

Article

# Stabilization and Crystal Characterization of Electric Arc Furnace Oxidizing Slag Modified with Ladle **Furnace Slag and Alumina**

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Abstract: Ladle furnace slag (LFS) is a by-product of a steel plant. As the chemical composition and free lime (f-CaO) content of each batch of slag are significantly different, it is difficult to use the same operation method to recover LFS. In this study, three types of LFS were used to partially replace lime in the dephosphorization process, and the compositions were adjusted to a fixed range by adding  $Al_2O_3$ . This method reduced the effect of different LFS components and significantly reduced the  $Ca_2SiO_4$  amount (from 31.4% to 17.1%) in the produced modified oxidizing slag. Furthermore, after dephosphorization, the X-ray diffraction (XRD) patterns of the three LFSs indicated transformation into gehlenite and wustite. The modified oxidizing slag f-CaO content was 0.41%, which was lower than that in the electric arc furnace oxidizing slag (1.2–1.4%) and the LFS (0.9–3.4%). In addition, the expansion test results of the modified oxidizing slag showed almost no expansion, which conforms to the ASTM D2940 standards; thus, this material can be used for preparing paving materials. This study provides an approach for LFS treatment that could reduce costs within the steel industry.

Keywords: gehlenite; Ca<sub>2</sub>SiO<sub>4</sub>; f-CaO; volume expansion; dephosphorization; Image-Pro-Plus

# 1. Introduction

The electric arc furnace oxidizing slag (EAFS) and ladle furnace slag (LFS) are by-products of a metallurgical process. LFS is produced in the final stages of steelmaking and is composed of over 50% CaO and MgO by weight. Free lime (f-CaO) is produced in LFS as a result of undissolved CaO solids, which affect LFS volumetric instability. The dissociation of dicalcium silicate (β-Ca<sub>2</sub>SiO<sub>4</sub>, C<sub>2</sub>S) and tricalcium silicate (Ca<sub>3</sub>SiO<sub>5</sub>, C<sub>3</sub>S) produces f-CaO hydrate in a short period and causes expansion [1–4]. Generally, in a steel plant, aging methods are used to treat slag [5]. In this method, the slag is crushed into an appropriate particle size and stacked in an open field to convert CaO into Ca (OH)<sub>2</sub> through hydration. However, at least three months are required to reduce the f-CaO content in the slag to achieve stability, and the higher the f-CaO content, the longer is the duration needed for stabilization. This also increases the costs of a steel plant. Different operation practices in a steel plant may substantially affect the chemical composition of the slag [1]. In addition, the f-CaO content of LFS in each batch differs, making it difficult to recycle LFS with different components as fixed materials or supplements. LFS has a low recovery potential because of the fine LFS particles and unfavorable leaching performance with water (a pH of between 11.7 and 12.8) [6]; therefore, about 80% of LFS produced in the European Union is landfilled [6,7].

The steel industry produces a large amount of solid LFS every year. Taiwan production of LFS is estimated at around 460 thousand tons (total production of crude steel multiplied by 0.02%) [8], so its final disposal is an important issue and has prompted researchers to seek alternative methods for slag reuse.



Several studies have explored the characteristics of LFS and potential solutions for LFS reuse [3,9–14]. There are two methods of recycling LFS. The first is to use steel slag as a raw material to prepare cement clinker because slag mineral composition includes  $C_3S$ ,  $C_2S$ , tetracalcium aluminoferrite ( $C_4AF$ ), and dicalcium ferrite ( $C_2F$ ), which show cementitious properties when mixed with water [15–18]. However, the effect of different f-CaO contents on cement, the proportion of LFS in the cement, and the limitations due to various regulations are problems hindering practical applications. The second method is to use LFS to partially replace lime in a metallurgical process, given that approximately 50% of LFS is CaO by weight [19,20]. In Taiwan, the estimated volume of lime used in steel is 920 thousand tons. The amount of lime used is greater than the production of LFS. This approach has the potential to effectively reuse LFS. However, as mentioned previously, significant differences in LFS compositions affect the stability of the metallurgical process in a steel plant. Therefore, the application described above has not been widely used in Taiwan.

EAFS has good physical and mechanical properties [21,22], and it is easier to treat and recycle than LFS. EAFS can be used in the road base layers and the hot asphalt mixtures [23,24]. However, several researchers [25,26] have shown that the typical hydrated phase (such as portlandite and calcium silicate) in EAFS releases toxic elements such as Ba, Cr, and V. These hydrated phases may increase the risk of expansion or degradation. However, some studies [26,27] have indicated that gehlenite (Ca<sub>2</sub>Al<sub>2</sub>SiO<sub>7</sub>) has non-hydraulic properties, and that increasing the gehlenite phase content in the slag can improve slag stability.

