 \text{ cm}^3/\text{g}$ respectively. In especial, a significant decrease was observed after being soaked in 1.0% SMA/ SiO_2 solutions, and the surface area and pore volume were reduced to $10.33 \text{ m}^2/\text{g}$ and $0.02186 \text{ cm}^3/\text{g}$ respectively. Results indicated that SMA/ SiO_2 was able to effectively plug the shale pores and fractures, and thus prevent water invading into shale samples.

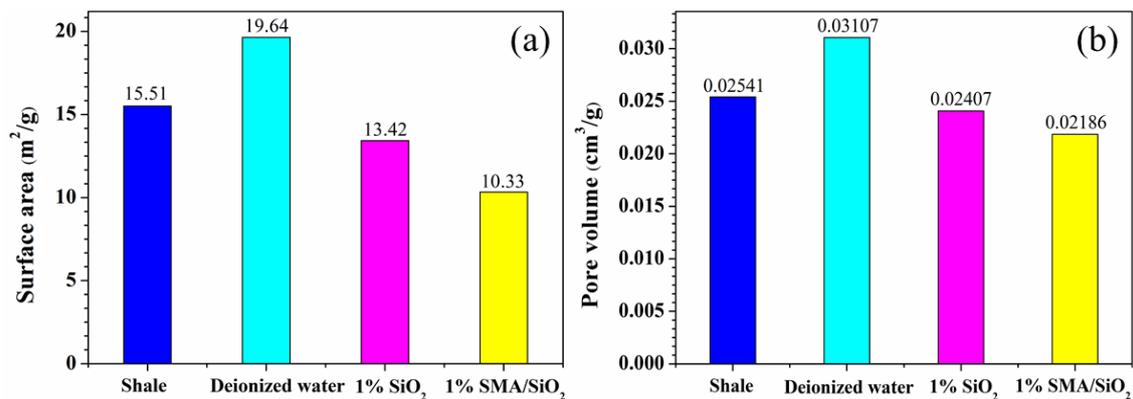


Figure 11. (a) The surface area and (b) pore volume of shale cores after soaked in different fluids.

3.4. Rolling Dispersion Experiment

In order to evaluate the hydration inhibition property of SMA/ SiO_2 , KCl and JHC as good shale inhibitors were used for comparison. The results of the rolling dispersion experiment were presented in Figure 12. The rolling recovery rate of shale in deionized water was 40.2%, demonstrating that the shale samples possessed strong hydration dispersion ability. This could be attributed to the high content of smectite in shale samples. With the increase in SMA/ SiO_2 dosage, the recovery rate was enhanced significantly. When the concentration of SMA/ SiO_2 was 2.0%, the shale recovery rate was up to 93.6%. In addition, compared with KCl, JHC and SiO_2 , the higher recovery rates were observed in SMA/ SiO_2 solutions at various concentrations. Therefore, SMA/ SiO_2 was able to reduce the tendency of shale dispersion and exhibited strong hydration inhibition. The results can be explained by the shale hydration inhibition mechanism of amphiphilic polymer [41]. The hydrophilic segments in SMA/ SiO_2 were capable of enhancing the adsorption between SMA/ SiO_2 and the shale, because shale is hydrophilic. Thus, SMA/ SiO_2 could occupy the adsorption sites in shale instead of water. As a result, the hydrophobic segments provided by St and MMA in the amphiphilic polymer could greatly change the wettability of shale. The shale surface became more hydrophobic after adsorbed by SMA/ SiO_2 , which was in favor of preventing the water invading into the shale. Therefore, the excellent hydration inhibition of SMA/ SiO_2 was achieved.

