

Article

Additives to Coal-Based Fuel Pellets for the Intensification of Combustion and Reduction in Anthropogenic Gas Emissions

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Abstract: Cylinder-shaped fuel pellets that were 3 mm in diameter and 3 mm in height, with a mass of 20 mg, were produced by compressing dry coal processing waste under the pressure of 5 MPa. The first group of pellets from coal dust with a particle size less than 140 µm did not contain any additives. The pellets of the second group of fuel compositions contained an oil-impregnated porous polymer material particle with a size of 0.5 mm in the central part of the experimental sample. The particle was surrounded by coal dust from all sides. The ratio of components was 90:10% for coal dust: polymer particle. The latter value almost completely corresponds to the fraction of oil in the fuel composition, since the mass of a porous polymer material particle is negligible. The third group of compositions was a 70:30% mixture of coal dust with wood sawdust with a particle size less than 45 µm, or 45–100, 100–200 and 200–500 µm. The ignition and combustion of single fuel pellets were studied under radiant heating in an air medium while varying the temperature from 800 to 1000 °C. The processes during the fuel combustion were recorded by a high-speed video camera, and the concentrations of the main anthropogenic emissions in flue gases were measured by a gas analyzer. The main characteristics were established—ignition delay times (2–8 s) and duration of burnout (40–90 s)—at different heating temperatures. A difference was established in the combustion mechanisms of the pellets, when adding various components to the fuel mixture composition. This has a direct influence on the induction period duration and combustion time, other conditions being equal, as well as on the concentration of nitrogen and sulfur oxides in the flue gases. Adding an oil-impregnated porous polymer particle to the fuel composition intensifies ignition and combustion, since the times of ignition delay and complete burnout of fuel pellets under threshold conditions decrease by 70%, whereas adding wood sawdust reduces the content of nitrogen and sulfur oxides in the flue gases by 30% and 25%, respectively.

Keywords: fuel pellets; coal waste; wood sawdust; oil waste; combustion; anthropogenic emissions

1. Introduction

The current development of the global economy leads to a steady growth of energy consumption [1], which is conditioned not only by an increase in the population, but also by the annual growth of energy consumption per capita (from 72 to 76 GJ per capita during the last 10 years). Solid fossil fuel is one of the main energy resources, accounting for more than 35% of primary energy in the structure of global energy generation [2]. The extensive usage of coal is promoted by its rather low and stable cost,

abundance of deposits, and vast stocks in many regions of the world. According to expert estimates, the global stocks of coal were over 1054 billion tons by the end of 2018 [1]. The global consumption of coal has risen by 68% in the last 30 years [2,3]. This is caused not only by a greater amount of energy, generated by coal-fired thermal power plants, and energy consumption by different industries, but also by a wide use of coal as a raw material in the metallurgical, chemical, and construction industries [4–6].

One of the negative implications of large-scale coal mining and consumption is that a large amount of coal processing waste is accumulated in the landfills of coal washing plants; it has not been reclaimed for industrial application up until recently [7]. Such waste is referred to as a filter cake (FC). It is a slurry of fine coal dust (80–140 μm) and water (40–50%). Coal processing waste is normally stored at open-air disposal sites, thus, being exposed to strong impact of natural factors (wind, sun, and air). Storing it this way causes moisture to evaporate, while wind scatters coal dust onto the surrounding areas, polluting the land and water bodies, suitable for agricultural purposes, with acid-forming substances and heavy metals [5]. Moreover, dry fine coal dust can ignite spontaneously [8–10], therefore, the industrial landfills of FC are fire hazardous for coal washing plants and nearby populated areas.

One way to diminish the impact of such waste on the environment and to satisfy the growing needs of thermal power engineering for energy resources is to involve low-grade solid fuels and coal processing waste as resources into the energy industry [11,12]. At the initial stage of solving this problem, it is a promising approach to develop composite compositions based on FC with the addition (if necessary) of some amount of solid or liquid components to enhance energy performance [13,14], and environmental [15–18], characteristics, as well as for the production of fuel briquettes and pellets for grate-firing. Using briquettes and pellets reduces the fire hazard of the fuel (as compared with coal dust). Moreover, it cuts transportation and storage costs, as well as decreases the amount of fuel falling through the grate in the boiler furnace. However, the extensive use of such solid fuel briquettes in real practice involves the problem of long and energy-consuming combustion initiation, relatively low (as compared with high-grade coals) heat of combustion, possible significant underburning, and poor physical and mechanical characteristics. However, a distinct advantage of such pellets as a fuel for local heat supply sources is their very low cost as compared with fuel oil [19], which is a widespread energy resource of the local power industry. Even considering the ash removal costs (when using FC-based pellets as fuel), the cost of a unit of energy, produced by a local heat supply system, will be significantly lower than when using fuel oil. Moreover, oil prices and, thus, petroleum product prices are unpredictable and influenced by many factors. However, the cost of coal processing waste is made up of trans-shipment and storage expenses, while the fuel pellet production cycle (per a thermal unit) is less expensive than the fuel oil production technology [19]. Another factor to be considered is that the FC-based pellet price is independent of the global political situation. That is why, in the medium term, this energy resource looks much more attractive than fuel oil.

In the production of fuel briquettes and pellets, now there are a number of standards to comply with in order to provide regulatory values of their characteristics: ISO 17225-1:2014; DIN 51731 / DIN plus (Germany); CTI-R 04/5 (Italy); ÖNORM M7135 (Austria); SS 18 71 21 (Sweden); GOST R 57016-2016 and GOST 33103.1-2017 (Russia). The main requirements are set for the physical and mechanical characteristics (compressive strength according to GOST 21289-75, water absorption according to GOST 21290-75, stickiness, thermostability, yield of volatiles according to GOST 6382-80, mass fraction of total sulfur according to GOST 2059-75, ash content, shock resistance, lowest heat of combustion, and mechanical strength). This requires the addition of expensive binders or complicates the pellet production technology. There are research results that offer various methods of producing fuel briquettes and pellets [20,21]. Such studies mainly investigate their physical and mechanical characteristics, as well as analyze the thermotechnical properties of fuel compositions [22–24]. For example, it was established that low-temperature pyrolysis affects the calorific value of pellets based on coal sludge and straw [23], their limit of hygroscopy, emissions of gaseous combustion products, and the efficiency of boiler operation when burning the fuel in a fluidized bed at 800–900 °C. Quite often [24,25] the resistance of briquettes to mechanical stress is studied alongside their thermotechnical and thermophysical

properties (flame temperature, calorific value, and thermal conductivity), the characteristics of solid deposits and dynamics of slagging of energy generation equipment heating surfaces. Moreover, most of the studies [26] focus on the thermogravimetric analysis of coal pellets, containing various biomass (wood and grass waste).

However, the practical application of fuel briquettes and pellets from low-rank energy resources relies primarily on the research findings for ignition and combustion processes—ignition delay times vs. temperature in the boiler furnace, burning time, and composition of flue gases. The purpose of present work is to experimentally study the influence of a group of fuel composition additives, based on coal processing waste, on the ignition and combustion characteristics of fuel pellets, as well as anthropogenic gas emissions. Achieving this goal necessitates two types of experiments:

1. Combustion of single fuel pellets in a muffle furnace while recording the processes under study by a high-speed video camera and subsequent analysis of the video recordings to establish the mechanisms of physical and chemical processes, as well as temporal characteristics of ignition and combustion.
2. Combustion of a group of fuel pellets of identical component composition in a muffle furnace to analyze the typical anthropogenic gas emissions (CO , CO_2 , NO_x , SO_x) in flue gases.

2. Experimental Setup and Method

2.1. Materials

Fuel pellets were produced from dry FC (Table 1). This waste was preliminarily dried at 105 °C (according to ISO 5068-1). The first fuel group (composition No. 1) consisted of coal dust (dry FC) with a particle size no more than 140 μm without any additional components. The pellets of the second group of fuel compositions (compositions No. 2–No. 4) contained a 0.5 mm particle of porous polymer material in the central part of the experimental sample, which was impregnated with a combustible liquid and was surrounded by coal dust from all sides. We formulated a hypothesis, requiring experimental verification, that an additive (porous polymer material impregnated with a combustible liquid) in the fuel pellet composition must facilitate combustion. The ratio of components in the fuel compositions of the second group was 90:10%. The latter almost completely corresponds to the fraction of oil in the fuel, since the mass of a porous polymer material particle is negligible (less than 1%). The third group of compositions (compositions No. 5–No. 8) was a 70:30% mixture of coal dust with wood sawdust with a particle size less than 45 μm , 45–100 μm , 100–200 μm , and 200–500 μm . Wood sawdust is typical biomass, widely used as an additive to enhance the characteristics of solid fossil fuel combustion [26]. Thus, it is interesting to evaluate the effect of the dimensions of sawdust particles on the mechanism and characteristics of fuel pellet combustion. It is possible that particles of a larger size, when exposed to rapid heating, may release moisture and volatiles with a higher concentration. Hence, they may have a more significant effect on combustion. The analytical calculation of the heat of combustion was made using the methods from [27], and values of heat of combustion for fuel components (Tables 2 and 3). The obtained results are presented in Table 1.