Lime can react with phosphorus in the dephosphorization process in electric furnaces, thus playing an important role in the process. LFS has a low melting point of around 1400–1500 °C [28,29]. This can accelerate slag liquefaction during dephosphorization. The chemical reactions involved in dephosphorization are as follows:

$$2[P] + 5[O] = (P_2O_5), \tag{1}$$

$$[Fe] + [O] = (FeO),$$
 (2)

$$2[P] + 5 (FeO) + 3 (CaO) = (3CaO \cdot P_2O_5) + 5[Fe],$$
(3)

where [] corresponds to molten iron and () corresponds to the slag. As oxygen is injected into the bath (molten steel), FeO and  $P_2O_5$  are formed and float up to the slag layer. Then,  $3CaO \cdot P_2O_5$  precipitates in the oxidizing slag. Finally,  $3CaO \cdot P_2O_5$  forms a stable  $Ca_3P_2O_8 \cdot Ca_2SiO_4$  solid solution with  $C_2S$  [27]. At this point, adding a certain amount of  $Al_2O_3$  into the oxidizing slag can effectively reduce the amount of  $C_2S$  and form  $Ca_2Al_2SiO_7$ , as shown in the following equation [30]:

$$Ca_{3}P_{2}O_{8} \cdot yCa_{2}SiO_{4} + x(Al_{2}O_{3}) = xCa_{2}Al_{2}SiO_{7} + Ca_{3}P_{2}O_{8} \cdot (y - x)Ca_{2}SiO_{4},$$
(4)

In this study, the methods that enable LFS to be used as a renewable material in dephosphorization were evaluated. Different types of LFS were employed in the induction furnace to simulate the electric arc furnace (EAF) primary refining process (dephosphorization), and  $Al_2O_3$  was added to adjust the composition to a fixed range in the dephosphorization process. This improved stability and reduced the influence of the differences in LFS compositions. Moreover, LFS can be transformed into modified oxidizing slag during dephosphorization. The amount of the hydrated phase (C<sub>2</sub>S) in the EAFS was reduced as much as possible, and the final modified oxidizing slag was transformed into a non-hydraulic phase (Ca<sub>2</sub>Al<sub>2</sub>SiO<sub>7</sub>) with low f-CaO content and low volume expansion. Please note that the composition of the modified oxidizing slag after dephosphorization is similar to that of EAFS (20–45% T-Fe), so the modified oxidizing slag is defined as a modification of EAFS in this study.

## 2. Materials and Methods

#### 2.1. Slag Sampling and Characterization

The slag samples used in this study were supplied by ten different steel plants to understand the current composition of slag. The chemical compositions of the slags were analyzed by wavelength

dispersive X-ray fluorescence (WDXRF) spectroscopy (Supermini 200, Rigaku Corp., Tokyo, Japan) and are listed in Table 1. The major LFS oxides are CaO (40–56 wt.%), Al<sub>2</sub>O<sub>3</sub> (3–29 wt.%), SiO<sub>2</sub> (5–27 wt.%), and MgO (4–18 wt.%). The LFS samples could be divided into three types: (1) a high SiO<sub>2</sub> content (19–27 wt.%), (2) a high Al<sub>2</sub>O<sub>3</sub> content (19–29 wt.%), and (3) a high MgO content (13–18 wt.%). The method to distinguish between LFS and EAFS is the T-Fe content of EAFS (20–45% T-Fe). Because the composition of the modified oxidizing slag is similar to that of EAFS, EAFS will be used as a control group to compare with the modified oxidizing slag.

**Table 1.** Compositions of LFS and EAFS as determined by WDXRF spectroscopy. Types of LFS: (1) a high  $SiO_2$  content, (2) a high  $Al_2O_3$  content, and (3) a high MgO content.

Specimen	Types	Chemical Composition (wt.%)								
Specimen	Types	CaO	SiO <sub>2</sub>	$Al_2O_3$	MgO	T-Fe	MnO	S		
LFS 1	(1)	45.9	21.6	4.2	8.6	1.8	0.3	0.867		
LFS 2	(2)	50.2	11.7	19.9	4.9	2.1	0.3	0.727		
LFS 3	(3)	44.1	17.5	3.4	17.9	2.3	0.6	0.567		
LFS 4	(1)	55.4	27.2	2.7	5.8	1.5	0.4	0.547		
LFS 5	(1)	52.1	19.3	14.8	4.9	0.7	0.1	0.994		
LFS 6	(2)	52.3	5.1	28.9	5.4	0.5	0.1	0.911		
LFS 7	(1)	46.4	21.1	3.9	7.0	1.6	0.5	0.772		
LFS 8	(1)	52.6	23.6	4.2	8.8	0.3	0.2	0.828		
LFS 9	(3)	40.3	15.9	4.8	13.1	4.5	0.6	0.542		
LFS 10	(1)	47.7	21.8	4.3	10.4	2.2	0.7	0.690		
EAFS 1		37.8	11.2	7.4	6.2	25.9	3.4	0.102		
EAFS 2		28.8	11.9	6.4	3.7	28.6	4.9	0.241		
EAFS 3		35.6	10.7	4.5	6.9	28.4	4.5	0.097		

The phase diagram of the CaO–FeO–SiO<sub>2</sub>–Al<sub>2</sub>O<sub>3</sub> system of the analyzed slags is shown in Figure 1 [31]. In Figure 1, the three regions are marked as 1, 2, and 3. The path of the slag in the experiment was  $1\rightarrow 2\rightarrow 3$ . Region 1 corresponds to LFS obtained by LF refining (desulfurization), and the major phases are Ca<sub>2</sub>SiO<sub>4</sub> (C<sub>2</sub>S), Ca<sub>3</sub>SiO<sub>5</sub> (C<sub>3</sub>S), and CaO. Region 2 corresponds to the EAFS obtained by EAF primary refining (dephosphorization), and the major phases are C<sub>2</sub>S and wustite (FeO). Region 3 corresponds to the region expected to be modified by the experiment, and the major phases are gehlenite (C<sub>2</sub>Al<sub>2</sub>SiO<sub>7</sub>) and FeO.



