

Article

Application of Photocatalysts and LED Light Sources in Drinking Water Treatment

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Abstract: This study investigates a cross-section of TiO_2 compositions for which existing evidence suggests the prospect of improved performance compared to standard Degussa P25. In the context of a program aimed toward a 365 nm LED based photo-reactor, the question is whether a distinctly superior photocatalyst composition for drinking water treatment is now available that would shape design choices. An answer was sought by synthesizing several photocatalysts with reported high reactivity in some context in the literature, and by performing photocatalysts reactivity tests using common pollutants of water system including Natural Organic Matter (NOM) and Emerging Contaminants (ECs) from the pesticide and pharmaceutical classes. 365 nm Light Emitting Diodes (LEDs) were used as the irradiation source. Since LEDs are now available in the UV, we did not examine the TiO₂ modifications that bring band gap excitation into the region beyond 400 nm. The results suggest that the choice of the photocatalyst should be best made to fit the reactor design and photocatalyst composition overall, superior for all classes emerged.

Keywords: photocatalyst; Light Emitting Diodes; fulvic acids; emerging contaminants

1. Introduction

There is lively current interest in the prospects for implementation of Advanced Oxidation Processes (AOPs) for water treatment [1,2]. AOPs refer to processes like electrochemical, ultrasound, UV/O₃, UV/H₂O₂, Fenton and photo Fenton processes, photocatalysis, *etc.* The focus of this study is on moving towards TiO₂ photocatalysts with UV- LED light sources. LED light sources, beyond being a reliable and continuous source (unlike solar), are inexpensive and promise high current-to-light conversion efficiency, with little heating (more efficient than many conventional mercury discharge lamps). DC operation could also be readily adapted to solar photovoltaic battery off-grid power.

Along with demonstrating UVA (as found in current LED light sources) this work is aimed at selecting among well characterized and readily prepared photocatalysts of reported high reactivity in at least one context (Table 1 in the Appendix lists some of the synthesized photocatalysts reported in the literature - mostly rare earth doped TiO_2 - and the model compounds used for the reactivity test). The results and discussion section opens with an account of selection of candidate photocatalysts.

So far, UV LED light sources along with TiO_2 photocatalysts (mostly Degussa P25) have been successfully used for degradation of dyes like Methylene Blue, Rhodamine B and Congo Red in aqueous medium [3–6]. Degradation of airborne 2-propanol, trichloroethylene, dimethyl sulfide and perchloroethylene has also been studied in gas phase [7–10]. Ghosh *et al.* in 2009 used visible LEDs (436 nm) for sensitized degradation of 4-chlolophenol (4-CP) using cumorine dye along with TiO_2 nanofibers, tin-doped TiO₂ nanofibers as well as Degussa P25 [11,12].

This work is a precursor to design a reactor for small and/or remote water systems. One typical requirement for the small systems is simplicity, with a minimum number of treatment steps. Photocatalysis with TiO_2 is a broad gage treatment technique. Especially in the case of small systems, a single barrier approach is used and simple chlorination deals only with pathogens and creates a DBP problem. The broad applicability of UV photocatalysis offers hope for more comprehensive treatment. There is a growing literature on UVA-LED photocatalysis, but little of it has addressed environmental applications. Therefore, a contemporary statement of the problem faced by small systems would focus on three issues in the common order of priority: pathogens, disinfection by products (DPBs), and emerging micro-pollutants (arising from pesticides, pharmaceutical and personal care products). The first two are already being regulated and ECs may soon be regulated. Literature reviews document the broad spectrum capability of TiO_2 photocatalysis to destroy microbes [13,14]. Thus, in this paper, representatives from the DBPs precursor Natural Organic Matter (Suwannee River Fulvic Acids-SRFA) and from ECs (4-CP & sulfamethoxazole) were selected.

