

## Article

# Experimental and Modeling Study on the Removal of Mn, Fe, and Zn from Fiberboard Industrial Wastewater Using Modified Activated Carbon

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**Abstract:** In this work, the use of agricultural waste from oil palm petioles (OPP) as a raw material for the production of activated carbon (AC) and its characterization were examined. By soaking these chars in nitric acid (HNO<sub>3</sub>) and potassium hydroxide (KOH) at a 10% concentration, AC with favorable high-porosity carbons was generated. To maximize AC synthesis, the AC was pyrolyzed at 460, 480, and 500 °C temperatures for 20 min. Based on micrographs of formed pores and surface functional groups, 480 °C carbonization temperature on both chemical HNO<sub>3</sub> and KOH was shown to be the best. The FTIR measurements reveal that chemical activation successfully transformed the raw material into AC. Moreover, FESEM micrographs show the pores and cavities of the prepared AC achieve a high surface area. This is further supported by BET results of HNO<sub>3</sub> OPP AC and KOH OPP AC with surface areas of 883.3 and 372.4 m<sup>2</sup>/g, respectively, compared with the surface area of raw OPP of 0.58 m<sup>2</sup>/g. Furthermore, the tests were revealed by an optimization model, namely response surface methodology (RSM), using a central composite design (CCD) technique. The findings showed that all three parameters (pH, time, and dose) had a substantial impact on the removal of Zn, Fe, and Mn. Analysis of variance (ANOVA) and analytical error indicated that the models were accurate, with a low error value and a high R<sup>2</sup> > 0.9. Remarkably, the good correlation between actual and predicted removal values showed that the modified activated carbon is a promising adsorbent for heavy metal removal from wastewater.

**Keywords:** oil palm; activated carbon; fourier transform infrared spectroscopy (FTIR); field emission scanning electron microscopy (FESEM); response surface methodology (RSM)



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## 1. Introduction

Fiberboards are wood fiber agglomerates which are mainly used for furniture manufacture. This product has been on the increase for years, given its high resistance, stability, and quality finish, coupled with reasonable costs. In the fiberboard industry, the processing procedure has harmful effects on the aquatic environment due to important concentrations of dangerous chemicals. These products require the use of large quantities of water. According to Kloch and Toczyłowska-Mamińska [1], the plants producing wood-based panels use between 0.1 and 1.5 m<sup>3</sup> of water per 1 m<sup>3</sup> of panel produced, and they estimated that the global wood-based panel industry can generate up to 600 million m<sup>3</sup> of wastewater every year.

One of the most water-consuming processes during wood-panel processing is wood chip washing [2]. Leaching takes place when the chips are being washed. Metal ions, such as calcium, potassium, manganese, magnesium, and iron, are naturally occurring components in wood [3]. The extraction of organic acids from the wood gives the wastewater a low pH of 5.5 [4]. Santos et al. [5] detected several heavy metal ions from wood chip leachings such as copper, iron, and manganese. This is also in line with [6] findings, whereby, during the woodchip flushing analysis, metal ions as such copper (Cu), aluminum (Al), zinc, manganese (Mn), barium, and iron (Fe) was detected.

Some heavy metals are required in small amounts by humans, but the majority of them are harmful even at low concentrations and toxic at higher concentrations. Heavy metals specifically are more dangerous owing to their non-biodegradability [7]. Regardless of wood species, the majority of wood chip leaching shows significant solute metal ions. The phenomenon results from different conditions of wood treatment and different origins of logs [1]. Consequently, the degradation of such toxic substances in wastewater is a significant processing problem and of high importance. Furthermore, the current environmental regulations have restricted their ultimate discharge into water bodies [2].

Extensive research has been conducted over the past years to find low-cost, high-capacity adsorbents for metal ion removal [8,9]. Activated carbon has been gaining attention from researchers, especially as a contaminant removal media worldwide. It has long been recognized as an effective adsorption material due to its large surface area, large number of surface-active adsorption sites, and high adsorption capacity. Activated carbon can be manufactured from any type of carbonaceous material. In commercial practice, the most common raw materials used are coal, peat, lignite, wood, and coconut shell [10–12]. However, according to Bakar et al. [13] and Duan et al. [10], commercial activated carbons are very expensive and non-renewable. Thus, many researchers have shifted to developing a new low-cost activated carbon from waste material that is more affordable and abundantly available [14,15]. El-Bendary et al. [14], for example, modified corn cobs and luffa using aluminum chloride as effective low-cost adsorbents for the removal of Fe(III) from aqueous solutions. Additionally, the increased demand for the commercial adsorbent activated carbon has caused its price to rise. Therefore, by converting the commercial adsorbent into agricultural waste, according to Ayob et al. [15], this process is more environmentally friendly.

In Malaysia, oil palm plantations have produced 135 million tons of agricultural waste annually [16]. Oil palm fronds are one of the massive wastes in oil palm plantations [17]. Dungani et al. [16] and Said et al. [18] estimated that 4.16 million tons of frond waste is from replanting activities, and 51.66 million tons are from pruning activities. Previous studies have shown that different parts of oil palm waste can be utilized as activated carbon, i.e., empty fruit bunches [19–21], palm kernel shell, mesocarp fibers, and trunks [6]. A study from Ujile and Okwakwam [22] used empty fruit bunches (EFB) as activated carbon, and they were able to remove 57% of iron, 99.6% of copper, and 90% of cadmium. Meanwhile, a study from Baby and Hussein [23] shows that oil palm kernel shells impregnated with phosphoric acid removes 99% of chromium, 80% of cadmium, 80% of zinc, and 99% of lead.

Similar to other biomaterials, activated carbon generated from oil palm waste is normally developed via physical or chemical activation [24]. Physical activation is a two-stage process that begins with carbonization in the presence of inert gas and ends with activation with the help of an oxidizing gas, while chemical activation, often known as “wet oxidation”, is a one-stage process in which carbonization and activation occur concurrently [11,13,25]. Both kinds of activation have advantages and disadvantages; nevertheless, chemical activation is preferred by researchers due to its low heating temperature, quick processing time, high carbon yield, well-controlled porosity, and high specific surface area [10,25].

Chemical activation has long been known and used in the production of biomaterials such as activated carbon. One of the important elements in chemical activation is the type of activating agent used. The main functions of chemical reagents are to degrade or dehydrate

the organic components during the activation process to suppress the depolymerization of hydrocarbons on the carbon surface [10]. Activating agents may be grouped into four groups based on the acid–base theory and activation mechanism, such as alkaline, acidic, neutral, and self-activating agents [25]. These types of activating agents will react differently with carbon precursors and lead to various activation mechanisms [25].

An efficient statistical method known as Response Surface Methodology (RSM) offers an exploratory approach to optimization. Additionally, it is a set of mathematical and statistical methods used to maximize the relevance of several influencing elements, even when complicated interactions are present [24]. The primary goal of using RSM is to identify the optimum operating parameters for the process or an area that complies with the operating requirements [25]. By integrating RSM with a central composite design (CCD) approach to optimize all the influencing factors simultaneously, the limitations of standard analytical optimization methods may be completely removed [26].

Thus, in this study, activated carbon derived from oil palm petiole (OPP) is prepared using two different types of activating agents, namely acid and alkaline. The effect of the activating agent on the physio-chemical characteristics and adsorption efficiency of activated carbons (AC) was identified and further discussed. Moreover, the AC was evaluated for the simultaneous adsorption of three different metal ions that represented contaminants in fiberboard processing industrial wastewater. Furthermore, Expert Design Software version 13 was used to evaluate the predicted removal (%) of Zn, Fe, and Mn from aqueous solution by KOH-impregnated AC and impregnated HNO<sub>3</sub>. In order to optimize the three parameters (pH, adsorbent dose, and contact time) that affect the removal of Zn, Fe, and Mn metals, the RSM model with a central composite design (CCD) technique was applied. Additionally, to validate the accuracy of the models, the performance of the model was evaluated using statistical analysis and coefficient of determination (R<sup>2</sup>).

## 2. Materials and Methods

### 2.1. Material Preparation

Oil palm fronds were collected from a local oil palm plantation located at Kg. Rahmat, Batu Pahat, Johor. The leaf was exiled from the oil palm fronds and only the petiole of the oil palm was employed in this study, as shown in Figure S1 (The Picture of oil palm petiole (OPP) that has been extracted from oil palm fronds). The OPP was parched for 2 weeks and pretreated using hydrochloric acid to remove visible dirt and accumulation of impurities from the surface before being oven-dried. The oven was set to 80 °C and left for 24 h to remove all moisture content. For activation, two types of impregnation chemicals were prepared, namely potassium hydroxide (KOH) ( $\geq 85\%$ , pellets) and nitric acid (HNO<sub>3</sub>) ( $\geq 70.0\%$ ) purchased from Sigma-Aldrich (Burlington, MA, USA) (M) Sdn Bhd. Dried OPP was soaked in 1000 mL of 10% diluted KOH or HNO<sub>3</sub> and left for 24 h. Subsequently, the impregnated OPP was dried in an oven and carbonized using a muffle furnace with activation temperatures of 460, 480, and 500 °C. The activation temperature was selected, based on the findings of the thermogravimetric analyzer (TGA) analysis.