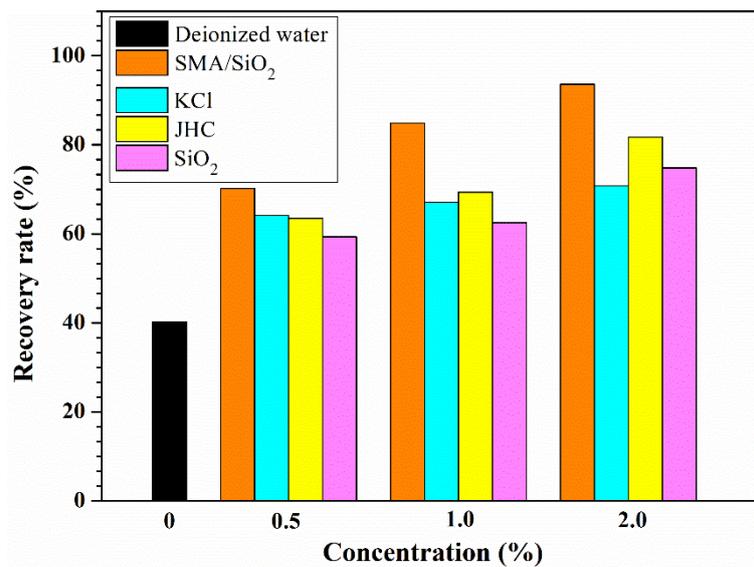


Figure 12. The results of rolling dispersion experiment.

3.5. Contact Angle Test Results

The influence of SMA/SiO₂ on the wettability of the shale surface was measured, and the test results were shown in Figure 13. The original shale was strongly hydrophilic with a contact angle of 34.4°. With the increase of SMA/SiO₂ concentration, the contact angle was gradually enlarged. After treatment with 2.0% SMA/SiO₂ solutions, the contact angle was increased to 72.7°. Thus, a more hydrophobic shale surface would be formed after treatment with SMA/SiO₂. Less water intrusion into the shale due to the hydrophobic surface was more conducive to the shale stability [48].

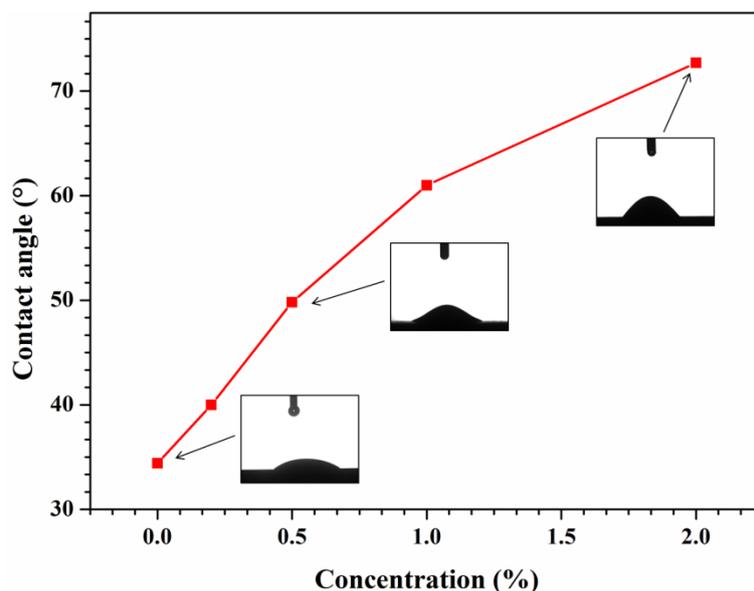


Figure 13. The results of contact angle test.

3.6. Probable Shale Stabilization Mechanism

A possible shale stabilization mechanism of SMA/SiO₂ could be summarized in view of the research findings from this work and some previous researches. Under the drilling pressure differential, the nanoparticles in SMA/SiO₂ are pressed into the nanopores and cracks in the shale. A plugging layer is formed on the shale, resulting in a lower pressure transmission rate and shale permeability.