Dry processing waste of bituminous coal with a particle size less than 140 μm was used as the main solid combustible component for preparing fuel compositions. FC was sieved through a sifter with a corresponding mesh size (in accordance with ISO 3310-1:2000) before producing pellets. The main characteristics of FC are listed in Table 2.

An additional component of the second group of fuel compositions No. 2–No. 4 is a fine polymer material (construction sealant), impregnated with one of three combustible liquids: rapeseed oil (composition No. 2), water-oil emulsion based on rapeseed oil (composition No. 3) or water-oil emulsion based on used turbine oil (composition No. 4). The main characteristics of fuel components are presented in Table 3.

Table 1. Fuel compositions.

Composition	FC	Additive	Q, MJ/kg
No. 1	100%	–	24.74
No. 2	90%	10%—porous polymer material impregnated with rapeseed oil	26.73
No. 3	90%	10%—porous polymer material impregnated with water-oil emulsion (rapeseed oil)	26.05
No. 4	90%	10%—porous polymer material impregnated with water-oil emulsion (turbine oil)	26.63
No. 5	70%	30%—dry sawdust (particle size of less than 45 µm)	22.07
No. 6	70%	30%—dry sawdust (particle size of 45–100 µm)	
No. 7	70%	30%—dry sawdust (particle size of 100–200 µm)	
No. 8	70%	30%—dry sawdust (particle size of 200–500 µm)	

Table 2. Results obtained from proximate and ultimate analysis of filter cake (FC) and pine sawdust [12,28,29].

Component	Proximate Analysis					Ultimate Analysis				
	A ^d (%)	W ^a (%)	V ^{daf} (%)	Q ^a _{s,V} (MJ/kg)	T _{ign} (°C)	C ^{daf} (%)	H ^{daf} (%)	N ^{daf} (%)	S ^{daf} (%)	O ^{daf} (%)
FC	26.5	–	23.1	24.83	450	87.2	5.1	2.1	1.1	4.5
Sawdust	2.0	19.8	73.52	16.45	340	50.3	6.0	0.2	0.1	43.4

Table 3. Properties of oils [28,30].

Oil	Density at 20 °C (kg/m ³)	W ^a (%)	A ^d (%)	T _f (°C)	T _{ign} (°C)	Q ^a _{s,V} (MJ/kg)
Rapeseed oil	911	0.28	0.03	242	–	39.52
Used turbine oil	868	–	0.03	175	193	44.99

The third group of compositions No. 5–No. 8 contained pine sawdust of different particle size as an additional combustible component. Air-dried wood was ground by an SW-2 cutting mill (HT Machinery, Japan-Taipei, Taiwan) and sieved using a laboratory plansifter with a set of sieves (according to ISO 3310-1:2000) to obtain sawdust of different particle size: less than 45 µm (composition No. 5), 45–100 µm (composition No. 6), 100–200 µm (composition No. 7), and 200–500 µm (composition No. 8). See Table 2 for the characteristics of sawdust.

Cylinder-shaped fuel pellets with a mass of 20 mg, 3 mm in diameter and 3 mm in height were produced by pressing coal dust with some other components or without them in a pellet die at a pressure of 5 MPa. A pellet die consists of three parts: a hollow steel cylinder with a through opening 3 mm in the internal diameter, which is located along the symmetry axis of the cylinder; a steel cap for air-tight sealing of the steel cylinder from one side; a steel piston to compress fuel pellets through the second opening in the steel cylinder. The said pressure was built up using a Heavy Duty Shop (Cluj-Napoca, Romania) Press 20 ton hydraulic press. This is a common method of briquette and pellet production by pressing [25,31,32]. It is quite easy to implement and requires no complicated or costly equipment, like it is, e.g., in the thermal processing pelletization [33,34]. The main idea of this research is to study the influence of the component composition of fuel pellets on the mechanisms and characteristics of their combustion, but not the influence of the fuel pellet production technique on their physical and mechanical characteristics. Therefore, experimental samples were obtained using the cold (25 °C) pressing method (without additional heating of fuel components or adding binders). In the preparation of compositions No. 2–No. 4 for pressing, FC (90 wt%) was divided into two parts of identical mass. The first part was put into a pellet die. Then a porous polymer material, impregnated with a combustible liquid, was added to it. The second part of FC was put over it in the press die, and the mass was compressed. In the production of compositions No. 5–No. 8, FC (70 wt%) was preliminarily mixed with sawdust (30 wt%) of the corresponding particle size. Then the mixture

was compressed to produce fuel pellets. The above size (3 mm in diameter and 3 mm in height) of fuel pellets was chosen intentionally to conduct laboratory experiments considering two main limitations. First, the high-temperature medium of pellet combustion is generated in the rotary muffle furnace, whose dimensions are limited. Second, the fuel pellet combustion duration corresponds to the maximum recording time of the high-speed video camera, used to capture the processes under study.

2.2. Experimental Setup

The characteristics and consistent patterns of processes, developing during the ignition and combustion of composite fuel pellets (Table 1) were studied using an experimental setup, schematically represented in Figure 1. The radiant heating conditions in a high-temperature air medium were simulated in a tube muffle furnace Loiplf50/500-1200 (Laboratory Equipment & Instruments ZAO, Saint-Petersburg, Russia). The tube was 50 mm in the inner diameter and 500 mm in length; the temperature was varied in the range 20–1200 °C and measured with an in-built type K thermocouple.

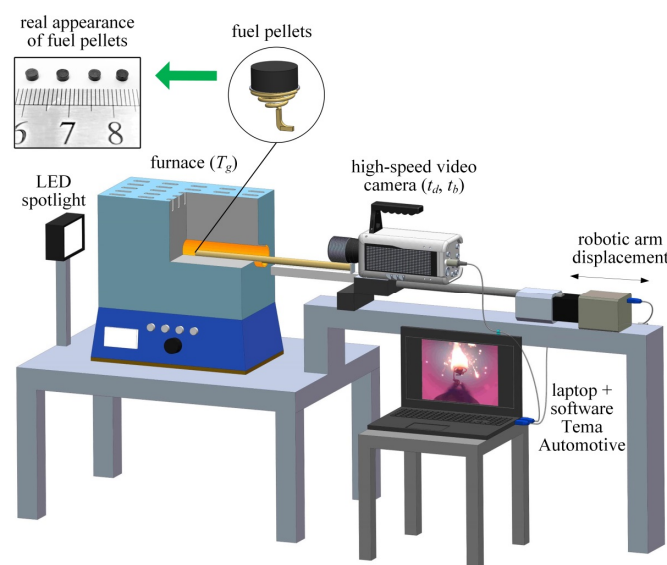


Figure 1. Scheme of experimental setup.

When FC-based pellets are burned under optimum conditions—in small-sized boiler furnaces of local heat supply with a small chamber volume—the velocity of pellets is somewhat different from that of the carrier medium (a mixture of air with combustion products). Thus, the radiant heat flux density significantly exceeds the convective heat exchange density.

A set of 7–10 experiments were performed under identical initial conditions. In each of them the furnace was heated to a given temperature (T_g). Single fuel pellets, located on the holder (Figure 1), were fed into the furnace at a rate of 0.1 m/s along the symmetry axis of the tube up to its middle, where the given temperature T_g was maintained. Experimental samples of all the fuel compositions (No. 1–No. 8) were identical. They were cylinder-shaped pellets with a mass of 20 mg, 3 mm in diameter and 3 mm in height. The heating value of such fuel pellets was different (Table 1). However, this factor had a less significant effect on the difference in the ignition delay times of fuel compositions No. 1–No. 8 than the mass and dimensions of the fuel pellets. An SPSH20-23017/2000Z manipulator (Mechatronic Product Factory ZAO, Saint-Petersburg, Russia) moved the fuel sample holder and a Phantom V411 high-speed video camera (Vision Research, Wayne, NJ, USA) at the same time. The filming rate was 500 frames per second at resolution 800 × 600 pixels. An LED projector was fixed on the muffle furnace opposite the video camera for better contrast of fuel pellet images during video recording (Figure 1). Tema Automotive software (Image Systems AB, Linköping, Sweden) was used to process the video frames.

The ignition delay time (t_d) was calculated by how much time passed after the pellet started heating (on entering into the muffle furnace) up until the fuel ignited. The latter event (Figure 2a) was captured by the moment when controlled luminous intensity was achieved in the recording area, similarly to the methods in [35–39]. In the Tema Automotive software, the video recording processing algorithm monitored all the video frames in sequence. The values of the shades of gray (from 0 to 255, which corresponds to the range from black to white) were measured in each point (pixel) of the recording area (Figure 2a) for each video frame. The initial video recordings in color were converted into black and white. Thus, the interval of luminous intensity from 220 to 255 corresponded to the fuel combustion (luminance around the pellet as a result of a rapid exothermic reaction). The moment of ignition was recorded automatically by the values of the luminous intensity reaching or exceeding 220 (in the shades of gray) in any point around the pellet being monitored. For example, in Figure 2a the red cross indicates a point, in which the highest luminous intensity is reached in the shortest time, as compared with other points in the recording area. Once the ignition moment was determined, the video recording processing algorithm was used to monitor the development of the process by the growth of the mean luminous intensity value in the recording area, which indicated the fuel ignition sustainability.

