

# Article Supplementary Material to "Analytical Determination of the Nucleation-Prone, Low-Density Fraction of Subcooled Water"

### Olaf Hellmuth <sup>1,\*</sup> and Rainer Feistel <sup>2</sup>

- <sup>1</sup> Leibniz Institute for Tropospheric Research (TROPOS), Permoserstraße 15, D-04318 Leipzig, Germany
- <sup>2</sup> Leibniz Institute for Baltic Research (IOW), Seestraße 15, D-18119 Rostock-Warnemünde, Germany; rainer.feistel@io-warnemuende.de
- \* Correspondence: olaf.hellmuth@tropos.de

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### <sup>1</sup> Contents

- <sup>2</sup> SM-1 The Thermodynamic Equation Of Seawater 2010 (TEOS-10)
- 3 SM-2 On the Relevance of the Two-State Character of Subcooled Water for Ice Crystallization
- SM-3 IAPWS G12-15 Formulation for the Properties of Subcooled Water
- 5 SM-3.1 Equation of State
- 6 SM-3.2 Thermodynamic Properties
- 7 SM-3.3 Validity Range
- 8 SM-3.4 Constraints on the Numerical Solution of Equation (SM-3.8)
- SM-3.5 IAPWS G12-15 Thermodynamic Reference Values for the Check of the Correct
- 10 Computer Implementation
- <sup>11</sup> SM-4 Analytical Solution of a Cubic Equation
- 12 SM-5 Table Values of the Computer-Program Verification
- <sup>13</sup> SM-6 Table Values of the Deviations of the Analytical from the IAPWS G12-15 [1] Reference
- 14 Formulation
- 15 SM-7 Table Values of the Deviation of the Analytically from the Numerically Determined
- 16 Thermodynamic Properties of Subcooled Water
- 17 SM-7.1 Mass Density
- 18 SM-7.2 Thermal Expansivity
- 19 SM-7.3 Compressibility
- 20 SM-7.4 Isobaric Heat Capacity
- 21 SM-7.5 Sound Speed
- 22 SM-7.6 Gibbs Energy and Entropy
- 23 References

### <sup>24</sup> SM-1 The Thermodynamic Equation Of Seawater 2010 (TEOS-10)

<sup>25</sup> TEOS-10 is based on four independent thermodynamic potentials, defined as functions of the

<sup>26</sup> independent observables temperature, pressure, dry-air mass fraction, density, and salinity: (i) a

<sup>27</sup> Helmholtz function of fluid water (Wagner and Pruß [2], IAPWS R6-95 [3], known as "IAPWS-95"), (ii)

a Gibbs function of hexagonal ice (Feistel and Wagner [4], IAPWS R10-06 [5]), (iii) a Gibbs function 28 of seasalt dissolved in water (Feistel [67], IAPWS R13-08 [8]), and (iv) a Helmholtz function for dry 29 air (Lemmon et al. [9]). In combination with air-water cross-virial coefficients (Hyland and Wexler 30 [10], Harvey and Huang [11], Feistel *et al.* [12]) this set of thermodynamic potentials is used as the 31 primary standard for pure water (liquid, vapor, and solid), seawater and humid air from which all 32 other properties are derived by mathematical operations, i.e., without the need for additional empirical 33 functions. 34 The IAPWS-95 fluid-water formulation is based on the evaluation of a comprehensive and consistent data set which was assembled from a total of about 20,000 experimental data of water. 36 Wagner and Pruß [2] took into account all available information given in the scientific articles which 37 described the data collection underlying the development of the thermal equation of state of water. 38 The authors critically reexamined the available data sets with respect to their internal consistency and 39 their basic applicability for the development of a new equation of state for water. Only those data 40 were incorporated into the final nonlinear fitting procedure, which were judged to be of high quality. 41 These selected data sets took into account experimental data which were available by the middle of 42 the year 1994 (Wagner and Pruß [2]). The availability of reliable experimental data on subcooled liquid 43 water (i.e., metastable with respect to the solid form of water) was restricted to a few data sets for 44 several properties only along the isobar p=1013.25 hPa, which set the lower limit of the temperature 45 range for the validity of IAPWS-95 for liquid water (and so of TEOS-10) to T=236 K. This temperature is called the temperature of homogeneous ice nucleation (or homogeneous freezing temperature) at 47 p=1013.25 hPa and represents the lower limit below which it is very difficult to subcool water at this 48 pressure. The assessment of the accuracy of the IAPWS-95 formulation in the temperature range of 49 subcooled liquid water (Wagner and Pruß [2], Section 7.3.2 therein) revealed that TEOS-10 fully satisfies 50 the meteorological needs with respect to accuracy down to this temperature. The IAPWS-95 fluid-water 51 formulation is valid in the entire *stable* fluid region of  $H_2O$  from the melting-pressure curve to 1273 K 52 at pressures up to 1000 MPa; the lowest temperature on the melting-pressure curve is 251.165 K (at 53 208.566 MPa) (IAPWS R6-95 [3], Section 5 therein). In the stable fluid region, the formulation can also 54 be extrapolated beyond these limits. Based on a comparison with experimental data, the formulation 55 was reported to behave reasonably when extrapolated into the metastable regions, i.e., for superheated liquid at positive pressures (liquid-gas metastable region), and for subcooled liquid (solid-liquid

energy formulation, but some recent high-pressure data are not represented within their uncertainties 59

(IAPWS R6-95 [3], Section 5 therein). 60

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#### On the Relevance of the Two-State Character of Subcooled Water for Ice SM-2 61 Crystallization 62

metastable region). The available data were reported to be in fair agreement with the Helmholtz free

The two-state character of subcooled water has implications for ice crystallization which arise 63 from an empirical judgement of Ostwald [13] (pp. 306–309 therein), according to which "in the 64 course of transformation of an unstable (or metastable) state into a stable one the system does not go directly to the most stable conformation (corresponding to the modification with the lowest free energy) but prefers to reach intermediate stages (corresponding to other possible metastable modifications) having the closest 67 free energy difference to the initial state" (e.g., Schmelzer et al. [1415], Schmelzer [16], Schmelzer et al. 68 [17], Gutzow and Schmelzer [18], Schmelzer and Abyzov [19]). Later, this perception has become 69 70 known as Ostwald's rule of stages. However, with respect to phase transformation processes Schmelzer et al. [14] and Gutzow and Schmelzer [18] emphasized the existence of exceptions from this rule, 71 leading to the conclusion that Ostwald's rule of stages cannot be considered as a generally valid 72 thermodynamically founded law. This statement is in line with results from statistical mechanical 73 modelling of anisotropic nanoparticle crystallization carried out by Hedges and Whitelam [20], who 74 argued that although often upheld, the rule is without theoretical foundation and is not universally obeyed.

In advancing Ostwald's rule of stages Schmelzer *et al.* [15] (see also Schmelzer *et al.* [17], Gutzow 77 and Schmelzer [18], Schmelzer and Abyzov [19], Schmelzer et al. [21]) proposed its generalization as 78 follows: "In phase transformation processes, the structure and properties of the critical nucleus may differ 79 qualitatively from the properties both of the ambient and the newly evolving macrophases. Those classes of critical 80 clusters determine the process of the transformation which correspond to a minimum of the work of critical 81 cluster formation (as compared with all other possible alternative structures and compositions which may be 82 formed at the given thermodynamic constraints)." As emphasized by those authors, this generalization 83 implies - as in Ostwald's formulation - that critical clusters with quite different compositions may be formed but does not restrict these possible cluster states to structures and compositions essentially 85 determined by the evolving possibly stable or metastable macrophases. In Schmelzer et al. [15], [22], 86 [21], [17], the generalized Ostwald's rule of stages was employed as a well-founded principle for 87 a generalization of Gibbs' classical way of determination of the work of critical cluster formation 88 (Gibbs [23]), known as generalized Gibbs' theory. In the latter, as reference states for the determination 89 of the bulk contributions to the properties of the critical clusters, the authors did not choose the 90 quantities of the respective macrophase in equilibrium with the ambient phase; instead, they used 91 bulk contributions which correspond to the most appropriate structure and properties, i.e., to those 92 structures and properties which result in a minimum of the work of critical cluster formation. 93 Upon undercooling of water at sufficiently high pressure the character of the liquid changes 94 by transformation from a dense, high-entropic phase to a less dense, low-entropic (more ordered) 95 phase (Debenedetti and Stanley [24]). According to Ostwald's rule of stages, the low-entropic, more 96 ordered phase can be thought as an intermediate stage (corresponding to other possible metastable 97 modifications) having the closest free energy difference to the initial state. Following this perception, 98 new ice embryos are expectable to be more likely formed from the low-density water fraction B 99 rather than from the high-density fraction A. This would imply that the thermodynamic driving 100 force of ice crystallization (see, e.g., Hellmuth et al. [25]) should be scaled in terms of the difference 101  $\Delta G^{\rm B}_{\beta\alpha} = G^{\rm B}_{\beta}(T,p) - G_{\alpha}(T,p)$  between the Gibbs energies of low-density water B (represented by 102  $G^{\rm B}_{\beta}(T,p)$  with subscript  $\beta$  for subcooled water) and ice (represented by  $G_{\alpha}(T,p)$  with subscript  $\alpha$  for 103 ice) rather than in terms of the difference  $\Delta G_{\beta\alpha} = G_{\beta}(T, p, x) - G_{\alpha}(T, p)$  between mean-state water 104 (represented by  $G_{\beta}(T, p, x)$ ) and ice. Such perception of heterogeneity has some conceptual similarity 105 to that employed in Abyzov et al. [26], who assumed an increase of the average size of the "structural 106 units" of the maternal phase with decreasing temperature. This structural coarsening is identified 107 with the cooperatively rearranging regions in the liquids, the increase of which is a consequence of a 108 more complex kinetics as compared to a quasi-one-component description of the liquid commonly 109 employed in classical nucleation theory. As a consequence, crystal nucleation in glass-forming liquids 110 is assumed to proceed with detectable rates only in the liquid-like (soft) regions and to be suppressed 111 in solid-like (rigid) parts of the liquid. In their model, the fraction of liquid-like and solid-like regions 112 in dependence on temperature serves as a closure parameter, determined to achieve a comprehensive 113 agreement between classical nucleation theory and experiment not only at relatively high temperatures 114 but also at temperatures lower than that of the nucleation rate maximum. 115

An implication of these considerations is the determination of the nucleation rate as a mean value. Owing to the nonlinear dependence of the nucleation rate coefficient on temperature and pressure, the nucleation rate coefficient at mean-state conditions, J, differs from the mean-state nucleation rate coefficient,  $\overline{J}$ , tentatively defined by the following mixing rule:

$$J(\Delta G_{\beta\alpha}) \neq \bar{J} \approx \underbrace{xJ(\Delta G_{\beta\alpha}^{B})}_{\text{from structure B}} + \underbrace{(1-x)J(\Delta G_{\beta\alpha}^{A})}_{\text{from structure A}},$$
  

$$\Delta G_{\beta\alpha} = G_{\beta}(T, p, x) - G_{\alpha}(T, p),$$
  

$$\Delta G_{\beta\alpha}^{A} = G_{\beta}^{A}(T, p) - G_{\alpha}(T, p),$$
  

$$\Delta G_{\beta\alpha}^{B} = G_{\beta}^{B}(T, p) - G_{\alpha}(T, p).$$

The quantification of the differences  $\Delta J_1 = J(\Delta G^B_{\beta\alpha}) - J(\Delta G_{\beta\alpha})$  and  $\Delta J_2 = J(\Delta G_{\beta\alpha}) - \overline{J}$  is, however, beyond the scope of the present analysis.

