

Article

Modelling the Hindered Settling Velocity of a Falling Particle in a Particle-Fluid Mixture by the Tsallis Entropy Theory

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Abstract: The settling velocity of a sediment particle is an important parameter needed for modelling the vertical flux in rivers, estuaries, deltas and the marine environment. It has been observed that a particle settles more slowly in the presence of other particles in the fluid than in a clear fluid, and this phenomenon has been termed ‘hindered settling’. The Richardson and Zaki equation has been a widely used expression for relating the hindered settling velocity of a particle with that in a clear fluid in terms of a concentration function and the power of the concentration function, and the power index is known as the exponent of reduction of the settling velocity. This study attempts to formulate the model for the exponent of reduction of the settling velocity by using the probability method based on the Tsallis entropy theory. The derived expression is a function of the volumetric concentration of the suspended particle, the relative mass density of the particle and the particle’s Reynolds number. This model is tested against experimental data collected from the literature and against five existing deterministic models, and this model shows good agreement with the experimental data and gives better prediction accuracy than the other deterministic models. The derived Tsallis entropy-based model is also compared with the existing Shannon entropy-based model for experimental data, and the Tsallis entropy-based model is comparable to the Shannon entropy-based model for predicting the hindered settling velocity of a falling particle in a particle-fluid mixture. This study shows the potential of using the Tsallis entropy together with the principle of maximum entropy to predict the hindered settling velocity of a falling particle in a particle-fluid mixture.

Keywords: entropy; Tsallis entropy; probability distribution; hindered settling velocity; particle-fluid mixture

1. Introduction

In sediment transport dynamics, the settling velocity of the sediment particle is an important parameter needed for modelling vertical sediment flux in rivers, estuaries, deltas and marine environments [1–3]. In a still and clear fluid, a falling particle can accelerate downward due to gravitational force and reach its terminal velocity when the upward drag and submerged weight are in balance [4,5]. Many models for predicting the settling velocity of the particle (not limited to sediment particles) have been proposed [1,2,4–7]. By contrast, for a sediment-laden flow, it has been observed that the settling velocity of a falling particle is reduced compared to the settling of a particle in still fluid due to increased suspension concentration [8–10], which has been termed ‘hindered settling’.

The Richardson and Zaki [11] equation is a widely used expression for relating the hindered settling and the settling in clear fluid, as follows:

$$\omega_m = \omega(1 - c)^{n_H}, \quad (1)$$

where ω_m and ω are the settling velocities of the sediment particle in a sediment-laden flow and in a clear fluid, respectively, c is the volumetric concentration of the sediment particle, and n_H is the exponent of reduction of the settling velocity in a sediment-fluid mixture, which depends on the particle's Reynolds number R given by $\omega d_p / \nu_0$, where d_p is the particle's diameter and ν_0 is the kinematic viscosity of a clear fluid.

However, several experiments under various conditions have shown that the experimental settling velocity of the particle is lower than that predicted by Equation (1) [8,12,13]. To that end, many empirical or semi-empirical studies have been carried out to modify the expression of n_H to a better accuracy with the experimental data. Garside and Al-Dibouni [14] proposed an empirical expression of n_H as $(5.1 - n_H) / (n_H - 2.7) = 0.1R^{0.9}$, which shows good agreement with the experimental data. Chien and Wan [15] also showed that the exponent n_H is a function of R . Cheng [12] pointed out that the exponent n_H not only depends on the particle's Reynolds number but also on the particle's mass density and volumetric concentration. A theoretical form of the exponent n_H as a function of the mass density of the particle and the volumetric concentration was derived by Pal and Ghoshal [8] by introducing the concept of the apparent diameter of a particle, and the derived expression has shown good agreement with previously published experimental data. Furthermore, Baldock et al. [16] carried out an experiment to investigate the settling velocity of sediment particles with different combinations of particle diameters and particle mass densities, whereas the study of Tomkins et al. [17] incorporated the effect of the shape of the sand grains. The segregating effect between the sediment grains and the mud flows was discussed in the numerical simulation work of Van and Bang [18].

These studies have provided some physical insights to the hindered settling process of the particle in a particle-fluid mixture. During recent decades, some researchers have adopted the probability method based on entropy theory to investigate some classic hydraulic engineering problems, including predicting the one-dimensional and two-dimensional velocity distributions in open channels [19–21], estimating the sediment concentration distribution [22–26] and calculating the shear stress [27,28]. Recently, Singh et al. [29] reviewed the progress in the application of the entropy theory into water engineering problems. These works indicated that the probability method-based on the entropy theory could provide an easy and feasible tool for predicting some hydraulic problems besides the traditional deterministic methods.

Recently, Kumbhakar et al. [13] have used the Shannon entropy theory to derive the expression of the exponent of reduction of the settling velocity of the particle in a particle-fluid mixture. Another entropy, called the Tsallis entropy, which is a generalization of the Shannon entropy, has not been adopted for estimating the exponent of reduction of settling velocity. Thus, it may be interesting to explore the hindered settling velocity based on the Tsallis entropy. This study attempts to derive an entropy-based expression for the exponent of reduction of the settling velocity of a particle in particle-fluid mixture, by using the Tsallis entropy theory. Section 2 derives the expression for the exponent of reduction of the settling velocity of a particle using the Tsallis entropy theory. The derived expression is tested against some experimental data collected from the literature in Section 3, and Section 4 contains the comparisons of the expression with some existing deterministic models and the Shannon entropy-based expression. Finally, Section 5 presents concluding remarks.

2. Methodology for Determination of the Exponent of Reduction of Settling Velocity

It is assumed that the exponent of reduction of settling velocity n_H is a continuous random variable. Determination of the exponent of reduction of settling velocity using the Tsallis entropy entails the following steps: (1) definition of the Tsallis entropy; (2) specification of the constraints;

(3) maximization of the entropy; (4) determination of the Lagrange multiplier; (5) the hypothesis regarding the cumulative probability distribution; and (6) derivation of the expression for the exponent of reduction of the settling velocity.

