

Article

## Co-Al Mixed Oxides Prepared via LDH Route Using Microwaves or Ultrasound: Application for Catalytic Toluene Total Oxidation

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**Abstract:** Co<sub>6</sub>Al<sub>2</sub>HT hydrotalcite-like compounds were synthesized by three different methods: co-precipitation, microwaves-assisted and ultrasound-assisted methods. The mixed oxides obtained after calcination were studied by several techniques: XRD, TEM, H<sub>2</sub>-TPR and XPS. They were also tested as catalysts in the reaction of total oxidation of toluene. The physico-chemical studies revealed a modification of the structural characteristics (surface area, morphology) as well as of the reducibility of the formed mixed oxides. The solid prepared by microwaves-assisted synthesis was the most active. Furthermore, a relationship between the ratio of Co<sup>2+</sup> on the surface, the reducibility of the Co-Al mixed oxide and the T<sub>50</sub> in toluene oxidation was demonstrated. This suggests a Mars Van Krevelen mechanism for toluene total oxidation on these catalysts.

**Keywords:** mixed oxide; LDH; microwaves; ultrasound; toluene; catalytic oxidation

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## 1. Introduction

The emissions of Volatile Organic Compounds (VOCs) in industrial activities are now strictly regulated due to their harmfulness towards public health and the atmospheric environment. Among the many technologies available for VOCs control, catalytic oxidation of these pollutants to carbon dioxide and water has been recognized as one of the most promising ones. Supported noble metals are generally considered as efficient catalysts for VOCs oxidation [1–5] and their efficiency at low temperature can sometimes be considered as a key advantage favoring the use of such catalysts compared with mixed oxide catalysts. However, due to the high cost of noble metals, many researchers have recently devoted strong efforts to the development of suitable catalysts containing only transition metal oxides [6–10]. In this domain, special attention has been focused on cobalt materials in the spinel form [10], on oxide catalysts [11,12] and on mixed oxides issued from hydrotalcite precursors [13,14]. For the generation of well-dispersed, active and very stable mixed oxides, the Layered Double Hydroxides (LDH) route shows much potential. Indeed, LDH, also referred to as hydrotalcite-like compounds, constitute a large group of natural and synthetic minerals whose physico-chemical properties have strong analogies with clay minerals and more particularly with cationic clay minerals. This class of layered double hydroxides consists of positively charged metal hydroxide layers separated from each other by anions and water molecules. The wide range of possible cations and anions that can be incorporated in the Hydrotalcite (HT) structure gives rise to a large number of materials [7,13,14]. In addition, a high surface area, a good thermal stability, a good mixed oxides homogeneity, basic properties and a high metal dispersion are obtained after thermal treatment [10,15].

The interest in applying calcined LDH as catalysts in the environmental field has already been demonstrated. For example, mixed oxides have been shown to be very active and selective in the decomposition of nitrogen oxides [16] or in the total oxidation of Volatile Organic Compounds [13,14]. Also, mixed oxides obtained after calcination were used equally as catalysts [13,17] or as catalytic support [18–20] in redox reactions such as the selective oxidation of hydrocarbons or the total oxidation of VOCs [21,22].

The conventional and most widely used method to prepare LDH is co-precipitation [7,8,13,14]. However, alternative methods providing well-crystallized materials have also been studied [23,24]. In particular, the use of microwaves during the synthesis of catalytic materials presented several advantages over conventional methods. Thus, Ran *et al.* [24] have synthesized ternary oxides of  $\text{La}_{0.7}\text{Sr}_{0.3}\text{MnO}_{3+\lambda}$  using microwaves and they have highlighted the benefits of this synthesis method, compared to conventional sol-gel synthesis, in terms of rapidity (3–5 min compared to several hours), energy efficiency, uniformity of heating (no hot spot in the solution), homogeneity of the obtained solid (larger specific surface area and small particle sizes). Kaddouri *et al.* [25] showed that a  $\text{La}_{1-x}\text{B}_x\text{MnO}_{3.15}$  perovskite type solid synthesized under microwaves exhibit better catalytic properties than the same solid synthesized conventionally. Similarly, the use of ultrasounds in the synthesis of material was reported to be beneficial due to the phenomenon of acoustic cavitation that corresponds to the formation, growth and collapse of bubbles generated in the solution. Zhou *et al.* [26] performed the impregnation of zirconium and cobalt supported on  $\text{SiO}_2$  ( $\text{Co/Zr/SiO}_2$ ) with sonication and they noted that ultrasounds increase the specific surface area and lead to a better dispersion of the cobalt particles on the substrate surface due to such cavitation effects. Similar cavitation phenomena have allowed obtaining a better

catalytic reactivity of solids in the Fischer-Tropsch reaction. Recently, microwaves radiation heating [27–29] and ultrasound [27,30,31] have been applied to the synthesis of hydrotalcites with different chemical compositions as an alternative to the conventional hydrothermal treatments. Several of the advantages listed above have been observed, especially the shorter treatment times needed to achieve enhanced crystallinity degrees, the higher specific surface area and the improved metallic dispersions [28,32,33].

A previous study in our laboratory has shown that Co-Al mixed oxide catalysts present interesting catalytic activity for total oxidation of toluene [13]. In order to improve this type of catalytic materials, the aim of the present work was to investigate the effect of treatment by microwaves or by ultrasound during the preparation of the LDH samples. Thus, mixed oxides were prepared by calcination of hydrotalcite like compounds precursors (Co<sub>6</sub>Al<sub>2</sub>HT and Mg<sub>6</sub>Al<sub>2</sub>HT) using three different routes (microwaves (MW), ultrasound (US) and conventional treatment (CT)) and the catalytic properties of the samples were tested in the total oxidation of toluene. The mixed oxide properties were also characterized by several techniques: powder X-ray Diffraction (XRD), Transmission Electron Microscopy (TEM) Hydrogen Temperature Programmed Reduction (H<sub>2</sub>-TPR) and X-ray photoelectron spectrometry (XPS).

