



# **Binding Materials for MOF Monolith Shaping Processes: A Review towards Real Life Application**

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Abstract: Metal-organic frameworks (MOFs) could be utilized for a wide range of applications such as sorption, catalysis, chromatography, energy storage, sensors, drug delivery, and nonlinear optics. However, to date, there are very few examples of MOFs exploited on a commercial scale. Nevertheless, progress in MOF-related research is currently paving the way to new industrial opportunities, fostering applications and processes interconnecting fundamental chemistry with engineering and relevant sectors. Yet, the fabrication of porous MOF materials within resistant structures is a key challenge impeding their wide commercial use for processes such as adsorptive separation. In fact, the integration of nano-scale MOF crystallic structures into bulk components that can maintain the desired characteristics, i.e., size, shape, and mechanical stability, is a prerequisite for their wide practical use in many applications. At the same time, it requires sophisticated shaping techniques that can structure nano/micro-crystalline fine powders of MOFs into diverse types of macroscopic bodies such as monoliths. Under this framework, this review aims to bridge the gap between research advances and industrial necessities for fostering MOF applications into real life. Therefore, it critically explores recent advances in the shaping and production of MOF macro structures with regard to the binding materials that have received little attention to date, but have the potential to give new perspectives in the industrial applicability of MOFs. Moreover, it proposes future paths that can be adopted from both academy and industry and can further boost MOF exploitation.

**Keywords:** polymer binders; inorganic binders; metal–organic frameworks; monoliths; shape engineering; applications

### 1. Introduction

Metal–organic frameworks (MOFs) are organic–inorganic hybrid crystalline microporous materials [1]. They consist of positively charged metal ions interconnected with organic ligands [2]. This regular array of metal ions can therefore be formed as a network with up to three dimensions [3]. MOFs are typically characterized by high porosity, low density, and excellent biocompatibility [4]. These properties render them excellent candidates for applications related to sorption, catalysis, chromatography, energy storage, sensors, drug delivery, and nonlinear optics [5–7]. Recently, apart from an in-lab investigation, MOFs have been examined for industrial applications as well. In fact, the large production of a small number of MOFs, such as HKUST-1, ZIF-8, MOF-5, MIL-101, and MOF-177, has been successful and they are currently available on the market [8]. However, in order to develop MOF materials of high efficiency into real life applications, high-tech and sophisticated engineering is necessary for tuning their chemical structure and, hence, their properties at the macroscopic scale [9]. For example, at an industrial scale, properties such as the size and the shape of the corresponding MOF have profound effects on both the



Citation: Ntouros, V.; Kousis, I.; Pisello, A.L.; Assimakopoulos, M.N. Binding Materials for MOF Monolith Shaping Processes: A Review towards Real Life Application. *Energies* 2022, *15*, 1489. https:// doi.org/10.3390/en15041489

Academic Editor: Cai Shen

Received: 25 January 2022 Accepted: 15 February 2022 Published: 17 February 2022

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**Copyright:** © 2022 by the authors. Licensee MDPI, Basel, Switzerland. This article is an open access article distributed under the terms and conditions of the Creative Commons Attribution (CC BY) license (https:// creativecommons.org/licenses/by/ 4.0/). performance and the processes of the final application, and therefore need to be tailored accordingly [10].

Conventional MOFs are typically synthesized in the form of a crystalline powder with crystallite sizes that range from the nano- to hundreds of micron-scale [11–15]. Nevertheless, MOFs in powder form cannot be easily utilized in industrial applications. In fact, it is reported that a MOF powder may decrease the pressure within a pipeline, reduce, or even completely block the flow [16]. It can also lead to abrasion owing to powder blowing, while the significant reduction of the pure MOF component is also reported due to powder application. Moreover, other reported issues related to MOF powder are dustiness, clogging, and transfer and handling impediment [8,17]. Aiming to overcome these intrinsic issues that MOF powders are prone to, several other synthesis protocols have been tested and evaluated for industrial applications. These synthetic formulation methodologies aim to agglomerate MOF crystallites and shape them into granules, films, foams, gels, monoliths, tablets, or pellets [18,19].

The main criteria for choosing the appropriate synthetic methodology for industrial scale applications of MOFs are their mechanical strength, surface area, chemical stability, and the binder used [20]. Good mechanical strength is necessary for withstanding the pressure exerted by a reactor or column in which the gas flow takes place for gas absorption or separation, catalysis, and similar applications [8,21]. However, MOFs in powder form are not suitable for such applications due to poor mechanical performance, and therefore, they need to be shaped with respect to the desired applications and their process conditions [22,23]. Apart from the mechanical properties, the shaped MOF should have a sufficient size for maintaining the diffusion effect among particles and should maintain as much as possible the porosity and crystallinity of the powder form [5]. Thus, several comparative techniques have been applied for ensuring the good porosity of the developed MOF structures such as those explored by Lorignon et al. in their respective review study [24]. Ensuring the chemical stability of the developed MOF is also crucial. In fact, particularly when the performance of a MOF depends on the pH, chemical stability tests should be carried out for selecting the appropriate binder [25–27]. Choosing the appropriate binder is of high importance, since it ensures the good performance of MOF materials. In fact, MOFs typically lack cohesive force and their crystallinity/porosity can be easily damaged when high pressure is applied. Therefore, in many cases, a binder is applied during their synthesis for reducing the energy and thus improving the efficiency of the process [8].

Several shaping methods are reported within the literature and are typically categorized as (i) non-pressurized processes without binders [28], (ii) pressurized processes without binders [29], (iii) pressurized processes with binders [30], and (iv) non-pressurized processes with binders [31]. The resulting structures of shaped MOFs vary with respect to the application and can be monoliths, pellets, tablets, foams, or granules. For instance, granulation is a conventional non-pressurized technique for agglomeration shaped MOF powders without modifying the chemical characteristics [32]. The addition of binders, such as graphite, silica, and cellulose ester, has been found to enhance the mechanical stability, yet it may decrease the effective surface area of the MOF since the binder may cover the crystals' surface. Pelletization is a pressurized particle agglomeration technique involving applying pressure to powders, either by adding a binder (wet pelletization) or not (dry). Similar to the agglomeration techniques, although the addition of a binder may improve the mechanical stability of the MOF pellet, it could also decrease the surface area of the MOF as it blocks the pores [33].

Since their introduction in the late 1990s [34], MOFs have been utilized in numerous applications [35]. Given the blossoming research around MOFs, today's questions might find their answers sooner than expected, as experiments or real-life applications of MOFs surface rapidly [36]. MOFs' intrinsic features may make them suitable for applications in sectors in which these materials might not have had traditional uses. For example, a sector in which there is much space for improvement with regard to the applications MOFs might

be suitable for is the building sector (i.e., to improve the indoor air quality, in filters for air purification, in dehumidifiers, integrated into heat transformation cycles for heating and cooling applications, natural gas storage, CO<sub>2</sub> capture and storage); however, given the powdery nature of MOFs, as is the case in most industrial sectors, it is still not possible for MOFs to be integrated into the envelopes of buildings or in their systems, and as a result, there are few applications that link MOFs' intrinsic characteristics with the elements of a building (e.g., the walls, systems, and interior decoration objects). Bearing this in mind, the solution to pave the way for MOFs to find their position within the building stock and in other industrial topologies might be hidden due to the lack of information on how to turn powder into a monolith [37], which would make it easier to find an application such as hydrogen or natural gas storage [38–40]. Within this context, we conducted a literature review with regard to the binders used for MOF shape processing into monoliths, granules, or pellets, since their ease of handling and more rigid nature compared to thin films, foams, and gels make them more suitable for in-house applications.

#### 2. Materials and Methods

A synthetic approach is followed in the methodology design of this review study (Figure 1). In this review, we aggregated and assessed the outcomes from a set of strategically chosen target publications in order to juxtapose the results of diverse experimental investigations. Evidence-based research methodologies that aim to provide consolidated outcomes, such as identifying scientific gaps/challenges and clearing the path for future breakthroughs in the relevant sector, were included. In this approach, the following four sub-steps were included in order to reduce biases and random errors:

- 1. Identify a scientific problem that must be solved.
- 2. Establish precise inclusion/exclusion requirements for studies related to the topic under consideration.
- 3. Conduct a critical analysis of the studies that have been chosen.
- 4. Draw a conclusion to the research blank spots and suggest future directions.

Initially, the next research question was outlined as the major impetus of this systematic review study:

(a) What are the most suitable binding materials for MOF monolith shape engineering processes such as granulation and pelletization?

As a result, for a more precise investigation, the sub-questions below were put in place.

- i. What are the recent advances in MOFs granulation and pelletization shape engineering processes?
- ii. In what kind of applications were the engineered products used?

For the purposes of this study, Web of Science (WoS) and Scopus were considered the principal online search engines. Furthermore, Google Scholar was used to locate (a) grey literature relevant to the research problem, (b) key researchers' work from the author's perspective, and (c) cited articles encountered in previously reviewed studies within the presented review. The web search was conducted between December 2021 and January 2022.

Following this, unique search phrases linked to "binders", "monoliths", and "shape engineering processes" for MOFs were defined and merged for use in academic databases using the logical operators "and" and "or". The results from both online scholarly databases were then combined and repetitions were checked. Inclusion criteria were then applied to the remaining papers to determine whether or not they were eligible for inclusion in the analysis. No time-frame exclusion parameters were used in order to capture the continuity of the advances in the field through time. Despite this, most of the papers analyzed were from 2017 to 2021.





Eventually, three screening procedures were implemented. Studies both for binders and shaping processes were either included or excluded in the first phase by scanning the respective abstracts, and in the second phase by continuing to read the entire article. The articles were collected using a snowball selection method in the final screening stage [41]. More specifically, several articles were not discovered immediately using the keyword search results, but rather through the reference lists of the publications chosen in the second screening test, and their results were deemed significant. In the end, the total number of articles included in the study was 61.

In addition, the VOS Visualizer tool [42] was used to refine the abovementioned search terms in order to explore the way multi-objective optimization (MOO) models [43] are used throughout the MOF shape engineering processes. The artificial intelligence-based tool puts the keywords provided in order as well as the elements found in the articles' titles and



abstracts, and then performs a classification to cluster the most frequent words into groups (Figure 2).

🔥 VOSviewer

**Figure 2.** Clustering of keywords set by the authors, and words found in the selected articles' titles and abstracts. (Source: https://www.vosviewer.com/, accessed on 24 January 2022).

