

Article

Studies on the Mechanism of Cu(II) Ion Sorption on Purolite S 940 and Purolite S 950

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Abstract: The aim of the presented research was to investigate the mechanism of sorption of Cu(II) ions on the commercially available Purolite S 940 and Purolite S 950 chelating ion exchangers with the aminophosphonic functional groups. In order to understand better the sorption mechanism, the beads were cut with an ultramicrotome before and after the Cu(II) ion sorption process. The cut beads were examined by scanning electron microscopy (SEM) with an EDX detector. The performed linear profiles of the elemental composition allowed us to examine the depth with which the sorbed metal penetrates into. For further investigations concerning the mechanism of the sorption process, the Fourier transform infrared spectroscopy (FTIR) analysis using the attenuated total reflectance (ATR) technique and the X-ray photoelectron spectroscopy (XPS) methods have been used. The comparison of FTIR and XPS spectra before and after the sorption of Cu(II) ions showed that free electron pairs from nitrogen and oxygen in the aminophosphonic functional groups participate in the process of copper ion sorption. In addition, the microscopic studies suggested that the process of ion exchange between Na(I) ions and sorbed Cu(II) ions takes place on the Purolite S 940 and Purolite S 950. This study concerning the in-depth understanding of Cu(II) sorption mechanism, using modern analytical tools and research methods could be very useful for its further modifications leading to the improvement of the process efficiency.

Keywords: heavy metals; sorption mechanism; ion exchangers; copper; Purolite S 940; Purolite S 950

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1. Introduction

Nowadays due to growing industrialization, society has to face various environmental problems. Among them, one of the greatest priorities is water pollution caused by heavy metal ions [1,2]. Metals of a density larger than $4.5 \times 10^{-3} \text{ g/cm}^3$ belong to the heavy metal group [2,3]. In chemical reactions, they tend to donate electrons forming simple cations. They show good thermal and electrical conductivity in the solid as well as liquid states, have a gloss, and are opaque. They have high melting and boiling points and are characterized by reducing properties [4,5]. Some of these heavy metals like copper are required by living organisms in a smaller quantity but at higher concentrations, its presence results in toxic effects [6]. They are found in raw sewage and they are not degraded in the sewage treatment being very harmful to living organisms causing mutagenic changes, damage to the central nervous system, and cancer [7–10]. Among them, copper

which is present in fertilizers, tanning, and photovoltaic cells can cause allergies, cystic fibrosis, adreno-corticol hyperactivity, alopecia, arthritis, diabetes, hemorrhaging, and kidney disorders [11]. Copper is considered to process carcinogenic properties through the interaction of its ions with lipids finally resulting in DNA and tissue damage [12]. Therefore, one of the most important activities to protect human health and the natural environment is the improvement of water quality and sewage management [13–16].

Among different methods for wastewater treatment, ion exchange can be considered as one of prime importance as it is technologically simple and enables efficient removal of even traces of impurities from solutions [17–19].

The main advantage of using the ion exchange process for the electroplating treatment is that it has the greatest metal ion removal efficiency compared to the conventional methods such as reverse osmosis, electrolysis, or evaporation. At the same time, the ion exchange process requires the use of the smallest amount of energy for wastewater treatment compared to the above-mentioned methods. However, the disadvantage of this method is the need to use chemical reagents in the wastewater treatment process.

The use of natural sorbents would be a much more ecological solution. Yet, a much smaller efficiency of metal ion removal is obtained and is associated with some technical problems such as flow resistance through the ion exchange column.

The ion exchange process is very often used in many stages of technological processes in electroplating. They apply regeneration of chromium plating bath and pickling in phosphoric acid(V), regeneration of rinse water, regeneration of baths for passivation of zinc coatings, recovery of precious metals from rinse waters, final polishing of neutralized sewage. The selective ion exchangers with the aminophosphonic functional groups play a special role in the processes of galvanic wastewater treatment. They are used to remove residues that were not removed during treatment with conventional physicochemical methods.

In the wastewater treatment process, chelating ion exchangers are commonly used. A special feature of this type of resins is the ability of selective sorption of one metal ion in the presence of others. Selective sorption of metal ions is usually not possible using typical cation exchangers because the affinity for the metal ion present in the solution is only determined by the electrostatic interactions. The ability of selective sorption of transition metal ions allows the use of chelating ion exchangers in industrial wastewater treatment processes and recovery of valuable metals from ores and sludges [20–22].

As follows from the literature data, the chelating ion exchangers containing aminophosphonic functional groups are characterized better performance in the process of removing Cu(II) and Zn(II) ions from industrial waste, compared to other chelating resins [23]. They also have a weak affinity for Ca(II) and Mg(II) ions. An example of this type of materials is commercially available Purolite S 940 and Purolite S 950. There are numerous papers and research works concerning the sorption studies of copper ions [14–16], however, there is a lack of knowledge concerning the in-depth understanding of the mechanism of this process which can improve its efficiency greatly.

In the present study, the mechanism of Cu(II) ion sorption was examined based on the chosen ion exchangers using modern analytical techniques such as X-ray photoelectron spectroscopy (XPS), Fourier transform infrared spectroscopy (FTIR), and scanning electron microscopy (SEM). The presented results will allow us to learn more about the sorption mechanism using the chelating ion exchangers Purolite S 940 and Purolite S 950.

2. Materials and Methods

2.1. Material

Purolite S 940 and Purolite S 950 are macroporous chelating resins with the aminophosphonic functional groups. The matrix of the above-mentioned ion exchangers is pol-

ystyrene cross-linked with divinylbenzene. Their chemical structure is presented in Figure 1. The selected physicochemical parameters of Purolite S 940 and Purolite S 950 are presented in Table 1.

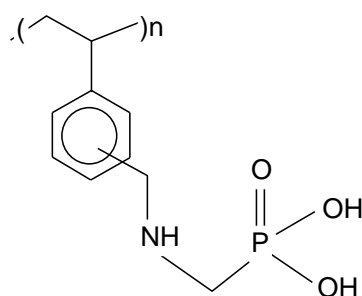


Figure 1. Chemical structure of Purolite S 940 and Purolite S 950.