### <sup>118</sup> SM-3 IAPWS G12-15 Formulation for the Properties of Subcooled Water

### 119 SM-3.1 Equation of State

The EoS according to the IAPWS G12-15 [1] formulation (Equation (1) therein) is given by the dimensionless Gibbs energy  $\psi$  as function of temperature *T* and pressure *p*:

$$\psi(T,p) = \frac{\widehat{g}(T,p)}{R_{\rm W}T_{\rm LL}}$$

$$= \psi^{\rm r}(\tau,\pi) + (\tau+1) \left[ x_{\rm e}L(\tau,\pi) + x_{\rm e}\ln x_{\rm e} + (1-x_{\rm e})\ln(1-x_{\rm e}) + \omega(\pi)x_{\rm e}(1-x_{\rm e}) \right].$$
(SM-3.1)

Here,  $\hat{g}(T, p)$  denotes the specific Gibbs energy of subcooled water. The quantity  $x_e$  is the equilibrium mole fraction of the low-density structure of water in the two-state water mixture, and serves as a determinable parameter of the EoS. The other quantities are the temperature of the liquid-liquid critical point  $T_{LL}$ , the specific gas constant of water  $R_W$ , the dimensionless function of the ordering field L, the dimensionless interaction parameter  $\omega$ , and the reduced temperature  $\tau$  and the reduced pressure  $\pi$  defined as (IAPWS G12-15 [1], Equation (2) therein):

$$\tau = \frac{T}{T_{\rm LL}} - 1, \quad \pi = \frac{p}{\hat{\varrho}_0 R_{\rm W} T_{\rm LL}}.$$
(SM-3.2)

The quantity  $\hat{\varrho}_0$  is the reference mass density of subcooled water. The values of  $T_{LL}$ ,  $\hat{\varrho}_0$ , and  $R_W$  are given in Table SM-3.1.1. The dimensionless background Gibbs energy  $\psi^r$  reads (IAPWS G12-15 [1], Equation (3) therein):

$$\psi^{\mathbf{r}}(\tau,\pi) = \sum_{i=1}^{20} c_i (\tau+1)^{a_i} (\pi+\pi_0)^{b_i} \exp\left[-d_i (\pi+\pi_0)\right] \,. \tag{SM-3.3}$$

The reference dimensionless pressure  $\pi_0$  is defined by

$$\pi_0 = \frac{p_0}{\widehat{\varrho}_0 R_W T_{LL}} , \qquad (SM-3.4)$$

with  $p_0$  given in Table SM-3.1.1. The coefficients  $a_i$ ,  $b_i$ , and  $c_i$  are presented in Table SM-3.1.2. The order field  $L(\tau, \pi)$  is defined by the following relations (IAPWS G12-15 [1], Equations (4) and (5) therein):

$$L(\tau, \pi) = L_0 \left(\frac{K_2}{2k_1k_2}\right) \left[1 + k_0k_2 + k_1(\pi + k_2\tau) - K_1(\tau, \pi))\right],$$
  

$$K_1(\tau, \pi) = \sqrt{\left[1 + k_0k_2 + k_1(\pi - k_2\tau)\right]^2 - 4k_0k_1k_2(\pi - k_2\tau)},$$
  

$$K_2 = \sqrt{1 + k_2^2}.$$
(SM-3.5)

The values of  $L_0$ ,  $k_0$ ,  $k_1$ , and  $k_2$  are given in Table SM-3.1.1. The quantity  $\omega$  denotes the interaction parameter, which depends linearly on pressure (IAPWS G12-15 [1], Equation (6) therein):

$$\omega(\pi) = 2 + \omega_0 \pi \,. \tag{SM-3.6}$$

The reference parameter  $\omega_0$  is given in Table SM-3.1.1. The equilibrium mole fraction of the low-density structure of water is a function of temperature and pressure,  $x_e = x_e(T, p)$ , which is determined by minimizing the Gibbs energy in dependence on  $x_e$  at isothermal and isobaric conditions (IAPWS G12-15 [1], Equation (7) therein):

$$\left(\frac{\partial\psi(T,p,x)}{\partial x}\right)_{T,p} = 0.$$
 (SM-3.7)

Parameter Unit Value Parameter Value 0.521 226 9  $300 \times 10^{6}$ Ра  $\omega_0$  $p_0$ 0.763 179 54 228.2 Κ  $L_0$  $T_{LL}$  $\,kg\,m^{-3}$  $k_0$ 0.072 158 686 1081.6482  $\widehat{\varrho}_0$  $J \, \mathrm{kg}^{-1} \, \mathrm{K}^{-1}$  $k_1$ -0.31569232 $R_{W}$ 461.523 087  $k_2$ 5.299 260 8

**Table SM-3.1.1.** Parameter values for the equation of state given by Equations (SM-3.1)–(SM-3.8). Taken from IAPWS G12-15 [1] (Table 1 therein).

**Table SM-3.1.2.** Parameter values for the dimensionless regular background Gibbs energy  $\psi^{r}$  in Equation (SM-3.3). Taken from IAPWS G12-15 [1] (Table 2 therein).

i	Ci	a <sub>i</sub>	b <sub>i</sub>	$d_i$
1	$-8.1570681381655{ imes}10^{0}$	0	0	0
2	$1.2875032\! imes\!10^{0}$	0	1	0
3	$7.0901673598012{\times}10^{0}$	1	0	0
4	$-3.2779161 imes10^{-2}$	-0.2555	2.1051	-0.0016
5	$7.3703949{ imes}10^{-1}$	1.5762	1.1422	0.6894
6	$-2.1628622{ imes}10^{-1}$	1.6400	0.9510	0.0130
7	$-5.1782479{ imes}10^{0}$	3.6385	0	0.0002
8	$4.2293517{ imes}10^{-4}$	-0.3828	3.6402	0.0435
9	$2.3592109{ imes}10^{-2}$	1.6219	2.0760	0.0500
10	$4.3773754{ imes}10^{0}$	4.3287	-0.0016	0.0004
11	$-2.9967770 \times 10^{-3}$	3.4763	2.2769	0.0528
12	$-9.6558018{ imes}10^{-1}$	5.1556	0.0008	0.0147
13	$3.7595286 \times 10^{0}$	-0.3593	0.3706	0.8584
14	$1.2632441\! imes\!10^{0}$	5.0361	-0.3975	0.9924
15	$2.8542697{ imes}10^{-1}$	2.9786	2.9730	1.0041
16	$-8.5994947{ imes}10^{-1}$	6.2373	-0.3180	1.0961
17	$-3.2916153{ imes}10^{-1}$	4.0460	2.9805	1.0228
18	$9.0019616{ imes}10^{-2}$	5.3558	2.9265	1.0303
19	$8.1149726{ imes}10^{-2}$	9.0157	0.4456	1.6180
20	$-3.2788213{ imes}10^{0}$	1.2194	0.1298	0.5213

Evaluation of Equation (SM-3.7) with  $\psi(T, p, x_e)$  from Equation (SM-3.1) leads to the following transcendental equation  $\mathcal{F}(x_e)=0$ , the numerical root of which yields the sought-after value of  $x_e$  (IAPWS G12-15 [1], Equation (8) therein):

$$\mathcal{F}(x_{\rm e}) = L(\tau, \pi) + \ln\left(\frac{x_{\rm e}}{1 - x_{\rm e}}\right) + \omega(\pi)(1 - 2x_{\rm e}) = 0.$$
 (SM-3.8)

120

### <sup>121</sup> SM-3.2 Thermodynamic Properties

According to IAPWS G12-15 [1] (Equations (12)–(17) and Table 3 therein) the thermodynamic properties can be derived from the derivatives of  $\psi(T, p)$  at the equilibrium mole fraction  $x_e$ . As a matter of convenience the corresponding dependencies are expressed in terms of the order parameter  $\phi$  and the susceptibility  $\chi$  (IAPWS G12-15 [1], Equation (12) therein):

$$\phi(x_{\rm e}) = 2x_{\rm e} - 1$$
,  $\chi(\pi, x_{\rm e}) = \left(\frac{2}{1 - (\phi(x_{\rm e}))^2} - \omega(\pi)\right)^{-1}$ . (SM-3.9)

**Table SM-3.2.1.** Derivatives of  $L(\tau, \pi)$  and  $\psi^{r}(\tau, \pi)$ . To simplify the annotation of the derivatives of  $\psi^{r}$  (right column), the following shorthand definitions are used:  $\overline{\tau} = \tau + 1$  and  $\overline{\pi} = \pi + \pi_{0}$ . Taken from IAPWS G12-15 [1] (Table 3 therein).

Derivatives of L	Derivatives of $\psi^{r}$
$L_{\tau} = \frac{L_0 K_2}{2} \left( 1 + \frac{1 - k_0 k_2 + k_1 (\pi - k_2 \tau)}{K_1} \right)$	$\psi^{ m r}_{ au} = \sum_{i=1}^{20} c_i a_i \overline{ au}^{a_i-1} \overline{\pi}^{b_i} e^{-d_i \overline{\pi}}$
$L_{\pi} = \frac{L_0 K_2 (K_1 + k_0 k_2 - k_1 \pi + k_1 k_2 \tau - 1)}{2k_2 K_1}$	$\psi^{\mathbf{r}}_{\pi} = \sum_{i=1}^{20} c_i \overline{\pi}^{a_i} \overline{\pi}^{b_i - 1} (b_i - d_i \overline{\pi}) e^{-d_i \overline{\pi}}$
$L_{\tau\tau} = -\frac{2L_0K_2k_0k_1k_2^2}{K_1^3}$	$\psi^{\mathbf{r}}_{ au au} = \sum_{i=1}^{20} c_i a_i (a_i - 1) \overline{ au}^{a_i - 2} \overline{\pi}^{b_i} e^{-d_i \overline{\pi}}$
$L_{\tau\pi} = \frac{2L_0K_2k_0k_1k_2}{K_1^3}$	$\psi^{\mathbf{r}}_{ au\pi} = \sum_{i=1}^{20} c_i a_i \overline{ au}^{a_i-1} \overline{\pi}^{b_i-1} (b_i - d_i \overline{\pi}) e^{-d_i \overline{\pi}}$
$L_{\pi\pi} = -\frac{2L_0 K_2 k_0 k_1}{K_1^3}$	$\psi_{\pi\pi}^{\mathbf{r}} = \sum_{i=1}^{20} c_i \overline{\tau}^{a_i} \overline{\pi}^{b_i - 2} \Big[ (d_i \overline{\pi} - b_i)^2 - b_i \Big] e^{-d_i \overline{\pi}}$

- In the following equations, the subscripts  $\tau$  and  $\pi$  indicate partial derivatives with respect to the subscripted quantities  $\tau$  and  $\pi$ . Expressions for the derivatives of  $L(\tau, \pi)$  and  $\psi^{r}(\tau, \pi)$  with respect to  $\tau$  and  $\pi$  are presented in Table SM-3.2.1. As the equilibrium value of  $x_{e}$  is defined by Equation (SM 3.7) it is considered a function of  $\tau$  and  $\pi$
- (SM-3.7), it is considered a function of  $\tau$  and  $\pi$ .

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1. Specific volume  $\hat{v}=1/\hat{\varrho}$  (with  $\hat{\varrho}$  denoting the mass density) (IAPWS G12-15 [1], Equation (13) therein):

$$\widehat{v}(\tau,\pi) = \frac{1}{\widehat{\varrho}_0(\tau,\pi)} \left\{ \frac{\tau+1}{2} \left[ \frac{\omega_0}{2} \left( 1 - \phi^2(x_e) \right) + L_{\pi}(\tau,\pi) \left( \phi(x_e) + 1 \right) \right] + \psi_{\pi}^{\mathbf{r}}(\tau,\pi) \right\}.$$
(SM-3.10)

2. Specific entropy  $\hat{s}$  (IAPWS G12-15 [1], Equation (14) therein):

$$\begin{split} \widehat{s}(\tau,\pi) &= -R_{\rm W} \Biggl\{ \frac{(\tau+1)L_{\tau}(\tau,\pi)}{2} \Biggl( \phi(x_{\rm e}) + 1 \Biggr) \\ &+ \Biggl[ x_{\rm e}L(\tau,\pi) + x_{\rm e}\ln x_{\rm e} + (1-x_{\rm e})\ln(1-x_{\rm e}) + \omega(\pi)x_{\rm e}(1-x_{\rm e}) \Biggr] + \psi_{\tau}^{\rm r}(\tau,\pi) \Biggr\} \,. \end{split}$$
(SM-3.11)

3. Isothermal compressibility,  $\kappa_T$ , thermal expansion coefficient,  $\alpha_p$ , specific isobaric heat capacity,  $\hat{c}_p$  (IAPWS G12-15 [1], Equation (15) therein):

$$\kappa_T(\tau,\pi) = \frac{\widehat{\varrho}(\tau,\pi)}{\widehat{\varrho}_0^2 R_W T_{LL}} \left\{ \frac{\tau+1}{2} \left[ \chi \left( L_\pi(\tau,\pi) - \omega_0 \phi(x_e) \right)^2 - \left( \phi(x_e) + 1 \right) L_{\pi\pi}(\tau,\pi) \right] - \psi_{\pi\pi}^{\mathrm{r}}(\tau,\pi) \right\},$$

$$\begin{split} \alpha_{p}(\tau,\pi) &= \frac{\widehat{\varrho}(\tau,\pi)}{\widehat{\varrho}_{0}R_{W}T_{LL}} \Biggl\{ \frac{L_{\tau\pi}(\tau,\pi)}{2}(\tau+1) \Bigl( \phi(x_{e})+1 \Bigr) \\ &+ \frac{1}{2} \Biggl[ \frac{\omega_{0}\left(1-\phi^{2}(x_{e})\right)}{2} + L_{\pi}(\tau,\pi) \Bigl( \phi(x_{e})+1 \Bigr) \Biggr] \\ &- \frac{(\tau+1)L_{\tau}(\tau,\pi)}{2} \chi \Bigl( L_{\pi}(\tau,\pi) - \omega_{0}\phi(x_{e}) \Bigr) + \psi_{\tau\pi}^{r}(\tau,\pi) \Biggr\} , \end{split}$$
(SM-3.12)  
$$\widehat{c}_{p}(\tau,\pi) &= -R_{W}(\tau+1) \Biggl\{ L_{\tau}(\tau,\pi) \Bigl( \phi(x_{e})+1 \Bigr) \\ &+ \frac{1}{2} (\tau+1) \Biggl[ L_{\tau\tau}(\tau,\pi) \Bigl( \phi(x_{e})+1 \Bigr) - (L_{\tau}(\tau,\pi))^{2} \chi \Biggr] + \psi_{\tau\tau}^{r}(\tau,\pi) \Biggr\} . \end{split}$$