## 2. Results and Discussion

Table 1 indicates the code names and the specific surface areas of the mixed oxides obtained after calcination of the hydrotalcite precursors. With the aim to study the effect of the preparation method, the cobalt-based materials are compared in this table to reference Mg-Al-O materials having more conventional hydrotalcite compositions but synthesized following the same protocols as those used for the preparation of the Co-Al mixed oxides. Compared to the samples prepared by coprecipitation, a significant increase of the specific surface area is observed when the mixed oxides were prepared using either the US or the MW method. This result was already reported in the literature [28,30,31]. Indeed, Neto *et al.* [31] have shown on LDH synthesis by sonication that ultrasounds not only accelerate crystal formation but also better disperse small particles, thus reducing their aggregation during nucleation and crystal growth and giving rise to increased specific surface area. Moreover, concerning the effect of microwaves during the LDH preparation, it was observed that MW radiation for short time leads to faster nucleation, which produces a larger number of small crystals and therefore an increase of the surface area [28]. Thus, the treatment by microwaves or by ultrasounds during synthesis improves the specific area of the obtained materials.

Table 1 also reports the chemical compositions of the solids. It can be clearly seen that the ratio  $M^{2+}/Al^{3+} = 3$  is well respected for each solid. The  $T_{50}$  values reported as well in Table 1 (temperature at which 50% of the toluene is converted) show that the catalytic performances of the samples in toluene total oxidation follow the order:

$$Co_6Al_2HTMW500 > Co_6Al_2HTUS500 > Co_6Al_2HTCT500 >> Mg_6Al_2HTMW500 > Mg_6Al_2HTUS500 > Mg_6Al_2HTCT500 \quad (1)$$

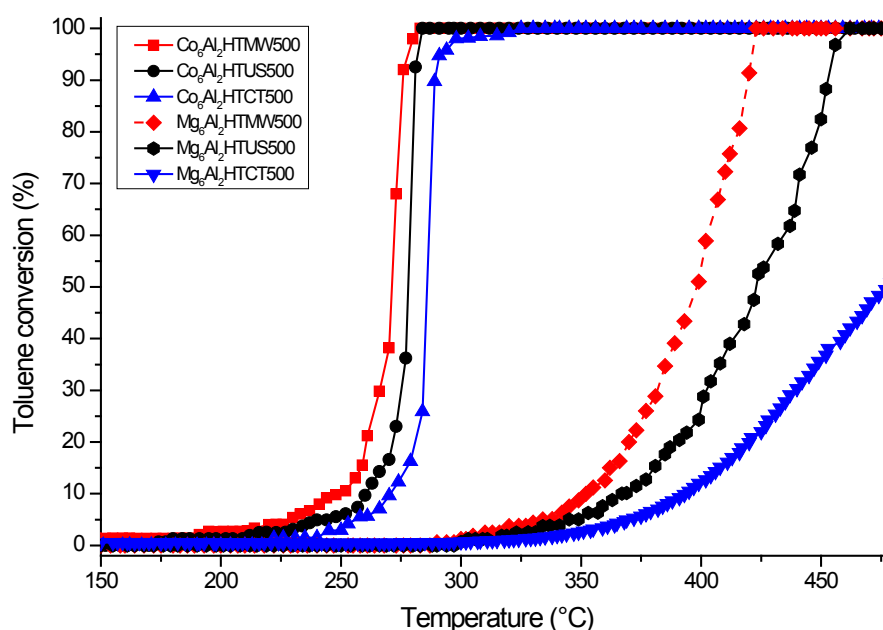
This order is also illustrated in Figure 1 that shows the evolution of the conversion levels as a function of the temperature. From these data, it can be concluded that the replacement of the bivalent cation  $Mg^{2+}$

by  $\text{Co}^{2+}$  in the chemical composition of sample has a significant effect. This observation is in line with a previous work [13] that indicated the importance of the nature of the bivalent cation in the sample. Moreover, an increase of the catalytic activity is clearly observed for the solids prepared by microwaves or ultrasounds methods.

**Table 1.** Code name, BET specific area, chemical composition, crystallite size and temperature of 50% toluene conversion ( $T_{50}$ ) of catalysts.

Solids	Specific surface area ( $\text{m}^2 \cdot \text{g}^{-1}$ )	Chemical composition $\text{M}^{2+}/\text{Al}^{3+}$		$T_{50}$ ( $^{\circ}\text{C}$ )	Crystallite size of oxide * (nm)
		Theoretical	Experimental		
$\text{Mg}_6\text{Al}_2\text{HTCT500}$	216	3	2.79	477	11.6
$\text{Mg}_6\text{Al}_2\text{HTUS500}$	272	3	2.84	421	4.5
$\text{Mg}_6\text{Al}_2\text{HTMW500}$	342	3	2.95	395	3.7
$\text{Co}_6\text{Al}_2\text{HTCT500}$	123	3	2.85	287	9.4
$\text{Co}_6\text{Al}_2\text{HTUS500}$	157	3	3.15	278	7.0
$\text{Co}_6\text{Al}_2\text{HTMW500}$	167	3	3.00	271	7.6

\* Estimated by the XRD measurement.