### 2.2. Material Characterization

The physicochemical features and morphological structure of OPP were investigated. Lignocellulose analysis was carried out to determine the presence of crude fibers such as cellulose, hemicellulose, and lignin in OPP. A simple standard was adopted in this analysis in order to extract three different detergent fibers, namely natural detergent fiber (NDF), acid detergent fiber (ADF), and acid detergent lignin (ADL) using fiber hot and cold extraction. Prior to the analysis, the OPP precursor was ground into small pieces (75 mesh) and oven-dried (80 °C) until the constant weight was less than 1% within 24 h.

Thermal decomposition analysis was carried out by using a thermogravimetric analyzer (TGA) before the carbonization process. TGA analysis was performed using a TGA Instruments 500. Ten mg of OPP was placed in a platinum pan. The samples were

then heated under the nitrogen atmosphere at 30 mL/min at 10 °C min<sup>-1</sup> with the heating rate equilibrated at 30 °C to 900 °C [27].

For qualitative analysis, FTIR and Field Emission Scanning Electron Microscope (FESEM) analysis were carried out. For FESEM analysis, a JFM 7200F Field Emission Scanning Electron Microscope (JEOL, Tokyo, Japan) with electron beam lithography was used. Prior to the analysis, each sample was sputtered with gold using the JFC-1600 Auto Fine Coater (JOEL, Tokyo, Japan) for 40 s at 30 mA under a high vacuum until they were completely covered. The purpose of sample sputtering is to avoid charges dissipating during imaging.

Next, the FTIR spectrometer (Perkin Elmer Spectrum 100, Waltham, MA, USA) was employed in this study to determine the presence of surface functional groups in OPP. The spectra were set to the range of 4500–500 cm<sup>-1</sup> for all the samples. The activated carbon's specific surface area and pore distribution were determined with a multiple-point Brunauer, Emmet, and Teller (BET) gas adsorption measurement using the Micromeritics ASAP 2020 operated at 77 K. The t-plot micropore volume was used to compute the micropore volume. The amount of N<sub>2</sub> adsorbed at relative pressures near unity ≈ 0.99 corresponds to the total amount adsorbed (VT) in both the micropores and the mesopores; consequently, the subtraction of the micropore volume from the total amount will provide the volume of the mesopores [28,29]. The pore size distribution will be determined by using Barrett Joyner Halenda's (BJH) model.

The production of activated carbon was further discussed in terms of yield. The yield of OPP activated carbon (OPP-AC) was applied to calculate the following Equation (1):

$$\text{Yield (\%)} = \frac{W_i - W_f}{W_i} \times 100 \quad (1)$$

where  $W_i$  is the initial weight and  $W_f$  is the final weight.

### 2.3. Batch Adsorption

In order to determine the efficiency of AC produced, batch adsorption was carried out. Wastewater from the fiberboard industry was used as polluted water media. The initial investigation found that zinc (Zn), manganese (Mn), and iron (Fe) were the highest metal concentration in this wastewater; thus, these elements were chosen to be further treated. The batch adsorption study is investigated through optimum parameters. The optimal adsorption removal and adsorption capacity of a composite adsorbent were investigated under several conditions, including pH, adsorbent dosage, and contact time [30].

The pH range of the heavy metals (Mn, Fe, and Zn) was specified to be observed between acidic 6 and alkaline 14, or (6, 8, 10, 12, and 14). To achieve the optimum pH for heavy metal removal, the dose, shaking speed, contact time, and solution volume were kept constant at 0.2 g, 100 revolutions per minute, 90 min, and 100 mL, respectively. The impact of adsorbent dose was next examined by measuring the optimum pH value. According to our early research, the dose was set at 0.1, 0.2, 0.3, 0.4, 0.5, and 0.6 g/mL in order to determine the optimum dosage for heavy metal removal. According to our preliminary investigation, the impact of contact time was tested using 100 mL of wastewater with 0.2 g and 0.3 of KOH-impregnated AC and HNO<sub>3</sub>-impregnated AC adsorbent dose, respectively, with 100× g of shaking speed and contact time varied from 0 to 180 min.

The concentration difference between before and after the removal was used to calculate the Zn, Fe, and Mn ions' removal percentage (R%) as follows [31]:

$$(\text{R}\%) = \frac{C_i - C_e}{C_i} \times 100 \quad (2)$$

where:  $C_i$ : The initial concentration of Zn, Fe, and Mn ions in mg/L;  $C_e$ : The final concentration of Zn, Fe, and Mn ions in mg/L;  $M$ : The mass of KOH-impregnated AC and HNO<sub>3</sub>-impregnated AC adsorbent (g);  $V$ : The volume of the solution (L)

#### 2.4. Design of Experimental Using RSM

The statistical design of experiments and data analysis were performed using Design Expert Software (version 13). RSM was used in this investigation to evaluate the relationships between the responses (Zn, Fe, and Mn removal%) and the independent factors (pH, adsorbent dose, and contact time), as well as to improve the necessary conditions of the variables in order to predict the optimal value of the responses. Among other RSM designs, CCD was used to examine the effects of the three components individually and together on the responses [32]. In order to analyze the interactions between parameters, CCD is suited for fitting a quadratic surface and aids in optimizing the effective parameters with a minimal number of tests [33]. Three factors were taken into account: pH ( $X_1$ ), adsorbent dose ( $X_2$ ), and contact time ( $X_3$ ). We selected these three variables and their associated ranges based on our initial study.

Table 1 lists the levels and ranges of the variables analyzed. The efficiency of Mn, Fe, and Zn removal was examined to assess the process' performance. Based on some exploratory studies, each independent variable was adjusted at the indicated ranges among two levels of +1 and 1. Twenty tests were completed overall for the three factors ( $=2^k + 2k + 6$ ), where  $k$  is the total number of factors ( $k = 3$ ) [34]. Six replications were added to fourteen trials to help determine the simple error. The quadratic model is the proper one, since there are only two levels for each factor:

**Table 1.** Independent variables and their coded levels for CCD.

	Name	Units	Low	High	−Alpha	+Alpha
A [ $X_1$ ]	pH		6	14	3	14
B [ $X_2$ ]	Dosage	g/L	0.1	0.5	−0.05	0.7
C [ $X_3$ ]	Time	Min	15	180	−47	242

Analysis of variance (ANOVA) is used to evaluate and determine the importance of each variable as stated in Equation (3) [34]:

$$Y = \beta_0 + \sum_{i=1}^k \beta_i \chi_i + \sum_{i=1}^k \beta_{ii} \chi_i^2 + \sum_{i=1}^k \beta_{ii} \chi_i^2 + \sum_{i=1}^{k-1} \sum_{j=i+1}^k \beta_{ij} \chi_i \chi_j + \varepsilon \quad (3)$$

where  $Y$  is the observed responses,  $\chi_i$  is the independent variables, and  $\beta_0$  is the constant variables;  $\beta_i$ ,  $\beta_{ii}$ , and  $\beta_{ij}$  represent the coefficients for linear, quadratic, and interaction effects, respectively, and  $\varepsilon$  denotes the random error.

Contour plots and 3D surfaces are used to analyze the interactions and ideal operating conditions for heavy metal removal [35]. To determine the interaction between the process factors and the replies, graphs of the data were analyzed using analysis of variance (ANOVA). The coefficient of determination ( $R^2$ ) and analytical error analysis was used to describe how effectively the model matched the data [36]. Model F-value (Fisher variation ratio) and probability value (Prob > F) were the primary metrics used to show the model's applicability and significance.

#### 2.5. Analytical Error Analysis

To determine the best fitting of models onto removal data, the error function must be calculated [37]. It is necessary to analyze error functions in order to assess how well the models match the experimental data. The coefficient of determination ( $R^2$ ) is probably the function that is used the most often in research to choose the best models [38]. The best-fit model is selected based on the size of the coefficient of determination. The best match is often considered to be the model with the greatest coefficient of determination value ( $R^2$ ) [39]. Additionally, the fit for the removal data is improved by reducing the numerical value of the error functions for a particular model. The following are the formulas for the coefficient of determination and other error functions.

### 2.5.1. Coefficient of Determination ( $R^2$ )

The coefficient of determination ( $R^2$  or r-squared), which measures the percentage of variation in the dependent variable that can be explained by the independent variable, is a statistical metric used in regression analysis. Additionally, the coefficient of determination shows how well the data match the model (the goodness of fit). The possible values are 0 to 1 for the coefficient of determination. Additionally, this is how the statistical metric is often expressed [38]:

$$R^2 = 1 - \frac{\sum_{i=1}^n (M_t - A_t)^2}{\sum_{i=1}^n (A_t - A_{\bar{x}})^2} \quad (4)$$

### 2.5.2. Mean Square Error (MSE)

The most used error measure is probably mean square error (MSE). Due to the higher effect of squaring bigger numbers than smaller ones, it penalizes larger mistakes. The MSE is calculated as follows by dividing the total squared errors by the total number of observations:

$$MSE = \frac{1}{n} \sum_{i=1}^n (A_t - M_t)^2 \quad (5)$$

### 2.5.3. The Root Mean Square Error (RMSE)

The root mean square error (RMSE), which may be expressed as the following equation, is the square root of the mean square error (MSE):

$$RMSE = \sqrt{\frac{1}{n} \sum_{i=1}^n (A_t - M_t)^2} \quad (6)$$

### 2.5.4. The Mean Absolute Deviation (MAD):

The total absolute difference between the actual value and the prediction divided by the number of observations is the mean absolute deviation (MAD), which can be written as the equation below:

$$MAD = \frac{\sum_{i=1}^n |A_t - M_t|}{n} \quad (7)$$

### 2.5.5. Mean Absolute Percentage Error (MAPE)

The following is how to express mean absolute percentage error (MAPE), which is the average of absolute errors divided by the actual observation values:

$$MAPE = \frac{\sum_{i=1}^n \left| \frac{A_t - M_t}{A_t} \right|}{n} \quad (8)$$

where:  $A_t$ : Experiment data,  $M_t$ : Model date,  $n$ : number of experiments carried out.

