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SSH-Aerosol v1.1: A Modular Box Model to Simulate the Evolution of Primary and Secondary Aerosols

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Abstract: Particles are emitted by different sources and are also formed in the atmosphere. Despite the large impact of atmospheric particles on health and climate, large uncertainties remain concerning their representation in models. To reduce these uncertainties as much as possible, a representation of the main processes involved in aerosol dynamics and chemistry is necessary. For that purpose, SSH-aerosol was developed to represent the evolution of the mass and number concentrations of primary and secondary particles, across different scales, using state-of-the-art modules, taking into account processes that are usually not considered in air-quality or climate modelling. For example, the particle mixing state and the growth of ultra-fine particles are taken into account in the aerosol dynamics, the affinity of semi-volatile organic compounds with water and viscosity are taken into account in the partitioning between the gas and particle phases of organics and the formation of extremely low-volatility organic compounds from biogenic precursors is represented. SSH-aerosol is modular and can be used with different levels of complexity. It may be used as standalone to analyse chamber measurements. It is also designed to be easily coupled to 3D models, adapting the level of complexity to the spatial scale studied.

Keywords: secondary aerosols; viscosity; ultra-fine particles; mixing state; partitioning

1. Introduction

With the impact of air pollution on health and ecosystems being a great concern, models, such as chemical-transport models (CTM), are often used to simulate air quality, i.e., to compute the concentration of atmospheric gases, aqueous-phase species and particulate matter (PM). Particles, especially fine particles, lead to adverse effects on human health [1], as well as visibility reduction. They also affect the manner in which radiation passes through the atmosphere [2] and represent an uncertain component of climate changes due to direct and indirect effects on the Earth's radiative budget. Particles are complex mixtures made of several compounds, and of size ranging from a few nanometres to several micrometres. They can be emitted directly from various sources (e.g., natural such as wild fires, sea-salt, dust and anthropogenic) or can be formed in the atmosphere from the transformations of organic or inorganic gas precursors. The aerosol dynamics is governed by condensation/evaporation of condensable compounds (semi-volatile compounds that can condense on particles), coagulation and nucleation. The underlying processes are particularly complex, and they may be represented using different approaches. Hence, several aerosol models have been developed [3–16]), either as box stand-alone models, or as coupled to a 3D model.

The SSH-aerosol model is based on the coupling of three state-of-the-art modules: SCRAM (Size-Composition Resolved Aerosol Model [17]) for the dynamic evolution, SOAP (Secondary Organic Aerosol Processor, [18]) for gas/particle partitioning of organic compounds and H₂O (Hydrophobic/Hydrophilic Organics [19–21]) for the formation of condensable organic compounds.

1.1. Aerosol Dynamics

The PM size distribution may be modelled using different approaches, among which the most common ones in CTMs are the sectional size distribution (the size distribution is discretised into sections, e.g., [3–10]) and the modal size distribution (the size distribution is discretised into log-normal modes, e.g., [11–14]). Because Sartelet et al. [14], Devilliers et al. [22] showed that modal models have difficulties in dealing with the growth of ultra-fine particles, SCRAM uses a sectional approach. For 3D applications, because each section or mode is transported individually, the size range of each section or mode needs to be constant throughout the simulation. As particles grow/shrink with condensation/evaporation, the bounds of the sections evolve, and it is necessary to redistribute the number and mass on fixed section bounds, introducing numerical errors. Different approaches are implemented in SCRAM depending on whether the mean diameter of the section is allowed to vary or not [22].

In CTMs, internal mixing is often assumed, i.e., a chemical composition is associated to each particle size section [5,15,16,23–25]. Although this assumption may be appropriate for air masses far from emission sources, it may be unrealistic close to emission sources, where emitted particles can have compositions that are very different from background particles and from particles emitted from other sources. The mixing state is partially resolved in models (e.g., [12,26]) which consider particles to be either mixed or not mixed. In numerous climate models, the mixing state is often treated implicitly by using an ageing time to convert freshly emitted particles from externally to internally mixed [27]. The mixing state is explicitly resolved in SCRAM; both the particle size distribution and the mass fraction of chemical compounds inside particles are discretised into sections. In other words, the chemical composition of particles in each size section is discretised according to the percentage of one or more of its compounds, as detailed in [28]. A similar discretisation is performed for the percentage of black carbon in [10,29]. SCRAM was used to show that, over Greater Paris in summer, more than half (up to 80% during rush hours) of black carbon particles are barely mixed at the centre of Paris, while BC particles are more mixed outside [30]. Mixing-state resolved simulations show higher nitrate and lower ammonium concentrations in the particle phase than internal-mixing simulations, leading to differences up to 22% in inorganic concentrations, 80% in the water content of particles and 72% in aerosol optical depth [30].

1.2. Formation of Condensable

Secondary pollutants such as ozone (O₃) and PM precursors are formed during the gas-phase degradation of anthropogenic and biogenic compounds: oxides of nitrogen and volatile organic compounds (VOCs). Because of its health impact and its link to the oxidation capacity of the atmosphere, the formation and destruction of O₃ have been extensively studied, and different condensed chemical mechanisms have been developed: lumped structure mechanisms (CB05 [31]) and lumped species mechanisms (RACM2 [32] and SAPRC [33]).

As organic gases are oxidised in the gas phase (by OH, O₃ and NO₃), their volatility evolves. It may decrease by the addition of polar functional groups (such as hydroxyl, hydroperoxyl, nitrate and acid groups). On the other hand, some oxidation products may have higher volatility than the parent organic gases due to the cleavage of carbon–carbon bonds. Products of low volatility may condense on the available particles to establish equilibrium between the gas and particle phases. The formation of these semi-volatile organic species (SVOC) is often not considered in the mechanisms described previously,

which were originally developed to model O₃ concentrations. To be able to represent SOA formation using these models, additional oxidation products corresponding to surrogate SVOC species are added to most 3D models using different approaches [19,34,35], as now detailed.

