

Article

Modelling Spray Pressure Effects on Droplet Size Distribution from Agricultural Nozzles

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Featured Application: A theoretical model that allows analyzing the effects of spray pressure on drop size distribution was devised. The model can be used to predict nozzle spray quality parameters under ordinary working conditions.

Abstract: For spray applications, drop size is the most important feature as it affects all aspects of a phytosanitary treatment: biological efficacy, environmental pollution, and operator safety. In turn, drop size distribution depends on nozzle type, liquid properties, and working pressure. In this research, three nozzles were studied under ordinary working conditions and the effect of pressure on drop size distribution was assessed. The nozzles under test, all from Albus (France), were an orange hollow cone nozzle ATR 80 (European color code), an air induction flat spray nozzle AVI 11003, and an air induction hollow cone nozzle TVI 8002. The ATR 80 and the TVI 8002 nozzles were tested at four pressure values: 0.3, 0.5, 1.0, and 1.5 MPa; the AVI 11003 nozzle was tested at 0.3 and 0.5 MPa. The drop size measurement technique was based on the liquid immersion method by using a custom-made test bench; spray quality parameters were computed by means of suitable functions written in R language. Results showed that an increase in working pressure caused an increase in drop pulverization regardless of the type of nozzle, and drop pulverization was higher for the turbulence nozzle than for the two air induction nozzles. Based on skewness and kurtosis values, the theoretical gamma distribution was the most adapt to fit the experimental data. The scale parameter showed a decreasing trend with the increase in the pressure, a clear index of higher drop pulverization.

Keywords: droplet pulverization; liquid immersion method; image analysis; ImageJ; gamma distribution



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1. Introduction

The application of Plant Protection Products (PPPs) is affected by many factors, among which drop size is the most important as it affects biological efficacy [1], environmental pollution [2,3], and operator safety [4–6]. In fact, the correct spray spectrum is capable of ensuring the required dose on the target, minimizing drift and ground losses, and reducing dermal and inhalation worker exposure. A research of Ferguson et al. (2016) [7] aimed at assessing spray deposit and canopy penetration of nozzles with different spray qualities in an oat canopy, showed that droplet number densities were inversely related to the droplet size produced by the nozzles, yet coverage was increased more by application volume rate than droplet size. Another study by Zwervaegher et al. (2014) [8] showed that drop size also affects spray retention, i.e., the overall capture of spray droplets by plants on initial or subsequent impact, so influencing efficacy, economic losses, and environmental contamination. The most known example of the environmental impact of pesticide application related to drop size is spray drift: small droplets are more easily deflected out of the target area by wind action [9]. The adoption of low-drift nozzles [10–12], sprayer calibration

by means of test benches [13–15], and direct or indirect drift measurement [16–19], are common practices to reduce spray drift.

To know the drop size distribution of nozzles under ordinary working conditions is, therefore, of great interest to guide the most appropriate choice in relation to target structure, liquid properties, and environmental conditions. Drop size measurement is based on several principles, both intrusive and non-intrusive.

Intrusive measurement techniques include the image analysis of the drop stains on water sensitive papers (WSPs) and the liquid immersion method. WSPs are semi-rigid papers, with one side covered with a special yellow film that turns deep blue when hit by a drop of water [20]. The analysis of stains by means of image processing software, under some limitations, allows sizing the drop diameters [21–25]. In the liquid immersion method, droplets are collected on Petri dishes containing lightly viscose liquids, such as Vaseline, light mineral oil, and silicone oil, which cause drops to form spherical shapes. They are immediately photographed or observed with a microscope, allowing drop counting and size measurement [26,27].

Non-intrusive methods include high speed imaging (HSI) [28–30], laser diffraction (LD) [31–33], and Phase Doppler Particle Analyzers (PDPA) [34–36]. HSI and PDPA methods also allow measuring of drop velocity.

Each measurement technique gives results that are significantly different, depending on measuring protocol, settings, and type of measuring equipment [35,37,38], so much so that the international standard ISO 25358:2018 [39] recommends basing nozzle classification on comparison with reference nozzles.

In this study, a low-cost custom-made system that allows measuring of the drop size of agricultural spray nozzles under ordinary working conditions was used. The design of the equipment was mainly based on the ISO 5682-1 standard [40], which exploits the liquid immersion method. Three nozzles were tested, all from Albus (France): an orange hollow cone nozzle ATR 80 (European color code), an air induction flat spray nozzle AVI 11003, and an air induction hollow cone nozzle TVI 8002. The ATR 80 and the TVI 8002 nozzles were tested at four pressure values: 0.3, 0.5, 1.0, and 1.5 MPa; the AVI 11003 nozzle was tested at 0.3 and 0.5 MPa. For each test condition, the usual spray parameters were computed: the arithmetic mean diameter, the Sauter mean diameter, the volumetric diameters D_{v10} , D_{v50} , and D_{v90} , and the Relative Span Factor (RSF). Finally, the theoretical drop size distribution that best fitted the experimental data was devised and the effects of spray pressure were analyzed.

2. Materials and Methods

2.1. The Test Bench for Drop Size Measurement

The test bench used for spray drop size measurement is fully described in [41,42], here summarized for completeness. The design was based on the ISO 5682-1 standard [40], exploiting the liquid immersion method to measure droplet size [26,27]. The hydraulic circuit was designed to reproduce the circuit installed on commercial sprayers. A two-diaphragm pump (AR 30, Annovi Reverberi, Reggio Emilia, Italy), driven at 56 rad/s (540 rpm) by a 2.2 kW AC motor with a gearbox, was used to provide the required pressure at the nozzle under test. The fluid in excess was recirculated into the 70 L main tank by means of a manual pressure regulator. Pressure near the nozzle and liquid flow rate were measured in real time by a pressure transmitter (Series 22 S, Keller Italy Srl, Milano, Italy) and a flow rate meter (SF800-6, Swissflow BV, The Netherlands). The two sensor signals were acquired by two Advantech Ethernet modules (ADAM6024 and ADAM6060). An ASCII UDP based protocol was used for communication with host PC, where a specifically designed user interface was running.

