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# Parametric Robust Control of the Multivariable $2 \times 2$ Looper System in Steel Hot Rolling: A Comparison between Multivariable QFT and $H_\infty$

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**Abstract:** Two robust multivariable controllers,  $H_\infty$  and a decentralized quantitative feedback theory (QFT), are designed in the frequency domain for the  $2 \times 2$  looper system in a steel hot rolling mill to keep stability in the presence of parametric uncertainties. The  $H_\infty$  controller is designed by using the mixed sensitivity approach, while the multivariable decentralized QFT is designed by the extension of the sequential loop closing method presented elsewhere. Stability robustness conditions are verified in the frequency domain, while simulations in time domain are carried out to evaluate the controllers and compare their performance along with that of proportional + integral (PI) and single input single output (SISO) QFT controllers designed earlier. The QFT controller shows the best balance among the performance indicators analyzed here; however, at the expenses of using higher power in one of the control inputs.

**Keywords:** robust control; multivariable control; QFT;  $H_\infty$ ; hot rolling; looper control; parametric uncertainties

## 1. Introduction

A hot strip mill (HSM) is a process that rolls steel slabs into coiled strips. The finishing mill (FM), where the strip takes the final thickness, is the most critical process in an HSM because of the great number of variables involved, interactions between them, and hence its modeling complexity and uncertainty [1,2]. On the other hand, as with many other industrial processes, the environment is highly noisy.

The FM has to attain desired strip thickness and finishing temperature, therefore, controlling these variables and those that have an impact on them is highly important. Most FMs are controlled by proportional + integral (PI) control strategies, which are not designed to compensate for the above-mentioned difficulties. During the past two decades, control of relevant aspects related to thickness has been an active research topic in the literature [3–8]. Special attention has been paid to the looper system variables, tension and looper angular position, owing mainly to their great influence on strip thickness and finishing temperature [2]. Several control approaches for these variables with the aim of achieving stability and performance in the presence of uncertainties and interactions have been proposed.

$H_\infty$  control schemes were proposed for thickness and mass flow loops to achieve robustness in the presence of sensor failures [9]. A  $2 \times 2$  multivariable robust parametric  $H_\infty$  controller was designed for thickness and looper angular position [10]. Two  $H_\infty$  robust controllers for strip tension were presented; one of them designed using Lyapunov–Krasovskii method and LMIs and the other by the conventional 2-Riccati-equation based method [11]. Chen et al. proposed a discrete-time  $H_\infty$  robust controller [12];

while a two nested closed loop scheme, a decoupling decentralized control and an  $H_\infty$  robust controller, was presented in [13].

Hearns and Grimble [14] proposed an inferential control designed by the quantitative feedback theory (QFT) technique for strip tension control. The same authors [15] have presented a control based on QFT technique for the looper system, however, the standard approach found in the literature [16,17] was modified for that particular application.

Two single loop QFT parametric robust controllers for strip tension and looper angular position were designed [18]. Tests under parametric uncertainty have been conducted within a  $2 \times 2$  scheme of the looper system, comparison with conventional PI controllers have also been carried out. A single loop parametric robust QFT controller for strip thickness was also designed [19]. It was also tested in a  $2 \times 2$  scheme together with the looper angular position presented in [18] and performance was compared with that of PI controllers.

Although the present work is concerned with those techniques using a fixed linear robust controller in the frequency domain, it is worth mentioning that model based predictive controllers (MPC) [20–23] as well as non-linear techniques [24,25] have been applied to the looper system.

As shown by the above survey, there is as great concern about achieving robustness and interaction rejection for the looper system in an HSM by  $H_\infty$  and QFT control design techniques. Hence, anticipating potential applications on an actual HSM, it would be worthwhile to evaluate the techniques and compare their performance using controllers designed by standard approaches commercially available in control design software tools such as MATLAB. Thus, in this work, two multivariable parametric robust controllers are designed, QFT and  $H_\infty$ , for the multivariable  $2 \times 2$  looper system. As far as the author knowledge is concerned, MIMO QFT controllers have not been applied to the looper system in an HSM. The QFT controller is designed by the decentralized QFT control technique for multivariable processes (mvQFT) as given in Yaniv [26] using the MATLAB/QFT toolbox; while the  $H_\infty$  controller was designed by the mixed sensitivity approach and the standard 2-Riccati-equation solution using the MATLAB HINF function. The controllers are also compared with PI controllers, which are the current controllers in most HSMs worldwide, and the two SISO QFT controllers presented in [18], when applicable; evaluating in this way, the potential benefits of compensating for interactions and parameter uncertainty. The multivariable linearized HSM model presented and experimentally validated in Obregon et al. [2] has been built in Simulink to perform time domain tests.

The paper is organized as follows. Section 2 describes briefly the model used in this work. Section 3 presents the fundamentals of the QFT and  $H_\infty$  control techniques. Section 4 deals with the controllers designed for the looper system. In Section 5 the simulation results are presented and discussed, and finally, Section 6 presents the conclusions.

## 2. FM Multivariable Model

Two FM contiguous stands,  $i$  and  $i + 1$ , and the looper  $i$  between them were represented by a linear  $4 \times 4$  multivariable model [2]. The assumption of a linear behavior is realistic, since the mill operates under small signal regime once the steel bar has been threaded.

Figure 1 is a schematic representation of the two modeled stands, while the model block diagram is shown in Figure 2a. To validate the model, it was built in Simulink and tests were performed with data from the real mill, concluding that it was a good approximation of the process [2]. To derive the model some blocks were represented directly in Laplace while the nonlinear static relations involved were linearized around an operating point. The operating conditions were defined according to the rolling practice of the most commonly rolled product in stands 3 ( $i$ ) and 4 ( $i + 1$ ). In Figure 2a,  $\delta$  denotes small perturbation; the symbol  $K_x^y$  denotes a static gain obtained from linearization, this being  $\frac{\partial y}{\partial x}$  evaluated at the operating conditions; a plus symbol (+) or a minus symbol (−), on either the superscript or the subscript of  $K_x^y$  denote  $i + 1$  and  $i - 1$  stands respectively. The symbology is shown in Table 1.

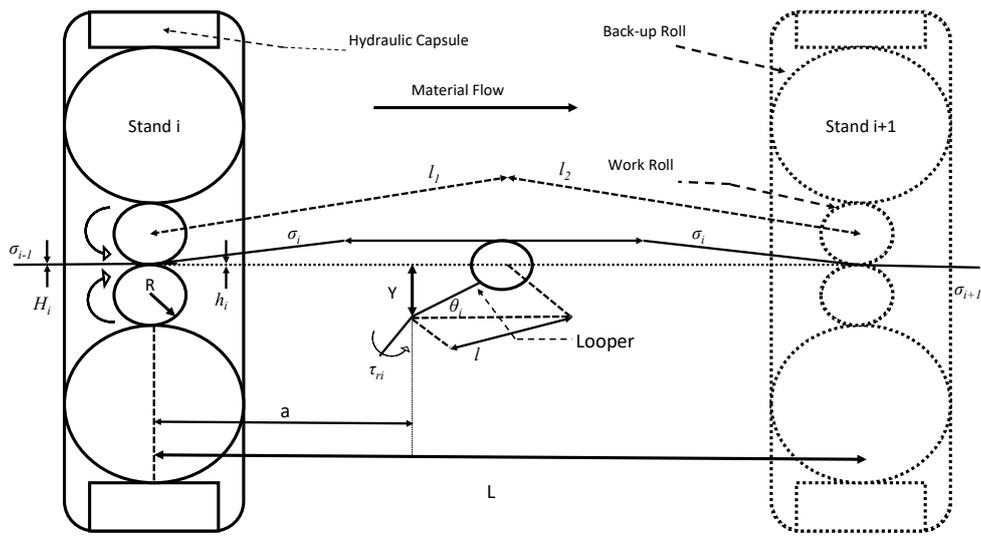


Figure 1. Schematic of two contiguous stands in an FM.