Due to the lack of knowledge and the sheer number and complexity of organic species, most chemical reaction schemes for organics are very crude representations of the true mechanism. Different categories of SOA models exist: the widely used two-compound Odum approach [36] and the more recent volatility basis set (VBS) approach [35,37,38]. H²O represents the formation of SOA using surrogate molecules with representative physico-chemical properties for gas/particle partitioning [19]. This approach allows us to take into account the most relevant processes for SOA formation (completeness of the precursor VOC list [21], ideality assumption, treatment of oligomerization, importance of low-NO_x vs. high-NO_x regimes and treatment of SOA affinity with water) [39]. Although only a few surrogates are used to represent the SOA formation, the oxidation properties and the affinity with water of organic particles are well represented in the H²O model by comparison to measurements made in the south of France (Europe) in summer, when the biogenic contribution to SOA is important Chrit et al. [20], Freney et al. [40]. However, in winter time, when the anthropogenic contribution of SOA is dominant, both the surrogate and the VBS approaches underestimate the oxidation degree of SOA [41]. The SOA affinity with water, which is often ignored in 3D models [15,16,35], largely influences the formation of organic aerosols. The measurements of Chrit et al. [20] showed that about 64% of the organic carbon is soluble in Corsica (France) in summer. The modelling study of [39] estimated that twice more isoprene SOA is formed over Europe if isoprene SOA is assumed to be hydrophilic rather than hydrophobic. Furthermore, considering not only water but also inorganic and hydrophilic organic aerosols in the absorbing mass of the aqueous phase leads to an increase of organic aerosol concentrations by about 10% on average over the whole of Europe in summer [42].

1.3. Gas/Particle Partitioning of Organics

Whereas most models use a simple partitioning approach assuming ideality and absorption on a single organic phase, SOAP [18] is a thermodynamic model that computes the partitioning of organic compounds, taking into account several processes involved in the partitioning of SVOC (hygroscopicity, absorption into the aqueous phase of particles, non-ideality and phase separation) and computes the formation of organic aerosol either with a classic equilibrium representation (the partitioning of organic compounds is instantaneous) or with a dynamic representation (where the model solves the dynamic of the condensation/evaporation limited by the low diffusivity in the particle due to its high viscosity). Viscosity is not taken into account in 3D models. However, the sensitivity study of Kim et al. [42] showed that assuming a highly viscous organic phase leads to an increase in SOA concentrations during daytime, which can be as high as 20% for highly-volatile compounds.

This paper aims at presenting the SSH-aerosol model, which is designed to represent the formation of aerosols, across different scales (the model being able to take into account slow or fast processes involved on the evolution of particles over short distances), using state-of-the-art approaches for each of the important processes involved in their formation: gas-phase transformation leading to the formation of condensable (semi-volatile compounds that can condense on particles), dynamic evolution of the composition and size distribution of particles and partitioning between the gas and particle phases. It models the formation of aerosols from gaseous precursors and their evolution. It simulates the mass concentrations of aerosols, as well as their number concentrations and mixing states. SSH-aerosol can represent explicitly the evolution of the mixing state of particles, allowing different mixing states not only to co-exist, but also to evolve with time, taking into account nucleation, coagulation, condensation/evaporation. Furthermore, SSH-aerosol takes into account not only the absorption of semi-volatile organic compounds onto an organic phase (as commonly assumed), but also the absorption onto an aqueous phase, formed by water and

inorganics. SSH-aerosol is designed to be easily implemented in air-quality models of different scales, such as chemistry-transport models or Computational Fluid Dynamics models, or to be used as a 0D box model for comparison to measurement chambers and to simulate the processes leading to secondary aerosol formation (taking into account the gas/particle partitioning of semi-volatile compounds). The model is described in Section 2, and test cases to validate and present the modelled aerosol processes are detailed in Section 3.

2. Description of the Model

The SSH-aerosol model is designed to be modular, so that the user can choose the physical and chemical complexity required, depending on the scale and the processes studied.

The code metadata are detailed in Appendix A.

2.1. Input Data and Model Results

The SSH-aerosol package contains different repertoires for source code, configuration files, input files, output files and visualisation of outputs.

The configuration file (*namelist.ssh*) specifies the user's choices for parameterisations and processes that are taken into account in the simulation, as detailed in the users' guide. It points to the list of species and their properties, as well as to the initial concentrations and emissions. The configuration file allows the user to use the same code for different applications with different levels of complexity.

SSH-aerosol considers several particle compounds: mineral dust, black carbon, inorganics (sodium, sulphate, ammonium, nitrate and chloride) and organics (primary organic aerosol POA and secondary organic aerosol SOA) compounds (detailed in Appendix B), with size ranging between a nanometre and tens of micrometres. SSH-aerosol can classify particles by their both composition and size, based on a comprehensive combination of all chemical species and their mass-fraction sections. All three main processes involved in aerosol dynamics (coagulation, condensation/evaporation and nucleation) are included.

During the simulation, gas-phase, particle phase (in each aerosol layer for organics) and total (gas + particle) mass concentration ($\mu\text{g m}^{-3}$) of each compound are output, as well as the number concentrations ($\# \text{ m}^{-3}$) and mean diameter (μm) of each size and composition section.

The bounds of the size and composition sections are defined in the configuration file. The bounds of the size section may evolve during the simulation if the user simulated only condensation/evaporation with redistribution (see the next section for more details).

Different mechanisms are available to use for gas-phase chemistry, e.g., the Carbon Bond 05 mechanism (CB05) [31] and RACM2 [32]. The gaseous species of SSH-aerosol are then those of the gas-phase chemistry scheme used to which species dedicated to the modelling of SOA are added. Five classes of SOA precursors are considered [19,39]: intermediate and semi-volatile organic compounds of anthropogenic emissions, aromatic compounds, isoprene, monoterpenes and sesquiterpenes. For each precursor, only a few surrogates are used to represent all the species formed. The mechanism leading to the formation of isoprene SOA is detailed in [43]; for monoterpenes and sesquiterpenes in [20,44]; for toluene and xylenes and intermediate and semi-volatile organic compounds in [19]; and for guaiacol, syringol, benzene, phenol, catechol, cresol, furan, naphthalene and methylnaphthalene in [21]. Note that the chemical reactions go through a chemical preprocessor in SSH-aerosol, making it easy to modify them if needed.