2. Results and Discussion

2.1. Selection of Potential Photocatalyst Compositions and Reactivity Evaluation

Selection of appropriate photocatalyst compositions requires one to consider factors influencing the performance of photocatalysts. These factors are subtle and complex, but in broad terms they can be divided into (a) issues of efficient delivery of the targets to the photocatalyst's surface and (b) target species reactivity on the surface. A key factor in delivery to the surface is adsorption on the surface, which relates to some specific interaction possibilities (e.g., chemisorption), point of zero charge and

surface areas. Increasing the surface area of the photocatalysts results in increased both equilibrium and dynamic rates [15]. This calls for inclusion of preparations of nanotubes and wires or to mesoporous structures, all affording a high surface area. Another factor in reactivity on the surface is hole-electron recombination. It is argued that the success of P25 arises from the effect of the mixture of anatase and rutile phases, which reduces the recombination rate [16]. Recent research on nanoparticles of second oxides on TiO₂ shows efficient separation of the hole and electron and delay of recombination. This even allows post-irradiation energy storage [17,18]. Existence of anatase and rutile phases, primary particle size and secondary particle size are other physical and structural properties, which affect the photocatalytic activities [19].

A review of literature suggested the following photocatalysts reported to have advantages such as outperforming Degussa P25 in at least one case: (a) mesoporous TiO_2 and TiO_2 nanofibers, which are reported to have large surface area [20,21]; (b) rare earths doped TiO_2 , to increases the separation efficiencies of electron and hole pairs and modifying the microstructure of the photocatalyst [22], and (c) photocatalysts with energy storage capability (WO₃/TiO₂ and Ni(OH)₂/TiO₂). The electron storage capability of WO₃/TiO₂ extends lifetimes and as a consequence improves the interfacial transfer yield [18]. In contrast, surface coating with amorphous Ni(OH)₂, which is a hole trap, can enhance the substrate adsorption as well [17]. All tests were also performed using Degussa P25 as a reference. In so far as the major factors in choice of a photocatalyst preparation can be captured by taking surface area as a surrogate for delivery of substrate to the surface and modeling charge separation by modification of the structure or creating opportunity for electron (WO₃) or hole (Ni(OH)₂) inter phase transfer, this set should provide a reasonable guide to the issues (since the reaction in case of WO₃/TiO₂ was efficient at pH around 3, this photocatalyst was not tested in this paper).

In the selection process, we also considered opportunities for immobilization, because there are considerable simplifications of reactor design if the photocatalyst is on a robust fixed bed. In this case, photocatalyst particle separation is not required. We have tested mesoporous TiO_2 , which could be representatives of mesosponge TiO_2 prepared by anodization of titanium [5,23] and TiO_2 nanofibers, which can also be obtained by anodization and could also represent nanofibers grown on a surface such as glass [24].

Since water may contain several classes of contaminants, the reactivity of the photocatalysts was tested on models of priority classes of water pollutants. Three main issues in drinking water treatment systems are pathogens, disinfection by products (DPBs), and emerging micro-pollutants, for which the potential of TiO_2 photocatalysis (an alternate AOP) is especially promising. With respect to AOPs based on photocatalysis, an extensive literature on TiO_2 demonstrates that oxidation with holes or hydroxyl radical equivalents on the TiO_2 surface is an extremely powerful and versatile method of disinfection that has been recently reviewed [25,26]. Thus, we will not focus on testing a variety of catalysts over a variety of indicator organisms at this stage of UVA photocatalyst selection. The selection begins with the evaluation of candidate photocatalysts for degradation of the NOM model. NOM oxidation offers protection from DPB formation on the chlorination needed for the distribution system. Choices passing this test can then be evaluated for degradation of 4-CP as a challenging recalcitrant pesticide model and finally for sulfamethoxazole as an example of emerging pharmaceutical contaminants in water. This is consistent with Ryu and Choi's suggestion [27] to

perform multiple reactivity tests for a specific photocatalyst, since a single activity test shows only a limited part of the variable activity.

It should be mentioned that for the reactivity tests, though the best loading for each photocatalyst was verified, the same loading of photocatalysts was used for the comparison purposes. This was not necessarily the optimized loading for each case, but reflects the expectation that a treatment system would not be altered for each contaminant. The 2.5 g/L of photocatalysts used in this study was in the acceptable range for P25, TiO₂ nanofibers and Ni(OH)₂/TiO₂ but 5 g/L was the best loading for mesoporous TiO₂. The UV irradiation source is 365 nm LEDs.

