

Supporting Information

A Complexed Initiating System AlCl₃·Phenetole/TiCl₄·H₂O with Dominant Synergistic Effect for Efficient Synthesis of High Molecular Weight Polyisobutylene

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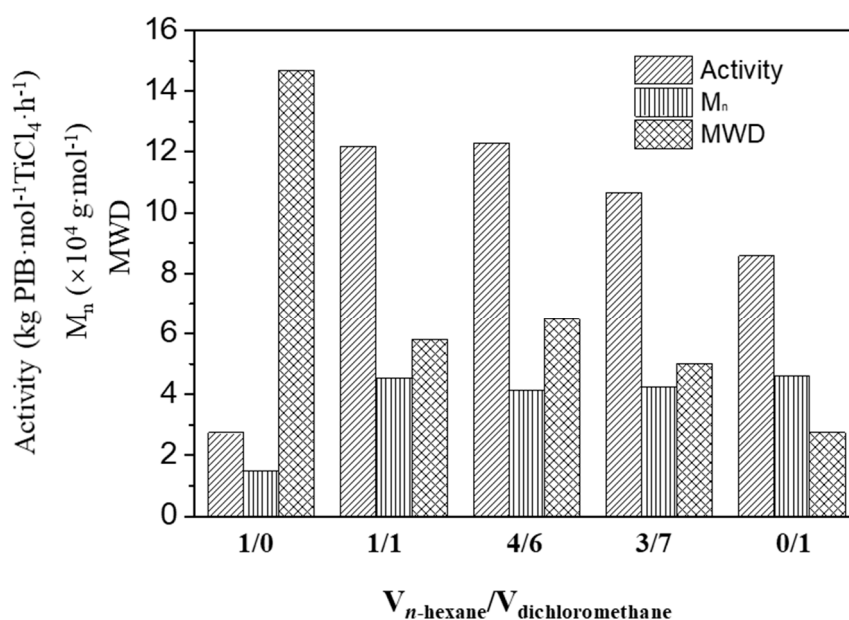


Figure S1. The effect of solvent polarity on TiCl₄/H₂O for IB polymerization ([IB] = 2.9 mol·L⁻¹; [H₂O] = 20 mmol·L⁻¹; [TiCl₄] = 30 mmol·L⁻¹; t_p=30 min; T_p = -60 °C.).

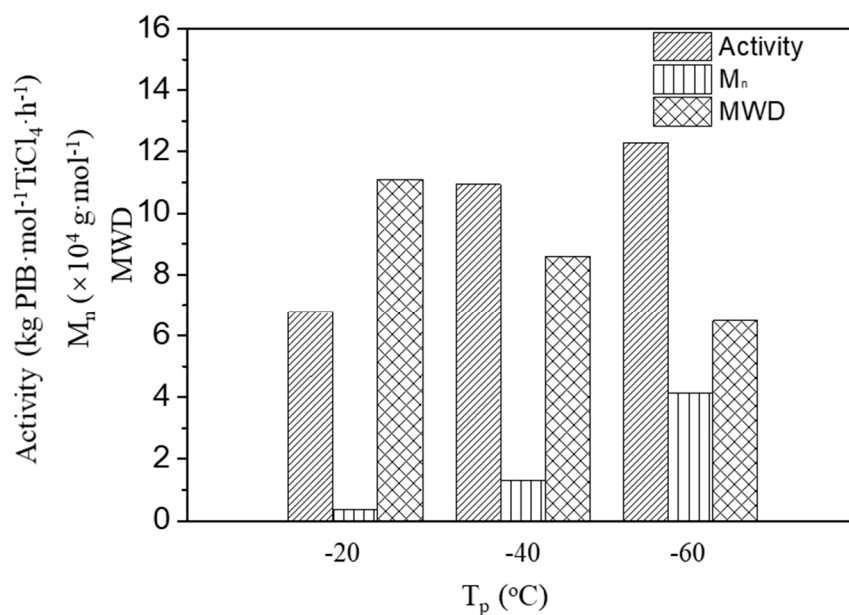


Figure S2. The effect of T_p on $\text{TiCl}_4/\text{H}_2\text{O}$ for IB polymerization ($[\text{IB}] = 2.9 \text{ mol}\cdot\text{L}^{-1}$; $[\text{H}_2\text{O}] = 20 \text{ mmol}\cdot\text{L}^{-1}$; $[\text{TiCl}_4] = 30 \text{ mmol}\cdot\text{L}^{-1}$; 60 mL $\text{C}_2\text{H}_2\text{Cl}_2$; 40 mL n-hexane; $t_p = 30 \text{ min}$)