## 3. Results and Discussion

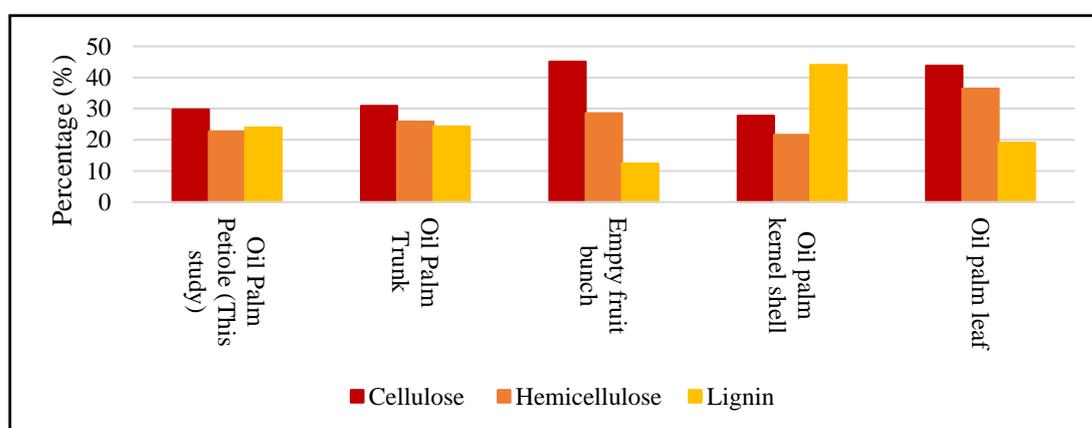
### 3.1. Cellulose, Hemicellulose, and Lignin Content

Lignocellulosic material is regarded as a mixture of cellulose, hemicellulose, and lignin. Cellulose and hemicellulose are made up of carbohydrates and make up holocellulose [40]. Cellulose is a glucose-based linear polymer with extra hydrogen bonds that make it hard, solid, and difficult to break. Hemicellulose, on the other hand, is found in secondary cell walls and is made up of tiny, highly branched chains of different pentoses and hexoses. Meanwhile, lignin, a very complex substance with a three-dimensional cross-linked polyphenolic structure, is present between the cellulose and hemicellulose cell walls [18].

Lignocellulose elements play an important role in the development of AC. According to Yunus et al. [41], materials with high lignin content developed AC with high macropores and materials with high cellulose yield developed AC with a predominantly microporous

structure. Among these elements, lignin presents a significant advantage because it is resistant to chemical and biological degradation. Lignin is also said to be the most abundant component of charred materials. In addition, according to Baker et al. [13], lignin content appeared to correlate with the fixed carbon content and increased significantly after carbonization. The adsorption process is also strongly influenced by the chemical composition of the lignocellulosic fibers, especially the –OH and aromatic groups [40].

Figure 1 classifies the lignocellulosic of OPP from this study and other oil palm waste used as precursors for AC preparation. The results show that OPP has a high quantity of cellulose and a moderate amount of lignin, with values of 25.95 and 16.81%, respectively. This was also in line with Said et al. [18], who said that cellulose is the most essential element of oil palm biomass. In view of AC production, biomass with greater hemicellulose and cellulose content will almost certainly require a high conversion rate during carbonization [42]. In the present study, the percentage amount of cellulose in OPP is lower than in other types of palm oil biomass. Thus, the time taken for the degradation on OPP was relatively shorter, and the lower temperature was used to degrade the biomass constituents.



**Figure 1.** Lignocellulosic of OPP and other oil palm waste used as precursors for AC preparation.

By comparing the range of ash of the other precursors, it was found that OPP gives a lower percentage of ash, which was 1.71% [43,44]. This value was also less than the maximum limit set by ASTM D-2866-94, which was 5%. The purpose of measuring the ash content of activated charcoal is to quantify the metal oxide content of AC and also as an indication of high-grade carbon. In this study, OPPs are ideally suited to be employed as AC's precursor.

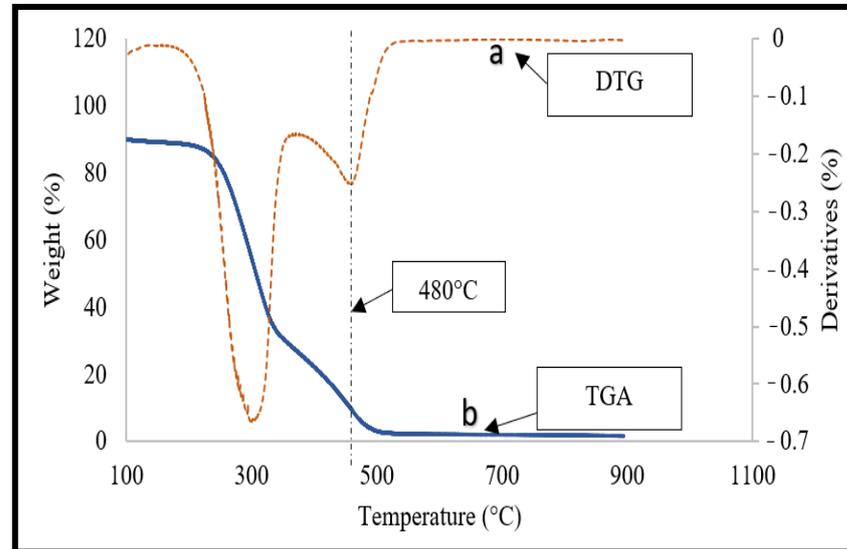
### 3.2. Thermal Degradation (TGA Analysis)

The pyrolysis weight loss profiles (TGAs) and related derivative weight loss profiles (DTGs) of OPP were generated using heat rates of  $10\text{ }^{\circ}\text{C min}^{-1}$  in an inert nitrogen flow, as shown in Figures 2 and 3. The peak appearance in the DTG profile that corresponds to the greatest mass loss rate is represented by the temperature ranges for the peak appearance.

When the heating rate is increased, the TGA and DTG profiles are shifted from about  $30\text{ }^{\circ}\text{C}$  to a higher temperature profile (i.e., towards the right). Aside from that, increasing the heating rate leads to less weight loss, as shown by the TGA profile (Figure 2). Poor heat transmission from the surrounding environment to the inside of the solid is thought to be responsible for this occurrence. When the heating rate is high, the biomass has a shorter residence time to devolatilize, resulting in a greater concentration of solid residue.

It should be noted that although increasing the heating rate skews the TGA and DTG profiles towards the higher temperature side, it does not change the shape of either the TGA or DTG profile. In accordance with the TGA profile, the pyrolysis of OPP proceeded in three major phases, i.e., (I) moisture evaporation and light volatiles removal ( $30\text{--}80\text{ }^{\circ}\text{C}$ ), (II) rapid de-volatilization, mostly degradation of hemicellulose ( $80\text{--}340\text{ }^{\circ}\text{C}$ ),

(III) char formation from the degradation of cellulose, and the slow de-volatilization of lignin (340–480 °C), and (IV) > 480 °C shows a horizontal line, which represents the depletion of fixed carbon and the amount of final unburned residual called ash content at the final temperature. The results are comparable with another study conducted by Nyamful et al. [45], which utilized oil palm kernel shells as activated carbon.



**Figure 2.** DTG (a) and TGA (b) curve of raw-OPP.



**Figure 3.** (a) OPP-AC after activation process using KOH (b) OPP-AC after activation using HNO<sub>3</sub>.

Hence, from the TGA and DTG results, the carbonization temperatures of 460, 480, and 500 °C were set for this study, since it involved a variety of low, medium, and high temperatures in order to obtain an optimum yield, in addition to having good physicochemical properties.

### 3.3. Yield Percentage

Yield analysis was carried out in order to predetermine the capability of oil palm petiole-activated carbon (OPP-AC) as an adsorbent. The yield of OPP-AC was calculated by dividing the mass of the resultant AC by the initial mass of the raw material used for activation described in Equation (1) [46]. The percentage yield of OPP-AC is performed at various carbonization temperatures and expressed in Table 2.

The results show that the yields of OPP-AC impregnated with KOH are higher than HNO<sub>3</sub>. The ranges were 60–90 and 40–60%, respectively. The yield is comparable to that obtained in Maulina and Anwari's [47] studies, which also utilized oil palm waste as AC. Moreover, according to Ukanwa et al. [48], the use of KOH, in the temperature range of 230–650 °C, results in a high char yield. Temperatures of 460 °C to 480 °C resulted in a significant increase in yield, which then gradually decreased at 500 °C. This was in

agreement with TGA analysis results, whereby after 480 °C the profile shows a horizontal line, which represents the depletion of fixed carbon and indirectly affects the final weight of OPP-AC.