2.1. Definition of the Tsallis Entropy

Let the exponent of reduction of the settling velocity n_H be the random variable with probability density function $f(n_H)$. The Tsallis function, $H(n_H)$, can be written as [30]

$$H(n_H) = \frac{1}{m-1} \left\{ 1 - \int_{n_0}^{n_1} [f(n_H)]^m dn_H \right\} \quad (2)$$

where n_0 and n_1 are the lower and upper limits of n_H , respectively, and m is the entropy index and is a real number not equal to 1. The Tsallis entropy is a non-extensive entropy that can reduce to the Shannon entropy if the exponent $m \rightarrow 1$ in Equation (2) [31]. Theoretically, the Tsallis entropy is maximum when the probability density function is uniform within its limits. Equation (2) expresses a measure of uncertainty of $f(n_H)$ or the average information content of sample n_H .

2.2. Specification of Constraint

If the observations of n_H are available, then we can express the information about the random variable in terms of constraints [31]. First, the total probability law must be satisfied for the probability density function $f(n_H)$, that is

$$\int_{n_0}^{n_1} f(n_H) dn_H = 1. \quad (3)$$

The other constraint equation is given as

$$\int_{n_0}^{n_1} n_H f(n_H) dn_H = \bar{n}_H, \quad (4)$$

where \bar{n}_H is the mean value of n_H . Equation (4) is the mean constraint.

2.3. Maximization of Entropy

It should be noted that there are an infinite number of probability density distributions satisfying the constraint equations, Equations (3) and (4). Thus, in order to choose among all of the distribution functions satisfying the constraint equations, we use the principle of the maximum entropy developed by Jaynes [32–34] in this study. This principle requires that the derived probability distribution is the one that corresponds to the maximum entropy or uncertainty. To that end, the method of the Euler-Lagrange calculus of variation was adopted [29]. Consequently, the Lagrangian function L can be written as follows:

$$L = \frac{1}{m-1} \left\{ 1 - \int_{n_0}^{n_1} [f(n_H)]^m dn_H \right\} - \lambda_0 \left[\int_{n_0}^{n_1} f(n_H) dn_H - 1 \right] - \lambda_1 \left[\int_{n_0}^{n_1} n_H f(n_H) dn_H - \bar{n}_H \right] \quad (5)$$

where λ_0 and λ_1 are two Lagrange multipliers that need to be determined from the constraint equations, Equations (3) and (4). Treating n_H as the independent variable and $f(n_H)$ as the dependent variable, the Euler-Lagrange equation becomes

$$\frac{\partial L}{\partial f} - \frac{d}{dn_H} \left(\frac{\partial L}{\partial f'} \right) = 0, \quad (6)$$

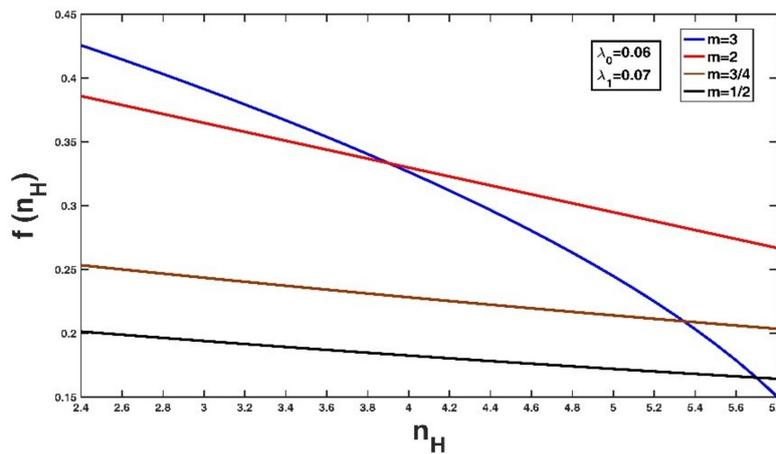
where f' denotes the derivative of f with respect to n_H . From Equation (5) it is obvious that the Lagrangian function is not a function of f' , thus Equation (6) becomes

$$\frac{\partial L}{\partial f} = 0 \Rightarrow \frac{1}{m-1} \left[1 - mf(n_H)^{m-1} \right] - \lambda_0 - \lambda_1 n_H = 0, \tag{7}$$

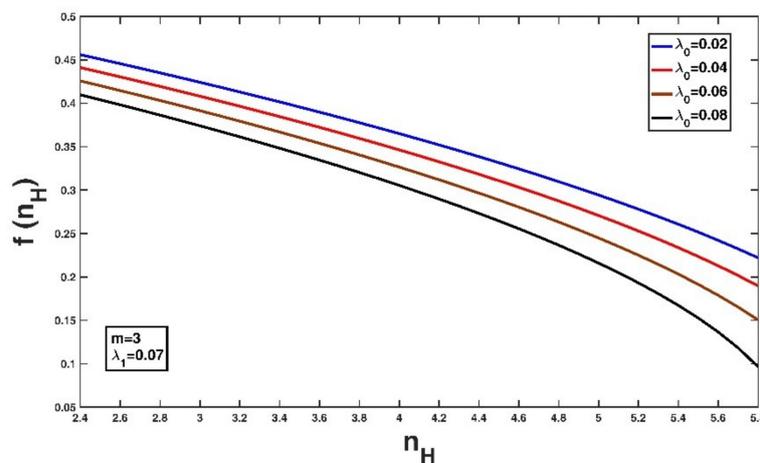
leading to the following expression for $f(n_H)$:

$$f(n_H) = \left[\frac{m-1}{m} \left(\frac{1}{m-1} - \lambda_0 - \lambda_1 n_H \right) \right]^{\frac{1}{m-1}} \tag{8}$$

Assuming some fixed values of Lagrange multipliers, the variation of this probability density function $f(n_H)$ with m is shown in Figure 1a. It can be seen that when m is smaller than 2, $f(n_H)$ decreases almost linearly with the increase in n_H . Keeping one value fixed, the variation of the probability density function $f(n_H)$ with the other Lagrange multipliers is shown in Figure 1b,c. Figure 1b shows the variation of $f(n_H)$ with λ_0 : as λ_0 decreases, $f(n_H)$ tends to increase at a fixed n_H value. Figure 1c shows the variation of $f(n_H)$ with λ_1 : as λ_1 increases, $f(n_H)$ tends to decrease at a fixed n_H .