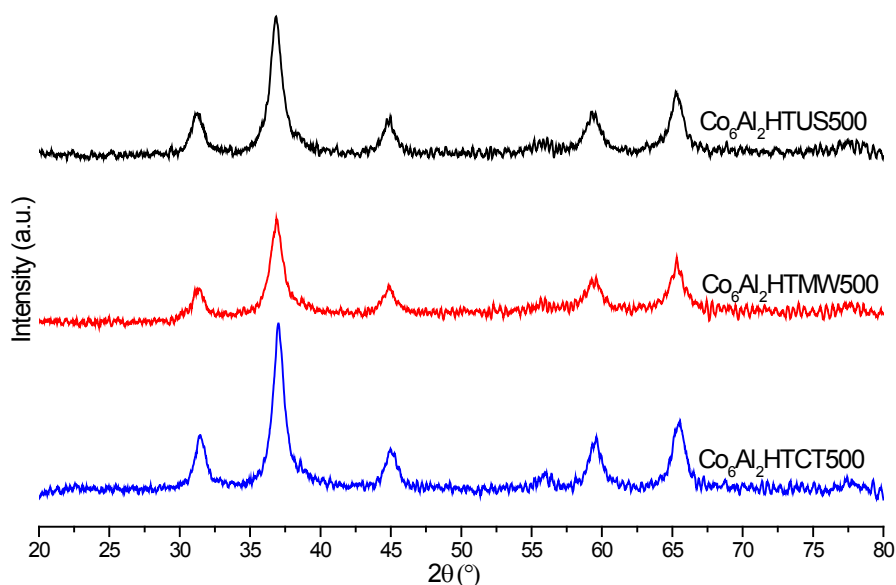


**Figure 1.** Conversion of toluene (%) on mixed oxide vs. reaction temperature ( $^{\circ}\text{C}$ ).

When toluene conversion was complete,  $\text{H}_2\text{O}$  and  $\text{CO}_2$  were the only products observed. However, during toluene conversion at lower temperatures on all samples, few ppm of benzene and CO were detected. Different reaction paths have been already recognized [34]. The most important reaction route is the one initiated by attack on the methyl group with subsequent oxidation steps; however, direct dealkylation of toluene into benzene is possible.

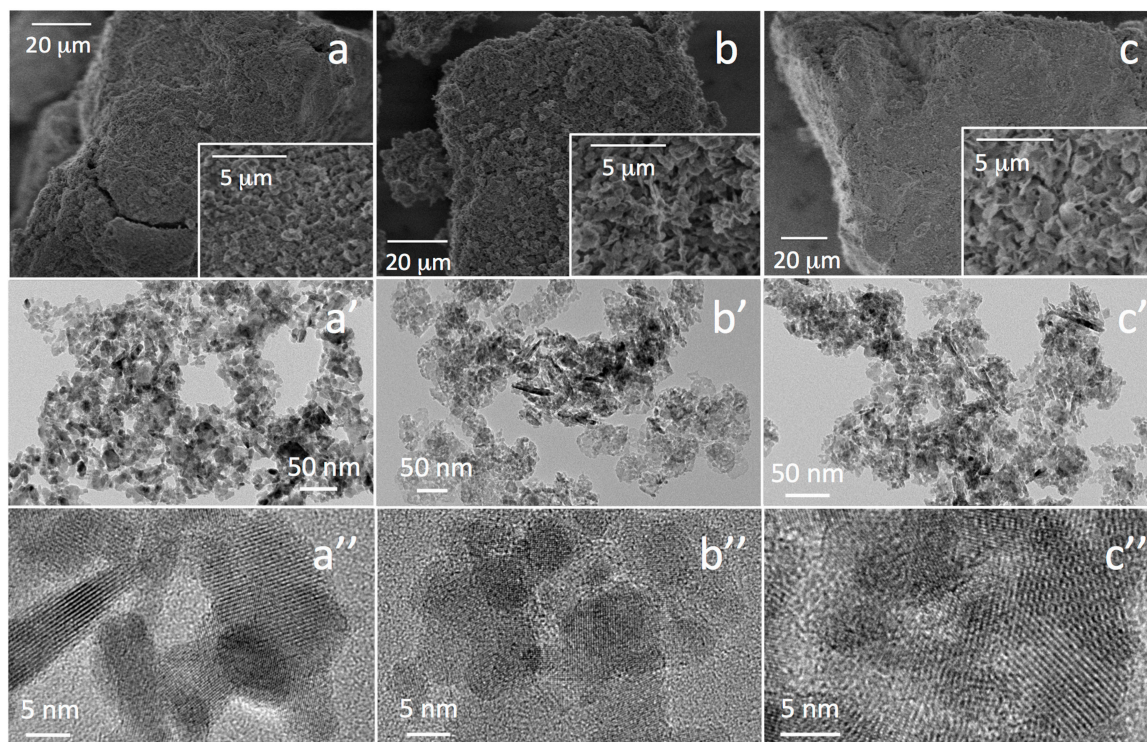
For a better understanding of the effect of these preparation methods on the catalysts, physico-chemicals characterizations of the Co-Al mixed oxides were performed. Firstly, XRD was done to investigate the structure of the samples. The X-ray diffraction patterns (Figure 2) reveal several crystalline spinel phases. These spinel phases are divided into two groups: the spinel phase of cobalt (II)

and cobalt (III) ( $\text{Co}_3\text{O}_4$  (JCPDS-ICDD 42-1467)) and cobalt aluminum spinel  $\text{CoAl}_2\text{O}_4$  phases (JCPDS-ICDD 44-0160) and  $\text{Co}_2\text{AlO}_4$  (JCPDS-ICDD 38-0814). The presence of the first phase ( $\text{Co}_3\text{O}_4$ ) is due to the easy oxidation of  $\text{Co}^{2+}$  to  $\text{Co}^{3+}$  in contact with the air and the greater thermodynamic stability of this phase compared to  $\text{CoO}$  [35]. However, the three diffraction patterns of these three spinel phases are very similar in position and in intensity [36–38]. For this reason, it is not possible to differentiate the phases by XRD. The Co-Al mixed oxide leads to the normal spinel, *i.e.*,  $\text{CoAl}_2\text{O}_4$  corresponding to the  $\text{Co}^{2+}$  in the tetrahedral positions and the  $\text{Al}^{3+}$  in the octahedral position. However, a slight decrease in the crystallite size of the oxide is observed for solids prepared using the microwaves or ultrasound methods (Table 1).



**Figure 2.** X-ray diffraction patterns of the mixed oxides.

In order to investigate the morphology of the samples prepared via the three different routes, TEM analysis was performed. From the representative micrographs shown in Figure 3, some morphological differences can be observed depending on the cobalt based mixed oxide. Firstly, the SEM images show that the three samples are formed of agglomerates (with sizes in the mm range), themselves composed of an aggregation of very small particles. As seen by both SEM (Figure 3a–c) and TEM (Figure 3a'–c') images, the size of these individual particles is bigger and less regular in the solid resulting from the conventional synthesis. By contrast, the other two samples have a sharper size distribution of grains with more uniform particle sizes, less than 10 nm. Moreover, the grains appear much thinner, especially in the case of  $\text{Co}_6\text{Al}_2\text{HTMW500}$  (see insets in SEM images). These observations are consistent with the assessment of the crystallite size made during the XRD analysis (Table 1). Moreover, the HR-TEM images confirm that all three samples are composed of grains with crystalline structure. Finally, the various TEM images suggest a difference in porosity among the three samples, being more important on the solid resulting from both the Ultrasonic and microwave assisted syntheses compared to the solid issued from the conventional route.



