



Article

# The Positive Effect of Iron Doping in the Electrocatalytic Activity of Cobalt Hexacyanoferrate

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**Abstract:** The lack of an earth-abundant, robust, and fast electrocatalyst for the oxygen evolution reaction (water oxidation) is a major bottleneck for the development of an scalable scheme towards the production of electrolytic hydrogen and other synthetic fuels from renewable energy and natural feedstocks. While many transition metal oxides work reasonably well in basic media, very few alternatives are available in neutral or acidic media. One promising candidate comes from the Prussian blue family, cobalt hexacyanoferrate. This electrocatalyst offers robust activity in a large pH range (0 < pH < 13), although current densities are limited due to slow charge transfer kinetics. Herein, we report how the partial substitution of catalytically active Co centres by additional Fe boosts current densities, reaching over  $100 \text{ mA/cm}^2$ , more than double the performance of the parent Co<sub>2</sub>[Fe(CN)<sub>6</sub>]. Those new results clearly increase the opportunity for this catalyst to become relevant in industrial-ready electrolyser architectures.

Keywords: electrocatalysis; oxygen evolution reaction; Prussian blue analogues

#### 1. Introduction

Prussian blue analogues (PBA) have proven to exhibit a very rich and diverse electrochemistry [1,2]. Their redox properties can be tuned by stoichiometry and oxidation state of the constituent metal centres, incorporation of interstitial ions, or preparation methods. In the cyanide-bridged framework, which forms an infinite, porous 3D network, the d orbitals of C-bonded metal atoms are stabilised through  $d-\pi^*$  back-donation, while the d orbitals of N-bonded metals M' are destabilised due to a larger  $\sigma$ -donating character of the cyanide N-terminal. As a consequence, both positions are inequivalent, controlling the redox properties. In addition, the general deficiency of cyanometallates (M-M' < 1) generates a lattice of water molecules connecting the coordinatively unsaturated M' positions [3]. As a result, the M'-OH<sub>2</sub> centres are electroactive sites with interesting electrocatalytic redox properties [4–6]. Recently, they have been investigated as robust, earth-abundant catalysts for energy conversion applications, including some key processes, such as water oxidation/oxygen evolution (OER) [7–10], oxygen reduction [11–14], and hydrogen peroxide decomposition [15]. Cobalt hexacyanoferrates have been the most promising derivatives towards water oxidation catalysis in acidic and neutral media, thanks to the activity of the Co<sup>II</sup> active centres, whereas the coordinatively saturated Fe<sup>III</sup> moieties play an structural role, participating in the charge transfer dynamics [16,17].

In this direction, we reported how hexacyanoferrate vacancies in cobalt hexacyanoferrate could lead to a higher density of available electroactive Co-aqua sites. However, this gain was mitigated by a slower charge transport process [10]. Looking for chemical strategies to improve the OER catalytic activity of this family, we looked into doping alternatives. Among PBAs, the all iron Prussian blue exhibits the highest electrical conductivity due to its mixed valence nature, facilitating charge

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delocalization along the Fe <sup>II</sup>–C–N–Fe<sup>III</sup> bridges. With this in mind, we decided to investigat the effect of Fe doping on the electrocatalytic activity of cobalt hexacyanoferrate, as a means to improve charge transfer kinetics, intending to enhance its electrocatalytic performance. Here, we disclose how the substitution of Co <sup>II</sup> by Fe<sup>II</sup>/III</sup> enhances the OER activity of these PBA-based electrodes, allowing them to reach very high current densities, in neutral or acidic media, superior to other PBAs, but also to the corresponding phosphate-stabilised metal oxides in the same pH range.