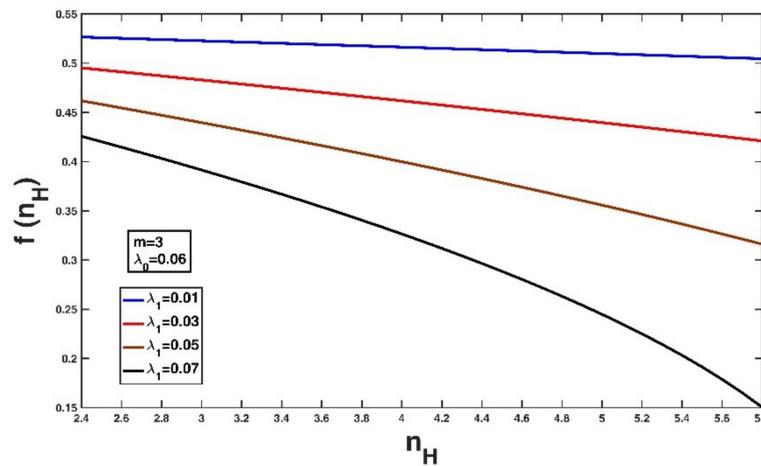


(a)



(b)

Figure 1. Cont.



(c)

Figure 1. Variation of the probability density functions with different m (a), λ_0 (b) and λ_1 (c) when keeping other the values constant.

Thus, the cumulative distribution function (CDF) of $n_H, F(n_H)$, can be obtained by simply integrating Equation (8) from n_0 to n_H as

$$F(n_H) = \left(\frac{m-1}{m}\right)^{\frac{m}{m-1}} \frac{1}{\lambda_1} \left[\left(\frac{1}{m-1} - \lambda_0 - \lambda_1 n_0\right)^{\frac{m}{m-1}} - \left(\frac{1}{m-1} - \lambda_0 - \lambda_1 n_H\right)^{\frac{m}{m-1}} \right] \quad (9)$$

The maximum entropy function $H(n_H)$ is obtained by inserting Equation (8) into Equation (2) as follows:

$$H(n_H) = \frac{1}{m-1} \left\{ (n_1 - n_0) + \left(\frac{m-1}{m}\right)^{\frac{m}{m-1}} \frac{1}{(2m-1)\lambda_1} \times \left[\left(\frac{1}{m-1} - \lambda_0 - \lambda_1 n_1\right)^{\frac{2m-1}{m-1}} - \left(\frac{1}{m-1} - \lambda_0 - \lambda_1 n_0\right)^{\frac{2m-1}{m-1}} \right] \right\} \quad (10)$$

It can be seen from Equations (8)–(10) that all of the probability density functions, the CDF and the entropy function depend on two Lagrange multipliers, λ_0 and λ_1 , which can be determined by the constraint equations.

2.4. Estimation of Lagrange Multipliers

Substituting Equation (8) into Equation (3) can yield

$$\frac{1}{\lambda_1} \left(\frac{m-1}{m}\right)^{\frac{m}{m-1}} \left[\left(\frac{1}{m-1} - \lambda_0 - \lambda_1 n_1\right)^{\frac{m}{m-1}} - \left(\frac{1}{m-1} - \lambda_0 - \lambda_1 n_0\right)^{\frac{m}{m-1}} \right] = 1 \quad (11)$$

whereas by substituting Equation (8) into Equation (4), we obtain

$$\begin{aligned} & n_1 \left(\frac{1}{m-1} - \lambda_0 - \lambda_1 n_1\right)^{\frac{m}{m-1}} - n_0 \left(\frac{1}{m-1} - \lambda_0 - \lambda_1 n_0\right)^{\frac{m}{m-1}} \\ & + \frac{(m-1)}{(2m-1)} \frac{1}{\lambda_1} \left[\left(\frac{1}{m-1} - \lambda_0 - \lambda_1 n_1\right)^{\frac{2m-1}{m-1}} - \left(\frac{1}{m-1} - \lambda_0 - \lambda_1 n_0\right)^{\frac{2m-1}{m-1}} \right] \\ & + \lambda_1 \bar{n}_H \left(\frac{m}{m-1}\right)^{\frac{m}{m-1}} = 0 \end{aligned} \quad (12)$$

It can be seen that Equations (11) and (12) constitute a non-linear equation system for the Lagrange multipliers λ_0 and λ_1 . This equation system can be solved numerically for given values of \bar{n}_H, n_0, n_1 and the entropy index m by virtue of a non-linear equation solver in MATLAB software.

2.5. Hypothesis on the Cumulative Distribution Function

To derive the explicit expression for the exponent of reduction of settling velocity in the real (space) domain, an equation connecting the probability domain to the space domain is needed [29]. Thus, a hypothesis regarding the CDF of the exponent of reduction of the settling velocity should be made so that the hypothesised CDF can reflect the characteristics of n_H . Several previous studies have shown that n_H should be connected to the particle's Reynolds number R , the volumetric concentration of the sediment and the mass density of the sediment [8,12]. In addition to this, the hypothesised CDF should have the following characteristics: (1) it is continuous and differentiable; (2) it is between 0 and 1; and (3) as R becomes large, CDF should approach zero, whereas as R decreases, CDF should approach 1. Although there are many types of CDFs satisfying the aforementioned characteristics, Kumbhakar et al. [13] proposed the following power-type hypothesis regarding the CDF to be an obvious and appropriate choice:

$$F(n_H) = \exp \left[-A \left(\frac{R}{c\Delta_p} \right)^\eta \right], \quad (13)$$

where A and η are two parameters that should be positive real numbers, and $\Delta_p = s - 1$ (here s is the ratio of the mass density of the sediment particles and that of the fluid).

2.6. Derivation of the Expression of n_H

By equating Equations (9) and (13) and using Equation (11), we can obtain the expression for the exponent of reduction of the settling velocity n_H as

$$n_H = -\frac{1}{\lambda_1} \left\{ \left(\frac{1}{m-1} - \lambda_0 - \lambda_1 n_0 \right)^{\frac{m}{m-1}} - \left[\left(\frac{1}{m-1} - \lambda_0 - \lambda_1 n_0 \right)^{\frac{m}{m-1}} - \left(\frac{1}{m-1} - \lambda_0 - \lambda_1 n_1 \right)^{\frac{m}{m-1}} \right] \exp \left[-A \left(\frac{R}{c\Delta_p} \right)^\eta \right] \right\}^{\frac{m-1}{m}} - \frac{\lambda_0}{\lambda_1} + \frac{1}{\lambda_1(m-1)}$$

Equation (14) denotes the Tsallis entropy-based expression for the exponent of reduction of the settling velocity. The hindered settling velocity of a particle in the particle-fluid mixture can be estimated from Equations (1) and (14) for given values of R , c and Δ_p .