The nozzle under test was anchored to a mobile platform, capable of translating along two 3 m long rails while spraying above the target plane at a distance of 0.5 m. The motion was handled by a motor control unit (MDC1460 model, Roboteq Inc., Scottsdale, AZ, USA), capable of controlling position, speed, and acceleration profiles.

The software user interface, running on a Windows 10 PC, was designed to allow the management of all the aspects of the spray trials, including data save in a text Comma Separated Value (CSV) file. A schematic view of the whole system is reported in Figure 1.

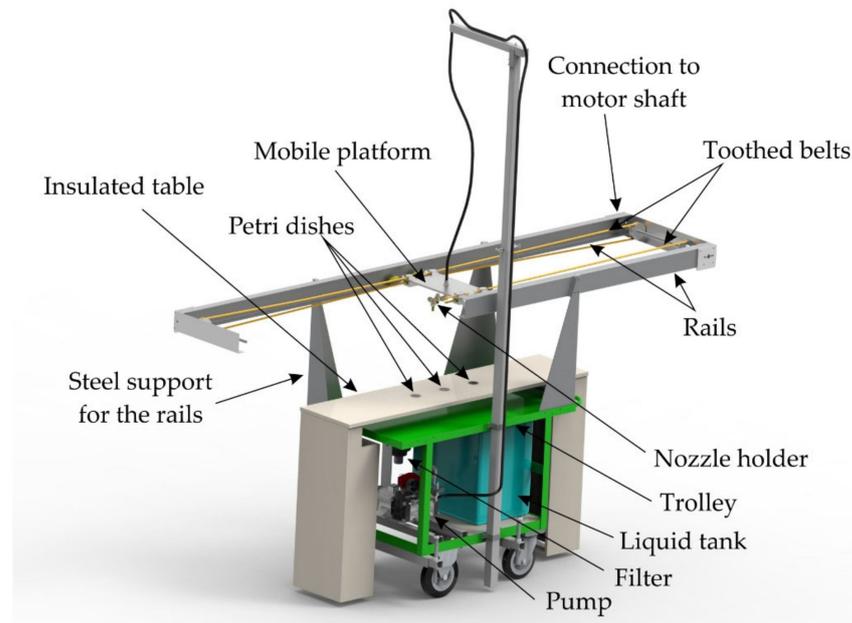


Figure 1. Scheme of the test bench for drop size measurement.

Sprayed droplets were captured by Petri dishes containing silicone oil as immersion liquid positioned on the target plane and then photographed in situ by a high resolution (4000×6000 pixel) Digital Single-Lens Reflex (DSLR) camera (Nikon D5500, Nikon Corporation, Tokyo, Japan), equipped with a macro lens (Nikon Micro Nikkor AF-S 60 mm f/2.8 G ED, Nikon Corporation, Tokyo, Japan) and an electronic flash (Neezer 48 Macro LED Ring Flash, Shenzhen, Guangdong, China). Images, saved as high-quality JPEG files, were then analyzed by means of an image processing software, capable of detecting and measuring the size of all the drops.

2.2. The Experimental Trials

Spraying tests were carried out using three Albus (France) commercial nozzles: an orange hollow cone nozzle ATR 80 (European color code), an air induction flat spray nozzle AVI 11003, and an air induction hollow cone nozzle TVI 8002. The ATR 80 and the TVI 8002 nozzles were tested at four pressure values: 0.3, 0.5, 1.0, and 1.5 MPa; the AVI 11003 nozzle was tested only at 0.3 and 0.5 MPa to respect its working range.

All tests were carried out at the same velocity of the mobile platform: 1.5 m/s. Spray droplets were captured by means of three Petri dishes, with diameter of 55 mm, aligned with the movement direction of the nozzle, spaced 195 mm apart. Each Petri dish contained 5 mL of silicone oil (AR200, Sigma-Aldrich, Milan, Italy) with dynamic viscosity of 200 mPa·s and volumetric mass of 1050 kg/m^3 . A water solution containing 2 g/L of the coloring agent red Ponceau (Novema Srl, Turin, Italy) was sprayed as test liquid; the red color of the solution facilitated the subsequent image segmentation process to identify the droplets with respect to the background (Figure 2). In these first trials, the surface tension of liquid was not measured.

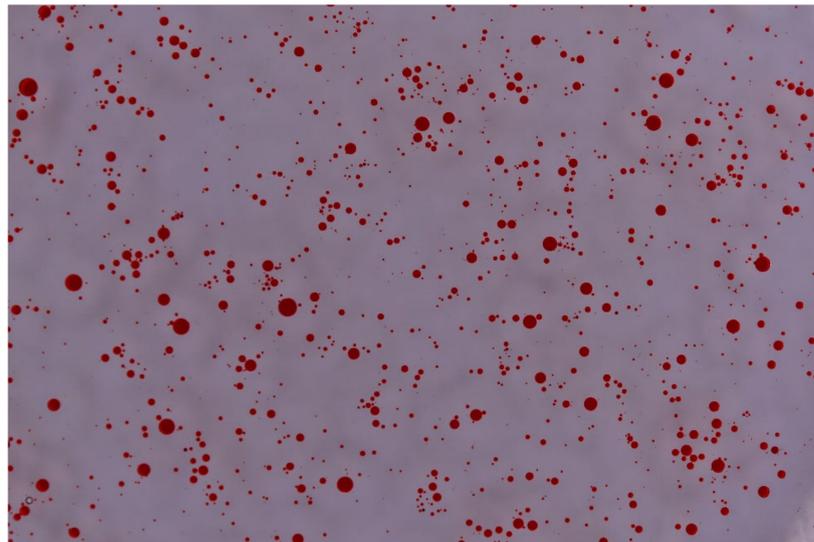


Figure 2. Example of image with droplets.

Photos were taken without moving the Petri dishes and immediately after each spraying test. To this end, the camera was applied to a metallic frame, which in turn was manually hung to the rails in fixed positions with respect to the Petri dishes (Figure 3). The camera was remotely controlled via the qDslrDashboard Version 3.5.3 application (<http://dslrdashboard.info>, accessed on 26 April 2018) running on an Android tablet. Three repetitions were carried out for each test condition (nozzle type \times spraying pressure), for a total of 90 photos.



