



Article Biocatalytic Cascade of Sebacic Acid Production with In Situ Co-Factor Regeneration Enabled by Engineering of an Alcohol Dehydrogenase

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Abstract: Sebacic acid (1,10-decanedioic acid) is an important chemical intermediate. Traditional chemical oxidation methods for sebacic acid production do not conform with "green" manufacturing. With the rapid development of enzymatic technologies, a biocatalytic cascade method based on the Baeyer–Villiger monooxygenase was developed. The most attractive point of the method is the oleic acid that can be utilized as raw material, which is abundant in nature. However, this bio-catalysis process needs co-factor electron carriers, and the high cost of the co-factor limits its progress. In this piece of work, a co-factor in situ regeneration system between ADH from Micrococcus luteus WIUJH20 (MIADH) and BVMO is proposed. Since the co-factors of both enzymes are different, switching the co-factor preference of native *MI*ADH from NAD⁺ to NADP⁺ is necessary. Switching research was carried out based on in silico simulation, and the sites of Tyr36, Asp 37, Ala38, and Val39 were selected for mutation investigation. The experimental results demonstrated that mutants of MIADH_D37G and MIADH_D37G/A38T/V39K would utilize NADP+ efficiently, and the mutant of MIADH_D37G/A38T/V39K demonstrated the highest sebacic acid yield with the combination of BVMO. The results indicated that the in situ co-factor generation system is successfully developed, which would improve the efficiency of the biocatalytic cascade for sebacic acid production and is helpful for simplifying product isolation, thus, reducing the cost of the enzymatic transformations process.

Keywords: co-factor regeneration; alcohol dehydrogenase; sebacic acid; enzymatic cascade reaction; in silico simulation

1. Introduction

Long-chain α , ω -dicarboxylic acids (α , ω -DCAs) are frequently and widely applied to produce various chemicals and intermediates, such as nylon, preservatives, lubricants, plasticizers, fragrances, and cosmetics [1]. Traditionally, α , ω -DCAs are produced from petrochemical raw materials or special fatty acids (ricinoleic acid) through oxidative cracking with harsh reaction conditions, involving high temperature, high pressure, strong acid catalysts (e.g., H₂SO₄, HNO₃), and toxic oxidants (e.g., ozone, peroxide) [2,3]. Due to the uncontrolled reaction, the process always had low yields, high energy consumption, and uncontrollable by-products, which were seriously harmful for the environment and did not meet the modern topic of "green and sustainable development" [4]. By contrast, enzymatic synthesis could be an alternative with advantages of having mild conditions; being environmentally friendly; and having high regio-, stereo-, and enantioselectivity [5]. Therefore, exploring a novel biocatalytic synthesis of α , ω -DCAs is a subject of profound significance.



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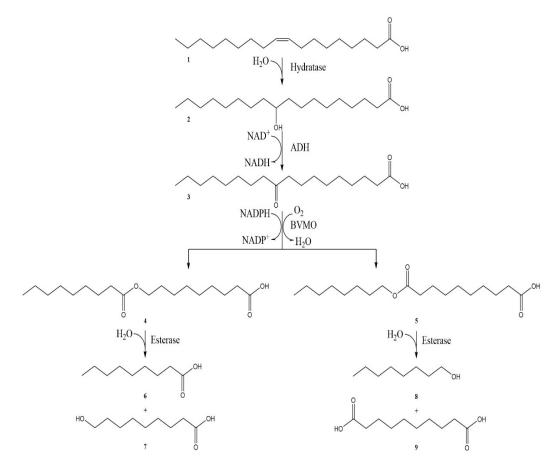
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In recent years, there are more and more reports on cascade biocatalytic reactions. The advantages of cascade reactions are as follows: (1) the multi-step reaction can be carried out in a reactor and does not require the separation of intermediates; (2) less solvents and chemicals are needed; (3) intermediates are quickly consumed in continuous steps, which can reduce waste emissions. Therefore, cascade biocatalytic reactions can shorten the reaction time and cost [6,7]. Song et al. reported an enzymatic cascade process (Scheme 1, [8]) for sebacic acid (1,10-decanedioic acid, Compound 9) production with oleic acid (Compound 1) as raw material, which is a natural unsaturated fatty acid present in most kinds of vegetable oils. In this cascade reaction, hydratase hydrates the unsaturated carbon-carbon double bond of oleic acid firstly, and then the hydroxy group is further converted into carbonyl through the dehydrogenation reaction catalyzed by a NAD-dependent alcohol dehydrogenase (ADH). Subsequently, a Baeyer-Villiger (BV) oxidation reaction was introduced. Two kinds of esters would form as the results of BV oxidations, and sebacic acid would be obtained as the hydrolysis product of ester compound 5. Among the cascade process, the regioselectivity of the Baeyer–Villiger monooxygenase (BVMO) is the key point. Only part of natural BVMO tend to transfer oxygen atoms to less substituted carbon centers during the catalytic process to generate esters with "abnormal" configurations (compound 5) [8,9]. BVMO from Pseudomonas aeruginosa (PaBVMO) [10] and Pseudomonas fluorescens DSM 50106 (*Pf*BVMO) [11] were the only two reported enzymes that have "abnormal" regioselectivity fit for sebacic acid production.