2.2. Reduction of Natural Organic Matter (NOM) by UVA

In North America, almost universally, small systems rely on chlorine disinfection and residual chlorine for distribution system protection. Many do not include coagulation or filtration or NOM removal. Thus, DBPs (trihalomethanes or THMs and haloacetic acids or HAAs) formation (increasingly regulated) stands out. DBPs are the result of reactions between NOM and chlorine. Removal of the NOM before chlorination is a desirable barrier. There are two photocatalytic options for degradation of NOMs: degradation by "self sensitization" under visible light irradiation or degradation under UV irradiation. A detailed and comprehensive study on NOM self sensitization using Degussa P25 has been pursued in this laboratory [28,29], which provides the proof of concept of applicability of this method for degradation of FAs and NOM, leading to inhibition of formation of DBPs. We report UV degradation of FAs in this paper since UV will be required for the other contaminants.

As it was mentioned in the introduction, SRFA in raw water model was used as the NOM model. Reactivity of the following photocatalysts was tested for degradation of SRFA (by following the characteristic fluorescence under 350 nm excitation as a function of time) in solution: Nd and Eu doped TiO₂, Degussa P25, TiO₂ nanofibers, Ni(OH)₂/TiO₂ WO₃/TiO₂ and mesoporous TiO₂. Upon band gap irradiation of the photocatalysts, electrons are excited to the conduction bands of TiO₂ and leave highly oxidizing holes in valance band. In presence of NOM, these take part in a series of oxidative-reductive reactions, which includes electrons forming O_2^{--} and the powerful hole oxidant.

One of the critical factors in degradation of Fulvic Acids (FAs) is adsorption of FAs on the surface of the photocatalysts. Adsorption on the surface is strongly pH dependent with the optimum pH depending on surface properties, and the reactivity on the surface shows some pH dependence. Though the efficiency is higher at lower pHs, our goal here was to use the synthesized photocatalysts at natural water pH. Figure 1 shows dark adsorption of FAs on the chosen catalysts at pH around 6.7. For the same loading of photocatalysts (not necessarily optimal), mesoporous TiO₂ and Ni(OH)₂/TiO₂ are the best candidates. P25, TiO₂ nanofibers and Nd doped TiO₂ showed similar, lesser, adsorption efficiencies. The results for WO₃/TiO₂ are not reported here, because adsorption of FAs on the surface was not efficient, unless the pH was reduced to near 3. The narrow band near 400 nm in this and all fluorescence spectra below is a water Raman band with constant intensity serving as an internal intensity standard.

Figure 1. Dark adsorption of fulvic acids (FAs) (3 times diluted samples) on the surface of the selected photocatalysts (2.5 g/L) at pH = 6.7, indicated by reduction in fluorescence intensity. Fluorescence spectra were recorded for $\lambda_{\text{excitation}} = 350 \text{ nm}$ (3 times diluted samples).



Figure 2 presents a typical result upon irradiation in 365 nm LED reactor using TiO₂ nanofibres.

Figure 2. Degradation of FA (10 ppm) using TiO₂ nanofibers (2.5 g/L) in the 365 nm LED reactor, the fluorescence spectra were recorded for $\lambda_{\text{excitation}} = 350$ nm at different irradiation times. Irradiation times are converted to required energy per volume in (kJ/L) for the corresponding removal of FA shown on the *Y* axis.



Figure 3. Final fluorescence spectra (3 times diluted samples) for $\lambda_{\text{excitation}} = 350$ nm of 10 ppm FA solutions using 2.5 g/L of each photocatalyst after a light dose of 4.05 kJ/L (1 h) for runs in the 365 nm LED reactor (in case of Degussa P25, 2.25 kJ/L (0.5 h) was applied).