**Table 2.** Percentage yield of activated carbon from oil palm petiole.

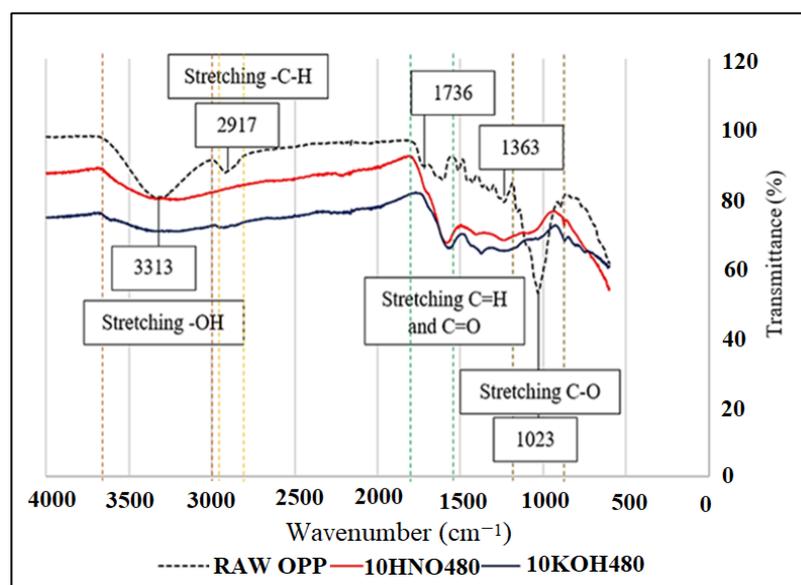
Temperature (°C)	Percentage Yield (%)	
	KOH	HNO <sub>3</sub>
460	78.4	46.56
480	91.4	53.46
500	67	49

Additional characterization was made on OPP-AC activated at 480 °C for both HNO<sub>3</sub> and KOH and labeled as 10HNO480 and 10KOH480, respectively. Depending on the type of activation agents used, different precursors react differently to give a variety of surface areas, pore volumes, and yield. The reaction of the activating agent with cellulose, hemicellulose, lignin, or polysaccharide in carbon precursor leads to various activation mechanisms [25]. Figure 3a,b show the 10HNO480 and 10KOH480.

### 3.4. Fourier Transform Infrared (FTIR) Spectroscopy

The functional groups present in raw OPP and OPP-AC were identified using Fourier transform infrared spectroscopy (FTIR). This also provides information on the effect of the activation process that was carried out as evidence of the phase transformation that occurred in both precursors and AC. Most lignocellulosic materials tend to have almost the same spectra [49].

The existing frequency peak of C-O stretching for raw OPP was detected at around 1000–1200 cm<sup>-1</sup>, which represents the structure of lignin. The identified peak also represents the functional group of cellulose and hemicellulose structure. Other typical frequency peaks that occurred in raw OPP in this study include 3313 cm<sup>-1</sup> (–OH), aliphatic. Some of the peaks are also consistent with findings, which represent the stretching of the C–O functional group [50]. It can be suggested from carbonyl, ethers, and alcohol groups, which are normally present in plant cellulose. As shown in Figure 4, the C–H group is at 2917 cm<sup>-1</sup>, the amide C=O group is at around 1602 cm<sup>-1</sup>, and moderate intensity stretching is at 1229 cm<sup>-1</sup>.



**Figure 4.** FTIR of raw OPP, 10HNO480, and 10KOH48.

Figure 4 illustrates that the raw OPP, 10HNO480, and 10KOH480 all displayed bands at  $3500\text{--}3300\text{ cm}^{-1}$ , which corresponds to the O–H stretch in alcohols, phenols, and adsorbed water. This was attributed to the O–H stretching vibration of hydroxyl functional groups. The band is more intense for the raw OPP, which means that this fraction contains many more alcohols, phenols, and adsorbed water than 10HNO480 and 10KOH480.

During the carbonization and activation processes, most of the adsorption peaks of functional groups disappeared [51]. The most notable example was the vibrations of bands at  $2905\text{ cm}^{-1}$ . This band is assigned to aliphatic C–H stretching, which identifies the composition of polysaccharides in cellulose and hemicellulose, respectively [52]. This band was only visible in raw-OPP and vanished once it was carbonized.

Another example was at bands  $1228$  and  $1029\text{ cm}^{-1}$ . Similar to Hidayu et al. [53], raw OPP showed these bands, which corresponded to the stretching of the C–O functional group. However, these bands disappeared, and the surface became broad at the 10HNO480 and 10KOH480 surfaces. The disappearances of adsorption peaks at 10HNO480 and 10KOH480 could be due to the decomposition of adsorbed water and hydroxyl groups, which indicates the raw OPP spectrum was vaporized as volatile materials when the heat was supplied to the sample [52,54]. According to Hidayu et al. [53], this demonstrates that the activation procedure was completed successfully.

At  $1000\text{--}1100\text{ cm}^{-1}$ , which includes C–O in carboxylic acid, alcohols, and esters, a significant reduction was also observed. A similar pattern of reduction was also found by Hesas et al. [55] using different types of agricultural waste. In addition to the reduction and disappearance of adsorption peaks, new peaks were observed in the 10HNO480 spectra at  $1595\text{ cm}^{-1}$ , which can be attributed to asymmetric and symmetric vibration of the nitro ( $-\text{NO}_2$ ) group. This suggests that the  $\text{HNO}_3$  functionalization also introduces nitrogen-containing functional groups on the surface of the OPP-AC [21]. Gokce and Aktas [56] also reported on the use of  $\text{HNO}_3$  to modify waste tea-activated carbon.

### 3.5. Field Emission Scanning Electron Microscopy (FESEM)

The morphological changes as the effect of impregnation and carbonization temperature of the OPP-AC product were observed using FESEM analysis. Figure 5a,b depict the surface morphology of OPP before it was activated. It shows a thick and flat pattern with small fractures in between. This was attributed to the high amount of lignin, a phenolic polymer that gives the plant structural strength and gives it a hard and rough wood-like structure. In Figure 5b, the precursors were found to have a compacted surface with a shallow and clogged pore pattern on it. This can be due to the reaction of the pretreatment and heating process during oven drying. From Figure 5a,b, the surface is clearly illustrated as an unsatisfied adsorptive material due to the presence of the non-porous OPP surface.

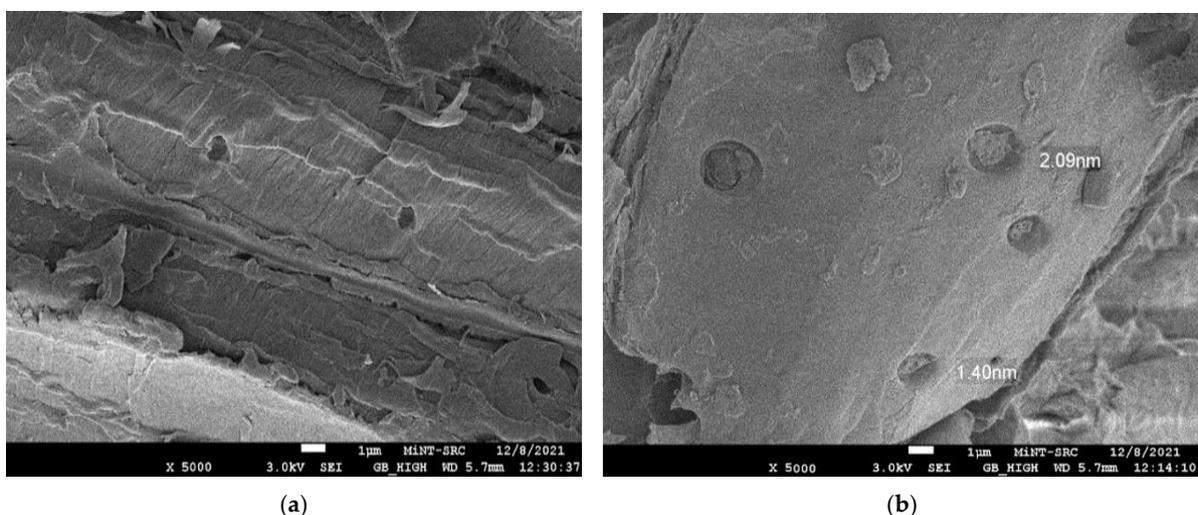
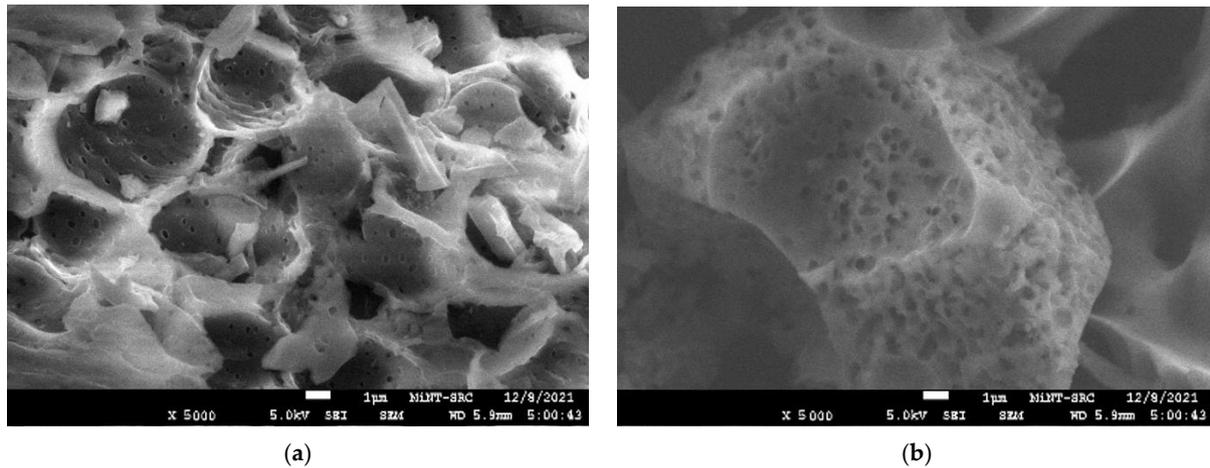


Figure 5. (a,b) surface morphology of raw OPP.