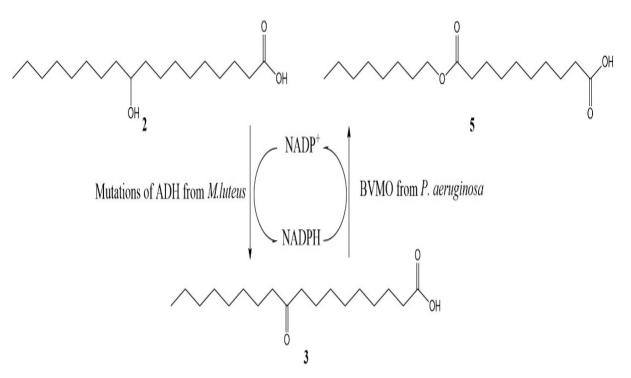


Scheme 1. Biotransformation pathway [8]. Oleic acid (1) is converted into either n-nonanoic acid (6) and ω -hydroxynonanoic acid (7) or n-octanol (8) and 1,10-decanedioic acid (9) by multistep enzyme-catalyzed reactions.

Beside the regioselectivity of BVMO, there is another limitation for the process. For the biocatalytic cascade of sebacic acid production, the co-factor specificity of two oxidoreductases is different, NAD⁺ was required for ADH, while NADP⁺ was required for BVMO. Thus, it is necessary to introduce other reaction systems for the co-factor regeneration to reduce the cost of this in vitro cascade reactions [12–14]. For example, NADPH regeneration systems, commonly used in BVMO, catalyzed oxidation reactions include glucose-6-dehydrogenase (GDH) [15] and formate dehydrogenase (FDH) [16]. For NAD⁺ regeneration, NADH oxidase (NOX) was the most applied enzymatic regeneration system [17,18]. However, the multiple enzymes operating under uniform reaction conditions may not be optimal for one of the enzymes. The complicated enzymatic cascades require optimization to facilitate the enzyme rate match for maximum catalytic efficiency, and, consequently, the number of enzymes can continue to enhance the multi-enzyme catalysis system. This will not only increase the complexity of the system to match each other but also introduce other by-products, thus, increasing the difficulty of sebacic acid purification. Therefore, construction of a co-factor regeneration system for the cascade reaction of Scheme 1 without additional enzymes is necessary.

The modification of co-factor specificity through protein engineering provides a desired solution for the above problems. Based on the technique of molecular simulation, the mechanism of co-factor switching was investigated [19]. It could be noticed that the structural difference in the phosphate group of the adenosine ribose ring moiety determined the co-factor specificity of oxidoreductases [20,21]. The key residues that influenced the co-factor preference are mainly surrounding around these phosphate group binding sites [22,23]. Rational or semi-rational design works based on the alteration of the size or electrostatic state of the key residues with the help of molecular simulation were carried out for the co-factor switching of virous oxidoreductases. Seo et al. switched the co-factor specificity of secondary alcohol dehydrogenase (Micrococcus luteus, MIADH) from NAD⁺ to NADP⁺ through a reconstruction of the structure of NADP⁺ binding sites. Then, the engineered enzyme was successfully coupled to a NADPH-dependent BVMO from Pseudomonas putida KT2440 for redox-neutral biotransformation of long chain unsaturated fatty acid into medium chain length chemicals [24]. Bommareddy et al. successfully altered the co-factor specificity of glyceraldehyde 3-phosphate dehydrogenase (Corynebacterium glutamicum) from NAD⁺ to NADP⁺ dependent [25]. Beier et al. switched the preference of cyclohexanone monooxygenase from Acinetobacter sp. NCIMB 9871 from NADPH to NADH by using computational design [26]. Other successful examples included imine reductase [27], secondary alcohol dehydrogenase [28], and dihydrodipicolinate reductase [29], among others.