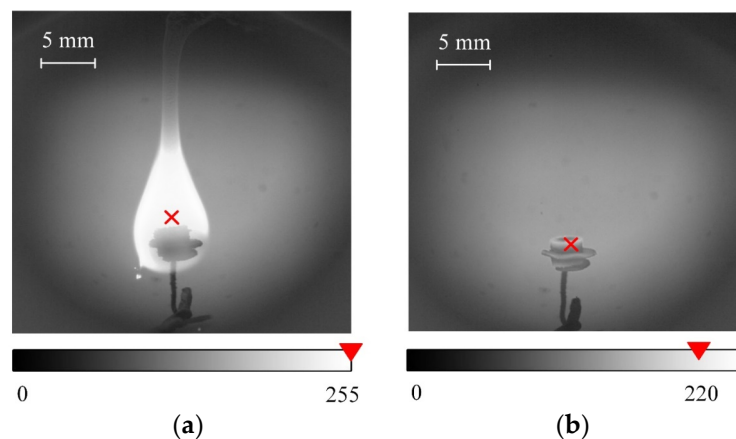


Figure 2. Example of implementing the algorithm of video recording processing with Tema Automotive software for fuel pellet combustion: (a) moment of ignition ($t = t_d$); (b) moment of combustion completion ($t = t_d + t_b$).

The fuel burnout duration was determined in a similar way (t_b). This is a time interval between the ignition moment and combustion completion moment of the fuel components. The latter event was recorded automatically by a reduction in the luminous intensity to less than 220 (in the shades of gray) all over the fuel pellet surface (Figure 2b). The systematic errors of determining the times t_d and t_b , conditioned by the video recording rate, did not exceed ± 0.001 s. The random errors for a set of 7–10 experiments under identical initial conditions were less than 15%.

Separate experiments were conducted to establish the concentrations of the main anthropogenic emissions in flue gases from the fuel pellet combustion. A Testo 340 gas analyzer (Testo SE & Co. KGaA, Stuttgart, Germany) was mounted on the setup (Figure 1) in place of the high-speed camera. It comes with four sensors: CO (measuring range 0–10,000 ppm, resolution 1 ppm, accuracy $\pm 10\%$), NO_x (measuring range 0–4000 ppm, resolution 1 ppm, accuracy $\pm 5\%$), O₂ (measuring range 0–25%, resolution 0.01%, accuracy $\pm 0.2\%$), SO₂ (measuring range 0–5000 ppm, resolution 1 ppm, accuracy $\pm 10\%$). The CO₂ concentration (measuring range 0–25%, resolution 0.1%, accuracy $\pm 0.2\%$) was calculated automatically by the results of O₂ concentration measurement. The experimental procedures were similar to those in [40]. Fuel pellets with a total mass of at least 1 g were placed into a pre-heated muffle furnace, using a manipulator. The mass was chosen to fit the gas analyzer specifications and meet a condition of identical heating value, when burning fuel samples with different compositions

(Table 1). Reliable measurement results necessitated supplying certain minimum volumes of flue gases. These were collected using a gas analyzer probe, inserted into the rotary muffle furnace. Thermal insulator material was used to seal the ceramic tube apertures (Figure 1) to prevent the escape of flue gases during the experiments. Sets of 3–5 experiments were performed under identical initial conditions. Further, the experimental results will be presented as average experimental data values. Glushkov et al. [40], established that the higher the temperature, at which ignition and combustion of hydrocarbon fuels occur, the higher the anthropogenic emission concentrations in flue gases. The maximum temperature, generated by the electric muffle furnace being used, is 1000 °C. In this study, the concentrations of carbon, nitrogen, and sulfur oxides were established from the combustion of fuel pellets per a unit of energy, released at 1000 °C, which corresponds to the boiler furnace temperature. That means that the gas concentrations obtained will be maximum for the temperature range of 800–1000 °C, in which the combustion times were investigated. Such approach made it possible to establish differences in the anthropogenic emission concentrations from the combustion of fuel pellets based on coal processing waste when adding various components in the conditions corresponding to the real-scale technological process. The results of the corresponding study will be presented below in the following format: relative emissions, reduced to the allocated identical amount of heating value, when burning different fuel compositions with various mass of fuel samples.

3. Results and Discussion

Figures 3 and 4 present the video frames of ignition and combustion of a group of solid composite fuel pellets with various components and without them. It is clear (Figures 3 and 4) that adding a single particle of porous polymer material, impregnated with different combustible liquids, or wood sawdust of different particle size to the fuel pellet composition intensifies the ignition and combustion of these compositions, as compared with pellets, produced from FC without any additional components (composition No. 1). In general, the physical and chemical processes, occurring during the heating of pellets of fuel compositions under study (Table 1), follow almost identical patterns, since their main component is FC.

High-speed video recordings made it possible to distinguish the following main stages of the process under consideration, when single pellets are heated in motionless heated air: inert heating of the fuel; evaporation of liquid components (water or oils for compositions No. 2–No. 4); thermal decomposition of solid combustible components (FC, polymer material for compositions No. 2–No. 4, wood for compositions No. 5–No. 8); formation of gas-vapor mixture around the pellet under the conditions of diffusive-convective heat and mass transfer in the oxidizer medium; its ignition on reaching critical conditions and subsequent burnout; heating of the solid residue from the heat of the gas-phase combustion; its ignition and subsequent burnout. The gas-phase combustion develops most rapidly for FC-based fuel pellets with sawdust (Figure 4). This result is attributed to a much higher content of volatiles in wood, as compared with FC (Table 2). Compositions No. 5–No. 8, as compared with composition No. 1, are characterized not only by a larger (by 10–20%) area around the pellet, in which the combustion of the gas mixture occurs, but also a longer (by 20–25%) duration of this process. Additionally, the burnout times of solid components (t_b) differ by 15–20%, which is also conditioned by differences in their ultimate analyses. The content of carbon in wood is almost one third lower than in FC. Therefore, the solid residue of compositions No. 5–No. 8 burns out much faster than that of composition No. 1 (Figure 4). Similar patterns were established when the characteristics of ignition and combustion for fuel compositions No. 2–No. 4 were compared with those for composition No. 1 (Figure 3), even when the concentration of an additional component is only 10%. In this case, the ignition delay times and complete burnout times differ (Figure 5) due to different combustion mechanisms. A detailed analysis of the latter will be carried out below when describing typical schemes (Figure 6) of combustion of fuel pellets with various components.