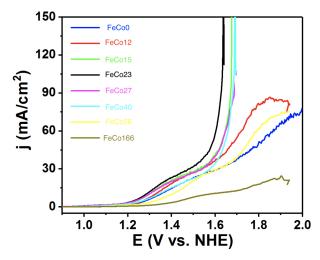
### 2. Results and Discussion

# 2.1. Electrode Preparation

For the preparation of PBA-modified electrodes, the good adhesion between catalyst crystallites and the underlying conductive substrate (fluoride-doped tin oxide, FTO) is essential to ensure fast electron transfer through the interface. So, we followed a chemical etching method [10] by transformation of a  $CoO_x$  film by liquid treatment with hexacyanoferrate. In order to incorporate additional Fe as the dopant in the Co positions, the corresponding Fe-doped  $CoO_x$  films were obtained by using a mixture of cobalt and iron precursor salts,  $Co(NO_3)_2$ ) and  $Fe(NH4)_2(SO_4)_2$ , in the desired stoichiometry for the preparation of the initial Fe-doped  $CoO_x$  film under hydrothermal conditions (see methods section for details). In a second step, the oxide film was transformed into the PBA structure by treatment with an aqueous solution of hexacyanoferrate. The stoichiometry of the intermediate oxide films, and that of the final PBA films, were determined by EDX analysis. The ratio in the as-prepared oxo-hydroxide was in perfect agreement with that of the starting reagents during the synthesis. The oxo-hydroxide transformation into the packed Fe-doped PBA produces an enrichment in Co in the final products, with general formula  $Fe_xCo_{2-x}[Fe(CN)_6]$  (Table S1). For clarity, all samples are labelled as  $FeCo_Z$ , (Z = x/(2-x)), according to the Fe/Co ratio (Z) in the water-bound position in the cubic network. All M(CN)<sub>6</sub> positions are occupied by Fe coming from the hexacyanoferrate precursor.

### 2.2. Electrocatalysis in Neutral pH

The OER activity of **FeCo***Z* electrodes was investigated by linear sweep voltammetry (Figure 1). The Fe doping does not significantly affect the onset overpotentials, which are almost identical following an analogous trend during the low current regime. Indeed, the Tafel regime is almost identical for all derivatives, with all Tafel slopes in a very narrow range of  $\pm 10$  mV/decade (Figure S1), in good agreement with the original **FeCoo** [10]. This suggests no major changes in the rate-limiting step, and no modifications in the mechanistic pathway.

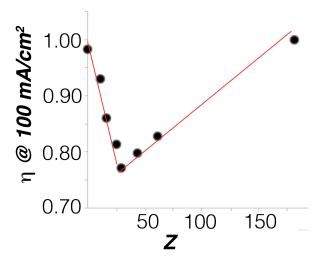


**Figure 1.** Linear sweep voltammetry recorded (1 mV/s) for the **FeCo**Z electrodes. Electrolyte: 0.1 M KPi + 1 M KNO<sub>3</sub>, pH = 7.

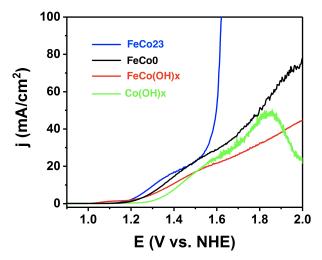
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However, significant differences appear at higher overpotentials, where the parent FeCo0 enters the diffusion limited range. As Co is substituted by Fe, enhanced currents appear. FeCo12 already shows a better response, and the initial diffusion limited range is overcome above FeCo15, while the current density keeps increasing very fast, reaching values above  $150 \text{ mA/cm}^2$ . This enhancement reaches its maximum for about 20% Fe doping, with additional increments in Fe content becoming detrimental. Overall performance becomes worse than in the original FeCo0 for Z > 1. This trend is in agreement with our initial hypothesis. Fe doping is not directly improving (at least significantly) the catalytic activity of the Co centers, but improving the charge transfer, allowing to reach higher current densities. However, as Fe doping increases, this also decreases the density of active sites, since Fe is not active for OER at this overpotentials and conditions, as confirmed by the inactivity of the all iron Prussian blue [18].

Taking the overpotentials at 100 mA/cm<sup>2</sup>, a volcano trend was found, indicating an optimum composition around 20 % for FeCo23 (Figure 2). We compared the activity of this FeCo23 with that of both oxo-hydroxide precursors, FeCoO<sub>x</sub> and Co(OH)<sub>x</sub>—intermediate phases in its preparation. As shown in Figure 3, FeCo23 performance is superior to all of them, especially at high current densities, easily reaching 100 mA/cm<sup>2</sup> when all other catalysts are entering what appears to be a diffusion limited regime (Table S2).



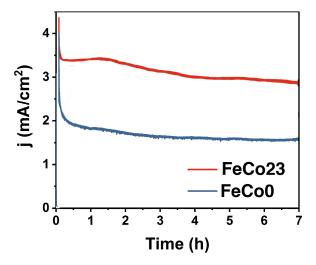
**Figure 2.** Plot of the overpotential ( $\eta$ ) needed to reach a current density of 100 mA/cm<sup>2</sup> in the series of **FeCo**Z anodes. Electrolyte: 0.1 M KPi + 1 M KNO<sub>3</sub>, pH = 7.