In this work, an in situ NADP⁺ regeneration system (Scheme 2) is proposed between ADH from *Micrococcus luteus* WIUJH20 (*Ml*ADH) and *Pa*BVMO by reconstruction of the co-factor binding region of the native *Ml*ADH from NAD⁺ to NADP⁺ dependent. Thus, a NADPH regeneration system would be built to improve the catalytic efficiency of the multienzyme system and to reduce the production costs. The molecular simulation works were carried out for the mutation design. The co-factor preference and its catalytic performance of mutagenesis were also tested. The results of the work are promising to reduce the cost of enzymatic transformations of sebacic acid and the simplified products isolation.



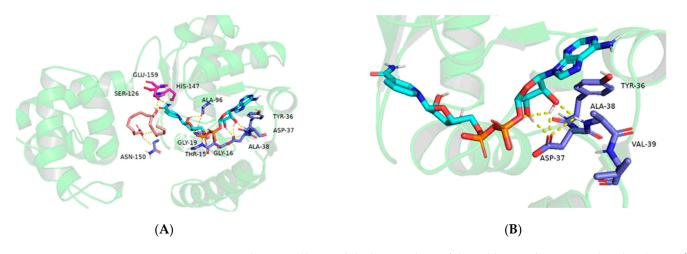
Scheme 2. Construction of a NADPH regeneration system by altering the co-factor specificity of a native NAD⁺-dependent ADH to NADP⁺.

2. Results and Discussion

2.1. Probing the Targeted Residues that Determining the Co-Factor Specificity of MIADH

The discrimination between NAD⁺- and NADP⁺-dependent enzymes is the consequence of differences in the size and structure of the co-factor binding pocket, as well as the physicochemical properties of the surrounding amino acid residues [30]. Initially, a homology model of *MI*ADH was built based on the template of a diketoreductase crystal structure (Protein Data Bank code: 4E12, and the sequence identity with *MI*ADH is 49.12%) through the SWISS-MODEL (https://swissmodel.expasy.org, accessed on 23 May 2019). Then, two steps of molecular docking were performed, with the homology model of *MI*ADH as the receptor and NAD⁺ and 10-hydroxyoctadecanoic acid as the ligand, respectively.

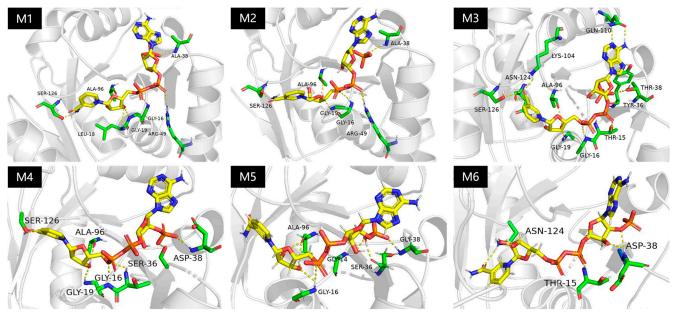
From the structure and catalytic mechanism analysis of diketoreductase (PDB code:4E12), three residues of His-Ser-Glu and the active hydrogen from NAD⁺ formed the catalytic triad of the enzyme [9]. From the comparison of docking results (Figures 1 and S2) with the structure of PDB 4E12, the possible active center of MIADH should be Ser 126, His 147, and Glu 159. The 10-hydroxyoctadecanoic acid fits into the active site cleft and its 10-hydroxyl group lies between the imidazole ring of His147 and the nicotinamide of NAD⁺. Another side of the NAD⁺ molecule binds to the enzyme through hydrogen bonds and hydrophobic forces, with the 2' active hydrogen of the nicotinamide moiety of NAD⁺ facing the cleft between the two binding domains, which formed a proton transfer channel between the solution and the active site. The essential difference between NADP⁺ and NAD⁺ is that the 2'-hydroxyl group of the adenosine ribose ring of NAD⁺ is replaced by a phosphate group. It could be noticed that the carboxylate group of Asp 37 forms a hydrogen bond with the 2'-hydroxyl of the adenosine ring of NAD⁺, which would stabilize the binding of NAD⁺ with the enzyme. However, when the co-factor switched to NADP⁺, the phosphate group on the adenosine ring may have electrostatic repulsion and steric hindrance with the Asp 37 residue [31]. Therefore, the substitution of Asp 37 by other positively charged and polarized residues may enable NADP+ to form hydrogen bonds and stabilize the co-factor binding with the enzyme [32]. In addition, it could be noticed that three other residues Tyr36, Ala38, and Val39 also influenced the interaction between NADP⁺ and peptide chain of MlADH, which determined the stability of NADP⁺ in the co-factor binding pocket. Thus,



except for Asp 37, these three residues were also considered as potential targets for further mutation selection.