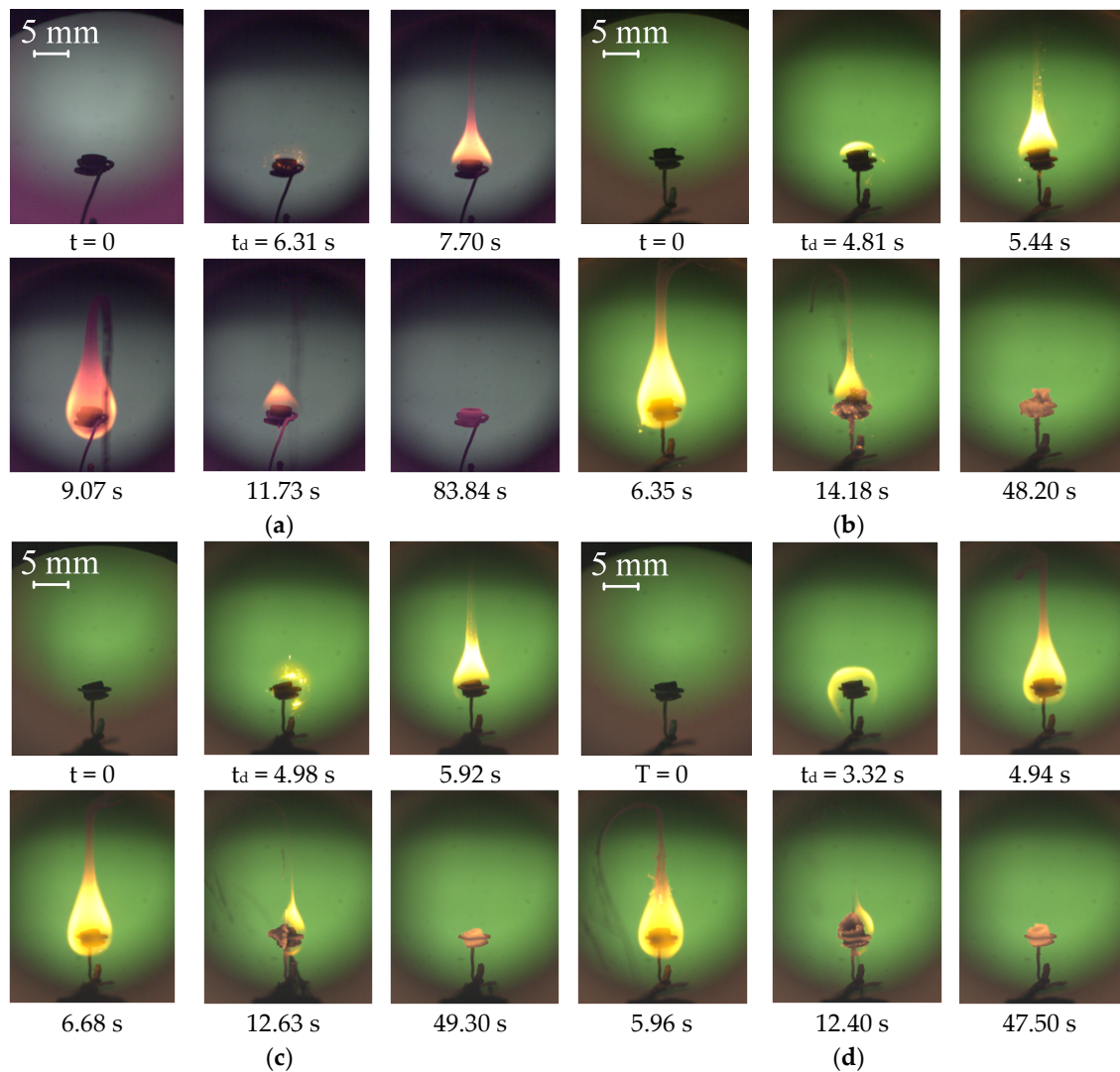


Figure 3. Video frames of ignition and combustion of FC-based fuel pellets with porous polymer material, impregnated with combustible liquid at $T_g = 850^\circ\text{C}$: (a) fuel composition No. 1: FC; (b) fuel composition No. 2: FC + porous polymer material, impregnated with rapeseed oil; (c) fuel composition No. 3: FC + porous polymer material, impregnated with oil-water emulsion (rapeseed oil); (d) fuel composition No. 4: FC + porous polymer material, impregnated with oil-water emulsion (turbine oil).

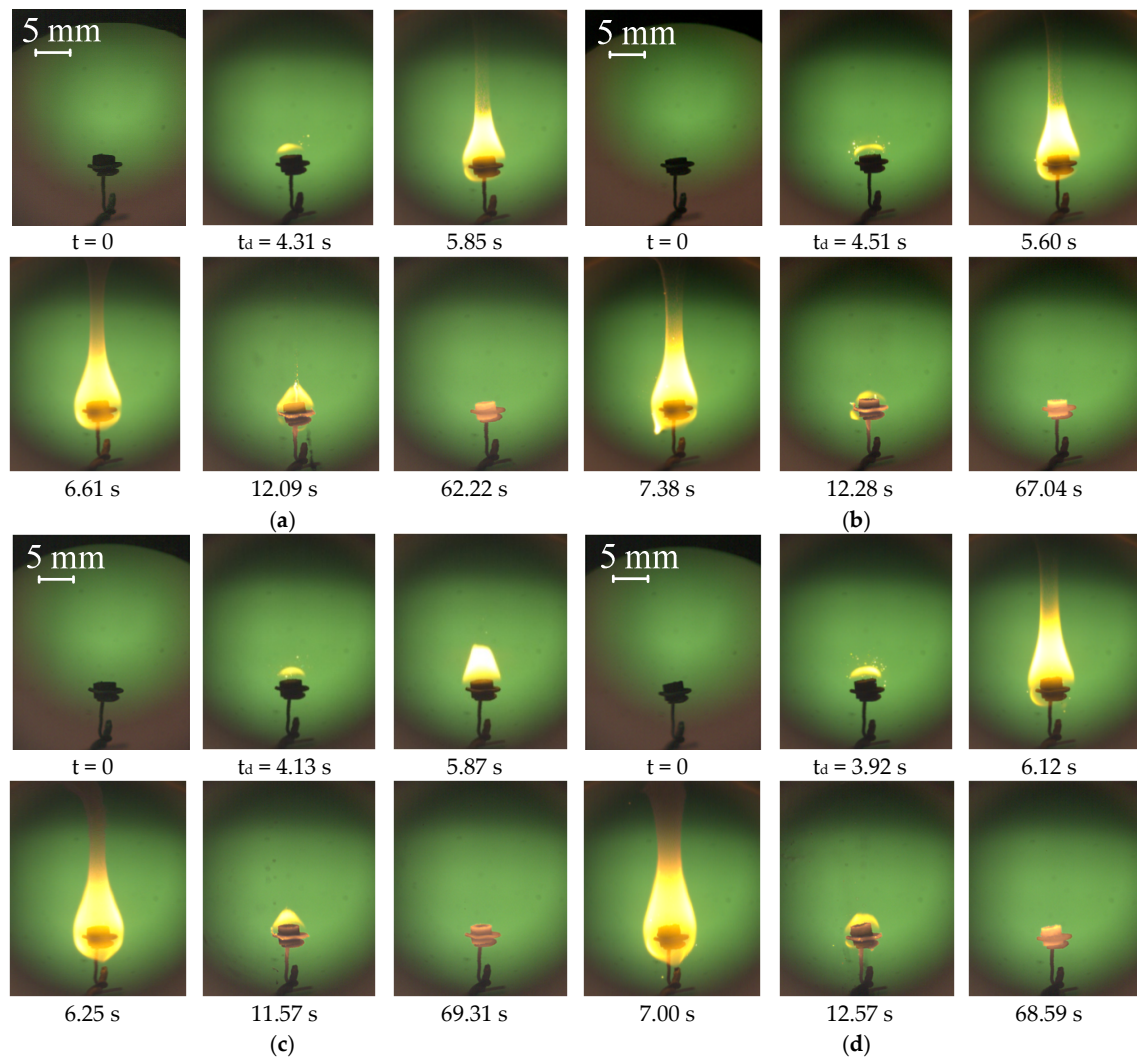


Figure 4. Video frames of ignition and combustion of FC-based fuel pellets with sawdust of different particle size at $T_g = 850$ °C: (a) fuel composition No. 5: FC + sawdust (less than $45\ \mu\text{m}$); (b) fuel composition No. 6: FC + sawdust ($45\text{--}100\ \mu\text{m}$); (c) fuel composition No. 7: FC + sawdust ($100\text{--}200\ \mu\text{m}$); (d) fuel composition No. 8: FC + sawdust ($200\text{--}500\ \mu\text{m}$).

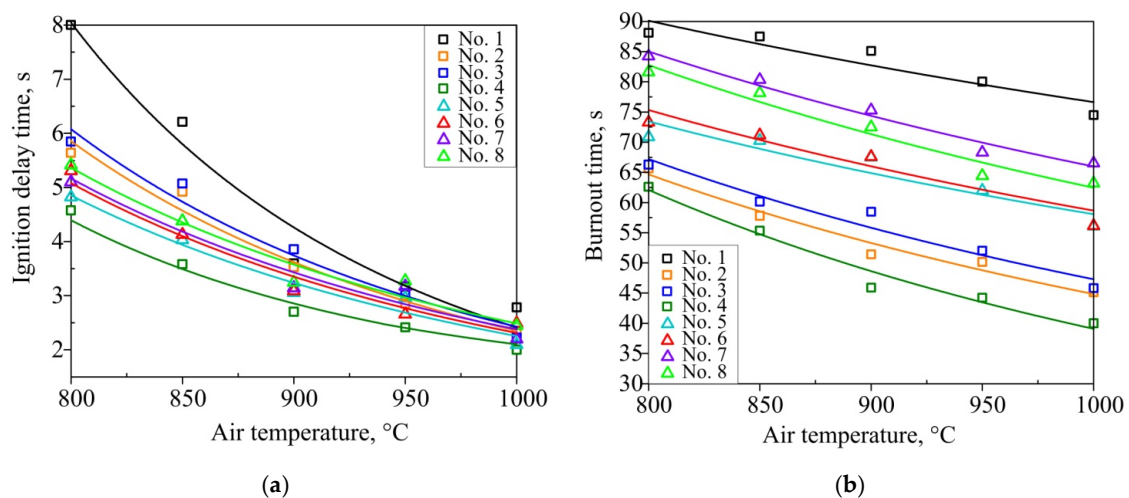


Figure 5. Ignition delay times (a) and complete burnout times (b) of fuel pellets vs. the ambient temperature.