2.2. Structure of the Model

The gaseous chemistry and aerosol modules of SSH-aerosol are called in the routine *ssh-aerosol.F90*. It first reads the configuration file detailing the user's choice for the modelling; then, it initialises the different variables, such as meteorological parameters and concentrations, and computes partition coefficients for coagulation if necessary. After initialisation, within a time loop, photolysis rates and

emissions are read from files if required by the user, and the gaseous chemistry (H₂O module) and aerosol dynamics (SCRAM and SOAP modules) are solved sequentially. The time step for this loop is determined by the user and corresponds to the time step where concentrations are output. Note that the time steps used to solve gaseous chemistry and aerosol dynamics are different from the time step of this loop. In each module, the time step is adapted using the numerical algorithm of the module: Rosenbrock for gaseous and organic chemistry [45] and the explicit trapezoidal rule of order 2 (ETR) for aerosol dynamics [14,46]. For aerosol dynamics (SCRAM), coagulation, nucleation and condensation/evaporation of dynamic sections and low-volatility species are solved fixing the initial time step to the minimum value chosen by the user, and then adjusting the time step using the first- and second-order approximations provided by ETR. Two algorithms may be used to solve these processes: coagulation can also be solved simultaneously to nucleation and condensation/evaporation or split (solved separately) depending on the user's choice. If they are split, coagulation is solved first, because it is the slowest process. Because nucleation and condensation/evaporation may be competing for the availability of gases, they are then solved simultaneously. If bulk thermodynamic equilibrium is assumed for small size sections, then it is calculated at the end of each main time step after solving coagulation, nucleation and condensation/evaporation of dynamic sections and low-volatility species. The thermodynamics of condensation/evaporation uses the model ISORROPIA [47] for inorganics and SOAP for organics [18].

2.3. Coupling to 3D Models

Regarding the coupling of SSH-aerosol and 3D codes, a dedicated Application Programming Interface (API) is available in SSH-aerosol. It allows the 3D code to easily initialise, read or modify the internal variables and perform time-advancement if transport and chemistry processes are coupled in the 3D code by a first order scheme [48]. The usual work-flow allowing to couple a 3D code with SSH-aerosol using the API is now briefly described.

Once the 3D code has loaded the SSH-aerosol shared library, a call to the API function `api_sshaerosol_initialize_` performs the initialisation steps specific to SSH-aerosol. This function must be called only once, at the beginning of the simulation. Then, at each time step, after solving transport, emission and deposition processes, a loop over the computational cells of the 3D domain should be performed.

For each cell, the 3D code should first update the key internal variables of SSH-aerosol using API functions such as `api_sshaerosol_set_temperature_` to update the temperature or `api_sshaerosol_set_aero_` to update the aerosol concentrations. Dedicated API functions allow the external code to set the pressure, temperature, humidity and gas and aerosol concentrations. After such modifications, a call to the API function `api_sshaerosol_init_again_` is required to update the auxiliary internal variables of SSH-aerosol. Then, gaseous chemistry and aerosol dynamic can be advanced by one time step using the API functions `api_sshaerosol_gaschemistry_` and `api_sshaerosol_aerodyn_`. Note that the internal time step of SSH-aerosol may be lower and different from the input time step, as described in Section 3.5. Finally, the 3D code can retrieve the updated concentrations using API functions such as `api_sshaerosol_get_aero_`.

The repository of the code provides a small C program showing how such a shared library can be used. Please note that the shared library can also be used from other languages, such as Fortran or Python.

3. Aerosol Processes

Different test cases are set up to illustrate the different aerosol processes taken into account, the software functionalities, and to validate the model by comparison to simulations carried out using other models (coagulation, condensation of extremely low-volatility compounds, condensation/evaporation and Kelvin effect) or chamber measurements (organic aerosol formation). The test cases are now briefly

described (more details and other test cases are available in the users' guide). Different representation of aerosol processes (more or less time consuming) are available and can be chosen by the user.

3.1. Coagulation and Condensation of Extremely Low-Volatility Compounds

Brownian coagulation is believed to be the dominant mechanism of particle coagulation in the atmosphere. When two particles coagulate, the resulting particle may belong to a section different from the initial sections of the particles (as it has a larger diameter than the diameters of the particles that coagulate). The partitioning of coagulated particles between sections is computed with partition coefficients, which are defined at the beginning of SSH-aerosol. They can be read from a file and computed using a Monte-Carlo approach, as defined in [28]. The partition coefficients are computed/read initially and kept constant throughout the simulation, which is possible because section bounds are constant.

The condensation rate of low-volatility compounds, such as sulphate, depends on the particle surface available and thus on the diameter and number of particles [8].

In the literature, to test the overall behaviour of PM models, the following basic tests of condensation and coagulation of sulphate are often considered [11,49,50]. A tri-modal PM distribution is considered initially, with particles being made exclusively of sulphate. The parameters of the initial distribution considered here are those of hazy conditions for the condensation test with a sulphuric acid production rate of $9.9 \mu\text{g m}^{-3}$ and those of urban conditions for the coagulation test [49,50], because these two tests represent the two most stringent conditions for coagulation and condensation. Temperature is taken as 283.15 K. Simulations are conducted for 12 h. The reference solutions for the coagulation and condensation tests are those of Zhang et al. [50] obtained with another model, and those simulated with the SIREAM [8].

As shown in Figures 1 and 2, SSH-aerosol does very well in representing the growth of particles by coagulation and condensation of sulphate.

Figure 1. Coagulation test case. Number (**left**) and volume (**right**) concentrations as a function of particle diameter. Initial concentrations are in green and concentrations after 12 h of simulation are in red. The concentrations simulated with SIREAM are plotted with orange stars and those simulated by Zhang et al. in purple.