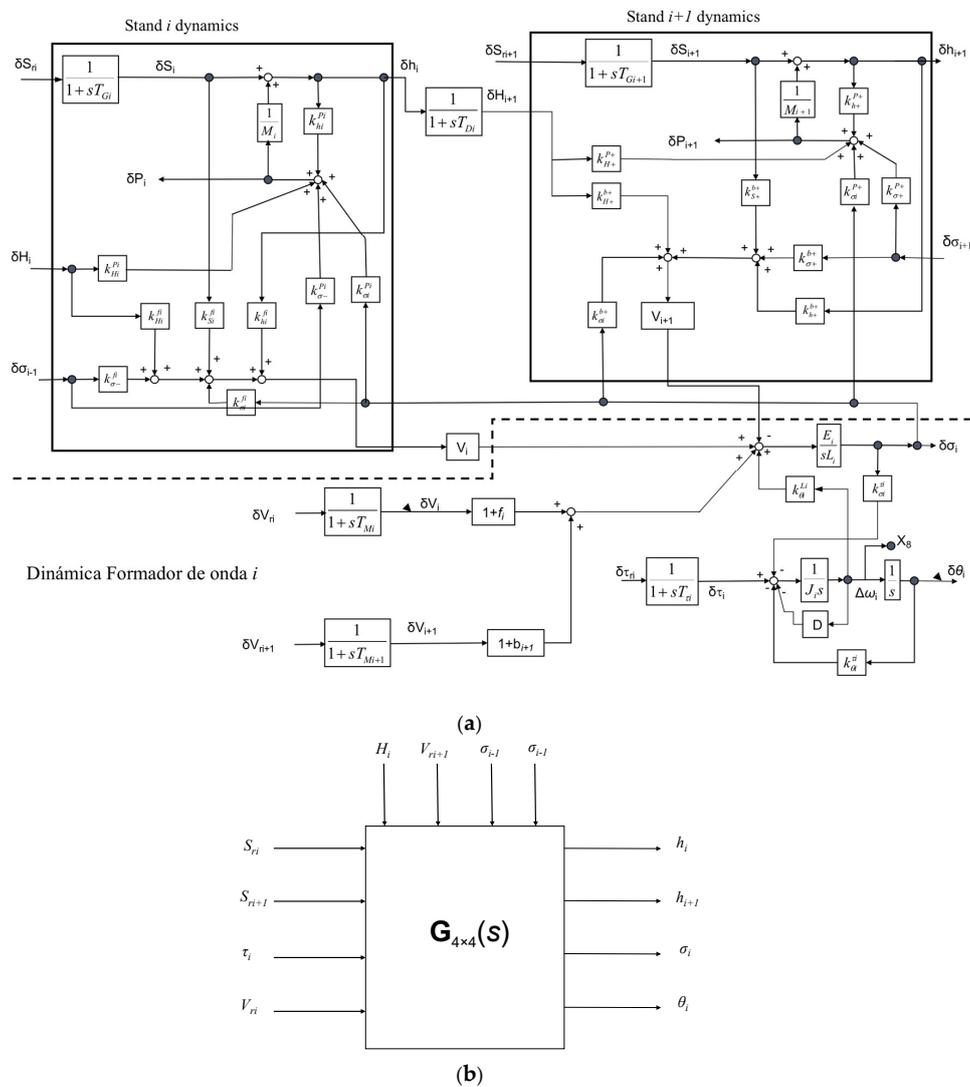


Figure 2. (a) Block diagram of the multivariable linear model of two contiguous stands of an FM, and (b) One-block representation of the model.

**Table 1.** Variables and physical parameters.

Variable	Symbol	Units	Parameter	Symbol	Units
Stand $i$ hydraulic cylinder position reference	$S_{ri}$	m	Stand $i$ mill modulus	$M_i$	N/m
Stand $i + 1$ hydraulic cylinder position reference	$S_{ri+1}$	m	Stand $i + 1$ mill modulus	$M_{i+1}$	N/m
Stand $i$ roll linear velocity reference	$V_{ri}$	m/s	Steel Young's modulus at operating temperature	$E_i$	N/m <sup>2</sup>
Looper $i$ torque reference	$\tau_i$	Nm	Looper $i$ roll radius	$r$	m
Stand $i$ exit thickness	$h_i$	m	Distance between stand $i$ and $i + 1$ backup roll centers	$L_i$	m
Stand $i$ entry thickness	$H_i$	m	Steel density	$\rho$	Kg/m <sup>3</sup>
Stand $i + 1$ exit thickness	$h_{i+1}$	m	Looper $i$ momentum of inertia	$J_i$	Kgm <sup>2</sup>
Stand $i - 1$ exit tension	$\sigma_{i-1}$	N	Looper $i$ friction	$D_i$	Nm/rad/s
Stand $i$ roll linear velocity	$V_i$	m/s	Stand $i$ cylinder position regulator time constant	$T_{Gi}$	s
Stand $i + 1$ roll linear velocity reference	$V_{ri+1}$	m/s	Stand $i + 1$ cylinder position regulator time constant	$T_{Gi+1}$	s
Stand $i$ exit tension	$\sigma_i$	N	Time constant of delay approximation between $h_i$ y $H_{i+1}$	$T_{Di}$	s
Stand $i + 1$ exit thickness	$\sigma_{i+1}$	N	Stand $i$ work roll speed regulator time constant	$T_{Mi}$	s
Looper $i$ length	$l_i$	m	Stand $i + 1$ work roll speed regulator time constant	$T_{Mi+1}$	s
Looper $i$ angular position	$\theta_i$	Radians	Looper $i$ torque regulator time constant	$T_{\tau i}$	s
Stand $i$ roll separation force	$P_i$	N	Stand $i$ forward slip	$f_i$	-
Stand $i + 1$ roll separation force stand $i + 1$	$P_{i+1}$	N	Stand $i + 1$ backward slip	$b_{i+1}$	-

The four model outputs are: (1) stand  $i$  exit strip thickness ( $h_i$ ), (2) stand  $i + 1$  exit strip thickness ( $h_{i+1}$ ), (3) strip tension ( $\sigma_i$ ), and (4) looper  $i$  angular position ( $\theta_i$ ). Their corresponding control inputs according to the conventional coupling are: (1) position reference for stand  $i$  hydraulic cylinder ( $S_{ri}$ ), (2) position reference for stand  $i + 1$  hydraulic cylinder ( $S_{ri+1}$ ), (3) torque reference for looper  $i$  motor ( $\tau_{ri}$ ), and (4) speed reference for stand  $i$  motor ( $V_{ri}$ ). The stand  $i$  input thickness ( $H_i$ ), the speed reference for stand  $i + 1$  motor ( $V_{ri+1}$ ), the stand  $i - 1$  tension ( $\sigma_{i-1}$ ), and the stand  $i + 1$  tension ( $\sigma_{i+1}$ ) are considered to be perturbations. A remark is worthwhile here, although  $V_{ri+1}$  is the drive speed reference for the stand  $i + 1$  motor, it is the control input for  $\theta_{i+1}$  controlled by the upstream controller; however, it may cause variations on  $\sigma_i$ , acting as a perturbation for the looper  $i$  controller. Figure 2b shows the model representation in one block.

In this work, two robust controllers for the  $2 \times 2$  looper system will be designed. The reduced  $2 \times 2$  plant is a 5th order matrix transfer function (TFM) with one pair of complex poles. The TFM  $\mathbf{G}(s)$  of the linearized system is given by:

$$\begin{bmatrix} \sigma_i \\ \theta_i \end{bmatrix} = \mathbf{G}(s) \begin{bmatrix} \tau_i \\ V_{ri} \end{bmatrix}, \quad (1)$$

where

$$\mathbf{G}(s) = \begin{bmatrix} g_{11}(s) & g_{12}(s) \\ g_{21}(s) & g_{22}(s) \end{bmatrix} \text{ and}$$

$$\begin{aligned}
 g_{11}(s) &= \frac{-107.8s^2 - 52.83s}{s^5 + 9.129s^4 + 1939s^3 + 1.124 \times 10^4 s^2 + 8495s + 1336} \\
 g_{21}(s) &= \frac{12.12s^2 + 49.4s + 16.45}{s^5 + 9.129s^4 + 1939s^3 + 1.124 \times 10^4 s^2 + 8495s + 1336} \\
 g_{12}(s) &= \frac{81.59s^3 + 44.32s^2 + 1.606 \times 10^4 s + 7873}{s^5 + 9.129s^4 + 1939s^3 + 1.124 \times 10^4 s^2 + 8495s + 1336} \\
 g_{22}(s) &= \frac{1.578 \times 10^4 s - 7737}{s^5 + 9.129s^4 + 1939s^3 + 1.124 \times 10^4 s^2 + 8495s + 1336}
 \end{aligned}$$

Six parameters are considered to be uncertain, owing to the huge complexities involved on the parameter uncertainty identification, being generally subject to measurement uncertainties and noise, the uncertainty regions will be assumed to have a given size depending on each parameter as explained below.