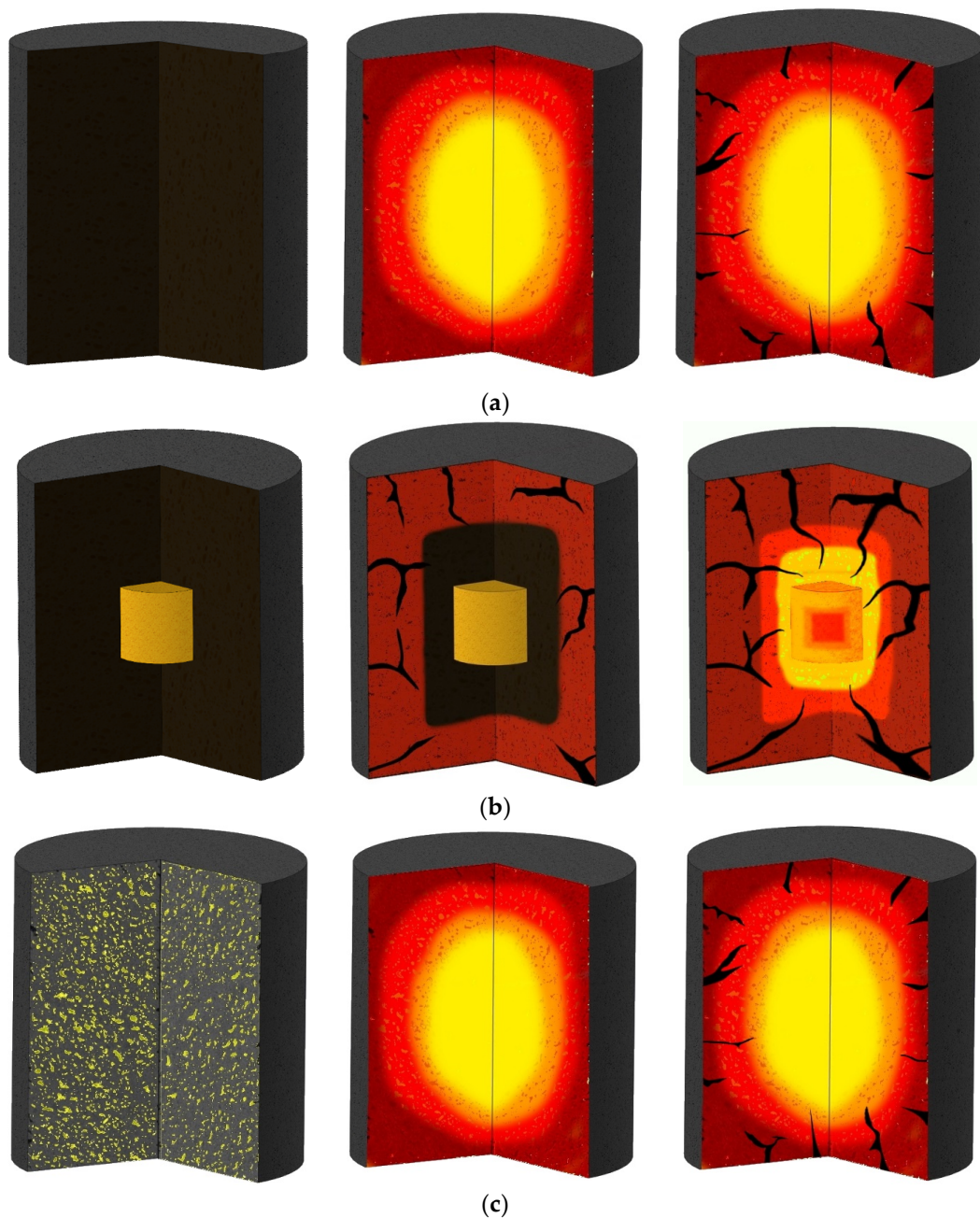


Figure 6. Schemes of combustion mechanisms of FC-based fuel pellets with different components: (a) fuel composition No. 1: FC; (b) fuel compositions No. 2–No. 4: FC + porous polymer material, impregnated with a combustible liquid; (c) fuel compositions No. 5–No. 8: FC + sawdust.

Figure 5 presents the ignition delay times (t_d) vs. burnout times of fuel pellets (t_b) when varying the heated air temperature in a wide range: $T_g = 800$ – 1000 °C. The temperature range limit on the left ($T_g = 800$ °C) corresponds to threshold (minimum) ignition conditions. At air temperatures under 800 °C, the pellets of all the eight fuel compositions (Table 1) did not ignite. Under such conditions, moisture evaporated and solid components thermally decomposed. However, the intensity of these processes and the oxidizer temperature were not enough for the forming gas mixture to ignite. The combustible gases and vapors diffused into the environment, but their concentration around the fuel pellet was decreasing as the fuel components thermally decomposed (and the content of volatiles decreased). The ambient air temperature was not high enough for the solid residue to ignite.

The mean ignition delay times of pellets of different compositions (with various additives) decrease from 5–6 s to 2.5 s in the air temperature (T_g) range from 800 °C to 1000 °C (Figure 5a). Their combustion becomes more intense under such conditions. The burnout times of fuel pellet components decrease by 20–25% (Figure 5b). It was established that the t_d values for the FC-based fuel compositions under study decrease sequentially (other conditions being equal) when the following components are added to them: a polymer material particle, impregnated with oil-water emulsion (based on rapeseed oil); a polymer material particle, impregnated with rapeseed oil; wood sawdust with a particle size of 200–500 μm ; wood sawdust with a particle size of 100–200 μm ; wood sawdust with a particle size of 45–100 μm ; wood sawdust with a particle size of less than 45 μm ; a polymer material particle, impregnated with oil-water emulsion (based on turbine oil). That means that fuel pellets with the latter component (composition No. 4) are characterized by the lowest ignition delay times. The highest values of t_d are typical of pellets, produced from FC without any additional components (composition No. 1).

At ambient temperatures 800–850 °C, the t_d values for the compositions with various components differed by about 70% at the most (Figure 5a). At $T_g \rightarrow 1000$ °C and higher, the intensity of physical and chemical processes is so high that the ignition delay times for all the fuel compositions differ by no more than 5%, thus being less than the random error of t_d measurement (Figure 5a). Under near-threshold ignition conditions, the physical and chemical processes occur less rapidly. Most of the induction period (80–90%) is made up of the thermal preparation stage, characterized largely by heat and mass transfer processes both in the condensed phase and in the gas medium. Therefore, the differences in the ignition characteristics of fuel compositions with different components are more pronounced at $T_g = 800$ °C.

As it was mentioned above, the gas-phase combustion develops most rapidly for FC-based fuel pellets with additives (sawdust and porous polymer material, impregnated with combustible liquid). This result is attributed to a much higher content of volatiles (Tables 1 and 2) in fuel compositions No. 2–No. 8, as compared with FC (composition No. 1) without any additives. Besides, a further analysis will show that compositions No. 2–No. 4, as compared with composition No. 1, are characterized not only by a higher content of volatiles, but also by a significant difference in the combustion mechanism. A rapid evaporation of combustible liquid leads to the emergence and formation of a developed structure of pores, whose sizes are comparable with the typical pellet size. Under such conditions, the vapors and gases with low resistance enter the oxidizing medium from the deep pellet layers through open pores. The concentration of combustible gases in the vicinity of the pellet grows rapidly, and the gas-phase ignition occurs with a short delay (as compared with fuel composition No. 1).

The experimental results enable to draw an important conclusion. Including lumber waste (wood sawdust) in the composition of FC-based pellets in the volumes not affecting the physical and mechanical characteristics of pellets leads to significant (up to 70%) reduction in the ignition delay times at relatively low (800–850 °C) temperatures. Since the emission of nitrogen oxides in combustion products of coal and coal processing waste is minimum, and this temperature range in boiler furnaces of local heat supply is the most preferred, it can be concluded that including wood sawdust in the composition of fuel pellets based on coal processing waste is highly practical.

The times of complete burnout of fuel pellets (Figure 5b) are in good agreement with their ignition delay times. It was established that the t_b values for FC-based fuel compositions under study decrease sequentially (other conditions being equal) when the following components are added to them: wood sawdust with a particle size of 200–500, 100–200, 45–100 μm and less than 45 μm ; a polymer material particle, impregnated with oil-water emulsion (based on rapeseed oil); a polymer material particle, impregnated with rapeseed oil; a polymer material particle, impregnated with oil-water emulsion (based on turbine oil). This means that fuel pellets with the latter component (composition No. 4) are characterized by the lowest burnout times of components. The highest values of t_b are typical of pellets produced from FC without any other components added to them (composition No. 1). As it will be shown below, the obtained result can be explained by the differences in the elemental

composition of fuel components and in the combustion mechanisms (the combustion front of fuel pellets with pores has a rather complex structure; the developed structure of pores increases the combustion area, thus, accelerating the burnout of fuel pellet components). Solid fuel pellets with a polymer material particle, impregnated with oil-water emulsion, burn out within 62 s at relatively low ambient temperatures ($T_g = 800\text{ }^{\circ}\text{C}$), which is 30% lower than t_b of fuel composition No. 1 based on FC without any additional components, and at $T_g = 1000\text{ }^{\circ}\text{C}$, the difference in the burnout times is 45%. Thus, adding extra components (a polymer particle, impregnated with oil-water emulsion; wood sawdust) to FC intensifies both the ignition and burnout of fuel pellets.