**Figure 1.** Samples identified on the CaO–FeO–SiO<sub>2</sub>–Al<sub>2</sub>O<sub>3</sub> system with a SiO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub> weight ratio of 2.2, reproduced from [31], with permission from Elsevier, 2001

In this study, experiments were performed using 35 kg steel reinforcing bar and 200 g iron powder, and all the experiments were carried out under a normal atmosphere in an induction furnace (Five Power Electric Machinery Mfg. Corp., Taipei, Taiwan). The 35 kg steel reinforcing bar has a phosphorus content of 0.027 wt.%. The furnace was heated at a rate of 20 °C/min up to 1520–1600 °C. Ferrophosphorus was added to adjust the percentage of phosphorus in the molten metals to 0.04–0.05 wt.% (similar to the phosphorus content of scrap steel). The furnace output power ranging from 35 kW to 40 kW was controlled to maintain the necessary temperature, which are shown in Figure 2. A disposable type-B thermocouple was inserted into the molten metals every 5 min to measure the temperature and ensure that the molten metals were held at a fixed temperature (around 1550–1560 °C) for 10–20 min. Supplements (Table 2) were then added for dephosphorization. The dephosphorization time was 20 min. The molten metals were sampled at 0 and 20 min. Finally, the chemical composition of the molten metals was examined by using an optical emission spectrometer (Q8 MAGELLAN, Bruker Corp., Hamburg, Germany). The final slag was analyzed by scanning electron microscopy with energy-dispersive X-ray spectroscopy (SEM-EDS) (IT–100, JEOL Ltd., Tokyo, Japan) and X-ray diffraction (XRD) (D8, Bruker Corp., Fremont, CA, USA).

**Table 2.** Materials of supplement, reagent grade CaO, and  $Al_2O_3$  were used. The amount of  $Al_2O_3$  is 15% to 25% by weight of the slag, depending on the initial chemical composition of the LFS.

Supplements	LFS (g)	CaO (g)	Al <sub>2</sub> O <sub>3</sub> (%)
A (for 200 g metal)	3	3	15-25
A	525	525	15-25
В	1050	0	15-25
С	0	1050	15–25

For the 200 g sample, the experiment differed from that for the 35 kg sample in certain aspects: Iron powder (>99% purity) was placed in an alumina crucible, which in turn was placed in a graphite crucible for heating. The furnace was heated until the desired equilibrium temperature was achieved, and supplements were then added into the molten metals for dephosphorization. The dephosphorization time was 6 min. The molten metals were sampled at 0 and 6 min. This test was performed only on the slag of LFS 1, LFS 2, and LFS 3 (Table 1). Each LFS was subjected to dephosphorization tests three times between 1520 and 1600 °C to ensure the repeatability of the experiment.

#### 2.3. XRD and SEM Analysis

The slags were ground and polished for characterization at room temperature (25 °C) by XRD. Diffraction patterns were measured in a 2 $\theta$  range of 20° to 80° by employing Cu K $\alpha$  radiation at 40 kV and 30 mA, and at a scan speed of 2° min<sup>-1</sup>. The local chemical composition of the slags was measured by SEM-EDS. SEM analysis in the backscattered electron imaging (BEI) mode was performed to identify and verify the different phases indicated by XRD patterns.

#### 2.4. Image-Pro-Plus Processing and Analysis

Image-Pro Plus software (Media Cybernetics Inc., Rockville, MD, USA) was used to quantify the percentage of  $C_2S$  phase in the SEM-BEI images. Ten SEM-BEI images were randomly selected, and the  $C_2S$  phases were filled with color by Color Cube Base of Segmentation in the software. The area of the  $C_2S$  phase was calculated in units of pixels and then divided by the total area to calculate the percentage.

#### 2.5. f-CaO Content Determination

F-CaO content determination testing is carried out according to the patent I600903 [32]. First, 100 mL of deionized water (25 °C) and 6 g of sucrose were added to an Erlenmeyer flask and then stirred until the sucrose completely dissolved. Then, 0.5 g of slag powder (<2 mm particle size) was placed in the Erlenmeyer flask, covered with a cork stopper and stirred with magnetite for 2 h. The solution in the Erlenmeyer flask was then filtered with No. 5C filter paper and was washed twice with 10–20 mL of deionized water. The filtrate was then collected in a flask, and 2.5 mL triethanolamine and 2.5 mL deionized water were added and poured into the filtrate. The pH of the filtrate was adjusted to 13 by using an aqueous solution of 30% KOH. When 0.3 g of the NN indicator was added to the filtrate, the filtrate turned magenta. Titration was carried out using 0.05 M EDTA, and the terminal point was set when the filtrate turned from magenta to blue. The amount of f-CaO can be calculated, as shown in Equation (5).

