

# Utilizing Novel Lignocellulosic Material from Hart's-Tongue Fern (*Asplenium scolopendrium*) Leaves for Crystal Violet Adsorption: Characterization, Application, and Optimization

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**Table S1.** The non-linear equations of the adsorption isotherms and kinetic models used to assess the adsorption process.

Adsorption isotherm	Equation
Langmuir isotherm	$q_e = \frac{q_m \cdot K_L \cdot C_e}{1 + K_L \cdot C_e}$
Freundlich isotherm	$q_e = K_F \cdot C_e^{1/n_F}$
Temkin isotherm	$q_e = \frac{R \cdot T}{b} \cdot \ln(K_T \cdot C_e)$
Sips isotherm	$q_e = \frac{Q_{sat} \cdot K_S \cdot C_e^n}{1 + K_S \cdot C_e^n}$
Redlich-Peterson isotherm	$q_e = \frac{K_{RP} \cdot C_e}{1 + a_{RP} \cdot C_e^{\beta_{RP}}}$
Kinetic model	Equation
Pseudo-first-order kinetic model	$q_t = q_e (1 - \exp^{-k_1 \cdot t})$
Pseudo-second-order kinetic model	$q_t = \frac{k_2 \cdot t \cdot q_e^2}{1 + k_2 \cdot t \cdot q_e}$
Elovich kinetic model	$q_t = \frac{1}{a} \ln(1 + a \cdot b \cdot t)$
Avrami kinetic model	$q_t = q_{AV} [1 - \exp(-k_{AV} \cdot t)^{n_{AV}}]$
General order kinetic model	$q_t = q_n - \frac{q_n}{[k_n \cdot (q_n)^{n-1} \cdot t \cdot (n-1) + 1]^{1/1-n}}$

where:

-  $q_m$  and  $Q_{sat}$  are the maximum absorption capacities;  $K_L$ ,  $K_F$ ,  $K_T$ ,  $K_S$  and  $K_{RP}$  are the Langmuir, Freundlich, Temkin, Sips and Redlich-Peterson isotherms constants;  $1/n_F$  is an empirical constant indicating the intensity of adsorption;  $R$  is the universal gas constant;  $T$  is the absolute temperature;  $b$  is Temkin constant which related to the adsorption heat;  $n$  is Sips isotherm exponent;  $a_{RP}$  is Redlich-Peterson isotherm constant and  $\beta_{RP}$  is Redlich-Peterson exponent which can vary between 0 and 1.

-  $q_t$  is the dye amount adsorbed at time  $t$ ;  $k_1$ ,  $k_2$ ,  $k_n$  and  $k_{AV}$  are the rate constants of pseudo-first-order, pseudo-second-order, general order and Avrami kinetic models;  $q_e$ ,  $q_n$  and  $q_{AV}$  are the theoretical values for the adsorption capacity;  $a$  is the desorption constant of

Elovich model;  $b$  is the initial velocity;  $n$  is the general order exponent and  $n_{AV}$  is a fractional exponent.

**Table S2.** The calculation equations for error parameters  $R^2$ ,  $\chi^2$ , SSE and ARE.

Function name	Equation
Determination coefficient ( $R^2$ )	$R^2 = 1 - \frac{\sum_{i=1}^n (y_{i,exp} - y_{i,mod})^2}{\sum_{i=1}^n (y_{i,exp} - \overline{y_{i,exp}})^2}$
Sum of square error (SSE)	$SSE = \sum_{i=1}^n (y_{i,exp} - y_{i,mod})^2$
Chi-square ( $\chi^2$ )	$\chi^2 = \sum_{i=1}^n \frac{(y_{i,exp} - y_{i,mod})^2}{y_{i,mod}}$
Average relative error (ARE)	$ARE = \frac{100}{n} \sum_{i=1}^n \left  \frac{y_{i,exp} - y_{i,mod}}{y_{i,mod}} \right $

where:  $y_{i,exp}$  is the experimental value;  $y_{i,mod}$  is the modeled value;  $\overline{y_{i,exp}}$  is the mean values and  $n$  is the total amount of information.

