

## Article

# Stripping of Cu Ion from Aquatic Media by Means of $\text{MgY}_2\text{O}_4\text{@g-C}_3\text{N}_4$ Nanomaterials

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**Abstract:** In this study, quaternary  $\text{MgY}_2\text{O}_5\text{@g-C}_3\text{N}_4$  nanomaterials were produced using a simplistic ultrasonic power technique in the presence of an organic solvent, and their capability to abolish Cu (II) from an aqueous solution was evaluated. As validated by powder X-ray diffraction, the synthesized nanomaterials possessed excellent crystallinity, purity, and tiny crystalline size. According to BET and TEM, the nanomaterials with high porosity nanosheets and perfect active sites made Cu (II) removal from water treatment feasible. At a pH of 3.0, the  $\text{MgY}_2\text{O}_5\text{@g-C}_3\text{N}_4$  displayed good Cu (II) adsorption capability. The Cu (II) adsorption adhered to the Langmuir adsorption model, with an estimated theoretical maximum adsorption aptitude of 290 mg/g. According to the kinetics investigation, the adsorption pattern best fitted the pseudo-second-order kinetics model. Depending on the FTIR results of the nanocomposite prior to and after Cu (II) uptake, surface complexation and ion exchange of Cu (II) ions with surface hydroxyl groups dominated the adsorption of Cu (II). The  $\text{MgY}_2\text{O}_5\text{@g-C}_3\text{N}_4$  nanomaterials have great potential as adsorbents for Cu (II) removal due to their easy manufacturing process and high adsorption capacity. Additionally, the reuse of  $\text{MgY}_2\text{O}_4\text{@g-C}_3\text{N}_4$  nanomaterials was tested through the succession of four adsorption cycles using  $\text{HNO}_3$ . The result showed the good stability of this material for mineral pollution removal.

**Keywords:**  $\text{MgY}_2\text{O}_4\text{@g-C}_3\text{N}_4$  nanomaterials; Cu (II) ions adsorption; pH impact; sorption kinetics modeling



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## 1. Introduction

Heavy metals are found everywhere in the natural world, and as human evolution has progressed; the possibility of being poisoned by metallic substances has increased [1]. This is because the body cannot process the remaining heavy metals, which are poisonous [2]. Industrial effluent contains several toxic metals, such as lead, chromium, copper, etc. Copper is a highly desirable metal that is widely used in several industrial applications including metal polishing, electricity, and metrological uses [3,4]. In recent decades, environmental knowledge of the problems presented by the release of copper-containing wastewater has developed in tandem with the quantity of copper-containing effluent from the electronics sector [5]. Furthermore, copper is a highly hazardous metal, even in small quantities. As per the U.S. Environmental Protection Act (USEPA), the highest permissible copper ions for industrial effluents are 1.3 mg/L whereas the World Health Organization recommends a concentration of no more than 2 mg/L for drinking water [6]. Thus, copper-contaminated

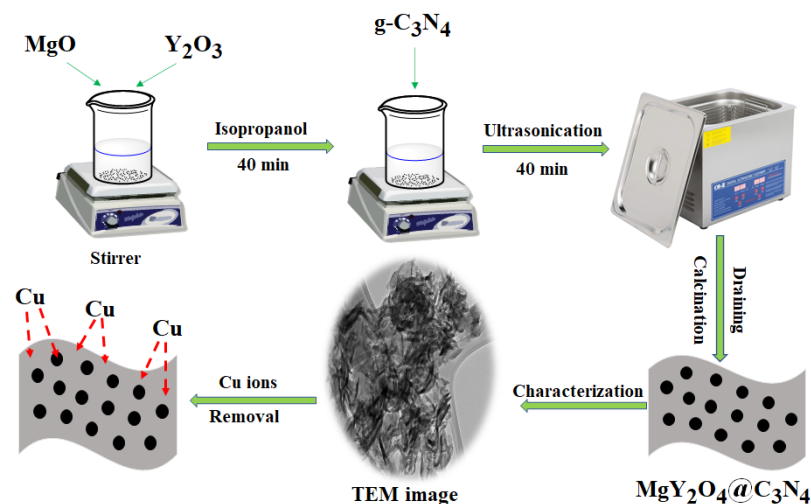
effluent should be cleaned prior to being released into the environment because of its toxic effects [3]. In recent years, various innovative strategies for removing copper ions from industrial effluents have been introduced, including adsorption, complexation, membrane filtering and electrocoagulation [7–9]. The adsorption of pollutants on the surfaces of adsorptive materials is an efficient technique for cleaning heavy metals [10,11]. Numerous materials, such as activated carbon, bentonite, and zeolite, are effective and competitive substances for use in heavy metal elimination from the aquatic environment [12–14].

Investigators have dedicated time and energy to invent suitable adsorption materials for removing heavy metals from wastewater [15]. Although these substances are economically affordable, we should develop methods to overcome their limitations, which are represented by their inefficiency and generation of secondary waste [16]. Recently, nanomaterials have drawn great interest for their exceptional ability to eradicate pollutants from the water system [17,18]. Enormous attempts have been made to manufacture nanocomposites with different properties by hybridizing and modification [19,20]. Different nanostructured materials exhibit several intriguing features, including particle size, mesoporosity, and large surface area [21,22]. Graphitic carbon nitride ( $g\text{-C}_3\text{N}_4$ ) has emerged as an enticing research area, attracting wide multidisciplinary interest as a photocatalyst and environmental remediation material [23,24]. A  $g\text{-C}_3\text{N}_4$  is a polymer composed of carbon and nitrogen atoms; it can be altered to change its surface properties without changing its composition and structure [25]. Because of the polymer characteristics of  $g\text{-C}_3\text{N}_4$ , its surface properties could be efficiently modified at the molecular scale through nanostructured materials [26]. In this work, for the first time to the best of our knowledge, we reported the synthesis of a  $\text{MgY}_2\text{O}_4@g\text{-C}_3\text{N}_4$  composite by considering the synergistic advantage of the nontoxic  $\text{MgO}$ ,  $\text{Y}_2\text{O}_3$  oxide decoration on a  $g\text{-C}_3\text{N}_4$  platform. Then, we demonstrated its application for the successful abolishing of  $\text{Cu(II)}$  ions from aqueous solutions, where we inspected the influence of different experimental conditions on  $\text{Cu(II)}$  ions removal, and conferred the plausible mechanism for the  $\text{Cu(II)}$  ions' interaction with the  $\text{MgY}_2\text{O}_4@g\text{-C}_3\text{N}_4$ .

## 2. Experimental Procedures

### 2.1. Preparation of $\text{MgY}_2\text{O}_4@g\text{-C}_3\text{N}_4$ Nanostructures

For  $\text{MgY}_2\text{O}_4@g\text{-C}_3\text{N}_4$  nanosorbent, 0.011 moles of  $\text{MgO}$  and 0.002 moles of  $\text{Y}_2\text{O}_3$  nanoparticles (Sigma Aldrich) were disseminated in 0.110 L of isopropanol for 0.40 h utilizing an ultrasonic bath. After adding 0.89 g of  $g\text{-C}_3\text{N}_4$  nanosheet to the alcoholic solution, the mixture was sonicated for an additional 0.40 h at 500 rpm. The mixtures were then heated for 24 h at  $75^\circ\text{C}$  in an electric drying oven, and the obtained nano-sorbent was ground prior to calcination. The resulting materials were then subjected to an annealing process lasting for 1.5 h at  $145^\circ\text{C}$  as demonstrated in Scheme 1.