#### 3. Findings from Literature

MOFs are usually shaped through approaches such as extrusion (Figure 3), granulation (Figure 4) or compression (Figure 5) that have traditionally been utilized to shape other porous materials like zeolites or porous carbons. The main shaping procedure involves (i) mixing the MOFs with adhesive agents; (ii) forming the MOF powder-additives paste into a body; (iii) removal of solvents; and (iv) thermal treatment of the macrostructure, whereas the main criteria for shape engineering the MOFs are mechanical strength, surface area and porosity, and chemical and thermal stability. Extrudates in the form of pellets, thin wafers, tablets, monoliths, beads, spheres, or granules are the most popular forms of MOFs macrostructures. In order to attain a sufficient mechanical strength, most of these structures require an adhesive agent or binder that allows them to behave as a shaped body instead of a powder. Interestingly, there are occasions in which monoliths are produced by applying high pressure to the powder in the absence of any binding agent; however, this applies to MOFs that can withstand high compression forces without losing their porosity and crystal structure. Thus, in most cases, adding an organic and/or an inorganic binder into slurry MOF pastes is necessary for the macrostructure's mechanical strength and chemical and thermal stability in order for a rigid and robust body to be shaped that maintains its porous characteristics. For example, when selecting the proper binder, its chemical and physical characteristics (e.g., solubility, viscosity, chemical bonding groups, temperature of calcination) should be considered in relation to the MOF's characteristics, as the former may influence the latter, and as a result, the shaped body might not be as effective as expected in the application for which it was initially designed. Therefore, a good knowledge of MOFs' characteristics when shaped into monoliths, as well as the requirements of the target application, will further help in the selection of a successful binder among organic (i.e.,



polymers, cellulose, sucrose) and inorganic (i.e.,  $\rho$  alumina, clays, silica) binders, or may even indicate binderless procedures.

Figure 3. Schematic illustration of a single screw extrusion process and the formed extrudates.



Figure 4. Schematic illustration of a wet granulation process.



Figure 5. Schematic illustration of a pressing procedure and the formed pellet.

# 3.1. Processes with Organic Binders

The shaping processes of MOFs into monoliths, granules, or pellets usually utilize polymer-type adhesive agents, as this type of binder is easily mixed with MOFs, inducing non-covalent bonding (i.e., hydrogen bonding); in addition, they are soluble to volatile agents [44]. In general, organic binders are synthesized by polymers with a chain-like structure of various lengths, where polar groups exist [45]. The most widely used polymer-type binders in MOF shaping processes is polyvinyl alcohol (PVA) and polyvinyl butyral

(PVB). PVA, with its molecular formula being  $C_2H_4O$ , is a white powder that has good solubility in water, is less soluble in ethanol, and is insoluble to most organic solvents. This hydrophilic binder has a melting point between 212 and 267 °C, depending on the degree of hydrolysis of the polyvinyl acetate during its production [46,47]. On the other hand, PVB ( $C_{16}H_{28}O_5$ ), a white powder synthesized from PVA and butyraldehyde with a melting point in the range of 165–185 °C, is insoluble in water, but soluble in solvents frequently used in MOF production, such as ethanol, methanol, and DMF; however, its solubility is strongly dependent on the vinyl alcohol content [47,48].

Less frequent binders used in MOF shaping processes are polyethersulfone (PES), polyvinyl pyrrolidone (PVP), methyl cellulose (MC), and hydroxypropyl cellulose (HPC). PES,  $(C_{12}H_8O_3S)_n$ , comes in light amber pellets. It is insoluble in water, but soluble in high polar solvents. It is the most temperature-resistant thermoplastic commercially available; PES absorbs moisture due to its highly hygroscopic sulfone groups [49,50]. PVP,  $(C_6H_9NO)_n$ , also named povidone, is soluble in water as well as in ethanol and methanol. It comes as a white hygroscopic powder and melts at 160 °C [51]. MC is a hydrophilic white or yellow-white powder, with a melting point in the range of 290–305 °C. Interestingly, MC is soluble in cold water, but insoluble in hot water or ethanol [52]. Finally, HPC is a white to cream powder that melts at 371 °C and is soluble in water and organic solvents such as methanol and ethanol [53]. As seen, organic binders' high melting points that allow for MOFs' heat treatment or drying, and their solubility in water and/or in organic solvents frequently used in MOF synthesis, make them promising candidates as adhesive agents that provide the required mechanical stability in MOFs' shaped engineered structures. Zheng et al. used PVB to pelletize TIFSIX-2-Cu-I, SIFSIX-3-Ni, GEFSIX-2-Cu-i, and SIFSIX-2-Cu-I MOFs and the process was deemed to have a great potential for industrial applications [27]. It was found that although PVB reduced MOFs' surface area (2.9%, 17.5%, 12.7%, and 15.2%, respectively), it had negligible influence on the adsorption of  $C_2H_2$ , whereby it did not severely affect the structure of the MOFs. In the same study, Mg-MOF-74, HKUST-1, and MIL-101-Cr were also pelletized with PVB as the binding material and then tested for their CO<sub>2</sub> adsorption performance, showing that they kept the characteristics of CO<sub>2</sub> adsorption capacity; for 90% of the loaded pellets with MOF content, 11.2%, 13.6%, and 19.3% reductions in  $CO_2$  adsorption quantity were observed, respectively. Gaikwad et al. also used PVB (4%) to shape MOF-177 and MOF-177-TEPA-20% powder samples into pellets, and reported a reduction in  $CO_2$  uptake for both samples due to pore blockage and impacts on crystallinity as a result of the process. The MOF-177-TEPA-20% pellet adsorbed 3.3 mmol/g of  $CO_2$  (4 mmol/g in powder form), which was 5.8 times higher than that of the pristine MOF-177 pellet [54]. Taddei et al. used PVB, PVA, and sucrose as binders to form MOF-801 pellets using the single screw extruder method. While the sucrose pellets were brittle, the PVA and PVB pellets had good mechanical stability, with PVB showing the highest durability in drop and shake tests. PVB pellets prepared under lower compression (146 MPa for 15 s) were found to have better  $CO_2$  working capacity than those prepared under higher compression (438 MPa, 15 s) [55]. Sucrose was also used as adhesive agent (10 wt%) for pelletizing active Zr-MOF crystals for hydrogen storage applications [56]. The shaped Zr-MOF with the use of a centrifugal granulator had good mechanical strength, but lost almost half of the H<sub>2</sub> uptake and surface area compared to the pristine powder. In Chanut et al., a polymer–binder mixture containing PVA and PVB was used to shape UiO-66(Zr), UiO-66(Zr)-NH<sub>2</sub>, MIL-100(Fe), and MIL-127(Fe) MOF granules and test them on their adsorption of various gases such as methane, carbon dioxide, carbon monoxide, and others. The granules showed decreased BET areas in the order of 10% or higher for MIL-100(Fe) and UiO-66(Zr), whereas this reduction for the other two granules was in the order of 4–5%. Interestingly, when activating MIL-127(Fe) powder and granules, higher enthalpies were observed for the powder, and this might be an indication that the binding material may act as a "stabilizer" in a greater oxidized state [57]. Hindocha and Poulston utilized PVA (2 wt%) to form CPO-27(Ni), MIL-100(Fe), and Cu-BTC granules through wet granulation and tested their ammonia adsorption performance for applications in

respiratory protection filters [58]. CPO-27(Ni) and MIL-100(Fe) displayed similar uptake capacities for ammonia (51 and 50 mg/g, respectively), whereas for Cu-BTC, this was equal to 19 mg/g.

In a notable study [29], ZIF-8 crystals were shaped into resistant pellets by employing 55 different binder recipes, i.e., cellulose-acetate (CA), polyvinylchloride (PVC), polyvinylformal (PVF), polyetherimide (PEI), and polystyrene (PS). For the formulation of the structures, the researchers followed an extrusion-crushing-sieving (ECS) method. The binder recipes were evaluated with respect to their stability in terms of mechanical, acid/base, hydrothermal, and life span. The results of the chemical stability and mechanical strength tests showed that the PVF binder outperformed the others. In another study, also conducted by Cousin-Saint Remi et al., a composite ZIF-8/PVF material with an 85% MOF content in the form of beads was developed that demonstrated high crushing strength (3.09 N/Pc) and thermal stability up to 200 °C. Again, the amount of binder in the material proportionally reduced its adsorption capacity [59]. Similarly, Abbasi et al. utilized a phase inversion method and polyethersulfone as a binder to develop rigid, easy to handle, and recyclable ZIF-8/PES composite beads for oil sorption applications, which was able to retain up to 88% of its sorption capacity after five regeneration cycles [60]. Hastürk et al., through freeze-casting, successfully developed hydrothermal stable Alfum, MIL-160(Al), and MIL-101(Cr) monoliths using various polymer binders. From those, the monoliths with the PVA binder showed the highest mechanical stability; PEI exhibited the least, given that it is a liquid at room temperature, whereas sodium polyacrylate (PAANa) was the most hydrophilic, according to its water vapor uptake in contrast to polyethylene glycol (PEG) [61].

In [62], Cu<sub>3</sub>(BTC)<sub>2</sub> was combined with PVA to form pellets. After pelletizing, the structural integrity was preserved, but the textural qualities decreased to some extent. The  $Cu_3(BTC)_2$  powder was very hydrophilic, and following pelletization, its water-sorption capacity decreased. Despite a minor decrease in saturation capacity compared to the powders,  $CO_2$  adsorption employing ground/sieved  $Cu_3(BTC)_2$  pellets provided a better breakthrough pattern. Finsy et al. investigated the adsorption of CH<sub>4</sub>/CO<sub>2</sub> mixtures from MIL-53(Al) pellets produced with a PVA binder. As shown, the use of polyvinyl alcohol as a binder leads to a 32% reduction in total capacity, as demonstrated by  $N_2$  adsorption isotherms [63]. In another study, a novel approach employed a Pickering High Internal Phase Emulsion (HIPE) template to prepare UiO-66/PVA monoliths with PVA playing a key role, not only as an adhesive, but also as a stabilizer to Pickering HIPEs [64]. According to Grande et al., when UTSA-16 was combined with PVA as binder and a mixture of water and propanol as a plasticizer and then extruded, it was revealed that if more PVA is used, the crushing strength increases significantly at the expense of a reduction of the surface area; a content of 3% of PVA results in a surface area reduction of 5%, given that the sample is activated at 393 K [65]. Based on the same shaping technique, Agueda et al. prepared UTSA-16 extrudates with PVA and measured the adsorption equilibrium and kinetic data of hydrogen, methane, and other important gases, and then simulated a pressure swing adsorption process for hydrogen purification from the steam methane reforming off-gases [66]. According to the study, a higher than 93% recovery of hydrogen can be achieved with 99.9% purity.

In another study, Alfum and MIL-101(Cr) were formatted into monoliths with PVA as an adhesive material using a phase separation approach, whereby in order to maintain the monolith shape and avoid shrinkage, vacuum drying is preferred over supercritical and freeze-drying [67]. Edubilli and Gumma [68] pelletized UiO-66 powder with PVA as a binding agent (15 wt% PVA in water) and it was observed that about 9.3 wt% of PVA was required to make mechanical stable pellets against the drop test. As noted, the formation into pellets decreased the  $CO_2$  gravimetric adsorption capacity by about 14%. PVA was also used as an adhesive agent to form MIL-101(Cr) tablets in a study [69] that addressed the characteristics of MIL-101(Cr) as a methanol adsorbent for adsorptive heat transformation (AHT) cycles, a technology for heating and cooling. As revealed,

adding PVA to MIL-101(Cr) did not impact its adsorption equilibrium with methanol vapor. Delgado et al. reported a smaller than 3% decrease in surface area for a PVA loading of 2.9% in ZIF-8 and HKUST-1 extrudates [70]. The findings showed that the nitrogen adsorption capacity of the extrudates drops as the PVA concentration increases, but the curve of the adsorption isotherms is not altered, showing that the PVA molecule does not reduce the sample's micropore volume and, hence, is not maintained in the MOF's pores. Pellets with 80% MOF content, in the order of millimeters, were produced through the freeze granulation approach in [71] for sorption-driven chiller systems with PVA as an adhesive. The four different MOF pellets (MOF-801, UiO-66, Alfum, and MIL-160(Al)) were highly resistant to mechanical stress exerted from 14 N up to 79 N, while the MOFs maintained their uptake capacity and porosity. Lorignon et al. obtained MIL-96(Al) from Li-Ion battery waste through a Pickering emulsion template, added PVA, and produced oval, rice-like monoliths. The PVA stabilized the emulsion and increased the creation of pore throats, which enhanced the porous network's interconnections [72]. Khabzina et al. [31] reported on an upscaled fabrication and shaping of a zirconium-based MOF, i.e., UiO66-COOH, for NH<sub>3</sub> air purification. Freeze granulation and extrusion techniques were chosen for the shaping. Through freeze granulation, they developed MOF beads, while with extrusion they developed MOF extrudates, both of a particle size ranging between 425 and 600  $\mu$ m.