Table 1. Selected physicochemical parameters of Purolite S 940 and Purolite S 950.

Ion Exchanger	Purolite S 940	Purolite S950
Manufacturer	Purolite International Ltd.	Purolite International Ltd.
Matrix	styrene-divinylbenzene copolymer	styrene-divinylbenzene copolymer
Structure	macroporous	macroporous
Functional groups	aminophosphonic	aminophosphonic
Physical form	white spherical grains	white spherical grains
Ionic form	Na ⁺	Na ⁺
Maximum working temperature	163.15 K	163.15 K
Specific gravity	1.11	1.13
Grain size	0.425–0.850 mm	0.3–1.2 mm
pH range	H ⁺ form: 2–6 Na ⁺ form: 6–11	H ⁺ form: 2–6 Na ⁺ form: 6–11
Specific surface area	15.8 m ² /g	15.7 m ² /g

2.2. Methods

The research was carried out using the commercial ion exchangers Purolite S 940 and Purolite S 950 (Purolite Ltd., King of Prussia, PA, USA). The aim of the research was to select an appropriate commercial ion exchanger for polishing galvanic wastewater for electroplating plants. The research was carried out using the model solutions and real galvanic wastewater. This paper presents the results of the studies on the sorption of Cu(II) ions on Purolite S 940 and S 950 ion exchangers from the model 0.001 M CuCl₂ solution.

The selection of the appropriate model concentration was preceded by the studies on the effect of the solution-ion exchanger phase contact time. Kinetic studies have also been carried out. These sorption tests were carried out using the following solutions on the Purolite S 940 and Purolite S 950 ion exchangers: 0.001 M CuCl₂, 0.005 M CuCl₂, 0.001 M CuSO₄, 0.005 M CuSO₄. In the process of removing Cu(II) ions, it should be stated that the chloride system is more favorable for the sorption process compared to the sulfate system with the initial concentration of Cu(II) ions amounting to 0.001 M. The tests proved that the equilibrium state for the solution with the concentration of 0.001 M is achieved in the case of sorption of the Cu(II) ions sorption on all tested ion exchangers after about 40 min. At 0.005 M concentration, equilibrium is reached in a shorter period of time. For example, for the Purolite S 950 ion exchanger, it is about 5 min. 0.001 M CuCl₂ was selected as the model solution. The standard solution with a concentration of 0.001 M was prepared from the CuCl₂·2H₂O salt (POCh S.A. Gliwice). Additionally, 63.54 g of salt was weighed and

dissolved in 1 L of redistilled water. It was adjusted to pH = 4 with NaOH solution and HCl.

Kinetic parameters for the pseudo first-order and pseudo second-order equations as well as intraparticle diffusion were determined.

The linear relationship $t/q_t = f(t)$ and the values of the determination coefficients $R^2 = 0.998$ (close to unity), $q_2 = 8.17$ mg/g, $k_2 = 0.076$ g/mg min, $h = 5.105$ mg/g min as well as good agreement with the experimental data showed that the pseudo second-order kinetic model is fully suitable for the description of the Cu(II) sorption on Purolite S 940. For the IPD model the k_i values were equal to 0.259 [mg/g min^{0.5}] and $R^2 = 0.829$ for Purolite S 940. The same results were obtained for Cu(II) ions on the Purolite S 950 ion exchanger. The linear relationship $t/q_t = f(t)$ and the values of the determination coefficients $R^2 = 0.998$ (close to unity), $q_2 = 9.72$ mg/g, $k_2 = 0.048$ g/mg min, $h = 4.537$ mg/g min. For the IPD model the k_i value was equal to 0.259 [mg/g min^{0.5}] and $R^2 = 0.829$. Good agreement with the experimental data showed that the pseudo second-order kinetic model is fully suitable for the description of the sorption process.

The final pH was in the range of 4–5.5. The final concentration of the copper solution after sorption on Purolite S 940 ion exchanger was: 20.09 mg cm⁻³ and for Purolite S 950 ion exchanger was: 14.15 mg cm⁻³.

The process of Cu(II) ions sorption on Purolite S 940 and Purolite S 950 was conducted in 100 mL Erlenmeyer flasks shaken by means of a laboratory shaker type 357 (Elpin Plus) with a rotation rate of 180 rpm. 0.20 g of the resin was added to 20 mL of 0.001 M CuCl₂ metal ion solution. After being shaken at 298 K for 2 h, the solution was separated from the resin. The resin was dried at room temperature.

2.2.1. Microscopic Studies

In order to examine the chemical structure and explain the mechanism of Cu(II) ion sorption on Purolite S 940 and Purolite S 950, the beads were cut through by means of ultramicrotome EM UC7 (Leica) and examined using the optical SMZ 1500 stereoscopic microscope (Nikon). To examine the distribution of elements and the sorbed metal Cu(II) ions, the linear profiles of elemental compositions for the cut beads after the Cu(II) sorption were prepared. In this stage of the study, the scanning electron microscope Quanta 3D FEG with the EDS/EBSD (FEI) system was used.

2.2.2. Fourier Transform Infrared Spectroscopy with Attenuated Total Reflection (FTIR-ATR)

In order to investigate the structure of ion exchangers before and after the Cu(II) sorption, the FTIR-ATR spectra of Purolite S 940 and Purolite S 950 using the FTIR Nicolet 8700 spectrometer (Thermo Scientific, Waltham, MA, USA) were recorded. They were performed by means of an ATR method with a diamond crystal in the range of wave numbers 4000–400 cm⁻¹ and the spectral resolution of 4 cm⁻¹. The spectra were recorded directly from the surface of the samples at room temperature.