**Scheme 1.** Scheme of constructed of the  $\text{MgY}_2\text{O}_4@g\text{-C}_3\text{N}_4$  nanocomposites.

## 2.2. Characterizations of MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> Nanostructures

The crystallinity and structural features of MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> nanocomposites were examined using an XRD system equipped with a Cu-K radiation source ( $\lambda = 1.5418 \text{ \AA}$ ). The surface area of the nanocomposite was estimated by N<sub>2</sub> adsorption/desorption at 196 °C using a Micro-metrics ASAP 2020 analyzer (Norcross, Georgia, USA). A transmission electron microscope (TEM) combined with electron dispersive X-ray (EDX) spectrometry was utilized for morphology and elemental composition identification. X-ray photoelectron spectroscopy (XPS) was used to probe the synthesized nanomaterials surface chemistry. FTIR was employed to study the variations of MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> nanomaterials functional groups before and after Cu (II) elimination.

## 2.3. Cu (II) Adsorption Test

The isotherms for Cu (II) adsorption on MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> nanohybrid were examined in batch experiments. In 0.025 L glass vials, 10 mg MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> was added to Cu (II) at various concentrations from 5 to 200 ppm. The solution was stirred continuously for 24 h. After equilibrium was attained, the nanocomposite was filtered, and atomic absorption spectroscopy was used to quantify Cu (II) concentrations. The quantity of Cu (II) ions adsorbed at any given time and consequent equilibrium magnitudes  $q_t$  and  $q_e$  were computed utilizing Formulas (1) and (2).

$$q_t = \frac{1}{m} (C_0 - C_t)V \quad (1)$$

$$q_e = \frac{1}{m} (C_0 - C_e)V \quad (2)$$

where the terms  $V$ ,  $C_0$ ,  $C_e$  and  $C_t$  stand the solution volume (L), initial concentration, equilibrium concentration, and concentration at time  $t$  of Cu (II) metal ions (mg/L) in solution, and  $m$  the adsorbent's mass (g). The average of triplicate measurements was taken. The regeneration experiment was conducted according to [9] where the solution after Cu (II) ions adsorption adsorbent was filtered to separate the adsorbent, washed three times with de-ionized water, soaked in diluted HNO<sub>3</sub> and finally filtered after shaking at 300 rpm for 60 min. Then, the adsorbent was washed with deionized water and left to dry at 80 °C for 15 h before performing the next adsorption cycle.

The Freundlich [27], Langmuir [28], Dubinin–Radushkevich [29], and Temkin [30] numerical methods were applied to the experimental analysis to determine the adsorption equilibrium mechanism of the adsorbent.

$$q_e = K_F C_e^{1/n} \quad (3)$$

$$q_e = \frac{Q_{max} K_L C_e}{1 + K_L C_e} \quad (4)$$

$$q_e = q_m e^{-K\epsilon^2} \quad (5)$$

$$q_e = q_m \exp(-\beta\epsilon^2) \quad (6)$$

The isotherm of Cu (II) adsorption on MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> nanomaterials was examined via adding a specified quantity of adsorbent (10 mg) to a Cu (II) solution (5 to 300 mg/L) at room temperature for 1440 min.

Identifying the adsorption kinetics characteristics of the sorbent is essential in the environmental remediation of heavy metals [31]. Thus, Pseudo-first order (PFO), pseudo-second order (PSO), and intra-particle diffusion models (IPD) were used to analyze the adsorption of Cu (II) ions on MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> nanomaterials. The three nonlinear mathematical models used in this study are given in equations below.

Kinetics Model	Equation		Plots	Ref.
Pseudo-first-order	$q_t = (q_e - e^{-k_1 t})$	(7)	$q_t$ vs $t$	[1]
Pseudo-second-order	$q_t = \frac{q_e^2 k_2 t}{1 + q_e k_2 t}$	(8)	$q_t$ vs $t$	[2,3]
Elovich	$q_t = \frac{1}{\beta} \ln(1 + \alpha \beta t)$	(9)	$q_t$ vs $t$	[4]
Intra-particle Diffusion	$q_t = k_{diff} t^{1/2} + C$	(10)	$q_t$ vs $t^{1/2}$	[5,6]
Mass Transfer	$\ln(C_0 - C_t) = \ln(D) - k_0 \cdot t$	(11)	$\ln(C_0 - C_t)$ vs $t$	[5,6]

### 3. Results and Discussions

#### 3.1. MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> Nanomaterial Structural Analysis

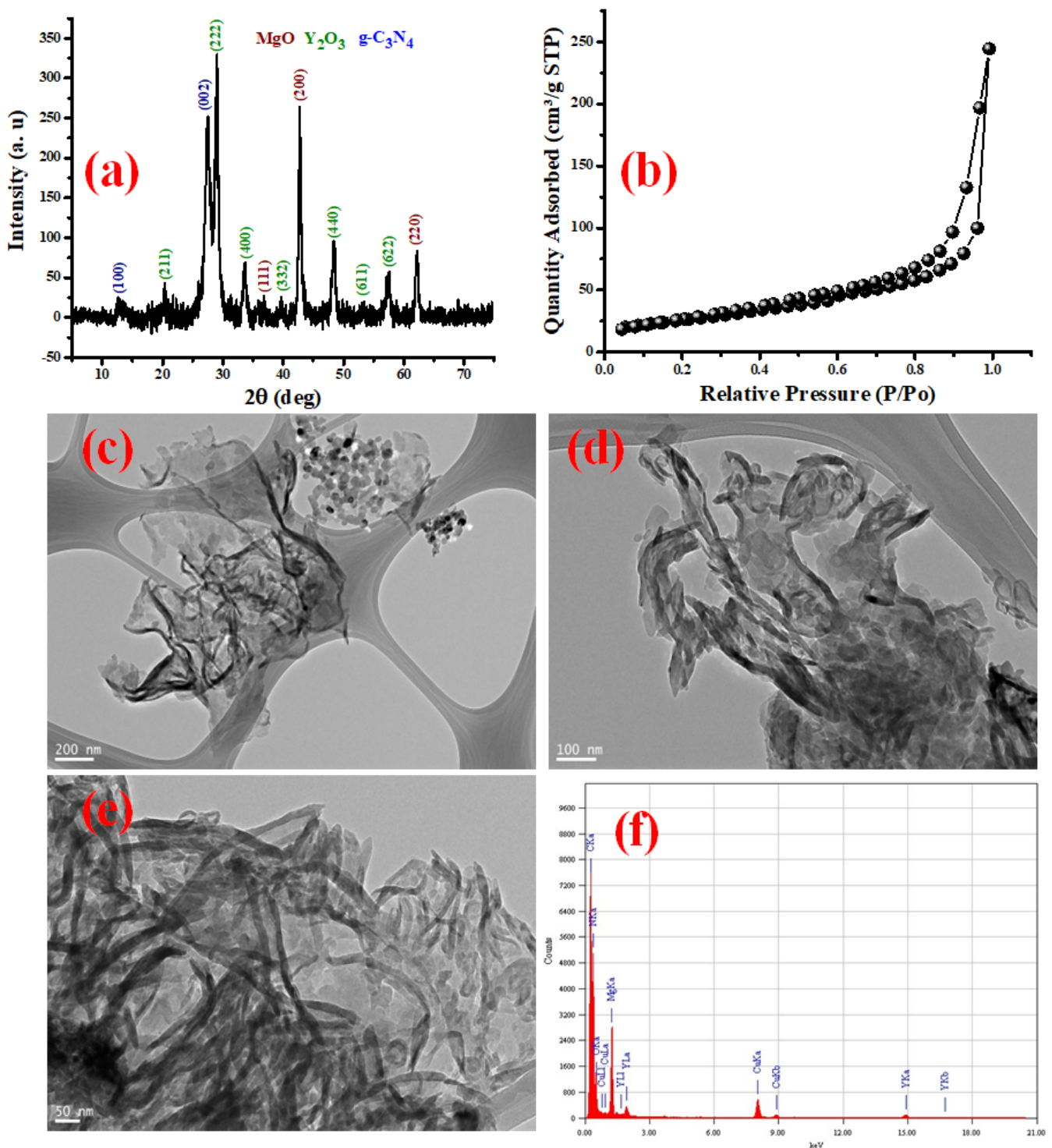
As illustrated in Figure 1a, the XRD pattern of MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> nanomaterials indicates sharp diffraction peaks with comparative widening and intensities, indicating the production of a well-nano-crystallized phase. Employing the High Score instrument to identify peaks demonstrates the existence of MgO, Y<sub>2</sub>O<sub>3</sub>, and g-C<sub>3</sub>N<sub>4</sub> phases. The g-C<sub>3</sub>N<sub>4</sub> nanosheet diffraction peaks at  $2\theta = 12.84^\circ$  and  $27.36^\circ$  match with the in-plane structural contents pattern (100) and interlayer stacking plane (002) of the hexagonal structure (JCPDS card No. 87-1526) [32]. The different peaks observed at  $2\theta$  of  $36.72^\circ$ ,  $42.84^\circ$ , and  $61.84^\circ$  are assigned to the (111), (200), and (220) planes of the MgO cubic symmetry [33]. Besides the peaks 20.30, 29.31, 33.74, 39.72, 48.41, 53.02, and  $57.51^\circ$  correspond to the (211), (222), (400), (332), (440), (611) and (622) Miller indices of pure body-centered cubic Y<sub>2</sub>O<sub>3</sub>, respectively (JCPDS No. 41-1105) [34].