**Figure 3.** (a–c) SEM; (a'–c') TEM and (a''–c'') HR-TEM images of samples of (a,a',a'') Co<sub>6</sub>Al<sub>2</sub>HTCT500, (b,b',b'') Co<sub>6</sub>Al<sub>2</sub>HTUS500 and (c,c',c'') Co<sub>6</sub>Al<sub>2</sub>HTMW500.

Regarding the grains morphology, each grain has solid elliptical shapes of larger or smaller size. However, in the case of solids issued from unconventional syntheses, the presence of elongated grains forms (“rods”) is observed. This form of grain may be due to two factors: the orientation of the grain in the analysis is perpendicular to the plane or the grain has “rod” type morphology. Such rod shape morphology has been already observed in the literature for solid cobalt oxide (Co<sub>3</sub>O<sub>4</sub>) [39,40] and it has been interestingly related to samples having good performances in the oxidation of carbon monoxide at low temperatures.

Analysis of the samples by Temperature-Programmed Reduction (H<sub>2</sub>-TPR) was next performed (Figure 4). The reduction profile has a similar shape for the three samples but the reduction temperature of samples slightly differs depending on the preparation method of the solid. Indeed, the solid resulting from the synthesis with microwaves is reduced at lower temperatures. In order to identify more specifically the reduction peaks, deconvolution of these peaks using Gaussian-type components was done. This peak deconvolution (Figure 4), with a correlation factor greater than 0.999, reveal that the reduction of Co<sub>6</sub>Al<sub>2</sub>HT500 consists of two steps at low temperatures ( $T < 400$  °C) for the Co<sub>3</sub>O<sub>4</sub> species and three steps at high temperature ( $T > 400$  °C) for cobalt/aluminum spinel species [39,41–43].

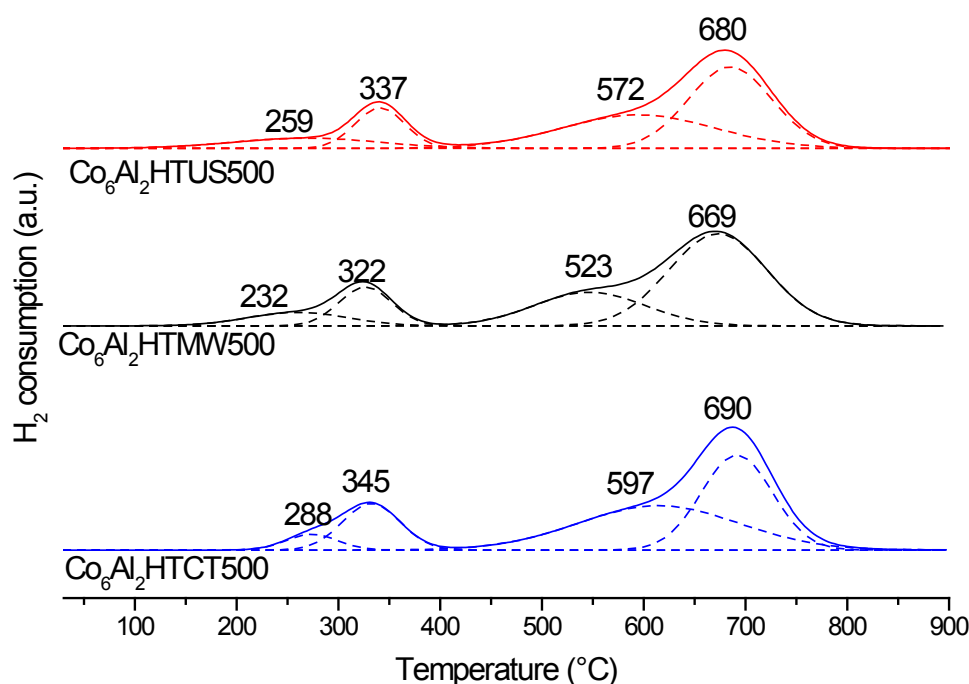
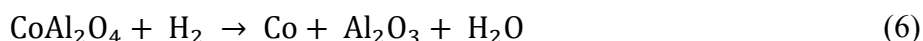
At  $T < 400$  °C



At  $T > 400$  °C







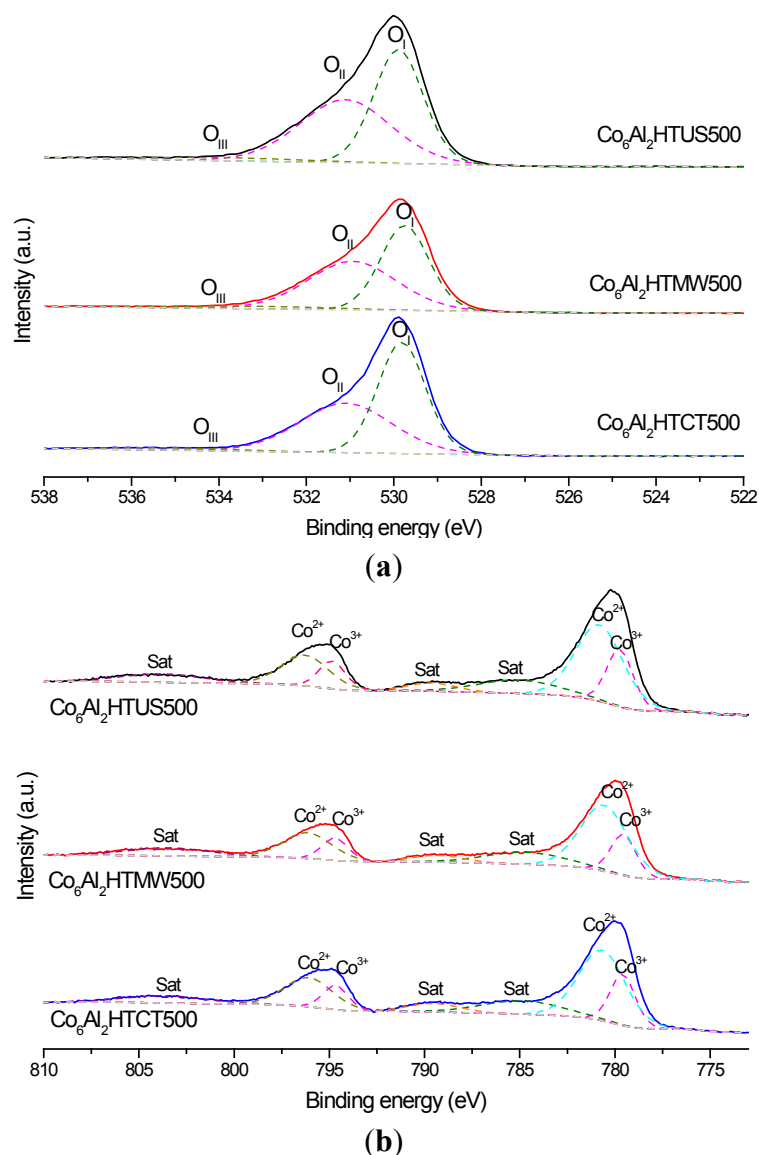
**Figure 4.** H<sub>2</sub>-TPR profiles of the mixed oxides.