3. Comparison with Existing Experimental Data

Eleven experimental data sets regarding the reduction of the settling velocity of the falling particle were collected from the literature to test the validity of the Tsallis entropy-based expression (Equation (14)), including beach sand (Wilhelm and Kwauk [35]), crushed sand (Fouda and Capes [36]), beach sand (Baldock et al. [16]), gravel (Baldock et al. [16]), filter sand (Cleasby and Woods [37]), glass spheres (Baldock et al. [16]), filter sand (Cleasby and Fan [38]), crushed flint (Cleasby and Fan [38]), filter sand (Baldock et al. [16]), crushed rock (Wilhelm and Kwauk [35]) and crushed sand (Jottrand [39]). These collected data are derived from different experiments by various researchers; they contain sand, gravel, glass, flint and crushed rock particles, varying in size d_p from 0.06 to 3 mm and relative mass density of the particle s from 2.50 to 2.65. The data were chosen to cover both low and high particle Reynolds number conditions, R ranging from 0.22 to 1200.

By analysing these observation data, the lower limit, the upper limit and the mean value of the reduction of the settling velocity of the falling particle, n_0 , n_1 , \bar{n}_H can be taken to be 2.40, 5.80 and 3.64, respectively. With these values taken from the collected experimental data, we can solve the non-linear equation system (Equations (11) and (12)) for the Lagrange multipliers λ_0 and λ_1 as $\lambda_0 = 0.06$ and $\lambda_1 = 0.07$ for $m = 3$. The value of $m = 3$ was simply adopted in this study, as adopted by some researchers [21,24,26]. Substituting these values into Equation (14) yields

$$n_H = -14.29 \times \left\{ 0.15 - 0.14 \times \exp \left[-A \left(\frac{R}{c\Delta_p} \right)^\eta \right] \right\}^{\frac{2}{3}} + 6.29. \tag{15}$$

To test the performance of the model developed against the collected experimental data and other models, an error analysis was carried out in this study by calculating the correlation coefficient k , defined as $k = [\text{cov}(m, o) / \sigma_m \sigma_o]^2$, and the normalised root mean square error ($NRMSE$), defined as $NRMSE = \sqrt{\frac{1}{N} \sum_{i=1}^N (m_i - o_i)^2} / (\max\{o_i\} - \min\{o_i\})$, where m and o are the modelled and observed points, respectively, and N is the number of observed experimental points. It was found that the goodness of fit increases when the value of k increases and the value of $NRMSE$ decreases.

Figure 2 shows the comparison of the Tsallis entropy-based expression (Equation (15)) with the collected experimental data, and the values of the fitting parameters A and η are taken as 0.08 and 0.45, respectively, after fitting the model with the experimental data. In Equation (15), the values of Δ_p and c are required. For the eleven collected experimental data sets, most of the falling particles have a relative mass density of 2.65, and $\Delta_p = 1.65$ was thus adopted in this study. Because the collected experimental data sets are for low as well as high suspension concentrations, an average value of $c = 0.2$ is taken for the estimation of n_H in this study. It can be seen from Figure 2 that the Tsallis entropy-based model shows a good agreement with the experimental data with a high coefficient of determination ($k = 0.90$) and a low $NRMSE$ value ($NRMSE = 0.10$).

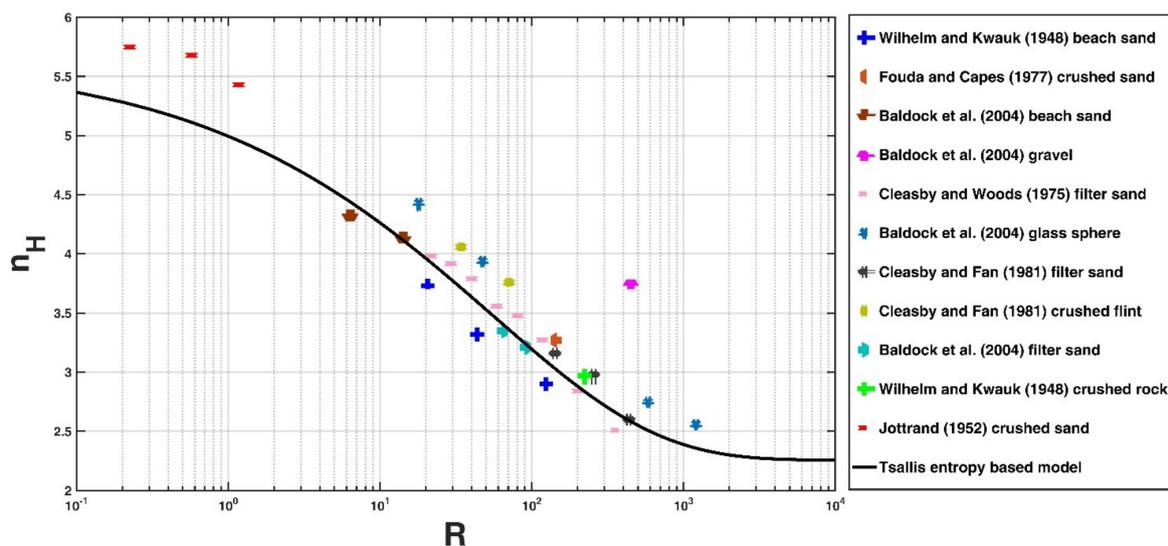


Figure 2. Comparison of the Tsallis entropy-based model (Equation (15)) with the eleven experimental data sets collected.

4. Discussion

4.1. Comparison with other Deterministic Models

Five existing deterministic models for n_H with R in the literature were collected to compare with the developed Tsallis entropy-based model in this study. Table 1 lists the formulations of these models. We compare them with eleven collected experimental data sets regarding the reduction of settling velocity of the falling particle in the literature in Figure 3, as well as the Tsallis entropy-based model developed in this study. The calculated values of k and $NRMSE$ for each model are presented in Table 2. It can be seen from this table that the Tsallis entropy-based model has the highest k value and the lowest $NRMSE$ value compared with the other five deterministic models for all of the collected experimental data, even though most of the models had a high coefficient of determination larger than 0.8. Thus, this study shows the potential of the Tsallis entropy together with the principles of maximum entropy to predict the exponent of reduction of the settling velocity of the particle in a particle–fluid mixture.