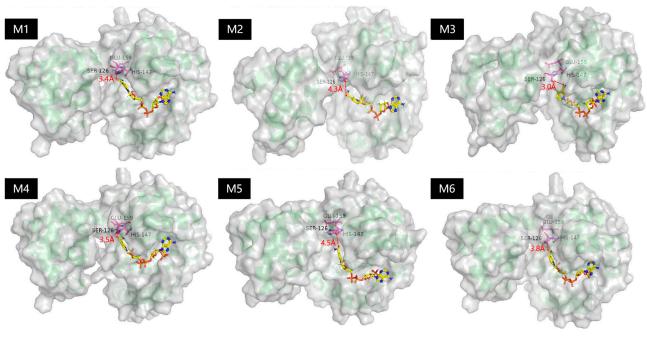
Figure 1. Homology modeling and docking analysis of the wildtype *MI*ADH complexed with NAD⁺. (A) Enzyme conformation when binding NAD⁺ to substrate. (B) Binding force analysis of NAD⁺ and enzyme.

Since the site of Asp 37 should be replaced by a small and uncharged residue, glycine and alanine were promising candidates. For the sites of Tyr 36, Ala 38, and Val 39, the residues of serine, threonine, glutamic acid, aspartic acid, lysine, and asparagine were assessed in the investigation. The NADP⁺ docking effects of all the possible mutation combinations were simulated. In terms of the docking results of co-factor position, the electron transfer efficiency of co-factor with active site Ser 126 (the distance of active hydrogen of NADP⁺ to the hydroxy of Ser 126 is less than 4.5 Å), and the lowest binding energy of the co-factor with enzymes, 6 of the more reasonable candidates (M1: D37G, M2: D37G-V39S, M3: D37G-A38T-V39K, M4: Y36S-D37G-A38D, M5: Y36S-D37G-A38D-V39K) were chosen from 432 possibilities (Figure 2) and were examined in the further experimental characterization.



(A)

Figure 2. Cont.

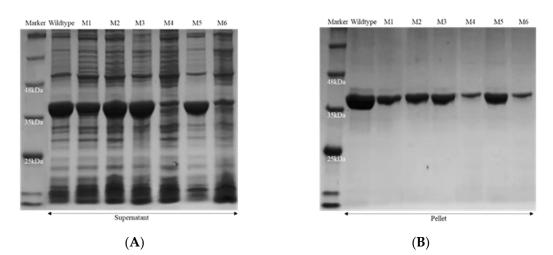


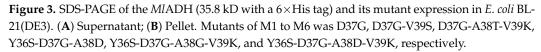
(B)

Figure 2. Simulation results of reasonable mutation candidates. (**A**) The binding conformation of NADP⁺ in the enzyme; (**B**) The whole conformation of the ADH with NADP⁺. Mutants of M1 to M6 were D37G, D37G-V39S, D37G-A38T-V39K, Y36S-D37G-A38D, Y36S-D37G-A38G-V39K, and Y36S-D37G-A38D-V39K, respectively.

2.2. Enzyme kinetics

Based on the simulation results, six mutational targets were performed through the method of site-directed mutagenesis, and all the engineered protein was heterologously expressed in *E. coil* BL21(DE3). The results of SDS-PAGE indicated that most of the *Ml*ADH mutants could be successful expressed; only mutant M4 (Y36S-D37G-A38D) and M6 (Y36S-D37G-A38D-V39K) had relatively low expression rate (Figure 3A,B).





In order to investigate the enzymatic properties of each variant, the proteins were purified through Ni-NTA affinity chromatograph. Then, the kinetics parameters were assayed through the dehydrogenation of 10-hydroxyoctadecanoic acid with co-factor of $NAD(P)^+$. Based on the characters that the reduced form of NAD(P)H absorbs at 340 nm, which the aromatic oxidized form does not [33], the changes of the absorbance at 340 nm (OD_{340}) along with reaction times were detected. With the substate-loading variation, the kinetic parameters of each variant were calculated based on the Michaelis–Menten equation and the Hanes–Woolf method [34] (Figure S3).

As shown in Table 1, the wild type of *Ml*ADH has a good performance with the co-factor of NAD⁺ but without detectable activity toward NADP⁺. The mutants of M5 (Y36S/D37G/A38G/V39K) and M6 (Y36S/D37G/A38D/V39K) were more receptive to NAD⁺ and unable to utilize NADP⁺. Four other mutants were enabled to utilize NAD⁺/NADP⁺ at the same time with preference of NADP⁺. However, the catalytic efficiency (k_{cat}/K_m) and the maximum reaction rate (V_{max}) of these mutants were reduced, compared with the wild type. Notably, among these mutants, the single point mutation of M1 (D37G) has the best performance with the co-factor switching to NADP⁺, followed by the combinatorial mutation of M3 (D37G/A38T/V39K) and M2 (D37G/V39S). Since the aim of this work is similar to that of Seo et al. [24], the results were compared with them. For the results of Seo et al., the variant of D37S/A38R/V39S/T15I performed the best NADP+ utilization performance, which is different from ours, and the difference may come from the mutation design method. Meanwhile, the enzyme activity of this investigation was much lower than that of Seo et al. (even for the wild type of *Ml*ADH). The variation may derive from the difference of strain culture, enzyme purification, and enzymatic reactions. The results of this work could complement the work of Seo et al.