2.2.3. X-ray Photoelectron Spectroscopy (XPS)

In order to examine the chemical structure and explain the mechanism of Cu(II) ion sorption on Purolite S 940 and Purolite S 950, XPS tests were made using the Ultra High Vacuum multi-chamber analytical system (Prevac). The tests were carried out for Purolite S 940 and Purolite S 950 before and after the Cu(II) ion sorption. After being fixed on a molybdenum carrier, the samples were degassed at room temperature to the high constant vacuum of about $\sim 5 \times 10^{-8}$ mbar, in the UHV system sluice. After their introduction into the analytical chamber of the system, the appropriate analysis was performed by means of the XPS spectroscopy method. AlK α monochromatic radiation was used as a source of photoelectrons. Photoelectrons were stimulated by X-ray of a characteristic line AlK α of 1486.7 eV energy, generated by a VG Scienta SAX 100 lamp with an aluminum

anode with a VG Scienta XM 780 monochromator. The pressure in the chamber during the measurements was 2×10^{-8} mbar. The X-ray tube operating parameters were as follows: $U = 12$ kV, $I_e = 30$ mA. Photoelectrons were recorded by the hemispherical analyzer Scienta R4000. The measurements were made based on the following basic parameters: operating mode—sweeping, pass energy—200 eV, measured range of the binding energy of photoelectrons 0–1200 eV, measuring step 0.5 eV, collection time in a single step 0.2 s, and the number of iterations 5. The parameters of the analyzer for the high-resolution spectra were: operating mode sweeping, pass energy 50 eV, measuring step 0.1 eV, and collection time in a single step 0.667 s.

3. Results and Discussion

3.1. Microscopic Studies

Photographs of Purolite S 940 and Purolite S 950 were obtained using optical microscopy show a spherical shape and homogeneous structure of the examined ion exchangers (Figures 2 and 3). The SEM microscopic photographs (Figure 4) allow us to observe the similarly developed porous structure of both. These tests are consistent with the BET-specific surface analysis using the Micrometitics ASAP 2420 apparatus (Table 1). The specific surface area for the Purolite S 940 ion exchange resin according to the BET method was $15.8 \text{ m}^2 \text{ g}^{-1}$, whereas for the Purolite S 950 ion exchanger, it was $15.7 \text{ m}^2 \text{ g}^{-1}$.

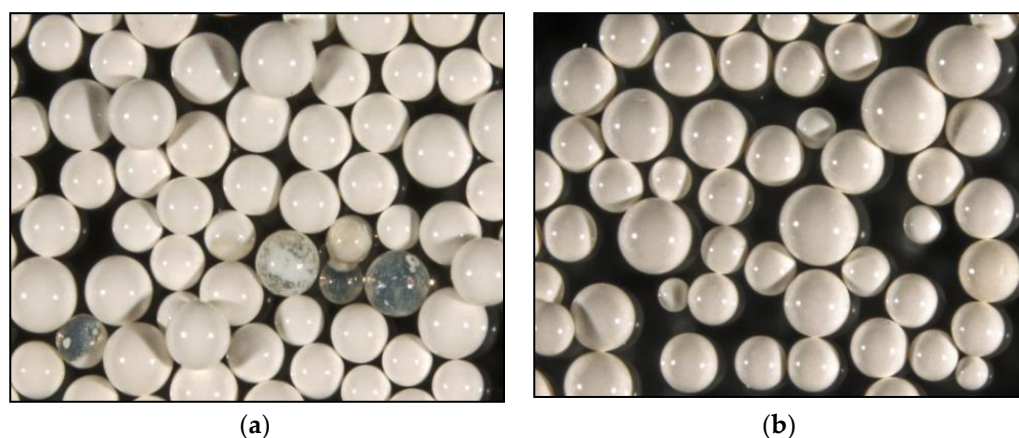


Figure 2. Photographs of (a) Purolite S 940, (b) Purolite S 950.

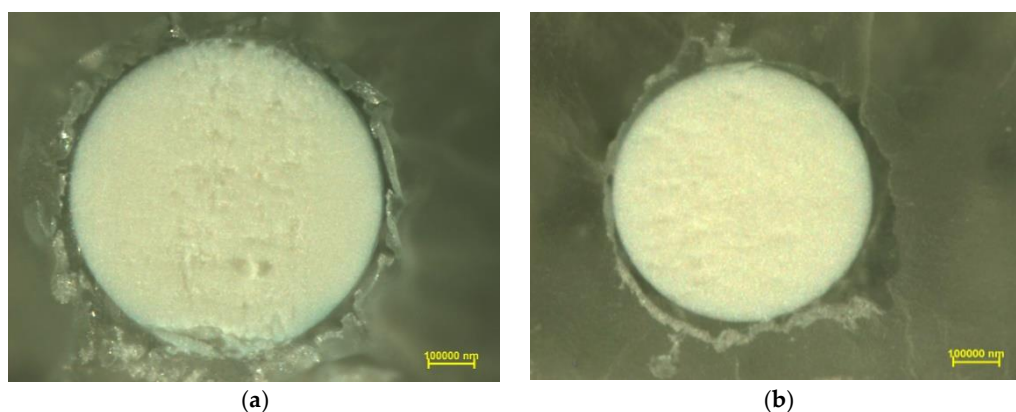


Figure 3. Photographs of cut (a) Purolite S 940, (b) Purolite S 950 after the Cu(II) ion sorption process.

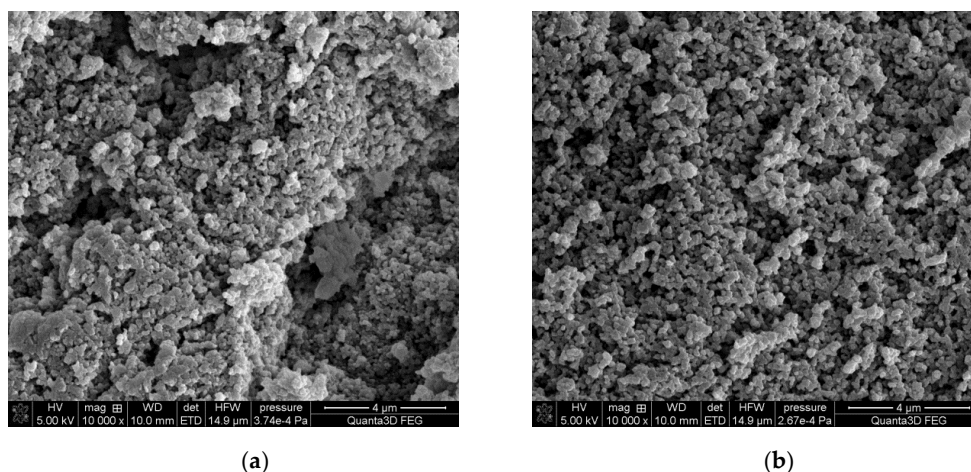


Figure 4. SEM images of cut (a) Purolite S 940, (b) Purolite S 950 after the Cu(II) ions sorption process.

