



Article Peroxymonosulfate Activation by Palladium(II) for Pollutants Degradation: A Study on Reaction Mechanism and Molecular Structural Characteristics

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Abstract: Compared with certain transition metals (e.g., iron, cobalt, and manganese), noble metals are less frequently applied in peroxymonosulfate (PMS)-based advanced oxidation processes (AOPs). Palladium (Pd), as one of noble metals, has been reported to possess the possibility of both radical mechanisms and electron transfer mechanisms in a heterogeneous Pd/PMS system, however, data are still sparse on the homogeneous Pd/PMS system. Therefore, this work aims to explore the homogeneous reactivity of PMS by Pd(II) ions from the aspects of reaction parameters, radical or non-radical oxidation mechanisms, and the relationship between pollutants' degradation rate and their molecular descriptors based on both experimental data and density functional theory (DFT) calculation results. As a result, the reaction mechanism of Pd(II)/PMS followed a radical-driven oxidation process, where sulfate radicals (SO4 $^{\bullet-}$), rather than hydroxyl radicals (HO \bullet), were the primary reactive oxidant species. BO_x and E_{HOMO} played significant roles in pollutant degradation during the Pd(II)/PMS system. It turned out that the bond's stability and electron donation ability of the target compound was responsible for its degradation performance. This finding provides an insight into PMS activation by a noble metal, which has significant implications for scientific research and technical development.

Keywords: peroxymonosulfate (PMS); Pd(II); sulfate radical; BOx; EHOMO

1. Introduction

The fast development of industrialization can lead to not only the enhancement of the quality of human life, but a growing number of problems concerning environmental pollution, in particular wastewater as well. Thus, wastewater treatment has been considered one of the primary challenges over the past decades since it contains numerous pathogenic or disease-causing microorganisms and toxic compounds [1,2]. To this end, various technologies have been developed, such as adsorption [3], biological treatment [4], membrane separation [5], and advanced oxidation processes (AOPs) [6]. Unfortunately, the traditional wastewater treatment plants that are based on biological strategies (e.g., activated sludge and biofilm) are insufficient to successfully neutralize a line of emerging contaminants with high toxicity and refractory molecular structure. Accordingly, AOPs have been regarded as promising techniques for wastewater treatment owing to their easy operation and versatility, outstanding removal efficiency, minimal energy consumption, and simultaneous decontamination of multiple pollutants within a short time, even seconds [7–9].

AOPs that are based on sulfate radical (SO₄ $^{\bullet-}$), produced from peroxymonosulfate (PMS) and peroxydisulfate (PDS), have attracted considerable attention due to their high



Citation: Yang, B.; Ma, Q.; Hao, J.; Sun, X. Peroxymonosulfate Activation by Palladium(II) for Pollutants Degradation: A Study on Reaction Mechanism and Molecular Structural Characteristics. *Int. J. Environ. Res. Public Health* **2022**, *19*, 13036. https://doi.org/10.3390/ ijerph192013036

Academic Editor: Paul B. Tchounwou

Received: 20 September 2022 Accepted: 9 October 2022 Published: 11 October 2022

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Copyright: © 2022 by the authors. Licensee MDPI, Basel, Switzerland. This article is an open access article distributed under the terms and conditions of the Creative Commons Attribution (CC BY) license (https:// creativecommons.org/licenses/by/ 4.0/). reactivity and selectivity in organic pollutants and complex environmental matrices [8,10]. Compared to conventional hydroxyl radicals (HO•), $SO_4^{\bullet-}$ contains a series of merits: (i) $SO_4^{\bullet-}$ has higher oxidation potential (2.5–3.1 V) than HO• (1.7–2.5 V) [11]; (ii) classical Fenton oxidation, which is commonly applied to generate HO•, works efficiently only in acidic conditions (pH \leq 4.0) [12–15], while $SO_4^{\bullet-}$ could react effectively with organic pollutants under a wide pH range of 2.0–12.0 [16–18]; and (iii) $SO_4^{\bullet-}$ (30–40 µs) possesses a longer half-life period than HO• (<1 µs), which could enable sulfate radicals to have more stable mass transfer and react better with organic pollutants [19,20]. In this regard, several low-valent transition metals (i.e., Fe(II), Co(II), and Mn(II)) have been proven to be effective activators for wastewater treatment. For instance, Co(II) ion and cobalt oxides (i.e., Co₃O₄) could effectively transform PMS into $SO_4^{\bullet-}$, thereby, the cobalt-induced PMS activation achieved outstanding treatment performance for wastewater involving 2,4-dichlorophenol (2,4-DCP), atrazine, naphthalene, bisphenol A (BPA), ciprofloxacin (CIP), chloramphenicol (CAP), and phenol [21–25].