4. Specific isochoric heat capacity,  $\hat{c}_v$  (IAPWS G12-15 [1], Equation (16) therein):

$$\widehat{c}_{v}(\tau,\pi) = \widehat{c}_{p}(\tau,\pi) - \frac{T(\alpha_{p}(\tau,\pi))^{2}}{\widehat{\varrho}(\tau,\pi)\kappa_{T}(\tau,\pi)} .$$
(SM-3.13)

5. Speed of sound, *w* (IAPWS G12-15 [1], Equation (17) therein):

$$w(\tau,\pi) = \left[\widehat{\varrho}(\tau,\pi)\kappa_T(\tau,\pi)\frac{\widehat{c}_v(\tau,\pi)}{\widehat{c}_p(\tau,\pi)}\right]^{-1/2}$$
  
= 
$$\left[\widehat{\varrho}(\tau,\pi)\kappa_T(\tau,\pi) - \frac{T(\alpha_p(\tau,\pi))^2}{\widehat{c}_p(\tau,\pi)}\right]^{-1/2}.$$
 (SM-3.14)

### 126 SM-3.3 Validity Range

The EoS of subcooled water given by Equations (SM-3.1)–(SM-3.14) is valid for metastable liquid water from the homogeneous ice nucleation temperature,  $T_{\rm H}(p)$ , to the melting temperature,  $T_{\rm M}(p)$ , at pressures in the interval  $0 \le p \le 400$  MPa:

$$T_{
m H}(p) \leq T \leq T_{
m M}(p)$$
 ,  $0 \leq p \leq 400 \, {
m MPa}$  .

The equation remains also valid for stable liquid states up to 300 K in the same pressure range, where IAPWS-95 remains the recommended formulation, and behaves reasonably when extrapolated to 1000 MPa. The homogeneous-ice nucleation curve can be approximated by the fits given in Equations (SM-3.15) and (SM-3.16) (IAPWS G12-15 [1], Equations (18) and (19) therein):

$$\frac{p_{\rm H}}{\rm MPa} = 0.1 + 228.27 \left(1 - \theta^{6.243}\right) + 15.724 \left(1 - \theta^{79.81}\right) , \qquad (SM-3.15)$$
  
$$\theta = T/235.15 {\rm K} , 0 {\rm MPa} \le p \le 198.9 {\rm MPa} ,$$

$$\frac{T_{\rm H}}{\rm K} = 172.82 + 0.03718 \left(\frac{p}{\rm MPa}\right) + 3.403 \times 10^{-5} \left(\frac{p}{\rm MPa}\right)^2$$

$$-1.573 \times 10^{-8} \left(\frac{p}{\rm MPa}\right)^3 , 198.9 \,\rm MPa \le p \le 1500 \,\rm MPa \,.$$
(SM-3.16)

The slope of the ice-nucleation curve exhibits a discontinuity at the break point  $(T_{BP}, p_{BP}) =$  (181.4 K, 198.9 MPa). At this point both curves intersect. Equation (SM-3.15) should be used for pressures  $p < p_{BP}$ , and Equation (SM-3.16) for pressures  $p_{BP} < p$ .

**Table SM-3.3.1.** Regression coefficients  $a_k$ ,  $n_k$  for  $p_M(T)$ , Equation (SM-3.17), and  $b_k$  for the  $T_M(p)$ , Equation (SM-3.18). Taken from Feistel [27].

	$p_{\mathbf{M}}(T)$ , Equation (	SM-3.17)	$T_{\rm M}(p)$ , Equation (SM-3.18)
k	a <sub>k</sub>	n <sub>k</sub>	$b_{\mathbf{k}}$
1	$0.119539337\cdot10^7$	3	$-1.66356104484551{\cdot}10^{-7}$
2	$0.808183159\cdot10^5$	25.75	$-2.13519241979406\cdot10^{-13}$
3	$0.333826860\cdot10^4$	103.75	$3.52967405341877\cdot10^{-20}$
4			$-2.73184525236281\cdot10^{-26}$

**Table SM-3.4.1.** Subintervals for the numerical determination of the equilibrium mole fraction of low-density water,  $x_e$ , in dependence on  $L(\tau, \pi)$  and  $\omega(\pi)$ . The "min" function returns the smallest value of its arguments. Taken from IAPWS G12-15 [1] (Table 4 therein).

$\omega$ interval	x <sub>e</sub>	subinterval
	Lower bound	Upper bound
$\omega < \frac{10}{9} [\ln(19) - L]$	0.049	0.5
$\frac{10}{9}[\ln(19) - L] \le \omega < \frac{50}{49}[\ln(99) - L]$	0.0099	0.051
$\frac{50}{49}[\ln(99) - L] \le \omega$	$0.99 \exp\left[-\frac{50L}{49} - \omega\right]$	$\min\left[1.1\exp(-L-\omega),0.0101\right]$

To complete the specification of the validity range of the EoS, here we include also the determination of the melting curve, which is not part of the IAPWS G12-15 [1] formulation. The correlation equation for the melting pressure was developed by Wagner (2006) (cited in Feistel [27], Appendix 1 therein) on the base of the guidelines IAPWS [28] and IAPWS [29] and deviates from the melting curve less than its predecessor published in Wagner and Pruß [2] (Equation (2.16) therein):

$$\frac{p_{\rm M} - p_{\rm TP}}{p_{\rm TP}} = \sum_{\rm k=1}^{3} a_{\rm k} \left[ 1 - \left( \frac{T}{T_{\rm TP}} \right)^{n_{\rm k}} \right] , \quad T_{\rm TP} = 273.16 \,\rm K \,, \quad p_{\rm TP} = 611.657 \,\rm Pa \,. \qquad (SM-3.17)$$

Here,  $T_{\text{TP}}$  and  $p_{\text{TP}}$  denote the temperature and pressure of the triple point. The correlation equation for the melting temperature was developed by Feistel [27] (Appendix 2 therein) also on the base of the guidelines IAPWS [28] and IAPWS [29] and deviates from the melting curve significantly less than its predecessor:

$$\frac{T_{\rm M} - T_{\rm TP}}{T_{\rm TP}} = \sum_{\rm k=1}^{4} b_{\rm k} \left[ \frac{p - p_{\rm TP}}{p_{\rm TP}} \right]^{\rm k} .$$
(SM-3.18)

<sup>130</sup> The regression coefficients  $a_k$ ,  $n_k$  and  $b_k$  are presented in Table SM-3.3.1.

### 131 SM-3.4 Constraints on the Numerical Solution of Equation (SM-3.8)

The numerical solution of Equation (SM-3.8) delivers the equilibrium mole fraction of low-density water, which is located in the interval  $0 < x_e < 1$ . Depending on the values of  $L(\tau, \pi)$  and  $\omega(\pi)$ , IAPWS G12-15 [1] (Table 4 therein) distinguished three different subintervals, defined by lower and upper limits of the sought-after equilibrium value of  $x_e$ , which are presented in Table SM-3.4.1.

# SM-3.5 IAPWS G12-15 Thermodynamic Reference Values for the Check of the Correct Computer Implementation

IAPWS G12-15 [1] (Table 5 therein) provides reference values for the check of the correct implementation of the EoS calculus. These values are listed in Table SM-3.5.1. In order to reproduce these table values to the number of given digits, the mole fraction  $x_e$  should be numerically determined with a resolution of  $10^{-10}$ .

kg 999.8	$\frac{\widehat{\varrho}}{\mathrm{m}^{-3}}$ 42.29	$\frac{\alpha_p}{10^{-4}\mathrm{K}^{-1}} \\ -0.683042$	$\frac{\kappa_T}{10^{-4} \mathrm{MPa}^{-1}}$ 5.088499	$\frac{\widehat{c}_p}{j\mathrm{kg}^{-1}\mathrm{K}^{-1}}$	$\frac{w}{\frac{\mathrm{ms^{-1}}}{\mathrm{1402.3886}}}$	<i>x</i> 0.096 654 715 5	L 0.621 204 74
968.0999	6	-29.633816	11.580785	5 997.563 2	1134.5855	0.2551028587	0.091 763 68
090.4567	5	3.267 768	3.361311	3708.3902	1668.2020	0.0304292667	0.72377081
185.028 0	0	6.716009	2.567 237	3338.5250	1899.3294	0.0071700809	1.1553965
(151.71517		4.929927	2.277 029	3757.2144	2015.8782	0.0053588366	1.4345145

Table SM-3.5.1. Thermodynamic reference values for check of the correct computer implementation. Taken from IAPWS G12-15 [1] (Table 5 therein).

### <sup>142</sup> SM-4 Analytical Solution of a Cubic Equation

Starting point of the analytical solution is the following general form of the cubic equation:

$$Ax^{3} + Bx^{2} + Cx + D = 0$$
,  $x \in \mathbb{C}$ ;  $A, B, C \in \mathbb{R}$ . (SM-4.1)

Here, *x* denotes the sought-after root of the equation, which is element of the complex numbers. The parameters *A*, *B*, *C*, and *D* are real numbers. Equation (SM-4.1) can be solved by means of *Cardano's method*, the rationale of which can be found, e.g., in Gellert *et al.* [30] (pp. 104–207 therein). Employing the transformations

$$r=rac{B}{A}$$
,  $s=rac{C}{A}$ ,  $t=rac{D}{A}$ ,  $A 
eq 0$ ,

one arrives at the normal form of the cubic equation:

$$x^{3} + rx^{2} + sx + t = 0$$
,  $x \in \mathbb{C}$ ;  $r, s, t \in \mathbb{R}$ . (SM-4.2)

In the set of complex numbers, each cubic equation has three solutions, which can coincide. One of these solutions is real, the other two are either real too or conjugate complex. According to Cardano's formula, the application of the transformation

$$x = y - \frac{r}{3} \tag{SM-4.3}$$

to the normal form yields the reduced form, in which the quadratic term is absent:

$$y^{3} + py + q = 0$$
,  $p = s - \frac{r^{2}}{3}$ ,  $q = \frac{2r^{3}}{27} - \frac{sr}{3} + t$ . (SM-4.4)

For the sought-after solution *y* the following ansatz is used:

$$y = u + v$$
.

This ansatz results in the following equation:

$$(u+v)^3 + p(u+v) + q = 0$$
 or, equivalently  $u^3 + v^3 + q + (u+v)(3uv + p) = 0$ .

This is one equation for the two unknown variables u and v. To satisfy the remaining degree of freedom, a side condition is employed which removes the term (u + v)(3uv + p):

$$3uv + p = 0$$
.

Therewith, one obtains the following two equations for the determination of u and v:

$$u^3 + v^3 = -q \quad \rightsquigarrow \text{ quadratization} \rightsquigarrow \quad u^6 + 2u^3v^3 + v^6 = q^2 , \quad (SM-4.5)$$

$$uv = -\frac{p}{3} \quad \rightsquigarrow \text{ four times the third power } \quad 4u^3v^3 = -4\left(\frac{p}{3}\right)^3$$
. (SM-4.6)

Subtraction of Equation (SM-4.6) from Equation (SM-4.5) yields:

$$(u^{3} - v^{3})^{2} = q^{2} + 4\left(\frac{p}{3}\right)^{3} = 4\underbrace{\left[\left(\frac{q}{2}\right)^{2} + \left(\frac{p}{3}\right)^{3}\right]}_{=\Delta} \quad \rightsquigarrow \quad u^{3} - v^{3} = \pm 2\sqrt{\Delta}.$$
 (SM-4.7)

Combining the first form in Equation (SM-4.5) with the second form in Equation (SM-4.7),

$$u^3+v^3=-q$$
 ,  $u^3-v^3=\pm 2\sqrt{\Delta}$  ,

one arrives at the following solutions for u and v:

$$u^{3} = -\frac{q}{2} \pm \sqrt{\Delta} , \quad v^{3} = -\frac{q}{2} \mp \sqrt{\Delta} .$$
 (SM-4.8)

<sup>143</sup> Upon interchanging the upper signs in front of the roots with the lower ones the quantity  $u^3$  migrates <sup>144</sup> to  $v^3$ , while the equations  $u^3 + v^3 + q = 0$  and uv = -p/3 remain unchanged. Therefore it is sufficient, <sup>145</sup> to consider only one pair of signs, e.g., the upper one.

