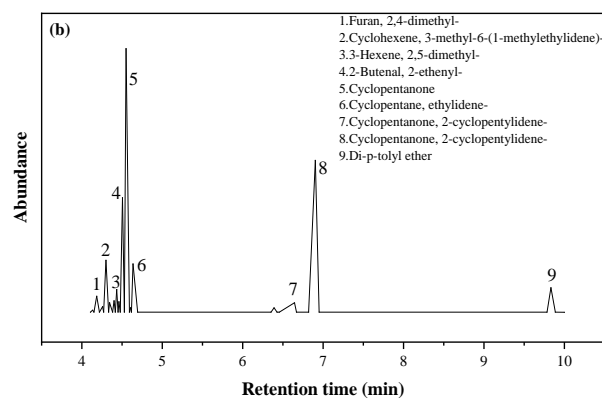
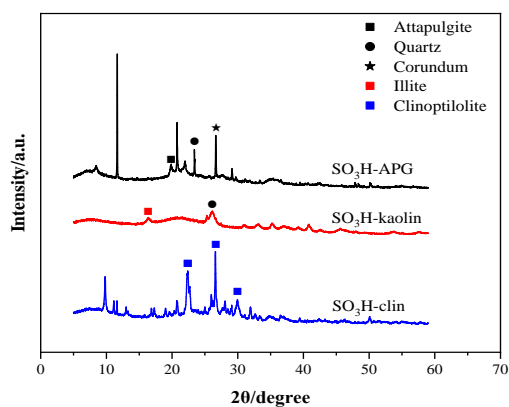


## 1 Products Analysis



**Figure S1.** Main products and TIC diagram of cyclopentanone condensation reaction on  $\text{SO}_3\text{H}$ -APG catalyst.



**Figure S2.** XRD patterns of clay-based catalysts.

## 2. Response Surface Methodology (RSM) Analysis

From the results of the path of steepest ascent experiment, the values of each factor were determined as 0 mL, 0.8 mL, 1.6 mL, 2.4 mL and 3.2 mL of -SH group loading; the reaction temperatures were 110 °C, 130 °C, 150 °C, 170 °C and 190 °C, and the reaction times were 2 h, 3 h, 4 h, 5 h and 6 h.

**Table S1.** Optimization of Box-Behnken test factors and levels for C10 yield conditions.

Factors	-1	0	1
X <sub>1</sub> -SH loading/ml	0	1.6	3.2
X <sub>2</sub> reaction temperature/°C	110	150	190
X <sub>3</sub> reaction time/h	2	4	6

**Table S2** Optimization of Box-Behnken test results and analysis for C10 yield conditions.

	X1	X2	X3	C10 yield/%
1	0	110	4	26.35
2	3.2	110	4	26.48
3	0	190	4	32.76
4	3.2	190	4	35.68
5	0	150	2	30.03
6	3.2	150	2	31.98
7	0	150	6	34.61
8	3.2	150	6	37.06
9	1.6	110	2	38.36
10	1.6	190	2	30.03
11	1.6	110	6	35.78
12	1.6	190	6	32.41
13	1.6	150	4	59.05
14	1.6	150	4	58.98
15	1.6	150	4	59.03
16	1.6	150	4	59.05
17	1.6	150	4	58.74

Using Design expert V8.0.6 software to fit the data in Table S2, the regression equation S1 was obtained.

$$Y = 58.97 + 0.93X_1 + 0.49X_2 + 1.18X_3 + 0.7X_1X_2 + 0.13X_1X_3 + 1.24X_2X_3 - 14.69X_1^2 - 13.96X_2^2 - 10.86X_3^2$$

(Eq. S1)

Analysis of variance was performed on the above regression equation and the results are tabulated in Table S3.

**Table S3** Variance analysis of response surface experiments results.

Variance Source	Square Sum	Degrees of Freedom	Mean Square	F-value	P-value	Salience
Model	2510.42	9	278.9	18.48	0.0004	**
X <sub>1</sub>	6.94	1	6.94	0.46	0.0396	*
X <sub>2</sub>	1.91	1	1.91	0.13	0.0225	*
X <sub>3</sub>	11.19	1	11.19	0.74	0.0479	*
X <sub>1</sub> X <sub>2</sub>	1.95	1	1.95	0.13	0.7302	
X <sub>1</sub> X <sub>3</sub>	0.063	1	0.063	0.0041	0.9505	
X <sub>2</sub> X <sub>3</sub>	6.15	1	6.15	0.41	0.5436	
X <sub>1</sub> <sup>2</sup>	908.46	1	908.46	60.17	0.0001	**
X <sub>2</sub> <sup>2</sup>	821.00	1	821.00	54.38	0.0002	**
X <sub>3</sub> <sup>2</sup>	496.70	1	496.70	32.90	0.0007	**
Residual	105.68	7	15.10			
Proposed item loss	105.61	3	35.20	2029.01	0.0591	
Error term	0.069	4	0.017			
Sum	2616.10	16				

Note: "\*" indicates a significant effect on the results ( $P < 0.05$ ); "\*\*\*" indicates a highly significant effect on the results ( $P < 0.01$ ).