**Table S3.** The equations of specific thermodynamic parameters.

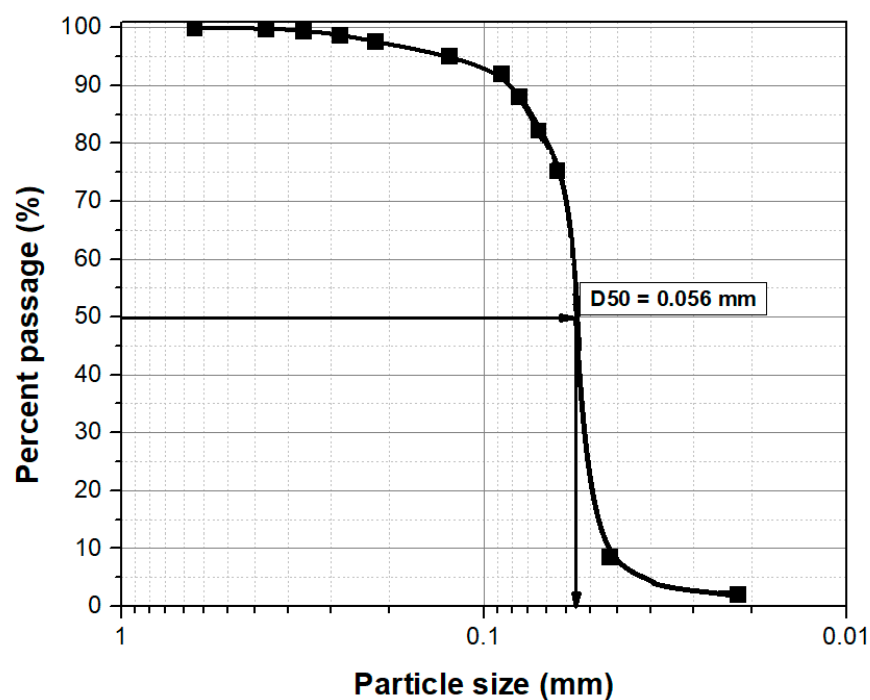
Thermodynamic parameters	Equation
Standard Gibbs free energy change	$\Delta G^0 = -RT \ln K_L$
Standard enthalpy change	$\ln K_L = \frac{\Delta S^0}{R} - \frac{\Delta H^0}{RT}$
Standard entropy change	

where:  $R$  represents the universal gas constant;  $K_L$  represents the Langmuir constant,  $T$  represents the absolute temperature.

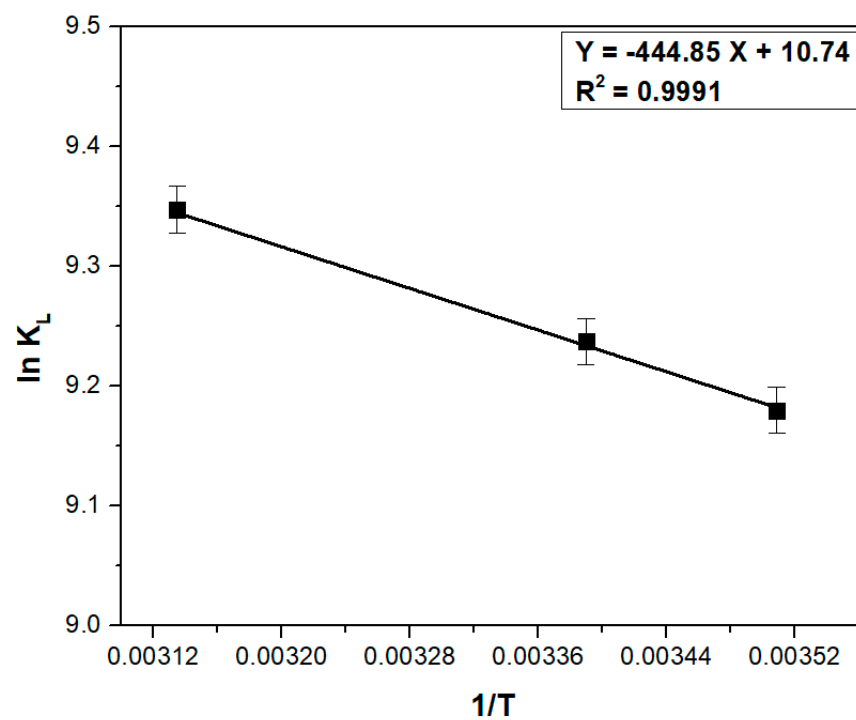
**Table S4.** The equation used to calculate the desorption efficiency

Desorption efficiency equation
$D(\%) = \frac{m_d}{m_a} \cdot 100$

where:  $m_d$  is the crystal violet amount liberated by the desorbing agent,  $m_a$  is the crystal violet amount adsorbed on the adsorbent material.



**Figure S1.** The particle size distribution of hart's-tongue fern (*Asplenium scolopendrium*) leaves powder



**Figure S2.** Plot of  $\ln K_L$  vs.  $1/T$  for the dye adsorption onto hart's-tongue fern (*Asplenium scolopendrium*) leaves powder