For the shaping, they used either PVA or polysiloxane (silicon resin) as the binder. Kreider et al. reported on the developments of a prototypical MOF, made with MOF-5 and acrylonitrile butadiene styrene (ABS), aiming to address one of the main drawbacks of MOFs, i.e, processibility [73]. The shaping into a filament was done with extrusion at 195 °C and the composite was fabricated with a commercially available thermoplastic 3D printer. The results showed that the incorporation of MOFs into polymers made with conventional 3D printers can maintain their intrinsic properties. Recently, polyvinylpyrrolidone (PVP) was used as the binding agent to form ELM-11 pellets [74]. As shown, the characteristic stepwise CO<sub>2</sub> uptake of the pristine powder was lost after the formation into pellets and a slacking of the gate adsorption was observed, which is considered to take place due to the weight of the polymer binder. In other work [75], PVP (2%) was utilized as a binding agent in a MIL-100(Fe)/RD silica gel composite monolith produced under compression with regard to an ultra-low heat-driven atmospheric water harvesting (AWH) system; the performance of the system was significantly increased compared to the silica gel-based AWH system—up to 187%.

Park et al., in a notable study, shaped MOF/polyvinylidene fluoride (PVDF) beads via a phase inversion approach and observed that the uptake  $CO_2$  capacity of the beads with 40% PVDF content was maintained after exposure to 60% humidity at room temperature for up to 30 days, which is a promising result for  $CO_2$  capture applications in indoor environments [76]. Munusamy et al. prepared granules of MIL-101(Cr) with sodium salt of carboxyl methyl cellulose (CMC) and starch as a binder and conducted volumetric sorption measurements of CO<sub>2</sub>, CH<sub>4</sub>, N<sub>2</sub>, and CO [77]. It was observed that the selectivity of gases for granules and powder did not change, although the uptake capacity of the granules reduced by 50% compared to the powder. Kriesten et al. reported the extruded pellets of MIL-53 and MIL-53-NH<sub>2</sub> employing methyl cellulose (MC) as an adhesive [78]. As revealed, the maximum mechanical stability was reached at 5% binder content, whereas the addition of MC did not change the pore breathing behavior during CO<sub>2</sub> uptake, showcasing the potential that shaped MOFs have for use in technical applications. Regufe et al. [79] reported on the fabrication and carbon dioxide  $(CO_2)$ , carbon monoxide (CO), nitrogen  $(N_2)$ , methane (CH<sub>4</sub>), and hydrogen  $(H_2)$  adsorption properties of MOF granulates, made with amino-functionalized titanium terephthalate MIL-125(Ti)\_NH<sub>2</sub> for syngas treatment applications aiming for hydrogen production. The powder was firstly finely ground, then mixed with a polyvinyl group binder (3 wt%) and finally shaped with a homemade fan-type granulator through a wet granulation process.

In [80], three M-gallate (M = Mg, Co, Ni) materials were pelletized (95.2% content of MOF) employing hydroxypropyl cellulose (HPC) as a binding agent. The HPC enhanced

the mechanical stability of the shaped pellets, which displayed a high regenerative ability. Experiments on adsorption showed a good separation performance for both  $C_2H_4/C_2H_6$ and  $C_2H_2/C_2H_4$  mixtures, whereby the  $C_2$  hydrocarbon uptake capacity of the pellets is not easily influenced after molding. HPC was also used as adhesive in the wet granulation of ZIF-8 with a compact high-shear mixer in [81]; when the binder content was increased, the adsorption capacity of the ZIF-8 granules fell marginally. The gate adsorption behavior of ZIF-8, on the other hand, remained nearly constant following the granulation procedure. In [82], MIP-202 was mixed with HPC and water and then the viscous substance was packed into a 2.5 mL syringe without a needle and squeezed into strips, which were then dried and cut into pellets. The shaped pellets presented great cyclic stability, easy regeneration, moderate water and moisture stability, and high  $CO_2/N_2$  and  $CO_2/CH_4$ selectivity. As a result, MIP-202 pellets are regarded as a promising porous material for real-life applications of CO<sub>2</sub> capture. Wickenheisser et al. [83], studying MIL-100(Fe,Cr) and MIL-101(Cr) for water adsorption applications, produced MIL/xerogel composite monoliths by employing a polymerized resorcinol-formaldehyde xerogel as the binder and demonstrated the water uptake these monoliths can achieve. The results showed that the monoliths have good stability and adsorption, which make them good candidates for heat transformation applications. As indicated, the blocking of pores from the binder could largely be avoided by the pre-polymerization of the native xerogel solution before mixing it with the powder. Bazer-Bachi et al. [84] investigated the effect of the fabrication process on the characteristics and stability of the catalytic activity of three types of MOF, i.e., ZIF-8, HKUST-1, and SIM-1, shaped by compression values from 0.3 to 5 kN. The outcomes showed that the higher the pressurization, the higher the mechanical strength, but the lower the porosity of the developed pellet. In Table 1, MOF macrostructures that utilize organic binders are summarized.

	Table	1.	Summary	<sup>,</sup> of sha	ped l	MOFs	with	organic	binders.
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MOF	Binder (wt%)	Shape	S <sub>BET</sub> Powder (m <sup>2</sup> g <sup>-1</sup> )	$\begin{array}{c} S_{BET} \ Body \\ (m^2 \ g^{-1}) \end{array}$	Application	Reference
TIFSIX-2-Cu-i	PVB (10%)	Pellet	740	719	Gas separation and storage	[27]
SIFSIX-3-Ni	PVB (10%)	Pellet	360	297	Gas separation and storage	[27]
GEFSIX-2-Cu-i	PVB (10%)	Pellet	755	659	Gas separation and storage	[27]
SIFSIX-2-Cu-i	PVB (9%)	Pellet	808	685	Gas separation and storage	[27]
ZIF-8	PEI (14%)	Pellet	-	-	Gas adsorption and separation	[29]
ZIF-8	PVC (23%)	Pellet	-	-	Gas adsorption and separation	[29]
ZIF-8	PVF (20%)	Pellet	-	-	Gas adsorption and separation	[29]
UiO66-COOH	PVA (4%)	Bead	710	359	NH <sub>3</sub> air purification	[31]
UiO66-COOH	Polysiloxane (5.5%)	Extrudate	710	418	NH <sub>3</sub> air purification	[31]
MOF-177	PVB (4%)	Pellet	2784	-	CO <sub>2</sub> adsorption	[54]
MOF-177-TEPA-20%	PVB (4%)	Pellet	585	-	$CO_2$ adsorption	[54]
MOF-801	PVB (5%)	Pellet	899	569	$CO_2$ and $H_2O$ adsorption	[55]
Zr-MOF	Sucrose (10%)	Pellet	1367	674	H <sub>2</sub> storage	[56]
UiO-66(Zr)	PVA/PVB (3%)	Granule	1065	1017	Gas adsorption	[57]
UiO-66(Zr)_NH2	PVA/PVB (3%)	Granule	958	795	Gas adsorption	[57]
MIL-100(Fe)	PVA/PVB (3%)	Granule	2261	2043	Gas adsorption	[57]
MIL-127(Fe)	PVA/PVB (3%)	Granule	1181	1117	Gas adsorption	[57]
CPO-27(Ni)	PVA (2%)	Granule	937	1319	NH <sub>3</sub> adsorption for Respiratory protection filters	[58]
MIL-100(Fe)	PVA (2%)	Granule	1212	1172	NH <sub>3</sub> adsorption for Respiratory protection filters	[58]
Cu-BTC	PVA (2%)	Granule	1605	147	NH <sub>3</sub> adsorption for Respiratory protection filters	[58]
ZIF-8	PVF (15%)	Bead	-	-	Gas adsorption and separation	[59]
ZIF-8	PES (25%)	Bead	1384.4	1030.6	Oil sorption	[60]
Alfum	PVA (20%)	Monolith	946	612	Water vapor sorption	[61]
MIL-160(Al)	PVA (20%)	Monolith	1134	800	Water vapor sorption	[61]
MIL-101(Cr)	PVA (20%)	Monolith	3171	2225	Water vapor sorption	[61]
MIL-53(Al)	PVA (13%)	Pellet	-	-	Separation of CO <sub>2</sub> /CH <sub>4</sub> mixtures	[63]
UiO-66	PVA (1%)	Monolith	-	-	MOF shape engineering	[64]