For the three solids, a distinction between the two reduction stages of Co<sub>3</sub>O<sub>4</sub> is possible. Similar discrimination was done earlier by Moulijn and Arnoldy [41] and explained by the reduction of Co<sub>3</sub>O<sub>4</sub> into CoO phase at around 240 °C. Then, the second peak (at 330 °C) corresponds to the reduction of either the CoO phase into Co<sup>0</sup> or of Co<sub>3</sub>O<sub>4</sub> into Co<sup>0</sup> [39,41–43]. Regarding the reduction of species at higher temperatures ( $T > 400$  °C), only a limited change in the shape of the profiles is observed. The observation of three stages of reduction is more difficult because they are in the same temperature range. Indeed, a smaller reduction temperature is observed in the case of the solids synthesized using microwaves or ultrasound. Cook *et al.* [44] showed the importance of the crystallite size for the reduction step. Thus, when the crystallite size decreases, the reducibility takes place at lower temperature. The consumption for all peaks is reported into Table 2. The stoichiometry of the first steps ( $T < 400$  °C) predicts a ratio equal to 3 for the consumption ratio peak 2/1. This ratio is respected for all samples, which confirms the hypothesis for the chemical equation. Concerning the second step, it is difficult to distinguish the three steps due to the position in the same temperature range. So, for the quantitative study, the first step (Co<sub>2</sub>AlO<sub>4</sub> → CoAl<sub>2</sub>O<sub>4</sub> and CoO) corresponds to Peak 3 and the last two correspond to Peak 4. The ratio between Peaks 4 and 3 is equal to 5 which is in accordance with the literature [39,41–44].

**Table 2.** Temperatures for H<sub>2</sub> consumptions by TPR experiments Co<sub>6</sub>Al<sub>2</sub>HT500 issued from different preparation methods.

Catalyst	Temperature (°C)				Consumption ratio peak 2/1	Consumption ratio peak 4/3	H <sub>2</sub> consumption (μmol·g <sup>-1</sup> )
	Peak 1	Peak 2	Peak 3	Peak 4			
Co <sub>6</sub> Al <sub>2</sub> HTCT500	288 °C 644	345 °C 2012	597 °C 1458	690 °C 7410	3.12	5.08	11715
Co <sub>6</sub> Al <sub>2</sub> HTUS500	259 °C 651	337 °C 2192	572 °C 1557	680 °C 7444	3.36	4.78	11845
Co <sub>6</sub> Al <sub>2</sub> HTMW500	232 °C 777	322 °C 2242	523 °C 1229	669 °C 7711	2.88	4.69	11961

The cobalt based catalysts were also characterized by XPS in order to examine the effect of the preparation method on the nature and the oxidation degrees of the surface species. The XPS spectra of O 1s and Co 2p are shown in Figure 5, and the XPS data are summarized in Table 3.

**Figure 5.** XPS spectra of (a) O 1s and (b) Co 2p from the mixed oxides.



**Table 3.** Binding energy ( $E_b$ ) for  $O_{1s}$  and  $Co_{2p}$  levels for the catalysts.

Catalyst	$E_b (O_{1s}) (eV)$			$E_b (Co_{2p}) (eV)$			
	$O_I$	$O_{II}$	$O_{III}$	$Co\ 2p_{1/2}$		$Co\ 2p_{3/2}$	
				$Co^{2+}$	$Co^{3+}$	$Co^{2+}$	$Co^{3+}$
$Co_6Al_2HTCT500$	529.8	531.1	533.9	796.1	794.7	780.7	779.6
$Co_6Al_2HTUS500$	529.9	531.1	533.8	796.1	794.7	780.8	779.7
$Co_6Al_2HTMW500$	529.8	531.0	533.5	796.2	794.8	780.7	779.6

Regarding the photopeak of oxygen 1s ( $O\ 1s$ ), three components are observed. The first component ( $O_{III}$ ) at 533–534 eV corresponds to the oxygen present in the form of carbonates or of water molecules [45]. The second component ( $O_{II}$ ) at 531 eV corresponds to adsorbed surface oxygen ( $O_2^-$  or  $O^-$ ) or hydroxyl groups ( $HO^-$ ) [46,47]. The last component ( $O_I$ ) which is located at a lower binding energy is consistent with lattice oxygen  $O^{2-}$ . The oxygen composition of the surface of the solid plays an important role in the catalytic activity in the oxidation reactions. Indeed,  $O_{II}$  species exhibit greater mobility than the lattice oxygen. In addition, several authors [46,47] have shown that the catalytic activity of the solid could be related to the presence of a relationship between oxygen  $O_{II}$  and the largest  $O_I$  oxygen. From the data, a ratio between the  $O_I$  and  $O_{II}$  species was calculated for all samples (Table 4). This revealed that for solids synthesized under ultrasound or microwaves, the ratio  $O_{II}/O_I$  increased.

**Table 4.** XPS data of  $Co_6Al_2HT500$  issued from different preparation methods and catalytic intrinsic activity calculated at 10% toluene conversion.