$$f-CaO(\%) = \frac{EDTA(mL) \times 28.04}{\text{sample weight (g)} \times 100}$$
(5)

## 2.6. Laboratory-Scale Volume Expansion Testing

Volume-expansion testing is carried out according to the potential expansion test method (ASTM D4792). The experimental method was described in detail by Wang et al. [33] and Deniz et al. [28]. In this work, the particle size of the oxidizing slag and LFS is 2.36–5 mm and 0.84–2 mm, respectively. The weight of the sample was 7–8 kg. The sample was measured using a dial gauge and compacted in standard molds (diameter = 1520 mm, height = 1650 mm). The sample was then immersed in hot water at a temperature of 70 ± 3 °C for seven days. During the test, an additional load of 4.54 kg was applied to the sample for seven days. In accordance with ASTM D2940, if the expansion of the sample is below 0.05% within seven days, then the sample can be used for preparing paving materials.

#### 3. Results and Discussion

#### 3.1. Dephosphorization of Modified Oxidizing Slag

In conventional EAF steelmaking operations, the phosphorus content of scrap steel is about 0.03–0.05%. The phosphorus content of general engineering steel is less than 0.03% to meet set standards. Therefore, when the dephosphorization rate reaches 40%, the phosphorus content of the steel can be lower than 0.03%. Lime is usually added for dephosphorization, and the temperature is continuously raised to above 1580 °C, before the final stage of LF refining. It is known that dephosphorization involves an exothermic reaction, and the dephosphorization ability decreases as the temperature increases. Therefore, the relationship between the dephosphorization rate and temperature is important for phosphorus-content calculations in a steel plant. The focus of this study is whether a wide range of LFS can use this approach to reduce phosphorus content to less than 0.03% (dephosphorization rate above 40%) and enable most LFS applications to meet the set standards of general engineering steel. In addition, LFSs 1–6 are already in the three types (Table 1). We believe that LFSs 1–6 are already representative, so LFSs 7–10 were not tested for dephosphorization.

Figure 2 shows the dephosphorization rate of modified oxidizing slag at different temperatures, and the materials of the supplement are shown in Table 2. Table 3 lists the results for different slag compositions. The experimental results showed that the dephosphorization rate when supplement A was used was >45%, and that when supplement B was used was lower. Furthermore, two dephosphorization tests of samples S5A and S5B showed that S5A could greatly improve the dephosphorization rate. In the control group without LFS (S-C), the dephosphorization rate was more than 80%. Supplement A can consume a part of LFS, resulting in the phosphorus content of the molten metal becoming <0.03 wt.%.



**Figure 2.** Relationship between the dephosphorization rate and temperature. S1 (A) is  $LF1 + CaO + Al_2O_3$ , S4 (B) is  $LF4 + Al_2O_3$ . S1–1 (A), S2–1 (A), and S3–1 (A) are tests for 200 g of metal.

Figure 2 shows that the dephosphorization rate and temperature can be fitted to a linear function. The slope values for samples S1-1(A), S2-1(A), and S3-1(A) were -0.23, -0.3, and -0.1, respectively. The composition of three types of LFS varied considerably (Table 1), affecting the slope of dephosphorization. The slope indicates the temperature sensitivity of the slags during the dephosphorization process. If the slag temperature sensitivity is low, it is possible to reduce the phosphorus from the molten slag and transfer it to the molten steel (rephosphorization). Sample S3–1(A) had the lowest temperature sensitivity and the largest slope of dephosphorization. Therefore, it was more stable than S1–1(A) and S2–1(A): its dephosphorization results do not vary greatly due to temperature changes. The reason for this could be that as the MgO content in the LFS 3 slag was 17.9% (Table 1), the slag melting point was higher than those of LFS 1 and LFS 2, and the rate of rephosphorization was reduced. In addition, the slope of S2-(A) was the smallest, and the dephosphorization rate decreased significantly as the temperature increased. The reason for this could be that because  $Al_2O_3$  in the LFS 2 slag was 19.9% (Table 1), dephosphorization was limited in the initial stages of melting as most of the  $C_2S$  phase had been replaced by  $Al_2O_3$ . According to this analysis, the dephosphorization rates of the high-SiO<sub>2</sub>-content slag (LFS 1) and the high-MgO-content slag (LFS 3) were still more than 50% at 1580 °C in case of a modification of the slags with Al<sub>2</sub>O<sub>3</sub>.

Table 3. The compositions of the slag; square brackets indicate the concentration in the metal.