Each third root of a complex number has three values; next to  $x_1$  there are two further solutions  $x_2$  and  $x_3$  with

$$x_2 = \varepsilon_2 x_1$$
,  $x_3 = \varepsilon_3 x_1$ ,  $\varepsilon_2 = \frac{1}{2} \left( -1 + i\sqrt{3} \right)$ ,  $\varepsilon_3 = \frac{1}{2} \left( -1 - i\sqrt{3} \right)$ .

Therewith, one obtains the following solutions for *u* and *v*:

$$u_{1} = \sqrt[3]{-\frac{q}{2} + \sqrt{\Delta}}, \quad u_{2} = \varepsilon_{2}u_{1}, \quad u_{3} = \varepsilon_{3}u_{1},$$
  

$$v_{1} = \sqrt[3]{-\frac{q}{2} - \sqrt{\Delta}}, \quad v_{2} = \varepsilon_{2}v_{1}, \quad v_{3} = \varepsilon_{3}v_{1}.$$
(SM-4.9)

For  $y = u_i + v_j$  with i = 1, 2, 3 and j = 1, 2, 3 one would obtain nine solutions of the cubic equation. However, the number of solutions reduces to the following three only,

$$y_1 = u_1 + v_1$$
,  $y_2 = u_2 + v_3$ ,  $y_3 = u_3 + v_2$ ,

because the side constraint  $u_i v_i = -p/3$  is fulfilled only for  $u_1 v_1$ ,  $u_2 v_3$  and  $u_3 v_2$  by virtue of

$$\varepsilon_2 \varepsilon_3 = \frac{1}{2} \left( -1 + i\sqrt{3} \right) \cdot \frac{1}{2} \left( -1 - i\sqrt{3} \right) = \frac{1}{4} (1+3) = 1.$$

Presuming that the radicand of the square root is nonnegative,

$$\Delta = \left(\frac{q}{2}\right)^2 + \left(\frac{p}{3}\right)^3 \ge 0 ,$$

the solution  $y_1$  is real,

$$y_1 = u_1 + v_1 = \sqrt[3]{-\frac{q}{2} + \sqrt{\Delta}} + \sqrt[3]{-\frac{q}{2} - \sqrt{\Delta}},$$
 (SM-4.10)

while  $y_2$  and  $y_3$  are conjugate complex, as can be seen below:

$$y_{2} = u_{2} + v_{3} = u_{1}\varepsilon_{2} + v_{1}\varepsilon_{3} = -\frac{1}{2}(u_{1} + v_{1}) + \left[\frac{1}{2}(u_{1} - v_{1})\right] \cdot i\sqrt{3} ,$$
  

$$y_{3} = u_{3} + v_{2} = u_{1}\varepsilon_{3} + v_{1}\varepsilon_{2} = -\frac{1}{2}(u_{1} + v_{1}) - \left[\frac{1}{2}(u_{1} - v_{1})\right] \cdot i\sqrt{3} .$$
(SM-4.11)

<sup>146</sup> The solution given by Equation (SM-4.10) is known as Cardano's formula.

For the case that the radicand of the square root is negative ("casus irreducibilis"),

$$\Delta = \left(rac{q}{2}
ight)^2 + \left(rac{p}{3}
ight)^3 < 0$$
 ,

there exist three real trigonometric solutions for y in Equation(SM-4.3). Introducing the auxiliary variables

$$r_0 = \sqrt{-\left(rac{p}{3}
ight)^3}$$
,  $\cos arphi = -rac{q}{2\sqrt{-\left(rac{p}{3}
ight)^3}}$ ,

these three real solutions read:

$$y_1 = 2\sqrt[3]{r_0} \cos\left(\frac{\varphi}{3}\right),$$
  

$$y_2 = 2\sqrt[3]{r_0} \cos\left(\frac{\varphi}{3} + \frac{2\pi}{3}\right),$$
  

$$y_3 = 2\sqrt[3]{r_0} \cos\left(\frac{\varphi}{3} + \frac{4\pi}{3}\right).$$
(SM-4.12)

The back transformation from the solutions of the reduced form,  $y_i$ , to the solutions of the normal form,  $x_i$ , is carried out using Equation (SM-4.3).

therein) from the IAPWS G12-15 [1] reference values (subscript \*, Table SM-3.5.1). Integer n denotes the number of equally spaced segments of the root interval of x<sub>e</sub>. coefficient  $\alpha_p$ , isothermal compressibility  $\kappa_T$ , isobaric heat capacity  $c_p$ , speed of sound w, equilibrium mole fraction of low-density water,  $x_e$ , and the ordering field L using the root finder of Press *et al.* [31] (Section 9.1) Relative deviations are given in parts per billion (ppb). Bold-styled values denote extrema.

$L - L_{\star}$	$L_{\star}$		-4.24	-45.23	-3.61	-29.13	-11.59																		
$x_{\rm e} - x_{\rm e\star}$	$x_{e,\star}$		0.65	0.0	1.14	3.32	3.30		-12.53	-3.28	-5.46	3.62	3.40		-35.71	57.56	13.32	6.35	0.93		-269.00	-561.33	-54.21	-50.74	61.19
$\frac{w-w}{w}$	*m		-25.29	-29.12	-21.75	-0.18	-20.41		-21.20	-29.00	-19.60	-0.23	-20.42		-14.01	31.16	-25.73	-0.65	-20.12		58.32	-9.13	-3.70	8.11	-27.61
$\widehat{c}_p - \widehat{c}_{p,\star}$	$\widehat{c}_{p,\star}$		-7.36	8.01	-10.95	-7.67	9.59	-	-10.15	3.03	-10.98	-7.67	9.58		-15.04	92.79	-10.90	-7.67	9.59		-64.31	-820.26	-11.19	-7.54	9.46
$\kappa_T - \kappa_{T,\star}$	$\kappa_{T,\star}$	$\mathbf{n} = 10^9$	91.40	34.53	-45.28	-135.49	109.62	$n = 10^{8}$	82.11	29.06	-49.39	-135.41	109.65	$\mathbf{n} = 10^7$	65.78	127.69	-37.68	-134.63	109.08	$n = 10^{6}$	-98.61	-875.69	-79.81	-150.79	122.99
$\alpha_p - \alpha_{p,\star}$	$10^{-4}{ m K}^{-1}$		$-0.49.10^{-6}$	$-0.28 \cdot 10^{-6}$	$0.11 \cdot 10^{-6}$	$-0.42 \cdot 10^{-6}$	$0.31.10^{-6}$		$-0.31 \cdot 10^{-6}$	$0.36 \cdot 10^{-7}$	$0.14.10^{-6}$	$-0.42 \cdot 10^{-6}$	$0.31 \cdot 10^{-6}$		$0.93.10^{-8}$	$-0.56 \cdot 10^{-5}$	$0.70 \cdot 10^{-7}$	$-0.42 \cdot 10^{-6}$	$0.31 \cdot 10^{-6}$		$0.32.10^{-5}$	$0.52 \cdot 10^{-4}$	$0.31 \cdot 10^{-6}$	$-0.41 \cdot 10^{-6}$	$0.29.10^{-6}$
$\widehat{\varrho} - \widehat{\varrho_{\star}}$	$\hat{o}^{\star}_{\star}$		1.40	-3.23	-1.88	-2.64	2.32		2.21	-2.87	-1.70	-2.64	2.32		3.63	-9.44	-2.21	-2.66	2.33		17.92	57.40	-0.37	-2.23	1.95
d	MPa		0.101325	0.101325	200	400	400		0.101325	0.101325	200	400	400		0.101325	0.101325	200	400	400		0.101325	0.101325	200	400	400
T	Х		273.15	235.15	250	200	250		273.15	235.15	250	200	250		273.15	235.15	250	200	250		273.15	235.15	250	200	250

F	n	$\dot{v} = \dot{v}$	$\alpha_n-lpha_{n+1}$	<i>κ</i> π – <i>κ</i> π ,	$\widehat{C}_n - \widehat{C}_n +$	-m	$\chi_{2} = \chi_{21}$	$I_{i} - I_{i+1}$
	$\frac{r}{MPa}$	$\frac{\alpha}{\hat{\varrho}_{\star}}$	$\frac{10-4}{10-4}$ K <sup>-1</sup>	$\frac{\kappa_{T,\star}}{\kappa_{T,\star}}$	$\frac{P}{\hat{c}_{p,\star}}$	$\frac{w}{w_{\star}}$	$\frac{\chi_{e,\star}}{\chi_{e,\star}}$	$\frac{L_{\star}}{L_{\star}}$
				$n = 10^{5}$				
15	0.101325	-124.98	$-0.29{\cdot}10^{-4}$	1545.41	428.40	-665.03	2064.05	
15	0.101325	-801.76	$-0.68 \cdot 10^{-3}$	12022.59	10916.90	-292.31	7394.27	
50	200	17.99	$0.27.10^{-5}$	-501.08	-14.16	216.56	-729.56	
00	400	-3.66	$-0.44.10^{-6}$	-96.93	-7.98	-21.07	139.56	
50	400	2.37	$0.31.10^{-6}$	107.56	9.60	-19.30	-5.67	
				$n = 10^{4}$				
.15	0.101325	4162.02	$0.93.10^{-3}$	-47775.34	-14352.32	21036.79	-67927.36	
.15	0.101325	7790.13	$0.67 \cdot 10^{-2}$	-116951.57	-106440.33	2543.51	-72161.87	
250	200	1670.25	$0.22 \cdot 10^{-3}$	-38414.77	-281.40	20040.61	-61509.86	
200	400	39.29	$0.46.10^{-6}$	-1712.79	5.15	854.42	-5569.52	
250	400	-10.22	$-0.40{\cdot}10^{-6}$	570.43	5.18	-268.67	1999.93	
				$n = 10^3$				
3.15	0.101325	47036.98	$0.11 \cdot 10^{-1}$	-540984.39	-162098.23	238206.89	-767841.48	
.15	0.101325	93738.95	$0.80 \cdot 10^{-1}$	-1405616.97	-1278231.17	31390.30	-867723.32	
250	200	-165.60	$-0.21 \cdot 10^{-4}$	3711.58	15.53	-1986.04	6023.81	
200	400	373.38	$0.74 \cdot 10^{-5}$	-14280.55	107.24	7663.89	-49973.49	
250	400	-52.19	$-0.28 \cdot 10^{-5}$	2113.33	-9.56	-1099.92	8685.26	
				$n = 10^2$				
.15	0.101325	190018.18	$0.42 \cdot 10^{-1}$	-2185035.19	-653781.33	964106.57	-3100888.54	
.15	0.101325	380627.98	0.32	-5687105.11	-5160921.64	133965.74	-3519594.82	
250	200	165107.11	$0.22 \cdot 10^{-1}$	-3785627.41	-26483.21	1985851.69	-6072006.33	
200	400	850.66	$0.17 \cdot 10^{-4}$	-32234.42	253.09	17391.91	-113407.72	
250	400	-3829.77	$-0.22 \cdot 10^{-3}$	140976.82	-1336.42	-75904.32	610364.54	
		-		$n = 10^{1}$				
.15	0.101325	-12287514.62	-2.95	145898351.27	48896156.92	-53603509.82	206873347.01	
6.15	0.101325	1341300.94	1.13	-19805072.01	-17848920.22	547357.55	-12359166.48	
250	200	1823017.78	0.24	-41455907.74	-266681.45	22491481.74	-66852307.68	
200	400	-32557.06	$-0.68 \cdot 10^{-3}$	1224714.96	-9955.36	-662964.78	4326988.81	
250	400	-8027.03	$-0.46 \cdot 10^{-3}$	295274.11	-2810.64	-159002.41	1278897.07	

Continuation of Table SM-5.1.

# SM-6 Table Values of the Deviations of the Analytical from the IAPWS G12-15 [1] Reference Formulation

**Table SM-6.1.** Deviation of the analytically determined mass density  $\hat{\varrho}$ , thermal expansion coefficient  $\alpha_p$ , isothermal compressibility  $\kappa_T$ , isobaric heat capacity  $c_p$ , speed of sound w, equilibrium mole fraction of low-density water,  $x_e$ , and the ordering field *L* according to Section SM-3.1 from the IAPWS G12-15 [1] reference values (subscript  $\star$ , Table SM-3.5.1). Relative deviations are given in parts per billion (ppb). Bold-styled values denote extrema.