Figure 2. Condensation test case. Number (left) and volume (right) concentrations as a function of particle diameter. Initial concentrations are in green and concentrations after 12 h of simulation are in red. The concentrations simulated with SIREAM are plotted with orange stars and those simulated by Zhang et al. in purple.

The condensation of low-volatility compounds does not concern only sulphate, but also organic compounds (see Section 3.4.1), such as extremely low-volatility organic compounds (ELVOCs) from monoterpene oxidation (surrogates Monomer and Dimer in H_2O) and compounds arising from the oxidation of intermediate and semi volatile organic compounds (surrogate SOAIP in H_2O).

3.2. Condensation/Evaporation

For condensation/evaporation, the mass transfer rate is governed by the gradient between the gas-phase concentration and the gas-phase concentration at the surface of the particle, as described in [17,18]. This gradient takes into account the Kelvin effect, i.e., the effect of the curvature of small particles, which leads to an increase of the volatility of chemical compounds, making their condensation more difficult and favouring their evaporation. The condensation/evaporation process is solved using a Lagrangian approach by letting the section bounds evolve.

3.2.1. Redistribution

As particles grow/shrink with condensation/evaporation, the bounds of the sections or modes evolve, and it is necessary to redistribute the number and mass on sections with fixed bounds, inducing numerical errors. This redistribution is necessary if coagulation is taken into account, because the partition coefficients are precomputed on fixed bounds. It is also necessary for 3D applications that the sections be of distinct size ranges throughout the simulations. Different approaches exist for redistributing the sections depending on whether the mean diameter of the section is allowed to vary or not [22]. Following the work of Devilliers et al. [22], the moving-diameter approach or the Euler-coupled approach is preferred here.

Redistributing the mass and number concentrations amongst bins leads to numerical diffusion, as can be seen in Figure 3, which shows the number and volume distribution of particles using these different redistribution algorithms.

Figure 3. Condensation test case with moving diameter (in green), Euler-coupled (in red) redistributions and no redistribution (in orange). Initial concentrations are in blue. Number (left) and volume (right) concentrations.

3.2.2. Thermodynamic Equilibrium

To gain computational time, the gas-phase concentration at the particle surface is often assumed to be equal to the bulk equilibrium gas-phase concentration. In other words, the dynamic modelling may be replaced with an assumption of thermodynamic equilibrium between the bulk gas and PM phases. Although this assumption may be valid for small particles, several measurements [51], as well as studies of time scales required to reach thermodynamic equilibrium [52], have shown that the assumption of thermodynamic equilibrium may not hold for larger inorganic particles [53]. Although the equilibrium approach is less accurate than the dynamic approach, it is attractive because it is computationally fast.

If global thermodynamic equilibrium is assumed, then the dynamic evolution of particles and condensation of low-volatility gases is first performed. Then assuming bulk equilibrium, the partitioning between particle and gas phases is computed using the thermodynamic model, and a weighting scheme is used to redistribute the bulk particle equilibrium concentrations between the different sections. The weighting scheme depends on the condensation/evaporation kernel of the condensation/evaporation rate [8,14]. A cutoff diameter may also be used to separate particles assumed to be at thermodynamic equilibrium to those for which the dynamic mass transfer between gas and particle should be computed. Sections of mean diameter above this cutoff diameter are computed dynamically and bulk thermodynamic equilibrium is assumed for sections of mean diameter below.

To illustrate this effect, the highly polluted day of 25 June 2001 in Tokyo (Japan) is simulated as in [14]. Measurements of PM and gaseous compounds made in Tokyo are taken as initial conditions. Note that these data were averaged continuously during 24 h under varying meteorological conditions. Because HNO_3 and NH_3 are the compounds the most influenced by the algorithm used to represent condensation/evaporation, the model concentrations simulated dynamically, assuming bulk equilibrium and using a cutoff of $0.01 \mu\text{m}$, are compared in Figure 4. Although the dynamic simulation of the partitioning is the most accurate, it is about three times slower than bulk thermodynamic equilibrium, while the hybrid method with a cutoff diameter of $0.01 \mu\text{m}$ is about 1.5 times slower than bulk thermodynamic equilibrium.

Figure 4. Condensation/evaporation of inorganic test case. Time evolution of HNO₃ concentrations (left) and NH₃ concentrations (right).

3.2.3. Kelvin Effect

To illustrate the importance of the Kelvin effect for the growth of ultra-fine particles, the test case of Devilliers et al. [22] concerning the growth of ultra-fine particles emitted from the exhaust of a diesel engine is simulated. As in [22], the typical diesel engine emission initial distribution from [54] is used here to study the gas/particle conversion of nonadecane ($\text{C}_{19}\text{H}_{40}$). It has a reference saturation vapour pressure of 6.1×10^{-4} Pa at $T = 298$ K, which is very close to that of the model surrogate POAmP (Primary Organic Aerosol of medium volatility, see Appendix B). Particles are assumed here to consist solely of POAmP. To show the importance of the Kelvin effect, two simulations are conducted: with and without the Kelvin effect.

The results in Figure 5 show clearly that the Kelvin effect must be taken into account when the evolution of small particles is simulated: particles are much less affected by condensation/evaporation when it is not included in the model. The ultra-fine particles of the initial distribution have been transferred to the gas phase while the coarse ones have grown to a greater size range.

Figure 5. Kelvin test case. Number (left) and volume (right) concentrations. The initial concentrations are in blue, those simulated by SSH-aerosol are in orange (with Kelvin effect) and in dashed green (without Kelvin effect), and those simulated by Devilliers et al. [22] with 48 size sections are displayed with red stars.

3.2.4. Particle Viscosity

The gas/particle mass transfer of hydrophobic organic aerosols may strongly be affected by particle viscosity.