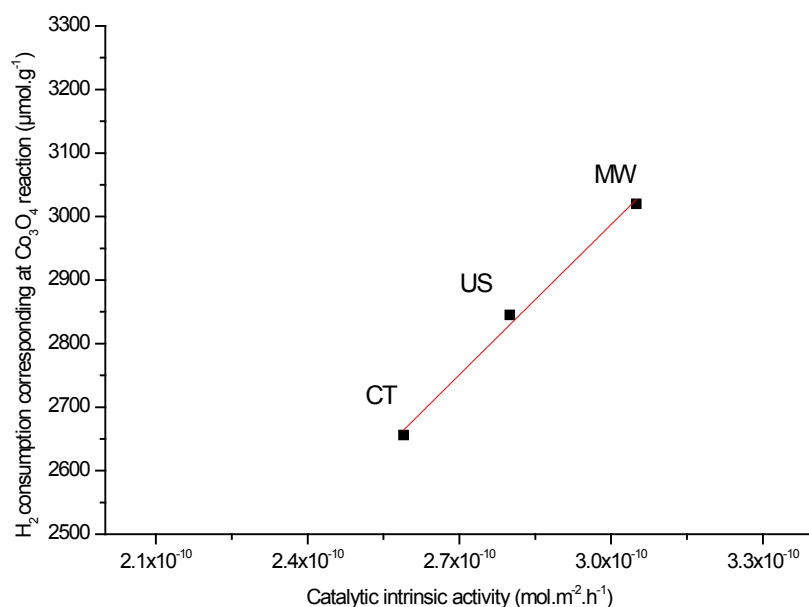
Catalyst	Surface Content (%) by XPS			$T_{50}$ (°C)	Catalytic intrinsic activity ( $mol \cdot m^{-2} \cdot h^{-1}$ )
	$O_{II}/O_I$	$Co^{2+}/Co^{3+}$	$Co/Al$		
$Co_6Al_2HTCT500$	0.86	2.38	2.9	287	$2.59 \times 10^{-10}$
$Co_6Al_2HTUS500$	1.01	2.69	2.9	278	$2.80 \times 10^{-10}$
$Co_6Al_2HTMW500$	1.05	2.98	3.3	271	$3.05 \times 10^{-10}$

Concerning the cobalt species (Table 3), an overlay of the photopeaks attributed to  $Co\ 2p$  is represented in Figure 5b. The observed profiles are characteristic of a mixture of  $Co^{2+}$  and  $Co^{3+}$  belonging to  $CoAl_2O_4$  or  $Co_3O_4$  species [48,49]. A relationship between the  $Co^{2+}$  and  $Co^{3+}$  species was calculated as the ratio of the area of the  $Co^{2+}$  signal component  $Co\ 2p_{3/2}$  and the  $Co^{3+}$  signal component  $Co\ 2p_{3/2}$  [6] (Table 4). This ratio suggests that the surface amount of  $Co^{2+}$  is higher in the  $Co_6Al_2HTMW500$  solid. It can be observed as well that the presence of oxygen defects is at a higher quantity in the case of the  $Co_6Al_2HTMW500$  mixed oxide, which could explain the best catalytic reactivity of the solid [6,48].

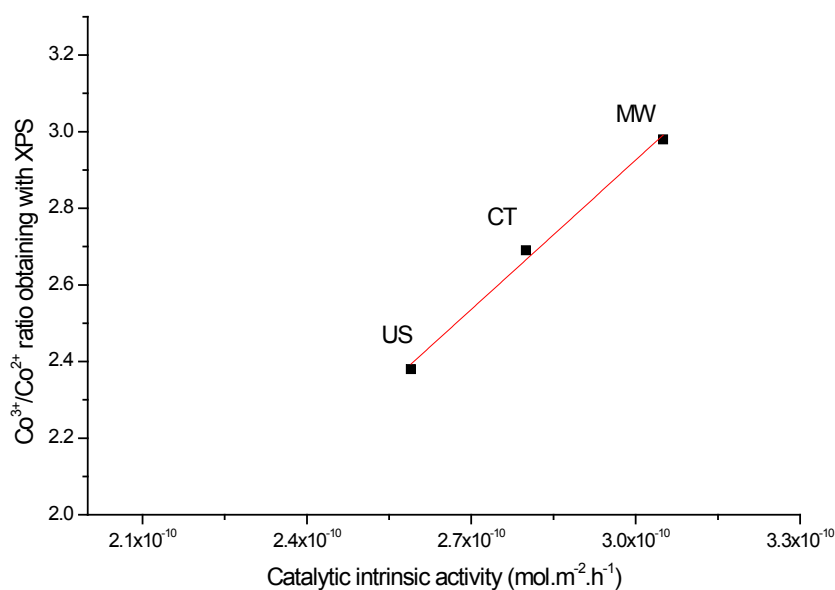
For the VOC oxidation on metal oxide based catalysts, several catalyst parameters, such as the surface area, the reducibility of the active species, the oxidation degree of the metal species or the oxygen species present on the surface, can affect the catalytic performances [6,50]. Thus, the better activity of the mixed oxides synthesized using microwaves can be related to a larger specific surface area. Indeed, this increased surface area can provide greater availability of the active phase for the reaction.

Moreover, a relationship between the  $H_2$  consumption of the first temperature peak (corresponding to the reduction of the phase  $Co_3O_4$  into  $Co^0$ ) between 0 and 400 °C and the catalytic intrinsic activity is

obtained (Figure 6). This relationship between the low-temperature reducibility and the toluene conversion suggests that  $\text{Co}_3\text{O}_4$  is the active phase. Then, a redox mechanism for this reaction can be proposed, corresponding to a Mars Van Krevelen mechanism [6,51]. This mechanism involves the participation of the lattice oxygen by a redox cycle. For the combustion of alkane with cobalt oxide, Solsona *et al.* [51] reported that  $\text{O}^{2-}$  anions participate in the total oxidation according to the redox mechanism. Moreover, Bahlawaue [52] showed that the reactivity depends on the fast migration of oxygen ions through the lattice cobalt oxide.