Sample —		Chemical	Compositi	Initial	Final	De-P <sup>1</sup>		
	CaO	SiO <sub>2</sub>	$Al_2O_3$	Fe <sub>x</sub> O	$P_2O_5$	[P]	[P]	(%)
S1 (A)	24.4	8.4	21.7	41.3	0.551	0.0477	0.0197	58.7
S2 (A)	25.8	7.9	20.1	40.2	0.455	0.0451	0.0211	53.2
S3 (A)	24.5	8.6	17.6	44.5	0.546	0.0432	0.0191	55.8
S4 (A)	27.2	7.3	22.3	27.2	0.643	0.0389	0.0156	59.9
S5 (A)	22.3	8.1	20.4	33.6	0.757	0.0496	0.0152	69.4
S4 (B)	23.4	9.9	15.3	35.6	0.445	0.0403	0.0221	45.2
S5 (B)	16.6	13.9	20.3	33.8	0.375	0.0314	0.0192	38.9
S6 (B)	20.8	8.8	24.8	25.9	0.397	0.0495	0.0324	34.5
S-(C)	32.1	4.3	28.7	26.2	0.844	0.0514	0.0081	84.2

<sup>1</sup> De-P = dephosphorization rate. [100 × (initial P – final P)/initial P = dephosphorization rate%]

#### 3.2. XRD Analysis

Figure 3 presents the XRD analysis results. Different LFSs (Figure 3a) have C<sub>2</sub>S, C<sub>3</sub>S, CaO, and MgO as the major phases. These phases were common in the LFS [34,35] and are the reason for the high probability of slag expansion. Slags with the C<sub>2</sub>S phase were classified as potentially hazardous waste. EAFSs (Figure 3b) have C<sub>2</sub>S and FeO as the major phases. In addition, the C<sub>2</sub>S peak has the highest intensity. The modified oxidizing slags after dephosphorization exhibited obvious structural phase transformations, and the major phases were FeO and Ca<sub>2</sub>Al<sub>2</sub>SiO<sub>7</sub> (Figure 3b). The FeO phase is a stable, inert phase [16]. Some studies [25,26] have shown that larnite ( $\beta$  or  $\gamma$ -C<sub>2</sub>S) is the main phase that undergoes hydration during the leaching of slags, which is the primary cause of the release of V and Ba, and is the main factor controlling the properties of the leaching solution. Ca<sub>2</sub>Al<sub>2</sub>SiO<sub>7</sub> is a non-hydraulic phase, while C<sub>2</sub>S is hydrated phase, the former does not expand unlike slag containing C<sub>2</sub>S. Therefore, this method can not only replace part of the lime in dephosphorization but also transform unstable LFSs into stable oxidizing slag. Thus, many of the problems associated with slag recycling are solved.



Figure 3. XRD results of (a) LFS; (b) EAFS and modified oxidizing slags.

#### 3.3. SEM Analysis

The microstructure development in the phosphorus-enriched phase was analyzed by SEM-EDS. The effect of alumina on the dephosphorization process and the change in the  $C_2S$  phase were observed. Figure 4 shows the SEM-BEI image of the oxidizing slags listed in Table 4, during furnace cooling.

In four samples, phase I, i.e., FeO and phase III, i.e.,  $C_2S$  were dispersed in phase II, i.e., the matrix. Wustite (white) was the main FeO or (Mg, Fe)O phase and had a dendritic form. The black striped phase III was dicalcium silicate with some aluminate. In the four samples, phosphorus was only present in phase III (Table 4). As shown in Equation (4), the phosphorus was in the form of a  $Ca_3P_2O_8 \cdot Ca_2SiO_4$  solid solution in the slag. With the increase in the amount of  $Al_2O_3$ ,  $C_2S$  gradually disappeared. The chemical composition of phase III in S1 and S3 showed that the Al content increases to about 2–8%. This indicates that some Al atoms replaced the Si atoms and dissolved into the  $C_2S$  phase to form  $Ca_2$  (Al, Si)O<sub>4</sub>.



(a)

(b)



**Figure 4.** SEM-BEI of modified oxidizing slags after dephosphorization (**a**) S1; (**b**) S2; (**c**) S3; and the control group from a steel plant (**d**) EAFS (Phase I = FeO; Phase II = matrix; Phase III =  $C_2$ S).

Sample	Dhaca	Chemical Composition, at.%								
	Phase	Ca	Si	Al	Fe	Mg	Р	0		
	I-FeO	1.9	0.0	0.6	41.1	6.6	0.00	49.8		
S1	II-matrix	14.8	5.8	14.0	7.1	0.8	0.00	57.4		
	III-C <sub>2</sub> S	25.7	10.4	2.6	1.1	0.3	0.32	59.5		
S2	I-FeO	2.5	0.2	0.9	40.1	7.6	0.00	48.7		
	II-matrix	14.5	5.3	14.5	8.7	1.2	0.00	55.9		
S3	I-FeO	0.9	0.0	0.4	36.7	13.1	0.00	48.9		
	II-matrix	15.1	6.1	13.2	5.8	1.0	0.00	58.9		
	III-C <sub>2</sub> S	28.6	8.2	7.3	1.1	0.4	0.28	54.1		
EAFS	I-FeO	1.1	0.2	0.7	35.8	8.3	0.00	53.9		
	II-matrix	13.3	4.6	14.8	4.5	0.1	0.00	61.9		
	III-C <sub>2</sub> S	33.1	17.5	0.4	1.0	0.1	0.47	47.4		

Table 4. Chemical composition of each phase shown by SEM-EDS.