To illustrate this effect, the condensation of hydrophobic organic surrogates of different volatilities is studied for different viscosities, represented by different values of the organic-phase diffusion coefficients D (10^{-18} , 10^{-19} , 10^{-20} , 10^{-21} , 10^{-22} , 10^{-23} and 10^{-24} $\text{m}^2 \text{s}^{-1}$). The value $D = 10^{-12}$ $\text{m}^2 \text{s}^{-1}$ corresponds to an inviscid particle, while the value $D = 10^{-24}$ $\text{m}^2 \text{s}^{-1}$ corresponds to a very viscous particle [55–57]. Each particle is discretised into five layers to model the flux of diffusion of the organic compounds in the particle. The test cases presented here are similar to those of the Figure 6 of [18]. Three organic surrogates (see Appendix B) of the SSH-aerosol model are successively studied: SOAIP (Secondary Organic Aerosol of low volatility), POAIP (Primary Organic Aerosol of low volatility) and POAmP (Primary Organic Aerosol of medium volatility) and which have partitioning coefficients K_p equal to about 100, 1 and 0.01 $\text{m}^3 \mu\text{g}^{-1}$. The surrogate that condenses is initially only in the gas phase, with a mass of 5 $\mu\text{g m}^{-3}$. It condenses on an organic phase of 5 $\mu\text{g m}^{-3}$ made of SOAIP, which has a very low volatility ($K_p = 100$ $\text{m}^3 \mu\text{g}^{-1}$). The condensation of the surrogates from different values of the viscosity is computed and Figure 6 represents the time variations of particle-phase organic concentrations of the surrogate (SOAIP in panel (a), POAIP in panel (b) and POAmP in panel (c)) for different values of viscosity. The surrogate of low volatility (SOAIP) condenses quickly onto the organic phase, independently of the viscosity (panel (a) of Figure 6). All the organic mass is then in the particle phase. Although the condensation of POAIP is influenced by the viscosity, a large fraction of the gas-phase concentration of POAIP condenses quickly (panel (b) of Figure 6). For POAmP, which is the most volatile of the three surrogates, high viscosity (low diffusion coefficient) strongly inhibits the condensation of POAmP (panel (c) of Figure 6). The computing time is influenced by the number of layers considered. In the viscous case, considering five layers, instead of 1, the computing time increases depending on the volatility of the compound by a factor 1.5, 5.4 and 36.4 for the test cases with SOAIP, POAIP and POAmP, respectively.

3.3. Mixing State

The test cases presented in the previous section relied on the internal-mixing assumption (one aerosol composition per aerosol size section). To illustrate how coagulation and condensation affect the mixing state of particles, the coagulation and condensation test cases are revisited by assuming that the initial particle distribution is made of two extremely low-volatility compounds of same density and volatility (sulphate and another extremely low-volatility compound). The mass and number concentrations of these two compounds are initially equal. Four and ten composition sections are used in the coagulation and condensation test cases, respectively. After 12 h of simulation, by summing the mass and number of particles of all size fraction sections, the size number and volume distribution are identical to those obtained with the internal mixing assumptions. The evolution of the mixing state of particles after 12 h of coagulation may be seen by comparing the two panels in Figure 7, which show the number concentration as a function of the size and fraction of sulphate, which is one of the two compounds of the particles. Similarly, the evolution of the mixing state of particles after 12 h of condensations may be seen by comparing the two panels in Figure 8, which shows the mass concentration as a function of size and fraction of sulphate. In the condensation test case, sulphuric acid condenses to form sulphate. Because the condensation rate is greater for particles of low diameters, the sulphate fraction is greater for those particles at the end of the simulation.

Figure 6. Viscosity test case: time evolution of organic concentrations ((a) SOAIP; (b) POAIP; and (c) POAmP) for several organic-phase diffusivities: 10^{-18} (dark blue), 10^{-19} (light blue), 10^{-20} (green), 10^{-21} (yellow), 10^{-22} (magenta), 10^{-23} (red) and 10^{-24} ($\text{m}^2 \text{s}^{-1}$).

In terms of computing time, compared to the internal mixing case, the coagulation test case is 16 times slower when discretising the composition into four sections, and the condensation test case is 13 times slower when discretising the composition into 10 sections.

Figure 7. Particle number concentration ($\# \text{m}^{-3}$) for the coagulation test case, as a function of size and composition: initial concentrations (left) and after 12 h of simulation (right).

Figure 8. Particle mass concentration ($\mu\text{g m}^{-3}$) for the condensation test case, as a function of size and composition: initial concentrations (**left**) and after 12 h of simulation (**right**).

3.4. Organic Aerosol Formation

3.4.1. Formation of Condensable

After emission into the atmosphere, the oxidation of VOCs leads to less volatile compounds than the precursors. They may condense onto particles and contribute to the increase of particle mass.

To illustrate the variety of precursors and the influence of oxidation, ageing experiments of exhaust emissions from a Euro 5 gasoline car are compared to the chamber measurements [58], where the total hydrocarbon mass (THC) as well as organic aerosol (OA) concentrations were monitored. Following Sartelet et al. [59], THC is assumed to be the sum of VOC and I/S VOCs (intermediate and semi-volatile VOCs). THC is initialised as measured in the experiments of [58] before lights-on (1.4 ppmv + 0.9 ppmv of propene). IVOCs are estimated from VOC emissions using a ratio of 0.17 [60], and NOx concentrations are initialised such as having a VOC/NOx ratio equal to 5.6 [58]. The speciation of VOCs to model species was done following Theloke and Friedrich [61]. Not only condensation/evaporation is considered but also gaseous chemistry. As in the experiment corrected for wall loss, after 5 h, the concentrations of particles is about $200 \mu\text{g m}^{-3}$. More than half of the mass originates from the condensation/evaporation of aged I/S VOCs, as shown in the left panel of Figure 9.

An arbitrary low sulphate initial concentration of $0.1 \mu\text{g m}^{-3}$ was fixed in simulation presented above, and ammonia emissions were not considered. However, to reduce NOx emissions, ammonia may also be emitted by recent vehicles [62]. To illustrate the potential influence of NH_3 emission on secondary aerosol formation, the initial conditions of the test case above are modified to include NH_3 emissions, assumed to be 10% of NOx emissions [62]. As shown in Figure 9, this leads to a large increase in inorganic aerosol concentrations (from $0.1 \mu\text{g m}^{-3}$ to about $37 \mu\text{g m}^{-3}$).