In order to investigate the distribution of elements, linear profiles of elemental composition were made. Figure 5 shows the microscopic photos of the cut ion exchanger beads on which the elemental composition analysis line was marked.

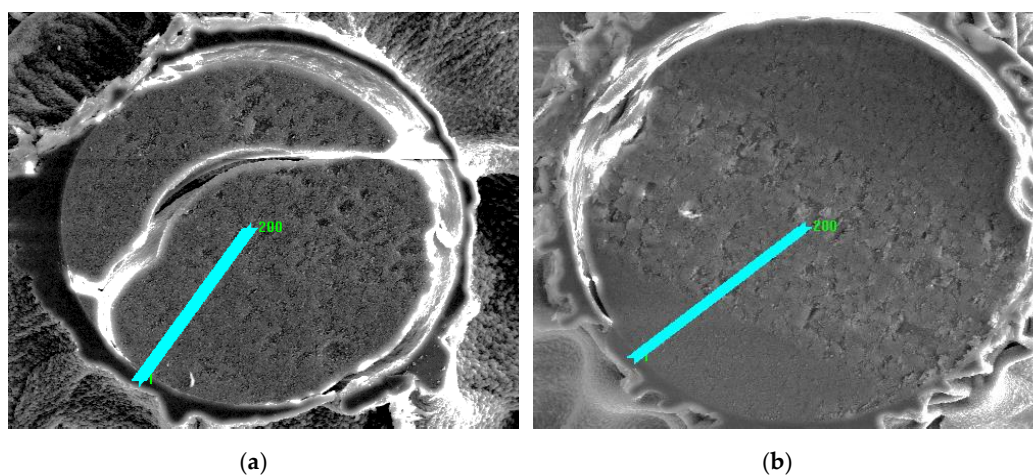


Figure 5. SEM images of lines for the analysis of the elemental composition of cut ion exchangers after the Cu (II) ion sorption process: (a) Purolite S 940, (b) Purolite S 950.

Figures 6 and 7 present the distribution of elements present in the examined ion exchangers. In Figure 8, the comparison with particular emphasis on Cu(II) ions is presented.

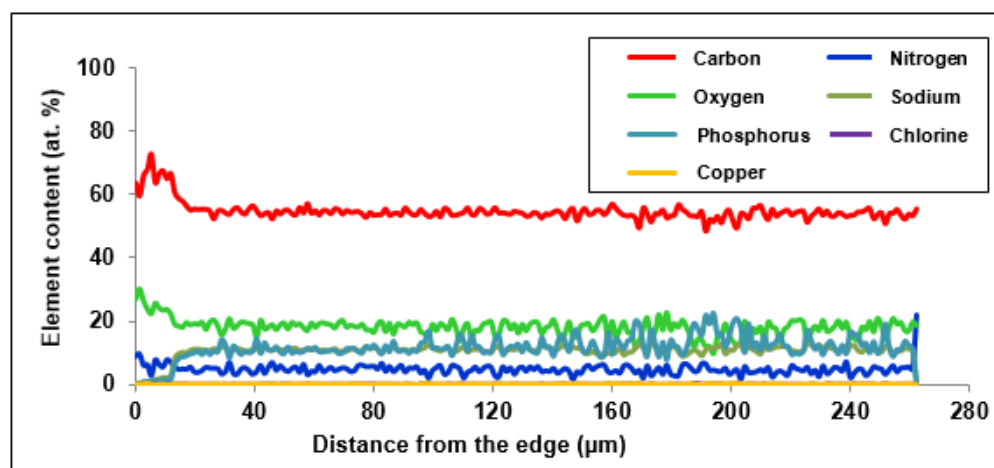


Figure 6. Distribution of the content of elements in the cut beads of Purolite S 940 after the Cu(II) ions sorption.

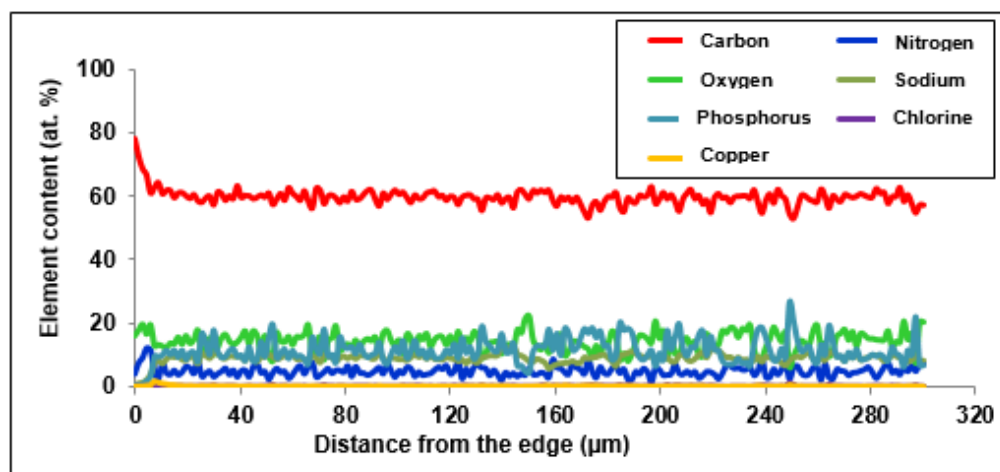


Figure 7. Distribution of the content of elements in the cut beads of Purolite S 950 after the Cu(II) ions sorption.