**Figure 6.** Relationship between catalytic intrinsic activity and  $\text{H}_2$  consumption during the  $\text{H}_2$ -TPR corresponding at  $\text{Co}_3\text{O}_4$  species.



**Figure 7.** Relationship between catalytic intrinsic activity and the ratio  $\text{Co}^{2+}$  and  $\text{Co}^{3+}$  species calculated with XPS analysis.

Moreover, another relationship could be identified as well, involving XPS results. Indeed, Figure 7 shows that the  $\text{Co}^{2+}/\text{Co}^{3+}$  ratio evaluated by XPS is also linearly related to the catalytic intrinsic activity. The relationship shows that the proportion of solid in the  $\text{Co}^{2+}$  is an important factor for achieving a good activity of the solid. Indeed, Figure 7 shows that the most active solid in the oxidation of toluene has the highest  $\text{Co}^{2+}$  proportion on the surface of the solid. This can also be linked to the increased presence of  $\text{O}_{II}$  species (adsorbed oxygen  $\text{O}_2^-$  or  $\text{O}^-$  type and oxygen vacancies in the surface of the solid). The greater presence of such a type of oxygen in the case of solids prepared by microwaves and ultrasound is an important feature that provides a higher availability of oxygen to effect the reaction (and the reduction of the solid) at low temperatures. Indeed, this oxygen is more mobile and therefore more available for reaction than in the case of the solid prepared conventionally.

### 3. Experimental Section

#### 3.1. Preparation of Catalysts

Conventional Hydrotalcite (HT) with Co:Al molar ratio 6:2 was prepared by the coprecipitation method. An aqueous solution containing appropriate amounts of  $\text{Co}(\text{NO}_3)_2$ ,  $6\text{H}_2\text{O}$  and  $\text{Al}(\text{NO}_3)_3$ ,  $9\text{H}_2\text{O}$  ions (solution A) was added drop-wise under stirring into an aqueous solution containing  $\text{Na}_2\text{CO}_3$  and  $\text{NaOH}$  (solution B). During the synthesis, the temperature and the pH were maintained at  $60\text{ }^\circ\text{C}$  and 10.5, respectively. The solution was aged at  $60\text{ }^\circ\text{C}$  during 18 h. Then, the precipitate was filtered, washed several times with hot deionized water ( $50\text{ }^\circ\text{C}$ ) and dried at  $60\text{ }^\circ\text{C}$  for 64 h. The obtained sample was called  $\text{Co}_6\text{Al}_2\text{HTCT}$  (where HTCT corresponds to the HT synthesized using the conventional method).

Two other samples were prepared using non-conventional methods involving either microwaves (MW) or ultrasounds (US). The first one was prepared by adding solution A (containing  $\text{Co}^{2+}$  and  $\text{Al}^{3+}$  ions, see above) into solution B (containing  $\text{Na}_2\text{CO}_3$  and  $\text{NaOH}$ ). The obtained gel was aged at  $80\text{ }^\circ\text{C}$  for 1 h, in a monomode reactor Synthewave Prolabo (Fontenay sous bois, France) 402 (300 W) equipped with an infrared pyrometer control and mechanical stirring. After the precipitate was filtered and washed until pH 7, the solid was dried at  $60\text{ }^\circ\text{C}$  for 12 h. The sample was labeled  $\text{Co}_6\text{Al}_2\text{HTMW}$  (where HTMW corresponds to the hydrotalcite preparation route with the microwaves procedure). The preparation of the last sample was carried out as described above, but adding the aqueous solution (A) containing the metal cations ( $\text{Co}^{2+}$  and  $\text{Al}^{3+}$ ) onto solution (B) containing the base while simultaneously submitting the mixture to ultrasounds irradiation (Branson sonifier (Danbury, CT, USA) 450 (20 kHz)). This procedure was carried out at atmospheric pressure and at ambient temperature. The precipitate was filtered, washed to eliminate the alkali metals and the nitrate ions until the pH 7, and then dried at  $60\text{ }^\circ\text{C}$  for 12 h. The sample was labelled  $\text{Co}_6\text{Al}_2\text{HTUS}$  (where HTUS corresponds to the HT synthesized using the ultrasound method).

Thermal treatment of all three samples was performed under flow of air ( $4\text{ L}\cdot\text{h}^{-1}$ ,  $1\text{ }^\circ\text{C}\cdot\text{min}^{-1}$ , 4 h at  $500\text{ }^\circ\text{C}$ ). The calcined samples were named  $\text{Co}_6\text{Al}_2\text{HTCT500}$ ,  $\text{Co}_6\text{Al}_2\text{HTMW500}$  and  $\text{Co}_6\text{Al}_2\text{HTUS500}$ .

Reference Mg-Al-O materials were also prepared to allow comparisons. These reference solids, derived from classic hydrotalcite compositions, were synthesized and calcined following the same protocols as the ones presented above for the preparation of Co-Al mixed oxides. These samples were respectively denominated  $\text{Mg}_6\text{Al}_2\text{HTCT500}$ ,  $\text{Mg}_6\text{Al}_2\text{HTMW500}$  and  $\text{Mg}_6\text{Al}_2\text{HTUS500}$ .

### 3.2. Characterization Techniques

Specific surface areas were evaluated by the BET method using a QSurf M1 apparatus (Thermo Electron, Waltham, MA, USA). The gas adsorbed at  $-196\text{ }^{\circ}\text{C}$  was pure nitrogen.

Crystalline structures were determined at room temperature from X-ray Diffractograms (XRD) recorded on a D8 Advance from Bruker AXS (Champs-Sur-Marne, France) diffractometer equipped with a copper anode ( $\lambda = 1.5406\text{ \AA}$ ) and a LynxEye Detector. The scattering intensities were measured over an angular range of  $10^{\circ} \leq 2\theta \leq 80^{\circ}$  for all samples with a step-size of  $\Delta(2\theta) = 0.02^{\circ}$  and a count time of 4 s per step. The diffraction patterns were indexed by comparison with the “Joint Committee on Powder Diffraction Standards” (JCPDS) files. Crystallite sizes were determined (Scherrer equation) using a graphic based profile analysis program (TOPAS from Bruker AXS).