A suitable adsorbent, such as MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> nanoparticles, must have a substantial number of adsorption sites. In other words, the material's surface area, pore-volume, and size should be sufficient. The nitrogen adsorption-desorption investigation (Figure 1b) demonstrates that MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> nanoparticles are a mesoporous material with an IUPAC type IV adsorption isotherm. The isotherm is associated with a type H1 hysteresis, suggesting a confined distribution of homogeneous mesoporous and inflexible networking impacts [35,36]. MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> nanomaterials have a surface area, total porous volume, and average pore size of 90.51 m<sup>2</sup>/g, 0.356 cc/g, and 2.53 nm, respectively. It is anticipated that the adsorbent's huge surface area and porosity will expose a significant number of adsorption sites, leading to high adsorption efficiency.

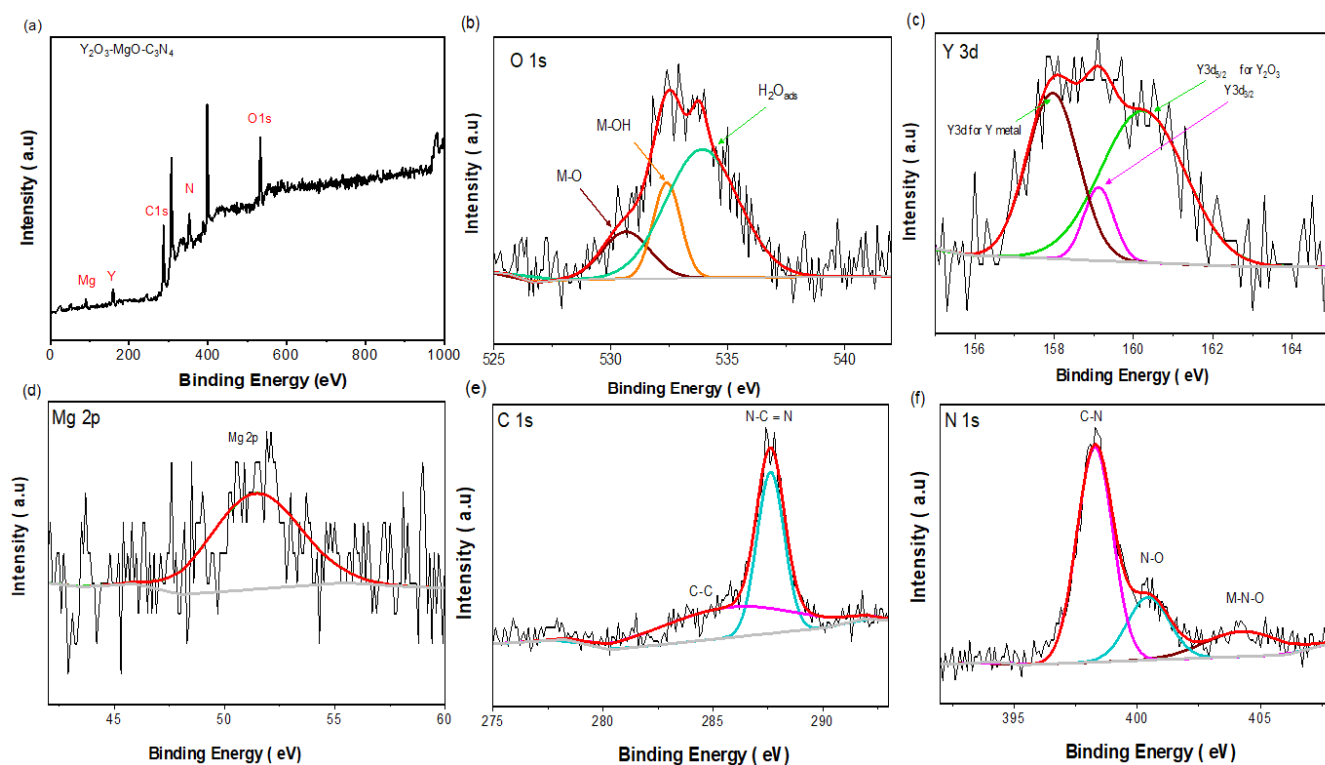
TEM images of the produced MgY<sub>2</sub>O<sub>5</sub>@g-C<sub>3</sub>N<sub>4</sub> nanomaterials revealed two-dimensional nanosheet-like nanoparticles, as publicized in Figure 1c–e. The combined MgO and Y<sub>2</sub>O<sub>3</sub> nanoparticles in the MgY<sub>2</sub>O<sub>5</sub>@g-C<sub>3</sub>N<sub>4</sub> nanomaterials exposed a particle with an average size between 20 and 50 nm, as observed. The EDX spectrum (Figure 1e) reveals recognizable Y, Mg, N, O, and C peaks, thus verifying the purity of the produced composite. In addition, the composition of C, N, O, Mg, and Y, as depicted in Figure 1f, clearly demonstrated the homogenous distribution of the elements across the examined particles.