$\frac{T}{K}$	$\frac{p}{MPa}$	$\frac{\widehat{\varrho} - \widehat{\varrho}_{\star}}{\widehat{\varrho}_{\star}}$	$\frac{\alpha_p - \alpha_{p,\star}}{10^{-4}\mathrm{K}^{-1}}$	$\frac{\kappa_T - \kappa_{T,\star}}{\kappa_{T,\star}}$	$\frac{\widehat{c}_p - \widehat{c}_{p,\star}}{\widehat{c}_{p,\star}}$	$\frac{w - w_{\star}}{w_{\star}}$	$\frac{x_{\rm e} - x_{\rm e\star}}{x_{\rm e,\star}}$	$\frac{L-L_{\star}}{L_{\star}}$
				$n = 10^9$				
273.15	0.101325	2.20	$-0.31 \cdot 10^{-6}$	82.19	-10.13	-21.23	-12.43	-4.24
235.15	0.101325	0.172·10 <sup>6</sup>	0.15	$-2.58 \cdot 10^{6}$	$-2.34 \cdot 10^{6}$	0.059·10 <sup>6</sup>	$-1.596 \cdot 10^{6}$	-45.23
250	200	-1.88	$0.11 \cdot 10^{-6}$	-45.26	-10.95	-21.76	1.16	3.61
200	400	-2.64	$-0.42 \cdot 10^{-6}$	-135.50	-7.67	-0.17	3.28	29.13
250	400	2.32	$0.31 \cdot 10^{-6}$	109.63	9.59	-20.41	3.31	-11.59

# SM-7 Table Values of the Deviation of the Analytically from the Numerically Determined Thermodynamic Properties of Subcooled Water

### 153 SM-7.1 Mass Density

**Table SM-7.1.1.** Relative deviation,  $(\hat{\varrho} - \hat{\varrho}_{num}) / \hat{\varrho}_{num}$  in parts per billion (ppb), of the mass density  $\hat{\varrho}$  using the analytically determined low-density water fraction from the mass density  $\hat{\varrho}_{num}$  using the numerically determined low-density water fraction at p=0.101325 MPa.

$\frac{T}{K}$	$\frac{\widehat{\varrho} - \widehat{\varrho}_{num}}{\widehat{\varrho}_{num}}$
235.15	172468.89
240.15	19920.96
245.15	3096.26
250.15	573.01
255.15	119.43
260.15	26.98
265.15	6.44
270.15	1.78
275.15	0.38
280.15	0.13
285.15	0.03
290.15	-0.03
295.15	-0.06
300.15	0.13

	303.15	0.05	0.00	0.12	-0.00	-0.01	-0.01	-0.01	-0.00	-0.01	-0.01	0.00	0.01	-0.01	-0.01	-0.01	-0.01	0.01	-0.00	-0.00	0.00	0.01	-0.00	0.01
	298.15	-0.13	0.03	0.10	-0.15	0.00	-0.09	-0.01	0.01	-0.01	-0.01	0.01	0.00	-0.01	0.01	-0.01	-0.01	-0.01	-0.02	-0.02	-0.01	-0.01	-0.00	-0.01
	293.15	-0.10	0.12	-0.15	-0.02	-0.11	-0.02	0.08	0.01	-0.12	-0.01	0.01	-0.01	0.00	-0.01	-0.01	-0.01	-0.02	0.01	-0.01	-0.01	0.01	0.01	-0.01
	273.15	0.79	0.49	0.52	0.29	0.29	0.26	0.07	0.01	0.14	-0.07	0.10	-0.13	-0.08	-0.09	-0.08	0.01	0.14	-0.16	-0.12	-0.00	-0.01	0.02	-0.01
	270.65	1.54	1.14	0.76	0.57	0.38	0.24	0.19	0.04	0.14	0.00	0.09	0.15	0.05	0.12	0.12	0.14	0.14	-0.11	0.17	-0.03	0.00	0.00	-0.01
X	268.15	2.95	2.09	1.52	1.18	0.66	0.44	0.28	0.35	0.24	0.26	0.02	0.20	-0.07	0.12	-0.01	0.14	-0.05	0.01	-0.07	0.05	-0.05	-0.00	0.00
T/	265.65	5.61	4.22	2.97	2.00	1.59	1.03	0.68	0.50	0.27	0.42	0.19	0.19	0.12	0.10	0.15	-0.04	0.02	0.10	0.09	-0.11	0.15	0.12	-0.01
	263.15	11.49	8.19	5.94	4.05	3.10	2.07	1.55	1.15	0.79	0.54	0.21	0.24	0.08	0.22	0.18	-0.02	0.19	-0.13	-0.05	0.14	0.03	0.17	0.10
	260.65	23.44	16.71	11.95	8.43	5.86	4.13	2.70	1.91	1.45	0.86	0.51	0.30	0.24	0.36	0.25	0.03	0.02	0.21	-0.08	-0.13	0.04	0.03	-0.12
	258.15	48.57	34.23	23.89	16.66	11.72	8.06	5.66	3.78	2.63	1.70	1.13	0.84	0.52	0.53	0.34	0.11	0.13	0.19	0.02	0.09	0.15	0.04	-0.10
	255.65	102.65	71.77	49.70	34.15	23.40	16.07	10.94	7.38	5.17	3.33	2.30	1.55	1.05	0.87	0.36	0.24	0.07	0.23	0.02	0.03	0.00	-0.06	-0.04
	253.15	220.99	152.68	104.40	71.10	48.26	32.52	22.14	14.96	9.99	6.75	4.56	2.98	2.04	1.48	0.76	0.66	0.47	0.12	0.18	-0.04	0.13	-0.00	0.05
<u>d</u>		0.1	5.0	10.0	15.0	20.0	25.0	30.0	35.0	40.0	45.0	50.0	55.0	60.0	65.0	70.0	75.0	80.0	85.0	90.0	95.0	100.0	105.0	110.0

**Table SM-7.1.2.** As Table SM-7.1.1, but for  $0.1 \le p/MPa \le 400$  and  $253.15 \le T/K \le 303.15$ .

$\frac{p}{MPa}$						T/	X					
	253.15	255.65	258.15	260.65	263.15	265.65	268.15	270.65	273.15	293.15	298.15	303.15
115.0	-0.08	0.03	0.14	-0.05	0.02	0.01	0.01	-0.00	-0.01	-0.01	-0.00	-0.01
120.0	0.15	0.00	0.16	-0.01	-0.01	0.00	-0.01	-0.00	-0.01	0.00	0.02	0.00
125.0	-0.16	-0.07	0.01	0.00	0.01	0.00	-0.02	-0.01	0.01	-0.00	-0.01	-0.01
130.0	-0.07	0.00	-0.01	0.00	-0.01	-0.01	-0.01	0.01	-0.01	0.00	-0.01	0.01
135.0	0.02	0.00	-0.01	0.01	-0.01	-0.01	0.00	-0.00	-0.00	-0.00	0.02	0.00
140.0	0.00	0.00	-0.01	0.00	0.00	0.02	-0.01	0.02	0.01	0.01	0.01	0.01
145.0	-0.00	-0.01	0.01	-0.01	0.00	0.00	-0.00	0.00	-0.01	0.01	0.01	-0.00
150.0	-0.01	-0.00	-0.01	-0.02	0.01	-0.00	-0.01	-0.00	-0.00	-0.01	-0.01	-0.01
155.0	0.01	0.01	-0.01	0.02	0.01	0.01	-0.01	0.02	-0.01	0.00	0.01	0.01
160.0	0.00	-0.00	-0.01	-0.01	-0.00	0.00	0.00	-0.01	-0.00	-0.01	0.01	0.01
165.0	0.01	0.01	0.00	0.02	-0.01	-0.01	0.00	0.01	0.01	-0.00	-0.01	0.00
170.0	-0.01	-0.01	-0.00	0.01	-0.01	-0.01	0.02	0.00	0.00	0.01	-0.01	-0.00
175.0	-0.01	-0.02	-0.01	-0.01	0.01	0.01	0.01	-0.01	0.00	-0.00	0.02	0.01
180.0	0.01	-0.02	-0.01	0.01	0.01	0.01	0.01	-0.01	-0.01	0.02	-0.01	0.01
185.0	-0.02	0.01	0.00	-0.00	0.00	-0.02	0.01	-0.01	-0.01	0.01	-0.01	0.01
190.0	0.01	-0.00	0.00	0.01	-0.00	0.00	0.01	-0.01	-0.00	0.01	0.01	-0.00
195.0	0.01	0.02	0.01	-0.01	-0.02	-0.02	0.01	0.01	-0.01	0.01	-0.00	0.01
200.0	-0.01	0.01	-0.01	-0.01	0.01	-0.02	0.01	0.02	0.01	-0.01	-0.01	-0.01
205.0	0.02	-0.01	0.01	0.00	0.00	0.02	-0.00	0.01	0.02	0.01	-0.00	0.01
210.0	-0.01	0.01	-0.00	-0.01	0.01	0.01	-0.00	-0.01	-0.00	0.01	0.01	-0.00
215.0	-0.00	-0.01	-0.01	0.01	-0.01	0.02	0.02	0.01	0.00	0.02	0.02	-0.01
220.0	-0.00	0.01	0.01	-0.00	0.02	0.02	0.01	0.01	-0.01	-0.00	0.02	-0.02
225.0	-0.01	0.00	0.01	0.00	0.01	-0.02	0.01	-0.01	-0.01	0.00	-0.02	0.01
230.0	-0.01	-0.01	-0.01	-0.01	-0.01	-0.02	0.02	0.00	0.00	-0.01	-0.01	-0.00
235.0	0.02	-0.01	0.01	-0.00	-0.01	-0.02	-0.00	-0.01	0.01	0.02	0.00	0.01
240.0	-0.01	-0.00	0.01	0.01	-0.00	-0.02	0.02	-0.00	-0.01	0.02	0.01	-0.01
245.0	-0.01	0.00	-0.00	-0.01	-0.00	-0.00	-0.02	0.00	-0.01	0.02	-0.00	-0.01
250.0	0.02	-0.00	-0.00	0.02	-0.01	0.02	-0.01	0.01	0.01	-0.01	-0.02	0.01

Continuation of Table SM-7.1.2.

	15	01	00	00	00	00	00	00	00	00	00	00	00	00	00	00	00	00	00	00	00	00	00	00	00	00	00
	303.	0.	-0.	0.	-0.	0.	-0.	-0.	-0.	0.	-0.	-0.	-0.	-0.	-0.	-0.	-0.	-0.	-0.	0.	0.	-0.	0.	-0.	0.	0.	0.
	298.15	0.00	0.00	0.02	-0.00	-0.00	0.00	0.00	-0.00	-0.00	-0.00	0.00	0.00	-0.00	0.00	0.00	-0.00	-0.00	-0.00	0.00	0.00	0.00	0.00	-0.00	-0.00	0.00	0.00
	293.15	0.01	0.00	0.00	0.02	-0.01	0.00	0.00	-0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	-0.00	-0.00	-0.00	0.00	-0.00	0.00	-0.00	0.00	0.00	0.00	-0.00
	273.15	-0.02	-0.02	0.01	-0.01	0.01	-0.01	0.01	-0.01	0.00	-0.02	0.00	0.00	-0.00	0.00	0.00	0.00	-0.00	-0.00	-0.00	-0.00	-0.00	0.00	0.00	0.00	0.00	0.00
	270.65	0.02	-0.00	0.02	-0.01	-0.01	-0.00	-0.00	-0.00	0.02	-0.01	0.00	-0.00	-0.00	0.00	-0.00	-0.00	0.00	-0.00	0.00	-0.00	-0.00	-0.00	0.00	-0.00	-0.00	0.00
K	268.15	0.02	-0.00	-0.01	0.01	0.02	-0.00	0.02	0.00	-0.01	-0.02	-0.00	-0.02	0.00	0.00	-0.00	0.00	-0.00	-0.00	0.00	0.00	0.00	-0.00	0.00	-0.00	-0.00	0.00
T/	265.65	0.01	0.02	-0.00	-0.02	-0.00	0.02	-0.00	0.02	-0.02	0.00	-0.01	-0.02	0.00	0.00	0.00	-0.00	0.00	-0.00	0.00	-0.00	-0.00	0.00	-0.00	0.00	0.00	0.00
	263.15	-0.01	-0.02	-0.01	0.01	-0.00	-0.01	-0.01	-0.01	0.01	-0.01	0.01	-0.00	-0.01	-0.00	-0.00	-0.00	-0.00	0.00	0.00	0.00	0.00	0.00	-0.00	-0.00	0.00	-0.00
	260.65	-0.00	-0.00	0.01	0.00	0.02	-0.01	-0.00	0.01	-0.00	0.01	-0.01	0.02	0.01	-0.00	-0.00	0.00	0.00	-0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	-0.00
	258.15	-0.02	0.02	0.00	-0.01	-0.02	0.02	-0.00	-0.00	0.01	0.01	0.01	-0.01	-0.02	-0.01	0.00	-0.00	0.00	-0.00	0.00	-0.00	0.00	0.00	0.00	-0.00	-0.00	0.00
	255.65	0.02	-0.00	-0.01	-0.02	-0.02	-0.00	-0.01	0.01	-0.01	0.02	-0.02	-0.01	0.01	0.02	0.00	-0.00	-0.00	0.00	0.00	0.00	0.00	-0.00	0.00	-0.00	-0.00	-0.00
	253.15	-0.02	-0.02	0.02	0.02	-0.01	0.00	-0.01	0.01	-0.01	-0.02	-0.02	-0.00	0.02	-0.01	0.00	0.00	0.00	0.00	-0.00	-0.00	-0.00	-0.00	0.00	-0.00	-0.00	0.00
<u>d</u>		255.0	260.0	265.0	270.0	275.0	280.0	285.0	290.0	295.0	300.0	305.0	310.0	315.0	320.0	325.0	330.0	335.0	340.0	345.0	350.0	355.0	360.0	365.0	370.0	375.0	380.0