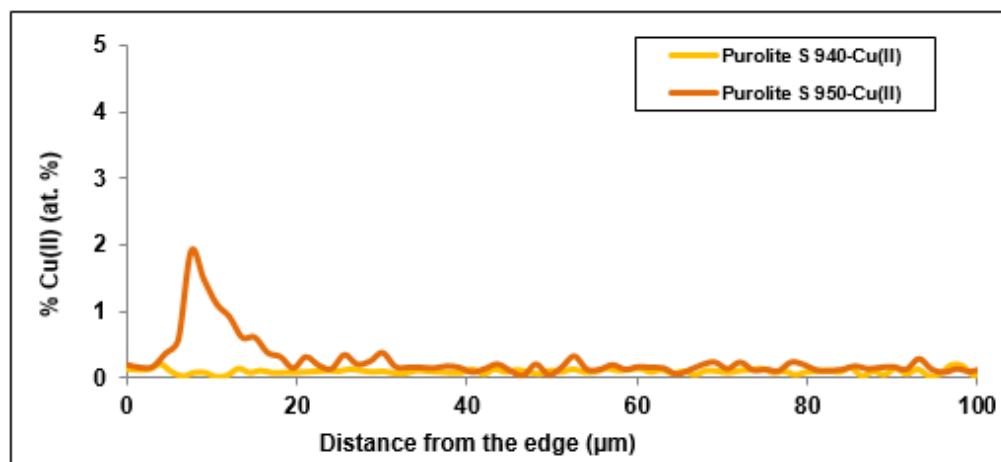


Figure 8. Distribution of copper ions in the cut beads of Purolite S 940 and Purolite S 950.

The study of the linear profile of the elemental composition of Purolite S 940 allowed us to determine the distribution of copper ions along the entire length of the profile. As follows from the research, it can be concluded that the concentration of copper ions is

evenly distributed over the entire length of the profile, with a slight increase in concentration on the surface of the tested grain. The thickness of the layer with the increased concentration is approx. 5 μm . A reduced sodium content was also observed on the grain surface in a layer with a thickness of about 12 μm (Figure 6). This may indicate the ion exchange process that takes place between Na(I) and Cu(II) ions. The distribution of the remaining elements is uniform along the entire length of the profile with a slight increase in the concentration of carbon and oxygen on the ion exchanger surface.

The study of the linear profile of the elemental composition of Purolite S 950 showed an increased content of absorbed copper ions on the grain surface. The thickness of the layer with the increased content of copper ions was approx. 16 μm . The maximum concentration in this layer was 1.9 at.% at a distance of approx. 9 μm from the edge of the ion exchanger. In the near-surface layer, where an increased concentration of copper ions was observed, the concentration of sodium ions decreased evidently. The thickness of the layer with the reduced content of sodium ions was approx. 10 μm (Figure 7). This phenomenon may suggest that the ion exchange process takes place between Na(I) and Cu(II) ions. The distribution of the remaining elements is practically uniform as is the case with Purolite S 940.

According to the literature data, the penetration depth of the sorbed Cu (II) ions on the Dowex M4195 chelating ion exchanger is approx. 40 μm [24]. In the case of the Purolite S 940 ion exchanger, the highest concentration of sorbed Cu (II) ions was observed at a distance of about 5 μm from the edge of the ion exchanger. In the case of the Purolite S 950 ion exchanger, the highest sorption of Cu (II) ions was observed for 16 μm from the edge of the ion exchanger. This was definitely a smaller penetration into the ion exchanger than in the case of Dowex M 4195. Smaller penetration into the ion exchanger grains was also observed compared with the galvanic wastewater sorption [25].

3.2. ATR-FTIR Analysis

The FTIR spectra of the ion exchangers are presented in Figures 9 and 10. Before the sorption process, a band of great intensity in the 3600–3200 cm^{-1} range was observed on the FTIR-ATR spectra of Purolite S 940 and Purolite S 950. This is related to the vibrations of the O-H and N-H groups. The bands in the range of 3000–2850 cm^{-1} correspond to the symmetric and asymmetric vibrations of aliphatic CH_2 groups. Skeletal vibrations were also observed in the range of 1600–1585 cm^{-1} and 1500–1400 cm^{-1} . The presence of bands related to the P=O stretching vibrations is observed in the range of 1350–1150 cm^{-1} and the P-OH group in the range of 1100–900 cm^{-1} [26]. The FTIR-ATR spectra also show the bands in the range 1250–1020 cm^{-1} derived from the C-N stretching vibrations of aliphatic amines. The bands in the range 730–675 cm^{-1} , corresponding to the out-of-plane deformation vibrations of the C-H groups were also observed [27–29].

The studies of Purolite S 940 and Purolite S 950 after the Cu(II) ion sorption process showed significant band shifts in the range of 1250–900 cm^{-1} . In this area, there are bands characteristic of the stretching vibrations of the P=O (1350–1150 cm^{-1}) and P-OH (1100–900 cm^{-1}) groups. Changes in the bands originating from the stretching vibrations of C-N groups present in aliphatic amines were also observed. These changes suggest the formation of a bond within the aminophosphonic functional group and Cu(II) ions.

