

# **Effects of ferrihydrite-impregnated powdered activated carbon on phosphate removal and biofouling of ultrafiltration membrane.**

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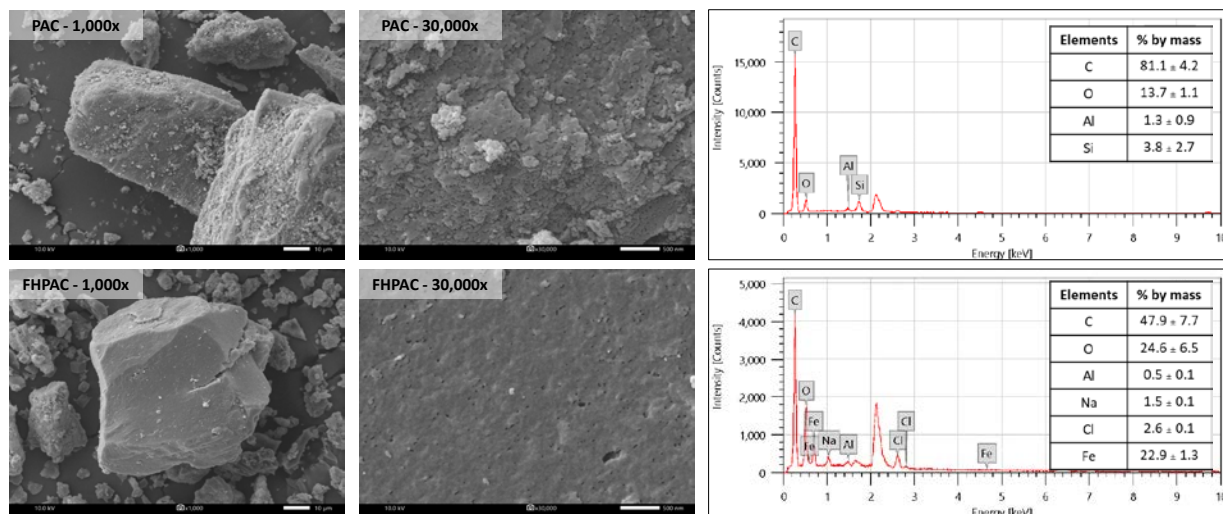
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## **Supplementary Data**

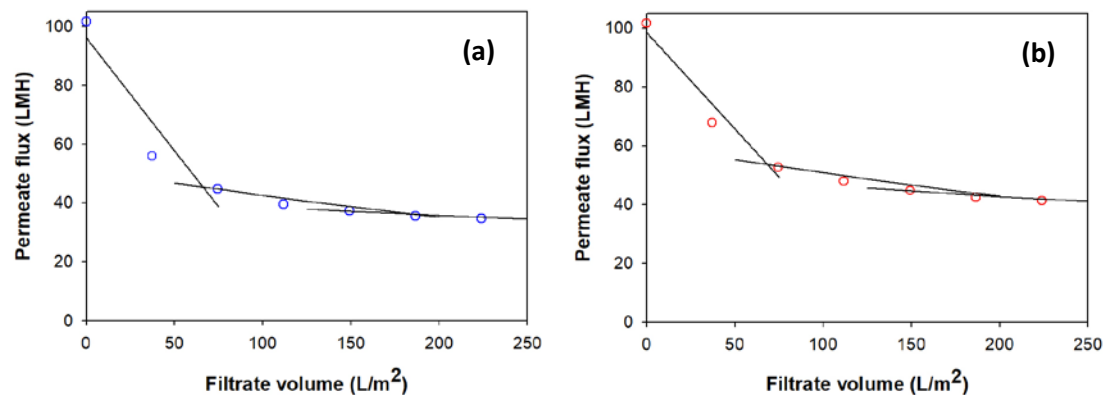
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**Figure S1** SEM images of PAC and FHPAC at different magnification levels (1,000x and 30,000x) and elemental compositions analysis by SEM-EDS.