Enzymes	Co-Factors	IU (U∙mg ^{−1})	V _{max} (mg·mL ^{−1} min ^{−1})	<i>K_m</i> (mM)	k _{cat} (min ⁻¹)	k_{cat}/K_m (mM ⁻¹ ·min ⁻¹)
Wildtype	NAD ⁺	13.56	4.13	2.08	8.05	3.86
	NADP ⁺	*ND	*ND	*ND	*ND	*ND
M1 (D37G)	NAD ⁺	1.21	0.02	0.60	0.04	0.07
	NADP ⁺	1.82	0.03	0.21	0.05	0.24
M2 (D37G-V39S)	NAD ⁺	0.46	0.14	1.56	0.15	0.10
	NADP ⁺	0.49	0.15	1.35	0.16	0.12
M3 (D37G-A38T-V39K)	NAD ⁺	2.31	0.29	16.48	0.77	0.05
	NADP ⁺	0.56	0.07	1.10	0.19	0.17
M4 (Y36S-D37G-A38D)	NAD ⁺	0.19	0.06	0.19	0.06	0.30
	NADP ⁺	0.19	0.06	0.64	0.06	0.09
M5 (Y36S-D37G-A38G-V39K)	NAD ⁺	0.24	0.01	0.04	0.04	0.99
	NADP ⁺	*ND	*ND	*ND	*ND	*ND
M6 (Y36S-D37G-A38D-V39K)	NAD ⁺	0.30	0.01	0.01	0.05	4.22
	NADP ⁺	*ND	*ND	*ND	*ND	*ND

Table 1. Enzyme kinetic parameters of wild-type *Ml*ADH and its variants.

*ND: not detected. One unit (U) of enzyme activity was defined as the amount of enzyme required to reduce 1 μ mol of NAD(P)⁺ in 1 min under the assay reaction conditions.

2.3. The Efficiency of In Situ NADP⁺ Regeneration System for Sebacic Acid Production

Firstly, the dehydrogenation conversion performance of the wild-type *Ml*ADH with NAD⁺ or NADP⁺ as co-factors was verified. The conversion rate of 10-hydroxyoctadecanoic acid (2) to 10-oxooctadecanoic acid (3) was over 98% when NAD⁺ was applied, whereas the yields of 10-oxooctadecanoic acid was only 15% when the co-factor changed to NADP⁺. The results indicated that the NADP⁺ is not a suitable co-factor for the wild-type *Ml*ADH. Subsequently, the reactions with three kinds of *Ml*ADH mutants as catalysts were carried out under the same conditions. When the NADP⁺ was utilized as the only source of co-factors, the yields of 10-oxooctadecanoic acid with the mutants M3, M1, M2 as catalysts was 56%, 36%, and 27%, respectively. The results of the dehydrogenation reaction of

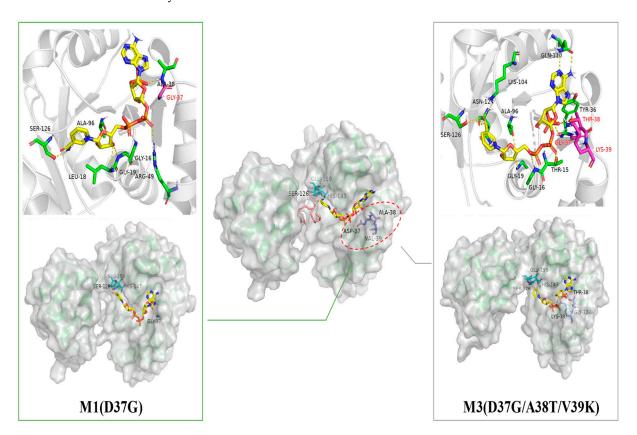
10-hydroxyoctadecanoic acid confirmed the switch of the co-factor preference of *Ml*ADH mutants M3 and M1.