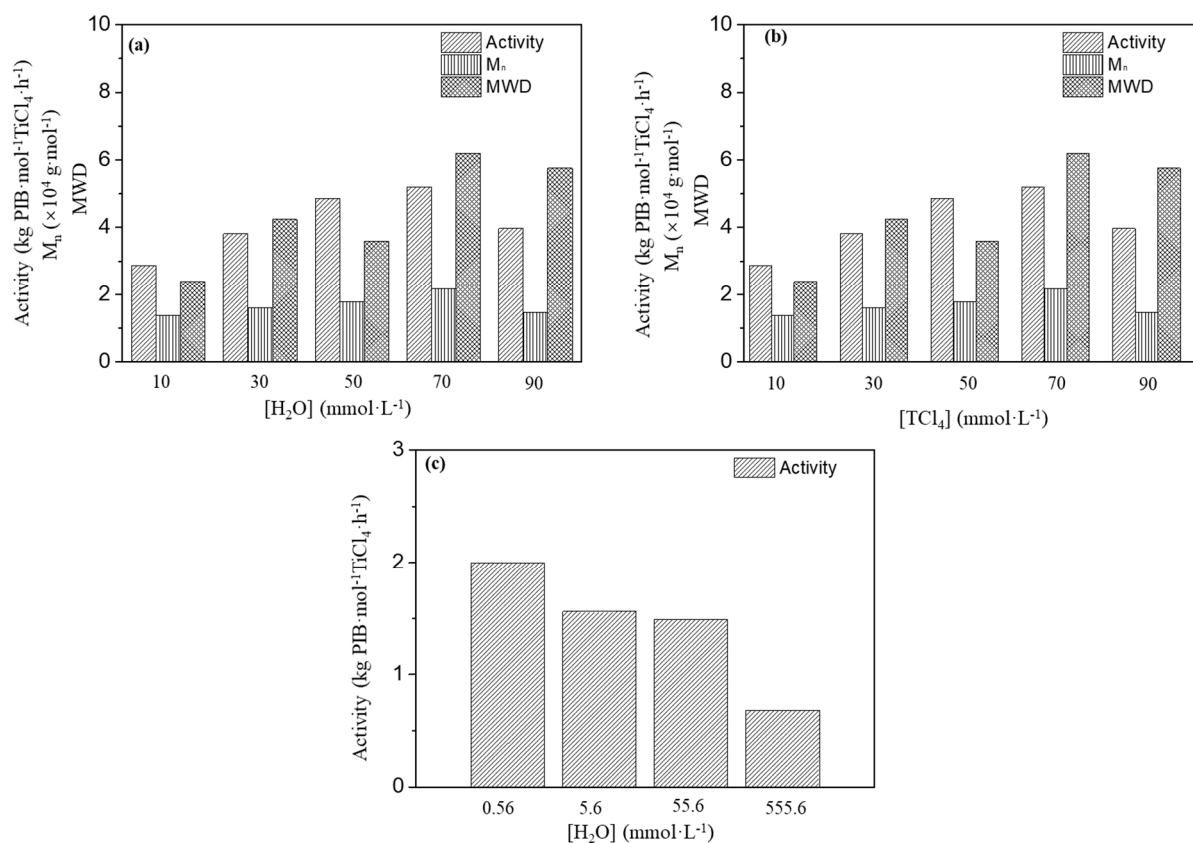


Figure S3. The effect of $[\text{H}_2\text{O}]$ and $[\text{TiCl}_4]$ on IB polymerization ((a) $[\text{TiCl}_4] = 50 \text{ mmol}\cdot\text{L}^{-1}$; (b) $[\text{H}_2\text{O}] = 40 \text{ mmol}\cdot\text{L}^{-1}$; (c) $[\text{TiCl}_4] = 4.56 \text{ mmol}\cdot\text{L}^{-1}$; Other conditions: $[\text{IB}] = 2.9 \text{ mol}\cdot\text{L}^{-1}$; 60 mL $\text{C}_2\text{H}_2\text{Cl}_2$; 40 mL n-hexane; $t_p = 30 \text{ min}$; $T_p = -60^\circ\text{C}$).