XPS was employed to examine the surface chemical composition of MgY<sub>2</sub>O<sub>5</sub>@g-C<sub>3</sub>N<sub>4</sub> nanomaterials, as well as the interaction between g-C<sub>3</sub>N<sub>4</sub> and Y<sub>2</sub>O<sub>3</sub> and MgO. The XPS survey spectra and high resolution XPS spectra of the O 1s, Y 3d, Mg 2p, C 1s and N 1s areas are shown in Figure 2. The survey spectra (Figure 2a) revealed the presence of C, N, O, Y, and Mg on the surface of MgY<sub>2</sub>O<sub>5</sub>@g-C<sub>3</sub>N<sub>4</sub> nanomaterials. The narrow O 1s peaks in Figure 2b may be deconvoluted to three peaks with binding energies of 530.64, 532.36, and 533.90 eV, which correspond to the lattice oxygen of the layer-structured Y<sub>2</sub>O<sub>3</sub>, and/or MgO and adsorbed H<sub>2</sub>O or surface hydroxyl oxygen, respectively [37]. The three primary peaks in Figure 2b, at 157.96 eV, 159.11 eV, and 160.25 eV, respectively, reflected the Y3d for Y metal and (3d5/2 and 3d3/2) of stoichiometric Y<sub>2</sub>O<sub>3</sub> oxide [38,39]. The signal at 51.45 eV in the Mg XPS spectrum (Figure 2c) might be attributed to the distinctive Mg 2p peak for MgO [23]. Figure 2e shows the high-resolution C 1s spectrum, which features two distinct contributions at 284.97 and 287.60 eV, which are attributed to carbon in the C-C and C=N/C=O states, respectively [40,41]. Figure 2f shows a high-resolution N 1s spectra with three distinct peaks centered at 398.27, 400.41, and 404.17 eV, which were attributed to the

pyridine N, pyrrolic N, and graphitic N, respectively [42], indicating that the  $\text{MgY}_2\text{O}_5@\text{g-C}_3\text{N}_4$  nanomaterials surface was rich in nitrogen-containing functional groups.



**Figure 1.** (a) XRD pattern; (b) BET surface area graph; (c–e) TEM images with different magnifications; and (f) EDX of  $\text{MgY}_2\text{O}_5@\text{g-C}_3\text{N}_4$  nanomaterials.

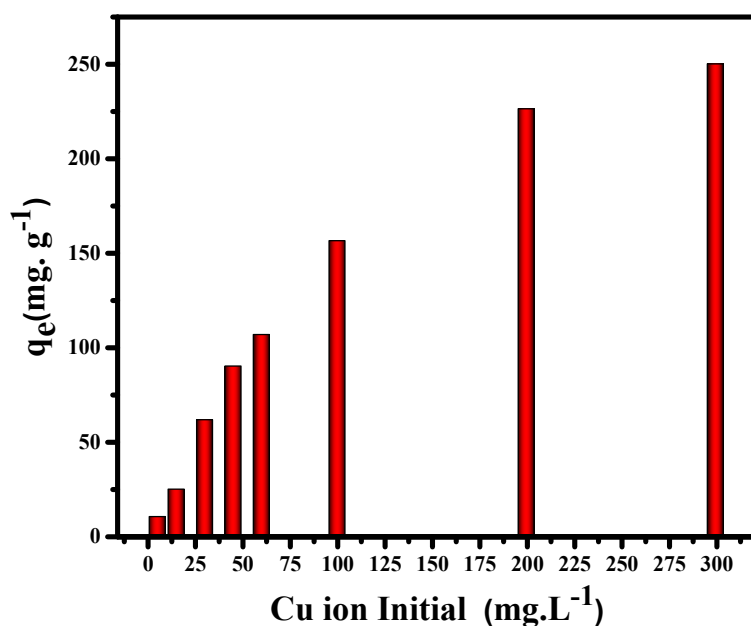


**Figure 2.** XPS spectra of (a) survey; (b) O 1s; (c) Y 3d; (d) Mg 2p; (e) C 1s; and (f) N 1s for  $\text{Y}_2\text{O}_3$ - $\text{MgO@g-C}_3\text{N}_4$  nanocomposite.

### 3.2. Cu (II) Removal onto $\text{MgY}_2\text{O}_4@g\text{-C}_3\text{N}_4$ Nanomaterial

#### 3.2.1. Effect of Cu (II) Initial Concentration

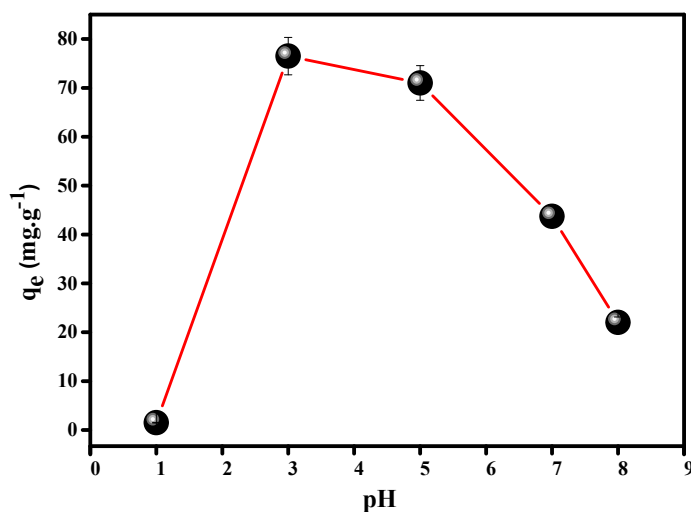
The impact of Cu (II) concentration was evaluated over a wide concentrations range (5 to 300 mg/L) within ideal operating conditions. These conditions comprised 10 mg of  $\text{MgY}_2\text{O}_4@g\text{-C}_3\text{N}_4$ , with a constant volume of Cu (II) (25 mL), room temperature, and a 24-h contact duration. The Figure 2 shows the variation of adsorption capacity as function of Cu (II) initial concentration by  $\text{MgY}_2\text{O}_4@g\text{-C}_3\text{N}_4$  nanomaterials. Figure 3 depicts the percentages and optimal adsorption capacity of Cu (II) on  $\text{MgY}_2\text{O}_4@g\text{-C}_3\text{N}_4$  sorbent. It can be observed that when the concentration of Cu (II) rises, the adsorbed amount also rises steadily from 9.85 to 250 mg/g. In this particular scenario, the primary driving force that rise in the initial Cu (II) concentration surmounted any impediment to Cu (II) movement from the solution [26]. Because of this, the fractional adsorption produced is directly proportional to the concentration. This behavior is similar to that obtained with Tran and his coworkers in the case of the removal of Pb (II) from aqueous media by a new design of Cu–Mg binary ferrite [36].



**Figure 3.** Variation of adsorption capacity of Cu (II) with the initial concentration (conditions: 25 °C; adsorbent dosage: 10 mg; stirring speed: 400 rpm; contact time: 24 h; initial Cu (II) concentration: 5–300 mg/L, pH = 7).

### 3.2.2. Cu (II) Removal and pH

The pH level is critical for realizing the rate of surface reactions between adsorbate (Cu (II)) and MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> sorbent. An investigation of the impact of pH on Cu<sup>2+</sup> adsorption has been conducted from pH 1.0 to 8.0. Figure 4 highlights the influence of pH on adsorption capacity (mg.g<sup>-1</sup>) of Cu ions where a maximum value was measured at pH 3. Adsorbate-adsorbent interactions decrease below pH = 3 because protonation takes place on the sorbent surface. A competition between H<sup>+</sup> and the positively copper ions for the available active sites at the adsorbent's surface rationalizes the reduced Cu ion adsorption at low pH values. These findings are in agreement with those reported in other studies [43]. Cu (II) has a pH dependence on its solubility as it exists as soluble free ions and Cu (OH)<sup>+</sup> at lower pH levels. Moreover, Cu (II) ions tend to precipitate as copper hydroxides (Cu(OH)<sub>2</sub>, Cu(OH)<sub>3</sub><sup>-</sup>, and Cu(OH)<sub>4</sub><sup>2-</sup>) above pH 7 [8]. Based on these findings, the quantitative Cu (II) ions elimination ability decline with the pH increase until it reaches a minimum value at pH = 8.