Table 1. Formulations of five existing deterministic models for n_H

Model Name	Formulation
Richardson and Zaki [11] model	$n_H = 4.65$, for $R < 0.2$ $n_H = 4.4 \times R^{-0.03}$, for $0.2 < R < 1$ $n_H = 4.4 \times R^{-0.1}$, for $1 < R < 500$ $n_H = 2.4$, for $R > 500$
Garside and Al-Dibouni [14] model	$n_H = \frac{5.1 + 0.27 \times R^{0.9}}{1 + 0.1 \times R^{0.9}}$
Chien and Wan [15] model	$n_H = 4.91$ at low R n_H is determined by graphical curve at moderate R $n_H = 2.25$ at high R
Cheng [12] model	$n_H = \frac{\ln\left(\frac{2-2c}{2-3c}\right) + 1.5 \times \ln\left\{\frac{-5 + \sqrt{25 + \left[\frac{(1-c)(2-3c)^2}{4+4\Delta_p c}\right]^{\frac{2}{3}} \left(R^{\frac{4}{3}} + 10 \times R^{\frac{2}{3}}\right)}}{-5 + \sqrt{25 + R^{\frac{4}{3}} + 10 \times R^{\frac{2}{3}}}}\right\}}{\ln(1-c)}$
Pal and Ghoshal [8] model	$n_H = \frac{\frac{4}{3} \times \ln(1-c) - \ln\left(1 - \frac{c}{c_{\max}}\right) + 3 \times \ln f - \frac{7}{8} \times \ln\left(\frac{38.1 + 5.74 \times f^{\frac{12}{7}} R^{\frac{4}{7}}}{38.1 + 5.74 \times R^{\frac{4}{7}}}\right)}{\ln(1-c)}$, where $f = \left[\frac{(1+\Delta_p)(1-c)^{\Delta_p} - 1}{\Delta_p} \left(1 - \frac{c}{c_{\max}}\right)^2 (1-c)^{-1}\right]^{\frac{1}{3}}$, c_{\max} is the maximum volumetric concentration of suspended particle

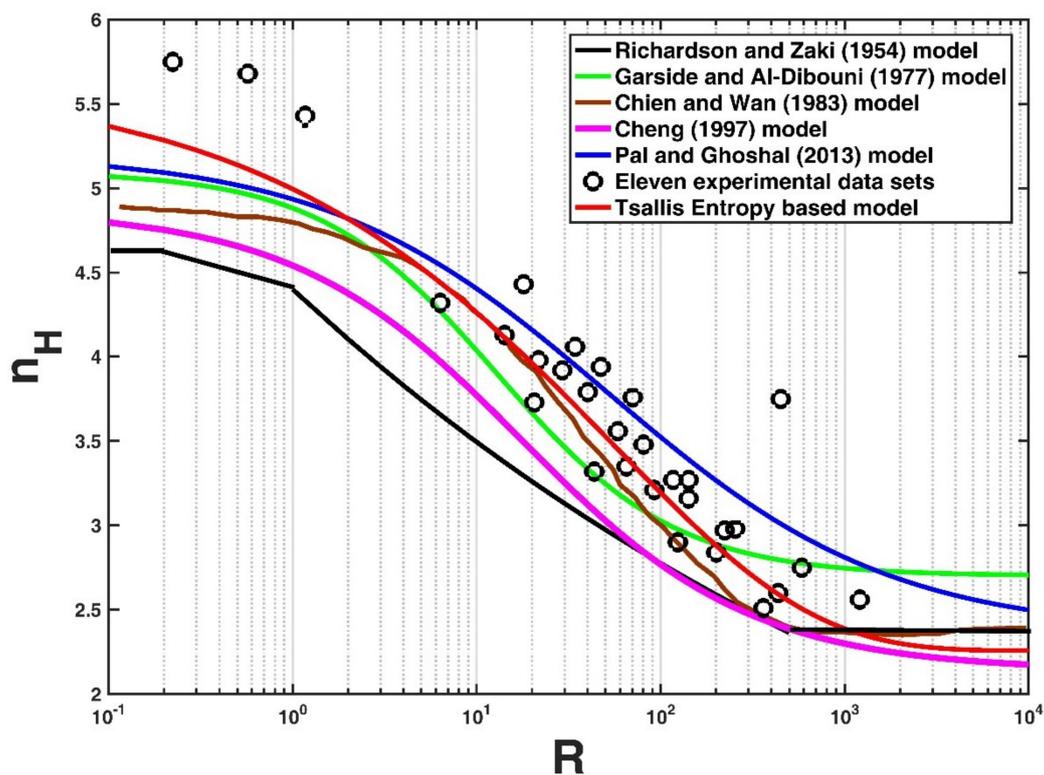


Figure 3. Comparison of five existing deterministic models for n_H with R using the eleven experimental data sets collected.

Table 2. Error analysis between five existing deterministic models and the eleven experimental data sets collected.

Model Name	k	$NRMSE$
Richardson and Zaki [11] model	0.88	0.22
Garside and Al-Dibouni [14] model	0.87	0.15
Chien and Wan [15] model	0.81	0.15
Cheng [12] model	0.88	0.21
Pal and Ghoshal [8] model	0.86	0.14
The Tsallis entropy-based model	0.90	0.10

4.2. Comparison with the Shannon Entropy-Based Model

We also attempted to compare the Tsallis entropy-based model with the Shannon entropy-based model proposed by Kumbhakar et al. [13] for the collected experimental data in this study, as shown in Figure 4. The calculated value of k and $NRMSE$ for the Shannon entropy-based model proposed by Kumbhakar et al. [13] are 0.90 and 0.08 respectively. Comparing the values of k and $NRMSE$ corresponding to the Tsallis entropy and the Shannon entropy, respectively, we can conclude that the Tsallis entropy developed in this study is comparable to the Shannon entropy-based model for predicting the hindered settling velocity of a falling particle in a particle-fluid mixture.