A large uncertainty was assumed to be of  $\pm 20\%$  around the operating value. This was assigned to two physical parameters  $E_i$  and  $D$  due to the following reasons. In [2],  $E_i$  was taken from the ASM manual [27], however, only values up to  $400^\circ\text{C}$  are provided. The strip temperature between stands 3 and 4 in the HSM of study is approximately  $800^\circ\text{C}$ ,  $E_i$  value was extrapolated by using the slope between the last two points provided. Notwithstanding, since  $E_i$  decreases more rapidly above  $400^\circ\text{C}$  [27], the slope should be steeper and hence a large uncertainty was assumed. On the other hand,  $D$  was experimentally tuned, assuming as well to have a large uncertainty.  $J_i$  was calculated from the looper geometry and it was considered to have a medium size uncertainty of  $\pm 10\%$ . The gains  $K_{\theta_i}^{L_i}$ ,  $K_{\sigma_i}^{\tau_i}$ , and  $K_{\theta_i}^{\tau_i}$  were calculated from linearization of well-established nonlinear relations as well as rolling practices long-accepted in the real-life mills; therefore, they were considered to be bounded within a small uncertainty region of  $\pm 5\%$ .

Figure 3a shows the largest and the smallest singular values in the frequency domain of the TFM  $\mathbf{G}(s)$ , denoted by  $\bar{\sigma}(\mathbf{G}(s))$  and  $\underline{\sigma}(\mathbf{G}(s))$  respectively.  $\bar{\sigma}(\mathbf{G}(s))$  and  $\underline{\sigma}(\mathbf{G}(s))$  are the largest and smallest possible gains for all input directions at each frequency. Five values uniformly distributed within each parameter uncertainty region were considered; given the six uncertain parameters aforementioned  $5^6$  different plants are obtained. Figure 3b shows  $\bar{\sigma}$  for all the  $5^6$  plants. It can be seen that the largest behavior deviation is between 30 and 70 rad/s.

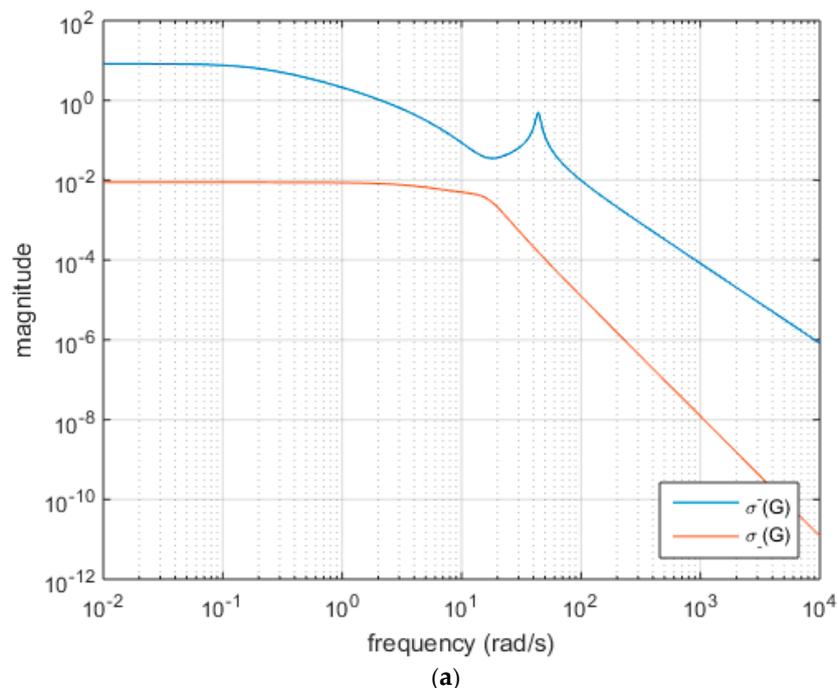


Figure 3. Cont.

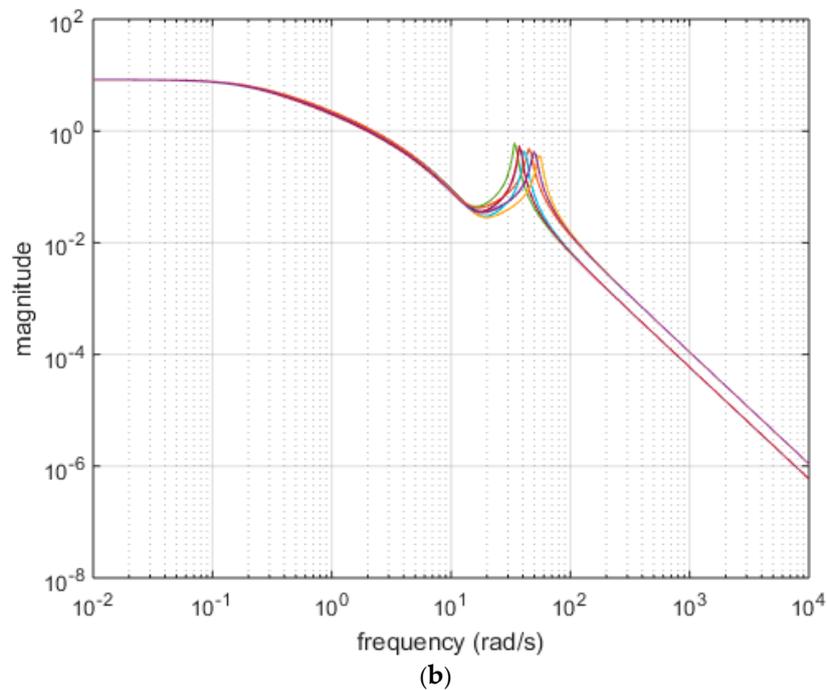


Figure 3. (a)  $\bar{\sigma}(G(s))$  and  $\underline{\sigma}(G(s))$ , and (b)  $\bar{\sigma}(G(s))$  for all possible plants.

### 3. Methodology

#### 3.1. Multivariable Decentralized Robust QFT Controller

The QFT robust control technique was originally proposed for single-input single-output (SISO) systems and it is aimed to keep stability and performance in the presence of parametric uncertainties [16,17]. The parametric uncertainty is modeled as a set of plants  $\{\Pi\}$  in which every particular plant  $G(s) \in \Pi$  is generated by a given set of parameter values.

A finite and sufficiently large number of plants  $G(s) \in \Pi$  is plotted in the frequency domain by using the Nichols chart for some determined working frequencies. A collection of points represents the frequency response of the plotted plants at any given working frequency. The outer points delimit an uncertainty area on the Nichols chart called “templates”. Considering the two-degrees of freedom unity feedback closed loop scheme of Figure 4, assuming the scalar case, the closed loop transfer function can be expressed as:

$$T(s) = \frac{G(s)K(s)}{1 + G(s)K(s)}F(s)$$

where  $K(s)$  and  $F(s)$  are the controller and the prefilter transfer functions respectively, and  $T(s)$  should remain stable for all  $G(s) \in \Pi$ .

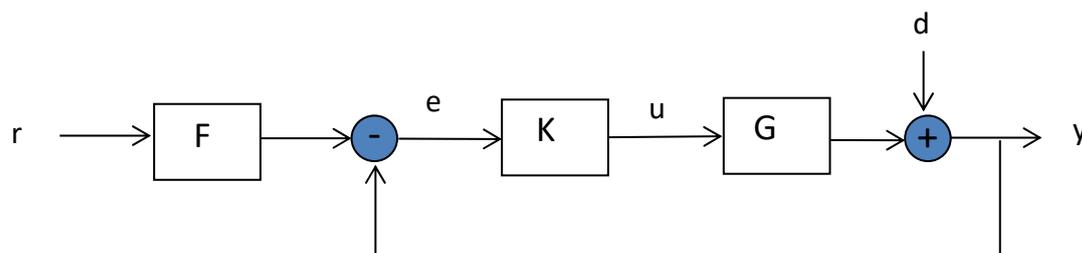


Figure 4. Two-degrees of freedom close loop system.

The closed loop system should also satisfy the following conditions:

1. for tracking specifications:

$$a(\omega) \leq |T(j\omega)| \leq b(\omega), \forall \omega \text{ and } G(s) \in \Pi \quad (2)$$

where  $0 \leq |a(\omega)| < |b(\omega)| \forall \omega$ .

2. and for disturbance rejection specifications:

$$|S(j\omega)| \leq d(\omega), \forall \omega \text{ and } G(s) \in \Pi \quad (3)$$

where  $S$  is the sensitivity function to output disturbances.

A nominal plant  $G_0(s) \in \Pi$  is arbitrarily chosen, then, by using the so-called M-circles, specification boundaries are obtained for the nominal open loop ( $L_0(j\omega)$ ) at each working frequency. The controller  $K(s)$  is designed by loopshaping such that the nominal plant is above the boundaries; however, the technique ensures all the possible open loops conformed by  $K(s)$  and all the plants within the template ( $L(j\omega)$ ) fulfill conditions given in Equations (1) and (2).