Figure 3 collects the final fluorescent spectra after a light dose of 4.05 kJ/L (2.25 kJ/L in case of Degussa P25) for a solution of 10 ppm FA after each individual of the seven photocatalysts was used for irradiation in the 365 nm LED reactor. The final curves imply essentially complete reaction to non-fluorescent products, except in the cases of Nd and Eu doped TiO₂, which show some remnant fluorescent photoproducts observed, even though the adsorption on the surface for rare earth doped TiO₂ is similar to that for P25 and TiO₂ nanofibers. It is possible that not all of the FA complex mixture's relevant components and oxidation intermediates are adsorbed on these surfaces. Also in the case of rare earth doped TiO₂, particle sizes are so small that recorded absorption spectra of the photocatalysts were as if the slurry was a homogeneous solution. Below the critical size, surface recombination becomes dominant, reducing efficiency [30]. Alternatively, it could be related to electron trapping properties of the dopants, if the energy level is too low to transfer electron efficiently and rapidly to oxygen [30].

2.3. Photocatalytic Degradation of Model Pesticide 4-CP under UVA Irradiation

Literature suggests that 4-CP is among the most recalcitrant pesticide related structures with respect to oxidation [31]. Mesoporous TiO₂, TiO₂ nanofibers, Ni(OH)₂/TiO₂ as well as P25 were compared for degradation of 4-CP in 365 nm LED reactor. The results are shown in Figure 4A. The first point in all graphs is the based on the concentration after 30 min dark time. Adsorption of 4-CP on photocatalysts surfaces was determined to be negligible except for Ni(OH)₂/P25, which was about 5%. Nd doped TiO₂, which is reported in the literature as the most efficient rare earth doped TiO₂ photocatalysts [32,33], was also tested for degradation of 4-CP under similar circumstances. The reaction rate was very close to that of TiO₂ nanofibers, but considering its poor performance on degradation of FA no more experiments were performed with this photocatalyst. In order to increase the efficiency of electron capture for the reactions, the photocatalysts were also tested under bubbling O₂ for degradation of 4-CP. O₂ is the electron acceptor and, increase of concentration may reduce hole and electron recombination. The positive effect of O_2 bubbling is shown in Figure 4B by shortening the overall degradation time. In both cases P25 was the most efficient photocatalyst followed by Ni(OH)₂/P25, TiO₂ nanofibers and mesoporous TiO₂. Rate constants in both cases are listed in Table 2, where *k* values are approximated by a pseudo first-order rate law.

Figure 4. Degradation of 4-CP (33 ppm) irradiated in 365 nm LED reactor using Degussa P25, TiO₂ nanofibers, Ni(OH)₂/TiO₂ and mesoporous TiO₂ without (**A**) and with O₂ bubbling (**B**). Absorbance at 246 nm was monitored. Irradiation times are converted to required energy per volume in (kJ/L) for the corresponding removal of 4-CP shown on the *Y* axis.



2.4. Degradation of Sulfamethoxazole Using UVA (365 nm) Irradiation

Degradation of sulfamethoxazole (SMX), which is one of the most commonly used antibiotics and one of the ECs [34], was also evaluated in the 365 nm LED reactor using Ni(OH)₂/TiO₂, TiO₂ nanofibers, mesoporous TiO₂ and P25. Figure 5 compares the results, where the first point corresponds to the normalized concentration after dark period. Adsorption of SMX on photocatalysts surfaces was determined to be negligible in all cases. Again the most efficient photocatalyst was P25 followed by $Ni(OH)_2/P25$. TiO₂ nanofibers and mesoporous TiO₂ showed similar reactivity towards degradation of SMX. Rate constants listed in Table 1 are approximated by a pseudo first-order rate law.

Figure 5. Degradation of SMX (33 ppm) irradiated in 365 nm LED reactor using Degussa P25, TiO₂ nanofibers and Ni(OH)₂/TiO₂. Absorbance at 266 nm was monitored. Irradiation times are converted to required energy per volume in (kJ/L) for the corresponding removal of SMX shown on the *Y* axis.