Figure 3. The camera applied to the rails above a Petri dish.

In addition, some photos of a 10×10 mm grid pattern engraved on a glass disc, placed in correspondence with the three Petri dish positions, as far from the camera focal plane as the drops, were used to calibrate the measurement system and to calculate the calibration factor C_f expressed in $\mu\text{m}/\text{pixel}$.

2.3. Spray Parameters Calculation

The images with the droplets were processed with the ImageJ analysis software, ver. 1.52a [43]. They were first converted in 8-bit gray scale images and then segmented to detect the droplets with respect to the background. After segmentation, the watershed binary filter was applied to separate some touching particles. Particles up to 4 contiguous pixels were considered as noise and then ignored.

Among the numerous characteristic parameters provided by the software for the i -th identified particle, only the area A'_i (pixel) was considered. Assuming that the droplet was a sphere and that it was not deformed by the silicone oil, its diameter D'_i (pixel) was calculated according to Equation (1)

$$D'_i = \sqrt{\frac{4A'_i}{\pi}} \quad (1)$$

The distance in pixel provided by Equation (1) was then converted in real world distance by applying the measured calibration factor C_f ($\mu\text{m}/\text{pixel}$)

$$D_i(\mu\text{m}) = C_f(\mu\text{m}/\text{pixel}) \cdot D'_i(\text{pixel}) \quad (2)$$

Knowing the diameter of all the N droplets detected in each repetition, the following mean diameters were calculated:

Arithmetic mean diameter

$$D_{10} = \frac{\sum_{i=1}^N D_i}{N} \quad (3)$$

Surface mean diameter

$$D_{20} = \sqrt{\frac{\sum_{i=1}^N D_i^2}{N}} \quad (4)$$

Volume mean diameter

$$D_{30} = \sqrt[3]{\frac{\sum_{i=1}^N D_i^3}{N}} \quad (5)$$

Sauter mean diameter (SMD)

$$D_{32} = \frac{\sum_{i=1}^N D_i^3}{\sum_{i=1}^N D_i^2} \quad (6)$$

Other diameters, usually adopted to classify agricultural nozzles in terms of spray quality, were computed with reference to the volume of liquid carried by the droplets. Given a droplet with diameter D_i (μm), its volume V_i (μm^3) was calculated according to Equation (7)

$$V_i = \frac{\pi}{6} D_i^3 \quad (7)$$

Sorting the droplets in increasing order by their diameter, the cumulative volume CV_{D_h} (%) corresponding to the diameter D_h was calculated according to Equation (8)

$$CV_{D_h} = \frac{\sum_{i=1}^h V_i}{V_T} \times 100 \quad (8)$$

V_T being the total volume carried by all the N droplets. Knowing the cumulative volume, the following volumetric diameters were computed:

D_{v10} : the diameter such that $CV_{D_{v10}} = 10\%$;

D_{v50} : the diameter such that $CV_{D_{v50}} = 50\%$, also known as Volumetric Median Diameter (VMD);

D_{v90} : the diameter such that $CV_{D_{v90}} = 90\%$.

In general, the volumetric diameter $D_{v\alpha}$ is the diameter such that the $\alpha\%$ of the total volume is carried by droplets with diameter lower than $D_{v\alpha}$. These diameters, especially the VMD, are used to classify the nozzles in terms of drop pulverization. An index of uniformity of the spray is provided by the Relative Span Factor (RSF, %)

$$\text{RSF} = \frac{D_{v90} - D_{v10}}{D_{v50}} \times 100 \quad (9)$$

All diameters were calculated for each repetition, considering the three Petri dishes together in such a way to have a significant drop sample (at least 2000 droplets), and mean values were reported. The calculations were carried out by means of custom functions written in R language, ver. 3.6.3 [44].

2.4. Drop Size Distribution Modelling

Drop size can be described by means of a suitable probability density function (PDF) of the number or the volume of the drops in function of the diameter. In a spray consisting of N_T drops, denoting the PDF of the drop number with $f_0(D)$, the quantity $N_T f_0(D)dD$ represents the number of drops whose diameter is between D and $(D + dD)$. Several PDFs have been proposed in the spray literature to describe the drop size distribution, among which the normal, the log-normal, the Rosin-Rammler, the Weibull, and the gamma [45–47]. In this study, the experimental data were analyzed, and the theoretical distribution, from those mentioned above, that best described them was devised, adjusting its parameters according to the operating conditions. The theoretical study of the atomization process as a function of nozzle characteristics, liquid properties, and test conditions is outside the scope of the research.

Based on skewness and kurtosis values of measured drop diameters, the theoretical distribution most suitable for fitting experimental data was the gamma distribution. The probability density function of the gamma distribution has the general form of Equation (10)

$$f(x) = \frac{1}{\beta^\alpha \Gamma(\alpha)} x^{\alpha-1} e^{-x/\beta} \quad (10)$$

defined for $x \geq 0$, $\alpha > 0$, and $\beta > 0$; α is the shape parameter, β is the scale parameter, and $\Gamma(z)$ is the gamma function, defined as

$$\Gamma(z) = \int_0^\infty t^{z-1} e^{-t} dt \quad (11)$$

Both shape and scale parameters affect the probability density and the cumulative distribution function (CDF) as shown in Figures 4 and 5.

In this study, the shape and scale parameters were estimated for each nozzle and working pressure by using the R package *fitdistrplus* ver 1.1-5 [48] and applying the Maximum Likelihood Estimation (MLE) method. In addition, their confidence interval was computed based on the bootstrap method. Goodness of fit was assessed by means of the Anderson–Darling (AD) test.