# 3.4. Image-Pro-Plus Analysis

To understand the effect of  $Al_2O_3$  on the  $C_2S$  phase (phase III in Figure 4), Image-Pro Plus software was used for analysis. Figure 5 shows the images of the  $C_2S$  phase (filled the black striped with red

by the software). As can be seen from the figure, the software can almost identify the  $C_2S$  phase (i.e., the black striped phase III). The red area of EAFS is larger than the red area of S4 (B). Figure 6 shows the effect of Al<sub>2</sub>O<sub>3</sub> on the C<sub>2</sub>S phase. The results show that as the Al<sub>2</sub>O<sub>3</sub> content exceeds 15%, the percentage of the C<sub>2</sub>S phase decreases from an average of 31.4 to 17.1%, and the C<sub>2</sub>S phase exists as a solid solution with 2–8% Al atoms (Table 4). The EAFS and modified oxidizing slag are showing in Figure 7. It was also confirmed from Figure 7 that the major phase of the slag is C<sub>2</sub>Al<sub>2</sub>SiO<sub>7</sub>.



**Figure 5.** C<sub>2</sub>S phase analysis of EAFS and S4 (B).



Figure 6. Effect of Al<sub>2</sub>O<sub>3</sub> content on C<sub>2</sub>S fraction of EAFS and modified oxidizing slag.

It can be concluded that three phase transformations took place successively during the dephosphorization of the molten slag. The complete phase transformation mechanisms of the slag are shown schematically in Figure 8. First, LFS was added to the molten metal. The main crystalline phases of LFS are CaO, MgO,  $C_2S$ , and  $C_3S$ . The slag then produced about 20–40% FeO after the metal oxidation, which changed the phase of the LFS. In addition, the main phase of the slag was either  $C_2S$  or FeO, which is common in the case of EAFS, and  $P_2O_5$  was also present in the  $C_2S$  phase [27]. Finally, as  $Al_2O_3$  started to melt,  $Al_2O_3$  in the slag began to reduce the amount of the  $C_2S$  phase. The final modified oxidizing slag was mainly composed of FeO,  $Ca_2Al_2SiO_7$ , and a small amount of  $C_2S$  or  $Ca_2$  (Al, Si)O<sub>4</sub>.



Figure 7. Samples identified on the CaO–40FeO–SiO<sub>2</sub>–Al<sub>2</sub>O<sub>3</sub> system at 1250 °C.

Al<sub>2</sub>O<sub>3</sub> (wt.%)

15

20

25

10

5



**Figure 8.** Schematic diagram showing the phase transition from LFS to modified oxidizing slag in the dephosphorization process and the crystalline phases of each stage.

#### 3.5. Comparison of Expansion and f-CaO Results

CaO (wt.%)

0

Further study of slag expansion and the f-CaO content are necessary to estimate the stability of the modified oxidizing slag. The slag-volume-expansion tests were performed according to ASTM D4792. According to ASTM D2940, the steel slag aggregates contain easily hydrated components, and the expansion values should not be more than 0.50% within seven days [28]. Therefore, the slag with no more than 0.5% expansion could be used for preparing paving materials.

It is well known that f-CaO can undergo hydration and expansion. As the f-CaO content of the slag increases, the slag volume also increases as a result of expansion. Therefore, the f-CaO content of the slag should be reduced as much as possible to control the volume expansion of the slag. The f-CaO content and volume expansion for various types of LFS are shown in Figure 9a. It shows that a 2.5–3.5% f-CaO content results in an expansion that varies greatly from 1% to 5%. This result also verifies the instability of LFS. Figure 9b shows the f-CaO and volume expansion of the modified oxidizing slag and EAFS. The detailed data is presented in Table 5. In this study, the expansion of the oxidizing slag was less than 0.5%. Furthermore, for unmodified EAFS, the f-CaO content is as high as 1.4%. However, the f-CaO content of the modified oxidizing slag is only 0.13–0.41%. The results show that as the CaO content in the supplement increases, the f-CaO content tends to increase. This means that the addition of LF and Al<sub>2</sub>O<sub>3</sub> can reduce the concentration of f-CaO in CaO.

Thus, the experimental results showed that the LFS with more than 2.5% f-CaO content could be transformed into oxidizing slag with 0.41% f-CaO content by modification at 1520–1600 °C. Although

the volume expansions of modified oxidizing slag and EAFS are significantly different, the values (0.037% and 0.17%, respectively) are lower than 0.5%, as required by the ASTM D2940 standards. Therefore, the modified oxidizing slag can be used for preparing paving materials.



**Figure 9.** The content of f-CaO and volume expansion for various types of slag: (**a**) LFS; (**b**) modified oxidizing slag and EAFS.

Sample	S1A	S2A	S3A	S4A	S5A	S4B	S5B	S6B	S-C	EAF1	EAF2
f-CaO (%) Expansion (%)	0.31 0.027	0.31 NA <sup>1</sup>	0.26 NA <sup>1</sup>	0.41 0.037	0.37 NA <sup>1</sup>	0.18 0.023	0.13 0.029	0.21 NA <sup>1</sup>	0.7 0.11	1.2 0.17	1.4 0.15
$^{1}$ NA = Not Analyzed.											

Table 5. The results of f-CaO and volume expansion for oxidizing slag.