Introducing a superior photocatalyst requires that a given candidate exhibits higher levels of photocatalytic activity for several reactions with different reaction conditions. P25 was the most efficient photocatalyst for degradation of the candidate pollutant at pH 6-7 (balanced properties of P25: surface are of 50 m²g⁻¹, primary particle size of 30 nm and combination of anatase and rutile structures makes P25 one of the best photocatalysts known up to date [19]) but for a real water sample with pH of 8, Ni(OH)₂/P25 was more efficient than P25 in degrading FAs.

Compound	Photocatalyst					
	Degussa P25	Ni(OH) ₂ /P25	TiO ₂ nanofibers	Mesoporous TiO ₂		
4-CP	$k = 0.0132 \text{ min}^{-1}$	$k = 0.0066 \text{ min}^{-1}$	$k = 0.0026 \text{ min}^{-1}$	$k = 0.0013 \text{ min}^{-1}$		
	$R^2 = 0.9702$	$R^2 = 0.9924$	$R^2 = 0.9994$	$R^2 = 0.9968$		
4-CP, O ₂	$k = 0.0503 \text{ min}^{-1}$	$k = 0.0156 \text{ min}^{-1}$	$k = 0.0106 \text{ min}^{-1}$	$k = 0.0039 \text{ min}^{-1}$		
	$R^2 = 0.9425$	$R^2 = 0.9900$	$R^2 = 0.9929$	$R^2 = 0.9911$		
SMX	$k = 0.0283 \text{ min}^{-1}$	$k = 0.0119 \text{ min}^{-1}$	$k = 0.0083 \text{ min}^{-1}$	$k = 0.0089 \text{ min}^{-1}$		
	$R^2 = 0.9739$	$R^2 = 0.9886$	$R^2 = 0.9850$	$R^2 = 0.9727$		

Table 1. Pseudo first order rate constants and R^2 for 4-CP (with and without O₂ bubbling) and SMX.

2.5. Choosing Appropriate Photocatalysts for Water Treatment Purposes

The first step for photocatalytic treatment of water is to define characteristics of the water to be treated in terms of water composition and pH. Normally we are faced with three basic types of source water: ground water, ground water affected by surface water (GUDI) and surface water. NOM is present in surface water but rarely in ground water unless it is contaminated from surface water. So based on the presence or absence of NOM (FAs as representatives of humic substances) the following options (Scheme 1) are available:

Scheme 1. Photocatalytic degradation of water pollutants and side reactions in presence or absence of NOM under UV or Visible irradiation. * Passive NOM sensitization is the case, where TiO_2 is not directly excited by UV light. NOM absorb visible light to start the reaction.



Degradation of ECs has been shown to be efficient when UV light sources are used. FAsphotosensitized degradation of ECs was also verified for degradation of 4-CP and it was efficient [29]. However, the NOM sensitized processes will vary greatly with the NOM composition and concentration.

Reviewing the reactivity tests performed using candidate photocatalysts, P25 was the most effective for degradation of 4-CP and SMX. If FAs (NOM) are present Ni(OH)₂/P25 and mesoporous TiO₂ are specifically good because of the very efficient adsorption of FAs (NOM) on the surface. Ni(OH)₂/P25 has been shown to be applicable at high pHs (around 8), where P25 is not efficient. Another advantage of this photocatalyst is, its easy separation compared to other photocatalyst. If a slurry is to be made using mixed photocatalysts (e.g., Ni(OH)₂/TiO₂ and P25) then one can take advantage of both photocatalysts. TiO₂ nanofibers and mesoporous TiO₂ are interesting candidates if a fixed bed reactor is to be used. There are different reported methods for growing TiO₂ nanofibers on a surface [24] or to form mesoporous structure on a surface. An example is mesosponge TiO₂ formed on Ti foil surface by anodization [23]. However, what is perhaps the most interesting conclusion is that despite the fact that the present results illustrate the need to compare photocatalysts by exploring a range of substrates [27], differences seen here are in the main not large and there will be little incentive to develop reactors with a photocatalyst choice dedicated to a single target substrate.