In addition to transition metals, certain noble metals have recently been reported to be activators for PMS. Ahn et al. performed a comprehensive survey on 20 transition and noble metals. They found transition metals (i.e., Co, Cu, and Mo) could induce radical degradation mechanisms in the PMS system. In contrast, noble metals (i.e., Au, Ir, Pt, and Rh) followed electron transfer activation without involving the generation of radical species, such as HO• and $SO_4^{\bullet-}$. Interestingly, palladium (Pd), as one of the noble metals, had the possibility of both radical mechanisms and electron transfer mechanisms [26]. By comparing Pd nanoparticles that were anchored on various supporters such as Al_2O_3 , TiO_2 , SiO_2 , $g-C_3N_4$, C, and TiC, Feng et al., found that Pd-SiO_2 obtained the highest reactivity of decomposing 1,4-dioxane in the PMS system. According to radical quenching tests, methanol was oxidized to formaldehyde (HCHO) by the whole Pd nanoparticles, which indicated that the degradation pathway followed a radical mechanism [27]. Furthermore, both the abovementioned works mainly focused on heterogeneous Pd, however, data are still sparse on the homogeneous Pd/PMS system.

Therefore, this study aims to further explore the homogeneous reactivity of PMS by Pd(II) ions, primarily focusing on (1) examining the effect of operating parameters such as the initial Pd(II) dosage, PMS amount, pH, and temperature; (2) exploring the main reactive oxygen species involving radicals (HO• and $SO_4^{\bullet-}$) and non-radicals (¹O₂); (3) investigating the degradation performance of 16 pollutants containing pharmaceutical and personal care products (PPCPs), endocrine-disrupting chemicals (EDCs), dyes, as well as other emerging and traditional contaminants; and (4) revealing the relationship between the degradation rate and molecular structural characteristics based on the density functional theory (DFT) method. The findings from this work would provide an insight into PMS activation by noble metals, which has significant implications for scientific research and technical development.

2. Experimental

2.1. Chemicals and Materials

Phenol was regarded as a model contaminant for investigating the effect of operating parameters. A total of 16 organic pollutants were selected to systematically evaluate the reactivity of the Pd(II)/PMS system, namely carbamazepine (CBZ) and caffeine for PPCPs; bisphenol A (BPA) for EDCs, acid orange 74 (AO74) and rhodamine B (RB) for dyes; as well as phenol, 4-chlorophenol (4-CP), 2,4-dichlorophenol (DCP), 2,4,6-trichlorophenol (TCP), 4-nitrophenol (NP), 1,4-dioxane (1,4-D), 4-hydroxyphenylacetic acid (4-HBA), 4-nitrobenzoic acid (4-NBA), 4-nitroaniline (4-NA), benzoic acid (BA), and nitrobenzene (NB) for emerging and traditional contaminants. Oxone (2KHSO₅·KHSO₄·K₂SO₄) and Na₂PdCl₄ were used as the oxidant and activator, respectively. A complete list of the chemicals is shown in Table S1.

2.2. Experimental Procedures

Unless otherwise specified, the degradation of different target pollutants (50 μ M) was performed in a 50 mL reactor (50 mL wide-mouth glass bottle) with magnetic stirring of 800 rpm at room temperature under air-equilibrated conditions. The experimental suspensions typically consisted of a 0.25 mM PMS, and 25 μ M Pd(II) ions activator. The initial solution pH was designed as 4.0 \pm 0.1 based on containing 0.25 mM PMS. A total of 1 M of HClO₄ or NaOH was used as a pH adjuster for investigating the effect of the initial pH. Sample aliquots were withdrawn from the reactor at the desired reaction time using a 1 mL syringe, filtered through a 0.45 μ m PTFE filter (Millipore), then transferred into a 2 mL vial containing 20 μ L MeOH (equal to ~0.5 M in 1 mL sample) to scavenge the possible residual oxidants. The brief experimental process is shown in Scheme S1 in the Supplementary Materials.