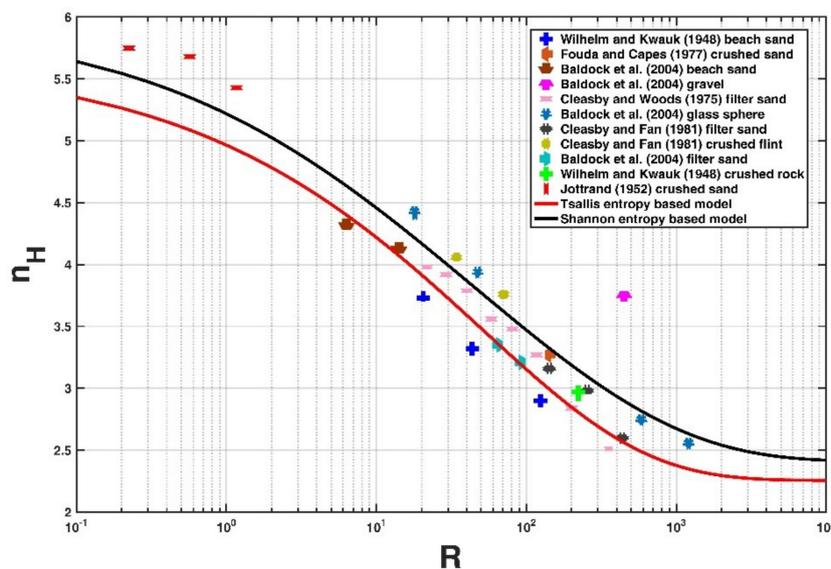


Figure 4. Comparison of the Shannon entropy-based model with the eleven experimental data sets collected, as well as the Tsallis entropy-based model in this study.

4.3. Estimation of the Hindered Settling Velocity

Substituting Equation (15) into Equation (1) and fitting the values of A and η , we can obtain the hindered settling velocity of a falling particle in the particle-fluid mixture as follows:

$$\frac{\omega_m}{\omega} = (1 - c)^{-14.29 \times \{0.15 - 0.14 \times \exp[-0.08(\frac{R}{c\Delta\rho})^{0.45}]\}}^{\frac{2}{3}} + 6.29 \tag{16}$$

Regarding the settling velocity of the sediment particle in a clear fluid ω , Song et al. [40] proposed the following expression,

$$\omega = \frac{v_0}{d_p} d_*^3 \left(38.1 + 0.93 \times d_*^{\frac{12}{7}} \right)^{-\frac{7}{8}}, \tag{17}$$

where d_* is the non-dimensional particle diameter and can be written as $d_* = \left(\frac{\Delta p g}{\rho_0}\right)^{\frac{1}{3}} d_p$, which shows good agreement with the experimental data. Substituting Equation (17) into Equation (16) leads to the expression for the hindered settling velocity of a falling particle in the particle-fluid mixture as follows:

$$\omega_m = \frac{v_0}{d_p} d_*^3 \left(38.1 + 0.93 \times d_*^{\frac{12}{7}}\right)^{-\frac{7}{8}} (1 - c)^{-14.29} \times \left\{ 0.15 - 0.14 \times \exp \left[-0.08 \frac{d_*^{\frac{27}{20}} (38.1 + 0.93 \times d_*^{\frac{12}{7}})^{\frac{12}{9}} - \frac{63}{160}}{(c \Delta p)^{\frac{20}{9}}} \right] \right\}^{\frac{2}{3}} + 6.29 \quad (18)$$

Seven experimental data sets of the settling velocity of Baldock et al. [16] as also presented in the work of Kumbhakar et al. [13], including four data sets of glass particles of various sizes, two sets of beach sand of different sizes, and a set of gravel particles, are adopted in this study to test the validity of Equation (18). Figure 5 shows the comparison results between Equation (18) and each experimental data set, as well as the Shannon entropy-based model proposed by Kumbhakar et al. [13]. Table 3 presents the calculated values of k and $NRMSE$ for each case. It could be found that both Equation (18) and the Shannon entropy-based model have a good agreement with the observed values. For five cases of $d_p = 0.35$ mm, 0.5 mm, 1.85 mm, 0.22 mm and 0.32 mm, Equation (18) has a slightly high prediction accuracy for data sets than the Shannon entropy-based model, whereas the Shannon entropy-based model could provide better results than Equation (18) for two cases of $d_p = 3$ mm, and 2.42 mm. These show the potential of the proposed Tsallis entropy-based expression, as well as the developed Shannon entropy-based model, to predict the hindered settling velocity of a falling particle in the particle-fluid mixture, as an addition to existing deterministic models.

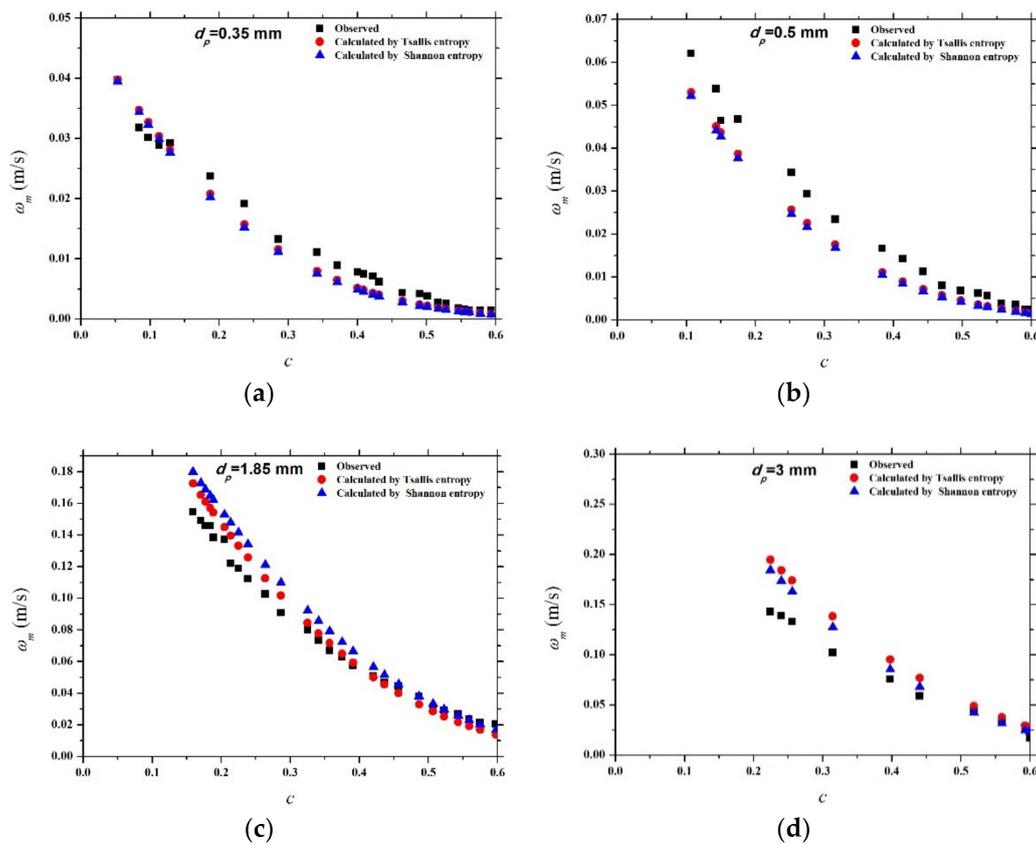


Figure 5. Cont.