3. Materials and Methods

3.1. Materials

The following chemicals were used in the experiments: europium (III) oxide (99.9%) provided by REaction/Alfa Aesar (Ward Hill, MA, USA); neodymium (III) oxide (99.9%) ; phosphotungstic acid (reagent grade) and nickel(II) nitrate hexahydrate (99.999%) supplied by Sigma-Aldrich (St. Louis, MO, USA); Sulfamethoxazole by Fluka (St. Louis, MO, USA); Pluronic P-123 (a triblock copolymer: Poly(ethylene glycol)-block-poly(propylene glycol)-block-poly(ethylene glycol) by Sigma- Aldrich (St. Louis, MO, USA); isopropyl alcohol (99.99%) by EMD (OmniSolv) (Gibbstown, NJ, USA); 4-chlorophenol by Aldrich and Suwannee river fulvic acid (a reference sample widely studied) from the International Humic Substance Society (IHSS) (St. Paul, MN, USA). Distilled deionized water was used as required in the experiments.

3.2. Preparation of the Photocatalysts

TiO₂ nanofiber, which was kindly provided by Ghosh *et al.* [12], was prepared by the following procedure outlined by Sui *et al.*, in which a mixture of heptane, acetic acid and titanium isopropoxide was heated to 60 °C until a gel was formed [20]. The gel was aged for 5 days, then dried at 80 °C and finally calcined at 400 °C for 2 h.

A sol gel method described by Xu *et al.* was used to prepare the Eu and Nd doped photocatalysts [22]. Diluted titanium isopropoxide with isopropanol was added to the aqueous solution of Eu or Nd oxides with pH of 1.5. The mixture was kept refluxing at 75 °C for 24 h and then the precipitate was dried at 60 °C. Ni(OH)₂ cluster-modified TiO₂ (Ni(OH)₂/TiO₂ nanocomposite) was fabricated using a precipitation method presented by Yu *et al.* using Degussa P25 as support and Ni(NO₃)₂ as precursor. Degussa P25 was dispersed in 1.0 M NaOH aqueous solution, to which was added Ni(NO₃)₂ aqueous solution. The mixed solutions were stirred for 24 h at room temperature. After that, the precipitates were collected and washed with distilled water and alcohol respectively and dried at 80 °C for 24 h [17]. WO₃/TiO₂ nanohybrid was also prepared by a sol gel method with titanium isopropoxide and phosphotungstic acid (H₃PW₁₂O₄₀ deionized water. The mixture was aged for 2 h, the gel was dried at 100 °C and sintered at 500 °C for 5 h. The powder was washed thoroughly with water and then dried at 80 °C [18].

Finally mesoporous TiO₂ was prepared by a method suggested by Calleja *et al.*: Pluronic P-123 was first dissolved in a mixture of 2-propanol and HCl in water [21]. The resulting solution was stirred for 4 h and then it was added to a solution of titanium isopropoxide and 2-propanol under vigorous stirring at 40 °C, obtained sol was kept under stirring until a gel appeared (molar ratio H₂O/Ti = 6 and grams of P-123 per 0.01 mol of Ti = 1). The gel was aged at 40 °C and dried under ambient conditions. Finally, to extract the surfactant, the solid product was refluxed with ethanol for 24 h.

Table 2 lists the physical properties of the synthesized photocatalysts reported in the original papers. It should be noted that the band gap for the synthesized photocatalyst is at least 3.2, which is the intrinsic band gap of anatase. In contrast to all of the others, in case of Eu and Nd doped TiO_2 , there is a shift to lower energies (longer wavelengths), which is not fully characterized.

Photocatalyst	Crystalline structure	Average particle size (nm)	composition
TiO ₂ nanofibers [20]	Anatase	13	-
Ni(OH) ₂ /TiO ₂ [17]	Anatase and Rutile	24 (Anatase), 46 (Rutile)	$Ni(OH)/Ni(OH)_{2}^{+}$ P25 = 0.1
WO ₃ /TiO ₂ [18]	Anatase	9.5–10	W/Ti(mole ratio) = 0.04
Mesoporous TiO ₂ [21]	Anatase	2.8 (pore size)	-
Eu doped TiO ₂ [22]	Anatase with a little	5 5	Eu ₂ O ₃ /Ti(OiPr) ₄ (mole
	brookite	brookite	

Table 2. Physical properties of the synthesized photocatalysts.