For an  $n \times n$  multi-input multi-output (MIMO) system, assuming a diagonal controller, the problem was replaced by  $n \times n$  single loops [16,17]. The method was further developed using iteratively the sequential loop closing technique [26]. In this work, this method is used to design a decentralized mvQFT controller for the looper system.

Given a multivariable two-degrees of freedom closed loop scheme (Figure 4) with  $G \in \Pi$  the plant TFM,  $\Pi$  the set of uncertain MIMO plants, and  $K$  and  $F$  the controller and prefilter TFMs respectively, the complementary sensitivity TFM is given by:

$$T = GK(I + GK)^{-1}F, \quad (4)$$

should remain stable  $\forall G \in \Pi$ .

Assuming a square  $n \times n$  plant  $G$ , the conditions given in Equations (1) and (2) are extended for multivariable systems as follows:

$$a_{ij}(\omega) \leq |t_{ij}(j\omega)| \leq b_{ij}(\omega), \forall \omega \text{ and } G(s) \in \Pi, \quad (5)$$

and

$$|1 + L_i^n| \geq D_i(\omega), \forall \omega \text{ and } G(s) \in \Pi, \quad (6)$$

where  $i = 1, \dots, n, j = 1, \dots, n, t_{ij}$  is the  $(i, j)$  element of  $T$ , and  $L_i^n$  is the  $i$ -loop transfer when only the  $i$ -loop is open.

It has been shown that by using the sequential loop closing method, condition (5) is fulfilled, and for condition (6) to be satisfied, the recursive procedure proposed in [26] is sufficient. Such procedure was used in this work.

### 3.2. $H_\infty$ Robust Controller

The  $H_\infty$  controller is designed by the mixed-sensitivity approach, which is based on the general control problem scheme depicted in Figure 5a. The general control problem scheme is built from the conventional control scheme given in Figure 4, assuming  $F = I$ . In Figure 5a,  $w$  represents the external inputs,  $z$  is the output vector with the functions to be minimized,  $P$  is the generalized or augmented plant TFM,  $K$  is the controller TFM and  $\Delta$  is a block diagonal matrix representing the uncertainties with  $\|\Delta\|_\infty \leq 1$ . Assuming again a square  $n \times n$  MIMO plant  $G(s)$ , the dimensions of  $P$  are multiples of  $n$ . The structure of  $P$  greatly depends on the particular control problem definition, a typical definition would be as follows.  $w$  and  $z$  are usually taken as  $w = [r \ d]^T$  and  $z = [e \ u \ y]^T$ , since  $r, d, e, u$  and  $y$ , are all vectors of dimension  $n$ ,  $w$  is a vector of dimension  $2n$  and  $z$  is a vector of dimension  $3n$ . Note that  $u$  is the plant ( $G$ ) input and it might be, as in this case, both, input and output of  $P$ , see Figures 4 and 5a.

On the other hand,  $v$  is the controller ( $K$ ) input, which is  $e$ , hence it is a vector of dimension  $n$ . Now assuming  $q$  sources of uncertainties,  $u_\Delta$  and  $y_\Delta$  are vectors of dimension  $qn$ . With this considerations,  $P$  would be a matrix of  $(q + 3 + 1)n \times (q + 2 + 1)n$ .  $P$ , in general, is an array of  $n \times n$  blocks expressed in terms of  $G$ ,  $0_{n \times n}$  or  $I_{n \times n}$ , depending on the particular input/output relations [28].

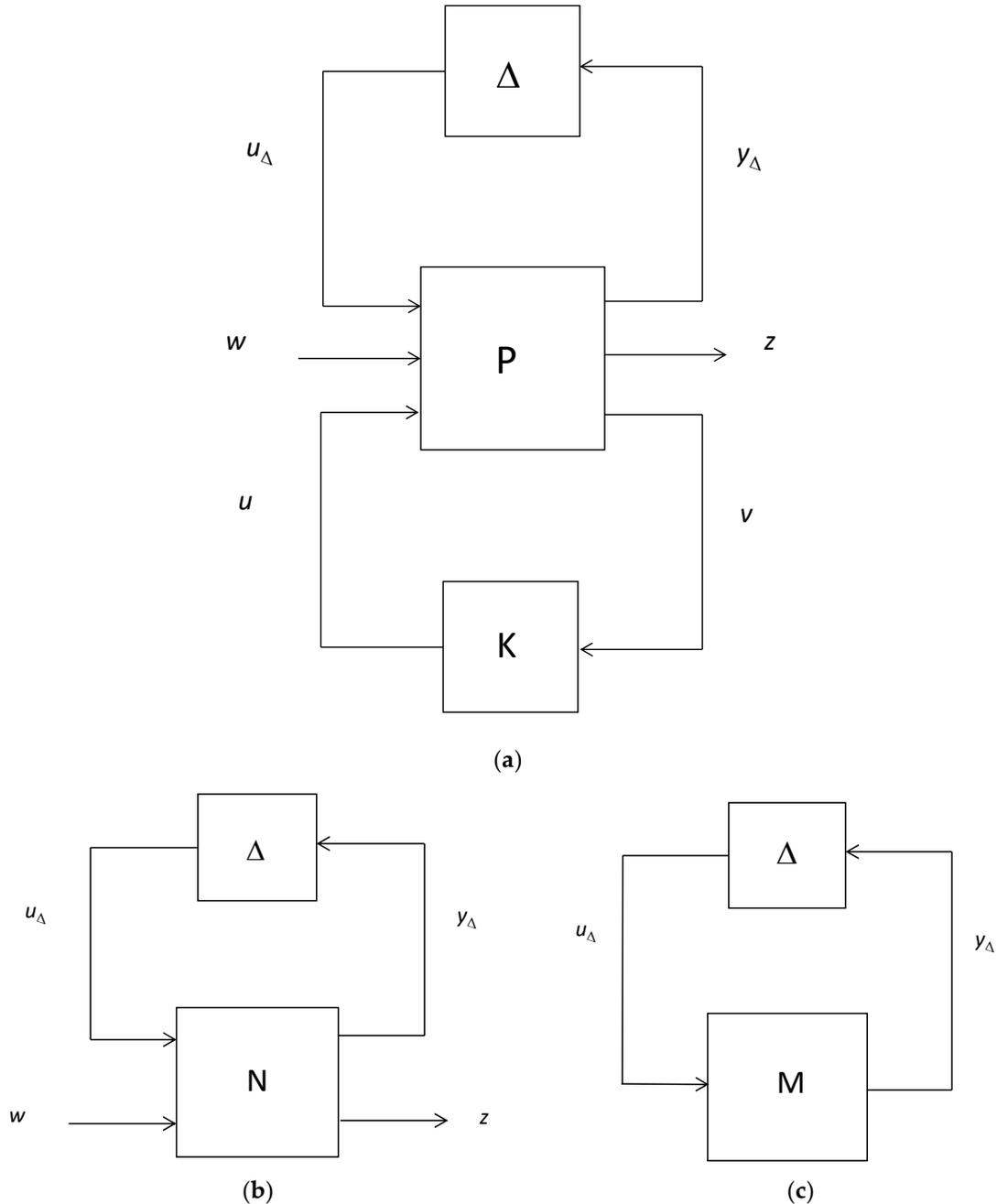


Figure 5. (a) General control configuration, (b) N- $\Delta$  structure, and (c) M- $\Delta$  structure.

The problem is to find a controller that minimizes the  $H_\infty$  norm of the closed-loop transfer function from  $w$  to  $z$ . For analysis purposes the controller can be incorporated and the scheme shown in Figure 5b is obtained. The closed loop transfer function is given by:

$$F_{zw}(N, \Delta) = N_{22} + N_{21}\Delta(I - N_{11}\Delta)^{-1}N_{12}, \tag{7}$$

For stable nominal open loop system and  $\Delta$ , the only source of instability in Equation (10) is the term  $(\mathbf{I}-\mathbf{N}_{11}\Delta)^{-1}$ , therefore, for robust stability in the presence of unstructured uncertainties, it is sufficient to analyzed the so-called “ $\mathbf{M}-\Delta$  structure” with  $\mathbf{M} = \mathbf{N}_{11}$ , and depicted in Figure 5c. The condition for robust stability in the presence of unstructured uncertainties [28] is given by:

$$\|\mathbf{M}\|_{\infty} < 1 \text{ with } \|\Delta\|_{\infty} \leq 1, \quad (8)$$

In this work, the parametric uncertainty will be represented by an unstructured output multiplicative uncertainty, then Equation (8) becomes:

$$\|\mathbf{W}_1 \mathbf{T} \mathbf{W}_2\|_{\infty} < 1 \text{ with } \|\Delta\|_{\infty} \leq 1, \quad (9)$$

where  $\mathbf{W}_1$  and  $\mathbf{W}_2$  are the uncertainty weights.