MOFBinder (wt%)ShapeSurp PowderSurp PowderSurp PowderApplicationReferenceCus(BTC):PVA (-)Pellet1727963HgO vapor and CO; activity (							
$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	MOF	Binder (wt%)	Shape	$S_{BET}$ Powder (m <sup>2</sup> g <sup>-1</sup> )	$\begin{array}{c} S_{BET} \ Body \\ (m^2 \ g^{-1}) \end{array}$	Application	Reference
$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	Cu <sub>3</sub> (BTC) <sub>2</sub>	PVA (-)	Pellet	1737	963	$H_2O$ vapor and $CO_2$	[62]
UTSA-16         PVA (-)         Cylindrical extradate         -         80         Case absorption SMR off gases           Altum         PVA (20%)         Monolith         1008         766         Water vapor sorption         [67]           MIL-101(Cr)         PVA (20%)         Monolith         2731         1820         Water vapor sorption         [67]           MIL-101(Cr)         PVA (20%)         Grain         2970         2610         adsorbert in Methanol adsorbert in CO <sub>2</sub> /H <sub>2</sub> ZIF-8         PVA (2.9%)         Cylindrical extradate         -         -         Separation/Nohydrogen         [70]           HKUST-1         PVA (2.9%)         Cylindrical extradate         -         -         Separation/Nohydrogen         [71]           UIO-66         PVA (2.9%)         Cylindrical extradate         -         -         Separation/Nohydrogen         [71]           UIO-66         PVA (25%)         Pellet         1225         1031         Water adsorption hat         [71]           MIL-160         PVA (25%)         Pellet         1122         866         transformation systems         [71]           MIL-96(A1)         PVA (25%)         Pellet         1122         866         transformation systems         [71]	UTSA-16	PVA (0-6.7%)	Pellet	-	-	$CO_2$ adsorption	[65]
UTSA-16         PVA (-)         estructate         -         805         pressure/H <sub>2</sub> purfaction from         [66]           Alfum         PVA (20%)         Monolith         1038         786         Water vapor sorption         [67]           ULO66         PVA (2)%)         Monolith         1038         786         Water vapor sorption         [67]           ULO66         PVA (2)%)         Feltet         1378         1274         CO <sub>2</sub> /N <sub>2</sub> partation         [67]           MIL-101(Cr)         PVA (2)%)         Grain         2970         2610         adsorption trains         [67]           ZIF-8         PVA (2)%)         Cylindrical         -         -         Separation/Molydrogen         [70]           UTSA-16         PVA (2)%)         Cylindrical         -         -         Separation/Molydrogen         [70]           UTSA-16         PVA (2)%)         Cylindrical         -         -         Separation/Molydrogen         [71]           USO-66         PVA (2%)         Pellet         1295         1031         twater adsorption heat         [71]           MIL-160         PVA (2%)         Pellet         1295         1031         twater adsorption heat         [71]           MIL-160         PVA (			Cylindrical			Gas adsorption (high	
$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	UTSA-16	PVA (-)	extrudate	-	805	pressure)/H <sub>2</sub> purification from SMR off-gases	[66]
$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	Alfum	PVA (20%)	Monolith	1038	786	Water vapor sorption	[67]
UIO-66PVA ()Pellet13781274CO <sub>2</sub> /N <sub>2</sub> sparation[68]MIL-101(Cr)PVA (10%)Grain29702610adsorption heat transformation[69]ZIF-8PVA (2.9%)CylindricalSeparation/biolydrogen[70]HKUST-1PVA (2.9%)CylindricalSeparation/biolydrogen[70]UTSA-16PVA (2.9%)CylindricalSeparation/biolydrogen[70]UTSA-16PVA (2.9%)CylindricalSeparation/biolydrogen[71]UTSA-16PVA (2.9%)Pellet12951031Water adsorption heat[71]Zr-fumPVA (2.5%)Pellet643479Water adsorption heat[71]Al-famPVA (2.5%)Pellet1122866Water adsorption heat[71]MIL-160PVA (2.5%)Pellet1122866Water adsorption heat[71]MIL-160PVA (0.5%)Monolith65591batteries/MOT 30-printed Hz[73]MIL-100(Fe)PVP (2%)Monolith19171673.7atmospheria[74]MIL-100(Fe)PVP (2%)Monolith19171673.7atmospheria[74]MIL-100(Fe)PVDFBeadC02 candriften Hz[75]MIL-100(Fe)PVDFBeadC02 candriften Hz[76]MIL-100(Fe)PVDFBeadC02 candriften Hz[76]MIL-100(Fe)PVP (2%)<	MIL-101(Cr)	PVA (20%)	Monolith	2731	1820	Water vapor sorption	[67]
$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	UiO-66	PVA (-)	Pellet	1378	1274	$CO_2/N_2$ separation	[68]
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	MII - 101(Cr)	PVA(10%)	Crain	2970	2610	Methanol adsorbent in	[60]
ZIF-8PVA (2.9%)Cylindrical extrudateColor Separation/biolydrogen $(C)/H_3$ HKUST-1PVA (2.9%)Cylindrical extrudateSeparation/biolydrogen $(C)/H_3$ [70] purificationUTSA-16PVA (2.9%)Cylindrical extrudateSeparation/biolydrogen $(C)/H_3$ [70] purificationUTSA-16PVA (2.9%)Cylindrical extrudateSeparation/biolydrogen (CO/H_3)[71] transformation systemsUTSA-16PVA (2.5%)Pellet12951031transformation systems[71] transformation systemsZr-fumPVA (2.5%)Pellet988595transformation systems[71]MIL-160PVA (2.5%)Pellet1122866transformation systems[71]MIL-60PVA (2.5%)Pellet1122866transformation systems[71]MIL-160PVA (2.5%)Pellet1122866transformation systems[71]MIL-160PVA (2.5%)Monolith65591batteries/MOF shape[72]MIL-160PVA (2.5%)Monolith19171673.7atmospheric water harvesting[73]MIL-100(Fe)PVP (25%)Monolith19171673.7atmospheric water harvesting[75]MIL-101(Cr)(5.5%) and starchGranule24711642Gas (Cog, CH4, N, CO)[76]MIL-101(Cr)(5.5%) and starchGranule24711642Gas (Cog, CH4, N, CO)[77] <td< td=""><td>WILL-IUI(CI)</td><td>1 VA (1078)</td><td>Giain</td><td>2970</td><td>2010</td><td>cvcles</td><td>[09]</td></td<>	WILL-IUI(CI)	1 VA (1078)	Giain	2970	2010	cvcles	[09]
ZIF-8PVA (2.9%)Cylindrical extrudateSeparation/biolydrogen ( $C_0$ , $H_2$ ( $C_0$ , $H_2$ )HKUST-1PVA (2.9%)Cylindrical extrudateSeparation/biolydrogen purfication $C_0$ , $H_2$ UTSA-16PVA (2.9%)Cylindrical extrudateSeparation/biolydrogen purfication[70]UTSA-16PVA (2.9%)Cylindrical extrudateSeparation/biolydrogen purfication[71]UiO-66PVA (2.5%)Pellet12951031Water adsorption heat transformation systems[71]Al-fumPVA (25%)Pellet1122866Water adsorption heat uransformation systems[71]MIL-160PVA (25%)Pellet1122866Water adsorption heat uransformation systems[71]MIL-60(Al)PVA (0.5%)Monolith65591batteries/MOF shape engineering engineering[72]MIL-100(Fe)PVP (10/20/31%)PelletGas storage and separation (AWI) system[74]MIL-100(Fe)PVP (2%)Monolith19171673.7armospheric wate harvesting environments[75]MIL-101(Cr)(5.5%) and starch (5.5%) and starchGranule24711642Gas (CO <sub>2</sub> , CH <sub>4</sub> , N <sub>2</sub> , CO) sorption[77]MIL-101(Cr)(5.5%) and starch (5.5%) and starchGranule24711642Gas (CO <sub>2</sub> , CH <sub>4</sub> , N <sub>2</sub> , CO) sorption[77]MIL-101(Cr)(5.5%) and starch (5.5%) and starchGranule-			Culindrical			$\dot{CO_2}/H_2$	
purificationHKUST-1PVA (2.9%)Cylindrical extrudateSeparation / biolydrogen CQ//H; CylindricationUTSA-16PVA (2.9%)Cylindrical extrudateSeparation / biolydrogen Q//H;UTSA-16PVA (2.9%)Cylindrical extrudateSeparation / biolydrogen Q//H;UTSA-16PVA (2.5%)Pellet12951031Water adsorption heat Water adsorption heat[71] transformation systemsZr-fumPVA (25%)Pellet988595Water adsorption heat[71] transformation systemsMIL-160PVA (25%)Pellet1122866Water adsorption heat Upcycling of Lion engineering[71]MIL-96(Al)PVA (0.5%)Monolith65591bitries/MOF shape[72] upcycling of Lion engineeringMIL-96(Al)PVA (0.5%)Monolith19171673.7atmospheric water harvesting[73] engineeringMIL-100(Fe)PVP (10/20/31%)PelletGas storage and separation[74] Ultra-low heat-drivenMIL-100(Fe)PVDF (30/40/50%)BeadCO2 capture in indoor sorption[76] environmentsMIL-101(Cr)(5.5%) and starch (GSM)Granule24/711642Gas (CO2, CH4, N2, CO) sorption[77] sorptionMIL-101(Cr)(5.5%) and starch (GSM)GranuleSyngas treatment atiming for H2 sorption[79] production separationsMIL-125(D)_NH2 <td>ZIF-8</td> <td>PVA (2.9%)</td> <td>extrudate</td> <td>-</td> <td>-</td> <td>Separation/biohydrogen</td> <td>[70]</td>	ZIF-8	PVA (2.9%)	extrudate	-	-	Separation/biohydrogen	[70]
HKUST-1PVA (2.9%)Cylindrical extrudateCU <sub>7</sub> /R2 purification(70) purificationUTSA-16PVA (2.9%)Cylindrical extrudateSeparation/biolydrogen purification(70) purificationUiO-66PVA (25%)Pellet12951031Water adsorption heat transformation systems(71)Zr-fumPVA (25%)Pellet643479Water adsorption heat transformation systems(71)Al-fumPVA (25%)Pellet988595Water adsorption heat transformation systems(71)MIL-160PVA (25%)Pellet1122866Water adsorption heat transformation systems(72)MIL-60(AI)PVA (0.5%)Monolith65591batteries/MOT shape torge engineering(72)MIL-96(AI)PVA (0.5%)Monolith65591batteries/MOT shape(72)MIL-100(Fe)PVP (10/20/31%)PelletGas storage and separation(74)MIL-101(Cr)(5.5%) and starch (5.5%) and starch CCC sodium saltGranule24711642Gas (CO <sub>2</sub> , CH <sub>4</sub> , N <sub>2</sub> , CO) sorption(77)MIL-101(Cr)(5.5%) and starch (5.5%)Cylindrical extrudate15251158CO <sub>2</sub> and CH <sub>4</sub> adsorption(78)MIL-101(Cr)(5.5%) and starch (GMM)GranuleSyngas transmat atiming for H2 production(79)MIL-101(Cr)(5.5%)Pellet638557Hydrocarbon separations(80)<			extructure			purification	