Successful preparation of the chosen photocatalysts was selectively confirmed by SEM/EDS: Scanning Electron Microscopy with X-ray microanalysis (Figure A1 in the Appendix). An extensive set of figures is not included here since the cited literature was confirmed.

3.3. Reactivity Evaluation

Suwannee river fulvic acids (FAs), representing NOM; 4-CP representing pesticide type molecules, and Sulfamethoxazole (SMX) representing pharmaceuticals, were chosen as model compounds to test the reactivity of the synthesized photocatalysts. 4-CP solution and SMX (33 ppm) were prepared by dissolving 4-CP or SMX in Milli- Q water without changing the pH. FAs samples were model "natural water samples", which were prepared using the following recipe: 0.020 g. of Suwannee river FA, 0.117 g of calcium chloride and 0.181 g of sodium bicarbonate was added to 2 L of boiling Milli-Q water. The pH of the solution was then adjusted between 7.1–7.3. The solution had about 10 ppm of FA. Reactivity tests were performed using 0.25% (*w*/*v*—2.5 g/L) photocatalysts slurries (see discussion for more detail). The slurries were agitated in dark for 30 min using a magnetic stirrer prior to irradiation.

The solutions were then subjected to irradiation for appropriate periods in a compact circular bench scale reactor equipped with 365 nm LED lamps [35]. The inside diameter and depth of the reactor are 9 and 7 cm respectively and it is equipped with 90 LED 3 mW output lamps (NSHU5518), which are evenly distributed in 15 rows (Figure A2 in the Appendix). The number of photons absorbed by the solutions was determined by chemical actinometry using potassium ferrioxalate [36]. Incident photon flux, measured under exactly the same conditions as in the photocatalytic experiments, was evaluated to be $4.3 \pm 0.2 \times 10^{16}$ photos/s for the LED reactor. This light intensity was used to calculate energy dosage. Energy dosage is calculated using the following equation:

$E = I \times t \times hc/1000\lambda$

where *E* is energy dosage delivered into the sample (in kJ), *I* is light intensity (photons/s), *t* is irradiation time(s), *h* is Planck's constant (Js), *c* is velocity of light in vacuum (m/s) and λ is wavelength of photon in m.

At predetermined time intervals, slurry samples were withdrawn, centrifuged and filtered through 0.45 μ filters. For the nanoparticles, addition of NaOH made the separation of the photocatalyst much easier and faster. In case of using Ni(OH)₂/TiO₂ as the photocatalyst , separation of the particles was easy and there was no need to modify the pH.

FAs samples were analyzed by studying changes in fluorescence spectra using an excitation wavelength of 350 nm. The efficiency of the photocatalysts was compared based on the physical adsorption of FAs on the surface and based on the disappearance of the fluorescent components of SRFA. No fluorescence detected after a certain irradiation time, does not mean complete degradation of SRFA or total mineralization. Longer irradiation times may be required to get the point of >95% mineralization, but our experience with SRFA suggests that fluorescence is a good measure, which is sensitive to changes in composition as the mixture reacts. Fluorescence could also provide mechanistic insights if band are observed to shift [28]. A Varian Cary Eclipse fluorescence spectrophotometer was used. The slit-widths were adjusted at 5 nm for both excitation and emission and the photomultiplier was set to operate at 1000 volts. To study the effect of O_2 concentration on the reaction, O_2 was bubbled through the solutions during photocatalytic degradation.