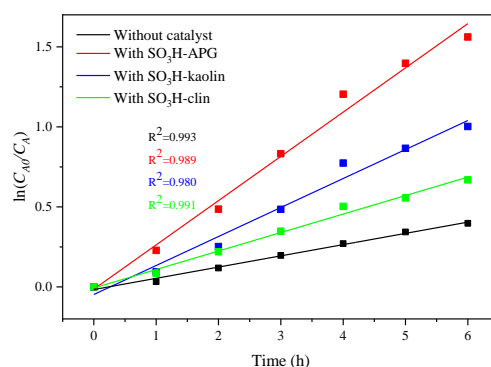
**Table S4** Ammonia and carbon dioxide desorption activation energy (DAE).

	CO <sub>2</sub>		NH <sub>3</sub>		E <sub>d</sub> (kJ/mol)	
	Yang		Hu		E <sub>d</sub> (kJ/mol)	
	0-150°C	150-450°C	0-150°C	150-450°C	Yang	Hu
APG	9.88	36.38	12.37	36.29	25.52	18.34
SO <sub>3</sub> H-APG	10.48	25.73	22.61	44.11	23.72	20.99
SO <sub>3</sub> H-kaolin	-	-	-	-	17.89	24.65
SO <sub>3</sub> H-clin	-	-	-	-	13.72	14.09

**Table S5** Physiochemical properties of catalysts.

	CO <sub>2</sub>		<i>E<sub>d</sub></i> (kJ/mol)		NH <sub>3</sub>	<i>E<sub>d</sub></i> (kJ/mol)
	Yang		Hu			
	0-150°C	150-450°C	0-150°C	150-450°C	Yang	Hu
APG	9.88	36.38	12.37	36.29	25.52	18.34
SO <sub>3</sub> H-APG	10.48	25.73	22.61	44.11	23.72	20.99
SO <sub>3</sub> H-kaolin	-	-	-	-	17.89	24.65
SO <sub>3</sub> H-clin	-	-	-	-	13.72	14.09

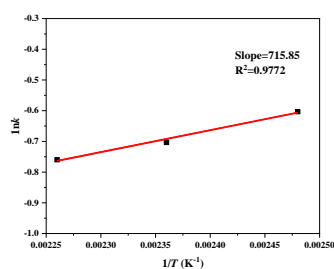
### 3. Reaction Kinetic Analysis

**Figure S3.** The kinetic plots for the cyclopentanone aldol condensation.

According to the Arrhenius equation:  $k = k_0 \cdot e^{\left(\frac{E}{RT}\right)}$ , take the logarithm to get  $\ln k = \ln k_0 - \frac{E}{RT}$ , make the graph of  $\ln k - \frac{1}{T}$ , the slope is  $-\frac{E}{R}$  and the intercept is  $\ln k_0$ .

**Table S6** The reaction rate constants  $k$  at different temperatures.

T/°C	130	150	170
$k$	0.5470	0.4949	0.4677
$\frac{1}{T}/K^{-1}$	0.00248	0.00236	0.00226
$\ln k$	-0.6033	-0.7034	-0.7599

**Figure S4.** The Arrhenius equation curve.

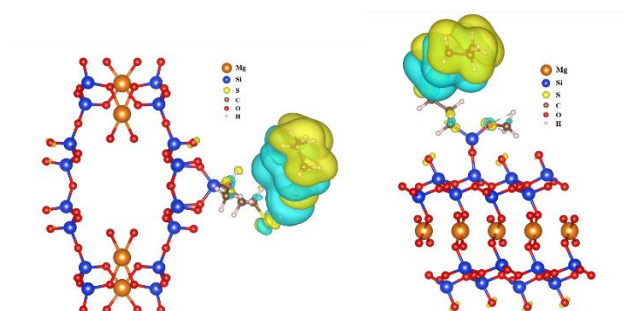
From the calculation, we could get  $E = -(715.85) \times 8.314 = 5952 \text{ J/mol}$ ;

$$k_0=0.093.$$

The reaction rate constant was  $k=0.093e^{(-\frac{5952}{RT})}$ , and the reaction rate equation was  $r_A=0.093e^{(-\frac{5952}{RT})}c_A$ .

#### 4. Modelling of cyclopentanone adsorption

Cyclopentanone adsorption on SO<sub>3</sub>H-APG catalyst was simulated by VASP. Sulfur atom got electron from cyclopentanone to build a stable chemisorption that would be conformed via DFT calculation. Adsorption energy  $E_{ad} = E_{tot} - (E_{sub} + E_{mol})$  was computed to determine the strength of reactant molecule adsorbed on the SO<sub>3</sub>H-APG catalyst, where  $E_{tot}$ ,  $E_{sub}$ , and  $E_{mol}$ , referred to the total energy of the combined system, the substrate alone and the adsorbate in the gas phase, respectively. And the  $E_{ad}$  was got as -0.511948 eV which was indicated a exothermal adsorption of cyclopentanone. Electron density increasing of the adsorbate will facilitate its activation and further condensation.



**Figure S5.** Charge density differences of cyclopentanone adsorption on SO<sub>3</sub>H-APG catalyst.

Blue and yellow areas represent electron accumulation and depletion, respectively. Atom

color: S-yellow, C-brown, O-red, and H-white.