InterventInterventextrudateInterventIntervent[7]UTSA-16PVA (2.9%)Cylindrical extrudateSeparation floshydrogen[70]UIO-66PVA (25%)Pellet12951031Water adsorption heat[71]Zr-fumPVA (25%)Pellet643479Water adsorption heat[71]Al-fumPVA (25%)Pellet988595Water adsorption heat[71]MIL-160PVA (25%)Pellet1122866Water adsorption heat[71]MIL-60PVA (25%)Pellet1122866Water adsorption heat[71]MIL-60PVA (0.5%)Monolith65591batteries/MOF shape[72]MIL-60PVA (0.5%)Monolith65591batteries/MOF shape[73]MIL-100(Fe)PVP (10/2013%)PelletGas storage ad separation[74]MIL-100(Fe)PVP (2%)Monolith19171673.7atmospheric water harvesting[75]MIL-101(Cr)(5.5%)Granule24711642Gas (CO2, CH4, N2, CO)[77]MIL-101(Cr)(5.5%)Granule24711642Gas (CO2, CH4, adsorption[78]MIL-101(Cr)(5.5%)GranuleSyngas treatment atiming for H2 production[79]MIL-101(Cr)(5.5%)GranuleSyngas treatment atiming for H2 production[79]MIL-101(Cr)(5.5%)Pellet434430 <td>HKUST-1</td> <td>PVA (2.9%)</td> <td>Cylindrical</td> <td>-</td> <td>_</td> <td><math>CO_2/H_2</math> Separation / biohydrogen</td> <td>[70]</td>	HKUST-1	PVA (2.9%)	Cylindrical	-	_	$CO_2/H_2$ Separation / biohydrogen	[70]
$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	11001-1	1 VA (2.570)	extrudate			purification	[70]
UTSA-16PVA (2.9%)Cyminital extrudateSeparation/biohydrogen[70] purificationUiO-66PVA (25%)Pellet12951031Water adsorption heat transformation systems[71] transformation systemsZr-fumPVA (25%)Pellet643479Water adsorption heat 			Culindrical			$CO_2/H_2$	
UiO-66PVA (25%)Pellet12951031Water adsorption heat transformation systems[71]Zr-fumPVA (25%)Pellet643479Water adsorption heat transformation systems[71]Al-fumPVA (25%)Pellet988595transformation systems[71]MIL-160PVA (25%)Pellet1122866transformation systems[71]MIL-96(Al)PVA (0.5%)Monolith65591batteries/MOF shape[72]MIL-96(Al)PVA (0.5%)Monolith65591batteries/MOF shape[73]MOF-5ABS (1/5/10%)variousGas storage adseparation[74]MIL-101(Fe)PVP (10/20/31%)PelletGas storage adseparation[76]MIL-100(Fe)PVP (2%)Monolith19171673.7atmospheric water harvesting[76]CMC sodium salt GMC sodium saltGranule24711642Gas (CO <sub>2</sub> , CH <sub>4</sub> , N <sub>2</sub> , CO)[77]MIL-101(Cr)(5.5%) and starch (5.5%)Granule24711642Gas (CO <sub>2</sub> , CH <sub>4</sub> , N <sub>2</sub> , CO)[77]MIL-125(Th)_NH2 Come solutionPolyvinyl group (CASM)GranuleSyngas treatment aiming for H2 production[79]MIL-125(Th)_NH2 CospilatePellet494480Hydrocarbon separations[80]MIL-126(Th)_DH2 CospilatePellet638557Hydrocarbon separations[80]MIL-126(Th)_NH2 CospilatePellet494	UTSA-16	PVA (2.9%)	extrudate	-	-	Separation/biohydrogen	[70]
$ \begin{array}{c ccccc} UiO-66 & PVA (25\%) & Pellet & 1295 & 1031 & Urater absorption (71) \\ transformation systems (72) \\ transformation systems (73) \\ transformation systems (74) \\ transformation systems (74) \\ transformation systems (76) \\ transformation system (76) \\ transformatio$						purification Water adcomption heat	
$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	UiO-66	PVA (25%)	Pellet	1295	1031	transformation systems	[71]
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	Zu hum		Dallat	642	470	Water adsorption heat	[771]
Al-fumPVA (25%)Pellet988595Water adsorption heat transformation systems[71]MIL-160PVA (25%)Pellet1122866Water adsorption heat transformation systems[71]MIL-96(Al)PVA (0.5%)Monolith65591batteries/MOF shape engineering[72]MIL-96(Al)PVA (0.5%)Monolith65591batteries/MOF shape engineering[73]MOF-5ABS (1/5/10%)3D-printed 	Zr-rum	PVA (25%)	Pellet	643	479	transformation systems	[/1]
$ \begin{array}{c cccc} \mbox{MIL-160} & PVA (25\%) & Pellet & 1122 & 866 & Water adsorption heat & [71] \\ \mbox{MIL-96(Al)} & PVA (0.5\%) & Monolith & 655 & 91 & batteries/MOF shape & [72] \\ \mbox{model} & aBS (1/5/10\%) & Monolith & 655 & 91 & batteries/MOF shape & [72] \\ \mbox{model} & aBS (1/5/10\%) & Pollet & - & - & H_2 adsorption (3D-printed H_2 storage devices & storage and separation (74) \\ \mbox{MIL-100(Fe)} & PVP (10/20/31\%) & Pellet & - & - & Gas storage and separation (74) \\ \mbox{MIL-100(Fe)} & PVP (2\%) & Monolith & 1917 & 1673.7 & atmospheric water harvesting (75) \\ \mbox{equation model} & (3/40/50\%) & Bead & - & - & CO_2 capture in indoor \\ \mbox{(3/40/50\%)} & Bead & - & - & CO_2 capture in indoor \\ \mbox{(3/40/50\%)} & Granule & 2471 & 1642 & Gas (CO_2, CH_4, N_2, CO) \\ \mbox{sorption} & Cylindrical \\ \mbox{extrudate} & 1525 & 1158 & CO_2 and CH_4 adsorption [78] \\ \mbox{MIL-53(Al)} & MC 4000 (10\%) & Cylindrical \\ \mbox{extrudate} & 1525 & 1200 & CO_2 and CH_4 adsorption [78] \\ \mbox{MIL-125(Th)_NH_2} & Oplicity opp \\ \mbox{(3/8)} & Pellet & 638 & 557 & Hydrocarbon separations [80] \\ \mbox{MIL-125(Th)_NH_2} & Polyving group \\ \mbox{(3/8)} & Pellet & 435 & 425 & Hydrocarbon separations [80] \\ \mbox{MIL-126(Th)} & HPC (4.5\%) & Pellet & 435 & 425 & Hydrocarbon separations [80] \\ \mbox{Nigallate} & HPC (4.5\%) & Pellet & 455 & 425 & Hydrocarbon separations [80] \\ \mbox{Nigallate} & HPC (4.5\%) & Pellet & 455 & 425 & Hydrocarbon separations [80] \\ \mbox{Nigallate} & HPC (4.5\%) & Pellet & 455 & 425 & Hydrocarbon separations [80] \\ \mbox{Nigallate} & HPC (4.5\%) & Pellet & 278.6 & - & & & & & & & & & & & & & & & & & $	Al-fum	PVA (25%)	Pellet	988	595	Water adsorption heat	[71]
MIL-160PVA (25%)Pellet1122866Intra Rotionation function[71] transformation systems[71]MIL-96(Al)PVA (0.5%)Monolith65591batteries/MOF shape[72] engineeringMOF-5ABS (1/5/10%)3D-printed various geometriesH2 adsorption/3D-printed H2 storage devices[73]ELM-11PVP (10/20/31%)PelletGas storage and separation[74] Ultra-low heat-drivenMIL-100(Fe)PVP (2%)Monolith19171673.7atmospheric water harvesting[75] (AWH) systemepn-MOFPVDF (30/40/50%)BeadCO2 capture in indoor environments[76] environmentsMIL-101(Cr)(5.5%) and starch (5.5%)Granule24711642Gas (CO2, CH4, N2, CO) sorption[77]MIL-53(Al)MC 4000 (10%)Cylindrical extrudate15251158CO2 and CH4 adsorption[78]MIL-125(Ti)_NH2Polyvinyl group (3%)GranuleSyngas treatment aiming for H2 production[79]Mg-gallateHPC (4.8%)Pellet435425Hydrocarbon separations[80]Ni-gallateHPC (4.8%)Pellet455425Hydrocarbon separations[80] R1MIL-101(Cr)R,F-xerogel (42%)Monolith30601350Water adsorption[81] R1MIL-102(Cr)R,F-xerogel (42%)Pellet455425Hydrocarbon separations[80] R1MIL-102(C		× ,				Water adsorption heat	
$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	MIL-160	PVA (25%)	Pellet	1122	866	transformation systems	[71]
$\begin{array}{c c c c c c c c c c c c c c c c c c c $						Upcycling of Li-ion	
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	MIL-96(Al)	PVA (0.5%)	Monolith	655	91	batteries/MOF shape	[72]
$\begin{array}{c c c c c c c c c c c c c c c c c c c $			3D printed			engineering	
Heregeometries geometriesstorage devices $[1^{24}]$ ELM-11PVP (10/20/31%)PelletGas storage and separation (MH-100(Fe) $[74]$ MIL-100(Fe)PVP (2%)Monolith19171673.7atmospheric water harvesting (AWH) system $[75]$ epn-MOFPVDF (30/40/50%) CMC sodium saltBeadCO <sub>2</sub> capture in indoor environments $[76]$ MIL-101(Cr)(55%) and starch (55%)Granule24711642Gas (CO <sub>2</sub> , CH <sub>4</sub> , N <sub>2</sub> , CO) sorption $[77]$ MIL-53(Al)MC 4000 (10%)Cylindrical extrudate15251158CO <sub>2</sub> and CH <sub>4</sub> adsorption $[78]$ MIL-53(Al)MC 4000 (10%)Cylindrical extrudate15251200CO <sub>2</sub> and CH <sub>4</sub> adsorption $[78]$ MIL-125(Ti)_NH2Polyvinyl group (3%)GranuleSyngas treatment aiming for H <sub>2</sub> production $[79]$ Mg-gallate L HPC (4.8%)Pellet638557Hydrocarbon separations[80]Ni-gallate L HPC (4.8%)Pellet455425Hydrocarbon separations[80]Ni-gallate L HPC (5%)Pellet278.6-separation/CO <sub>2</sub> capture geometring[81]MIL-101(Cr). R,F-xerogel (50%)Monolith30601350Water adsorption[83]MIL-100(Fe) R,F-xerogel (42%)Monolith1560570Water adsorption[83]MIL-100(Cr) R,F-xerogel (44%)Monolith1560570Water adsorption[83] <td>MOF-5</td> <td>ABS (1/5/10%)</td> <td>various</td> <td>-</td> <td>-</td> <td><math>H_2</math> adsorption/3D-printed <math>H_2</math></td> <td>[73]</td>	MOF-5	ABS (1/5/10%)	various	-	-	$H_2$ adsorption/3D-printed $H_2$	[73]
ELM-11PVP (10/20/31%)PelletGas storage and separation[74] Ultra-low heat-drivenMIL-100(Fe)PVP (2%)Monolith19171673.7atmospheric water harvesting (AWH) system[75] (AWH) systemepn-MOFPVDF (30/40/50%) CMC sodium saltBeadCO2 capture in indoor environments[76]MIL-101(Cr)(5.5%)Granule24711642Gas (CO2, CH4, N2, CO) sorption[77]MIL-53(Al)MC 400 (10%)Cylindrical extrudate15251158CO2 and CH4 adsorption[78]MIL-53(Al)MC 4000 (10%)Cylindrical extrudate15251200CO2 and CH4 adsorption[78]MIL-125(Ti)_NH2Polyvinyl group (3%)GranuleSyngas treatment aiming for H2 production[79]Mg-gallateHPC (4.8%)Pellet638557Hydrocarbon separations[80]Ni-gallateHPC (4.8%)Pellet455425Hydrocarbon separations[80]ZIF-8HPC (0-40%)GranuleMOF shape engineering[81]MIL-100(Fc)R,F-xerogel (50%)Monolith30601350Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83] <td></td> <td></td> <td>geometries</td> <td></td> <td></td> <td>storage devices</td> <td>[]</td>			geometries			storage devices	[]
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$\begin{array}{c c c c c c c c c c c c c c c c c c c $	MIL $100(E_0)$	$\mathbf{DVD}(2^{0/})$	Monalith	1017	1672 7	Ultra-low heat-driven	[75]
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	WIIL-100(1°C)	1 VI (270)	Wononun	1917	1075.7	(AWH) system	[75]