As mentioned above, this result is explained by different combustion mechanisms of fuel compositions (Table 1). Figure 6 presents schemes of combustion mechanisms for three groups of FC-based fuel pellets with different components, established from analyzing the frames of high-speed video recording. The differences established in the combustion mechanisms (Figure 6) are primarily attributed to the structure of fuel pellets. The compositions of the first and third groups (No. 1, No. 5–No. 8) have a uniform structure with a rather dense packaging of fine particles of solid components (coal dust and wood sawdust). Thus, when they are heated, the occurring processes are similar to the combustion of large (several millimeters) solid fossil fuel particles. Internal thermal stress leads to the formation of open pores (Figure 6a,c), through which the thermal decomposition products of solid components escape from the deep layers of fuel pellets into the oxidizer medium. These pores emerge and develop primarily in the near-surface layer of the pellet, and their size is much smaller than that of the pellet itself. Notably, the shape of pellets under such conditions remains almost the same as they burn (Figures 3a and 4). The solid residue burns out in layers. The front of combustion is formed in the near-surface layer of the pellet and moves steadily towards its deep layers.

This process is more intense for compositions No. 5–No. 8, containing wood sawdust, than it is for composition No. 1. Sawdust is actually a thermally active additive, evenly distributed throughout the pellet. The ignition temperature of wood is much lower than that of dry FC (Table 2). Thus, in the layer-by-layer combustion of the pellet, wood particles are the first to ignite in the combustion front, and then the heat released intensifies the coal component ignition (Figure 6c). It reduces the ignition delay of coal.

The compositions with a polymer material particle, impregnated with a combustible liquid, are characterized by a different mechanism of ignition and combustion intensification. When a fuel pellet is heated, the thermal decomposition of FC is accompanied by the endothermic evaporation of oil or water-oil emulsion. Under such conditions, the energy supplied to the pellet is spent on the phase transformation, which reduces the intensity of the process under study, on the one hand. On the other hand, the rapid evaporation of liquid in a small area, located inside the dense structure of pressed FC, results in a higher pressure of vapors in a closed space. This leads to the emergence and formation of a developed structure of pores (Figure 6b), whose sizes are comparable with the typical pellet size. Under such conditions, the fuel pellet shape changes significantly during combustion (Figure 3b–d). As with the other compositions, in the heating of compositions No. 2–No. 4, the vapors and gases with low resistance enter the oxidizing medium from the deep pellet layers through open pores (Figure 6b). However, the combustion front of such pellets has a rather complex structure. The developed structure of pores increases the combustion area and, thus, accelerates the burnout of fuel pellet components. Similar processes are typical of abnormal combustion modes of composite solid fuels when fuel charges crack or detach from the engine body walls [41].

The experimental research findings for the ignition delay times and duration of burnout of a group of fuel pellets at different heating temperatures provide a foundation for the development of an industrial technology of using such solid composite fuels to generate power by combustion, e.g., in hot-water boiler furnaces. The established temporal characteristics of ignition and combustion can be applied to calculate the thermal modes of boiler furnace operation. Moreover, it was shown that the burnout rate of fuel components may be increased or decreased by varying the component

composition of fuel pellets. Thus, the energy output per a unit of time can be varied in the temperature range of 800–900 °C, typical of hot-water boiler furnaces.

In addition to the ignition and combustion characteristics, we also analyzed the concentrations of anthropogenic emissions in flue gases from fuel pellet combustion. The concentrations of carbon oxides from the combustion of compositions No. 1–No. 8 are similar (the differences do not exceed several percent): CO₂—17–18%, CO—no more than 400 ppm. These values correspond to identical characteristics of coal dust combustion in a boiler furnace [5]. The concentrations of nitrogen and sulfur oxides from the combustion of fuel pellets with different components differ much more significantly (Figure 7).

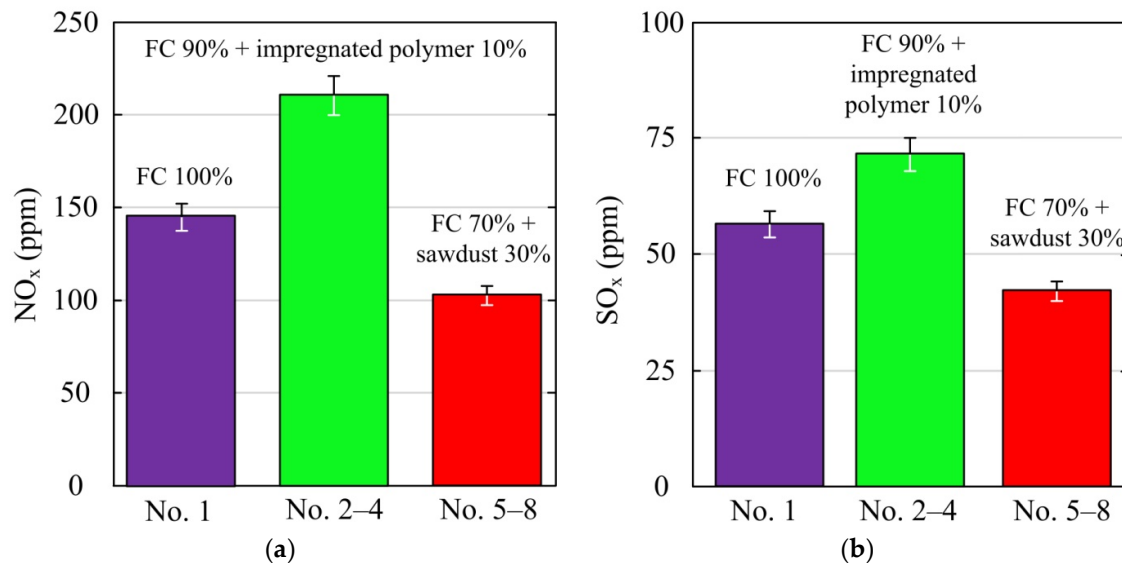


Figure 7. NO_x (a) and SO_x (b) concentrations in flue gases per a unit of heat released from fuel pellet combustion at $T_g = 1000$ °C.

In Figure 7, the NO_x and SO_x concentrations are presented per a unit of heat (emissions for identical heating value of fuel samples are compared), released from the combustion of fuel pellets of different component composition. Notably, the ratio of masses of fuel compositions from three groups (FC; FC + 10% polymer particle, impregnated with a combustible liquid; FC + 30% wood sawdust), identical in the calorific value, is 1: 0.92: 1.12. According to the ultimate analysis (Table 2), wood contains 10 times less nitrogen and sulfur. Therefore, adding wood sawdust to FC significantly reduces the NO_x and SO_x concentrations from the combustion of these fuel compositions of identical mass. However, the heat of combustion of wood is 35% lower than that of FC (Table 2). Therefore, the mass of the fuel composition based on FC with 30% of wood sawdust has to be 1.12 times bigger to generate the same amount of heat, as the combustion of FC does. Thus, the difference in the NO_x and SO_x concentrations for composition No. 1 and compositions No. 5–No. 8 (per a unit of heat, released from the fuel pellet combustion) is 30% and 25% (Figure 7), respectively. Moreover, the ash content of wood is an order of magnitude lower than that of FC, so, the combustion of a larger mass of fuel pellets with it will not increase the amount of non-combustible solid residue, but will, on the contrary, somewhat decrease it.

In its turn, adding a porous polymer particle, impregnated with a combustible liquid, to the fuel pellet composition, has a positive effect on its calorific value, since the heat of combustion of oil is almost twice as high as that of FC (Tables 2 and 3). Therefore, the mass of the fuel composition based on FC with 10% of porous polymer, impregnated with a combustible liquid, has to be 1.09 times smaller to generate identical amount of heat. Under such conditions, the difference in the NO_x and SO_x concentrations of the corresponding composition and FC without any components is 30% and 20% (Figure 7), respectively. The co-firing of dry coal with used oil increases the concentrations of the oxides of nitrogen and sulfur in flue gases. This is explained by a higher combustion temperature

of such fuel compositions. It was established that [5], adding used oils to composite fuels increases the combustion temperature by 100–200 °C. For fuel compositions containing municipal solid waste, higher combustion temperature reduces the concentration of carcinogens, e.g., PCDD/Fs, despite higher NO_x and SO_x concentrations [5].

Apart from the effect of adding combustible components with lower content of nitrogen and sulfur or with greater calorific value to FC, the concentration of anthropogenic emissions in flue gases also depends on the chemical interaction of a large group of substances and compounds in the gas medium at relatively high temperatures [4]. The temperature of gases in the flame can reach 1100–1400 °C [5]. Under such conditions, the water vapors, as well as oxides of alkaline and alkaline-earth metals, [4] can significantly reduce the anthropogenic emissions [42]. However, a detailed mechanism of chemical reactions, explaining the content of anthropogenic emissions in flue gases from the combustion of different fuel compositions based on hydrocarbons, has not been established yet. We did not consider solving this task in our study, since it requires independent research.