**Figure 3.** Comparative linear sweep voltammetry (1 mV/s) for the **FeCo23** compared with the related oxo-hydroxides. Electrolyte:  $0.1 \text{ M KPi} + 1 \text{ M KNO}_3$ , pH = 7.

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To confirm the electrocatalytic durability in water oxidation conditions, amperometric measurements were performed at an applied overpotential of 425 mV (Figure 4). FeCo23 displayed relatively stable electrocatalytic activity, analogous to the parent CoFe PBA. We characterised the electrocatalysts after eight hours under aqueous electro-oxidation conditions to identify any change or evolution in their structure, composition, or morphology. Electron microscopy confirmed the cubic structure is well-preserved, without suffering any significant changes in size, homogeneity, or aggregation (Figure S2). Elemental analysis did not show any evidence of leaching, or additional changes on catalysts composition. Further characterisation with Raman spectroscopy, a surface sensitive technique, confirmed no significant surface evolution occurs during working conditions (Figure S3), suggesting these catalysts are robust, and genuine catalysts in these conditions.

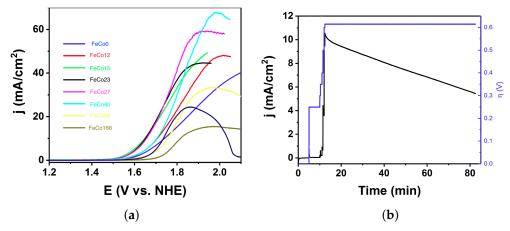


**Figure 4.** Comparative chronoamperometry with **FeCo23** or **FeCo0** electrodes. Electrolyte:  $0.1 \text{ M KPi} + 1 \text{ M KNO}_3$ , pH = 7.

### 2.3. Electrocatalysis in Acidic pH

One of the most promising features of PBAs is their stability in acidic environments, where only noble metals are suitable electrocatalysts for OER, due to the intrinsic instability of alternative earth-abundant metal oxides. The latter just dissolve in such working conditions [19–21]. Indeed, **FeCo0** was already incorporated into polymer electrolyte membrane (PEM) electrolysers with promising results [22], limited by the slow charge transfer of this material, requiring additional conducting support. The FeCoZ series shows enhanced performance for OER in acidic media (Figure 5a). For instance, the current density still rises sharply in a  $H_3PO_4$  pH = 1.5 solution with KNO<sub>3</sub> (1 M) electrolyte. However, at this pH, the performance is not as robust as in neutral media. We found a continuous decrease with time at pH < 1.5 (Figure 5b).

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**Figure 5.** (a) Linear sweep voltammetry (1 mV/s) with FeCoZ electrodes. (b) Chronoamperometry with a FeCo23 electrode. Electrolyte:  $H_3PO_4$  pH = 1.5 solution with KNO<sub>3</sub> (1 M) electrolyte.

#### 3. Conclusions

In summary, we have demonstrated the validity of our initial hypothesis. The slow charge transfer kinetics of the water oxidation electrocatalyst  $Co_2[Fe(CN)_6]$  can be overcome by doping with Fe in the series  $Fe_xCo_{2-x}[Fe(CN)_6]$ , based on the positive effect of the mixed-valence nature introduced by the  $Fe^{II}$ –CN–Fe<sup>III</sup> pairs. We found optimum performance in  $x\approx 0.4$ . The enhancement is particularly relevant at high current densities, one of the flaws of PBAs, for which it was able to support robust OER, but at limited currents. In the past, combination with conducting supports and nanostructuration were tested as plausible solutions to the problem. This new strategy opens an easier and simple alternative for further implementation into industrial electrolysers.