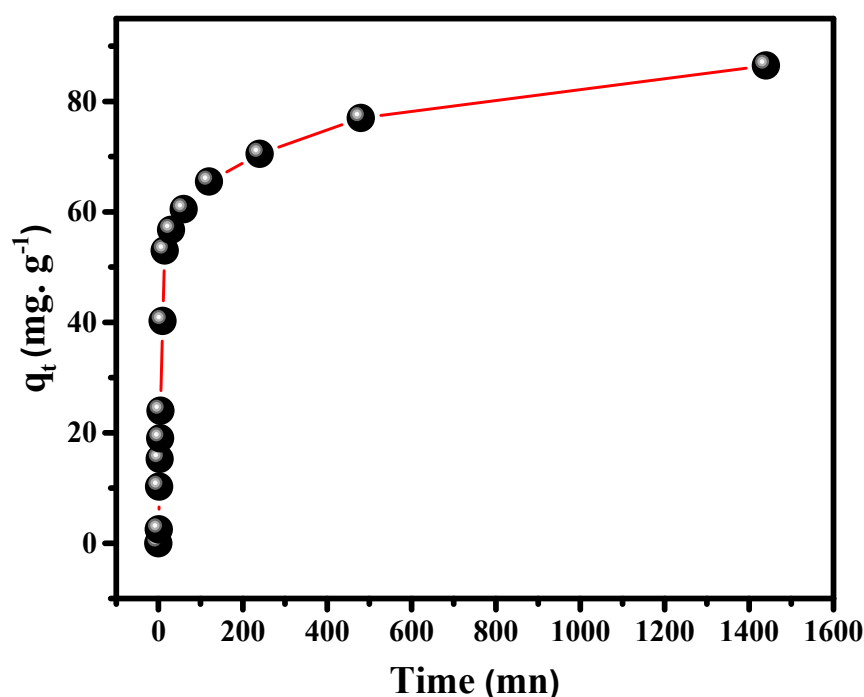


**Figure 4.** pH dependence of the adsorption capacity (mg.g<sup>-1</sup>) of Cu ions.

This behavior is similar to that obtained by Tran and his coworkers in the case of the removal of Pb (II) from aqueous media by a new design of Cu–Mg binary ferrite [36].

### 3.2.3. Cu (II) Elimination and Equilibrium Contact Time

The adsorption of 45 mg/L Cu (II) ions initial concentration on  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  nanosorbent was examined for periods of 0 to 1440 min as illustrates in Figure 5. In less than 40 min, the elimination of Cu (II) against the contact time reaches equilibrium. According to several active sites on the  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  surface, the Cu (II) sorbed quantity achieves around 86.65 mg/g. At equilibrium, the quantity of the active site normally declines, and the exclusion percentage stabilizes to a steady level. It is anticipated that the adsorbent's vast surface area and porosity will avail a huge sum of adsorption sites, leading to enhanced adsorption efficiency [44].



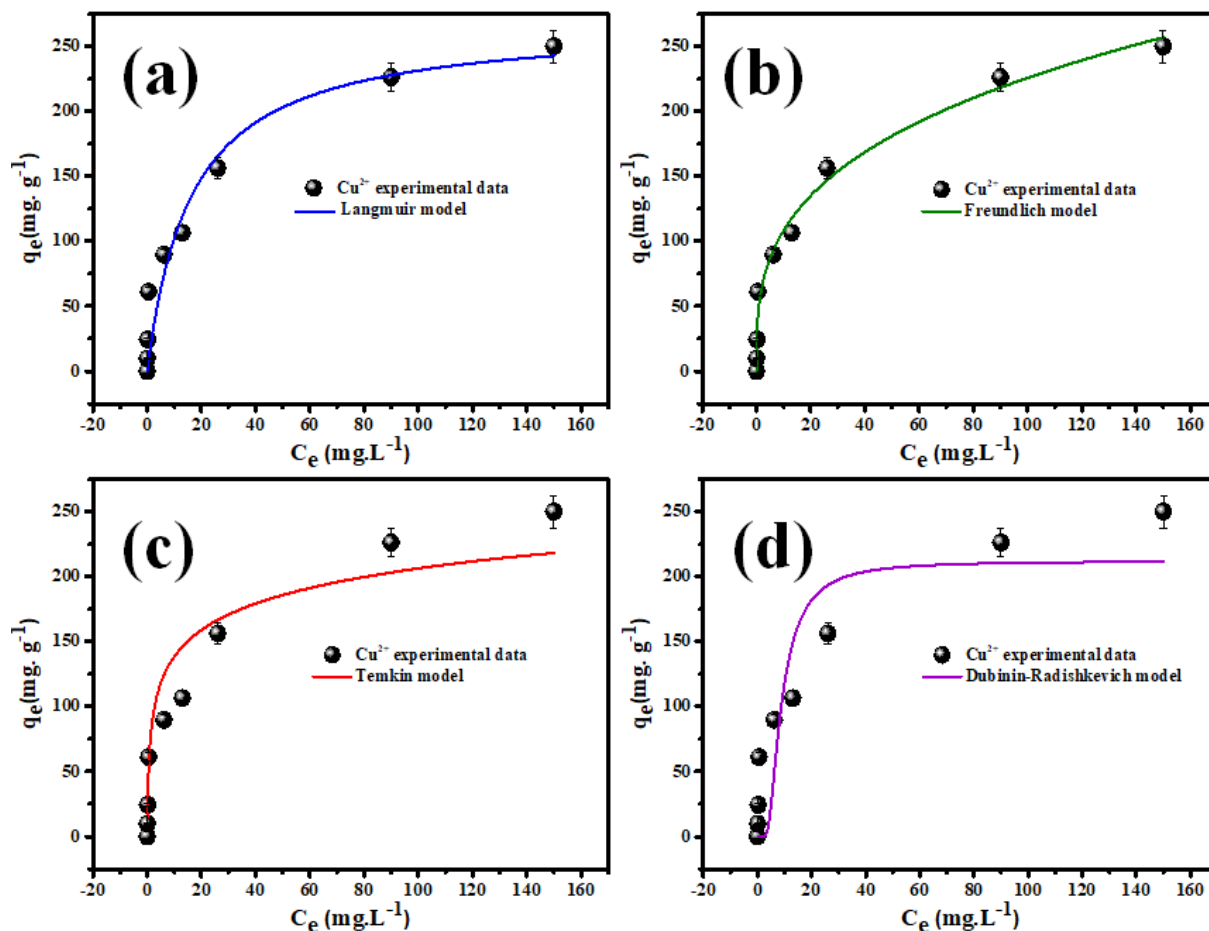
**Figure 5.** Impact of interaction time on the Cu (II) ions sorption onto  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$ .

### 3.2.4. Adsorption Isotherms Modeling

According to the initial concentration of 5 mg/L, the equilibrium concentration of Cu (II) is determined to be 9.5 mg/g, leading to an elimination rate higher than 99% (Figure 6 and Table 1). This result demonstrates that  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  is powerful in Cu (II) adsorption.

The Freundlich model parameters  $K$  and  $n$  are correlated to the bond force and dispersion. The Langmuir model defines  $q_{max}$  as the level of solid-phase encasement of all monolayer adsorption zones (Equation (4)).  $K_L$  is associated with the adsorption free energy. For the Langmuir: the feature of the sorbent is uniform; the adsorbed molecules or atoms are kept in separate and stable sites, and each location may accommodate just one molecule or atom. The adsorption energy is constant among all parts, and there is no interplay between bordering adsorbent surfaces and adsorbed molecules. Comparatively, the Freundlich model deals with non-homogeneous systems and reversible adsorption; however, monolayer adsorption is not restricted. Figure 6a–d displays graphs of experimental values modeled via Langmuir, Freundlich, Temkin and Dubinin–Radushkevich. The Langmuir model demonstrates a superior matching with the data with ( $R^2 = 0.9965$ ) compared to  $R^2 = 0.9644$  for the Freundlich model (Figure 6b). The Langmuir model (Figure 6a) reveals that the highest adsorption capacity of the  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  is 290.7 mg/g. The high capacity of the nanomaterial is owing to its improved surface area and large pores [45].