Thus, the excellent plugging performance of SMA/SiO₂ is achieved. In addition, the hydrophilic segments in SMA/SiO₂ can enhance the adsorption between SMA/SiO₂ and the shale. After being adsorbed by SMA/SiO₂, a more hydrophobic shale surface will be obtained due to the hydrophobic segments in SMA/SiO₂, which can further prevent the water invading into the shale. As a result, SMA/SiO₂ exhibits good hydration inhibition. Overall, the novel shale stabilizer SMA/SiO₂ has the advantages of both physical plugging and chemical inhibition.

In addition, in order to further optimize the molecular structure of SMA/SiO₂ and explore its shale stabilization mechanism, more detailed statistical analysis and refined structural characterization will be carried out in our future work [49,50].

3.7. Compatible Test

Table 2 presents the effect of SMA/SiO₂ on the rheological and filtration control properties of the WBMs. After being hot-rolled at 120 °C for 16 h, SMA/SiO₂ only created slight variations on the rheological parameters of the WBMs. In addition, the fluid loss of the WBMs with 2.0% SMA/SiO₂ was decreased from 8.2 to 6.4 mL, indicating a significant filtration control performance of SMA/SiO₂.

Table 2. Effect of SMA/SiO₂ on the rheological and filtration control properties of the WBMs (water-based muds).

Parameter	Before adding SMA/SiO ₂	After adding 2.0% SMA/SiO ₂
θ at 600 rpm (lbf/100 ft ²)	70	74
θ at 300 rpm (lbf/100 ft ²)	44	46
AV (mPa.s)	35	37
PV (mPa.s)	26	28
YP (Pa)	9	9
YP/PV	0.35	0.32
FL _{API} (mL)	8.2	6.4

4. Conclusions

The following conclusions can be drawn from the current work:

(1) An amphiphilic polymer/nano-silica composite (SMA/SiO₂) was prepared and characterized as a novel shale stabilizer for water-based muds. The novel shale stabilizer SMA/SiO₂ with spherical structure mainly distributed in the range of 43–122 nm and exhibited good high-temperature resistance.

(2) SMA/SiO₂ could effectively plug the shale pores and cracks, and slow down the pressure transmission rate. After being plugged by SMA/SiO₂, the core surface changed to be smooth and dense, and an isolation layer was formed on it. In addition, a significant decrease of the shale surface area and pore volume were observed after treatment by SMA/SiO₂.

(3) SMA/SiO₂ also showed good hydration inhibition, which was better than KCl and JHC. The hydrophilic segments in SMA/SiO₂ could enhance the adsorption between SMA/SiO₂ and the shale, and thus the hydrophobic segments could change the shale surface to become more hydrophobic after being adsorbed by SMA/SiO₂, which was in favor of further preventing the water invading into the shale.

(4) The excellent performance of physical plugging and chemical inhibition were achieved, and SMA/SiO₂ was expected to be a novel shale stabilizer to solve shale instability problems.

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Nomenclature

WBMs	water-based muds
St	styrene
MMA	methyl methacrylate
AM	acrylamide
SMA	poly(St-MMA-AM)
KH570	3-methacryloxypropyltrimethoxysilane
SDS	sodium dodecyl sulfate
OP-10	octylphenol polyoxyethylene ether
SMA/SiO ₂	poly(St-MMA-AM)/nano-SiO ₂ composite
JHC	polymeric alcohol
FT-IR	Fourier transform infrared spectra
NMR	nuclear magnetic resonance
PSD	particle size distribution
TEM	transmission electron microscope
SEM	scanning electron microscopy
TGA	thermogravimetric analysis
AV	apparent Viscosity
PV	plastic viscosity
YP	yield Point
API	American Petroleum Institute
FL _{API}	fluid loss
K	shale permeability
μ	viscosity of fluids
β	static compression ratio of fluids
V	enclosed volume
L	length of shale core
A	cross-sectional area of shale core
t	experimental time
P_m	upstream pressure
P_o	initial downstream pressure
$P(L, t)$	realtime downstream pressure

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