## 4. Conclusions

In this study, surplus CaO in LFS was used as a substitute for the lime material required in dephosphorization. Through the addition of Al<sub>2</sub>O<sub>3</sub>, the LFS was transformed into oxidizing slag with lower f-CaO. The major findings are summarized as follows:

- (1) The dephosphorization rate of different LFSs using supplement A (LF/CaO = 1/1, Al<sub>2</sub>O<sub>3</sub> content = 15–25%) was more than 45% between 1520 °C and 1600 °C. The phosphorus content of steel is less than 0.03% to meet the set standards of general engineering steel.
- (2) XRD results showed that different LFSs had C<sub>2</sub>S, C<sub>3</sub>S, CaO, and MgO as the major phases. The characteristics of LFS were altered after high-temperature slag modification, and the primary crystalline phases were FeO and gehlenite (Ca<sub>2</sub>Al<sub>2</sub>SiO<sub>7</sub>).
- (3) SEM analysis confirmed that phosphorus was concentrated in the  $C_2S$  phase during dephosphorization. As the Al<sub>2</sub>O<sub>3</sub> content exceeds 15%, about 2–8% of Al atoms replaced Si atoms, and the C<sub>2</sub>S phase fraction decreased from 31.4% to 17.1%.
- (4) The f-CaO content of the modified oxidizing slag was less than 0.41% (while those of LFS and EAFS were 0.9–3.4% and 1.2–1.4%, respectively). The modified oxidizing slag showed almost no expansion and conformed to the ASTM D2940 standards.

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## References

- 1. Setien, J.; Hernandez, D.; Gonzalez, J.J. Characterization of ladle furnace basic slag for use as a construction material. *Constr. Build. Mater.* **2009**, *23*, 1788–1794. [CrossRef]
- 2. Durinck, D.; Arnout, S.; Mertens, G.; Boydens, E.; Jones, P.T.; Elsen, J.; Blanpain, B.; Wollants, P. Borate distribution in stabilized stainless-steel slag. *J. Am. Ceram. Soc.* **2008**, *91*, 548–554. [CrossRef]
- 3. Shi, C.J. Characteristics and cementitious properties of ladle slag fines from steel production. *Cem. Concr. Res.* **2002**, *32*, 459–462. [CrossRef]
- 4. Shi, C.J.; Qian, J.S. High performance cementing materials from industrial slags—A review. *Resour. Conserv. Recycl.* **2000**, *29*, 195–207. [CrossRef]
- 5. Lee, H.-S.; Lim, H.-S.; Ismail, M.A. Quantitative evaluation of free cao in electric furnace slag using the ethylene glycol method. *Constr. Build. Mater.* **2017**, *131*, 676–681. [CrossRef]
- 6. Loncnar, M.; van der Sloot, H.A.; Mladenovic, A.; Zupancic, M.; Kobal, L.; Bukovec, P. Study of the leaching behaviour of ladle slags by means of leaching tests combined with geochemical modelling and mineralogical investigations. *J. Hazard. Mater.* **2016**, *317*, 147–157. [CrossRef]
- Bocci, E. Use of ladle furnace slag as filler in hot asphalt mixtures. *Constr. Build. Mater.* 2018, 161, 156–164. [CrossRef]
- 8. Worldsteel. Steel Statistical Yearbook. Available online: https://www.worldsteel.org/steel-by-topic/statistics/ steel-statistical-yearbook.html (accessed on 27 March 2020).
- 9. Serjun, V.Z.; Mirtic, B.; Mladenovic, A. Evaluation of ladle slag as a potential material for building and civil engineering. *Mater. Tehnol.* **2013**, *47*, 543–550.
- 10. Branca, T.A.; Colla, V.; Valentini, R. A way to reduce environmental impact of ladle furnace slag. *Ironmak. Steelmak.* **2009**, *36*, 597–602. [CrossRef]
- Okoye, P.U.; Abdullah, A.Z.; Hameed, B.H. Stabilized ladle furnace steel slag for glycerol carbonate synthesis via glycerol transesterification reaction with dimethyl carbonate. *Energy Conv. Manag.* 2017, 133, 477–485. [CrossRef]
- 12. Gu, X.; Yu, B.; Dong, Q.; Deng, Y. Application of secondary steel slag in subgrade: Performance evaluation and enhancement. *J. Clean. Prod.* **2018**, *181*, 102–108. [CrossRef]
- 13. Papayianni, I.; Anastasiou, E. Effect of granulometry on cementitious properties of ladle furnace slag. *Cem. Concr. Compos.* **2012**, *34*, 400–407. [CrossRef]
- 14. Guzzon, M.; Mapelli, C.; Sahajwalla, V.; Saha-Chaudhury, N.; Memoli, F.; Pustorino, M. The behaviour of the secondary metallurgy slag into the eaf. How to create a good foamy slag with the appropriate basicity using a mix of lime and recycled ladle slag as eaf slag former. In Proceedings of the 38th Seminário de Aciaria, Belo Horizonte, Brazil, 14 November 2019.
- 15. Li, J.X.; Yu, Q.J.; Wei, J.X.; Zhang, T.S. Structural characteristics and hydration kinetics of modified steel slag. *Cem. Concr. Res.* **2011**, *41*, 324–329. [CrossRef]
- 16. Wang, Q.A.; Yan, P.Y.; Feng, J.W. A discussion on improving hydration activity of steel slag by altering its mineral compositions. *J. Hazard. Mater.* **2011**, *186*, 1070–1075. [CrossRef] [PubMed]
- 17. Wang, Q.; Wang, D.Q.; Zhuang, S.Y. The soundness of steel slag with different free cao and mgo contents. *Constr. Build. Mater.* **2017**, *151*, 138–146. [CrossRef]
- Rashad, A.M. A synopsis manual about recycling steel slag as a cementitious material. *J. Mater. Res. Technol.* 2019, *8*, 4940–4955. [CrossRef]
- 19. Guzzon, M.; Mapelli, C.; Memoli, F.; Marcozzi, M. Recycling of ladle slag in the eaf: Improvement of the foaming behaviour and decrease of the environmental impact. *Rev. de Métall.* **2007**, *104*, 171–178. [CrossRef]
- 20. Varanasi, S.S.; More, V.M.R.; Rao, M.B.V.; Alli, S.R.; Tangudu, A.K.; Santanu, D. Recycling ladle furnace slag as flux in steelmaking: A review. *J. Sustain. Metall.* **2019**, *5*, 449–462. [CrossRef]
- 21. Skaf, M.; Manso, J.M.; Aragón, Á.; Fuente-Alonso, J.A.; Ortega-López, V. Eaf slag in asphalt mixes: A brief review of its possible re-use. *Resour. Conserv. Recycl.* **2017**, *120*, 176–185. [CrossRef]