This observation indicates that Cu (II) ions are captured as monolayers on the  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  surface by chemisorption, which is the predominant mechanism of the Langmuir model [46].



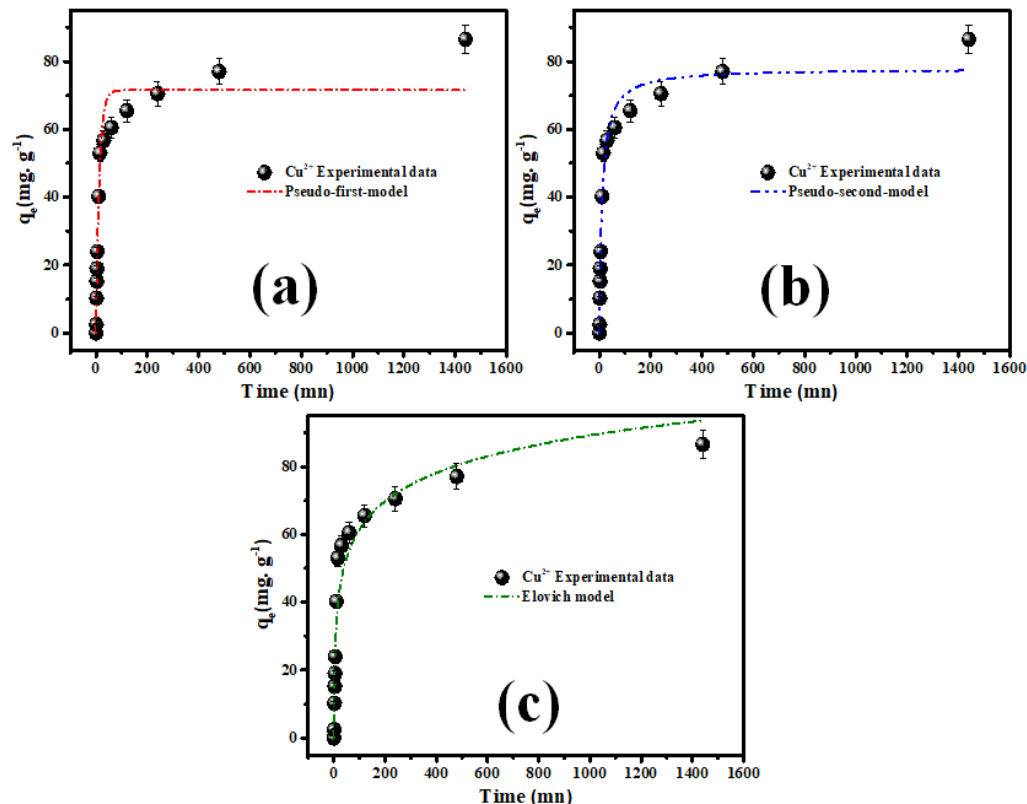
**Figure 6.** Removal of Cu (II) ions equilibrium data formfitting using non-linear: (a) Langmuir; (b) Freundlich; (c) Temkin; and (d) Dubinin-Radushkevich models.

**Table 1.** Various equilibrium Isotherm constants for Cu (II) adsorption by the nanocomposites  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$ .

Equilibrium Model	Parameters	$\text{Cu}^{2+}$
Langmuir	$qm$ ( $\text{mg}\cdot\text{g}^{-1}$ )	290.7
	$K_L$ ( $\text{mg}\cdot\text{g}^{-1}$ )	0.028
	$R_L$ ( $\text{L}\cdot\text{mg}^{-1}$ )	0.125
	$R^2$	0.9965
Freundlich	$n$	1.48
	$K_F$ ( $\text{L}\cdot\text{mg}^{-1}$ )	11.36
	$R^2$	0.9644
Temkin	$B$ ( $\text{J}\cdot\text{mol}^{-1}$ )	85.65
	$K_T$ ( $\text{L}\cdot\text{mg}^{-1}$ )	5.46
	$R^2$	0.9302
Dubinin-Radushkevich	$\beta$ ( $\text{mol}^2\cdot\text{J}^{-2}$ )	$2.095 \times 10^{-8}$
	$q$ ( $\text{mg}\cdot\text{g}^{-1}$ )	186.32
	$E$ ( $\text{J}\cdot\text{mol}^{-1}$ )	4886.5
	$R^2$	0.9833

### 3.2.5. Adsorption Kinetics Modeling

Formula (7) illustrates the Lagergren PFO kinetics model with  $k_1$  (1/min) rate constant and  $q_e$  is the highest quantity of Cu (II) ions eliminated at equilibrium. Regarding the PSO law (Formula (8)),  $k_2$  represents the rate constant (g/mg·min) and the initial sorption rate ( $h_0$ ) can be determined by  $h_0 = k_2 \cdot q_e$ . The half-life time,  $t_{1/2} = 1/(k_2 \cdot q_e^2)$ , is the time period over which Cu (II) metal ions are eliminated at half the equilibrium concentration of metal ions [47]. For the IPD mechanism model (Formula (10)), the parameters  $C$  that provides the thickness of boundary layer is obtained from the intercept, while the rate constant  $k_{dif1}$  (in mg/g·min<sup>1/2</sup>), is computed from the graph's slope (Figure 7). A regression coefficient  $R^2$  is applied to test the validity of these models. Table 2 shows variables estimated from the analysis of measured Cu (II) sorption values by kinetic models. It is apparent that the PSO model perfectly models the kinetics data of Cu (II) adsorption on MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> nano-materials since the  $R^2$  is 0.9978, indicating the presence of chemisorption supporting the Langmuir mode of adsorption [46]. Moreover, the computed quantity of  $q_e = 86.88$  mg/g is an exact match to the determined quantity of  $q_e = 86.88$  mg/g. Therefore, according to the literature, the PSO model can be employed to forecast the adsorption of metals ion on activated carbon [48]. The PSO kinetics model can be utilized to determine entire steps of the adsorption progression, such as outer film diffusion, adsorption, and internal particle diffusion [49]. Furthermore, the experimental data have been simulated by the Elovich by  $q_t$  vs.  $t$  graph (Figure 7), where the initial rate  $\alpha$  and  $\beta$  values were derived from the intercept and the slope, respectively. The parameters  $\alpha$  and  $\beta$  are the initial sorption rate constant (mg/g min) and the extent of surface coverage and the activation energy for chemisorption (g/mg). The data fitting to the Elovich model is indicated by the  $R^2$  (i.e., 0.9422) [50]. The relative matching with the Elovich equation corroborates a chemisorption control on the adsorption process in agreement with the PSO kinetic model [50,51].