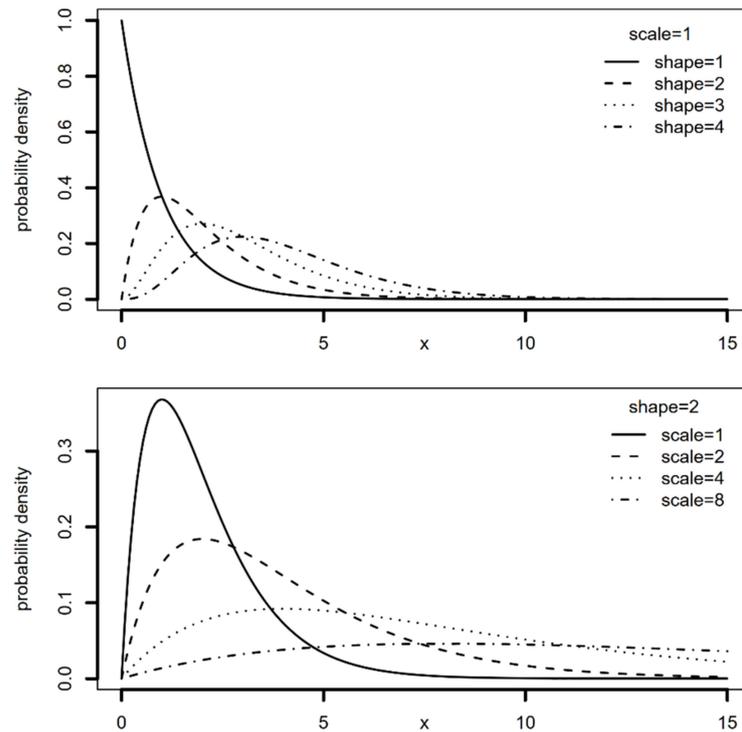


Figure 4. Effect of the scale and shape parameter on the gamma probability density function.

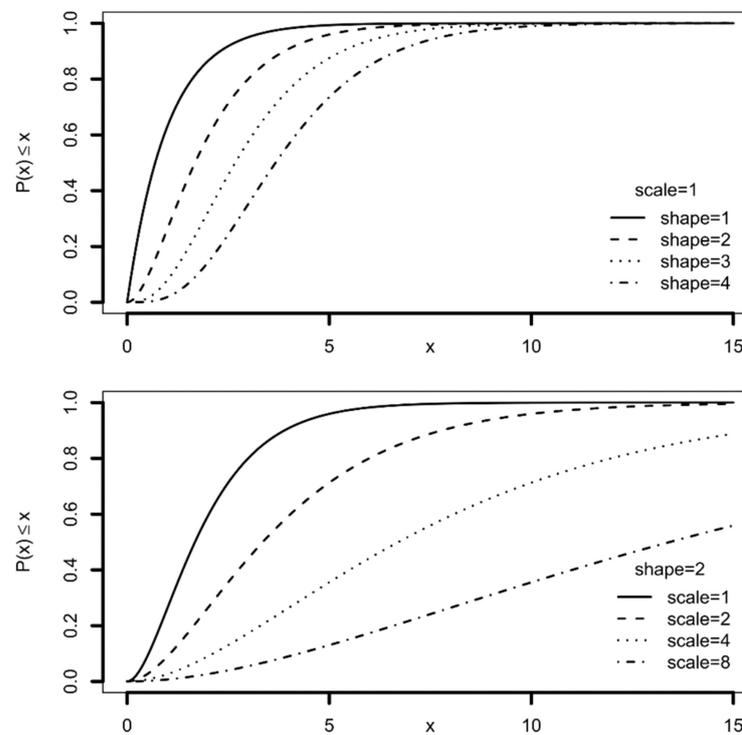


Figure 5. Effect of the scale and shape parameter on the gamma cumulative distribution function.

3. Results

3.1. General Results

Table 1 summarizes the nozzle flow rate values measured during the tests as affected by spraying pressure.

Table 1. Nozzle flow rate values in function of spraying pressure.

Nozzle Type	Measured Pressure, MPa	Measured Flow Rate, L/min	Reference Pressure, MPa	Reference Flow Rate, L/min
ATR 80 orange	0.311	0.78	0.3	
	0.517	0.98	0.5	0.99
	0.988	1.37	1.0	1.39
	1.445	1.64	1.5	1.69
TVI 8002	0.306	0.80	0.3	
	0.518	1.05	0.5	1.03
	1.031	1.47	1.0	1.46
	1.484	1.76	1.5	1.79
AVI 11003	0.296	1.18	0.3	1.20
	0.500	1.53	0.5	1.55

According to the nozzle manufacturer information, the relative deviations with respect to the nominal flow rates are always lower than the relative tolerance of $\pm 5\%$ admitted by the ISO 10625 reference [49].

The average resolution value of the image analysis system was 188.3 pixel/mm, ranging from 185.7 to 191.2 pixel/mm. The corresponding average calibration factor C_f was 5.31 $\mu\text{m}/\text{pixel}$, ranging from 5.23 to 5.39 $\mu\text{m}/\text{pixel}$. On average, to neglect particles lower than 5 contiguous pixels means neglecting drops with a diameter lower than 12 μm , and this can be considered an acceptable approximation with the used measurement system.

3.2. Drop Size Parameters

Table 2 summarizes the characteristic diameters of the sprays as affected by nozzle type and working pressure.

Table 2. Average characteristic diameters of the sprays (diameters in μm , RSF in percent).

Pressure, MPa	D_{10}	D_{20}	D_{30}	D_{32}	D_{v10}	D_{v50}	D_{v90}	RSF
ATR 80 orange								
0.3	81	97	112	150	94	174	263	97
0.5	70	83	95	126	79	147	236	107
1.0	57	69	82	115	70	138	227	114
1.5	54	67	79	112	66	136	220	113
TVI 8002								
0.3	195	293	391	695	440	861	1345	105
0.5	166	229	295	489	286	624	995	114
1.0	148	194	240	368	212	457	736	115
1.5	130	173	216	334	195	415	662	113
AVI 11003								
0.3	147	201	254	407	239	506	807	112
0.5	101	145	193	343	194	449	731	120

Results were consistent with expectations: in fact, drop pulverization was higher for the turbulence nozzle than for the two air induction nozzles. As an example, at the pressure of 0.5 MPa, VMD was 147 μm for the ATR 80 orange, 624 μm for the TVI 8002, and 449 μm for the AVI 11003 nozzle. In addition, all diameters were affected by pressure: an increase in the spraying pressure caused an increase in the drop pulverization, regardless of the type of nozzle. When the pressure increased from 0.3 to 1.5 MPa, VMD decreased by 21.8% for the ATR 80 (from 174 to 136 μm) and by 51.8% for the TVI 8002 (from 861 to 415 μm). The reduction in VMD for AVI 11003 was 11.3% (from 506 to 449 μm) when the pressure

increased from 0.3 to 0.5 MPa. Relative Span Factor values generally increased when the pressure increased for all nozzles, a sign of a lower uniformity in drop size distribution.