The concentrations of all the target pollutants were detected by high-performance liquid chromatography (HPLC, Agilent Infinity 1260, Santa Clara, CA, USA) that was equipped with a C-18 column and a UV/Vis detector. The mobile phase contained three tubes, namely H₃PO₄ solution (0.1%, v/v), pure acetonitrile (ACN), and pure MeOH. Formaldehyde (HCHO) that forms as a result of MeOH oxidation was quantitatively detected by HPLC after derivatization using 2 mM of 2,4-dinitrophenylhydrazine (DNPH) in ACN [28]. The details, such as solution ratio, wavelength, and flowrate, are presented in Table S2. PMS was detected according to the method that was suggested by Liang et al., based on the generation of iodine ($\lambda_{max} = 352$ nm) from the oxidation of I⁻¹ by PMS [29]. Bromate (BrO₃⁻) was measured by an ion chromatograph (IC, Dionex DX120, Sunnyvale, CA, USA) that was equipped with a Dionex IonPac AS-14 and a conductivity detector.

2.3. Computation Details

The information on the molecular characters that were used in this work is listed in Table S3. These descriptors have been successfully used in revealing the correlation between pollutant degradation performance and molecular parameters during other advanced oxidation processes (AOPs), e.g., Fenton oxidation, ozonation, and supercritical water oxidation [30–34]. The whole 17 molecular descriptors of the compounds were calculated by Material Studio 6.1 (Dmol3/GGA-BLYP/DNP(3.5) basis, Beijing, China) and Gaussian 09 (DFT B3LYP/6-311G level, Beijing, China). At first, the structure of the target compound was drawn and optimized through Gaussian 09 (DFT B3LYP/6-311G level). Thus, the exchange, correlation terms, and natural population analysis of atom charge were calculated by B3LYP function. Finally, certain molecular descriptors were achieved directly from the output files, such as dipole moment (μ), the total energy of a molecule in the B3LYP level (E_{B3LYP}) , the energy of the highest and lowest occupied molecular orbital (E_{HOMO} and E_{LUMO} , respectively), the positive partial charge on a hydrogen atom (q(H)_x), the negative or positive partial charge on a carbon atom $(q(C)_n \text{ and } q(C)_x, \text{ respectively})$, and the positive partial charge of a hydrogen atom connected to a carbon atom $(q(C-H)_n \text{ and } q(C-H)_x)$. As for bond order and Fukui indices, they were calculated via Material Studio 6.1 with DMol3 code, 6–311g (d,p) basis set and B3LYP function. A double numerical basis set with polarization functional was adopted at first. Afterwards, the density mixing and self-consistent field were set as 0.2 charge with 0.5 spin and 10^{-6} a.u., respectively. Then the results of bond order and Fukui indices were obtained from an outmol file, which included that the minimum and maximum number of chemical bonds between a pair of coterminous atoms (BO_n and BO_x), the minimum or maximum value of Fukui indices by radical attack ($F(0)_n$ and $F(0)_x$), by nucleophilic attack ($F(+)_n$ and $F(+)_x$), and by electrophilic attack $(F(-)_n \text{ and } F(-)_x)$. At last, the information on molecular descriptors was acquired from an outmol file.