The most noticeable differences between the activation processes employing different chemical bases are the patterns created on the surface of the OPP-AC, as shown in Figure 6a,b. AC impregnated with KOH and HNO<sub>3</sub> has a more homogeneous and comb-like pattern, whereas AC impregnated with KOH has significantly smaller pores and sparse distribution. Similar pore development on the surfaces of AC is also observed in the Okman et al. [57] study, in which the pattern of grape seeds impregnated with KOH produces a sponge-like structure with many holes. The pore size for AC activated with KOH was from 1.255 to 2.118 nm at 480 °C. Meanwhile, pore sizes in AC activated with HNO<sub>3</sub> ranged from 4.9 nm to 6.8 nm.



**Figure 6.** (a,b) surface morphology of 10HNO480 and 10KOH480.

### 3.6. Brunauer, Emmet, and Teller (BET) Surface Area and Pore Distributions Analysis

The physical components such as the specific surface area, micropore volume, and pore size are the most relevant to evaluate the capacity of adsorption. Porous materials are most commonly described in terms of pore diameters calculated from gas sorption data [58]. Conventions proposed by the International Union of Pure and Applied Chemistry (IUPAC) for categorizing pore sizes and gas sorption isotherms indicate the link between porosity and sorption [59].

Table 3 shows the specific surface area and pore size distribution of raw OPP, 10HNO480, and 10KOH480. As can be seen in Table 3, the average pore diameters of 10HNO480 and 10KOH480 are 5.89 and 1.43 nm, respectively. According to the International Union of Pure and Applied Chemistry (IUPAC) classifications, the pores can be divided into macropores ( $d > 50$  nm), mesopores ( $2 < d < 50$  nm), and micropores ( $d < 2$  nm). This indicates that 10HNO480 is mesopore-adsorbent and 10KOH480 is micropore-absorbent.

**Table 3.** Porous structures of raw OPP and OPP-AC impregnated with KOH and HNO<sub>3</sub>.

	$S_{\text{BET}}$ (m <sup>2</sup> /g)	$V_{\text{total}}$ (cm <sup>3</sup> /g)	$V_{\text{micro}}$ (cm <sup>3</sup> /g)	$V_{\text{meso}}$ (cm <sup>3</sup> /g)
Raw OPP	0.579	-	-	-
10KOH480	883.3	0.460	0.310	0.150
10HNO480	372.4	0.26	0.120	0.140

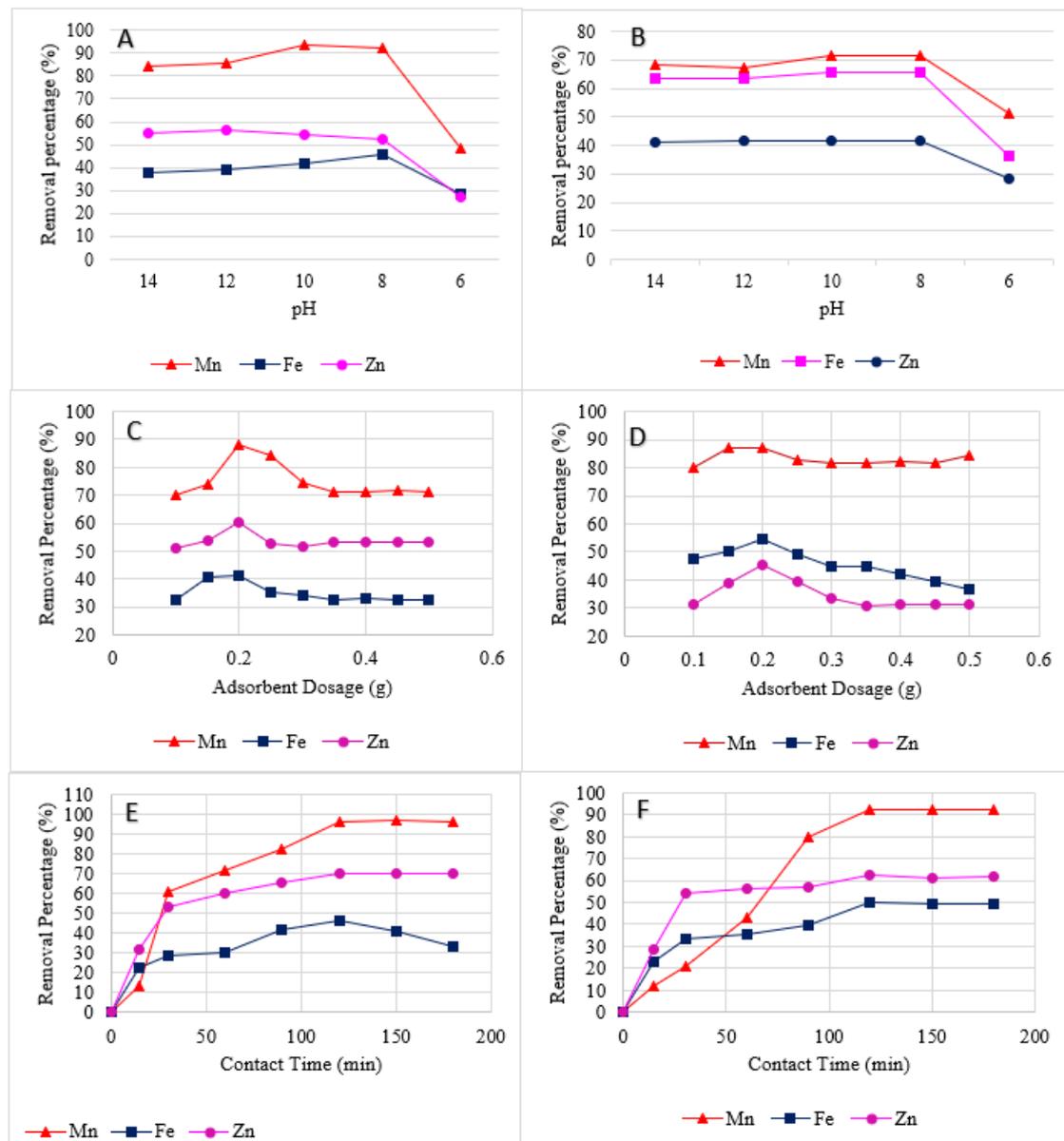
The surface areas occurring through BET are noticed to be 883.3 and 372.4 m<sup>2</sup>/g for 10KOH480 and 10HNO480, respectively. Meanwhile, raw OPP attained  $S_{\text{BET}}$  0.579 m<sup>2</sup>/g, which suggested the development of the porous structure after the activation process. This value is comparable to that study by Rugayah et al. [60] that utilized oil palm kernel shells as AC. It is clearly shown that the dehydration process by the chemical activating agent increases the surface area and porosity. Additionally, the results demonstrate that this study's KOH-AC has a dominantly microporous structure, while the HNO-AC exhibits a mesoporous structure.

### 3.7. Batch Adsorption

The optimum adsorption removal of a composite adsorbent was investigated under a variety of conditions, including pH, adsorbent dosage, and contact time, which is an important parameter in determining adsorption ability.

#### 3.7.1. Effect of pH

In the batch adsorption study, pH is a significant component that will affect the adsorption process by altering the surface charge distribution of the utilized adsorbents [61,62]. The pH-related effects on the heavy metals (Mn, Fe, and Zn) in wastewater from the processing of wood were observed in the ranges of 6 and 14, as shown below (6, 8, 10, 12, and 14). Figure 7A,B clearly show the best results are obtained on both OPP-ACs when using pH 8, respectively, for Mn, Fe, and Zn from fiberboard processing wastewater.



**Figure 7.** (A), effect of pH percentage on Zn, Fe, and Mn removal by KOH impregnated AC; (B), pH on Zn, Fe, and Mn removal by HNO<sub>3</sub>-impregnated AC; (C), effect of adsorbent dosage on Zn, Fe, and Mn removal by KOH-impregnated AC; (D), effect of adsorbent dosage on Zn, Fe, and Mn removal by HNO<sub>3</sub>-impregnated AC; (E), effect of contact time on Zn, Fe, and Mn removal by KOH-impregnated AC; (F), effect of contact time on Zn, Fe, and Mn removal by HNO<sub>3</sub>-impregnated AC.

The optimal pH of both 10KOH480 and 10HNO480 is eight. Based on the results, 10KOH480 provides a higher removal percentage of Mn compared with 10HNO480. The percentage removal of 10KOH480 and 10HNO480 is, respectively, 93.62% and 71.72% for Mn, 47.87% and 65.86% for Fe, and 54.42% and 41.52% for Zn at optimal pH.