The aim of this investigation was to set up an in situ co-factor regeneration system, which would benefit the biocatalytic cascade of sebacic acid production (Scheme 2). Accordingly, the feasibility of NADP⁺ regeneration system of *MI*ADH mutants and *Pa*BVMO combination was also examined. The traditional multi-enzymatic co-factor regeneration system was set as a controlled group, in which the NOX and the GDH was used for NAD⁺ and NADPH regeneration, respectively. As shown in Table 2, the final yield of sebacic acid was 41.2% for the controlled group. The combined catalysis of wild-type MlADH and PaBVMO still obtained a sebacic acid yield of 20.1% with a single addition of NADP⁺. This may attribute to the weak NADP utilization ability of *Ml*ADH or from the trace amounts of intracellular NAD⁺ in the lyophilized enzymes. Interestingly, the combination of *Ml*ADH mutants (M1 and M3) and PaBVMO with NADP⁺ as a co-factor were improved to various degrees, while the sebacic yield of mutant M3 group (49.3%) was higher than the traditional multi-enzymatic co-factor regeneration system (41.2%). Even from the results of Table 1, the kinetic parameters of our variants are not as good as the related work [24]; the usage of these variants in the cascade enzymatic reactions for sebacic acid production (Table 2) demonstrated the capability of these variants to create a cooperative NADP⁺ regeneration system with BVMO. Thus, the cascade method, combining a proper BVMO with *Ml*ADH variants preferring NADP⁺, might increase the sebacic acid productivity and reduce the cost of the process.

Table 2. Yields of sebacic acid by multistep catalytic reactions through different combinations of *Ml*ADH or its variants and *Pa*BVMO.

Enzymes	Co-Factors	Yields of Sebacic Acid (%)	
Wildtype <i>Ml</i> ADH & <i>Pa</i> BVMO & NOX & GDH	NAD ⁺ & NADP ⁺	41.2 ± 2.7	
Wildtype <i>Ml</i> ADH & <i>Pa</i> BVMO	NAD ⁺ NADP ⁺	6.7 ± 1.2 20.1 ± 3.9	
M1(D37G) & PaBVMO	NAD ⁺ NADP ⁺	$2.1 \pm 1.1 \\ 42.4 \pm 2.2$	
M2(D37G-V39S) & PaBVMO	NAD ⁺ NADP ⁺	5.3 ± 1.4 25.8 ± 3.2	
M3(D37G-A38T-V39K) & PaBVMO	NAD ⁺ NADP ⁺	$2.4 \pm 0.8 \\ 49.3 \pm 3.6$	

Molecular docking was introduced to analyze the benefit reason of above two positive mutants. As shown in Figure 4, the substitution of the amino acid residue of position 37 from Asp to Gly would expand the size of co-factor binding pocket, remove the potential electrostatic repulsion, decrease the effect of steric hinderance, and increase the binding affinity of NADP⁺ successfully. Except for position 37, the residue of Val 39 also affected the ADH to accept NADP⁺. However, the mutation of D37G-V39S does not display an obvious effect for the utilization of NADP+. For the combinatorial mutation of D37G/A38T/V39K, the simulation result revealed that the substitution of Ala 38 to Thr provide more intermolecular hydrogen bonds between peptide chain and the phosphate of NADP⁺. Meanwhile, from the binding energy analysis results in Table 3, the binding energy of wild-type MlADH to NADP+ is only -14.31 kJ/mol, which was significantly lower than that of each mutant. For each mutant of *Ml*ADH, the binding energy of NADP⁺ with protein changed significantly and comes to the same level of the wild-type MlADH with NAD⁺ (-34.60 kJ·mol⁻¹). Mutant *Ml*ADH_D37G-A38T-V39K demonstrated the best results of -34.96 kJ·mol⁻¹, which may explain the reversion of the better NADP⁺ utilization of MIADH mutant M3 (Table 2). However, the worse catalytic results of mutant M2 could



not be explained by the results of the docking simulation, and the reason needs further analysis.

Figure 4. Intramolecular interactions and enzyme surface structure analysis of the wildtype *MI*ADH complexed with NAD⁺ and its mutants of M1 and M3 complexed with NADP⁺. The dotted lines represent hydrogen bonds.

MlADH or Mutants	Co-Factors	Binding Energy (kJ·mol ^{−1})
Wildtype	NAD^+	-34.60
	NADP ⁺	-14.31
M1(D37G)	NAD ⁺	-29.79
	NADP ⁺	-27.69
M2(D37G-V39S)	NAD^+	-30.87
	NADP ⁺	-32.56
M3(D37G-A38T-V39K)	NAD^+	-31.73
	NADP ⁺	-34.96

Table 3. Docking and binding energy of *Ml*ADH and its mutants to NAD(P)⁺.