epiPMOP(30/40/50%) (30/40/50%)DeadIIenvironments[76]MIL-101(Cr)(3.5%)Granule24711642 $Gas (CO_2, CH_4, N_2, CO)$ sorption[77]MIL-53(Al)MC 400 (10%)Cylindrical extrudate15251158CO2 and CH4 adsorption[78]MIL-53(Al)MC 4000 (10%)Cylindrical extrudate15251200CO2 and CH4 adsorption[78]MIL-125(Ti)_NH2Polyvinyl group (3%)GranuleSyngas treatment aiming for H2 production[79]Mg-gallateHPC (4.8%)Pellet638557Hydrocarbon separations[80]Ni-gallateHPC (4.8%)Pellet455425Hydrocarbon separations[80]Ni-gallateHPC (0-40%)GranuleMOF shape engineering[81]MIP-202HPC (5%)Pellet278.6-CO2/CH4 and CO2/N2 separation/CO2 capture[82]MIL-100(Cr)R,F-xerogel (50%)Monolith30601350Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1	opp MOE	PVDF	Boad			$CO_2$ capture in indoor	[76]
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	epii-wor	(30/40/50%)	Deau	-	-	environments	[70]
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	MIL $101(C_r)$	CMC sodium salt $(5.5\%)$ and starsh	Cranula	2471	1642	Gas (CO <sub>2</sub> , CH <sub>4</sub> , N <sub>2</sub> , CO)	[77]
MIL-53(Al)MC 400 (10%)Cylindrical extrudate15251158CO2 and CH4 adsorption[78]MIL-53(Al)MC 4000 (10%)Cylindrical extrudate15251200CO2 and CH4 adsorption[78]MIL-125(Ti)_NH2Polyvinyl group (3%)GranuleSyngas treatment aiming for H2 production[79]Mg-gallateHPC (4.8%)Pellet638557Hydrocarbon separations[80]Co-gallateHPC (4.8%)Pellet494480Hydrocarbon separations[80]Ni-gallateHPC (4.8%)Pellet455425Hydrocarbon separations[80]ZIF-8HPC (0-40%)GranuleMOF shape engineering[81]MIL-101(Cr).R,F-xerogel (50%)Monolith30601350Water adsorption[83]MIL-100(Fe)R,F-xerogel (42%)Monolith1560570Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]ZIF-8Cellulose ester (-)Tablet14331420Catalysis/MOF shape engineering[84]HKUST-1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]	MIL-101(Cr)	(5.5%) and starch $(5.5%)$	Granule	2471	1642	sorption	[//]
MIL-33(AI)MC 400 (10%)extrudate15251138CO2 and CH4 adsorption[78]MIL-53(AI)MC 4000 (10%)Cylindrical extrudate15251200CO2 and CH4 adsorption[78]MIL-125(Ti)_NH2Polyvinyl group (3%)GranuleSyngas treatment aiming for H2 production[79]Mg-gallateHPC (4.8%)Pellet638557Hydrocarbon separations[80]Co-gallateHPC (4.8%)Pellet494480Hydrocarbon separations[80]Ni-gallateHPC (0-40%)GranuleMOF shape engineering[81]MIP-202HPC (5%)Pellet278.6-CO2/CH4 and CO2/N2 separation/CO2 capture[82]MIL-101(Cr).R,F-xerogel (50%)Monolith30601350Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[84] engineeringHKUST-1Cellulose ester (-)Tablet14331420Catalysis/MOF shape engineering[84] engineeringHKUST-1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84] engineeringHKUST-1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84] engineering		(0.070)	Cylindrical	1505	1150		[70]
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	MIL-35(AI)	IVIC 400 (10%)	extrudate	1525	1156	$CO_2$ and $CH_4$ adsorption	[70]
MIL-125(Ti)_NH2Polyvinyl group (3%)GranuleSyngas treatment aiming for H2 production[79]Mg-gallateHPC (4.8%)Pellet638557Hydrocarbon separations[80]Co-gallateHPC (4.8%)Pellet494480Hydrocarbon separations[80]Ni-gallateHPC (0-40%)GranuleMOF shape engineering[81]ZIF-8HPC (0-40%)GranuleMOF shape engineering[81]MIP-202HPC (5%)Pellet278.6-CO2/CH4 and CO2/N2 separation/CO2 capture[82]MIL-101(Cr).R,F-xerogel (50%)Monolith30601350Water adsorption[83]MIL-100(Fe)R,F-xerogel (42%)Monolith2200770Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]ZIF-8Cellulose ester (-)Tablet14331420Catalysis/MOF shape engineering[84]HKUST-1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]GM 1Catalysis/MOF shape[84]EM 1Catalysis/MOF shape[84]	MIL-53(Al)	MC 4000 (10%)	Cylindrical	1525	1200	CO <sub>2</sub> and CH <sub>4</sub> adsorption	[78]
MIL-125(Ti)_NH2ColumbraGranuleOptionproduction[79]Mg-gallateHPC (4.8%)Pellet638557Hydrocarbon separations[80]Co-gallateHPC (4.8%)Pellet494480Hydrocarbon separations[80]Ni-gallateHPC (4.8%)Pellet455425Hydrocarbon separations[80]ZIF-8HPC (0-40%)GranuleMOF shape engineering[81]MIP-202HPC (5%)Pellet278.6- $CO_2/CH_4$ and $CO_2/N_2$ separation/CO2 capture[82]MIL-101(Cr).R,F-xerogel (50%)Monolith30601350Water adsorption[83]MIL-100(Fe)R,F-xerogel (42%)Monolith2200770Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]ZIF-8Cellulose ester (-)Tablet14331420catalysis/MOF shape engineering[84]HKUST-1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]GM 1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]	/	Polyvinyl group	extrudate			Syngas treatment aiming for H <sub>2</sub>	
Mg-gallateHPC (4.8%)Pellet638557Hydrocarbon separations[80]Co-gallateHPC (4.8%)Pellet494480Hydrocarbon separations[80]Ni-gallateHPC (4.8%)Pellet455425Hydrocarbon separations[80]ZIF-8HPC (0-40%)GranuleMOF shape engineering[81]MIP-202HPC (5%)Pellet278.6- $CO_2/CH_4$ and $CO_2/N_2$ separation/CO2 capture[82]MIL-101(Cr).R,F-xerogel (50%)Monolith30601350Water adsorption[83]MIL-100(Fe)R,F-xerogel (42%)Monolith2200770Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]ZIF-8Cellulose ester (-)Tablet14331420Catalysis/MOF shape engineering[84]HKUST-1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]HKUST-1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]	MIL-125(Ti)_NH <sub>2</sub>	(3%)	Granule	-	-	production	[79]
Co-gallateHPC (4.8%)Pellet494480Hydrocarbon separations[80]Ni-gallateHPC (4.8%)Pellet455425Hydrocarbon separations[80]ZIF-8HPC (0-40%)GranuleMOF shape engineering[81]MIP-202HPC (5%)Pellet278.6- $CO_2/CH_4$ and $CO_2/N_2$ separation/CO2 capture[82]MIL-101(Cr).R,F-xerogel (50%)Monolith30601350Water adsorption[83]MIL-100(Fe)R,F-xerogel (42%)Monolith2200770Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]ZIF-8Cellulose ester (-)Tablet14331420catalysis/MOF shape engineering[84]HKUST-1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]CM1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]	Mg-gallate	HPC (4.8%)	Pellet	638	557	Hydrocarbon separations	[80]
NI-gallateHPC (4.8%)Pellet455425Hydrocarbon separations[80]ZIF-8HPC (0-40%)GranuleMOF shape engineering[81]MIP-202HPC (5%)Pellet278.6- $CO_2/CH_4$ and $CO_2/N_2$ separation/CO2 capture[82]MIL-101(Cr).R,F-xerogel (50%)Monolith30601350Water adsorption[83]MIL-100(Fe)R,F-xerogel (42%)Monolith2200770Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]ZIF-8Cellulose ester (-)Tablet14331420Catalysis/MOF shape engineering[84]HKUST-1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]CM1Callylice ester (-)Tablet1897453Catalysis/MOF shape engineering[84]	Co-gallate	HPC (4.8%)	Pellet	494	480	Hydrocarbon separations	[80]
ZIF-8HPC (0-40%)GranuleMOF shape engineering[81]MIP-202HPC (5%)Pellet278.6- $CO_2/CH_4$ and $CO_2/N_2$ separation/CO2 capture[82]MIL-101(Cr).R,F-xerogel (50%)Monolith30601350Water adsorption[83]MIL-100(Fe)R,F-xerogel (42%)Monolith2200770Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]ZIF-8Cellulose ester (-)Tablet14331420Catalysis/MOF shape engineering[84]HKUST-1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]GMA1Callyliage ester (-)Tablet570270Catalysis/MOF shape engineering[84]	Ni-gallate	HPC (4.8%)	Pellet	455	425	Hydrocarbon separations	[80]
MIP-202HPC (5%)Pellet278.6-CCO2/CH4 and CO2/N2[82]MIL-101(Cr).R,F-xerogel (50%)Monolith30601350Water adsorption[83]MIL-100(Fe)R,F-xerogel (42%)Monolith2200770Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]ZIF-8Cellulose ester (-)Tablet14331420Catalysis/MOF shape engineering[84]HKUST-1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]CM1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]	ZIF-8	HPC (0-40%)	Granule	-	-	CO <sub>2</sub> /CH <sub>2</sub> and CO <sub>2</sub> /N <sub>2</sub>	[81]
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	MIP-202	HPC (5%)	Pellet	278.6	-	separation/CO <sub>2</sub> capture	[82]
MIL-100(Fe)R,F-xerogel (42%)Monolith2200770Water adsorption[83]MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]ZIF-8Cellulose ester (-)Tablet14331420Catalysis/MOF shape engineering[84]HKUST-1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]CM1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]	MIL-101(Cr).	R,F-xerogel (50%)	Monolith	3060	1350	Water adsorption	[83]
MIL-100(Cr)R,F-xerogel (44%)Monolith1560570Water adsorption[83]ZIF-8Cellulose ester (-)Tablet14331420Catalysis/MOF shape engineering[84]HKUST-1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]CM 1Cellulose ester (-)Tablet1897453Catalysis/MOF shape engineering[84]	MIL-100(Fe)	R,F-xerogel (42%)	Monolith	2200	770	Water adsorption	[83]
ZIF-8       Cellulose ester (-)       Tablet       1433       1420       Catalysis/MOF shape engineering       [84]         HKUST-1       Cellulose ester (-)       Tablet       1897       453       Catalysis/MOF shape engineering       [84]         SIM 1       Callulose ester (-)       Tablet       1897       453       Catalysis/MOF shape engineering       [84]	MIL-100(Cr)	R,F-xerogel (44%)	Monolith	1560	570	Water adsorption	[83]
HKUST-1 Cellulose ester (-) Tablet 1897 453 Catalysis/MOF shape engineering [84] Catalysis/MOF shape [84] Catalysis/MOF shape [84]	ZIF-8	Cellulose ester (-)	Tablet	1433	1420	Catalysis/MOF shape	[84]
HKU51-1     Cellulose ester (-)     Tablet     1897     453     Catalysis/ MOF shape     [84]       CDV 1     Catalysis/MOF shape     F1(     270     Catalysis/MOF shape     [84]					.=-	Catalysis/MOF shape	10.17
CD4.1 Callulare actor () Tablet 51( 270 Catalysis/MOF shape 1941	HKUST-1	Cellulose ester (-)	Tablet	1897	453	engineering	[84]
SIM-1 Cellulose ester (-) Tablet 516 570 engineering	SIM-1	Cellulose ester (-)	Tablet	516	370	Catalysis/MOF shape engineering	[84]