Briefly, it can be observed that removal patterns for all the adsorbents increased as the pH of the water sample was increased, until the optimum pH was 8. This was due to the deprotonation of oxygen functional groups, which increased the active sites for heavy metal ions chelation and significantly increased the AC adsorption capacity [63]. The results also show that the different metal ions in the solution have different competitive adsorption effects [37]. For 10KOH480, the degree of influence from large to small was as follows: Mn > Fe > Zn, while for 15HNO480: Mn > Zn > Fe. Since the ion radius of Mn is smaller than that of other ions, the ability of Mn to compete for adsorption sites is higher than other ions, and the repulsive force is stronger to other metal ions after adsorption.

### 3.7.2. Effect of Adsorbent Dosage

Adsorbent dosage is a significant factor in investigating the quantitative uptake of pollutants. The results of Fe, Mn, and Zn removal by using various dosages of the 10KOH480 and 10HNO480 are shown in Figure 7C,D, respectively. A clear trend can be seen for the effect of adsorbent dosage. As expected, by increasing the amount of adsorbent, the removal of metals increased as well until it reaches the optimum stages. The highest adsorption percentage in this study was recorded on Mn removal using 10KOH480, which is 88% when 0.2 g of adsorbate was used. In contrast, 0.3 g/L of 10HNO480 is needed to remove 87% of Mn. By increasing the adsorbent dosage, a more active site for adsorption was available. This explains the trend where an increase in adsorbent dosage resulted in more removal of any pollutants [64,65].

### 3.7.3. Effect of Contact Time

Contact time shows a marked influence on the adsorption efficiency and can be used to elucidate the kinetics of the adsorption process [66]. Theoretically, the increase in contact time leads to an increase in removal percentage until it reaches a saturated level. The optimum pHs and adsorbent dosages of 10KOH480 and 10HNO480 were set constant to determine the optimum contact time. As can be seen in Figure 7E,F, low removal of Mn, Fe, and Zn from the wastewater using OPP-AC was recorded during the first 30 min of contact time. This behavior was due to the dissociation of water molecules that bore different types of pollutants and required a certain period of time for the reaction to occur effectively.

Overall, the results show that the optimal contact time at the highest removal percentages is 120 min for both 10KOH480 and 10HNO480. Comparing KOH-impregnated AC and HNO<sub>3</sub>-impregnated AC, 10KOH480 shows higher removal percentage, which is 96.14% for Mn and 70.05% for Zn but slightly lower for Fe with 45.93%. This may be due to the microporous pore structure of 10KOH480. According to Hui and Zaini [67], microporous activated carbon is most widely and suitably used for the adsorption of micropollutants and heavy metal ions. Because of its small pore diameter (<2 nm), larger size molecules (macropollutants) are therefore prevented from entering the pores.

In accordance with the results, the percentage removal and adsorption capacity trends for metals removal became invariable after 120 min, indicating a decrease in the available active adsorption sites on the composite adsorbent. This was due to time, which resulted in a limited mass transfer of the adsorbate molecules from the bulk liquid to the external surface of the composite adsorbent [68,69]. According to Mustapha et al. [70], the slow uptake in the later stages is most likely due to an attachment-controlled process caused by fewer available active sites for sorption, whereas the slight decrease in percentage removal with increasing contact time may be due to adsorbent surface saturation followed by subsequent adsorption and desorption.

### 3.8. Removal of Mn, Fe, and Zn under Optimum Conditions

The adsorption procedure was performed at optimum conditions obtained in previous experiments. For the OPP-AC after activation process using KOH and HNO<sub>3</sub>, the samples were added to a 100 mL solution containing Mn, Fe, and Zn ions and agitated at 125 × g. The highest removal percentage (%) under optimal conditions is listed in Table 4. This is the moment at which the treatment becomes stable, and no additional adsorption may occur due to the saturation of the surface area.

**Table 4.** Mn, Fe, and Zn removal from wastewater using modified activated carbon under optimum conditions.

		pH	Adsorption Dosage (g/L)	Contact Time (min)	Removal Percentage (%)
KOH-impregnated AC and	Mn	12	0.2	150	97
	Fe	10	0.2	120	46
	Zn	8	0.2	120	70
HNO <sub>3</sub> -impregnated AC	Mn	10	0.2	120	93
	Fe	10	0.2	120	66
	Zn	8	0.2	120	62

### 3.9. Prediction of Mn, Fe, and Zn Removal using the RSM Model

#### 3.9.1. Analysis of Variance

Through 20 iterations, the central composite design (CCD) approach was utilized to maximize the removal of Mn, Fe, and Zn ions from the solution. To show that the models were acceptable, an ANOVA was conducted, and the quality of the fitted model was evaluated using the F-value, p-value, and coefficient of determination. Table 5 shows the results of the models used to fit the experimental data in the form of an ANOVA for Mn, Fe, and Zn removal. Given that the p-values were less than 0.05, and the adjusted R<sup>2</sup> was more than 0.95, all of the models were significant at the 5% confidence level, as illustrated in Table 5. The models' projected response is more accurate the higher the F-value. According to the results of the current study, the values of adjusted R<sup>2</sup> for Mn, Fe, and Zn impregnated AC with KOH were 0.9967, 0.9619, and 0.9802, and for Mn-, Fe-, and Zn-impregnated AC with HNO<sub>3</sub> they were 0.9886, 0.9656, and 0.9515. A high R<sup>2</sup> value near 1 indicates strong agreement between the experimental and model findings within the experimentally reasonable range, and it suggests that a desired and acceptable agreement with adjusted R<sup>2</sup> is required for successful model fit [71]. The models provided in Table 5 were thus found to be sufficient to predict the data from the experimental removal of Mn, Fe, and Zn based on the statistical findings. Three models, namely the 2FI model for Mn removal by KOH-impregnated AC and HNO<sub>3</sub>-impregnated AC, the linear model for Fe by KOH-impregnated AC and Zn by HNO<sub>3</sub>-impregnated AC, and the quadratic model for Zn by KOH-impregnated AC and Fe by HNO<sub>3</sub>-impregnated AC, are significant model terms in the current study.

**Table 5.** Mn, Fe, and Zn removal from wastewater using modified activated carbon under optimum conditions.

		Model	F-Value	p-Value	Adjusted R <sup>2</sup>	Predicted R <sup>2</sup>
KOH-impregnated AC	Mn	2 FI	970.81	<0.0001	0.9967	0.9900
	Fe	Linear	160.95	<0.0001	0.9619	0.9423
	Zn	Quadratic	105.32	<0.0001	0.9802	0.9190
HNO <sub>3</sub> -impregnated AC	Mn	2FI	276.06	<0.0001	0.9886	0.9037
	Fe	Quadratic	60.17	<0.0001	0.9656	0.9137
	Zn	Linear	125.18	<0.0001	0.9515	0.9389

Additionally, the following equations describe the prediction models for the removal of Mn, Fe, and Zn by KOH- and HNO<sub>3</sub>-impregnated AC:

- Zn Removal by KOH impregnated

$$AC = 52.3672 + 1.46211 \times A + 7.44651 \times B + -8.47408 \times C + 0.75 \times AB + -0.75 \times AC + -0.5 \times BC + 0.771065 \times A^2 + 1.07081 \times B^2 + -2.09909 \times C^2 \quad (9)$$

- Fe Removal (%) by KOH impregnated

$$AC = 41.5781 + 5.15511 \times A + 1.84097 \times B + -0.846808 \times C \quad (10)$$

- Mn Removal (%) by KOH impregnated

$$AC = 74.4884 + -6.37378 \times A + 6.77829 \times B + -6.78895 \times C + -7.125 \times AB + -7.625 \times AC + -1.375 \times BC; \quad (11)$$

- Mn Removal (%) by HNO<sub>3</sub> impregnated

$$AC = 69.2799 + 0.961262 \times A + 24.19 \times B + -0.119858 \times C + -0.3125 \times AB + 0.0030303 \times AC + -0.0454545 \times BC \quad (12)$$

- Zn Removal by HNO<sub>3</sub> impregnated

$$AC = 52.1243 + 4.23571 \times A + 0.127807 \times B + -7.38892 \times C; \quad (13)$$

- Fe Removal (%) by HNO<sub>3</sub> impregnated

$$AC = 36.4747 + 4.34898 \times A + 7.30982 \times B + 1.5495 \times C + -2 \times AB + -3.75 \times AC + 6.5 \times BC + 9.88754 \times A^2 + 2.95883 \times B^2 + 4.7925 \times C^2 \quad (14)$$

where: A: pH, B: dosage, and C: time.