The effects of spray pressure on cumulative volumetric curves are shown in Figure 6 in function of drop diameters and nozzle types. The graph was obtained by considering all the drops of all repetitions. The effect of pressure on the hollow cone ATR 80 nozzle was more evident when the pressure increased from 0.3 to 0.5 MPa (VMD decreased from 174 to 147 μm), whereas above 0.5 MPa the cumulative volumetric curves were almost superimposed (VMD decreasing from 147 to 136 μm only). Instead, the cumulative volumetric curves were clearly distinct for the air induction nozzles, as well as the volumetric diameters.

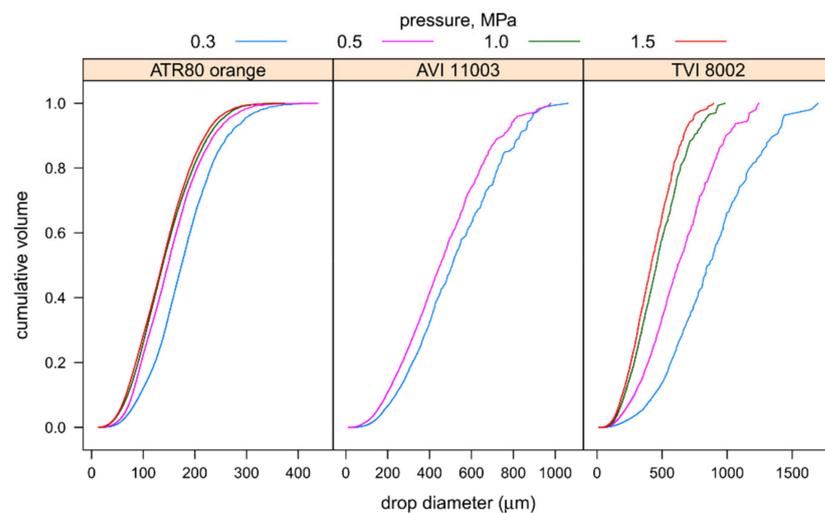


Figure 6. Cumulative volumetric droplet size distribution as affected by nozzle type and working pressure (data of all repetitions).

3.3. Drop Size Distribution Modelling

Table 3 reports the shape and scale parameters together with the 95% confidence interval for their median values and the results of the Anderson–Darling goodness of fit test in function of spray pressure and for each nozzle type.

Table 3. Shape and scale parameters of gamma distribution.

Pressure, MPa	Shape Parameter and 95% Confidence Interval of the Median			Scale Parameter and 95% Confidence Interval of the Median			AD Test p-value
	α	2.5%	97.5%	β	2.5%	97.5%	
ATR 80 orange							
0.3	2.3319	2.3101	2.3609	34.3492	33.9444	34.7725	0.2060
0.5	2.5450	2.5248	2.5720	27.4295	27.1150	27.7032	0.2043
1.0	2.4367	2.4205	2.4486	23.1820	23.0522	23.3008	0.0006
1.5	2.4511	2.4394	2.4626	22.1915	22.0771	22.3346	0.0006
TVI 8002							
0.3	1.1703	1.1344	1.2068	166.3876	160.1959	173.6039	0.0506
0.5	1.4243	1.3825	1.4638	116.5647	112.6313	120.4293	0.2788
1.0	1.5321	1.4890	1.5704	96.5119	93.5747	99.5777	0.4038
1.5	1.5101	1.4829	1.5482	86.3048	84.2055	87.8912	0.2655
AVI 11003							
0.3	1.3864	1.3524	1.4267	104.8953	101.6836	108.2892	0.2418
0.5	1.4305	1.4029	1.4475	70.3632	69.0494	71.9837	0.0114

For each nozzle type, the shape parameter was almost constant in function of the spray pressure. The 95% confidence interval for the median ranged from 2.310 to 2.572 for the ATR 80 orange nozzle, from 1.134 to 1.570 for the TVI 8002, and from 1.352 to 1.447 for the AVI 11003. On the contrary, the scale parameter was clearly decreasing when the pressure increased: from 34.349 (0.3 MPa) to 22.077 (1.5 MPa) for the ATR 80 orange nozzle, from 166.388 (0.3 MPa) to 86.305 (1.5 MPa) for the TVI 8002, and from 104.895 (0.3 MPa) to 70.363 (0.5 MPa) for the AVI 11003. The decreasing trend of the scale parameter with the increase in the pressure is an index of the higher drop pulverization (more drops of a lower diameter, Figures 4 and 5).

The comparison between the three nozzles in terms of probability density functions and cumulative distribution functions when varying the spray pressure is shown in Figures 7–9. According to the results of the AD test (Table 3), the best fitting was obtained for the nozzle TVI 8002 at every pressure, for the ATR 80 up to 0.5 MPa, and for the AVI 11003 at 0.3 MPa. As a general result, the gamma distribution tends to underestimate the number of drops smaller than 100 μm .