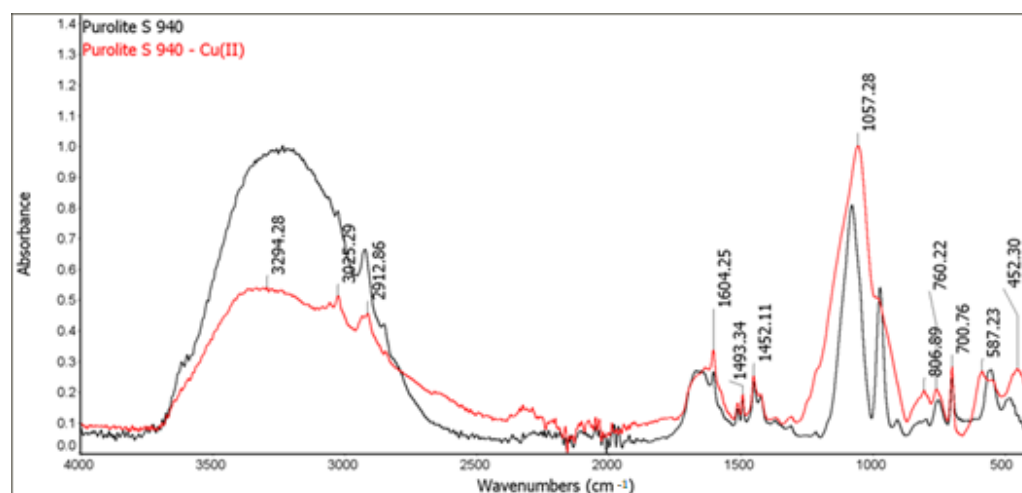


Figure 9. FTIR-ATR spectra of Purolite S 940 before and after the Cu(II) ion sorption process.

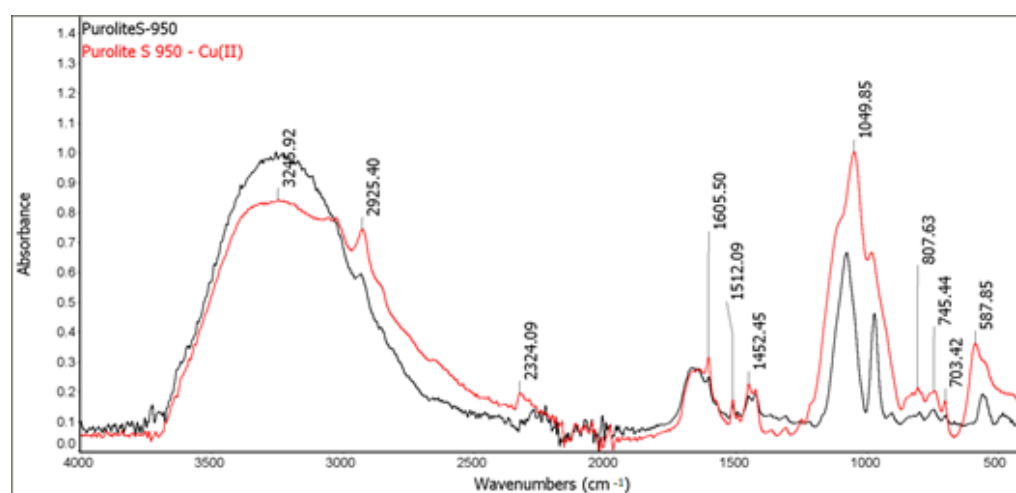


Figure 10. FTIR-ATR spectra of Purolite S 950 before and after the Cu (II) ion sorption process.

3.3. XPS Analysis

The XPS analysis was performed in wide and narrow ranges of bond energies for Purolite S 940 before the Cu(II) ion sorption process and the results are presented in Tables 2 and 3, respectively.

Table 2. The elemental composition of Purolite S 940 determined by the XPS method.

Name	Position (eV)	FWHM (eV)	Raw Area	% Atom Concentration	% Mass Concentration
C 1s	284.7	2.26	45,983.8	57.0	42.8
O 1s	531.1	2.80	46,629.1	19.7	19.7
N 1s	398.7	2.31	4747.1	3.3	2.9
Na 1s	1071.7	2.39	65,380.1	9.5	13.7
P 2p	132.2	2.35	7246.6	7.6	14.6
Cl 2p	198.2	2.45	5302.6	2.9	6.4

FWHM—full width at half maximum.

Table 3. The XPS analysis results obtained in the narrow range of binding energies for Purolite S 940.

Name	Position [eV]	FWHM [eV]	Raw Area	% Atom Concentration	Phase
O 1s	530.8	1.58	3321.4	62.0	-HPO ₃ Na
O 1s	532.3	1.50	1593.9	29.7	PO ₃ ⁻
O 1s	533.5	1.40	444.2	8.3	O-H
Na KLL	535.8	2.30	1308.2	-	-
C 1s	284.7	1.24	3598	79.2	C=C, C-C, C-H
C 1s	285.9	1.40	944.9	20.8	C-N
N 1s	399.2	1.21	289.1	58.0	C-N from an aliphatic amine
N 1s	400.3	1.27	87.5	19.2	N-H
N 1s	402.0	1.09	92.4	22.8	N quaternary
P 2p 3/2	132.3	1.58	513.1	100.0	-HPO ₃ Na
P 2p 1/2	133.2	1.70	256.5	-	
Cl 2p 3/2	198.2	1.43	345.5	100.0	NaCl
Cl 2p 1/2	199.8	1.41	172.7	-	

According to the presented results, 79.2% of the carbon present on the surface is in the form of C=C, C-C, and C-H binding. The other bonds are C-N. Of the total number of oxygen atoms, 62% are present in the form of -HPO₃Na combinations derived from the aminophosphonic functional group. The XPS tests showed the presence of three forms of nitrogen: 58.0% of nitrogen atoms are in the form of an aliphatic amine, 19.2% comes from the N-H binding of intramolecular or extra-molecular hydrogen bonds, and 22.8% of nitrogen atoms are in the form of quaternary nitrogen [30]. It is also possible to form a hydrogen bond inside the aminophosphonic group between the hydrogen of the N-H group and the adjacent oxygen or between these elements in adjacent aminophosphonic groups (Table 3) [31–39]. The percentages of individual elements are given in atomic %.

The XPS analyses were also performed in a narrow and wide range of binding energies for Purolite S 950 before the Cu(II) ion sorption process. The results are presented in Tables 4 and 5.

Table 4. The elemental composition of Purolite S 950 determined by the XPS method.

Name	Position [eV]	FWHM [eV]	Raw Area	% Atom Concentration	% Mass Concentration
C 1s	284.7	2.26	51,190	56.8	54.9
Na 1s	1071.2	2.39	65,739.4	8.6	15.9
N 1s	398.7	2.34	7124.4	4.4	5.0
P 2p	132.7	2.58	10,396	9.7	24.2
O 1s	530.6	2.55	54,043.2	20.5	26.4

Table 5. The XPS analysis results were obtained in the narrow range of binding energies for Purolite S 950.