The  $H_{\infty}$  mixed-sensitivity problem is to find a controller such that:

$$\left\| \begin{array}{c} \mathbf{W}_P \mathbf{S} \\ \mathbf{W}_U \mathbf{K} \mathbf{S} \\ \mathbf{W}_T \mathbf{T} \end{array} \right\|_{\infty} < 1, \quad (10)$$

with  $\mathbf{W}_2 = \mathbf{I}$  and  $\mathbf{W}_1 = \mathbf{W}_T$ ,  $\mathbf{W}_P$  is the nominal performance specification and  $\mathbf{W}_U$  is the plant input weight.

#### 4. Controller Designed

The controllers will be designed to attain stability in the presence of parametric uncertainties for the  $2 \times 2$  looper system assuming null inputs on  $S_{ri}$  and  $S_{ri+1}$ , see Figure 2b; note that the feedback blocks from  $\sigma_i$  to  $V_i$  are still taken into account, see Figure 2a. Six parameters will be considered to be uncertain, as mentioned in Section 2, however, bounded within a region around the parameter operating value. It is worth noting that the design methods used here assume uncertain time-invariant parameters.

The QFT technique models the parametric uncertainty in the frequency domain; hence, to allow a straight comparison, the parametric uncertainty will be modeled in the frequency domain as well for the  $H_{\infty}$  controller design. On the other hand, the controllers will be designed separately searching for the best performance that can possibly be achieved with each technique.

In this work, as in most works on looper control, it is assumed that tension measurement is available, even though it is not usually the case [21,25]. Nonetheless, the parametric uncertainty as modeled here, the plant templates in QFT and a diagonal output multiplicative uncertainty in  $H_{\infty}$  compensate, until certain extent, for the uncertainties introduced by the lack of tension measurements [14,27,29]; representing this a progress with respect to the currents controllers (PI) in the actual mills. Further study on this topic is left for future work.

##### 4.1. *mvQFT Robust Controller Design for the Looper System*

As mentioned, QFT is a frequency domain design technique based on Nichols charts. The design procedure is iterative, and it is usually given in five steps.

Step #1. Specification definition.

The stability robustness specifications are given as follows:

$$0 \leq t_{11} \leq 2 \text{ and } 0 \leq t_{22} \leq 1.9, \quad (11)$$

While the performance specifications that produced the best results given in terms of  $\mathbf{S}$  were the following:

$$\mathbf{S}(s) \leq \left[ \begin{array}{cc} 0.03 \frac{s^3 + 64s^2 + 748s + 2400}{s^2 + 14.4s + 169} & 0.75 \\ 5.2 & 0.045 \frac{s^3 + 64s^2 + 748s + 2400}{s^2 + 14.4s + 169} \end{array} \right], \quad (12)$$

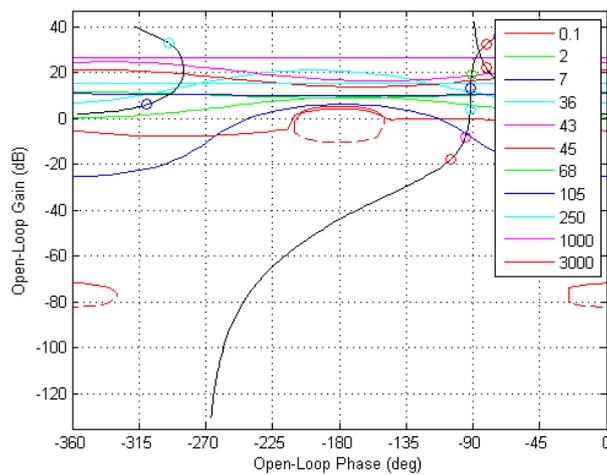
Note that Equation (6) may be obtained from Equation (12).

Step #2. Template generation.

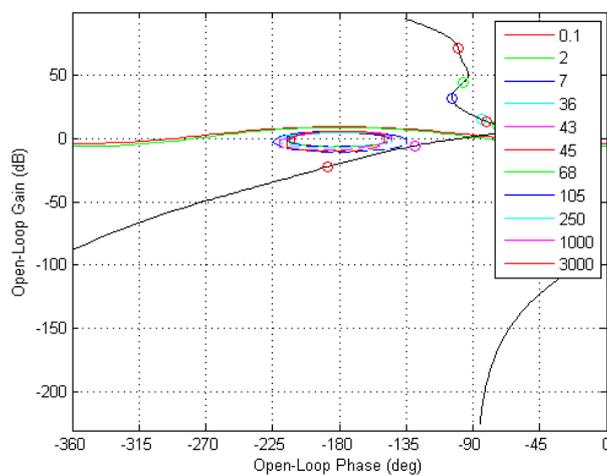
The working frequencies are first selected to plot the frequency response of  $g^l_{uu}(j\omega)$ , which is the diagonal element of  $\mathbf{G}^l \in \Pi$ , where  $\mathbf{G}^l$  is a square TFM as assumed in [26],  $l$  is a finite integer (1, 2, 3, ...,  $v$ ) denoting a given set of parameter values, see Section 2 and Figure 3b, and  $v$  is the total number of sets. This method does not guaranty the worst-case plant to be included; hence it was decided to use an exhaustive number of sets. As mentioned, five values uniformly distributed within each parameter uncertainty region were considered; given the six uncertain parameters aforementioned,  $v$  is equal to  $5^6$ . Therefore, a template is the plot of 15,625 points, corresponding each to every particular  $\mathbf{G}^l \in \Pi$  at any given working frequency. Only the templates for  $g^l_{uu}(j\omega)$  are needed, hence, for the sake of brevity, the plots are not shown here, however they can be found in [18], where it can be seen that the largest templates, meaning the largest uncertainty regions are consistent with Figure 3b. Since the procedure is iterative, the working frequencies were readjusted, the final selected working frequencies in rad/s were: 0.1, 2, 7, 36, 43, 45, 68, 105, 1000, and 3000.

Step #3. Specification boundaries generation.

The specifications boundaries for stability robustness and disturbance rejection are generated in this step; global boundaries are obtained, which are the union of all the particular boundaries for every specification at every working frequency. They are shown in Figure 6, for the sake of brevity they are shown along with  $L_{0u}$  ( $u = 1, 2$ , in this case) designed in the next step.



(a)



(b)

Figure 6. Boundaries and loop-shaping, (a)  $\sigma_i$ , and (b)  $\theta_i$ .

Step #4. Controller Design.

The controller has been designed by loop-shaping in the Nichols Chart by adding poles and/or zeros such that the close-loop system is stable and  $L_0$  is above the specification boundaries at each frequency. In this step the recursive design procedure, mentioned in Section 3.1 and given in [26], is executed assuming  $F = I$ .  $L_{01}$  and  $L_{02}$  for the final design are shown in Figure 6.

Step #5. Specification fulfillment verification.

Specification fulfillment is verified in the frequency domain. In Figure 7a,b plots of  $|t_{ii}(j\omega)|$  and  $|s_{ij}(j\omega)|$  are shown. As can be seen in the plots, the specifications are met.