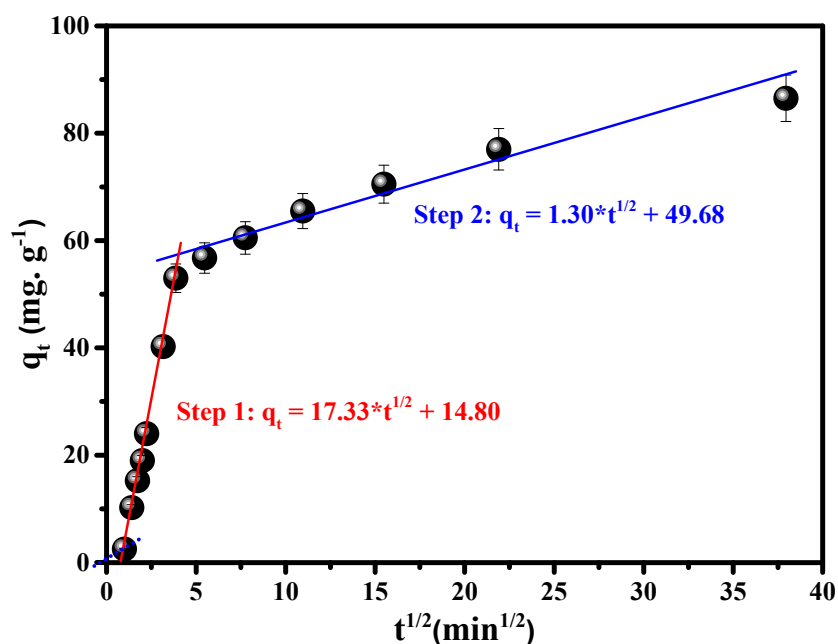
**Figure 7.** Nonlinear graphs: (a) PFO; (b) PSO; and (c) Elovich kinetics models for Cu (II) ions adsorption onto the fabricated MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> nanomaterials.

**Table 2.** Calculated kinetic model parameters for Cu (II) adsorption on MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> nanomaterials.

Pseudo-Second-Order Model						
Cu <sup>2+</sup>	$q_e(\text{Exp})$ (mg·g <sup>-1</sup> )	$t_{1/2}$ (min)	$h_0$ (mg·g <sup>-1</sup> ·min <sup>-1</sup> )	$q_e(\text{Cal})$ (mg·g <sup>-1</sup> )	$K_2 \times 10^4$ (g·mg <sup>-1</sup> ·min <sup>-1</sup> )	$r^2$
	89.75 ± 1.57	24.31 ± 0.86	3.57 ± 0.12	86.88 ± 1.23	4.73 ± 0.23	0.9978
Pseudo-First-order model			Elovich model			
	$q_e(\text{Cal})$ (mg·g <sup>-1</sup> )	$K_1 \times 10^3$ (min <sup>-1</sup> )	$r^2$	$\beta \times 10^2$ (g·mg <sup>-1</sup> )	$\alpha$	$r^2$
Cu <sup>2+</sup>	37.66 ± 1.98	2.31 ± 0.18	0.9378	8.38 ± 0.18	21.52 ± 1.26	0.9422

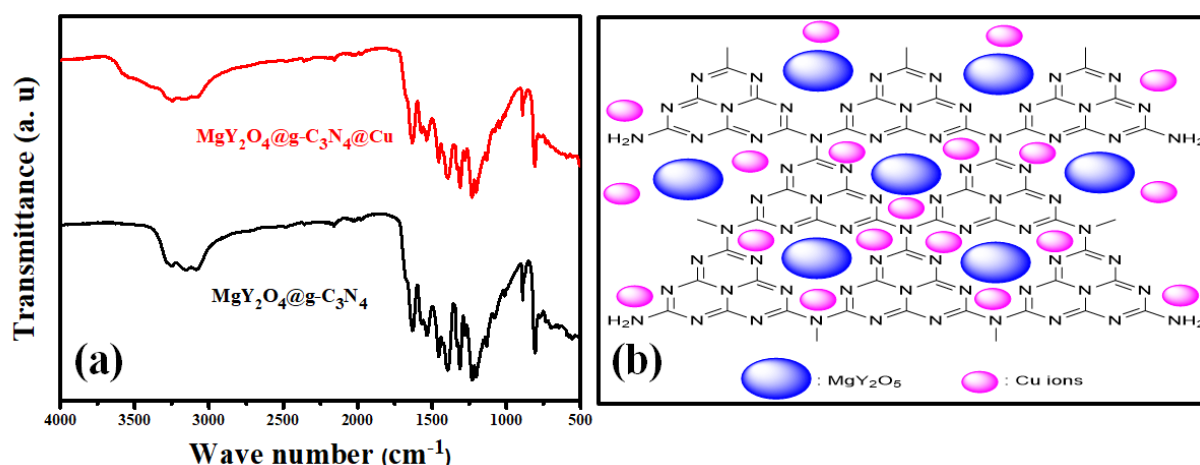
Consequently, the data from the kinetics experiment were evaluated with the intraparticle diffusion kinetic model (Figure 8). Numerous studies have shown that the intraparticle diffusion graph may exhibit multi-linearity, indicating that multiple steps may occur in the course of the adsorption process [52]. The results suggest that the majority of data points fall within two straight lines, as shown in Figure 8. The  $k_{dif2}$  estimate for the MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> nanomaterials is less than the  $k_{dif1}$  value nominates the intra-particle diffusion as the rate-determining step for Cu (II) adsorption onto the nanomaterials fabricated. In addition, it is essential to note that the slight deviation of the straight lines at the beginning suggests that intra-particle diffusion may not be the only rate-limiting step in the adsorption of Cu (II) ions onto MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> nanomaterials; additional probable surface adsorption processes are involved in the overall sorption rate also [53,54]. Additionally, it is significant to point out that the small deviation of the straight lines indicates that intra-particle diffusion might not be the only factor inhibiting the adsorption of Cu (II) on nanomaterials.

Intra-Particle Diffusion/Transport Model					
$k_{dif}$ (mg·g <sup>-1</sup> ·min <sup>-1/2</sup> )	C1	$r^2$	$k_{dif}$ (mg·g <sup>-1</sup> ·min <sup>-1/2</sup> )	C2	$r^2$
17.33	14.81	0.9987	1.30	49.78	0.9804

**Figure 8.** Intra-particle diffusion models (IPD) for Cu ions adsorption onto the prepared MgY<sub>2</sub>O<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> nanomaterials.

### 3.3. Mechanism of Cu (II) Adsorption onto $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$ Nanomaterial

The  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  FT-IR spectrum is depicted in Figure 9a. The spectrum exhibits broad and weak peaks at  $3030\text{--}3300\text{ cm}^{-1}$ , attributed to the N-H stretches and indicate the hydrogen attachment to the nitrogen atoms [55,56]. The peak located at  $2168\text{ cm}^{-1}$  corresponds to  $\text{C}\equiv\text{N}$ , but the sharp peak at  $804\text{ cm}^{-1}$  is belonging to the heptazine ring. The broad peaks in the  $900$  and  $1800\text{ cm}^{-1}$  range are indicative of s-triazine derivatives. The  $1445\text{ cm}^{-1}$  stretches can be allocated to the triazine ring ( $\text{C}_3\text{N}_3$ ), whereas the maxima at  $1316$  and  $1638\text{ cm}^{-1}$  come from heptazine ( $\text{C}_6\text{N}_7$ ) units [17]. The  $\text{g-C}_3\text{N}_4$  is a graphitic combination of  $\text{C}_3\text{N}_3$  and  $\text{C}_6\text{N}_7$  units, according to the FTIR spectrum analysis [57]. Cu (II) adsorption on  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  nanomaterials was identified by FTIR analysis. The FTIR spectra of  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  nanomaterials after Cu (II) adsorption is shown in Figure 9b. After adsorption, the stretching peaks of the O-H and ending amino groups are at lower frequencies. Meanwhile, the peak of the triazine ring mode shifts slightly to  $895\text{ cm}^{-1}$  from  $885\text{ cm}^{-1}$ . Further, both  $561$  and  $668\text{ cm}^{-1}$  stretching vibration patterns [7,58] have substantially turned orientation, showing a reaction between Cu (II) and oxygen atoms of  $\text{MgY}_2\text{O}_4$  by  $\pi$ - $\pi$  stacking bridge. The findings suggest that functional groups of  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  (OH, CN, and N-H) and p electron distributions of the triazine ring ( $\text{C}_3\text{N}_3$ ) may be responsible for the binding of the Cu (II) ions to the adsorbent surface through a chemisorption route. A study by (FTIR) demonstrated that the triazine ring functions as a Lewis base and aids in the Cu (II) elimination process, as proven by FTIR investigations. Figure 9b depicts a possible adsorption pathway for Cu (II) onto  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  relying on the FTIR measurements described above.