Name	Position (eV)	FWHM (eV)	Raw Area	% Atom Concentration	Phase
O 1s	530.8	1.47	3937.8	69.9	-HPO ₃ Na
O 1s	532.2	1.45	1223	21.7	PO ₃ ⁻
O 1s	533.3	1.45	472.3	8.4	O-H
C 1s	284.7	1.32	3755	81.4	C=C, C-C, C-H
C 1s	285.8	1.4	857.4	18.6	C-N

N 1s	399.1	1.17	380.2	67.7	C-N from an aliphatic amine
N 1s	400.1	1.30	98.5	17.2	N-H
N 1s	401.8	1.30	90.1	15.1	N quaternary
Na 1s	1071.7	1.77	7112.4	100	-HPO ₃ Na
P 2p 3/2	132.3	1.53	678.5	100	PO ₄ ³⁻
P 2p 1/2	133.3	1.70	339.2	-	-

In the case of Purolite S 950, 81.4% of carbon present on the surface is in the form of C=C, C-C, C-H binding, while 18.6% of carbon is in the form of CN binding. Out of the total number of oxygen atoms, 69.9% is in the form of -HPO₃Na binding derived from the functional aminophosphonic group, the other forms occur as the PO₄³⁻ and O-H bonds. As for nitrogen 67.7% is in the form of C-N bonds, 17.2% in the form of N-H bonds forming intramolecular or extra-molecular hydrogen bonds, and 15.1% of nitrogen atoms are in the form of quaternary nitrogen. Alike Purolite S 940, the formation of hydrogen bonds is not excluded [33–39]. In order to investigate changes in the chemical bonds of functional groups as a result of the sorption process, XPS tests were also performed for Purolite S 940 and Purolite S 950 after the Cu(II) ion sorption process. The test results for Purolite S 940 are presented in Tables 6 and 7 and in Figure 11. For Purolite S 950, the results are presented in Tables 8 and 9 and Figure 12.

Table 6. The elemental composition determined for Purolite S 940 after the Cu(II) ion sorption process.

Name	Position [eV]	FWHM [eV]	Raw Area	% Atom Concentration	% Mass Concentration
C 1s	284.7	2.31	55,326.2	64.2	47.6
O 1s	531.2	2.65	49,409	19.6	19.3
Cu 2p	932.7	3.83	63,978.2	2.9	11.5
P 2p	132.7	2.66	8811.87	8.6	16.4
N 1s	400.7	3.40	5819.9	3.8	3.2
Cl 2p	198.7	1.90	1779.63	0.9	2.0

Table 7. The XPS analysis results obtained in the narrow range of binding energies for Purolite S 940 after the Cu(II) ions sorption.

Name	Position (eV)	FWHM (eV)	Raw Area	% Atom Concentration	Phase
O 1s	531.2	1.50	2725.7	56.7	-HPO ₃ Na
O 1s	532.1	1.42	1242.7	25.9	PO ₃ ⁻
O 1s	533.1	1.50	837.5	17.4	O-H
C 1s	284.7	1.41	4240.3	75.9	C=C, C-C, C-H
C 1s	285.9	1.38	900.9	16.1	C-N
C 1s	286.9	1.40	197.1	3.5	C-N
C 1s	291.5	2.30	249.9	4.5	π→π*
N 1s	400.2	1.60	148.7	45.0	C-N from an aliphatic amine
N 1s	402.0	1.58	139.4	38.5	N-H
N 1s	403.4	1.60	62.9	16.5	N quaternary
P 2p 3/2	132.9	1.65	576.6	100.0	PO ₄ ³⁻
P 2p 1/2	133.8	1.67	288.3	-	

Cl 2p 3/2	198.6	1.60	108.2	83.1	CuCl ₂
Cl 2p 1/2	200.2	1.42	54.1	-	
Cl 2p 3/2	201.6	1.29	22	16.9	
Cl 2p 1/2	203.2	1.60	11	-	
Cu 2p 3/2	932.7	1.30	954.4	22.0	Cu(0), Cu(I)
Cu 2p 3/2	934.3	3.00	2181.2	50.3	
Cu 2p 3/2	939	3.00	218.1	5.0	Cu(II)
Cu 2p 3/2	941.8	3.50	654.4	15.2	
Cu 2p 3/2	944	2.00	327.2	7.5	

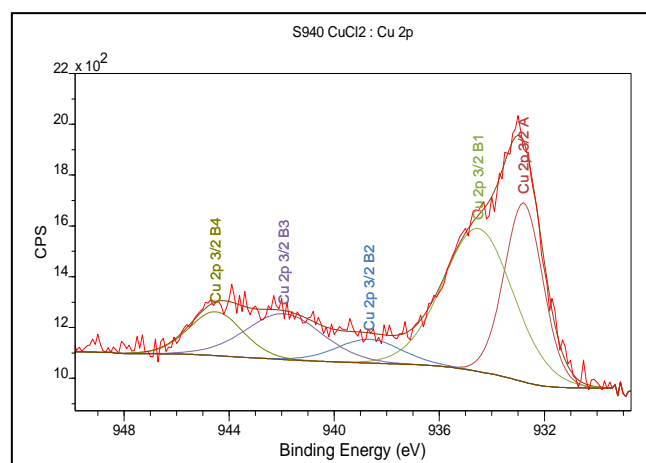


Figure 11. The XPS spectrum obtained in the narrow range of binding energy for Purolite S 940 after the Cu(II) ion sorption process.

Table 8. The Elemental composition determined for the Purolite S 950 after the Cu(II) ion sorption process.

Name	Position (eV)	FWHM (eV)	Raw Area	% Atom Concentration	% Mass Concentration
C 1s	284.7	2.36	25,887	57.6	43.3
Na 1s	1071.7	2.36	24,040.9	6.3	9.1
P 2p	132.7	2.33	5753.8	10.8	21.0
N 1s	399.2	3.94	3699.1	4.6	4.3
Cu 2p	933.7	2.96	6133.3	0.5	2.0
O 1s	531.2	2.61	26,609.4	20.2	20.3

Table 9. The XPS analysis results obtained in the narrow range of binding energy for Purolite S 950 after sorption of Cu(II) ions.