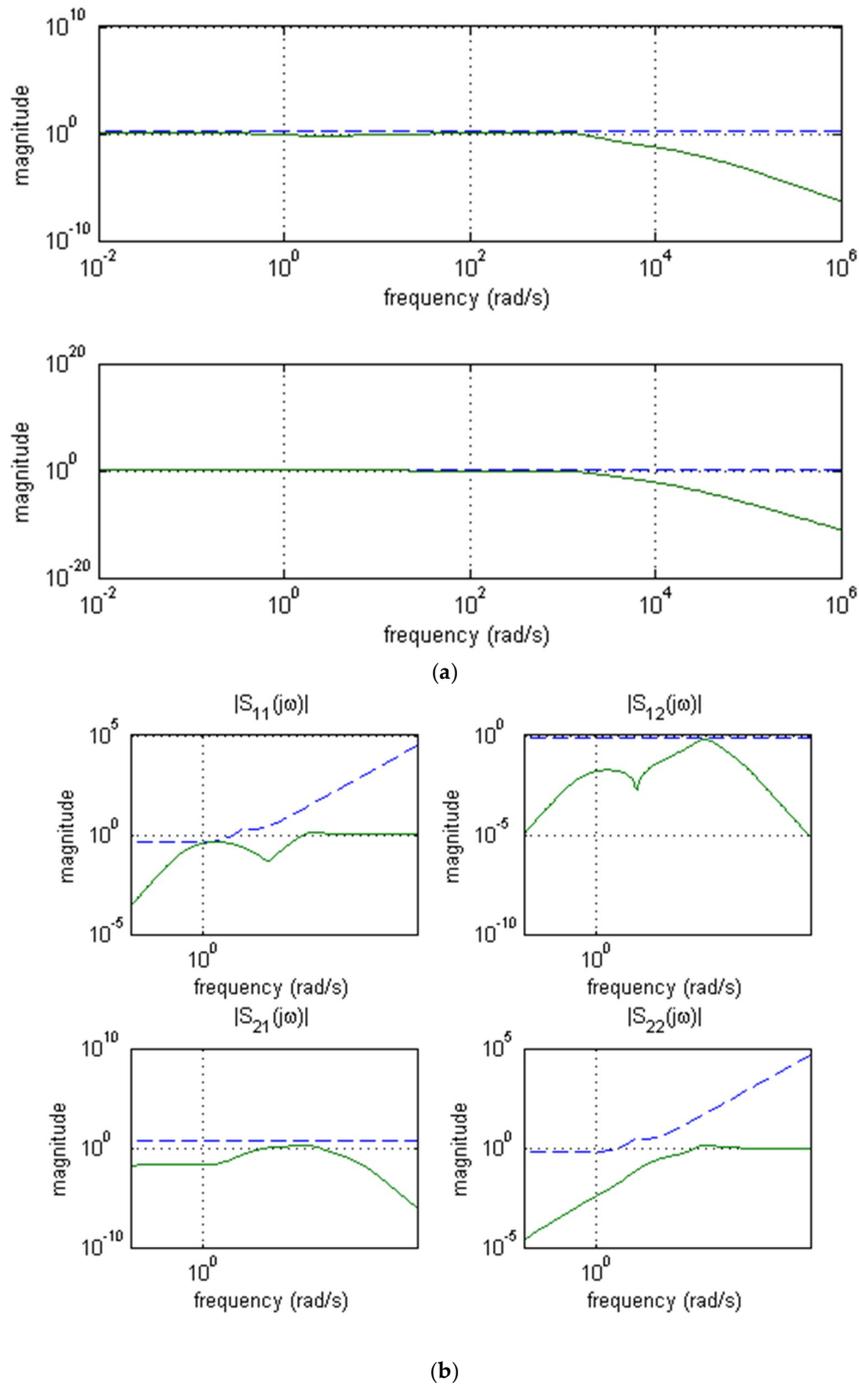


Figure 7. (a) Stability robustness verification and (b) performance robustness verification.

#### 4.2. $H_\infty$ Robust Controller Design for the Looper System

As mentioned, since the mvQFT technique models the parametric uncertainty in the frequency domain, they will also be modeled in the frequency domain for the application of the  $H_\infty$  technique to allow a more direct comparison. The uncertainty will be modeled as unstructured output multiplicative uncertainty with a scalar weight, assuming a disk shape uncertainty region. Using this method, the  $H_\infty$  technique has some disadvantage since only the radius magnitude is required, while QFT is taking into account the specific uncertainty shape, being thus the uncertainty modeling method used here for the  $H_\infty$  technique more conservative.

The disk shape uncertainty region radius magnitude can be expressed as:

$$l_0(\omega) = \max_{\mathbf{G}^l \in \pi} \bar{\sigma} \left[ \left( \mathbf{G}^l(j\omega) - \mathbf{G}_0(j\omega) \right) \mathbf{G}_0(j\omega)^{-1} \right]$$

where  $\mathbf{G}^l$  is as defined above.

The scalar uncertainty weight should be chosen such that:

$$w_O(j\omega) \geq l_0(\omega); \forall \omega$$

Figure 8a shows the plot of  $l_0(\omega)$  and  $w_O(j\omega)$  used for the design, it can be noticed that they are consistent with Figure 3b. Because a scalar weight is used, in Equations (9) and (10)  $\mathbf{W}_T = \mathbf{W}_1 = \mathbf{I}_{2 \times 2} w_O$ , thus, condition (9) can be expressed as

$$\bar{\sigma}(\mathbf{T}) < \frac{1}{|w_O(j\omega)|}, \forall \omega \text{ with } \|\Delta\|_\infty \leq 1, \quad (13)$$

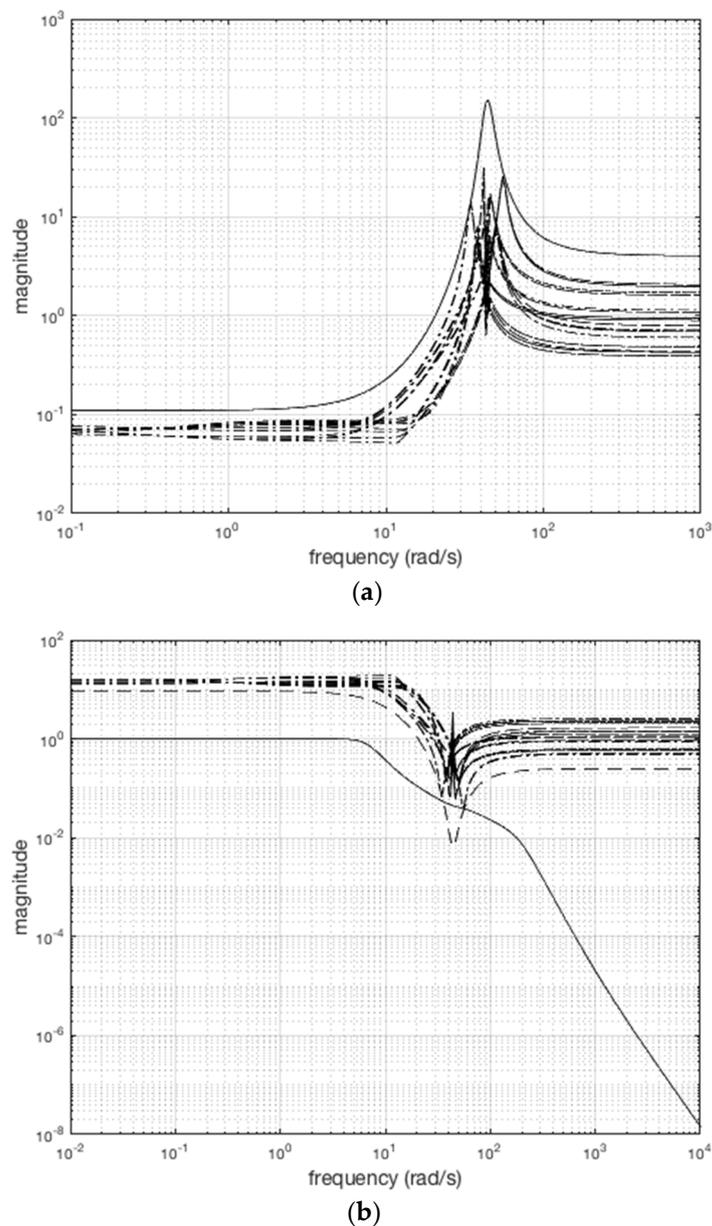
while in Equation (10),  $\mathbf{W}_P$  would be given as:

$$\mathbf{W}_P(s) = \begin{bmatrix} \frac{4 \times 10^3}{0.01^{+1}} & 0 \\ 0 & 2.24 \times 10^3 \frac{2.5s+1}{0.01^{+1}} \end{bmatrix}$$

and  $\mathbf{W}_U = \mathbf{I}_{2 \times 2} w_U(j\omega)$ , where

$$w_U(s) = 2 \times 10^3 \frac{\frac{s}{10} + 1}{1 \times 10^3 + 1}$$

Several designs with different  $w_O(s)$ ,  $\mathbf{W}_P(s)$ , and  $w_U(s)$  were performed trying to get the best results.  $\mathbf{W}_P(s)$ , and  $w_U(s)$  were kept simple to get simpler controllers. It is worth mentioning that using Equation (12) in  $\mathbf{W}_P(s)$  did not produce a stabilizing  $H_\infty$  controller. As can be seen in Figure 8b, condition (13) is not fulfilled. Notwithstanding, in order to get the best response, the design was taken to the limits of  $\frac{1}{|l_0(\omega)|}$ , instead of  $w_O$ , which would be a more realistic representation of the uncertainty set. The controller obtained was a 26th order TFM; however, it was possible to reduce the order to 13th applying balred MATLAB© (R2017a, MathWorks, Natick, MA, USA) function without a noticeable detriment on performance.