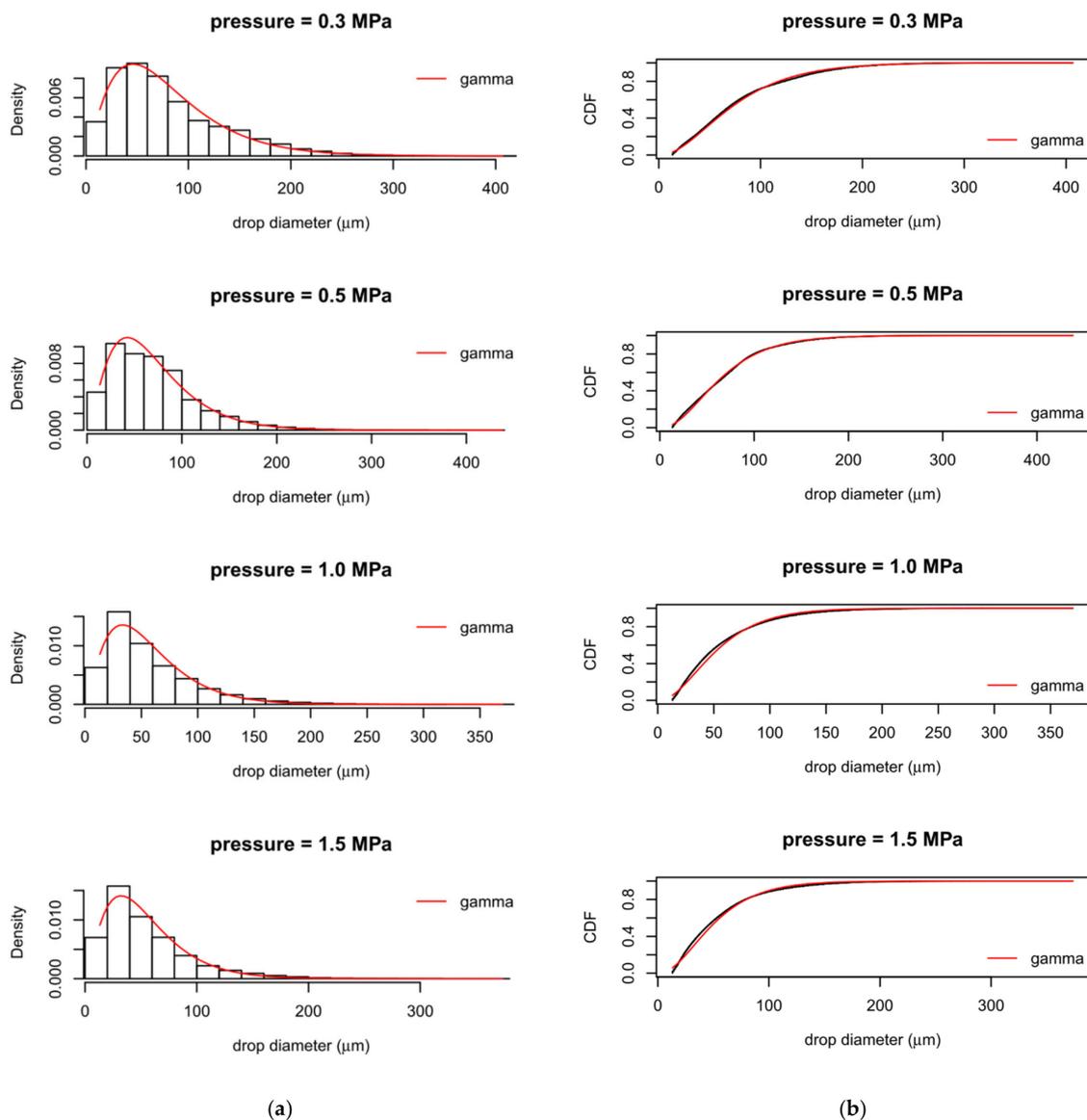


Figure 7. Comparison between measured and theoretical distribution for the ATR 80 orange nozzle. (a) Histograms and theoretical densities; (b) Empirical and theoretical cumulative distribution functions.