The analysis of anthropogenic emissions has shown that adding some biomass (from several percent to several-dozen percent) to FC significantly reduces the concentrations of sulfur and nitrogen oxides. This reduction in anthropogenic emissions is attributed to the following groups of factors. First, replacing some part of coal with components that contain much less sulfur and nitrogen (Table 2) reduces the NO_x and SO_x concentrations in flue gases, since solid fossil fuels are the main sources of the respective oxides [43], forming from the oxidation of volatiles and fuel coke during combustion. The second reason is that sulfur and nitrogen oxides interact with water vapors, as well as biomass pyrolysis and gasification components. This results in the formation of salts in the ash and reduces the NO_x and SO_x concentrations in the gas medium. The redox environment, conditioned by the presence of moisture, leads to the emergence of extra H and OH radicals. They can also interact with NO_x and SO_x in line with the reactions: $2\text{NO} + 4\text{H}_2 + \text{O}_2 \rightarrow \text{N}_2 + 4\text{H}_2\text{O}$ (at a temperature above 200 °C); $\text{SO}_2 + 3\text{H}_2 \rightarrow \text{H}_2\text{S} + 2\text{H}_2\text{O}$ (at temperatures above 1000 °C) [42]. The metal-containing components in the ash part of the dry biomass and FC can also interact with sulfur and nitrogen oxides ($\text{CaO} + \text{SO}_2 + 1/2\text{O}_2 \rightarrow \text{CaSO}_4$; $3\text{SO}_2 + 2\text{Fe}(\text{OH})_3 \rightarrow \text{Fe}_2(\text{SO}_3)_3 + \text{H}_2\text{O}$; $2\text{Fe} + 3\text{NO} \rightarrow 3/2\text{N}_2 + \text{Fe}_2\text{O}_3$) at temperatures above 800 °C [44]. This results in the formation of new substances that either end up as ash residue or participate in further chemical reactions in the gas medium without forming NO_x or SO_x. The final content of NO_x in flue gases is also affected by the type of nitrogen-containing compounds in the fuel. In biomass, most of the nitrogen is in volatile components that are released and burn out at the initial stage of ignition and combustion as compounds some of which do not produce nitrogen oxides [43]. As for coal and coal processing waste, nitrogen oxides are formed at the stage of the coke part oxidation at relatively high temperatures which are not achieved due to a decrease in temperature of fuel combustion when biomass is added [43].

Thus, it was experimentally established that adding extra components even with relatively low concentrations (10–30%) to fuel compositions based on fine coal processing waste or dust of low-grade coal significantly enhances the combustion of fuel pellets and reduces the concentrations of anthropogenic emissions in flue gases.

The fundamental research findings provide a scientific evidence of the prospects of using multicomponent fuel pellets in real practice. They serve as a foundation for the development of an industrial technology of producing such fuel pellets, in particular for the calculation of the mass fraction of various components. The results offer the potential for the industrial recovery of abundant existing and annually produced coal processing (FC) and woodworking waste that poses a serious fire and environmental hazard if stored at open-air disposal sites. The cost of such waste-derived fuel is largely made up of transportation expenses and is much lower than that of high-quality fossil fuels. Moreover, the possibility of varying the component composition of fuel pellets by adding biomass or a highly reactive component will enable us to make more effective use of power-generating equipment. The operation of a hot-water boiler with grate firing of solid fuels can be optimized by enhancing combustion not only when employing an automatic control system, but also when changing the fuel

composition to achieve the target indicators—for anthropogenic emissions (pellets with biomass) or power generation intensity (pellets with a highly reactive component).

4. Conclusions

Experimental studies have been conducted for three groups of fuel pellets based on coal processing waste with porous polymer material particles, impregnated with a combustible liquid, and wood sawdust of different particle size. The ignition and combustion of single fuel pellets were researched under radiant heating in an air medium, while varying the temperature from 800 to 1000 °C. Using a hardware and software system of high-speed video recording, the main characteristics of the processes were established: ignition delay times (2–8 s) and duration of fuel burnout at different heating temperatures (40–90 s). For the fuel compositions under study, the same main stages of the process were distinguished, when single pellets were heated in motionless heated air: inert heating of the fuel; moisture evaporation; thermal decomposition of solid combustible components; formation of gas-vapor mixture around the pellet under the conditions of diffusive-convective heat and mass transfer in the oxidizer medium; its ignition on reaching critical conditions and subsequent burnout; heating of the solid residue from the heat of the gas-phase combustion; its ignition and subsequent burnout. A difference was established in the combustion mechanisms of pellets, when adding various components to the fuel mixture composition. This has a direct influence on the induction period duration and combustion time, other conditions being equal. When wood sawdust is distributed evenly throughout the fuel pellet, solid components burn out layer-by-layer. The ignition temperature of wood is much lower than that of dry FC, therefore, wood particles are the first to ignite in the combustion front, and the heat released intensifies the ignition of the coal component. For compositions containing a polymer material particle, impregnated with a combustible liquid, the evaporation of oil or water-oil emulsion in a small area, located inside the dense structure of pressed FC, results in a higher pressure of vapors in a closed space. This leads to the emergence and formation of a developed structure of pores with sizes comparable with the typical pellet size. The combustion front of such pellets has a rather complex structure. The developed structure of pores increases the combustion area and, thus, accelerates the burnout of fuel pellet components. The component composition of fuel pellets also affects the concentration of anthropogenic emissions in flue gases. The concentrations of carbon oxides from the combustion of the fuel compositions under study are similar: CO₂—17–18%, CO—no more than 400 ppm. NO_x and SO_x concentrations in flue gases per a unit of heat, released from the fuel pellet combustion at 1000 °C, are by 30% and 25% lower for the compositions with 30% of wood sawdust, while being by 30% and 20% higher for compositions with 10% of porous polymer, impregnated with a combustible liquid, as compared with identical characteristics from the combustion of FC without any additional components. The NO_x and SO_x concentrations from the combustion of FC pellets are less than 150 and 60 ppm, respectively.

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Nomenclature

A^d	ash content, %
B_{fuel}	amount of fuel combusted, t
C^{daf}	fractions of carbon in the fuel component converted to a dry ash-free state, %
H^{daf}	fractions of hydrogen in the fuel component converted to a dry ash-free state, %
N^{daf}	fractions of nitrogen in the fuel component converted to a dry ash-free state, %
O^{daf}	fractions of oxygen in the fuel component converted to a dry ash-free state, %
$Q^{\text{a}}_{\text{s}, \text{v}}$	higher heating value, J/kg
S^{daf}	fractions of sulfur in the fuel component converted to a dry ash-free state, %
t_{b}	burning time, s
t_{d}	ignition delay time, s
T_{f}	flash point temperature, °C
T_{g}	ambient air temperature, °C
T_{ign}	ignition temperature, °C
V^{daf}	volatile content, %
W^{a}	moisture content, %

References

1. BP Statistical Review of World Energy 2019; Pureprint Group Limited: London, UK, 2019.
2. International Energy Agency (IEA). Coal Information 2019; Coal Information, OECD: Paris, France, 2019.
3. Enerdata. Consumption of Coal and Lignite. Global Energy Statistical Yearbook 2019; Enerdata: Grenoble, France, 2019.
4. Nyashina, G.S.; Legros, J.C.; Strizhak, P.A. Environmental, economic and energetic benefits of using coal and oil processing waste instead of coal to produce the same amount of energy. *Energy Convers. Manag.* **2018**, *174*, 175–187. [\[CrossRef\]](#)
5. Glushkov, D.O.; Paushkina, K.K.; Shabardin, D.P. Co-combustion of coal processing waste, oil refining waste and municipal solid waste: Mechanism, characteristics, emissions. *Chemosphere* **2020**, *240*, 124892. [\[CrossRef\]](#) [\[PubMed\]](#)
6. International Energy Agency (IEA). World Energy Prices; World Energy Prices, OECD: Paris, France, 2019.
7. Glushkov, D.O.; Kuznetsov, G.V.; Paushkina, K.K. Switching Coal-Fired Thermal Power Plant to Composite Fuel for Recovering Industrial and Municipal Waste: Combustion Characteristics, Emissions, and Economic Effect. *Energies* **2020**, *13*, 259. [\[CrossRef\]](#)
8. Glushkov, D.O.; Kuznetsov, G.V.; Strizhak, P.A. Experimental and numerical study of coal dust ignition by a hot particle. *Appl. Therm. Eng.* **2018**, *133*, 774–784. [\[CrossRef\]](#)
9. Lin, Q.; Wang, S.; Liang, Y.; Song, S.; Ren, T. Analytical prediction of coal spontaneous combustion tendency: Velocity range with high possibility of self-ignition. *Fuel Process. Technol.* **2017**, *159*, 38–47. [\[CrossRef\]](#)
10. Wu, D.; Norman, F.; Verplaetsen, F.; Van den Bulck, E. Experimental study on the minimum ignition temperature of coal dust clouds in oxy-fuel combustion atmospheres. *J. Hazard. Mater.* **2016**, *307*, 274–280. [\[CrossRef\]](#)
11. Kurgankina, M.A.; Nyashina, G.S.; Strizhak, P.A. Prospects of thermal power plants switching from traditional fuels to coal-water slurries containing petrochemicals. *Sci. Total Environ.* **2019**, *671*, 568–577. [\[CrossRef\]](#)
12. Glushkov, D.O.; Kuznetsov, G.V.; Paushkina, K.K.; Shabardin, D.P. The main elements of a strategy for combined utilization of industrial and municipal waste from neighboring regions by burning it as part of composite fuels. *Energies* **2018**, *11*, 2534. [\[CrossRef\]](#)
13. Glushkov, D.O.; Strizhak, P.A. Ignition of composite liquid fuel droplets based on coal and oil processing waste by heated air flow. *J. Clean. Prod.* **2017**, *165*, 1445–1461. [\[CrossRef\]](#)