**Figure 8.** (a)  $w_O(j\omega)$  (solid) and  $\iota_O(\omega)$  (dashed-dotted), and (b) robustness stability condition (13) verification,  $\bar{\sigma}(T)$  (solid),  $w_O(j\omega)$  (dashed) and  $\iota_O(\omega)$  (dashed-dotted).

## 5. Simulation Results and Discussion

In this section, simulation results in the time domain are presented and discussed. The controllers designed in previous section are tested, their performance is compared with each other and with that of SISO PI and SISO QFT [18] controllers designed earlier. Three close loop control systems were created in Simulink with the implementation of the model of Figure 3a built earlier [2] as the plant. Step responses of the MIMO  $2 \times 2$  closed loop systems for the controllers above designed are simulated,  $S_{ri}$  and  $S_{ri+1}$  were set to zero. Although the controllers would operate under a small signal regime in a real HSM, they are tested by step responses since these are standard test signals. The step inputs applied were equal in magnitude to the operating value of the corresponding input variables; while the outputs were normalized to the operating value of the corresponding output variable. Five scenarios are considered for the simulation tests:

- Nominal Condition Test (N-test). Step responses of the nominal closed loop systems are obtained.
- Decoupling Test (D-test). A step is applied on one reference input while the other remains zero, thus the impact of each reference input on the cross-coupling output is tested. The cross-coupling output response provides a measure of the column diagonal dominance of the closed loop system, i.e., the decoupling capabilities. Here, the value of such a response is referred to as “interaction level” (IL) and it is expected to be low. IL from  $\theta_{iref}$  to  $\sigma_i$  is denoted as  $\theta_i \rightarrow \sigma_i$ , while  $\sigma_i \rightarrow \theta_i$  denotes that from  $\sigma_{iref}$  to  $\theta_i$ . The nominal plant is used for this test. Although, in practice there are no standard limits for IL, in this work, an IL above 10% is considered to be undesirable.
- Parametric Uncertainty Test (U-test). Initially, each parameter takes a random value within its uncertainty region, changing randomly every 2s during the simulation time to allow the response to settle and confirm convergence. The methods used above to model the parametric uncertainties do not guarantee stability for the worst case; therefore, the parameters change randomly to test the system stability under the largest possible number of parameter value combinations (not under parameter variation, since the control techniques used here assume time-invariant uncertain parameters). During these tests, the perturbations inputs remain zero.
- Perturbation Test (P-test). This test is performed with the perturbation signals enabled, while the parameters remain constant on their operating values. Real signals of  $\sigma_{i-1}$  and  $\sigma_{i+1}$  were collected from the HSM and used for these tests.  $H_i$  and  $V_{ri+1}$  were not available, hence sinusoidal signals are used to simulate them, taking each one a random frequency value between 0 Hz and 7 Hz independently. Their frequencies remain constant during the simulation time.
- Uncertainty and Perturbation Test (P+U-test). The conditions of U-test and P-test are combined.

For the sake of brevity, results for the N-test, D-test and P+U-test are shown only. The P+U-test was run a number of times due to its random nature and some of the results with the most critical responses were selected to be shown.

As mentioned, real signals of  $\sigma_{i-1}$  and  $\sigma_{i+1}$  were collected from the HSM, since the mill operates under small perturbation, some small perturbation tests were also run using the real  $\sigma_{i-1}$  and  $\sigma_{i+1}$  and simulated  $H_i$  and  $V_{ri+1}$ , obtaining similar results to those shown here. The perturbation signal frequency range for the P-tests and P+U-test was selected based on a Fourier analysis of several signals collected from the real mill, including  $\sigma_{i-1}$  and  $\sigma_{i+1}$ .

Figure 9a,b shows the N-test responses. Table 2 shows the step response characteristics for each controller, the best characteristic by column is highlighted in bold characters. In Table 2,  $M_p$  is the maximum overshoot,  $t_p$  the time at which the maximum overshoot is presented, and  $t_s$  is the settling time using the 2% criterion. As can be seen, the best system in terms of  $M_p$  and  $t_p$  is that with the  $H_\infty$  controller, while in terms of  $t_s$  the mvQFT controller is the best. Note that the mvQFT controller presents a very short duration overshoot. It should be mentioned as well that the PI controllers were designed for the SISO loops, showing better responses when tested as such. In [18] the SISO QFT controller responses for the N-test are not presented, however they showed slower responses with larger  $M_p$  than  $H_\infty$  and mvQFT controllers. SISO QFT controllers also showed better responses when tested under SISO conditions.

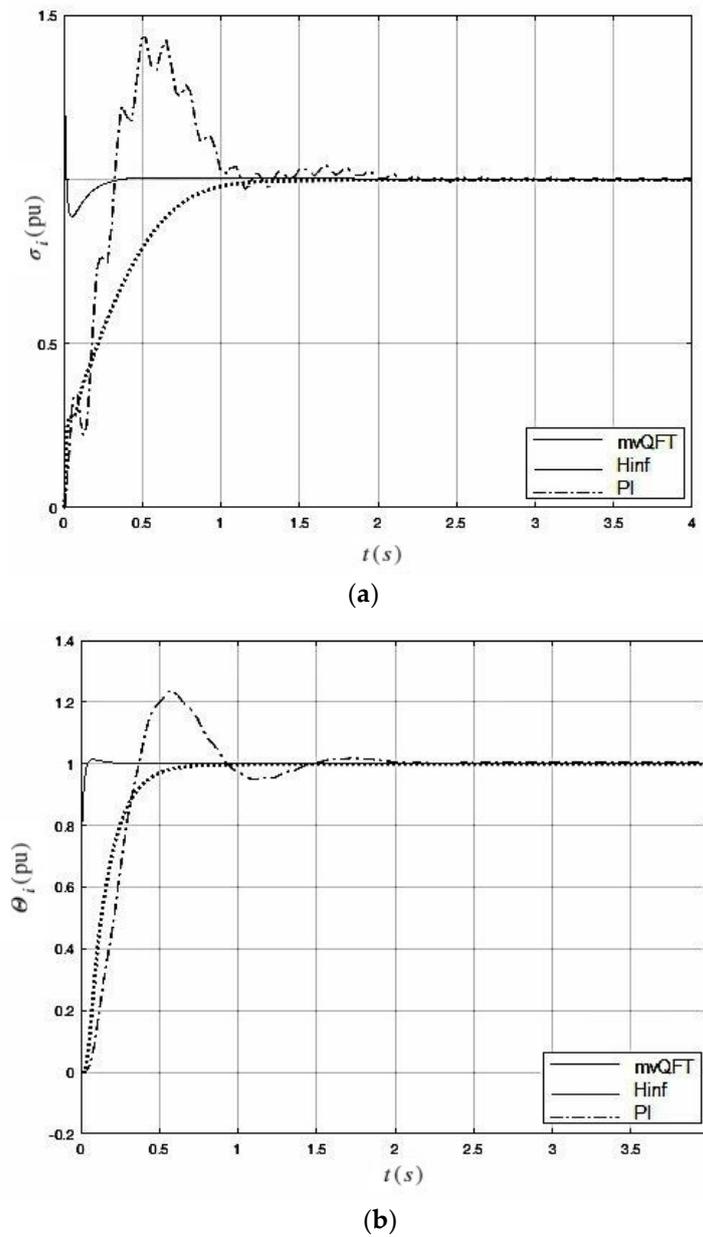


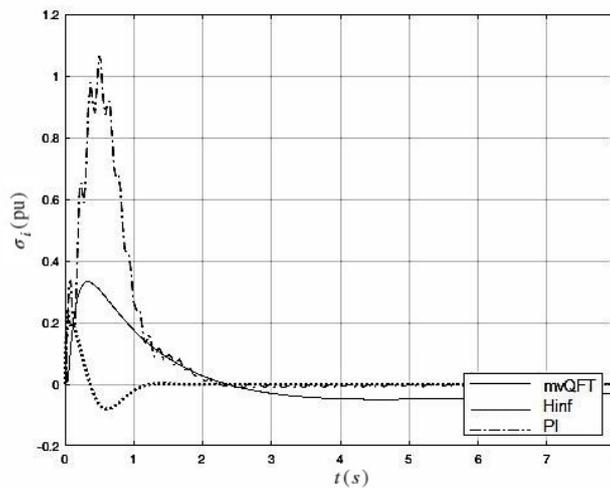
Figure 9. N-Test results (a)  $\sigma_i$ , and (b)  $\theta_i$ .

Table 2. N-test step response characteristics.