4. Conclusions

This study was undertaken as a part of a program aimed at evaluation of the opportunities for photocatalytic water treatment created by the emergence of LED light sources. At visible wavelengths, LEDs are already the most efficient converters of electrical energy to light and progress into the UV is proceeding on a learning curve parallel to that of visible counterparts. If solar energy use is desirable, as in remote locations, DC operated LEDs can be powered from a photovoltaic array. In this study, we selected a cross-section of TiO₂ compositions for investigations for superior performance as a candidate for application for water treatment. The main conclusion is that, of the photocatalysts investigated, none were outstandingly superior or totally inferior to Degussa P25 TiO₂. This then leads us to conclude that the choice of a particular photocatalyst for a reactor will depend primarily on photoreactor design issues. Some candidates appear to require slurry use, whereas others are obvious candidates are best for fixed beds. At this stage, it is difficult to nominate a substitute for inexpensive, commercial Degussa P25 as a broad spectrum photocatalyst for such reactors.

Appendix

This Appendix includes a list of TiO₂ photocatalysts reported in the literature, mostly rare earth doped, and their relative reactivities for specific model compounds compared to corresponding undoped catalysts and/or P25 (Table A1) and, Scanning Electron Microscopy with X-ray microanalysis SEM/EDS results for WO₃/TiO₂, Mesoporous TiO₂ and Eu doped TiO₂ (Figure A1).

Photocatalyst	Light source	Model compound	Reactivity compared to P25 or un-doped TiO ₂	Reference
Sm, N co-doped TiO ₂ nanoparticles	Tungsten lamp with cut off filter 420 nm	Salycilic acid	Not reported	[37]
mesoporous TiO_2 nanoparticles	black lamps	Rhodamine B	Better than both	[38]
doped TiO ₂ nanoparticles	Xenon arc lamp	Remazol Red RB-133	Not reported	[39]
Eu, Pr, Yb	Xe (Hg) lamp	p-Nitrobenzoic acid , p-chlorophenoxy acetic acid, aniline, salicylic acid and trans- cinnamic acid	Not reported	[40]
Eu, Pr, Yb	Xe(Hg) lamp	Salicylic acid and t-cinnamic acid	Not reported	[41]
La,Pr, Nd, Sm, Eu, Gd , Yb doped TiO ₂	medium pressure mercury lamp	Rhodamine B	Not reported	[42]
Sm doped TiO ₂	halogen tungsten lamp with a UV and IR cut-off filter	Methylene Blue	Not reported	[43]
Sm doped TiO_2	sunlight	Methylene Blue	Better than both	[44]
(Sm ³⁺ , Nd ³⁺ , Ce ³⁺ and Pr ³⁺) doped titania-silica	sunlight	Methylene Blue	Better than undoped titania-silica	[45]
Ce, Co, Eu, Sm, W and Yb doped TiO ₂	medium pressure Hg lamp	4-Nitrophenol	Sm and W doped TiO ₂ , better than P25	[46]
Eu, N	Halogen lamp with 400 nm cut off filter	Reactivebrilliant red X-3B	Better than both under visible light irradiation	[22]
La, Ce, Pr, Nd, Sm, Eu, Dy, Gd doped TiO ₂	254, 365 and 400 nm	Orange II dye	Nd highest reactivity, better than both at all wavelengths for Ce & Nd doped TiO2	[32]
La, Nd and Pr doped TiO_2	Solar irradiation	Methylene Blue	Better than undoped	[47]
La, Nd, Sm, Eu, Gd, Dy, Yb; B) Al, In	Xenon arc lamp	Toluene	Not reported	[48]

Table A1. Some of the synthesized photocatalysts reported in the literature, chosen model compounds for the reactivity test, light source and their relative reactivities compared to corresponding undoped catalysts and P25.

Figure A1. Scanning electron microscopy with X-ray microanalysis SEM/EDS was performed using a LEO 1530 (SEM images were taken with previous gold-coating) for: (A) WO₃/TiO₂; (B) Mesoporous TiO₂; (C) Eu doped TiO₂.



Other samples:

- Ni(OH)₂ coated on P-25;
- Nanofibre TiO₂ was supplied by the authors of reference [12]. Full characterization is found there.

Figure A2. Top view of 365 nm LED rector: (a) lights on (b) lights off, Adapted from reference [35].



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Conflicts of Interest

The authors declare no conflict of interest.

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