Figure 9. Time evolution of organic and inorganic concentrations for the exhaust test case: without NH_3 emissions (**left**) and with NH_3 emissions (**right**).

3.4.2. Absorption into an Aqueous or an Organic Phase

The SOA compounds formed from the exhaust are assumed to be mostly hydrophobic, and therefore condense onto an organic phase. SOA compounds formed from biogenic precursors have a stronger affinity with water [19,43], and they may prefer condensing onto an aqueous phase, formed by hydrophilic organic compounds and water absorbed by inorganics and hydrophilic organic compounds [42]. In the Mediterranean, at a remote site next to the sea, Chrit et al. [20] showed that about 64% of organic carbon is soluble, with a good agreement between SOAP and the measurements. To illustrate the influence of hygroscopicity, the exhaust test case of the previous section is simulated by adding $150 \mu\text{g m}^{-3}$ of isoprene. In the case when NH_3 is not emitted in the exhaust, biogenic condensables are formed but mostly stay in the gas phase, because they are mostly hydrophilic and they can not condense efficiently on the hydrophobic particles formed from the exhaust emission. As shown in Figure 10, if NH_3 is added to the exhaust, inorganic aerosol concentrations largely increase, leading to an increase in isoprene SOA, which can then condense onto aqueous particles.

Figure 10. Time evolution of isoprene SOA in the particle phase.

3.4.3. Ideality

In the previous test case (Section 3.4.2), the influence of activity coefficients on the SOA formation is not taken into account. Depending on the user's choice, short-range or short, medium and long-range activity coefficients can be modelled. If only short-range activity coefficients (interactions between

uncharged molecules) are modelled, then they are computed using the UNIQUAC Functional-group Activity Coefficients (UNIFAC) thermodynamic model [63], which is based on a functional group method. If short, medium and long-range activity coefficients are modelled, i.e., taking into account the influence of inorganic ions in the SOA aqueous phase, they are computed using the Aerosol Inorganic–Organic Mixtures Functional groups Activity Coefficients (AIOMFAC) model [64]. As already shown in the 3D studies in [19,42], and as shown here in Figure 10 for isoprene SOA, ideality strongly influences the partitioning between the gas and particle phase.

3.5. Nucleation and Coupling between Processes

The smallest particles are formed by the aggregation of gaseous molecules leading to thermodynamically stable clusters. The mechanism is poorly known and with large uncertainties [65]. Different schemes are implemented in SSH-aerosol: homogeneous binary nucleation of sulphate and water [66] and ternary nucleation of sulphuric acid–ammonia–water [67–69].

To assess the ability of SSH-aerosol to deal with simultaneous strong coagulation and condensation/nucleation, a nucleation test case similar to that presented in [14] is simulated. The initial distribution is the same as in the condensation of sulphuric acid test case of Section 3.1. It corresponds to the hazy conditions of [49]. The sulphuric acid production rate is $0.825 \mu\text{g m}^{-3} \text{h}^{-1}$, the temperature is 288.15 K and the relative humidity is 60%. The particles are initially assumed to be made of 70% sulphate and 30% of ammonium. The initial gas phase ammonia concentration is taken to be $8 \mu\text{g m}^{-3}$. The concentrations of gas phase ammonia and particulate-phase ammonium evolve with time due to both nucleation and condensation/evaporation. The ternary nucleation of Napari et al. [67] is used, but to avoid artificially large nucleation rates in the parameterisation of Napari et al. [67], a maximum nucleation rate of $1 \times 10^6 \text{ \# particles cm}^{-3}$ is set. The simulation is run for 1 h with output every 60 s.

Ultra-fine particles grow under the combined effect of coagulation, condensation of sulphate and nucleation. As shown in Figure 11, the nucleated particles clearly grow to larger particles with time. This growth can be accelerated by the presence low-volatility compounds, as shown in [70], underlying the importance of an accurate modelling of the formation of ELVOCs for the growth of ultra-fine particles. The simulation of Figure 11 is redone by adding $1 \mu\text{g m}^{-3}$ of a SSH-aerosol surrogate, Monomer, which is an ELVOC formed from the oxidation of terpenes. The comparison of the number concentration simulated with and without taking the surrogate Monomer into account shows that the particles have grown to larger diameters because of the presence of Monomer. The left panel of Figure 12 shows the time evolution of the number concentration for the different size sections without Monomer and the right panel of Figure 12 shows the same time evolution but with $1 \mu\text{g m}^{-3}$ of the surrogate Monomer condensing. The surrogate Monomer first condenses to existing particles around $0.01 \mu\text{m}$, making them grow to larger diameters.

In the simulations presented above, the condensation of the surrogate Monomer and sulphate is computed dynamically, simultaneously to coagulation and nucleation. The simultaneous computation of nucleation and condensation of sulphate is important, because they are competing processes. The combined effect of condensation and coagulation leads to a quick growth of particle around $0.01 \mu\text{m}$. Note that the coupling between condensation of low-volatility compounds, such as Monomer, and coagulation is crucial to correctly represent the growth of ultra-fine particles. As shown in Figure 11, the growth of ultra-fine particles is not well modelled if coagulation and the condensation of the species Monomer are not solved simultaneously, for example if the condensation of the surrogate Monomer is solved, as in the bulk equilibrium approach, after coagulation every output time step (60 s here).

Figure 11. Nucleation test case. Number (left) and volume (right) concentrations. The initial concentrations are in blue; the simulated concentrations without Monomer are in orange and with Monomer in green. The simulated concentrations with Monomer but solving condensation after coagulation every 60 s are in red.

Figure 12. Time evolution of the number distribution ($\# \text{ m}^{-3}$) for the different size sections, without Monomer (left) and with Monomer (right).