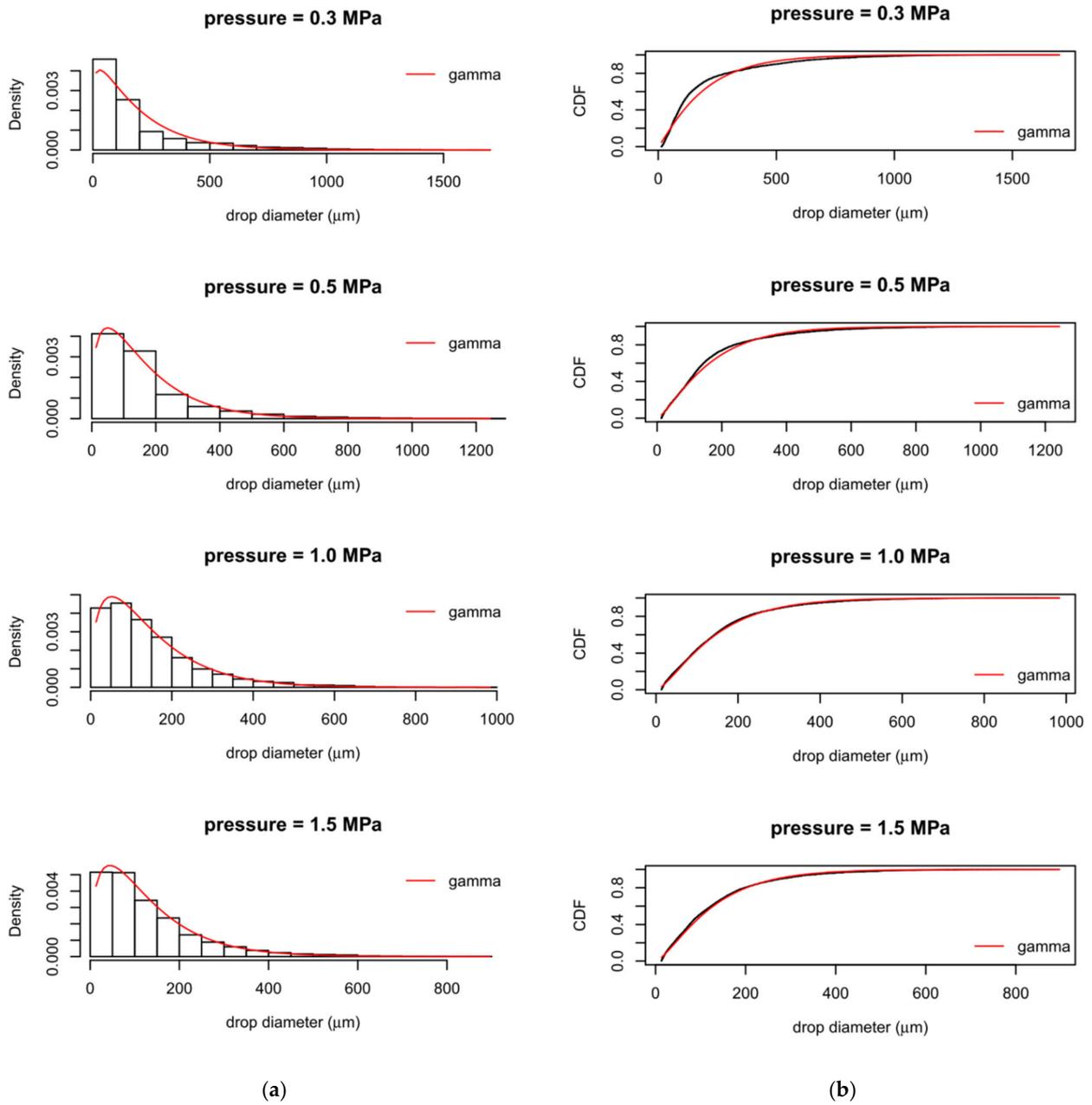


Figure 8. Comparison between measured and theoretical distribution for the TVI 8002 nozzle. (a) Histograms and theoretical densities; (b) Empirical and theoretical cumulative distribution functions.

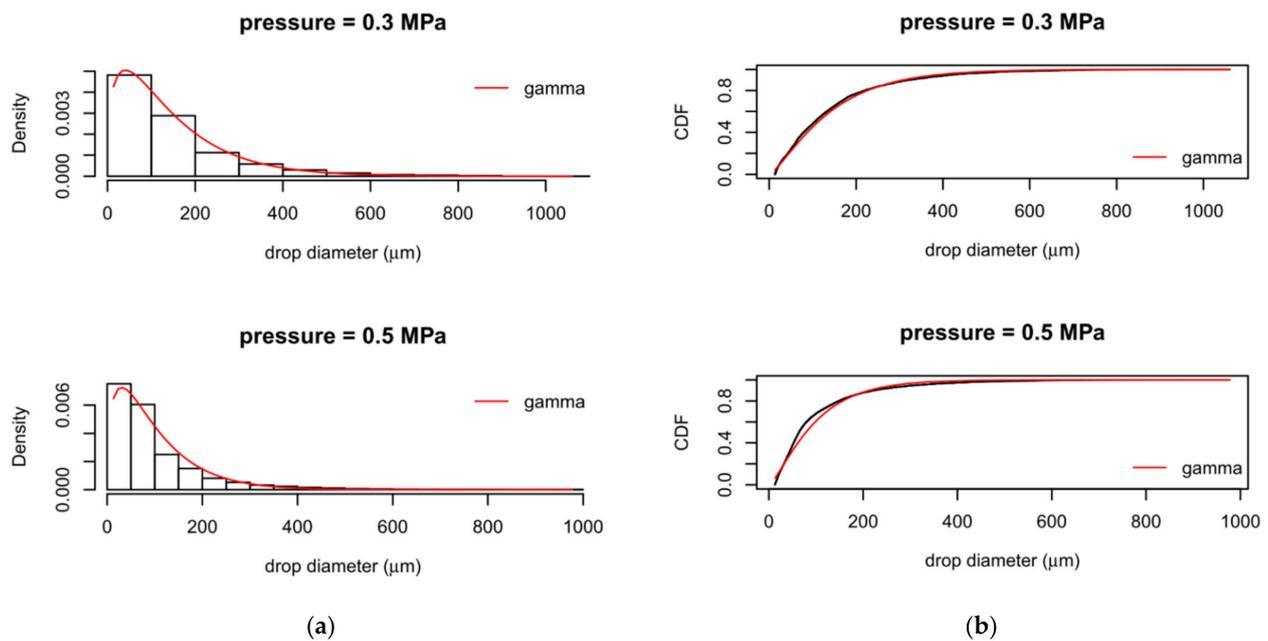


Figure 9. Comparison between measured and theoretical distribution for the AVI 11003 nozzle. (a) Histograms and theoretical densities; (b) Empirical and theoretical cumulative distribution functions.

4. Discussion

4.1. Drop Diameters

Measuring drop diameters in a spray is a very complex task that has been addressed in different ways and exploiting different techniques and physical principles. Unfortunately, each measurement technique may produce different results. As an example, a study aimed at comparing four different methods for measuring droplet size distributions (image analysis, custom-made stroboscopic imaging, PDPA, and laser diffraction), reported that the larger the droplets, the bigger the differences are between the results [38]. Another study [35] focused on 17 bibliographic references about the results obtained by testing reference nozzles, pre-screened for laboratory purposes, reported a wide range of absolute measurements: when median values of D_{v50} increased from about 140 to about 395 μm , the interquartile range was on average 24% of the median values (from 20 to 33%). Despite this wide range of results, nozzle classification in terms of spray quality was identical in 73% of the cases, and this quite uniform classification confirms the usefulness of the reference nozzles.

The results obtained in this study by applying the liquid immersion method almost always agree with manufacturer information (Albus catalog 2016) about spray quality based on VMD. In fact, ATR 80 orange nozzles are classified as Very Fine (VMD < 159 μm) at pressures greater or equal than 0.5 MPa (the measured VMD was 147 μm at 0.5 MPa and lower for higher pressures); TVI 8002 nozzles are classified as Ultra Coarse at 0.5–0.7 MPa (VMD > 553 μm , measured VMD = 624 μm at 0.5 MPa), Extremely Coarse at 1.0 MPa (484 μm < VMD < 553 μm , measured VMD = 457 μm) and Very Coarse at 1.5 MPa (386 μm < VMD < 484 μm , measured VMD = 415 μm); finally, AVI 11003 nozzles are classified as Extremely Coarse at 0.3 MPa (measured VMD = 506 μm) and Coarse at 0.5 MPa (326 μm < VMD < 386 μm , measured VMD = 449 μm). These results will be further investigated in future researches by also measuring the drop size distributions produced by the reference nozzles used to define the boundary regions, as recommended by the standard ISO 25358:2018 [39].