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$\frac{p}{MPa}$						$T_{/}$	ΪK					
5	253.15	255.65	258.15	260.65	263.15	265.65	268.15	270.65	273.15	293.15	298.15	303.15
385.0	0.00	-0.00	0.00	0.00	0.00	0.00	-0.00	0.00	0.00	-0.00	-0.00	-0.00
390.0	0.00	-0.00	0.00	-0.00	0.00	-0.00	-0.00	-0.00	0.00	-0.00	-0.00	-0.00
395.0	0.00	0.00	-0.00	0.00	0.00	-0.00	0.00	-0.00	0.00	-0.00	0.00	-0.00
400.0	-0.00	0.00	-0.00	-0.00	-0.00	0.00	0.00	0.00	-0.00	-0.00	-0.00	0.00

p/MPa		T,	/K	
	273.15	293.15	298.15	303.15
0.1	0.79	-0.10	-0.13	0.05
50.0	0.10	0.01	0.01	0.00
100.0	-0.01	0.01	-0.01	0.01
150.0	-0.00	-0.01	-0.01	-0.01
200.0	0.01	-0.01	-0.01	-0.01
250.0	0.01	-0.01	-0.02	0.01
300.0	-0.02	0.00	-0.00	-0.00
350.0	-0.00	-0.00	0.00	0.00
400.0	-0.00	-0.00	-0.00	0.00
450.0	0.00	-0.00	-0.00	0.00
500.0	-0.00	0.00	-0.00	-0.00
550.0	-0.00	0.00	-0.00	-0.00
600.0	-0.00	0.00	-0.00	0.00
650.0	0.00	0.00	0.00	0.00
700.0	-0.00	0.00	0.00	-0.00
750.0	-0.00	0.00	-0.00	-0.00
800.0	-0.00	-0.00	0.00	-0.00
850.0	0.00	-0.00	-0.00	0.00
900.0	0.00	-0.00	0.00	0.00
950.0	-0.00	0.00	-0.00	-0.00
1000.0	-0.00	0.00	-0.00	0.00

**Table SM-7.1.3.** As Table SM-7.1.1, but for  $0.1 \le p/MPa \le 1000$  and  $235.15 \le T/K \le 303.15$ .

T/K					p/hPa				
	1000	006	800	700	600	500	400	300	200
235.15	172494.11	172684.18	172874.63	173065.06	173255.86	173446.84	173638.00	173829.53	174021.05
240.15	19923.63	19942.33	19961.02	19979.90	19998.77	20017.41	20036.25	20055.29	20074.10
245.15	3096.52	3099.25	3101.81	3104.41	3107.06	3109.77	3112.29	3115.09	3117.71
250.15	572.97	573.37	573.85	574.42	574.82	575.31	575.64	576.06	576.56
255.15	119.34	119.46	119.59	119.47	119.60	119.73	119.87	120.00	120.14
260.15	26.97	27.21	27.03	27.22	27.27	27.17	27.18	27.30	27.27
265.15	6.54	6.59	6.56	6.47	6.57	6.59	6.54	6.69	6.49
270.15	1.72	1.58	1.71	1.82	1.63	1.71	1.78	1.83	1.58
275.15	0.31	0.57	0.58	0.33	0.40	0.50	0.34	0.50	0.41
280.15	0.09	0.05	0.08	0.18	0.05	-0.01	0.01	0.09	0.25
285.15	-0.10	-0.01	0.18	0.17	-0.03	0.17	0.17	-0.02	-0.11
290.15	0.13	-0.12	0.08	0.10	-0.06	-0.09	0.02	-0.05	0.01
295.15	-0.13	-0.02	-0.08	0.03	-0.03	0.07	0.02	0.12	0.06
300.15	-0.14	-0.03	-0.06	0.09	0.09	-0.04	0.00	-0.10	-0.02

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As Table SM-7.1.1, but for 200 $\leq$
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.4. As Table SM-7.1.1, but for $200 \le$
<b>.1.4.</b> As Table SM-7.1.1, but for $200 \le$
-7.1.4. As Table SM-7.1.1, but for $200 \le$
<b>1-7.1.4.</b> As Table SM-7.1.1, but for $200 \le 1$
M-7.1.4. As Table SM-7.1.1, but for $200 \le$
SM-7.1.4. As Table SM-7.1.1, but for $200 \le$
e SM-7.1.4. As Table SM-7.1.1, but for $200 \le$
<b>le SM-7.1.4.</b> As Table SM-7.1.1, but for $200 \le$
<b>ble SM-7.1.4.</b> As Table SM-7.1.1, but for $200 \le$
able SM-7.1.4. As Table SM-7.1.1, but for $200 \le$

## 154 SM-7.2 Thermal Expansivity

**Table SM-7.2.1.** Deviation,  $(\alpha_p - \alpha_{p,\text{num}}) / (10^{-4} \text{ K}^{-1})$ , of the thermal expansivity  $\alpha_p$  using the analytically determined low-density water fraction from the thermal expansivity  $\alpha_{p,\text{num}}$  using the numerically determined low-density water fraction for  $0.1 \le p/\text{MPa} \le 600$  and  $245.5 \le T/\text{K} \le 288.0$ .

<u>p</u>			Т	/K		
MPa	245 5	253.2	262.8	273.8	281.3	288.0
01	0.11F-02	0.68E-04	0.32E-05	0.16E-06	0.16E-07	0.65E-08
10.0	0.44E-03	0.31E-04	0.16E-05	0.81E-07	0.91E-08	0.31E-08
20.0	0.17E-03	0.14F-04	0.79E-06	0.49E-07	0.11E-07	0.14E-07
30.0	0.67E-04	0.59E-05	0.39E-06	0.15E 07	0.24E-07	-0.12E-07
40.0	0.26F-04	0.25E-05	0.18E-06	-0.14F-07	-0 52E-08	-0.84E-09
50.0	0.99E-05	0.10E-05	0.11E-06	-0 15E-07	-0 23E-07	0.98E-09
60.0	0.38E-05	0.47E-06	0.17E-07	0.16E-07	-0 29E-07	0.24E-08
70.0	0.15E-05	0.17E 00	0.20E-08	-0 35E-08	0.30E-07	-0.25E-08
80.0	0.10E 00	0.25E 00	0.10E-07	0.49E-08	-0.11E-08	0.14E-08
90.0	0.21E-06	0.70E-08	0.35E-07	0.27E-07	0.18E-08	-0.48E-09
100.0	0.12F-06	0.43E-07	-0.13E-08	-0.18F-09	-0.82E-09	0.10E 09
110.0	0.12E 00	-0.24E-07	-0.18E-08	0.10E 09	-0 19E-08	-0 24E-08
120.0	0.21E 07	-0.11E-07	0.10E 00	0.12E 00	0.68E-09	0.14E-09
120.0	-0.20E 07	-0.18E-07	0.23E 00	-0.96E-09	0.00E 09	-0.17E-08
140.0	0.21E 09	0.10E 07	-0 77E-10	-0.22E-08	0.21E 09	-0.20E-08
150.0	0.18E-08	0.92E 09	-0.80E-09	0.22E 00	0.25E-08	0.20E 00
160.0	-0.10E-00	-0.15E-09	-0.00E-09	-0.20E-08	-0.19E-08	0.00E-09
170.0	-0.18E-08	0.13E 09	-0.20E 00	0.20E 00	-0 24E-08	0.25E 00
180.0	0.10E 00	-0.32E-09	-0.21E 00	-0.23E-08	-0.24E 00	-0 19E-09
100.0	-0.13E-08	0.52E 09	-0.65E-09	-0 22E-09	-0.86E-09	0.17E 09
200.0	-0.15E-00	-0.13E-08	0.05E-09	-0.22E-09	0.76E-09	-0.14E-08
200.0	0.21E-09	-0.13E-00	-0.16E-08	-0.21E-00	0.70E-09	-0.14E-00
210.0	-0.21E-08	-0.21E-08	0.10E 00	0.22E 09	0.10E 00	-0.17E-08
220.0	0.21E 00	-0.21E 00	-0.20E-08	-0.18E-08	0.34E 09	0.17E 00
230.0 240.0	-0.05E-09	-0.20E-08	-0.20E-08	-0.10E-00	0.15E-08	0.10E-08
250.0	-0.45E-09	0.22E 00	0.19E-08	-0 57E-10	-0 77E-09	0.10E 00
260.0	-0.15E-09	0.32E 09	-0.10E-08	0.97E 10	0.68E-09	-0.68E-09
200.0	0.18E-08	0.50E-09	-0.18E-08	-0.23E-08	-0 19F-08	-0 18E-08
280.0	-0.12E-08	0.00E 09	-0.19E-08	-0.10E-08	-0.14E-08	-0.12E-08
290.0	-0.11E-08	0.11E 00	0.17E 00	-0.12E-08	-0 23E-08	-0.47E-10
300.0	0.17E-08	-0.64F-09	-0.67E-09	-0.35E-09	0.54E-10	0.17 E 10
310.0	0.17 £ 00	-0.12E-08	-0.66E-09	-0.16E-10	0.62E-11	0.15E 10
320.0	-0 70F-09	-0.12E-08	0.22E-10	-0.24E-10	-0 50E-10	-0.29E-10
330.0	-0 38F-09	-0 51E-10	-0 38F-10	-0 52F-10	-0.43E-11	0.35E-10
340.0	-0.65E-11	-0.43E-10	0.47E-10	0.49E-10	-0.42E-10	0.38E-10
350.0	0.22E-11	0.45E-11	-0.30E-10	-0.88E-11	-0.30E-10	0.39E-11
360.0	0.69E-11	-0.31E-10	0.12E-10	-0.24E-10	-0.52E-11	0.24E-10
370.0	0.13E-10	0.13E-10	0.31E-10	0.45E-11	-0.12E-10	0.39E-11
380.0	-0.26E-10	-0 23E-10	-0 23E-10	0.17E-10	-0.28E-10	-0.31E-10
390.0	0.13E-11	-0.18E-10	0.23E-10	-0.25E-10	-0.64E-11	-0.14E-11
400.0	0.47E-11	0.19E-10	0.20E-10	0.36E-11	0.99E-11	0.32E-11
410.0	-0.68E-11	-0.12E-10	-0.18F-10	0.63E-11	0.14F-10	0.32E 11
420.0	0.15E-10	-0.16E-10	-0.77E-11	0.15E-10	-0.14E-10	-0.12E-10
430.0	-0.53E-11	-0.11E-10	-0.43E-11	0.12E-10	0.31E-11	0.10E-11
440.0	0.11E-10	0.10E-10	0.14E-10	-0.57E-11	-0.17E-10	0.88E-11
450.0	0.55E-11	0.79E-11	0.68E-11	0.68E-11	0.19E-11	0.57E-11
460.0	-0.22E-11	-0.90E-11	-0.54E-11	0.12E-10	0.10E-10	0.14E-10
470.0	0.44E-13	-0.38E-11	-0.43E-11	0.13E-10	0.81E-11	-0.10E-10
480.0	-0.32E-11	-0.86E-11	-0.12E-11	0.28E-11	-0.95E-11	0.68E-11
490.0	-0.62E-11	-0.72E-11	-0.27E-11	0.81E-11	0.10E-10	-0.11E-10

Continuation of Table SM-7.2.1.

$\frac{p}{MPa}$			T,	/K		
	245.5	253.2	262.8	273.8	281.3	288.0
500.0	0.51E-11	-0.18E-11	-0.60E-11	-0.20E-11	-0.66E-11	0.68E-11
510.0	-0.12E-11	-0.48E-11	0.21E-11	-0.37E-11	0.41E-11	0.71E-11
520.0	0.30E-11	-0.41E-11	-0.54E-12	-0.42E-11	0.59E-11	-0.33E-11
530.0	0.29E-11	-0.34E-11	0.48E-13	-0.81E-12	0.25E-11	0.21E-11
540.0	-0.14E-11	0.34E-11	0.65E-14	0.40E-11	0.29E-11	0.34E-11
550.0	0.89E-12	0.98E-12	-0.38E-11	-0.46E-11	-0.37E-11	0.28E-11
560.0	0.14E-11	-0.24E-11	-0.32E-11	-0.98E-12	-0.44E-11	0.47E-11
570.0	-0.10E-11	-0.75E-13	-0.66E-12	-0.20E-11	-0.30E-11	0.35E-11
580.0	-0.11E-14	-0.47E-12	0.27E-12	-0.23E-11	-0.11E-11	-0.26E-11
590.0	-0.96E-12	0.21E-12	-0.16E-11	0.97E-12	0.15E-11	-0.58E-12
600.0	-0.88E-12	-0.12E-11	-0.93E-12	-0.69E-12	-0.32E-12	0.17E-11

### 155 SM-7.3 Compressibility

**Table SM-7.3.1.** Relative deviation,  $(\kappa_T - \kappa_{T,\text{num}}) / \kappa_{T,\text{num}}$  in parts per billion (ppb), of the isothermal compressibility  $\kappa_T$  using the analytically determined low-density water fraction from the thermal expansivity  $\kappa_{T,\text{num}}$  using the numerically determined low-density water fraction for  $0.1 \le p/\text{MPa} \le 190$  and  $235.15 \le T/K \le 300.15$ .