4. Discussion

The SSH-aerosol model is based on the coupling of three state-of-the-art modules (SCRAM, SOAP and H_2O), considering processes that are often ignored in the representation of aerosols in air-quality and climate models due to their complexities. As an illustration of the use of SSH-aerosol in 3D, it is coupled to the chemistry-transport model Polair3D of the Polyphemus air-quality platform [71], and a simulation over Europe is performed (see Appendix C).

Each of the state-of-the-art module of SSH-aerosol has previously been used separately in 3D simulations with chemistry-transport models. SCRAM was used in the first numerical studies showing that, in agreement with measurements, a large fraction of particles is not mixed in cities, with a mixing-state index of about 60% in Paris in summer [30,72]. The authors also showed that the mixing state influences not only secondary inorganic aerosol concentrations, but also the particle optical properties and the formation of cloud condensation nuclei. Further work is required for a more systemic use of this mixing-state representations in models. The mixing-state resolved representation may be used more widely over cities, or in climate models for black carbon to decrease the uncertainties linked to aerosol modelling.

Several publications modelled the SOA formation using SOAP and/or H_2O to study the relative importance of organic aerosol precursors [19–21,25,40–42,59,73–76]. They have been used for several pioneer studies: the influence of biogenic ELVOCs on SOA concentrations over Europe [20] and the impact of particle viscosity on SOA formation [42]. Further studies with a more accurate representation

of particle viscosity are now required. In the current version of the SSH-aerosol model, the surrogate approach is used to model the formation of condensable. Note that other approaches may be used, such as the Volatility Basis Set approach (VBS) [35,77], by modifying the properties of the organic species in the input file and by modifying the gas-phase reactions in the chemical preprocessor used. For example, the H₂O mechanism was modified by using a VBS approach to represent the ageing of intermediate volatile organic compounds [21,38,41], aromatics and monoterpenes based on the explicit mechanism of the model GECKO-A (Generator for Explicit Chemistry and Kinetics of Organics in the Atmosphere) [38]. The implementation of VBS approaches in SSH-aerosol will be done in future versions. Further work will also consist in improving the surrogate representation of organics by considering more surrogate compounds to better represent the organic properties of particles.

Because all aspects of aerosol formation are taken into account in SSH-aerosol, the use of the three modules jointly offers new research perspectives. For example, although previous studies focus on the influence of the mixing state on inorganic aerosols, the influence of the mixing state on SOA formation may now be assessed thanks to the coupling between SCRAM and SOAP.

The SSH-aerosol model may be used by itself for comparisons to chamber measurements, as in the ageing experiment of car emissions described here, and to assess the potential role of aerosol processes or newly emitted pollutants in aerosol formation. For example, the potential role of ammonia in aerosol formation from tailpipe emissions and the potential role of ELVOC in the growth of ultra-fine particles were shown in the test cases presented here.

The SSH-aerosol model may be implemented in 3D models of different scales, choosing the complexity depending on the scale of the model. Although the complexity may be chosen depending on the scale, using the same representation of aerosols across scales is crucial to improve downscaling.

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Conflicts of Interest: The authors declare no conflict of interest.

Appendix A. Code Metadata

Table A1. Code metadata.

Current code version	v1.1
Link to code/repository	https://github.com/sshaerosol/ssh-aerosol
Legal Code License	GNU license v3
Software code languages	C++, FORTRAN and python for visualisation
Link to manual	https://github.com/sshaerosol/ssh-aerosol/blob/master/user_manual
Support email for questions	ssh-aerosol-help@lists.enpc.fr

Appendix B. Aerosol Surrogates

The organic aerosol surrogates are detailed in Table A2.

Table A2. Characteristic of the surrogates for aerosol organic species: abbreviation of the surrogate type: Type A, hydrophilic; Type B, hydrophobic; Type C, hydrophobic non-volatile and not used to compute activity coefficients. Molecular structure, molecular weight MW ($\text{g}\cdot\text{mol}^{-1}$), OM/OC ratio r , Henry's law constant H ($\times 10^8 \text{ M/atm}$), partitioning constant K_p ($\text{m}^3 \mu\text{g}^{-1}$) for an ideal organic phase of molar mass 200 g/mol at 298 K , enthalpy of vaporization ($\text{kJ}\cdot\text{mol}^{-1}$), and precursors. The abbreviation n.v. means non volatile.

Surrogate	Type	Molecular Structure	MW	r	H	K_p	ΔH_{vap}	Precursor
BiMT	A	methyl tetrol	136	2.3	330	0.064	38	isoprene
BiPER	A	methyl dihydroxy dihydroperoxide	168	2.8	81	0.036	38	
BiDER	A	methyl tetrol	136	2.3	891	0.227	38	
BiMGA	A	methyl glyceric acid (MGA)	120	2.5	5.3	0.007	43	
BiNGA	B	nitrate derivative of MGA	165	3.5	0.4	0.007	43	
BiNIT3	B	methyl hydroxy trinitrate butane	272	4.6	0.4	0.064	38	
BiA0D	A	pinonaldehyde	168	1.4	0.02	0.0003	50	mono-terpenes
BiA1D	A	norpinic acid	170	1.5	1.12	0.428	50	
BiA2D	A	pinic acid	186	1.7	2.7	0.650	109	
BiA3D	B	3-methyl-1,2,3-butane tricarboxylic acid	204	2.1	-	n.v.	-	
BiNIT	B	Nitrooxy-limonene-ol	215	1.8	0.02	0.037	50	
Monomer	C	$\text{C}_{10}\text{H}_{14}\text{O}_9$	278	2.3	-	n. v.	-	
Dimer	C	$\text{C}_{19}\text{H}_{28}\text{O}_{11}$	432	1.9	-	n. v.	-	sesqui-terpenes
BiBIP	B	C15 hydroxy nitrate aldehyde	298	1.7	2.34	154.9	175	
BiBmP	B	C15 oxo aldehyde	236	1.3	-	0.309	175	
AnBIP	B	methyl nitro benzoic acid	167	2	2.48	1.37	50	xylenes and toluene
AnBmP	B	methyl hydroxy benzoic acid	152	1.6	12.4	0.011	50	
AnCIP	C	No structure	167	2	-	n. v.	-	
ACIDMAL	A	maleylacetic acid	158	2.2	8685	2.02	50	phenol catechol benzene
DHMB	A	dihydroxymethyl benzoquinone	154	1.8	36.2	0.026	50	methyl-catechol cresol
PSYR	A	$\text{C}_8\text{H}_{10}\text{O}_5$	186	1.9	14.5	0.0123	50	syringol
GHDPerox	A	SOA (hydroperoxide)	174	2.1	63.3	0.171	50	guaiacol
PAHIN	A	dihydroxytere	198	2.1	n. v.	-	-	naphtalene
	A	phthalic acid	166	1.7	14.9	0.093	50	methyl-PAHhN naphtalene
POAIP	B	primary OA of low volatility	280	1.3	-	1.1	106	-
POAmP	B	primary OA of medium volatility	280	1.3	-	0.0116	91	-
POAhP	B	primary OA of high volatility	280	1.3	-	0.00031	79	-
SOAIP	C	secondary OA of low volatility	392	1.8	-	110	106	POAIP
SOAmP	B	secondary OA of medium volatility	392	1.8	-	1.16	91	POAmP
SOAhP	B	secondary OA of high volatility	392	1.8	-	0.031	79	POAhP