3. Materials and Methods

3.1. Materials

The 10-oxooctadecanoic acid and 10-ketostearic acid were purchased from Kaiwei Chemical Technology Co., Ltd. (Shanghai, China). The 10-hydroxyoctadecanoic acid was purchased from Bide Pharmaceutical Technology Co., Ltd. (Shanghai, China). Other chemicals and reagents were purchased from BioRo Yee Ltd. (China), and all of them were of analytical grade. The strain of *E. coli* DH5 α (used for molecular cloning) and *E. coli* BL21 (DE3) (used for gene expression) were purchased from Shanghai Weidi Biotechnology Co., Ltd., China. The site mutation kit of "mut express II fast mutagenesis kit V2" was from Vazyme Biotech Co., Ltd. (China). Plasmid extraction kits and gel extraction kits were obtained from Omega Bio-tek (USA).

3.2. Molecular Modeling

Homology models of ADH from *Micrococcus luteus* (NCBI Reference Sequence: ADD83022.1, 310 amino acid residues) were generated based on the structures of diketoreductase (PDB code: 4E12, 283 amino acid residues) using the molecular modeling platform SWISS-MODEL (https://swissmodel.expasy.org, accessed on 23 May 2019) [35], the information of homology model was illustrated in Figure S1 The docking simulations of co-factor-MIADH complexes were performed with the YASARA software package (version 21.8.26). With the *MI*ADH homology model as the rigid receptor, the cofactor as the flexible ligand, and the carboxyl oxygen of Asp37 as the center, a 25×25 docking "box" was set. Then, AMBER 03 force field was used, and docking simulation was carried out at 298K and atmospheric pressure. The docking script "dock_run.mcr" was run to complete 50 rounds of docking, and the optimal docking conformation was screened according to the binding energy and binding conformation. The conformational clusters with correct docking conformation and the highest binding energy with co-factor were considered for further molecular dynamics (MD) simulations to improve the structure of the model. The MD simulations were carried out in aqueous environments with an AMBER03 force field at a pH of 7.5 and a temperature of 313K for 10 ns.

It should be noticed that there is a new structure of *Ml*ADH (PDB code: 6KQ9) published. To check the influence of the difference between our homology models from 4E12 and the experiment structure of 6KQ9, a series of simulation works with 6KQ9 as a template were carried out. The results of structure comparison of the homology model from different templates (Figure S7), the comparison of the simulation results of homology model from 4E12 and 6KQ9 (Figure S8), and the details of the structure of NADP⁺ binding sites analysis (in Figure S9) indicated that there were not significant alterations between the simulation results in the homology model from 4E12 and the *Ml*ADH structures of 6KQ9.

3.3. Gene Cloning and Expression of Recombinant Enzymes

The gene of *Pa*BVMO (BVMO from *Pseudomonas aeruginosa*, NCBI Reference Sequence: WP_003087250.1) and *MI*ADH (ADH from *Micrococcus luteus*, NCBI Reference Sequence: ADD83022.1) was synthesized by Inovogen Ltd. (China), and the sequence was inserted into the plasmid pET28a (+) and pET22b (+) between the NdeI and HindIII restriction nuclease sites, respectively.

Site-directed mutagenesis was performed by the MutExpress II Fast Mutagenesis Kit V2, and the operations were undertaken according to the manufacturer's instructions. The code of primers utilized for mutagenesis are shown in Table 4.

Mutants		Primer
M1(D37G)	F	CGGCACTGCACCATAGGCCATCAC
	R	GGCCTATGGTGCAGTGCCGGC
M2(D37G-V39S)	F	GCTGCCGGGCTTGCACCATAGGCCATCAC
	R	GATGGCCTATGGTGCAAGCCCGGCAGCAC
M3(D37G-A38T-V39K)	F	GTGCTGCCGGCTTTGTACCATAGGCCATCAC
M3(D3/G-A301-V39K)	R	GATGGCCTATGGTACAAAGCCGGCAGCAC
M4(Y36S-D37G-A38D)	F	CTGCCGGCACGTCACCACTGGCCATCACTTTTTG
M4(1303-D3/G-A36D)	R	GTGATGGCCAGTGGTGACGTGCCGGCAGCAC
M5(Y36S-D37G-A38G-V39K)	F	GTGCTGCCGGGCTTCCACCACTGGCCATCACTTTTTG
	R	GTGATGGCCAGTGGTGGAAGCCCGGCAGCACTGG
M6(Y36S-D37G-A38D-V39K)	F	GTGCTGCCGGGCTGTCACCACTGGCCATCACTTTTTG
1410(1505-D57G-A56D-459K)	R	GTGATGGCCAGTGGTGACAGCCCGGCAGCACTGG

Table 4. Primers used for mutagenesis.