3. Results and Discussion

3.1. Effect of Reaction Parameters

Several parameters, such as the Pd(II) dosage, PMS concentration, reaction temperature, and the initial pH, were examined for the degradation of phenol during the Pd(II)/PMS system (Figure 1). As expected, the degradation of phenol was largely enhanced with increasing Pd(II) dosage, PMS amount, and reaction temperature. In terms of Pd(II) dosage, the removal efficiency of phenol was 48% and 76% at 30 min for Pd(II) addition of 5 μ M and 10 μ M, respectively, while complete degradation of phenol was observed within 10 min and 2 min as Pd(II) dosage was enhanced to 25 μ M and 50 μ M, respectively (Figure 1a). For PMS concentration, merely 37% of phenol degradation was obtained at 0.1 mM PMS, and it increased to 76% as PMS was raised to 0.25 mM, then almost 100% was achieved within 5 min with promoting PMS to 0.5 mM and 1 mM (Figure 1b). As for the reaction temperature, the degradation efficiency of phenol was gradually improved to 60%, 76%, 89%, and 100% by augmenting the temperature from 4 °C to 65 °C (Figure 1c). Interestingly, the effect of pH showed a similar trend of phenol degradation in general (Figure 1d). This was attributed to the un-buffered solutions, where the presence of acidic Pd(II) and PMS stock solutions, as well as the release of H⁺ during the activation of PMS would lead to an unavoidable instant decline of pH (from the alkalescent or near-neutral to acidic condition). As displayed in Figure S1, the solution pH dropped to 2.9–4.1 at the end of the reaction. Besides, the control experiment regarding PMS or Pd(II) alone exhibited negligible phenol degradation (Figure S2), which elucidated that phenol removal by adsorption and direct PMS oxidation was marginal. As a result, the successful phenol degradation efficiency was mainly responsible for the activation of PMS by Pd(II). This was attributed to the decomposition of PMS by various Pd(II) dosages (Figure S3), therein, the more Pd(II) dosage that was added, the more PMS that was consumed after 30 min. Moreover, the homogenous Pd(II)/PMS system seems to display better phenol removal performance than the heterogeneous Pd-Al₂O₃/PMS system, where the removal efficiency of phenol was less than 70% [35].



Figure 1. Effect of Pd(II) dosage (**a**), PMS concentration (**b**), reaction temperature (**c**), and initial pH (**d**) on the degradation of phenol. Condition: (**a**). [phenol] = 50 μ M, [PMS] = 0.25 mM, pH_i = 4; (**b**). [phenol] = 50 μ M, [Pd(II)] = 10 μ M, pH_i = 4; (**c**). [phenol] = 50 μ M, [PMS] = 0.25 mM, [Pd(II)] = 10 μ M, pH_i = 4; (**d**). [phenol] = 50 μ M, [PMS] = 0.25 mM, [Pd(II)] = 10 μ M, pH_i = 4; (**d**). [phenol] = 50 μ M, [PMS] = 0.25 mM, [Pd(II)] = 10 μ M.

3.2. Reaction Mechanism

Several alcohol-based scavengers such as methanol (MeOH) and tert-butyl alcohol (TBA) are commonly used in quenching experiments to identify whether radical (i.e., HO• and $SO_4^{\bullet-}$) is the primary reactive oxidant species during PMS-AOPs [8,26,35]. In this regard, the degradation of phenol in the addition of MeOH and TBA was performed (Figure 2a), where the effect of TBA on phenol degradation was negligible. In contrast to that, an obvious quenching effect was found in the presence of MeOH. This was ascribed to $SO_4^{\bullet-}$, rather than HO \bullet , as the primary reactive oxidant during Pd(II)/PMS system, given that TBA is a specific HO• scavenger ($k_{HO•} = 6 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$ $k_{SO4\bullet-} = 7.6 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$) while MeOH can quench both HO• versus $(k_{HO\bullet} = 9.7 \times 10^8 \text{ M}^{-1} \text{ s}^{-1})$ and $SO_4^{\bullet-} (k_{SO4\bullet-} = 2.5 \times 10^7 \text{ M}^{-1} \text{ s}^{-1})$ [11,36]. Additional evidence for the generation of SO4^{•-} was achieved by monitoring the oxidant production of formaldehyde (HCHO) from MeOH and bromate (BrO_3^{-}) from bromide (Br^{-}) (Figure 2b). It showed a steep increase in both HCHO and BrO_3^- concentration. The $SO_4^{\bullet-}$ -driven oxidation is undergo through facile one-electron oxidation of Br⁻ to Br• by $SO_4^{\bullet-}$ (k = $3.5 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$) [36], then followed by oxidation to BrO_3^{-} through intermediates (BrO⁻ and BrO₂⁻) [37]. By contrast, the BA-to-4-HBA conversion failed (Figure 2b), which excluded that HO• played a significant role in the Pd(II)/PMS system, given that 4-HBA, as the main oxidant product of BA, was commonly detected during HO•-induced BA oxidation [38]. Analogous to the Pd(II)/PMS system, Co(II)/PMS, as a typical $SO_4^{\bullet-}$ driven oxidation system [39], also displayed similar phenomena in the production of HCHO, BrO₃⁻, and 4-HBA (Figure S4). Therefore, the reaction mechanism of Pd(II)/PMS probably followed $SO_4^{\bullet-}$ -driven oxidation.