#### 4. Materials and Methods

[Fe $_x$ Co $_{(2-x)}$ [Fe(CN) $_6$ ]: Iron and cobalt oxo/hydroxides were prepared following a procedure from the literature [10], using a Co/Fe mixture with the desired ratio. Briefly, Co(NO $_3$ ) $_2 \cdot 6$  H $_2$ O (77.5 mg), the desired stoichiometric amount of Fe(NH $_4$ ) $_2$ (SO $_4$ ) $_2 \cdot 6$ H $_2$ O, and urea (80.8 mg) were dissolved in 10 mL MilliQ water and transferred into a 20 mL Teflon-lined autoclave, with a FTO glass substrates immersed in the solution. The autoclave was maintained at 120 °C for 10 h and then cooled down to room temperature in air. Then, the coated FTO glass was rinsed with MilliQ water several times. Subsequently, the electrode was immersed in 9 mL of the freshly prepared K $_3$ Fe(CN) $_6$  aqueous solution (800 mg/100mL) in a sealed glass vial and heated at 60 °C for 24 h. During the reaction, the oxide starting material dissolved, being substituted by the Prussian blue derivative with the stoichiometry defined by the initial film. Finally, the electrodes were gently rinsed with MilliQ water, and left in an acid bath overnight to remove any remaining traces of oxo-hydroxide.

All electrochemical experiments were performed at the ambient conditions with a Bio-Logic VMP3 multichannel potentiostat/galvanostat. The three-electrode configuration was completed with a saturated calomel electrode (SCE) reference electrode, and a Pt mesh counter electrode. All potentials were measured against SCE, and are reported versus the normal hydrogen electrode (NHE) using the equation of E(NHE) = E(SCE) + 0.244 V. Overpotentials were computed using  $\eta = E(NHE) - 1.229 + 0.059$  pH. Ohmic drop was corrected for all electrochemical data by using the automatic current interrupt (CI) method implemented by the potentiostat software. In all cases, 0.1 M of phosphate buffer (KPi) solution at pH = 7 was firstly prepared by dissolving appropriate amounts of  $K_2HPO_4$  and  $KH_2PO_4$  solid in 1 M KNO3 solution. The pH was gradually increased or decreased by adding aliquots of concentrated KOH solution or concentrated  $H_3PO_4$  in pH = 7, 0.1 M KPi + 1 M KNO3 solution, while monitoring with pH meter. All cyclic voltammograms (CVs) were measured in a three-electrode, one-compartment configuration with 50 mL aqueous phosphate buffer solution. Linear sweep voltammetry (LSV) data were collected at a scan rate of 1 mV/s, unless otherwise noted.

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Chrono-potentiometric or chrono-amperometric measurements (CPs) were recorded at a constant current density in a fritted H-shaped cell under vigorous stirring. The platinum mesh electrode was inserted into one compartment (cathodic reaction), while the modified working electrode and a reference electrode were inserted in the anodic compartment. Steady-state current densities for Tafel analyses were collected at a variety of applied potentials during oxygen evolution at a constant pH. At each potential, the current was stabilised for 10 min to attain a steady-state value that was averaged for 30 s under stirring. All data were recorded at least three times from three different samples, finding good repeatability, with no significant deviations within experimental error.

Scanning electron microscopy (SEM) micrographs were acquired on an FEI Quanta 650 FEG ESEM, 20 kV, equipped with an Oxford EDX analyser (Oxford Instruments, Abingdon, UK). A total of 5 nm Pt was deposited onto the as-prepared PBA samples for SEM checking by using magnetron sputtering LEICA EM ACE600. Infrared transmittance spectra were recorded on a FTIR-ATR Cary 630 TR1 Ph2 spectrometer in the 4000–400 cm<sup>-1</sup> region. Raman spectroscopy was collected with a Renishaw in Via Reflex Raman confocal microscope, Gloucester-Shire, UK, light source: 514 nm.

**Supplementary Materials:** The following are available online at http://www.mdpi.com/2073-4344/10/1/130/s1. Figure S1: Tafel plot obtained with **CoFe23** electrodes in pH 7 KPi electrolyte. Figure S2: SEM images of as-prepared **CoFe23**, and after 10 h electrolysis at  $\eta = 500$  mv in pH 7 KPi electrolyte. Figure S3: Raman spectra of as-prepared **CoFe0**, **CoFe23**, and **CoFe166**; and of **CoFe23** after 10 h electrolysis at  $\eta = 500$  mv in pH 7 KPi electrolyte. Table S1: Metal ratio in reagents, and final products for the series Fe<sub>x</sub>Co<sub>2-x</sub>[Fe(CN)<sub>6</sub>]. Table S2: Overpotentials required to reach an specific current density in the **FeCoZ** series.

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Conflicts of Interest: The authors declare no conflict of interest.

#### **Abbreviations**

The following abbreviations are used in this manuscript:

PBA Prussian blue analogues

OER Oxygen evolution reaction

FTO Fluoride-doped tin oxide

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