No other measurement techniques were used to compare the results. However, Nuyttens et al. (2007) [35], using a PDPA system, reported for the ATR 80 orange nozzle at 0.3 MPa diameter values on average 15% greater than the actual ones (VMD = 191 μm vs. 174 μm), whereas Grella et al. (2017) [17] reported, for the same nozzle at 1.0 MPa,

a VMD value of 95 μm measured with a laser diffraction system compared with 138 μm obtained in this research. In both cases, despite the discrepancies in absolute results, the nozzle classification remained unchanged. In the same paper [17], a VMD of 606 μm was reported for the TVI 8002 nozzle at 1.0 MPa (vs. 457 μm obtained in this research), outside of the bounds of classification of the nozzle as Extremely Coarse. These results confirm the need to use the reference nozzles for classification purposes.

4.2. Drop Size Distribution

Modeling drop size distribution has been addressed via both empirical and analytical approaches. According to the first approach, suitable curves are fitted to measured data for a wide range of nozzles and operating conditions. This has led to the proposal of various theoretical distribution functions, such as Weibull, log-normal, Nukiyama–Tanasawa, gamma, able to fit experimental data more or less well and describe, as accurately as possible, the spray drop characteristics in terms of size and velocity [45,47,50].

The empirical approach was also adopted in this study: experimental data on drop diameters were analyzed and the theoretical gamma distribution was devised as the method that best described them. The scale and shape parameters were computed by means of the Maximum Likelihood Estimation method for each operating condition (nozzle type and spraying pressure). According to Villermaux et al. [51], the atomization process involves the fragmentation of ligaments into droplets, and the size distribution that reasonably fits the data is precisely the gamma probability distribution function.

The major drawback of this approach is the difficulty or the impossibility of covering conditions different from those observed. The analytical approach tries to predict the drop size distribution from an atomizer based on statistical/stochastic models such as the maximum entropy method [52,53] or general laws of conservation (mass, energy, momentum) [54,55]. In [54,55] the authors propose a closed-form equation capable of predicting the D_{32} diameter in function of liquid properties and droplet velocities, especially useful for the study of injectors used in combustion processes. Other formulae for estimating the D_{32} diameter in combustion studies are discussed in [56], including both empirical and physical principles.

Theoretical atomization models for agricultural spray nozzles used for pesticide applications are rare in the literature. Many studies are aimed at the measurement of drop diameters, at the tracing of the cumulative volumetric curves (Figure 6), and at the calculation of VMD, used for nozzle classification in terms of spray quality. In [57] the authors analyzed the influence of the spray parameters (spray angle, pressure, equivalent orifice diameter of nozzles) on drop size and velocity in the flow field. Suitable models were devised and successfully validated. Another work [58], using dimensional analysis, proposed a model to predict the volume median diameter of flat fan sprays in terms of common end-user parameters, namely nozzle size and operating pressure. However, in all cases, the models contain constants that must be estimated from experimental data.

5. Conclusions and Future Developments

The experimental activity allowed assessing the effect of spray pressure on drop pulverization in three Albus nozzle types (ATR 80 orange, AVI 11003, TVI 8002). The research, aimed at describing the experimental data and not the theoretical atomization process, as is common practice in the studies of nozzles for pesticide applications, produced results, especially in terms of volume median diameter, consistent with the expectations, with the nozzle manufacturer information, and with similar data found in the literature. Drop pulverization was higher for the turbulence nozzle than for the two air induction nozzles at every pressure, and an increase in the spraying pressure caused an increase in the drop pulverization, regardless of the type of nozzle. Thus, even if further experiments are necessary, the results validated the functionality of the proposed measurement system.

As regards the drop size distribution, the number probability distribution function that best described the experimental data was the gamma, whose scale and shape parameters

were adjusted in the function of nozzle type and spray pressure. The shape parameter was almost constant for each nozzle, while the scale parameter showed a clear decreasing trend with the increase in pressure, an index of higher drop pulverization. This aspect will be further investigated in future research considering other nozzle types, including the reference nozzles, and other pressures, in such a way as to extend the present results to a model able to reasonably estimate the drop size distribution and the most significant diameters in function of the operating conditions.

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Abbreviations

Symbols

A'_i	particle area (pixel)
D'_i	particle diameter (pixel)
D_i	particle diameter (μm)
C_f	calibration factor ($\mu\text{m}/\text{pixel}$)
D_{10}	arithmetic mean diameter (μm)
D_{20}	surface mean diameter (μm)
D_{30}	volume mean diameter (μm)
D_{32}	Sauter mean diameter (μm)
V_i	droplet volume (μm^3)
CV_{D_h}	cumulative volume corresponding to the diameter D_h (%)
D_{v10}	the diameter such that $CV_{D_{v10}} = 10\%$
D_{v50}	the diameter such that $CV_{D_{v50}} = 50\%$
D_{v90}	the diameter such that $CV_{D_{v90}} = 90\%$
$f_0(D)$	probability distribution function of the drop number
$\Gamma(z)$	gamma function
$\alpha > 0$	shape parameter
$\beta > 0$	scale parameter

Acronyms

AD	Anderson–Darling test
CDF	Cumulative Distribution Function
CSV	Comma Separated Value
DSLr	Digital Single-Lens Reflex
HSI	High Speed Imaging
LD	Laser Diffraction
MLE	Maximum Likelihood Estimation method
PDF	Probability Density Function
PDPA	Phase Doppler Particle Analyzer
PPP	Plant Protection Product
RSF	Relative Span Factor
SMD	Sauter Mean Diameter
VMD	Volumetric Median Diameter
WSP	Water Sensitive Paper

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