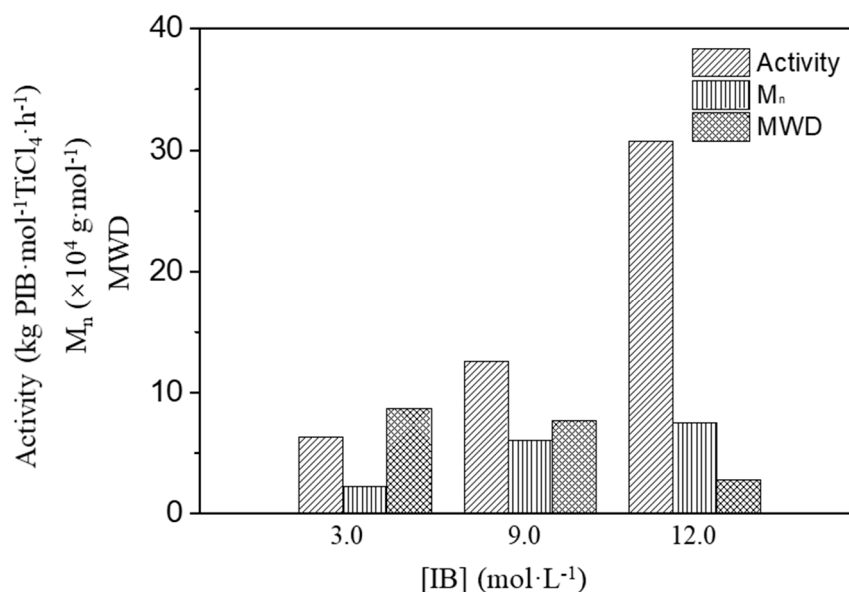


Figure S4. The effect of monomer concentration on $\text{TiCl}_4/\text{H}_2\text{O}$ for IB polymerization ($[\text{H}_2\text{O}] = 30 \text{ mmol}\cdot\text{L}^{-1}$; $[\text{TiCl}_4] = 20 \text{ mmol}\cdot\text{L}^{-1}$; 60 mL $\text{C}_2\text{H}_2\text{Cl}_2$; 40 mL n-hexane; $t_p = 30 \text{ min}$; $T_p = -60^\circ\text{C}$).

The effect of various reaction conditions on the polymerization behaviors of $\text{TiCl}_4/\text{H}_2\text{O}$ were investigated as well (see **Figure S1-S4**). The results indicated that $\text{TiCl}_4/\text{H}_2\text{O}$ was good at producing high or medium molecular weight polyisobutylene with $M_n = 1\sim 6 \times 10^4 \text{ g}\cdot\text{mol}^{-1}$ and the MWD of the polymer was relatively broad. In addition, this initiating system showed low efficiency, and activity $\approx 10 \text{ kg PIB}\cdot\text{mol}^{-1}\text{TiCl}_4\cdot\text{h}^{-1}$ could be observed in most cases, thus a much higher catalyst concentration was needed to achieve a reasonable monomer conversion. This was also in accordance with the reported work that the dimer of TiCl_4 was the active coinitiator for cationic polymerization, and a relatively high concentration of TiCl_4 was needed for achieving reasonable polymerization rate [S1].

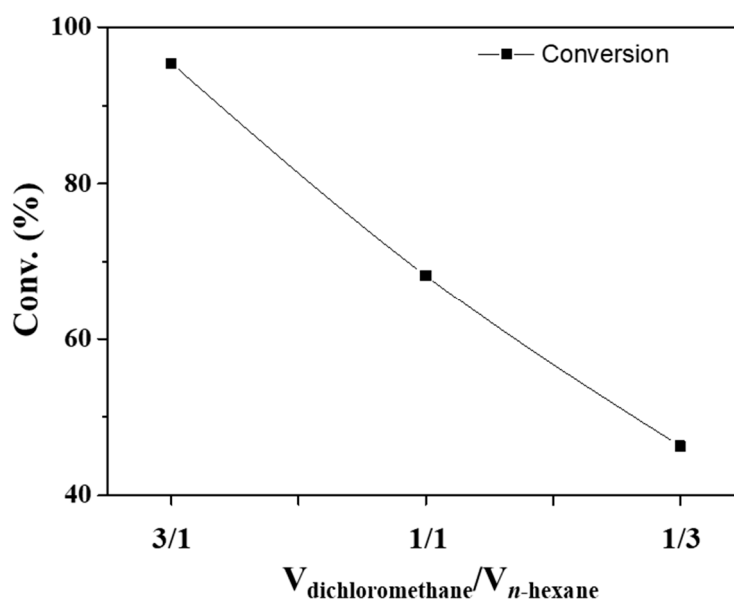


Figure S5. The effect of solvent polarity on monomer conversion with $\text{AlCl}_3/\text{phenetole}$ initiating system ($[\text{IB}] = 4 \text{ mol}\cdot\text{L}^{-1}$; $V_{\text{dichloromethane}} + V_{\text{n-hexane}} = 100 \text{ mL}$; $T_p = -60^\circ\text{C}$; $t_p = 30 \text{ min}$; $[\text{AlCl}_3]/[\text{phenetole}] = 1/1$).

According to **Figure S5**, a relatively stronger polarity of the solvent was more favored by the AlCl_3 /phenetole initiating system to achieve high monomer conversion, as more polar conditions could possibly help to produce more active ion pairs for IB polymerization ^[S2].

References

[S1] M. Tawada, R. Faust. *Macromolecules* **2005**, *38*, 4989.

[S2] L. Sipos, P. De, R. Faust. *Macromolecules* **2003**, *36*, 8282.



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