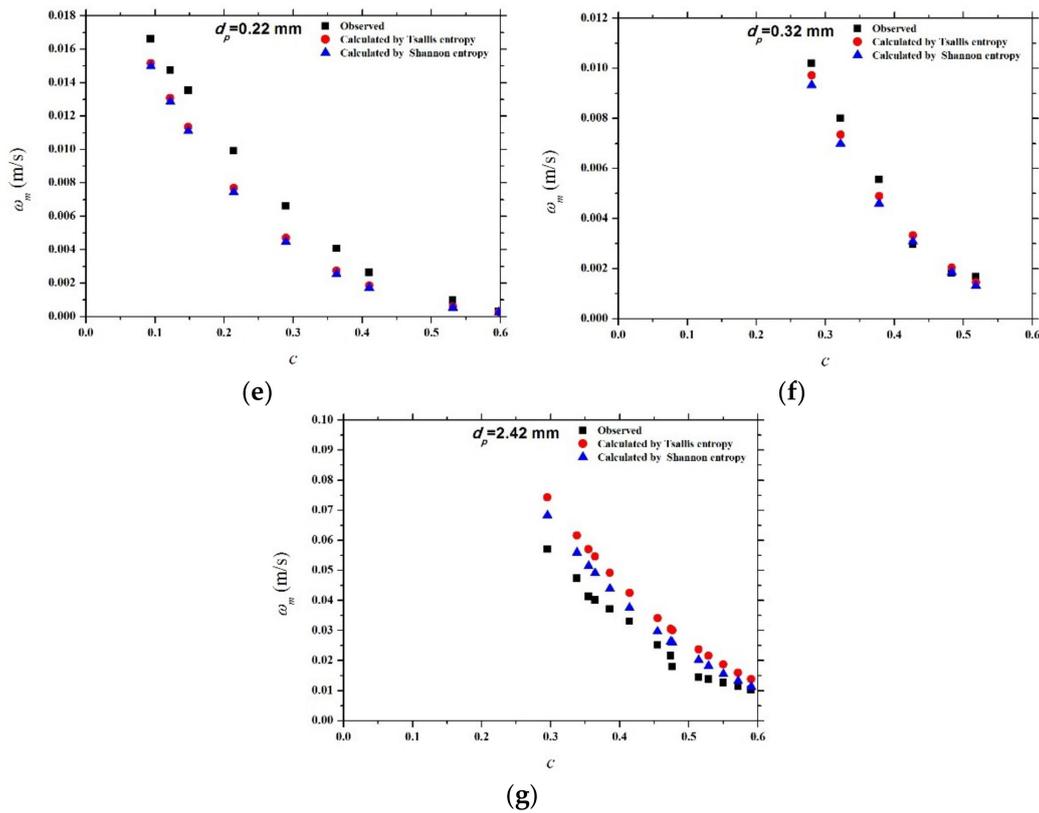


Figure 5. Comparisons between the observed hindered settling velocity values and the calculated settling velocity values based on the Tsallis entropy, as well as the Shannon entropy-based model, for glass particles with particle sizes 0.35 mm (a), 0.5 mm (b), 1.85 mm (c) and 3 mm (d), beach sand with particle sizes 0.22 mm (e), 0.32 mm and (f), gravel with a particle size of 2.42 mm (g).

Table 3. Error analysis between the observed settling velocity values and the calculated settling velocity values by the Tsallis entropy and the Shannon entropy.

Experimental Data Sets	Model Name	<i>k</i>	<i>NRMSE</i> ($\times 10^{-2}$)
$d_p = 0.35\text{mm}$	Tsallis entropy-based model	9.840	5.163
	Shannon entropy-based model	9.835	5.683
$d_p = 0.5\text{mm}$	Tsallis entropy-based model	9.890	8.484
	Shannon entropy-based model	9.851	9.498
$d_p = 1.85\text{mm}$	Tsallis entropy-based model	9.977	7.193
	Shannon entropy-based model	9.971	10.770
$d_p = 3\text{mm}$	Tsallis entropy-based model	9.953	23.350
	Shannon entropy-based model	9.944	17.200
$d_p = 0.22\text{mm}$	Tsallis entropy-based model	9.913	9.287
	Shannon entropy-based model	9.892	10.460
$d_p = 0.32\text{mm}$	Tsallis entropy-based model	9.966	5.470
	Shannon entropy-based model	9.954	8.093
$d_p = 2.42\text{mm}$	Tsallis entropy-based model	9.908	20.070
	Shannon entropy-based model	9.914	13.960

Figure 6 shows the variation of the non-dimensional hindered settling velocity expression ω_m/ω (Equation (16)) with R for different values of c . Here, the falling particle is fixed at $\Delta_p = 1.65$. It can be seen that for a given falling particle, the particle settles much more slowly in a high concentration suspension compared to a low concentration suspension. This could be attributed to three reasons: (1) return flow—a falling particle will generate a return flow, for other particles in the vicinity of this falling particle; they are always located within this return flow and thus their settling velocities will be affected; (2) viscosity—the effective viscosity of the suspension will increase with particle concentration;

and (3) buoyancy or reduced gravity—the particle settles in the remainder of the suspension with an increased bulk density, and thus the settling velocity decreases, as shown by Winterwerp [9].

Fixing d_p at 0.35 mm, Figure 7 shows the variation of the dimensional hindered settling velocity model ω_m (Equation (18)) with c for different values of Δ_p . It can be observed that for a falling particle due to a given size, a heavy particle settles more rapidly in the particle-fluid mixture than a light particle due to a stronger gravity. Fixing Δ_p at 1.5, Figure 8 shows the variation of the dimensional hindered settling velocity model ω_m (Equation (18)) with c for different values of d_p . It can be seen that for a falling particle of a given mass density, a large particle settles faster in the mixture than a small particle due to a greater gravity.