14. Glushkov, D.O.; Kuznetsov, G.V.; Strizhak, P.A. Simultaneous ignition of several droplets of coal–water slurry containing petrochemicals in oxidizer flow. *Fuel Process. Technol.* **2016**, *152*, 22–33. [\[CrossRef\]](#)
15. Heschel, W.; Rweyemamu, L.; Scheibner, T.; Meyer, B. Abatement of emissions in small-scale combustors through utilisation of blended pellet fuels. *Fuel Process. Technol.* **1999**, *61*, 223–242. [\[CrossRef\]](#)
16. Chiew, Y.L.; Shimada, S. Current state and environmental impact assessment for utilizing oil palm empty fruit bunches for fuel, fiber and fertilizer—A case study of Malaysia. *Biomass Bioenergy* **2013**, *51*, 109–124. [\[CrossRef\]](#)
17. Giungato, P.; Barbieri, P.; Cozzutto, S.; Licen, S. Sustainable domestic burning of residual biomasses from the Friuli Venezia Giulia region. *J. Clean. Prod.* **2018**, *172*, 3841–3850. [\[CrossRef\]](#)
18. Cong, H.; Zhao, L.; Mašek, O.; Yao, Z.; Meng, H.; Huo, L.; Yuan, Y.; Jia, J.; Wu, Y. Evaluating the performance of honeycomb briquettes produced from semi-coke and corn stover char: Co-combustion, emission characteristics, and a value-chain model for rural China. *J. Clean. Prod.* **2020**, *244*, 118770. [\[CrossRef\]](#)
19. Nyashina, G.S.; Vershinina, K.Y.; Shlegel, N.E.; Strizhak, P.A. Effective incineration of fuel-waste slurries from several related industries. *Environ. Res.* **2019**, *176*, 108559. [\[CrossRef\]](#) [\[PubMed\]](#)
20. Muazu, R.I.; Stegemann, J.A. Effects of operating variables on durability of fuel briquettes from rice husks and corn cobs. *Fuel Process. Technol.* **2015**, *133*, 137–145. [\[CrossRef\]](#)
21. Mustelier, N.L.; Almeida, M.F.; Cavaleiro, J.; Castro, F. Evaluation of Pellets Produced with Undergrowth to be Used as Biofuel. *Waste Biomass Valorization* **2012**, *3*, 285–294. [\[CrossRef\]](#)
22. Zhang, X.Y.; Chen, M.Q.; Huang, Y.W.; Xue, F. Isothermal hot air drying behavior of municipal sewage sludge briquettes coupled with lignite additive. *Fuel* **2016**, *171*, 108–115. [\[CrossRef\]](#)
23. Isemin, R.; Mikhalev, A.; Klimov, D.; Grammelis, P.; Margaritis, N.; Kourkoumpas, D.S.; Zaichenko, V. Torrefaction and combustion of pellets made of a mixture of coal sludge and straw. *Fuel* **2017**, *210*, 859–865. [\[CrossRef\]](#)
24. Massaro, M.M.; Son, S.F.; Groven, L.J. Mechanical, pyrolysis, and combustion characterization of briquetted coal fines with municipal solid waste plastic (MSW) binders. *Fuel* **2014**, *115*, 62–69. [\[CrossRef\]](#)
25. Pang, C.H.; Hewakandamby, B.; Wu, T.; Lester, E. An automated ash fusion test for characterisation of the behaviour of ashes from biomass and coal at elevated temperatures. *Fuel* **2013**, *103*, 454–466. [\[CrossRef\]](#)
26. Guo, F.; Zhong, Z. Optimization of the co-combustion of coal and composite biomass pellets. *J. Clean. Prod.* **2018**, *185*, 399–407. [\[CrossRef\]](#)
27. McAllister, S.; Chen, J.-Y.; Fernandez-Pello, A.C. *Fundamentals of Combustion Processes*; Springer: Berlin/Heidelberg, Germany, 2011; ISBN 9780387263960.
28. Valiullin, T.R.; Vershinina, K.Y.; Glushkov, D.O.; Shevyrev, S.A. Droplet ignition of coal–water slurries prepared from typical coal- and oil-processing wastes. *Coke Chem.* **2017**, *60*, 211–218. [\[CrossRef\]](#)
29. Vershinina, K.Y.; Kuznetsov, G.V.; Strizhak, P.A. Sawdust as ignition intensifier of coal water slurries containing petrochemicals. *Energy* **2017**, *140*, 69–77. [\[CrossRef\]](#)
30. Valiullin, T.R.; Egorov, R.I.; Strizhak, P.A. Perspectives of the use of rapeseed oil for the doping of waste-based industrial fuel. *Energy Fuels* **2017**, *31*, 10116–10120. [\[CrossRef\]](#)
31. Li, Y.-H.; Lin, H.-T.; Xiao, K.-L.; Lasek, J. Combustion behavior of coal pellets blended with Miscanthus biochar. *Energy* **2018**, *163*, 180–190. [\[CrossRef\]](#)
32. Kijo-Kleczkowska, A.; Środa, K.; Kosowska-Golachowska, M.; Musiał, T.; Wolski, K. Combustion of pelleted sewage sludge with reference to coal and biomass. *Fuel* **2016**, *170*, 141–160. [\[CrossRef\]](#)
33. Si, T.; Cheng, J.; Zhou, F.; Zhou, J.; Cen, K. Control of pollutants in the combustion of biomass pellets prepared with coal tar residue as a binder. *Fuel* **2017**, *208*, 439–446. [\[CrossRef\]](#)
34. Tabakaev, R.; Shanenkov, I.; Kazakov, A.; Zavorin, A. Thermal processing of biomass into high-calorific solid composite fuel. *J. Anal. Appl. Pyrolysis* **2017**, *124*, 94–102. [\[CrossRef\]](#)
35. Glushkov, D.O.; Shabardin, D.P.; Strizhak, P.A.; Vershinina, K.Y. Influence of organic coal-water fuel composition on the characteristics of sustainable droplet ignition. *Fuel Process. Technol.* **2016**, *143*, 60–68. [\[CrossRef\]](#)
36. Glushkov, D.O.; Syrodoy, S.V.; Zhakharevich, A.V.; Strizhak, P.A. Ignition of promising coal-water slurry containing petrochemicals: Analysis of key aspects. *Fuel Process. Technol.* **2016**, *148*, 224–235. [\[CrossRef\]](#)
37. Glushkov, D.O.; Kuznetsov, G.V.; Strizhak, P.A.; Syrodoy, S. V Mathematical model simulating the ignition of a droplet of coal water slurry containing petrochemicals. *Energy* **2018**, *150*, 262–275. [\[CrossRef\]](#)

38. Bazyn, T.; Krier, H.; Glumac, N. Combustion of nanoaluminum at elevated pressure and temperature behind reflected shock waves. *Combust. Flame* **2006**, *145*, 703–713. [[CrossRef](#)]
39. Vershinina, K.Y.; Egorov, R.I.; Strizhak, P.A. The ignition parameters of the coal-water slurry droplets at the different methods of injection into the hot oxidant flow. *Appl. Therm. Eng.* **2016**, *107*, 10–20. [[CrossRef](#)]
40. Glushkov, D.O.; Paushkina, K.K.; Shabardin, D.P.; Strizhak, P.A. Environmental aspects of converting municipal solid waste into energy as part of composite fuels. *J. Clean. Prod.* **2018**, *201*, 1029–1042. [[CrossRef](#)]
41. Timnat, Y.M. *Advanced Chemical Rocket Propulsion*; Academic Press: Cambridge, MA, USA, 1987; ISBN 0126913552.
42. Nyashina, G.S.; Kuznetsov, G.V.; Strizhak, P.A. Effects of plant additives on the concentration of sulfur and nitrogen oxides in the combustion products of coal-water slurries containing petrochemicals. *Environ. Pollut.* **2020**, *258*, 113682. [[CrossRef](#)]
43. Glushkov, D.O.; Nyashina, G.S.; Medvedev, V.V.; Vershinina, K.Y. Relative environmental, economic, and energy performance indicators of fuel compositions with biomass. *Appl. Sci.* **2020**, *10*, 2092. [[CrossRef](#)]
44. Akhmetshin, M.R.; Nyashina, G.S.; Strizhak, P.A. Comparative analysis of factors affecting differences in the concentrations of gaseous anthropogenic emissions from coal and slurry fuel combustion. *Fuel* **2020**, *270*, 117581. [[CrossRef](#)]



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