Name	Position (eV)	FWHM (eV)	Raw Area	% Atom Concentration	Phase
O 1s	530.7	1.42	1558.4	60.1	-HPO ₃ Na
O 1s	531.7	1.60	690.2	26.6	(PO ₃) ⁻
O 1s	532.9	1.54	343.9	13.3	O-H
C 1s	284.7	1.30	2032.6	81.0	C=C, C-C, C-H
C 1s	285.9	1.30	392.5	15.6	C-N
C 1s	291	2.01	83.6	3.3	π→π*
N 1s	399.3	1.32	212.0	61.5	C-N from an aliphatic amine
N 1s	400.7	1.38	43.8	12.8	N-H

Chelating ion exchangers can therefore behave as typical ion exchangers (a), they can undergo protonation reactions (b) or the reaction of complexing metal ions (c) can take place in the sorption process. In addition, it should be noted that, depending on the pH, the aminophosphonic group can exist in the following forms (Figure 14):

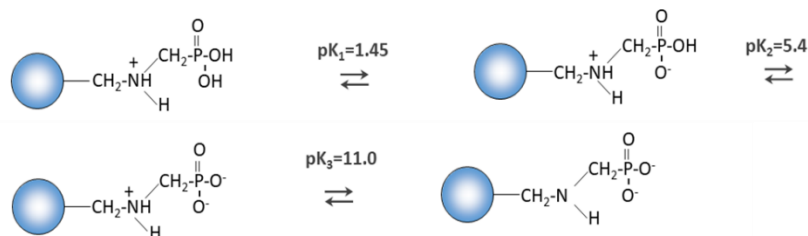


Figure 14. Forms of ion exchangers depending on the pH of the solution.

In the case of acidic solutions, as a result of the protonation of the nitrogen atom of the aminophosphonic group in the process of sorption of metal ions, connections with the following structure are formed (Figure 15):

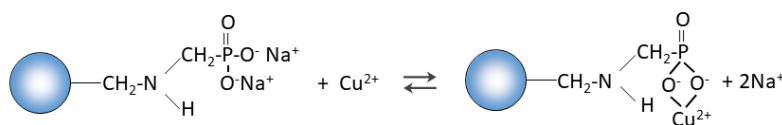


Figure 15. Forms of ion exchangers in acidic solution.

In the case of the conducted research, the participation of oxygen atoms in the sorption process of Cu (II) ions was observed as in Figure 15. Moreover, the XPS tests also showed the participation of nitrogen atoms in the formation of the bond with sorbed copper atoms, which made it possible to propose the following sorption process mechanism for Purolite S 940 and Purolite S 950 (Figure 16):

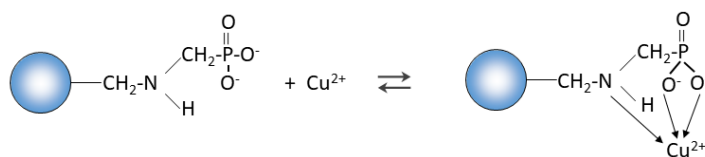


Figure 16. Proposed sorption mechanism.

The microscopic studies showed the possibility of ion exchange between Na(I) and Cu(II) (Figure 17).

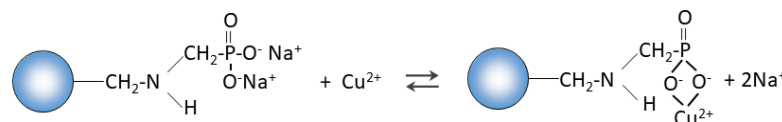


Figure 17. Possibility of ion exchange between Na(I) and Cu(II).

4. Conclusions

The studies with spectroscopic methods allowed for a comprehensive evaluation of the processes taking place during the sorption of Cu(II) ions on Purolite S 940 and Purolite S 950. The research allowed us to suggest the mechanism of Cu(II) sorption on the Purolite S 940 and Purolite S 950 chelating ion exchangers. The research confirmed that the sorption process takes place mainly on the surface of the examined ion exchangers.

The microscopic studies showed a different course of the Cu(II) sorption process on these ion exchangers. In the case of Purolite S 940, a uniform distribution of Cu(II) ion concentration was observed throughout the grain volume. In the case of Purolite S 950, the increased sorption of Cu(II) ions on the ion exchanger surface were demonstrated. The microscopic studies also showed the possibility of the ion exchange process between the Na(I) ions and the sorbed Cu(II) ions on Purolite S 940 and Purolite S 950.

The FTIR and XPS analyses exhibited some changes in the spectra of Purolite S 940 and Purolite S 950 before and after the process of Cu(II) ions sorption. These changes indicate the participation of nitrogen and oxygen present in the aminophosphonic functional groups in the sorption process. The research proved that in the process of sorption of Cu(II) ions on the chelating ion exchangers Purolite S 940 and Purolite S 950, both the ion exchange process and the formation of a coordination bond with the participation of free electron pairs of nitrogen and oxygen in the aminophosphonic functional groups take place.

The microscopic tests confirmed the kinetic test results in which the better efficiency of the Cu (II) ion sorption process was obtained for the Purolite S 950 ion exchanger.

The linear relationship $t/q_t = f(t)$ and the values of the determination coefficients (R^2) close to unity as well as good agreement with the experimental data showed that the pseudo second-order kinetic model is fully suitable for the description of the sorption process. The studies of the sorption of Cu(II) ions from the 0.001 CuCl₂ solutions showed better process efficiency on Purolite S 950 ion exchanger ($q_t = 9.88 \text{ mg g}^{-1}$) compared to Purolite S 940 ionite ($q_t = 8.66 \text{ mg g}^{-1}$).

The research allows us to state that spectroscopic methods are effective in the sorption processes studies.

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