-						
T/K			p/MPa			
	0.101325	10.0	50.0	100.0	150.0	190.0
235.15	-2583606.23	-868662.57	-12123.11	-86.13	-3.93	-0.25
240.15	-257131.42	-104712.54	-2534.75	-23.65	1.62	-0.25
245.15	-37519.10	-16968.92	-589.71	-6.69	0.17	-0.01
250.15	-6743.93	-3268.78	-149.13	-5.37	-0.30	-0.37
255.15	-1386.73	-705.53	-40.33	-2.79	-0.31	-0.03
260.15	-311.39	-165.93	-9.89	-2.20	0.15	0.36
265.15	-74.12	-40.47	-4.30	2.64	0.30	0.30
270.15	-20.46	-9.19	0.30	0.13	0.01	0.20
275.15	-4.39	-2.04	-0.40	0.25	-0.30	0.16
280.15	-1.45	-1.92	-0.75	-0.24	0.09	0.13
285.15	-0.36	1.46	2.08	0.07	0.00	-0.17
290.15	0.38	-1.44	1.76	0.13	0.25	-0.19
295.15	0.70	1.35	0.17	-0.01	-0.22	0.31
300.15	-1.50	0.38	-0.12	0.20	-0.12	-0.22

Version August 25, 2020 submitted to Journal Not Specified

### 156 SM-7.4 Isobaric Heat Capacity

T/K				p/MPa	a				
	0.101325	19.6	29.4	39.2	49.0	68.6	98.1	150.0	190.0
235.15	-2348083.25	-173405.05	-48054.63	-13614.26	-3938.60	-348.45	-10.17	-0.11	-0.00
240.15	-180561.64	-19872.54	-6502.75	-2131.01	-700.89	-76.96	-2.72	0.05	-0.00
245.15	-21310.20	-2984.89	-1091.15	-395.69	-142.83	-18.92	-1.09	0.01	-0.00
250.15	-3219.47	-533.75	-211.66	-83.07	-32.67	-4.87	-0.45	-0.01	-0.00
255.15	-574.24	-108.00	-45.56	-18.96	-8.24	-1.08	-0.30	-0.01	-0.00
260.15	-114.81	-24.04	-10.42	-4.96	-1.92	-0.35	-0.15	0.01	0.01
265.15	-24.87	-5.47	-2.52	-1.63	-0.60	0.20	0.06	0.01	0.01
270.15	-6.37	-1.77	-1.12	0.06	-0.27	-0.01	0.03	0.00	0.00
275.15	-1.29	-0.23	-0.34	-0.45	-0.08	-0.02	-0.01	-0.01	0.00
280.15	-0.41	0.25	0.23	-0.31	-0.33	-0.28	-0.03	0.00	0.00
285.15	-0.10	-0.11	0.34	0.04	-0.38	-0.00	0.02	0.00	-0.01
290.15	0.10	-0.17	0.37	0.01	0.12	-0.01	0.00	0.01	-0.01
295.15	0.18	-0.05	0.34	0.02	0.00	0.03	0.02	-0.01	0.01
300.15	-0.39	0.06	0.00	-0.01	-0.02	0.01	-0.00	-0.01	-0.01

**Table SM-7.4.1.** Relative deviation,  $(\hat{c}_p - \hat{c}_{p,\text{num}}) / \hat{c}_{p,\text{num}}$  in parts per billion (ppb), of the isobaric heat capacity  $\hat{c}_p$  using the analytically determined low-density water fraction from the isobaric heat capacity  $\hat{c}_{p,\text{num}}$  using the numerically determined low-density water fraction for  $0.1 \le p/\text{MPa} \le 190$  and  $235.15 \le T/\text{K} \le 300.15$ .

**Table SM-7.4.2.** As Table SM-7.4.1, but for  $200 \le p/hPa \le 1000$  and  $235.15 \le T/K \le 300.15$ .

T/K					p/hPa				
	1000	900	800	700	600	500	400	300	200
235.15	-2348501.21	-2351652.63	-2354810.49	-2357969.59	-2361135.13	-2364304.50	-2367477.70	-2370657.33	-2373838.17
240.15	-180590.11	-180791.41	-180992.64	-181195.73	-181398.75	-181599.77	-181802.65	-182007.38	-182210.10
245.15	-21312.37	-21334.25	-21354.89	-21375.87	-21397.20	-21418.86	-21439.30	-21461.65	-21482.76
250.15	-3219.34	-3221.96	-3225.06	-3228.62	-3231.30	-3234.44	-3236.69	-3239.42	-3242.61
255.15	-573.79	-574.47	-575.15	-574.62	-575.31	-576.01	-576.71	-577.42	-578.13
260.15	-114.80	-115.80	-115.05	-115.90	-116.11	-115.67	-115.73	-116.26	-116.16
265.15	-25.26	-25.46	-25.37	-25.00	-25.39	-25.49	-25.30	-25.88	-25.12
270.15	-6.14	-5.65	-6.11	-6.51	-5.85	-6.13	-6.37	-6.54	-5.65
275.15	-1.05	-1.94	-1.95	-1.10	-1.33	-1.67	-1.14	-1.69	-1.37
280.15	-0.30	-0.16	-0.25	-0.57	-0.16	0.02	-0.03	-0.30	-0.81
285.15	0.32	0.04	-0.56	-0.54	0.09	-0.53	-0.54	0.06	0.35
290.15	-0.39	0.35	-0.23	-0.29	0.19	0.27	-0.05	0.16	-0.02
295.15	0.37	0.07	0.23	-0.08	0.09	-0.22	-0.05	-0.35	-0.18
300.15	0.40	0.08	0.17	-0.26	-0.28	0.12	-0.00	0.29	0.06

p/MPa						T/	′K					
	253.15	255.65	258.15	260.65	263.15	268.15	273.15	278.15	288.15	293.15	298.15	303.15
0.1	821.07	404.34	201.15	101.40	51.64	14.15	3.99	0.56	0.57	-0.58	-0.80	0.31
10.0	448.92	223.04	111.30	57.55	29.48	7.95	2.86	-0.01	-0.21	-0.95	0.61	0.75
20.0	234.26	117.26	60.43	31.02	16.78	3.72	1.70	-0.38	-0.77	-0.71	0.01	-0.06
30.0	119.03	60.25	31.89	15.52	9.10	1.67	0.41	-0.19	-0.64	0.51	-0.07	-0.10
40.0	58.63	30.90	15.99	8.99	4.99	1.56	0.91	0.58	-0.99	-0.86	-0.08	-0.08
50.0	28.91	14.82	7.36	3.36	1.42	0.12	0.70	-0.97	0.25	0.05	0.10	0.01
60.0	13.87	7.19	3.63	1.70	0.60	-0.47	-0.58	-0.15	-0.00	0.02	-0.09	-0.11
70.0	5.50	2.65	2.53	1.83	1.35	-0.10	-0.62	-0.03	0.02	-0.05	-0.05	-0.05
80.0	3.58	0.52	0.98	0.13	1.48	-0.36	1.09	0.07	0.10	-0.13	-0.10	0.09
90.0	1.46	0.20	0.18	-0.68	-0.39	-0.56	-0.99	-0.01	-0.10	-0.09	-0.14	-0.00
100.0	1.06	0.02	1.31	0.31	0.24	-0.46	-0.08	0.09	0.01	0.07	-0.07	0.05
110.0	0.43	-0.39	-0.92	-1.03	0.85	0.02	-0.05	0.13	0.10	-0.08	-0.09	0.12
120.0	1.41	0.03	1.43	-0.06	-0.07	-0.06	-0.10	0.09	-0.04	0.04	0.15	0.02
130.0	-0.68	0.04	-0.05	0.02	-0.12	-0.13	-0.09	-0.08	-0.12	0.00	-0.12	0.11
140.0	0.01	0.04	-0.13	0.01	0.02	-0.11	0.11	-0.05	-0.03	0.13	0.13	0.12
150.0	-0.15	-0.03	-0.08	-0.16	0.06	-0.14	-0.02	0.14	0.15	-0.06	-0.15	-0.08
160.0	0.01	-0.05	-0.09	-0.13	-0.02	0.02	-0.05	-0.12	0.02	-0.09	0.07	0.13
170.0	-0.13	-0.13	-0.00	0.07	-0.08	0.16	0.05	-0.09	-0.17	0.09	-0.08	-0.01
180.0	0.15	-0.20	-0.14	0.06	0.11	0.14	-0.17	-0.03	0.15	0.18	-0.08	0.12

**Table SM-7.5.1.** Relative deviation,  $(w - w_{num}) / w_{num}$  in parts per billion (ppb), of the sound speed *w* using the analytically determined low-density water fraction from the sound speed  $w_{num}$  using the numerically determined low-density water fraction for  $0.1 \le p / MPa \le 400$  and  $253.15 \le T/K \le 303.15$ .

/) (D	1						/1/					
p/MPa						Τ,	<u>/K</u>					
	253.15	255.65	258.15	260.65	263.15	268.15	273.15	278.15	288.15	293.15	298.15	303.15
190.0	0.15	-0.01	0.04	0.08	-0.05	0.08	-0.05	-0.01	0.03	0.15	0.10	-0.01
200.0	-0.16	0.14	-0.12	-0.16	0.14	0.10	0.11	0.10	0.20	-0.13	-0.14	-0.12
210.0	-0.07	0.16	-0.03	-0.16	0.14	-0.04	-0.03	-0.23	0.12	0.10	0.06	-0.04
220.0	-0.01	0.09	0.13	-0.03	0.24	0.09	-0.09	0.02	0.16	-0.05	0.20	-0.23
230.0	-0.15	-0.19	-0.15	-0.13	-0.17	0.20	0.01	-0.10	0.09	-0.16	-0.11	-0.02
240.0	-0.07	-0.01	0.14	0.07	-0.05	0.20	-0.12	-0.11	0.01	0.23	0.13	-0.08
250.0	0.26	-0.02	-0.00	0.21	-0.12	-0.13	0.15	-0.25	0.19	-0.09	-0.23	0.08
260.0	-0.27	-0.01	0.23	-0.04	-0.24	-0.01	-0.23	-0.03	-0.11	0.05	0.03	-0.00
270.0	0.27	-0.25	-0.09	0.06	0.17	0.17	-0.21	0.08	-0.14	0.27	-0.01	-0.00
280.0	0.07	-0.04	0.25	-0.09	-0.16	-0.04	-0.08	-0.01	-0.22	0.00	0.01	-0.00
290.0	0.16	0.15	-0.02	0.17	-0.15	0.06	-0.17	0.24	-0.01	-0.00	-0.00	-0.01
300.0	-0.26	0.31	0.15	0.14	-0.13	-0.27	-0.31	0.00	0.01	0.00	-0.00	-0.00
310.0	-0.00	-0.10	-0.10	0.27	-0.07	-0.35	0.01	0.00	-0.00	0.00	0.01	-0.01
320.0	-0.16	0.28	-0.22	-0.01	-0.01	0.01	0.00	0.01	-0.00	0.00	0.00	-0.00
330.0	0.00	-0.01	-0.01	0.01	-0.01	0.00	0.01	0.01	0.00	-0.01	-0.00	-0.00
340.0	0.01	0.00	-0.00	-0.01	0.01	-0.01	-0.01	-0.00	0.01	-0.00	-0.00	-0.00
350.0	-0.00	0.00	-0.01	0.00	0.00	0.01	-0.01	-0.01	0.00	-0.00	0.00	0.00
360.0	-0.00	-0.00	0.01	0.00	0.01	-0.00	0.01	-0.01	-0.01	-0.00	0.00	0.01
370.0	-0.00	-0.00	-0.01	0.00	-0.00	-0.01	0.00	-0.01	-0.01	0.00	-0.00	0.00
380.0	0.00	-0.00	0.01	-0.01	-0.00	0.00	0.01	-0.00	-0.01	-0.00	0.00	0.00
390.0	0.00	-0.00	0.01	-0.00	0.00	-0.01	0.01	0.00	0.00	-0.00	-0.00	-0.00
400.0	-0.00	0.00	-0.00	-0.00	-0.00	0.00	-0.01	-0.00	-0.00	-0.00	-0.00	0.00

Continuation of Table SM-7.5.1.

p/MPa		T,	/K	
	273.15	283.15	293.15	303.15
0.1	3.99	-0.37	-0.58	0.31
50.0	0.70	-0.92	0.05	0.01
100.0	-0.08	-0.04	0.07	0.05
150.0	-0.02	-0.00	-0.06	-0.08
200.0	0.11	0.12	-0.13	-0.12
250.0	0.15	-0.04	-0.09	0.08
300.0	-0.31	-0.01	0.00	-0.00
350.0	-0.01	0.00	-0.00	0.00
400.0	-0.01	-0.00	-0.00	0.00
450.0	0.01	0.00	-0.00	0.00
500.0	-0.00	-0.00	0.00	-0.00
550.0	-0.00	0.00	0.00	-0.00
600.0	-0.00	0.00	0.00	0.00
650.0	0.00	-0.00	0.00	0.00
700.0	-0.00	-0.00	0.00	-0.00
750.0	-0.00	0.00	0.00	-0.00
800.0	-0.00	0.00	-0.00	-0.00
850.0	0.00	0.00	-0.00	0.00
900.0	0.00	0.00	-0.00	0.00
950.0	-0.00	-0.00	0.00	-0.00
1000.0	-0.00	-0.00	0.00	0.00

**Table SM-7.5.2.** As in Table SM-7.5.1, but for  $0.1 \le p/MPa \le 1000$  and  $273.15 \le T/K \le 303.15$ .

### 158 SM-7.6 Gibbs Energy and Entropy

**Table SM-7.6.1.** Relative deviation,  $(\hat{g} - \hat{g}_{num}) / \hat{g}_{num}$  in units of parts per billion (ppb), of the specific Gibbs energy  $\hat{g}$  using the analytically determined low-density water fraction (Section 3.2) from the specific Gibbs energy  $\hat{g}_{num}$  using the numerically determined low-density water fraction for 200  $\leq p/hPa \leq 1000$  and 235.15  $\leq T/K \leq 300.15$ .