**Figure 9.** (a) FTIR spectra of  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  nanomaterials previously and after Cu (II) adsorption; and (b) proposed adsorption mechanism.

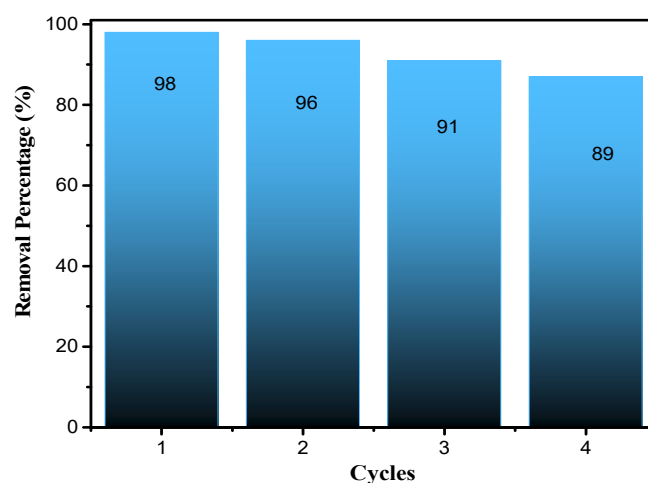
Consistent with the data in Table 3, the adsorption tendency of  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  nanomaterials towards aqueous Cu (II) was further evaluated and compared to different adsorbents that have been reported in the relevant literature.  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  nanomaterial removes Cu (II) from an aqueous solution quickly because it takes less time to reach equilibrium, which is only 40 min. Also, the hetero-nanostructure of the nanomaterials has a higher adsorption capacity than other nanostructures, at  $290.7\text{ mg/g}$  compared to  $7.4\text{--}150\text{ mg/g}$  for other nanostructures used. The high performance of  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  for removing Cu (II) is due to its remarkable nanostructure possessing high porosity. These findings make it a good and potentially competent adsorbent for abolishing various heavy metal ions in the aquatic phase. This behavior is similar that what obtained with Yang and his coworkers in the case of the amino modification of biochar for enhanced adsorption of copper ions from synthetic wastewater [54].

**Table 3.** Comparison of  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  adsorption parameters with various adsorbents.

Adsorbents Used	Removal Capacity (mg/g)	Refs.
Alg + CNC	53.4	[59]
CNC/Sulfate ( $-\text{SO}_3^-$ )	17.9	[60]
CNF/Tempo	49	[60]
MWCNTs/Chitosan nanocomposite	12.12	[61]
Corn straw	12.5	[62]
Sewage sludge	10.6	[63]
Hardwood	7.4	[64]
Pristine biochar (saw dust char)	16.1	[65]
Spartina alterniflora	48.5	[66]
GO/PEI	150.9	[67]
$\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{TiO}_2\text{-APTMS}$	50.5	[68]
$\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$	290.7	Current study

### 3.4. Reusability and Stability

The multiple uses of an adsorbent are considered by users to be of crucial importance in order to reduce wastewater management expenses and to limit the significant consumption of these adsorbents. To this end, a fairly extensive study through the succession of four adsorption cycles using the same  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  nanomaterials. The results presented in Figure 10 show that the percentage of degradation decreased slightly by less than 10% between the first and the fourth cycle. This decrease is mainly caused by a negligible saturation of the microporous part of  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  nanomaterials. This study confirms that  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  nanomaterials could be effectively reused for the treatment of wastewater loaded with mineral pollution. Likewise, this slight decrease is considered negligible because most industrial adsorbents have a lifespan of a few months after we note a saturation of the pores with a difficulty in desorption.

**Figure 10.** Variation of removal percentage of Cu (II) using  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  nanomaterials.

A sorbent with an interesting absorption capacity and an easy regeneration capability will be selected for other applications with real effluents (pharmaceutical, agricultural and textile effluents). This behavior is similar that obtained by with Yang and his coworkers in the case of the amino modification of biochar for enhanced adsorption of copper ions from synthetic wastewater [51].

An economic analysis for the  $\text{MgY}_2\text{O}_4@\text{g-C}_3\text{N}_4$  can be considered from different aspects. The adsorbent is prepared of the graphitic carbon nitride ( $\text{g-C}_3\text{N}_4$ ) which is feasibly synthesized from the most earth-abundant elements (carbon and nitrogen) to make strong covalent bonds in its conjugated layer structure and is bonded with the cheap precursors  $\text{Y}_2\text{O}_3$  and  $\text{MgO}$  cheap precursors [69]. In addition, the adsorbent has a high

adsorption capacity of 86.65 mg/g within 49 min and can be efficiently reused for four cycles. The amount of Cu (II) ions can be precipitated at high pH to obtain the hydroxides that can be employed to obtain the high-price copper entities [70].

For industrial-scale applications, the adsorbents can be sealed in a meticulous form by being lodged in an unyielding package, such as a synthetic or natural polymer, to ensure nanomaterial trapping and non-release in the water system. Such a prearrangement can be implemented to shuffle to a fixed-bed column for continuous flow treatment pilots [71].

#### 4. Conclusions

In conclusion,  $\text{MgY}_2\text{O}_5@\text{g-C}_3\text{N}_4$  nanomaterials were produced and tested as a Cu (II) adsorbent material in water. The BET and TEM analyses validated the material's nanomaterials morphology. At a pH of 3.0, the  $\text{MgY}_2\text{O}_5@\text{g-C}_3\text{N}_4$  nanomaterials displayed outstanding Cu (II) adsorption capability. Cu (II) adsorption on  $\text{MgY}_2\text{O}_5@\text{g-C}_3\text{N}_4$  nanomaterials followed the Langmuir isotherm model, with a maximum theoretical adsorption capacity of 290.7 mg/g. Adsorption kinetics suggested that the pseudo-second-order model may be used to describe the adsorption process. An FTIR examination revealed an abundance of hydroxyl groups on the surface of  $\text{MgY}_2\text{O}_5@\text{g-C}_3\text{N}_4$  nanomaterials and surface complexation dominated Cu (II) adsorption.  $\text{MgY}_2\text{O}_5@\text{g-C}_3\text{N}_4$  nanoparticles have tremendous potential as an adsorbent for removing Cu (II) from an aqueous solution in environmental pollution treatment due to their easy fabrication and high removal capability. Moreover, the results of the reusability analysis showed that the percentage of degradation decreased slightly by less than 10% between the first and the fourth cycle. This decrease is mainly caused by a negligible saturation of the microporous part of  $\text{MgY}_2\text{O}_5@\text{g-C}_3\text{N}_4$  nanomaterials. This study confirms that  $\text{MgY}_2\text{O}_5@\text{g-C}_3\text{N}_4$  nanomaterials could be effectively reused for the treatment of wastewater loaded with mineral pollution. The behavior of this material should be validated in other real matrices (containing a particle and mineral pollution. This will be the subject of our future investigations.

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