 Table 1. Cont.

#### 3.2. Processes with Inorganic Binders

Inorganic binders are less common than the polymer binders; however, they demonstrate high mechanical stability, which provides rigid forms to the shaped structures. Clays, alumina, and silica are widely used inorganic binders in MOF shaping processes. Clays, such as bentonite clays, come in various colored powder forms, are insoluble in water, and when mixed with water, form a colloidal solution and have high melting points; e.g., for bentonite, it is higher than 1200 °C [85]. Silica (SiO<sub>2</sub>), a white powder also known as silicon dioxide, melts in temperatures higher than 1700 °C, is rather insoluble in water, and is insoluble in ethanol [86]. Alumina (Al<sub>2</sub>O<sub>3</sub>) is a popular inorganic binder, with various crystal forms such as  $\alpha$ -,  $\beta$ -,  $\gamma$ -,  $\delta$ - and  $\rho$ - alumina, which also has the properties of a porous material, with mesoporous alumina exhibiting pores of between 2 and 50 nm [87]. Alumina, also called aluminum oxide, is a white crystalline powder, insoluble in water, with a melting point higher than 2000 °C [88]. Inorganic binders can operate in higher temperatures than their polymer counterparts and this is suitable for those materials that require heat treatments at relatively high temperatures.

Zhu et al. examined gas adsorption in shaped ZIF-8 tablets produced from a single push tablet pressing machine utilizing alumina, bentonite, silica, talc powder, SB powder (high-quality pseudo-boehmite), sesbania powder, and MC as binders [89]. The most suitable adhesive agents were found to be SB powder and talc powder, for which a 10–20% reduction in the uptake capacities (CO<sub>2</sub>, CH<sub>4</sub>, and other hydrocarbons) was observed on the shaped ZIF-8, and it is deemed that the shaped forms are able to satisfy the industrial demand. Moreira et al. synthesized UiO-66 tablets and consequently evaluated them in terms of selective adsorption and separation of xylene isomers [90]. The shaping of the tablets was carried out with the use of a rotary press tabletizer with graphite as the binder. Lefevere et al. 3D printed a ZIF-8 monolith with bentonite (16.7 wt%) as an adhesive agent in order to ensure the mechanical and thermal stability of the monolith and MC (16.7 wt%) to improve the rheology of the extruded paste [91]. As noted, adding bentonite shifts the hysteresis loop of the Ar isotherm on ZIF-8. Activating the monoliths at 450 °C removed MC and allowed for a high adsorption capacity in a reproducible manner with regard to n-butanol. In a study conducted by Tsalaporta and MacElroy [92], MC and bentonite were used as binders diluted in water to form pelletized UiO-66, ZIF-67, ZIF-8, and HKUST-1. ZIF-8 maintained its crystal structure in the presence of binders and water while ZIF 67 irreversibly lost it; for UiO-66 and HKUST-1, ethanol was used to reconstruct their crystallinity. Hong et al. formed MIL-101(Cr) monoliths with bentonite clay as the binding agent via paste extrusion with a powder-to-binder ratio of 75:25 [93]. To further improve the porosity of the monolith, Licowax C was added into the paste. Subsequently, the monolith was tested for its  $CO_2$  adsorption performance and compared with a 13X Zeolite monolith; the findings revealed that the MIL-101(Cr) monolith capacity outperformed that of 13X Zeolite by 37%, whereas its  $CO_2$  uptake capacity was enhanced as the temperature to regenerate the monolith was increased. In [94], bentonite clay (40 wt%) was also used in the single screw extrusion of MIL-101(Cr) paste. The prepared monoliths were mechanically stable, exhibited high CO<sub>2</sub> uptake capacity compared to pristine MIL-101(Cr), and they could be regenerated at 150 °C for repeated adsorption circles, thus making them a good candidate for industrial applications.

Valekar et al. reported on the fabrication of MOF millimeter-scale spheres made with MIL-100(Fe), MIL-101(Cr), UiO-66(Zr), and UiO-66(Zr)\_NH<sub>2</sub> through the wet granulation method [30]. The millimeter-scale pellets were shaped with the use of a hand-made pan-type granulator, by mixing the MOF-powder with mesoporous  $\rho$ -alumina (MRA) as a binder and water as a dispersion medium. They used MRA binder for developing well-shaped MOF structures, which retained their intrinsic properties after shaping, and evaluated CO<sub>2</sub> and N<sub>2</sub> adsorption performance, observing a high affinity for CO<sub>2</sub> over N<sub>2</sub> in all MOF samples tested. In [95], MIL-100(Fe) granules were produced, employing silica sol as an adhesive, to demonstrate MIL-100(Fe) as an adsorbent of high potential for SF<sub>6</sub>/N<sub>2</sub> separation. The physical and chemical properties of a powder-type MIL-

100 did not change significantly following the granulation procedure (Fe), except for a small reduction in pore volume. In another study [96], granules of MIL-127(Fe), MIL-100(Fe), and UiO-66(Zr) were produced utilizing  $\rho$ -alumina as a binder via wet granulation, and their sorption properties were investigated. MIL-127(Fe) depicted a nearly identical uptake behavior after granulation and is noted as a potential candidate for use in gas storage or separation applications. In general, alumina shaping is a promising approach to produce MOFs for applications in gas separation and gas storage; however, this might not apply to all MOF materials. In [97], MIL-101 pellets were shaped with sodium silicate, starch, and water as the adhesive mixture to the MIL-101 powder. The attained paste was extruded by a homemade extruder and then dried. The powder and pellets presented a  $CO_2$ uptake capacity of 9.72 mmol  $g^{-1}$  and 6.34 mmol  $g^{-1}$ , respectively. In [98], MIL-100(Fe) was formed into granules with silica (10 wt%) utilized as a binder and its hydrocarbon separation performance was explored through tests on mixtures of ethane or ethylene with propane. The gases were recovered in high rates (>86%) with great purities (>94%). Kusgens et al. reported on the fabrication of  $Cu_3(BTC)_2$  on monolithic structures through a two-step methodology [99]. The first step included the fabrication of a molding batch, by mixing of Cu<sub>3</sub>(BTC)<sub>2</sub> with Silres MSE 100 (binder) and Culmial MHPC 20,000 P (plasticizer) in a lab-scale kneader. During the second step, a ram extruder was utilized for extruding the molding batch to a monolithic strang. The results showed that the developed monoliths have good mechanical stability and should be considered for gas storage, catalysis, and separation applications. Pereira et al. [100] produced ZIF-8 and MIL-53(Al) pellets by extrusion with alumina as a binder. Various loadings (5, 10, and 15 wt%) of alumina were employed in the composite pellets and this increase resulted in improved mechanical strength, while the shaping process had less of an impact on the ZIF-8 adsorption properties than on the MIL-53(Al). In [101], Thakkar et al. utilized silica (15 wt%) as the binding agent in 3D-printed ZIF-7 monoliths. Silica enlarged the pores of the monolithic ZIF-7 and allowed  $N_2$  molecules to access the pores of the ZIF-7; as a result, the monolith presented a higher surface area than the pristine powder: 40 m<sup>2</sup> g<sup>-1</sup> compared to 16 m<sup>2</sup> g<sup>-1</sup>. The monolith was tested for its ethane/ethylene adsorption capacities and showed a 85%/87% uptake performance for  $C_2H_6/C_2H_4$  compared to the pristine ZIF-8 powder, and broke at 0.8 MPa in compression tests. In another similar work [102], Thakkar et al. 3D-printed MOF-74(Ni) and UTSA-16(Co) structures with bentonite clay (15 and 10 wt%, respectively) as an adhesive and PVA (5 wt%) as a plasticizer, and tested their  $CO_2$  adsorption performance. The results revealed that the monoliths' uptake performance was equal to the 79% and 87% of their pristine powder form, respectively. Bentonite clay (15 wt%) as a binder and PVA (5%) as a plasticizer were also used in a 3D-printing process to develop a MIL-101 monolithic structure [103]. The monolith was tested for  $CO_2$  removal from enclosed environments. The MIL-101 monolith presented a small surface area decrease of 200 m<sup>2</sup> g<sup>-1</sup> and achieved a 75%  $CO_2$  adsorption uptake compared to its powder analogue. In Table 2, a summary of shaped MOFs with inorganic binders is provided.

Table 2. Summary of shaped MOFs with inorganic binders.

MOF	Binder (wt%)	Shape	S <sub>BET</sub> Powder (m <sup>2</sup> g <sup>-1</sup> )	$\begin{array}{c} S_{BET} \text{ Body} \\ (m^2  g^{-1}) \end{array}$	Application	Reference
MIL-100(Fe)	ρ-alumina (5%)	Sphere	2088	1831	Ammonia adsorption	[30]
MIL-101(Cr)	ρ-alumina (5%)	Sphere	4066	3685	$CO_2$ adsorption	[30]
UIO-66(Zr)	ρ-alumina (5%)	Sphere	1050	911	$CO_2$ adsorption	[30]
UIO-66_NH <sub>2</sub>	ρ-alumina (5%)	Sphere	875	823	CO <sub>2</sub> adsorption	[30]
ZIF-8	Bentonite clay (10%)	Tablet	1022.8	820.6	-	[89]
ZIF-8	Alumina (10%)	Tablet	1022.8	947.9	-	[89]
ZIF-8	SB powder (10%)	Tablet	1022.8	959.2	Gas adsorption	[89]
ZIF-8	Talc powder (10%)	Tablet	1022.8	951.3	Gas adsorption	[89]
ZIF-8	Sesbania powder (10%)	Tablet	1022.8	846.4	-	[89]