In order to establish the model with the highest degree of accuracy, the predictions removing data were also subjected to error analysis and coefficient of determination (R<sup>2</sup>) analysis. The results are shown in Table 6. The highest observed and predicted removal efficiencies are for Mn (97% and 95%, respectively), whereas the lowest observed and predicted efficiencies are for Fe (46% and 49%, respectively). Table 6 shows that the predicted removal efficiency has low values for MSE, RMSE, MAD, and MAPE, and the R<sup>2</sup> values are more than 0.95 for all three metals. As a consequence, AC impregnated with

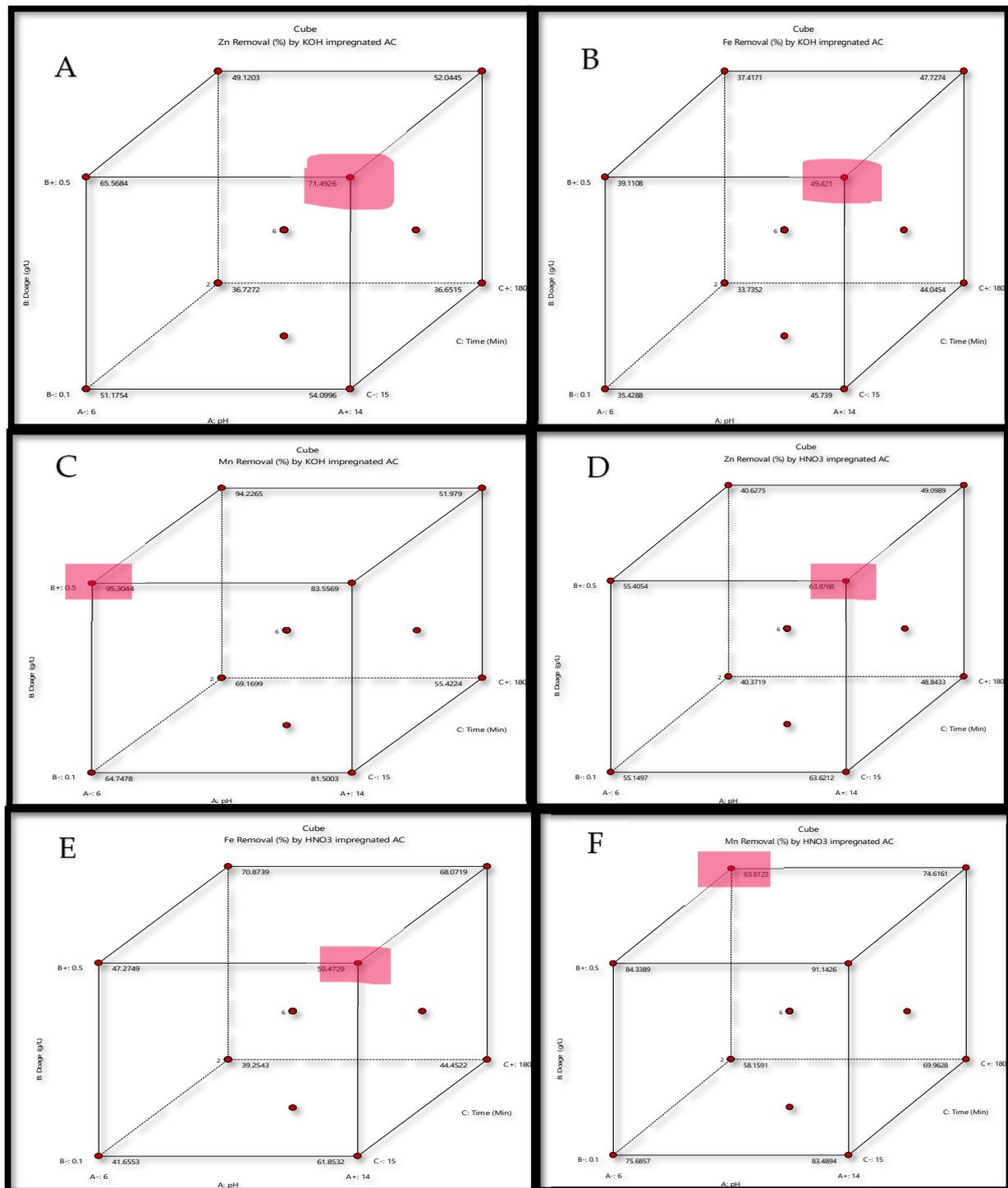
**Table 6.** Mn, Fe, and Zn removal from wastewater using modified activated carbon under optimum conditions.

Type of AC	Metal	Removal		Mean	MSE	RMSE	MAD	MAPE	R <sup>2</sup>
		Experiment	Prediction						
KOH-impregnated AC	Mn	97	95	2	4	2	2	0.021	0.9978
	Fe	46	49	3	9	3	3	0.065	0.9679
	Zn	70	71	1	1	1	1	0.014	0.9896
HNO <sub>3</sub> -impregnated AC	Mn	93	91	2	4	2	2	0.021	0.9922
	Fe	66	70	4	16	4	4	0.061	0.9819
	Zn	62	63	1	1	1	1	0.016	0.9591

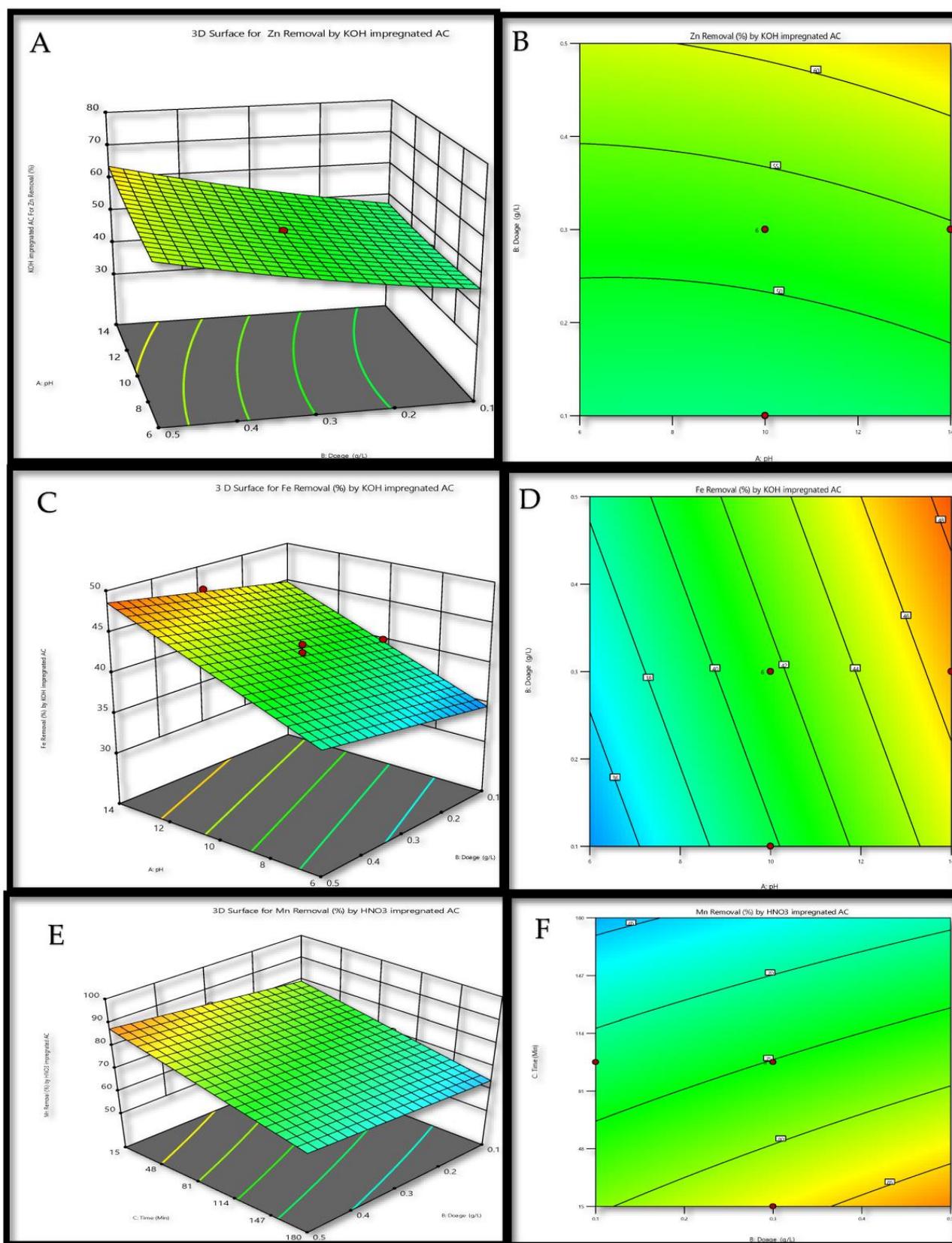
KOH or HNO<sub>3</sub> may be used as a natural adsorbent to remove Mn, Fe, and Zn ions. Error analysis showed that RSM models best reflect the removal data.

In addition, the optimal conditions for the removal of Mn, Fe, and Zn according to the prediction were also shown in Figure 8 as a cube plot, with the highest removal being highlighted in red on the cube. According to Figure 9, the highest removal was achieved

for Zn and Fe by KOH-impregnated AC (Figure 8A,B, as well as Zn and Fe by HNO<sub>3</sub>-impregnated AC (Figure 8D,E) at higher pH, adsorbent dosage, and lower contact time; however, the highest removal was achieved for Mn by KOH-impregnated (Figure 8C) and HNO<sub>3</sub>-impregnated AC (Figure 8F) at higher adsorbent dosage, lower pH, and contact time.



**Figure 8.** Cube plot of (A) Zn removal % using KOH-impregnated AC; (B) Fe removal % using KOH-impregnated AC; (C) Mn removal % using KOH-impregnated AC; (D) Zn removal % using HNO<sub>3</sub>-impregnated AC; (E) Fe removal % using HNO<sub>3</sub>-impregnated AC; (F) Mn removal % using HNO<sub>3</sub>-impregnated AC.