Appendix C. Example of a 3D Simulation by Coupling to a CTM

Although the three modules of SSH-aerosol (SCRAM, SOAP and H²O) have already been used separately in 3D CTMs [19–21,25,30,40–42,59,72–76,78] for different applications, they have never been used jointly. The SSH-model is coupled to the CTM Polair3D of the Polyphemus air-quality platform for evaluation. A simulation over Europe is performed between 1 June 2012 and 30 August 2012 using the CTM input data (emissions, boundary conditions and meteorology) detailed in [42]. As in [42], aerosols are assumed to be internally mixed, and the size distribution is discretised with five sections between 0.01 and 10 μm . Coagulation and condensation/evaporation are taken into account. Bulk equilibrium is assumed, and activity coefficients are computed using UNIFAC. Figure A1 shows a map of organic matter concentrations in PM₁ (OM₁) and the location of the stations where model to measurement comparisons are performed.

Table A3 compares model and measurement concentrations of organic carbon in PM_{2.5} (OC_{2.5}). The measurements were measured by high and low volume samplers at ACTRIS (European Research Infrastructure for the observation of Aerosol, Clouds and Trace Gases) stations, as detailed in the EBAS database [79]. OC is computed by dividing the simulated OM concentrations of each surrogate by the OM/OC ratio of the surrogate, as described in [19]. The concentrations of organics OM₁ are also compared to measurements performed using ACSMs (Aerodyne Aerosol Chemical Speciation Monitor) in Table A3. As shown in Table A3, the simulated concentrations of OC_{2.5} and OM₁ compare well to measurements, with a mean fractional error MFE below 75% and a mean fractional bias MFB below 60%, satisfying the performance evaluation criteria of Boylan and Russell [80] at each station. Furthermore, the error MFE satisfies the most strict goal evaluation criteria of Boylan and Russell [80] (MFE below 50%) at each station, and both the error MFE and the bias MFB satisfy the most strict goal evaluation criteria of Boylan and Russell [80] (MFE below 50% and MFB below 30%) on average over the stations.

For inorganic compounds of particles, Table A4 compares model and measured concentrations of sulphate (SO_{4,1}), nitrate (NO_{3,1}) and ammonium (NH_{4,1}) concentrations in PM₁. As for OM₁, the measurements were performed using ACSMs. The performance evaluation criteria are verified at each station for SO_{4,1} and the MFE satisfies the most strict goal evaluation criteria. The performance and goal evaluation criteria are both verified at each station for NO_{3,1} and NH_{4,1}, and on average over the stations for all particle compounds.

Table A3. Statistics (measured $\bar{o}$ and simulated $\bar{s}$ mean concentrations ($\mu\text{g m}^{-3}$), mean fractional error MFE (%) and mean fractional bias MFB (%)) of comparisons to measurements for daily concentrations of OC_{2.5} (OC₁₀ at Aspvreten) and OM₁ when available.

	OC _{2.5}				OM ₁			
	$\bar{o}$	$\bar{s}$	MFE	MFB	$\bar{o}$	$\bar{s}$	MFE	MFB
Montseny	2.4	3.1	33	22	7.6	4.9	46	−41
Melpitz	1.4	1.9	34	26	3.8	2.9	33	−24
Cabauw	–	–	–	–	2.9	2.7	21	0
Košetice	2.4	2.6	30	−5	–	–	–	–
Ispra	2.8	4.6	50	49	–	–	–	–
Aspvreten	2.2	1.6	40	−36	–	–	–	–
Average	2.2	2.8	38	11	4.8	3.5	33	−22

Table A4. Statistics (measured $\bar{o}$ and simulated $\bar{s}$ mean concentrations ($\mu\text{g m}^{-3}$), mean fractional error MFE (%) and mean fractional bias MFB (%)) of comparisons to measurements for daily concentrations of $\text{SO}_{4,1}$ and $\text{NH}_{4,1}$ and $\text{NO}_{3,1}$.

	$\text{SO}_{4,1}$				$\text{NH}_{4,1}$				$\text{NO}_{3,1}$			
	$\bar{o}$	$\bar{s}$	MFE	MFB	$\bar{o}$	$\bar{s}$	MFE	MFB	$\bar{o}$	$\bar{s}$	MFE	MFB
Montseny	2.5	1.7	41	−35	1.1	0.8	36	−30	0.6	0.6	51	0
Melpitz	1.6	1.1	46	−43	0.7	0.6	30	−11	0.8	0.7	47	−16
Cabauw	0.9	1.1	26	19	1.0	1.3	36	24	2.9	3.2	51	27
Average	1.7	1.3	38	−20	0.9	0.9	34	−6	1.4	1.5	49	4

Figure A1. Map of OM_1 concentrations ($\mu\text{g m}^{-3}$) averaged between 1 June 2012 and 30 August 2012.

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