MOF	Binder (wt%)	Shape	S <sub>BET</sub> Powder (m <sup>2</sup> g <sup>-1</sup> )	S <sub>BET</sub> Body (m <sup>2</sup> g <sup>-1</sup> )	Application	Reference
ZIF-8	Silica (10%)	Tablet	1022.8	945.9	-	[89]
UiO-66	Graphite (1%)	Tablet	1140	885	Selective adsorption and separation of xylene isomers Adsorptive	[90]
ZIF-8	Bentonite (20%)	Monolith	1415	1083	Separations/biobutanol recovery	[91]
ZIF-8	Bentonite (16.7%) and MC (16.7%)	Monolith	1415	1070	Adsorptive Separations/biobutanol recovery	[91]
HKUST-1	Bentonite (15%) and MC (15%)	Pellet	1271.2	605.1	MOF shape engineering	[92]
ZIF-8	Bentonite (15%) and MC (15%)	Pellet	2047	1471.5	MOF shape engineering	[92]
ZIF-67	Bentonite (15%) and MC (15%)	Pellet	1789.6	464.4	MOF shape engineering	[92]
UiO-66	Bentonite (15%) and MC (15%)	Pellet	1110.8	187.4	MOF shape engineering	[92]
MIL-101(Cr)	Bentonite (25%)	Monolith	-	-	$CO_2$ adsorption	[93]
MIL-101 (Cr)	Bentonite (25/40%)	Monolith	-	-	CO <sub>2</sub> adsorption	[94]
MIL-100(Fe)	Silica sol (10%)	Granule	1772	1619	Separation of SF <sub>6</sub> from SF <sub>6</sub> /N <sub>2</sub> mixture	[95]
UiO-66(Zr)	ρ-alumina (5%)	Bead	903	619	Room temperature gas adsorption/H <sub>2</sub> O and CH <sub>4</sub> adsorption	[96]
MIL-100(Fe)	ρ-alumina (5%)	Bead	1928	1451	Room temperature gas adsorption/H <sub>2</sub> O and CH <sub>4</sub> adsorption	[96]
MIL-127(Fe)	ρ-alumina (5%)	Bead	1413	1266	Room temperature gas adsorption/H <sub>2</sub> O and CH <sub>4</sub> adsorption	[96]
MIL-101	Sodium silicate and starch (7%)	Pellet	2730	1910	CO <sub>2</sub> adsorption	[97]
MIL-100(Fe)	Silica (10%)	Granule	-	1568	$C_2/C_3$ hydrocarbon separation	[98]
$Cu_3(BTC)_2$	Silres MSE 100 (13.8%)	Monolith	-	484	MOF shape engineering	[99]
ZIF-8	ρ-alumina (5/10/15%)	Pellet	-	-	$CH_4/N_2$ separation	[100]
MIL-53(Al)	ρ-alumina (5/10/15%)	Pellet	-	-	$CH_4/N_2$ separation	[100]
ZIF-7	Silica (15%)	Monolith	16	40	Adsorption of ethane and ethylene	[101]
MOF-74(Ni)	Bentonite (15%) and PVA (5%)	Monolith	1180	737	Gas adsorption	[102]
UTSA-16(Co)	Bentonite (10%) and PVA (5%)	Monolith	727	568	Gas adsorption	[102]
MIL-101	Bentonite (15%) and PVA (5%)	Monolith	2400	2200	CO <sub>2</sub> removal from enclosed environments	[103]

#### Table 2. Cont.

# 3.3. Processes without Binders

In addition to shaping processes that utilize a binding agent, there are forming procedures that do not require an adhesive. Dhainaut et al. [104] used a tableting instrument to form UiO-66, UiO-67, UiO-66-NH<sub>2</sub>, and HKUST-1 into tablets without utilizing a binding agent. As observed, with regard to the MOFs of the study, the mechanical stability is proportional to the tablet's bulk density, whereas the latter is disproportional to the surface area. In particular, for a 1.8 to 3.4-fold increase of the tablet's density, the surface area reduces from 0 up to 30%. Zhang et al. reported on the first high-internal-phase emulsion (HIPE) system developed with a metal–organic framework [28]. They stirred an assembly of MOF HKUST-1 nanocrystals together with a water and oil interface at room temperature and reported a HIPE with good stability suitable for highly porous applications of metal–organic aerogel monoliths. Similarly, Tian et al. reported on the production of four different types of ZIF-8 monoliths (ranging from 1 mm<sup>3</sup> to 1 cm<sup>3</sup>), abbreviated as ZIF-8HT, ZIF-8LT, ZIF-8LT-HT, and ZIF-8ER, according to the processing method followed, at room temperature and without the use of binders by following a sol-gel process [105]. The resulting monoliths are transparent and maintain both fluorescent capability and ZIF-8 porosity. Tian et al., in a following study [106], extended this approach to develop HKUST-1 binderless monoliths, which achieved an exceptional methane uptake capacity of 259 cm<sup>3</sup> (at standard temperatures and pressures (STP)) per cm<sup>3</sup> of MOF, reaching the US Department of Energy target [107] of 263 cm<sup>3</sup> (STP) cm<sup>-3</sup> for methane storage, opening the gate for real-life energy-related applications with regard to absorbed natural gas. Bueken et al. reported on the developments of Zr-MOF with a special focus on the presence of water, metal source, and reactant concentration [108]. They developed both monoliths and spheres by following xero gel and oil-drop granulation processes, respectively. The authors suggested that the methodology followed can be applied for further catalysis or

adsorption applications and the fabrication of transparent films and coatings.

Purewal et al. reported on the development of MOF-5 as a hydrogen storage material [109]. They fabricated MOF-5 powder and applied it by pressing it into pellets of various bulk density. The resulting structures were then evaluated with respect to their thermal conductivity, hydrogen adsorption, specific surface area, and crush strength. Tagliabue et al. investigated the fabrication of nickel-based MOF, i.e., CPO-27-Ni, as an adsorbent for gaseous fuels applications [110]. They developed pellets through the application of varied mechanical pressure (0.1–1 GPa) and compared them accordingly with respect to modifications to their crystal structure and methane specific capacity. Majchrzak-Kuceba and Sciubidlo reported on the fabrication of two types of MOF, i.e., CuBTC and MIL-53(Al), and the impact of tabletization, pressure, and time on their carbon dioxide adsorption property. They followed the no-binder pelletizing method by applying a varied pressure  $(3.7-59.2 \text{ kN m}^{-2})$  for different time-steps (0.5 and 2 min) [111]. Interestingly, Lim et al. reported a direct ink writing 3D-printing technique to develop a jelly-like HKUST-1 monolith without any binder, which was then tested for its methane storage capacity [112]. The monolith displayed a surface area of 1134 m<sup>2</sup> g<sup>-1</sup> and it retained high levels of crystallinity and porosity, making it a good candidate for energy or gas storage. On the contrary, in another study [113] that also explored the methane storage performance of binderless HKUST-1 macrostructures, it was shown that when HKUST-1 powder was subjected to high compression forces ranging from 0.5 to 5 tons to form wafers, its porosity diminished and its volumetric methane uptake capacity was significantly reduced. A list of MOF structures, formed without the addition of any binder is presented in Table 3.

Table 3. Summary of shaped MOFs without the addition of binders.

MOF	Binder	Shape	$S_{BET}$ Powder (m <sup>2</sup> g <sup>-1</sup> )	$\begin{array}{c} S_{BET} \ Body \\ (m^2 \ g^{-1}) \end{array}$	Application	Reference
Cu <sub>3</sub> (BTC) <sub>2</sub>	None	Monolith	307	834	No application/MOF shape engineering	[28]
UiO-66	None	Tablet	1426	1459	No application/MOF shape engineering	[104]
UiO-67	None	Tablet	2034	1549	No application/MOF shape engineering	[104]
UiO-66-NH <sub>2</sub>	None	Tablet	839	625	No application/MOF shape engineering	[104]
HKUST-1	None	Tablet	1288	1091	No application/MOF shape engineering	[104]
ZIF-8HT	None	Monolith	-	1387	No application/MOF shape engineering	[105]
ZIF-8LT	None	Monolith	-	1359	No application/MOF shape engineering	[105]
ZIF-8LT-HT	None	Monolith	-	1423	No application/MOF shape engineering	[105]
ZIF-8ER	None	Monolith	-	1395	No application/MOF shape engineering	[105]
HKUST-1	None	Monolith	-	1193	Methane adsorption	[106]
UiO-66	None	Sphere	1167	1127	No application/MOF shape engineering	[108]
MOF-5	None	Pellet	2762	2707	Hydrogen storage	[109]
CPO-27-Ni	None	Pellet	-	-	Methane storage	[110]
CuBTC	None	Pellet	-	-	$CO_2$ capture	[111]
MIL-53(Al)	None	Pellet	-	-	$CO_2$ capture	[111]
HKUST-1	None	monolith	-	1134	Methane storage	[112]
HKUST-1	None	tablet	1850	-	Methane storage/MOF shape engineering	[113]

## 4. Conclusions

Developing the powdery form of MOF into a monolith is of high importance to various sectors of the industry, as this would make the utilization of MOFs in technical applications much easier. Powders are not suitable for industrial applications, with the most important reasons being obvious: powder is not easy to handle, it is susceptible to abrasion, it blocks or reduces the flow of fluids, and mass loss due to powder blowing is another important issue. Therefore, shaping MOFs into macrostructures would made their utilization in real-life applications viable.

For this purpose, binding agents are widely utilized to develop the powder particles into bigger structures as depicted in Figure 6. Polymer binders (e.g., PVA, PVB, MC) and inorganic binders (e.g.,  $\rho$ -alumina, silica) are two suitable categories of adhesive agents that are used in either pressurized or non-pressurized processes to form a MOF into a pellet, a granule, or a monolith. As noted in other works [5,8,22,114] and also depicted in this study, polymer-type binders have lower weights compared to inorganic binders, which enhances the performance of the structure. These binders are more well-studied and are easier to handle, but on the other hand, there is an increased possibility of pore blockage and reduction of the specific surface area of the MOF, and subsequently, its uptake capacity to gases. However, inorganic binders demonstrate high thermal stability, enhanced mechanical stability, and provide high resistance to abrasion. Therefore, critical information about their behavior and their effects on the MOF structured monoliths will allow for the shaping of even better and more efficient structures. Thus, further research is required to investigate, for example, MOF/binder compatibility, the capabilities of the material after several regeneration cycles, and the improvement of the shaping procedures for reduced loss of MOF powder during the formation process.



Figure 6. Conclusions scheme.

MOFs are promising nanomaterials for successful applications in various sectors that, until now, the research community has not fully explored. The built environment, for example, is a field that may offer many applications for MOFs, given that they come in a form that is easy to handle. As seen in this review, although scarce, some pioneering applications using MOF shaped bodies try to address issues related to the built environment, such as (i) air purification, (ii) carbon dioxide capture from indoor environments, (iii) increased energy efficiency in water adsorption heat transformation systems as methane adsorbents, (iv) as dehumidifiers, and (v) as natural gas/methane or hydrogen storage agents, which may be a potential application in the future within buildings with regard to energy consumption and storage. Therefore, there are some initial signs that cooling and heating systems, dehumidifiers, filters for air purification, or even decorative indoor ornaments incorporating the porous characteristics of MOFs might gain added value to their functionality and capture  $CO_2$  or other greenhouse gases, paving the way for real decarbonization of our world. However, for this to be realized, MOFs should be available as rigid macrostructures that maintain their working capacities.

**Author Contributions:** Conceptualization, V.N.; methodology, V.N.; formal analysis, V.N. and I.K.; investigation, V.N. and I.K.; writing—original draft preparation, V.N. with support from I.K.; review and editing, I.K., M.N.A. and A.L.P.; supervision, M.N.A. and A.L.P. All authors have read and agreed to the published version of the manuscript.

Funding: This research has received funding from the European Union's Horizon 2020 research and innovation programme under the Marie Skłodowska-Curie Grant Agreement No. 765057-SAFERUP! Project.

Institutional Review Board Statement: Not applicable.

Informed Consent Statement: Not applicable.

Data Availability Statement: Not applicable.

Acknowledgments: The authors would like to acknowledge the European Union's Horizon 2020 research and innovation programme under the Marie Skłodowska-Curie Grant Agreement No. 765057 SAFERUP!, website https://site.unibo.it/saferup/en (accessed on 25 January 2022).

Conflicts of Interest: The authors declare no conflict of interest.

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