Elemental compositions of samples were analyzed using Inductively Coupled Plasma-Optical Emission Spectrometer (ICP OES, Thermo Electron (Waltham, MA, USA) ICAP 6300 DUO).

Samples morphologies were investigated by Transmission Electron Microscopy observations carried out in scanning (SEM) and transmission (TEM) modes. The SEM images were recorded on a Hitachi (Tokyo, Japan) SU-70 SEM-FEG microscope whereas both TEM and HR-TEM (high resolution) images were obtained on a JEOL (Akishima, Japan) JEM-2010 operating at 200 kV).

X-ray photoelectron spectroscopy (XPS) analyses were conducted on a Kratos (Manchester, UK) Axis Ultra DLD spectrometer with a monochromatic Al K $\alpha$  ( $h\nu = 1486.6\text{ eV}$ ) radiation source operated at 15 kV and 15 mA. The binding energy (BE) was calibrated based on the line position of C 1s (285 eV). The CasaXPS processing software (Casa Software Ltd. Teignmouth, UK) was used to estimate the relative abundance of the different species. The surface atomic ratios were calculated by correcting the intensity with theoretical sensibility factors based on the Scofield cross section and using a nonlinear Shirley background.

The atomic composition,  $N_A/N_B$ , between A and B was derived from the equation:

$$\frac{N_A}{N_B} = \frac{I_A \sigma_A}{I_B \sigma_B} \left( \frac{E_{CA}}{E_{CB}} \right)^{-0.23} \quad (7)$$

where  $\sigma$  is the cross section,  $E_C$  kinetic energy and  $I$  is the intensity of the peak.

Temperature-Programmed Reduction ( $\text{H}_2$ -TPR) experiments were carried out in an Altamira AMI-200 apparatus (Labor und Analysen Technik GmbH, Garbsen, Germany). Prior to the experiment, the sample (30 mg) was activated under argon at  $150\text{ }^{\circ}\text{C}$  for 1 h. The sample was then heated from ambient temperature to  $850\text{ }^{\circ}\text{C}$  under  $\text{H}_2$  flow (5 vol% in argon  $30\text{ mL}\cdot\text{min}^{-1}$ ) with a heating rate of  $5\text{ }^{\circ}\text{C}\cdot\text{min}^{-1}$ .

### 3.3. Catalytic Tests

The activity for toluene total oxidation of the catalysts (100 mg) was measured in a continuous flow system in a fixed bed reactor at atmospheric pressure. Before each test, the catalyst was reactivated *in situ* in flowing air ( $2\text{ L}\cdot\text{h}^{-1}$ ) at  $500\text{ }^{\circ}\text{C}$  for 4 h. The flow of reactant gases ( $100\text{ mL}\cdot\text{min}^{-1}$  with 1000 ppm of  $\text{C}_7\text{H}_8$  and 20%  $\text{O}_2$  in He) was adjusted using a instrument apparatus constituted of a saturator and mass flow controllers. After reaching a stable flow, the reactants were passed through the catalyst bed and the temperature was increased from room temperature to  $500\text{ }^{\circ}\text{C}$  ( $1\text{ }^{\circ}\text{C}\cdot\text{min}^{-1}$ ). The feed

and the reactor outflow gases were analyzed on line by a 490 Micro gas chromatography from Agilent Technologies France (les Ulis, France). Model 4400IR infrared analyzers from ADEV srl (Cesano Maderno, Italy) were also used to perform the analysis of both CO and CO<sub>2</sub>. The catalysts performance was assessed in terms of T<sub>50</sub> temperature, defined as the temperature at which 50% conversion was obtained.

Catalytic intrinsic activities were evaluated at 10% of toluene conversion and considering a plug-flow reactor:

$$A = \frac{Q \times 273.15 \times [C_7H_8]_0 \times X}{V_M \times T_{10} \times 10^6 \times m \times S_{BET}} \quad (8)$$

where:

$A$  is the catalytic intrinsic activity (mol·m<sup>-2</sup>·h<sup>-1</sup>);

$Q$  is the volume flow (L·h<sup>-1</sup>);

$V_M$  is the molar volume (L·mol<sup>-1</sup>);

$T_{10}$  is the catalyst temperature for 10% toluene conversion (K);

$[C_7H_8]_0$  is the toluene initial concentration (ppm);

$X$  is the toluene conversion (%);

$m$  is the catalyst mass (g);

$S_{BET}$  is the specific surface area of the catalyst (m<sup>2</sup>·g<sup>-1</sup>).

#### 4. Conclusions

Co<sub>6</sub>Al<sub>2</sub>HT hydrotalcite-like compounds were synthesized by three different methods: conventional co-precipitation, methods assisted by microwaves or ultrasounds. The mixed oxides obtained after calcination were studied. The specific surface areas of solids prepared under sonication method or using microwaves radiations are much higher than that obtained by coprecipitation. The H<sub>2</sub>-TPR analysis shows a reduction at lower temperatures of the Co<sub>3</sub>O<sub>4</sub> species. The XPS study shows that the solid resulting from the synthesis by microwaves leads to a higher content in Co<sup>2+</sup> species on the sample. These Co<sup>2+</sup> species induce a higher presence of oxygen vacancies that could explain the higher activity of the catalyst. Moreover, correlations between the T<sub>50</sub> of the toluene oxidation and the Co<sup>2+</sup>/Co<sup>3+</sup> ratio as well as the H<sub>2</sub> consumption of the solids are evidenced, suggesting a Mars Van-Krevelen mechanism. Thus, the preparation of cobalt-based mixed oxide via a Layer Double Hydroxide synthesis route using treatment by microwaves seems to be efficient to obtain a performing catalyst for VOCs oxidation.

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## Author Contributions

Eric Genty and Julien Brunet performed the synthesis of catalysts, carried out the TPR measurements, contributed to the XPS characterization and catalytic tests. Christophe Poupin achieved the XRD experiments. Sandra Casale and Pascale Massiani realized the TEM analysis. All the authors contributed equally to the data interpretation and discussion. Renaud Cousin and Stéphane Siffert coordinate the manuscript. Eric Genty and Renaud Cousin write the manuscript. Sylvie Capelle and Pascale Massiani improved the manuscript.

## Conflicts of Interest

The authors declare no conflict of interest.

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