For expression, the plasmid was transformed into *E. coli* BL21 (DE3). The transformants were cultured in 100 mL TB medium at 37 °C and 200 rpm until the optical

density at 600 nm (OD₆₀₀) reached 0.6–0.8, followed by adding 200 μ M of isopropyl- β -D-thiogalactopyranoside (IPTG), and then cultured at 16 °C for 24 h. After culture, cells were harvested by centrifugation (8000 *g*, 10 min) and washed twice using Tris-HCl buffer (50 mM, pH 7.5). The crude extract was prepared using sonication (400 W, 15 min), and the soluble expression of recombinant enzymes was analyzed via SDS-PAGE and purified by His-tag through Ni-NTA affinity chromatograph [10].

3.4. Enzyme Kinetics Assay

The kinetic measurements were performed by monitoring the absorbance of NAD(P)H at 340 nm on a UV-spectrophotometer (Enspize, PerkinElmer) at 25 °C. The assay mixture (200 μ L) contained a final concentration of 0.5–2.5 mM of 10-hydroxy-octadecanoic acid, 0.1 mM NAD(P)⁺, 50 mM Tris-HCl buffer (pH 7.5), and an appropriate amount of purified enzyme. The kinetic parameters of the purified enzymes were assayed by the Michaelis–Menten equation and Hanes–Woolf method (Figure S3A–C) [34].

3.5. Sebacic acid Production with In Situ NADP⁺ Regeneration System

Unless otherwise stated, the enzymatic cascade reaction contains 1.0 mM 10-hydroxyoctadecanoic acid, 1 mM NAD(P)⁺, 10 μ L Tween 20, 0.5 mg/mL *Ml*ADH (or its mutants), 1 mg/mL *Pa*BVMO. The total volume of reaction was 20 mL (50 mM Tris-HCl buffer, pH 7.5). The reactions were carried out at 25 °C for 24 h.

After reaction, the extraction was carried out with ethyl acetate as solvent. Then, the products were hydrolyzed by KOH (1.0 M) at 80 °C for 2 h [10]. After that, the mixture was acidified to pH 2.0 with diluted HCl, following extraction with 1:1 (v/v) ethyl acetate. Finally, the solvent was dried under nitrogen and derived by *N*-methyl-*N*-(trimethylsilyl) trifluoroacetamide (TMS).

Then, the content of sebacic acid as the hydrolytic product of each cascade reaction was measured by GC-MS with following chromatographic conditions. GC-MS (Agilent 7890A-5975C) was equipped with a HP-5 ms capillary column (30 m \times 0.25 mm \times 0.1 μ m, J&W Scientific Columns, Agilent Technologies, Shanghai, China) [10]. Peaks were identified with a library search of NIST98 and standard sample analysis of each compound. GC-MS results (Figures S4–S6) were quantified using the peak area normalization method, and all measurements were conducted in triplicate.

4. Conclusions

Sebacic acid is an important chemical intermediate. With the development of enzymatic technologies, the multi-enzymatic cascade reaction makes it possible to produce sebacic acid from natural oleic acid. However, the problem of co-factor regeneration limited the progress of this biochemical technique. An efficiency and stable co-factor regeneration system for this in vitro enzymatic process is necessary.

In this study, with the switch of co-factor preference of native *MI*ADH from NAD⁺ to NADP⁺ dependent, a NADP⁺/NADPH in situ regeneration system is established between *MI*ADH and *Pa*BVMO. In silico simulation results indicated that the position of amino acid residue 37 is a key site for the co-factor preference. Except for residue 37, the residue sites of 38 and 39 also influenced the co-factor dependence. The experimental results demonstrated that the mutant of M1(D37G) and M3(D37G/A38T/V39K) would efficiently utilize NADP⁺, and the in situ co-factor regeneration system of *MI*ADH_D37G/A38T/V39K and *Pa*BVMO combination has a higher sebacic acid yield than the multi-enzyme regeneration system. All the results indicated that the investigation is beneficial for the sebacic acid production and is helpful for simplifying product isolation, thus, reducing the cost of the enzymatic transformations process. Furthermore, the method could also facilitate the co-factor regeneration system design for other related biotransformation processes.

Supplementary Materials: The following are available online at https://www.mdpi.com/article/ 10.3390/catal12111318/s1, Figure S1: Homology modeling results based on 4E12. Figure S2: The structure comparison of *MI*ADH-NAD⁺ with 4E12-NAD⁺. Figure S3: Determination of kinetic parameters by Hanes-Woolf method. Figures S4–S6: GC chromatography of different enzymatic reactions. Figure S7: Structure comparison of homology model from PDB: 4E12 and PDB: 6KQ9. Figure S8: Comparison of simulation results of homology model from 4E12 and 6KQ9 with reasonable mutation candidates. Figure S9: Simulation results of reasonable mutation candidates with PDB 6KQ9 as templet.

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