T/K					p/hPa				
	1000	900	800	700	600	500	400	300	200
235.15	-945.79	-946.99	-948.19	-949.39	-950.60	-951.81	-953.02	-954.23	-955.45
240.15	-21.86	-21.87	-21.89	-21.90	-21.92	-21.93	-21.95	-21.96	-21.98
245.15	-0.89	-0.89	-0.89	-0.89	-0.89	-0.90	-0.90	-0.90	-0.90
250.15	-0.05	-0.05	-0.05	-0.05	-0.05	-0.05	-0.05	-0.05	-0.05
255.15	-0.00	-0.00	-0.00	-0.00	-0.00	-0.00	-0.00	-0.00	-0.00
260.15	-0.00	-0.00	-0.00	-0.00	-0.00	-0.00	-0.00	-0.00	-0.00
265.15	-0.00	-0.00	-0.00	-0.00	-0.00	-0.00	-0.00	-0.00	-0.00
270.15	0.00	0.00	0.00	-0.04	-0.00	-0.00	-0.00	0.00	-0.00
275.15	0.00	0.00	-0.00	-0.00	0.00	0.00	0.00	0.03	-0.00
280.15	0.00	-0.00	-0.00	-0.00	-0.00	0.00	-0.00	-0.00	-0.00
285.15	0.00	-0.00	-0.00	-0.00	0.00	-0.00	0.00	0.00	-0.00
290.15	-0.00	0.00	-0.00	-0.00	-0.00	-0.00	0.00	-0.00	0.00
295.15	-0.00	-0.00	-0.00	-0.00	0.00	-0.00	-0.00	0.00	0.00
300.15	-0.00	0.00	-0.00	-0.00	-0.00	0.00	-0.00	-0.00	0.00

**Table SM-7.6.2.** Relative deviation,  $(\widehat{s} - \widehat{s}_{num}) / \widehat{s}_{num}$  in parts per billion (ppb), of the specific entropy  $\widehat{s}$  using the analytically determined low-density water fraction from the specific entropy  $\hat{s}_{num}$  using the numerically determined low-density water fraction for  $200 \le p/hPa \le 1000$  and  $235.15 \le T/K \le 300.15$ .

T/K					p/hPa				
	1000	006	800	200	009	500	400	300	200
235.15	-856729.10	-857726.22	-858725.32	-859724.49	-860725.64	-861727.81	-862731.01	-863736.16	-864741.39
240.15	-110411.71	-110520.32	-110628.86	-110738.51	-110848.08	-110956.40	-111065.82	-111176.35	-111285.62
245.15	-19971.77	-19990.14	-20007.34	-20024.87	-20042.71	-20060.87	-20077.87	-20096.66	-20114.28
250.15	-4485.25	-4488.50	-4492.40	-4496.96	-4500.27	-4504.24	-4506.97	-4510.34	-4514.38
255.15	-1196.76	-1198.08	-1199.41	-1198.21	-1199.56	-1200.92	-1202.28	-1203.66	-1205.04
260.15	-376.89	-380.17	-377.66	-380.42	-381.08	-379.64	-379.78	-381.51	-381.14
265.15	-149.70	-150.88	-150.34	-148.10	-150.40	-150.99	-149.88	-153.30	-148.76
270.15	-105.74	-97.25	-105.11	-112.00	-100.59	-105.53	-109.49	-112.48	-97.18
275.15	29.42	54.17	54.67	30.89	37.33	46.74	31.88	47.23	38.31
280.15	2.52	1.36	2.13	4.81	1.37	-0.15	0.25	2.57	6.81
285.15	-1.66	-0.21	2.90	2.81	-0.48	2.77	2.82	-0.33	-1.82
290.15	1.48	-1.35	0.89	1.10	-0.72	-1.02	0.20	-0.62	0.08
295.15	-1.14	-0.20	-0.69	0.23	-0.26	0.65	0.15	1.06	0.54
300.15	-1.02	-0.20	-0.43	0.66	0.70	-0.32	0.00	-0.74	-0.15

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   New York, 1996.

## **List of Tables**

237	Table SM-3.1.1	Parameter values for the equation of state given by Equations	(
238		(5M-3.1)-(5M-3.8). Taken from TAPWS G12-15 [1] (Table 1 therein).	6
239	Table SM-3.1.2	Parameter values for the dimensionless regular background Gibbs energy $\psi^{i}$	
240		in Equation (SM-3.3). Taken from IAPWS G12-15 [1] (Table 2 therein).	6
241	Table SM-3.2.1	Derivatives of $L(\tau, \pi)$ and $\psi^{\mu}(\tau, \pi)$ . To simplify the annotation of the	
242		derivatives of $\psi^{i}$ (right column), the following shorthand definitions are	_
243		used: $\overline{\tau} = \tau + 1$ and $\overline{\pi} = \pi + \pi_0$ . Taken from IAPWS G12-15 [1] (Table 3 therein).	7
244	Table SM-3.3.1	Regression coefficients $a_k$ , $n_k$ for $p_M(T)$ , Equation (SM-3.17), and $b_k$ for the	
245		$T_{\rm M}(p)$ , Equation (SM-3.18). Taken from Feistel [27].	9
246	Table SM-3.4.1	Subintervals for the numerical determination of the equilibrium mole fraction	
247		of low-density water, $x_e$ , in dependence on $L(\tau, \pi)$ and $\omega(\pi)$ . The "min"	
248		function returns the smallest value of its arguments. Taken from IAPWS	
249		G12-15 [1] (Table 4 therein).	9
250	Table SM-3.5.1	Thermodynamic reference values for check of the correct computer	
251		implementation. Taken from IAPWS G12-15 [1] (Table 5 therein).	11
252	Table SM-5.1	Deviations of the numerically determined values of mass density $\hat{\varrho}$ , thermal	
253		expansion coefficient $\alpha_p$ , isothermal compressibility $\kappa_T$ , isobaric heat capacity	
254		$c_p$ , speed of sound $w$ , equilibrium mole fraction of low-density water, $x_e$ ,	
255		and the ordering field L using the root finder of Press et al. [31] (Section	
256		9.1 therein) from the IAPWS G12-15 [1] reference values (subscript *, Table	
257		SM-3.5.1). Integer n denotes the number of equally spaced segments of the	
258		root interval of $x_e$ . Relative deviations are given in parts per billion (ppb).	
259		Bold-styled values denote extrema.	15
260	Table SM-6.1	Deviation of the analytically determined mass density $\hat{\varrho}$ , thermal expansion	
261		coefficient $\alpha_p$ , isothermal compressibility $\kappa_T$ , isobaric heat capacity $c_p$ , speed	
262		of sound $w$ , equilibrium mole fraction of low-density water, $x_e$ , and the	
263		ordering field <i>L</i> according to Section SM-3.1 from the IAPWS G12-15 [1]	
264		reference values (subscript *, Table SM-3.5.1). Relative deviations are given	
265		in parts per billion (ppb). Bold-styled values denote extrema.	17
266	Table SM-7.1.1	Relative deviation, $(\hat{\varrho} - \hat{\varrho}_{num}) / \hat{\varrho}_{num}$ in parts per billion (ppb), of the mass	
267		density $\hat{\varrho}$ using the analytically determined low-density water fraction from	
268		the mass density $\widehat{\varrho}_{num}$ using the numerically determined low-density water	
269		fraction at $p=0.101325$ MPa.	18
270	Table SM-7.1.2	As Table SM-7.1.1, but for $0.1 \le p/MPa \le 400$ and $253.15 \le T/K \le 303.15$ .	19
271	Table SM-7.1.3	As Table SM-7.1.1, but for $0.1 \le p/MPa \le 1000$ and $235.15 \le T/K \le 303.15$ .	23
272	Table SM-7.1.4	As Table SM-7.1.1, but for $200 \le p/hPa \le 1000$ and $235.15 \le T/K \le 300.15$ .	24
273	Table SM-7.2.1	Deviation, $(\alpha_p - \alpha_{p,\text{num}}) / (10^{-4} \text{ K}^{-1})$ , of the thermal expansivity $\alpha_p$ using	
274		the analytically determined low-density water fraction from the thermal	
275		expansivity $\alpha_{p,\text{num}}$ using the numerically determined low-density water	
276		fraction for $0.1 \le p/MPa \le 600$ and $245.5 \le T/K \le 288.0$ .	26
277	Table SM-7.3.1	Relative deviation, $(\kappa_T - \kappa_{T,\text{num}}) / \kappa_{T,\text{num}}$ in parts per billion (ppb), of the	
278		isothermal compressibility $\kappa_T$ using the analytically determined low-density	
279		water fraction from the thermal expansivity $\kappa_{T,\text{num}}$ using the numerically	
280		determined low-density water fraction for $0.1 \le p/MPa \le 190$ and $235.15 \le 100$	
281		$T/K \le 300.15.$	28

282	Table SM-7.4.1	Relative deviation, $(\hat{c}_p - \hat{c}_{p,\text{num}}) / \hat{c}_{p,\text{num}}$ in parts per billion (ppb), of the	
283		isobaric heat capacity $\hat{c}_p$ using the analytically determined low-density	
284		water fraction from the isobaric heat capacity $\hat{c}_{p,\text{num}}$ using the numerically	
285		determined low-density water fraction for 0.1 $\leq p/MPa \leq 190$ and	
286		$235.15 \le T/K \le 300.15.$	30
287	Table SM-7.4.2	As Table SM-7.4.1, but for $200 \le p/hPa \le 1000$ and $235.15 \le T/K \le 300.15$ .	30
288	Table SM-7.5.1	Relative deviation, $(w-w_{num}) / w_{num}$ in parts per billion (ppb), of the sound	
289		speed <i>w</i> using the analytically determined low-density water fraction from	
290		the sound speed $w_{num}$ using the numerically determined low-density water	
291		fraction for $0.1 \le p/MPa \le 400$ and $253.15 \le T/K \le 303.15$ .	31
292	Table SM-7.5.2	As in Table SM-7.5.1, but for $0.1 \le p/MPa \le 1000$ and $273.15 \le T/K \le 303.15$ .	33
293	Table SM-7.6.1	Relative deviation, $(\hat{g} - \hat{g}_{num}) / \hat{g}_{num}$ in units of parts per billion (ppb), of	
294		the specific Gibbs energy $\hat{g}$ using the analytically determined low-density	
295		water fraction (Section 3.2) from the specific Gibbs energy $\hat{g}_{num}$ using the	
296		numerically determined low-density water fraction for $200 \le p/hPa \le 1000$	
297		and $235.15 \le T/K \le 300.15$ .	34
298	Table SM-7.6.2	Relative deviation, $(\hat{s} - \hat{s}_{num}) / \hat{s}_{num}$ in parts per billion (ppb), of the specific	
299		entropy $\hat{s}$ using the analytically determined low-density water fraction from	
300		the specific entropy $\hat{s}_{num}$ using the numerically determined low-density	
301		water fraction for $200 \le p/hPa \le 1000$ and $235.15 \le T/K \le 300.15$ .	35

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