Figure 2. (a) The effect of MeOH and TBA on the degradation of phenol, and (b) oxidant production of HCHO, bromate, and 4-HBA in Pd(II)/PMS system. Condition: (a). [phenol] = 50 μ M, [PMS] = 0.25 mM, [Pd(II)] = 25 μ M, [MeOH] = [TBA] = 200 mM, pH_i = 4; (b). [MeOH] = 200 mM, [Br⁻] = 0.1 mM, [BA] = 10 mM, [PMS] = 0.25 mM, [Pd(II)] = 25 μ M, pH_i = 4.

To investigate whether ${}^{1}O_{2}$ was involved in PMS activation by Pd(II), p-benzoquinone (p-BQ), furfuryl alcohol (FFA), azide ion (N₃⁻), and L-histidine were introduced to the quenching experiment based on k = $9.8 \times 10^{8} \text{ M}^{-1} \text{ s}^{-1}$ of (p-BQ) [40], $1.2 \times 10^{8} \text{ M}^{-1} \text{ s}^{-1}$ (FFA), $1.0 \times 10^{9} \text{ M}^{-1} \text{ s}^{-1}$ (N₃⁻), and $1.5 \times 10^{8} \text{ M}^{-1} \text{ s}^{-1}$ (L-histidine) for ${}^{1}O_{2}$ [41,42]. As shown in Figure 3, phenol degradation was largely suppressed by the presence of p-BQ, FFA, N₃⁻, and L-histidine. Whereas such inhibition was ascribed to the direct PMS depletion by these oxidant scavengers in their excess amounts (Figure S5), therein PMS was consumed around 98% for FFA, L-histidine, and N₃⁻, and over 93% for p-BQ at the reaction time of 0.5 min, which was also in agreement with recent works [43,44]. To further determine the occurrence of ${}^{1}O_{2}$ during the Pd(II)/PMS system, a control experiment was conducted in D₂O solution according to D₂O which could extend the lifetime of ${}^{1}O_{2}$ by tenfold [45],

thus the solvent exchange would promote the singlet oxygenation of pollutant [43]. In contrast, there was no enhancing effect on phenol degradation when H_2O was replaced by D_2O (Figure 3), which allowed us to discount the possible involvement of 1O_2 as a reactive oxidant in the Pd(II)/PMS system.



Figure 3. The effect of ${}^{1}O_{2}$ scavengers and $D_{2}O$ solution on phenol degradation in the Pd(II)/PMS system. Condition: [phenol] = 50 μ M, [PMS] = 0.25 mM, [Pd(II)] = 25 μ M, [FFA] = [L-histidine] = [N_{3}⁻] = 200 mM, [p-BQ] = 100 mM, pH_i = 4.