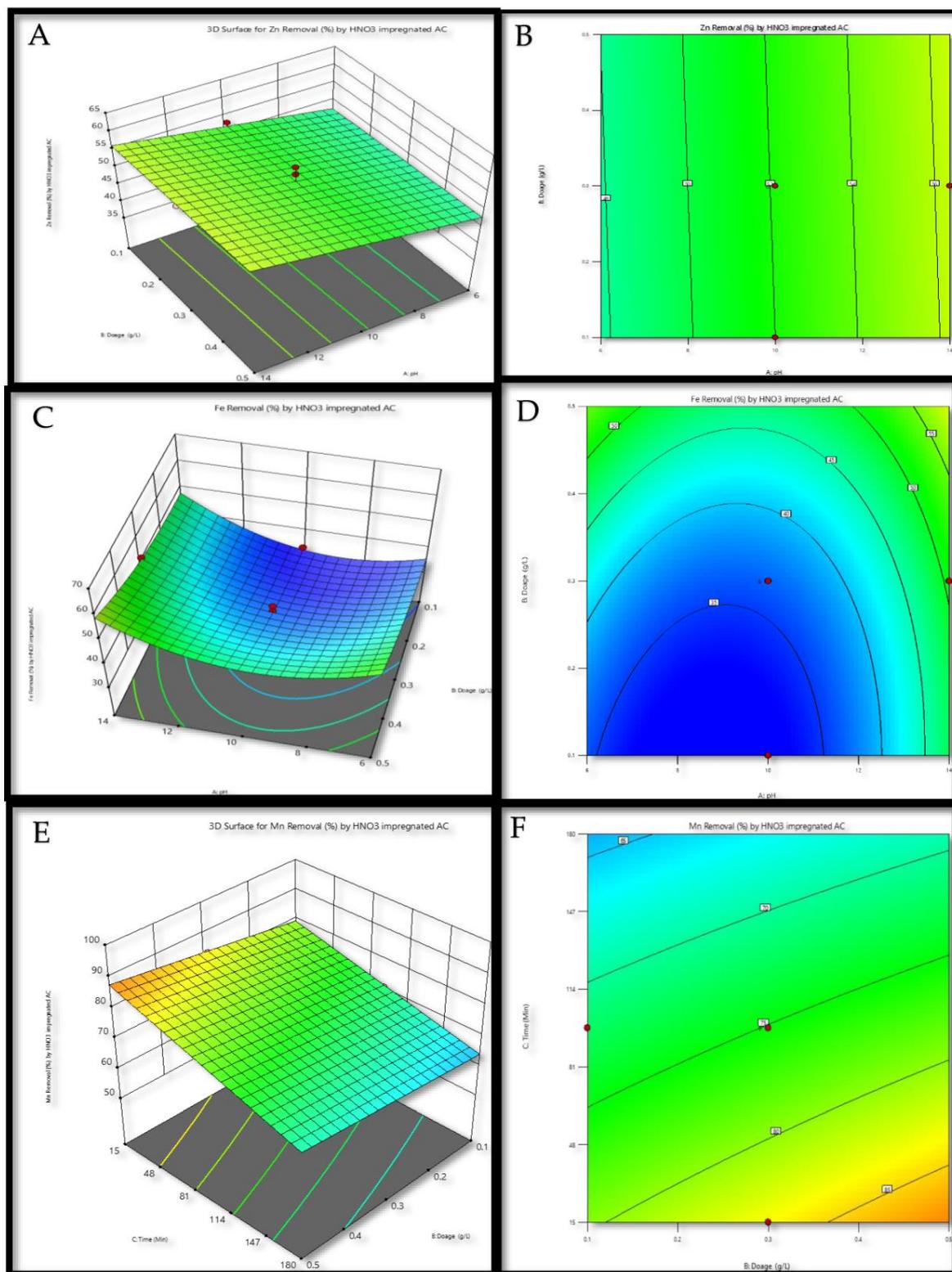


**Figure 9.** Response surface and contour plots for (A,B) Zn removal by KOH-impregnated AC; (C,D) Fe removal by KOH-impregnated AC; (E,F) Mn removal by KOH-impregnated AC.

### 3.9.2. Three-Dimensional Surface and Contour Plots for Mn, Fe, and Zn Removal

The Design Expert 13 software (version 13) was used to create three-dimensional (3D) surface response and contour plots in order to analyze the interaction correlations between independent factors and certain models' responses. The response surface models created to predict the removal of Mn, Fe, and Zn were considered reasonable in light of the findings [72].

Figure 9A–D show the three-dimensional response surface of the combined influence of pH and adsorbent dose when the contact time was kept at its optimal level ( $t = 120$  min). As a consequence, high pH (10–14) and high adsorbent dose (0.4, 0.5 g/L) yielded the highest Zn removal by KOH-impregnated AC, as shown in Figure 9A,B and Fe removal by KOH-impregnated AC, as shown in Figure 9C,D, while low pH (6) and low adsorbent dosage (0.1, 0.2 g/L) yielded poorer metal removal. While the pH was kept at its optimal level (pH = 8), Figure 9E,F show the three-dimensional response surface and contour plot of the combined influence of contact time and adsorbent dose for Mn percentage removal. As a consequence, KOH-impregnated AC demonstrated optimal Mn removal at low contact time (15–48 min) and high adsorbent dosage (0.4, 0.5 mg/L), KOH-impregnated AC demonstrated optimum Fe removal at low contact time (15–48 min) and adsorbent dosage (0.4, 0.5 g/L). In addition, the optimum pH and adsorbent dosage under optimal contact conditions ( $t = 120$  min) are shown on a three-dimensional response surface in Figure 10A–D. Therefore, as demonstrated in Figure 10A,B, Zn removal by HNO<sub>3</sub>-impregnated AC is the greatest at high pH (13–14) and high adsorbent dose (0.3, 0.5 g/L), but Fe removal is the worst at low pH (6–8) and low adsorbent dosage (0.1–0.3 mg/L). Figure 9E,F illustrate a three-dimensional response surface and contour plot of the combined impact of contact time and adsorbent dosage for Mn % removal while the pH was maintained at the optimum level (pH = 8). Therefore, HNO<sub>3</sub>-impregnated AC was found to be most effective at removing Mn when soaked in water for just 15 to 48 min at a high adsorbent dose (0.4 or 0.5 g/L), and the most effective at removing Fe when exposed to water for only 15 to 48 min at a high adsorbent dosage (0.3–0.5 g/L). Furthermore, according to the results of three-dimensional plots reported by Suwannahong et al. [73], the removal capacity for Cu (II) removal influenced all variable factors, particularly pH and dose, and it was found that these variables had an impact on Cu (II) removal efficiency. Moreover, Suwannahong et al. [74] used the classified reduced quadratic models to map the response surface in three dimensions (3D) and determine the optimum operating parameters for the Fenton oxidation process's effectiveness in removing color and COD (Chemical Oxygen Demand, mg/L). They demonstrated how the Fenton oxidation process's color and COD efficiency were predicted by the reduced quadratic model. The perturbation plots were also used to compare the impacts of all variable components under the optimum operating circumstances in terms of the percent range for color and COD removal effectiveness through the Fenton oxidation process.



**Figure 10.** Response surface and contour plots for (A,B) Zn removal by HNO<sub>3</sub> impregnated AC, (C,D) Fe removal by HNO<sub>3</sub> impregnated AC, and (E,F) Mn removal by HNO<sub>3</sub> impregnated AC.

#### 4. Conclusions

From the results of the current study, it can be concluded that KOH and HNO<sub>3</sub> can produce activated carbon (AC) with a faster process and low activation temperature. The optimal activated carbon of both KOH and HNO<sub>3</sub> was obtained at conditions

(10% impregnation ratio, 480 °C activation temperature, and 20 min activation time) which resulted in 883.3 and 372.4 m<sup>2</sup>/g surface areas, respectively.

The AC produced also possesses good pore development and high carbon yield. The activation process modifies more functional groups such as hydroxyl groups, carbonyl groups, and aromatic compounds than untreated raw material, which could enhance the adsorbent's performance. The 10KOH480 is highly microporous (pores with a size of fewer than 2 nm or 20 Å) when compared with that produced through HNO<sub>3</sub>. On the other hand, 10HNO480 has resulted in mesoporous (pores with sizes between 2 and 50 nm or 20 and 500 Å) carbon material.

This has resulted in a higher adsorption percentages of metal pollutants from wastewater using KOH, which are 96.14% for Mn, 70.05% for Zn, and approximately 50% for Fe at optimum parameters of pH, adsorbent dosage, and contact time. However, further optimum values of parameters such as temperature, metal initial concentration, and shaking speed could be considered in the future for more detailed results.

The predicted versus actual values of Mn, Fe, and Zn removal show an adequate agreement between real data and those gained from the models. Consequently, all predictive models achieved in this study can be used to predict heavy metal removal with high sufficiently and accuracy.

**Supplementary Materials:** The following supporting information can be downloaded at: <https://www.mdpi.com/article/10.3390/su15086734/s1>, Figure S1. The Picture of oil palm petiole (OPP) that has been extracted from oil palm fronds. The leaf was exiled from the oil palm fronds and only the petiole of the oil palm was employed in our study.

**Author Contributions:** Conceptualization, data curation, formal analysis, resources, visualization, writing—original draft, writing—review and editing, S.A.; supervision, resources, conceptualization, project administration, writing—original draft, writing—review and editing, W.A.H.A.; supervision, resources, funding acquisition, visualization, N.O.; validation and formal analysis, F.S.K.; investigation and formal analysis, S.S.; data curation, validation, funding acquisition, H.A.T.; data curation and validation, A.M.A.A. All authors have read and agreed to the published version of the manuscript.

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**Conflicts of Interest:** The authors declare no conflict of interest.

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