**Figure S2** Mathematical models of fouling mechanism in biofouling test of (a) PAC+UF and (b) FHPAC+UF

**Table S1** Tap water quality from the Metropolitan Waterworks Authority, Bangkok, Thailand  
(October 2020)

Parameters	Unit	Result
True color	TCU	1
Apparent color	Pt-Co	< 5
Turbidity	NTU	0.45
pH	-	6.88
Conductivity	μS/cm	299
Alkalinity	mg/L as CaCO <sub>3</sub>	66
Total solids	mg/L	180
Total dissolved solids	mg/L	179
Chloride	mg/L	21
Sulfate	mg/L	44
Ammonia-nitrogen	mg/L	ND
Nitrate-nitrate	mg/L	2.82
Nitrite-nitrite	mg/L	ND
Calcium	mg/L	26.0
Iron	mg/L	< 0.05
Fluoride	mg/L	0.34
Manganese	mg/L	0.056
Magnesium	mg/L	6.00
Chlorine residual	mg/L	1.98
Total Bacteria	CFU/ml	0
<i>E.Coli</i>	Detectable/100 ml	non-detectable

**Table S2** Kinetic parameters of phosphate onto PAC and FHPAC with an initial phosphate concentration of 1.0 mg PO<sub>4</sub><sup>3-</sup>/L.

Adsorbents	q <sub>e,exp</sub> (mg/g)	Pseudo-first-order			Pseudo-second-order		
		k <sub>1</sub> (min <sup>-1</sup> )	q <sub>e,cal</sub> (mg/g)	R <sup>2</sup>	k <sub>2</sub> (g mg <sup>-1</sup> min <sup>-1</sup> )	q <sub>e,cal</sub> (mg/g)	R <sup>2</sup>
PAC	0.80	3.34	0.71	0.298	2377.02	0.71	0.848
FHPAC	4.80	30.92	4.08	0.835	0.053	5.01	0.985

**Table S3** Isotherm parameters of phosphate onto FHPAC with the variation of initial phosphate concentration from 0.1 – 13.7 mg PO<sub>4</sub><sup>3-</sup>/L.

Adsorbents	Langmuir			Freundlich		
	q <sub>m</sub> (mg/g)	K <sub>L</sub> (L/mg)	R <sup>2</sup>	K <sub>F</sub> (L/mg)	n	R <sup>2</sup>
FHPAC	22.32	0.97	0.921	7.66	1.81	0.924

**Table S4** Mathematical models of fouling mechanism in biofouling test of PAC and FHPAC

Experiment	Complete blocking		Intermediate blocking		Cake filtration	
	K <sub>b</sub> (h <sup>-1</sup> )	R <sup>2</sup>	K <sub>i</sub> (m <sup>2</sup> L <sup>-1</sup> )	R <sup>2</sup>	K <sub>c</sub> (h m <sup>4</sup> L <sup>-2</sup> )	R <sup>2</sup>
PAC	0.762	0.891	0.0019	0.964	4×10 <sup>-5</sup>	0.985
FHPAC	0.656	0.954	0.0017	0.992	4×10 <sup>-5</sup>	0.987

**Table S5** Fouling mechanism of PAC+UF and FHPAC+UF bench scale operation via mathematical models.

Cycle	Complete blocking		Standard blocking		Intermediate blocking		Cake filtration	
	K <sub>b</sub> (h <sup>-1</sup> )	R <sup>2</sup>	K <sub>s</sub> (m <sup>2</sup> L <sup>-1</sup> )	R <sup>2</sup>	K <sub>i</sub> (m <sup>2</sup> L <sup>-1</sup> )	R <sup>2</sup>	K <sub>c</sub> (h m <sup>4</sup> L <sup>-2</sup> )	R <sup>2</sup>
<b>PAC</b>								
1	-0.0764	0.804	-0.0024	0.887	0.004	0.998	-1.4×10 <sup>-5</sup>	0.837
2	-0.0273	0.988	0.0004	0.900	0.0045	0.937	4.0×10 <sup>-6</sup>	0.790
3	-0.0274	0.787	0.0004	0.954	0.0051	0.981	6.0×10 <sup>-6</sup>	0.886
<b>FHPAC</b>								
1	0.0690	0.830	-0.0024	0.894	0.0036	0.996	-1.4×10 <sup>-5</sup>	0.840
2	0.0502	0.979	0.0002	0.897	0.0044	0.936	2.0×10 <sup>-6</sup>	0.820
3	0.0374	0.897	0.00016	0.740	0.0053	0.925	1.8×10 <sup>-6</sup>	0.572