3.3. Oxidative Degradation of Various Pollutants

In order to systematically evaluate the reactivity of PMS by Pd(II), sixteen kinds of organics on behalf of the emerging and traditional pollutants were introduced in our study. As displayed in Figure 4, various pollutants resulted in different degradation efficiencies, where nitrobenzene (NB) was removed by merely 38% at the reaction time of 30 min, while 4-CP, DCP, and TCP achieved 100% degradation efficiencies within 5 min. Such a discrepancy was attributed to the structural properties of pollutants. For instance, the electron-withdrawing groups (e.g., nitro and carboxylic groups in NB, 4-NBA, and BA) tend to be sluggish towards $SO_4^{\bullet-}$, while the electron-donating groups (e.g., hydroxyl and chloride groups in phenol, 4-CP, DCP, and TCP) exhibited high susceptibility to $SO_4^{\bullet-}$, which was analogous to the previous literature regarding sulfate radical-based AOPs [46]. In addition, the dyes like AO74 and RB acquired better degradation efficiencies, which contributed to their chromogenic group (i.e., diazo group) that could be easily attacked by radicals [47]. Similar results were also found in the recent work [35], where Ahn et al. investigated the heterogeneous Pd/PMS system using Pd-Al₂O₃ nanoparticles and observed the target compounds containing the electron-withdrawing groups (e.g., 4-NP, BA, and CBZ) were hardly removed, while the chemicals containing the electron-donating groups (e.g., phenol, BPA, 4-CP, and TCP) obtained better degradation performance.



Figure 4. Degradation of various pollutants in Pd(II)/PMS system. Condition: [pollutant] = 50 μ M, [PMS] = 0.25 mM, [Pd(II)] = 25 μ M, pH_i = 4. (**a**) for the target compounds of NB, 4-NBA, BA, NP, Caffeine, CBZ, 4-NA, and 4-HBA; (**b**) for BPA, AO74, RB, 1,4-D, Phenol, 4-CP, DCP, and TCP.

3.4. Relationship between k and Molecular Descriptors

The quantum properties of these contaminants were calculated by DFT to explore the further the correlation between oxidative degradation and molecular structural characteristics (Table S4). Furthermore, the degradation rate of pollutants was calculated by a pseudo-first-order kinetic model as follows:

$$\ln \frac{[C]_0}{[C]_t} = kt$$

where $[C]_0$ stands for the initial concentration of each compound (namely 50 μ M), $[C]_t$ indicates its concentration at time t, k represents the degradation rate constants of each compound, and t is the reaction time. Accordingly, all the k values, their respective molecular descriptors, and the correlation coefficients of 16 target pollutants are listed in Table S4. The correlation implied that $q(H)_{x,r}q(C)_n$, $F(-)_n$, $F(-)_x$, $F(+)_n$, $F(+)_x$, $F(0)_n$, and $F(0)_x$ were positively correlated to k, while μ , E_{B3LYP} , E_{LUMO} , E_{HOMO} , $q(C)_x$, $q(C-H)_n$, $q(C-H)_x$, BO_n , and BO_x were negatively correlated to k. The significance of molecular descriptors towards k on the basis of the absolute value followed the order that BO_x $(-0.543) > E_{HOMO} (-0.509) > E_{B3LYP} (-0.467) > F(0)_x (0.447) > F(-)_n (0.408) > F(-)_x (0.377)$ $> E_{LUMO} (-0.318) > F(0)_n (0.315) > F(+)_x (0.275) > q(C)_x (-0.265) > \mu (-0.242) > q(H)_x (0.228)$ $> F(+)_n (-0.210) > BO_n (-0.209) > q(C-H)_n (-0.203) > q(C)_n (-0.180) > q(C-H)_x (-0.101).$ It turned out that the most relative parameter was BOx, which greatly affected pollutant degradation in the Pd(II)/PMS system. Indeed, BO (bond order) reflects the number of the chemical bond between a pair of atoms, namely a higher value of BO could lead to more stability in the bond. In other words, the less the BO value was, the more easily it could be attacked, resulting in bond cleavage [48,49]. Besides, E_{HOMO}, as another essential molecular parameter, is a measure of the electron donation ability of the target compound. This was in agreement with the finding of Section 3.3. Therein the compounds containing electron-withdrawing groups (e.g., nitro and carboxylic groups in NB, 4-NBA, and BA) presented relatively lower k values, while the chemicals possessing electron-donating groups (e.g., hydroxyl and chloride groups in phenol, 4-CP, DCP, and TCP) showed better degradation performance (Figure 4). Besides, compared with the relationship between kand molecular descriptors in other AOPs, such as the supercritical water oxidation (SCWO) process [33], where $F(+)_n$, $F(-)_n$, $F(0)_n$, and E_{HOMO} achieved high correlation coefficients in the SCWO system, and followed an order that $F(-)_n$ (-0.425) > $F(+)_n$ (-0.417) > E_{HOMO} $(0.415) > F(0)_n$ (-0.402), which was lower than the correlation coefficients achieved in this work (i.e., BO_x (-0.543) > E_{HOMO} (-0.509) > E_{B3LYP} (-0.467) > $F(0)_x$ (0.447)). This indicates

the correlation coefficients that were acquired in this work had more significant correlation than those in SCWO process.