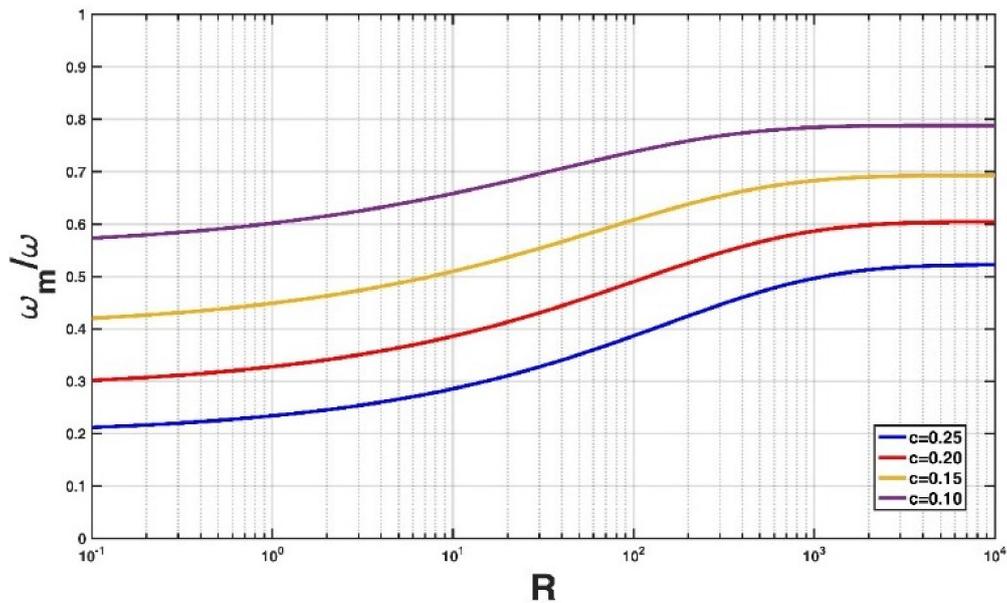


Figure 6. Variation of the non-dimensional hindered settling velocity model (Equation (16)) with R for different values of c .

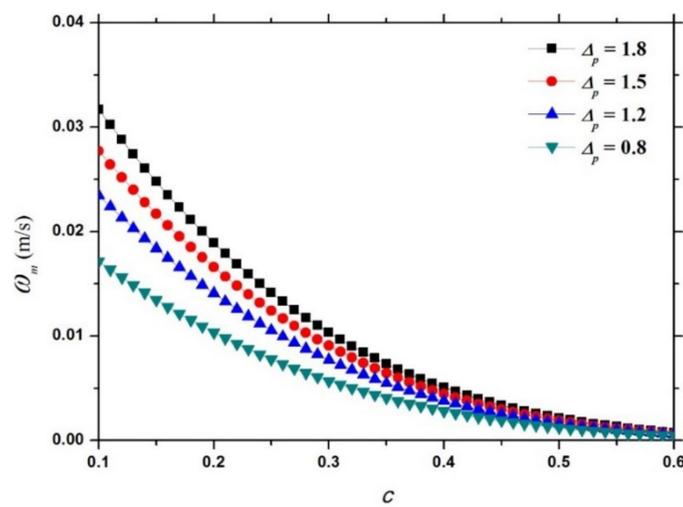


Figure 7. Variation of the dimensional hindered settling velocity model (Equation (18)) with c for different values of Δ_p .

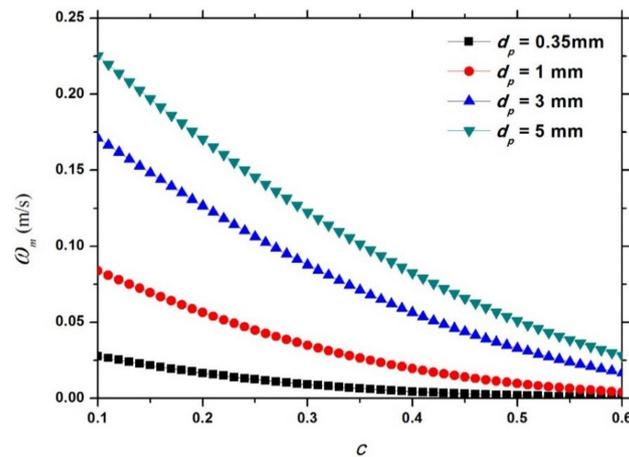


Figure 8. Variation of the dimensional hindered settling velocity model (Equation (18)) with c for different values of d_p .

Equation (16) provides a new expression for the hindered settling velocity of a falling particle in the particle-fluid mixture based on the Tsallis entropy theory. This expression has a simple mathematical form, contains fewer parameter inputs compared with other deterministic models such as the model of Cheng [12] and the model of Pal and Ghoshal [8] as presented in Table 1. However, it should be noted that some physical properties present in some existing deterministic models are not incorporated into the developed Tsallis entropy-based expression. For example, the effect of the suspension concentration on the kinematic viscosity of the sediment-fluid mixture has been incorporated into the model of Pal and Ghoshal [8], which introduced the maximum volumetric concentration of the suspended particle c_{\max} . However, the entropy-based expression does not contain this parameter.

5. Conclusions

This study attempts to derive an expression for the exponent of reduction of the settling velocity of a falling particle in a particle-fluid system based on the Tsallis entropy theory together with the principle of maximum entropy. The function of the exponent of the reduction of the settling velocity is derived by assuming that this exponent is a random variable, maximizing the Tsallis entropy function subject to two constraint equations and using the hypothesis regarding the cumulative distribution function of this exponent. The derived expression is a function of the volumetric concentration of the suspended particle, the relative mass density of the particle, and the particle's Reynolds number.

The Tsallis entropy-based expression is tested against eleven collected experimental data sets. Error analysis indicates that the model has a good agreement with the experimental data. The model is also compared with five existing deterministic models for the collected experimental data, and it shows better prediction accuracy compared to other deterministic models. Furthermore, the derived model is also compared with the existing Shannon entropy-based model for the collected experimental data, and the Tsallis entropy is comparable to the Shannon entropy-based model for predicting the hindered settling velocity of a falling particle in a particle-fluid mixture. Finally, an empirical expression for the hindered settling velocity is proposed, which shows high prediction accuracy for the experimental data regarding the hindered settling velocity. This study indicates the potential of using Tsallis entropy together with the principle of maximum entropy to predict the hindered settling velocity of a falling particle in a particle-fluid mixture.

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