- 22. Yildirim, I.Z.; Prezzi, M. Experimental evaluation of eaf ladle steel slag as a geo-fill material: Mineralogical, physical & mechanical properties. *Constr. Build. Mater.* **2017**, *154*, 23–33. [CrossRef]
- 23. Brand, A.S.; Roesler, J.R. Steel furnace slag aggregate expansion and hardened concrete properties. *Cem. Concr. Compos.* **2015**, *60*, 1–9. [CrossRef]
- 24. González-Ortega, M.A.; Cavalaro, S.H.P.; de Rodríguez Sensale, G.; Aguado, A. Durability of concrete with electric arc furnace slag aggregate. *Constr. Build. Mater.* **2019**, *217*, 543–556. [CrossRef]
- 25. Mombelli, D.; Mapelli, C.; Barella, S.; Gruttadauria, A.; Le Saout, G.; Garcia-Diaz, E. The efficiency of quartz addition on electric arc furnace (eaf) carbon steel slag stability. *J. Hazard. Mater.* **2014**, 279, 586–596. [CrossRef] [PubMed]
- 26. Mombelli, D.; Mapelli, C.; Barella, S.; Di Cecca, C.; Le Saout, G.; Garcia-Diaz, E. The effect of microstructure on the leaching behaviour of electric arc furnace (eaf) carbon steel slag. *Proc. Saf. Environ. Protect.* **2016**, *102*, 810–821. [CrossRef]
- Suito, H.; Inoue, R. Behavior of phosphorous transfer from cao-feto-p2o5(-sio2) slag to cao particles. *ISIJ Int.* 2006, 46, 180–187. [CrossRef]
- 28. Deniz, D.; Tutumluer, E.; Popovics, J.S. Evaluation of expansive characteristics of reclaimed asphalt pavement and virgin aggregate used as base materials. *Transp. Res. Rec.* **2010**, 10–17. [CrossRef]
- 29. Li, C.C.; Lin, C.M.; Hung, C.Y.; Chang, K.L.; Wu, W.T. Effect of al2o3/sio2 ratio on viscosity and structure of cao-al2o3-sio2-caf2mgo slag. *Int. J. Mater. Res.* **2019**, *110*, 247–252. [CrossRef]
- 30. Diao, J.; Xie, B.; Wang, Y.; Guo, X. Recovery of phosphorus from dephosphorization slag produced by duplex high phosphorus hot metal refining. *ISIJ Int.* **2012**, *52*, 955–959. [CrossRef]
- 31. Kondratiev, A.; Jak, E. Predicting coal ash slag flow characteristics (viscosity model for the al2o3-cao-'feo'-sio2 system). *Fuel* **2001**, *80*, 1989–2000. [CrossRef]
- Wu, W.; Lin, C.M.; Chen, J.H.; Li, C.C.; Lin, K.H. Detection of Calcium in the Active Oxide. I600903; 1 October 2017. Available online: https://twpat1.tipo.gov.tw/tipotwoc/tipotwkm?!!FR\_I600903 (accessed on 11 April 2020).
- 33. Wang, G.; Wang, Y.H.; Gao, Z.L. Use of steel slag as a granular material: Volume expansion prediction and usability criteria. *J. Hazard. Mater.* **2010**, *184*, 555–560. [CrossRef]
- Waligora, J.; Bulteel, D.; Degrugilliers, P.; Damidot, D.; Potdevin, J.L.; Measson, M. Chemical and mineralogical characterizations of ld converter steel slags: A multi-analytical techniques approach. *Mater. Charact.* 2010, 61, 39–48. [CrossRef]
- 35. Ortega-Lopez, V.; Manso, J.M.; Cuesta, I.I.; Gonzalez, J.J. The long-term accelerated expansion of various ladle-furnace basic slags and their soil-stabilization applications. *Constr. Build. Mater.* **2014**, *68*, 455–464. [CrossRef]



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