4. Conclusions

The homogeneous PMS activation by Pd(II) has been found to exhibit highly effective degradation performance for pollutants. The degradation efficiency was enhanced with increasing Pd(II) dosage, PMS concentration, and reaction temperature, while the initial solution pH showed a similar trend of pollutant degradation in a wide un-buffered pH range of 3–9. Sulfate radical (SO₄ \bullet^-) was proposed as the dominant reactive oxidant species based on the quenching effect with excess MeOH and the high amount of Br⁻-to- BrO_3^- conversion. In contrast, hydroxyl radicals (HO•) and singlet oxygen (1O_2) played minor roles in the Pd(II)/PMS system. According to the correlation between the degradation rate (k) and molecular descriptors, BO_x and E_{HOMO} were the critical parameters for 16 target pollutants degradation during the Pd(II)/PMS system. In other words, the bond's stability and electron donation ability of the target compound acted as an essential part of the pollutant degradation performance. In sum, the homogeneous Pd(II)/PMS system displayed an outstanding reactivity performance in a wide of pH and temperatures, therefore, a potential application of Pd(II)/PMS should be considered in practical wastewater treatment. Moreover, the findings from this work provide an insight into PMS activation by noble metals, which has significant implications for scientific research and technical development. Additionally, considering Pd is a kind of noble metal and its price is not economic, future work should focus on recycling the Pd(II) ions via introducing ligands, such as nitrilotriacetic acid (NTA), ethylenediamine tetraacetic acid (EDTA), oxalate acid, and citric acid.

Supplementary Materials: The following supporting information can be downloaded at: https:// www.mdpi.com/article/10.3390/ijerph192013036/s1. Figure S1: Final solution pH of the experiment regarding the effect of the initial pH of 3, 4, 5, 7, and 9 in the Pd(II)/PMS system. Figure S2: Degradation of phenol by PMS or Pd(II) alone. Figure S3: Decomposition of PMS by various Pd(II) dosages after 30 min. Figure S4: Oxidant production of HCHO, bromate, and 4-HBA in the Co(II)/PMS system. Figure S5: Comparison of PMS concentration with and without the presence of ¹O₂ scavengers at the reaction time of 5 min. Scheme S1. Typical experimental process in this work from sample preparation to detection by HPLC-UV. Table S1: Information of chemicals and materials. Table S2: Operating conditions for high-performance liquid chromatographic analysis. Table S3: The interpretation on 17 molecular characters. Table S4: Relationship between degradation rate (k) and 17 molecular descriptors of 16 target pollutants in the Pd(II)/PMS system.

Author Contributions: Conceptualization, J.H.; methodology, B.Y. and Q.M.; formal analysis, B.Y. and Q.M.; investigation, B.Y.; resources, B.Y.; data curation, B.Y.; writing—original draft preparation, B.Y.; supervision, X.S.; project administration, B.Y. and X.S.; funding acquisition, B.Y. and X.S. All authors have read and agreed to the published version of the manuscript.

Funding: This research was financially supported by the Open Fund of Sichuan Provincial Engineering Research Center of City Solid Waste Energy and Building Materials Conversion & Utilization Technology (GF2022ZC005), and the National Natural Science Foundation of China (No. 52070049).

Institutional Review Board Statement: Not applicable.

Informed Consent Statement: Not applicable.

Data Availability Statement: The data that support the findings of this study are available from the authors upon reasonable request.

Acknowledgments: Bowen Yang thanks Hongshin Lee for his fellowship and help.

Conflicts of Interest: The authors declare no conflict of interest.

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