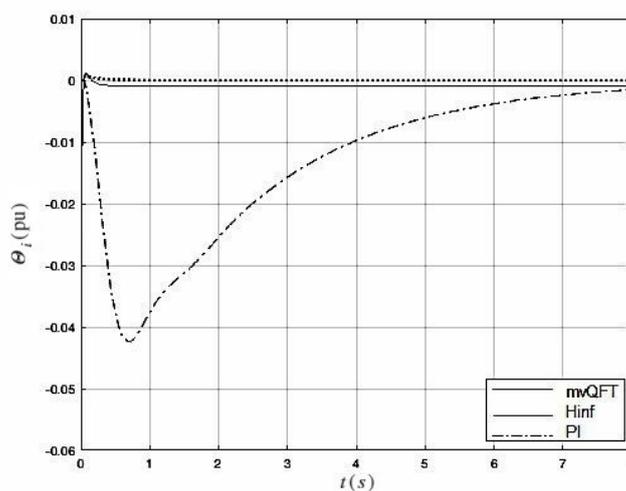
Controller	$\sigma_i$			$\theta_i$		
	$M_p$	$t_p$	$t_s$	$M_p$	$t_p$	$t_s$
PI	43.4%	0.52 s	1.97 s	23.5%	0.56 s	1.364 s
$H_\infty$	null	null	1.012 s	null	null	0.55 s
mvQFT	42%	$3.5 \times 10^{-3}$ s	0.23 s	1.4%	0.075 s	0.32 s

The D-test responses are depicted in Figure 10a,b. Figure 10a shows  $\theta_i \rightarrow \sigma_i$  and Figure 10b shows  $\sigma_i \rightarrow \theta_i$ . Table 3 shows the largest IL of each response during the transient and in steady state. The best IL by column is in bold characters. As can be seen, the  $H_\infty$  controller shows better decoupling capabilities than the mvQFT and PI, as expected since it is a full matrix MIMO TFM; however, the ILs with the mvQFT are satisfactory, less than 0.1 (10%). On the other hand, IL  $\theta_i \rightarrow \sigma_i$  with the PI controller is 1.066 pu (106.6%), which is unacceptable. The SISO QFT controllers in [18] showed higher

interaction levels than  $H_\infty$  and mvQFT controllers, while in the case of  $\theta_i \rightarrow \sigma_i$  was even larger than that presented by PI controllers.



(a)



(b)

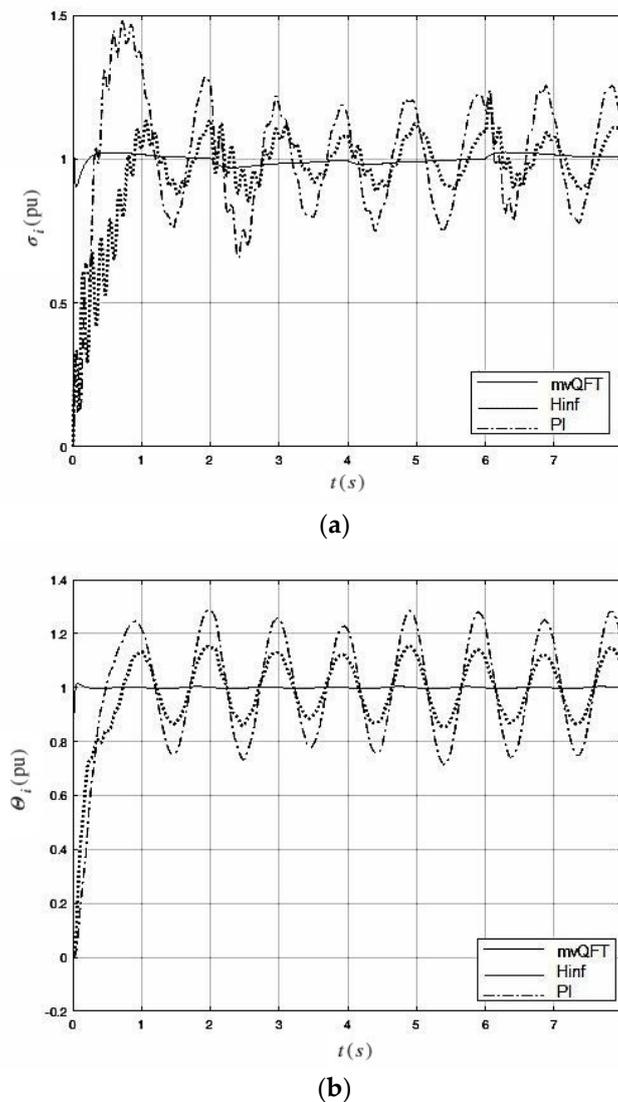
Figure 10. D-Test results (a)  $\sigma_i$  and (b)  $\theta_i$ .

Table 3. Interaction levels.

Controller	$\sigma_i \rightarrow \theta_i$		$\theta_i \rightarrow \sigma_i$	
	Transient	Steady State	Transient	Steady State
PI	-0.042	$1.5 \times 10^{-3}$	1.066	$-0.5 \times 10^{-3}$
$H_\infty$	$0.8 \times 10^{-3}$	null	0.24	null
mvQFT	-0.051	$0.83 \times 10^{-3}$	0.33	-0.03

Figure 11 shows one of the most representative results of the P+U-Test. As can be seen, the responses with PI and  $H_\infty$  controllers show oscillations caused by the perturbation signals; the amplitudes are 130% and 87% larger with the PI controllers, for  $\sigma_i$  and  $\theta_i$  respectively. The mvQFT have considerably better perturbation rejections. In Figure 11, the influence of the parameter changes can only be appreciated in  $\sigma_i$  response as some smaller and faster oscillations than those caused by the perturbations. This is consistent with the U-Test (not shown), the impact of the parameter changes is

larger for  $\sigma_i$  than for  $\theta_i$ . As can be seen in [18] the results for the P+U-Test are improved by the  $H_\infty$  and mvQFT controllers with respect to the response of the SISO QFT controllers.



**Figure 11.** P+U-Test results (a)  $\sigma_i$  and (b)  $\theta_i$ .

In general, the controllers provide absolute stability robustness for the parameter combinations tested. However, the relative stability margins are significantly better for the mvQFT controllers, while the PI controllers showed the worst ones. In fact, in some tests run with PI controllers, the  $\sigma_i$  loop responses showed  $M_p$  values as high as 50%. For the parameter combinations tested here, the mvQFT controller showed better balance between  $M_p$ ,  $t_p$ ,  $t_s$ , IL and robustness than  $H_\infty$ , PI, and SISO QFT [18] controllers; however, this is at the expenses of using greater power. The control signal power values for the three controllers are shown on Table 4. As can be seen, the power of  $\tau_{refi}$  with mvQFT controller is significantly higher than the other control signals. This makes evident the need for the introduction of some control input power limitation criteria in the mvQFT controller designed in future.

**Table 4.** Control input power.

Controller	$\tau_{ri}$	$V_{ri}$
PI	$4.5 \times 10^{-12}$	$3.6 \times 10^{-9}$
$H_{\infty}$	$4.5 \times 10^{-12}$	$5.4 \times 10^{-9}$
mvQFT	3.7	$6.8 \times 10^{-9}$

A great disadvantage of the  $H_{\infty}$  control designed method used here is that a high order full matrix multivariable controller is produced, while the mvQFT is a diagonal TFM of 3rd order. As mentioned, different designs using different weighting function were tested, however there was not a significant impact on the  $H_{\infty}$  control order neither in the power requested by the mvQFT controller. Therefore, these problems should be particularly study in future.

## 6. Conclusions

Two multivariable robust controllers in the presence of parametric uncertainties for the  $2 \times 2$  looper system were designed. These were a decentralized MIMO QFT and an  $H_{\infty}$  controllers, the former had not been applied before for the looper system. The parametric uncertainty was modeled in the frequency domain for both methodologies. The robustness conditions were verified in the frequency domain and time domain simulations were carried out. The performance of the design controllers was compared with each other and along with that of a PI controller and SISO QFT controllers designed earlier. In general, all controllers provided absolute stability robustness. The MIMO QFT controller showed the best balance among all performance indicators analyzed here: maximum overshoot, settling time, disturbance rejection, and interaction levels for different parameter sets; however, at the expense of using greater power on the looper torque control input. The results presented here showed the potential benefits brought by considering uncertainty and systems interactions during the controller designed stage, in this case by MIMO QFT and an  $H_{\infty}$  control techniques. There are some issues to addressed in future: (i) the design of  $H_{\infty}$  controllers of lower order than those designed here, (ii) to limit the power of the plant input for QFT technique, (iii) to study and overcome the problem of lack of tension measurement, and (iv) comparison with other techniques such as MPC and LMIs.

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