

Supplementary Information.

Improving Catalytic Activity towards the Direct Synthesis of H₂O₂ through Cu Incorporation into AuPd Catalysts

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Table S1. Synthesis details of the precursors used in the preparation of key bi- and tri-metallic 1%AuPd/ZSM-5 catalysts.

Catalyst	Au precursor	Precursor vol. / $\mu\text{L (mgmL}^{-1}\text{)}$	Au precursor	Precursor vol. / $\mu\text{L (mgmL}^{-1}\text{)}$	Tertiary metal precursor	Precursor vol. / $\mu\text{L (mgmL}^{-1}\text{)}$
1%AuPd _(1.00) /ZSM-5	HAuCl ₄ .3H ₂ O	530 (12.25)	PdCl ₂	585 (6.00)	-	-
1%AuPd _(0.0975) Cu _(0.025) /ZSM-5	HAuCl ₄ .3H ₂ O	517 (12.25)	PdCl ₂	570 (6.00)	CuCl ₂	106 (2.36)
1%AuPd _(0.0975) Zn _(0.025) /ZSM-5	HAuCl ₄ .3H ₂ O	517 (12.25)	PdCl ₂	570 (6.00)	Zn(NO ₃) ₂ .6H ₂ O	46 (5.43)
1%AuPd _(0.0975) Ni _(0.025) /ZSM-5	HAuCl ₄ .3H ₂ O	517 (12.25)	PdCl ₂	570 (6.00)	Ni(NO ₃) ₂	115 (2.18)

Note 1 : In the case of the tri-metallic catalysts the combined loading of Au and Pd is 0.975 wt.% (Au: Pd = (1:1 mol/mol)) and that of the tertiary metal (Cu, Zn or Ni) is 0.025 wt.%. In all cases catalyst are exposed to a reductive heat treatment prior to use (5%H₂/Ar, 400 °C, 4 h, 10°Cmin⁻¹). **Note 2:** values in parentheses for catalyst nomenclature refer to metal loading of (Au+Pd) or tertiary metal. In all instances total metal loading is 1 wt.% and Au: Pd: X = 1: 1 (mol/mol).

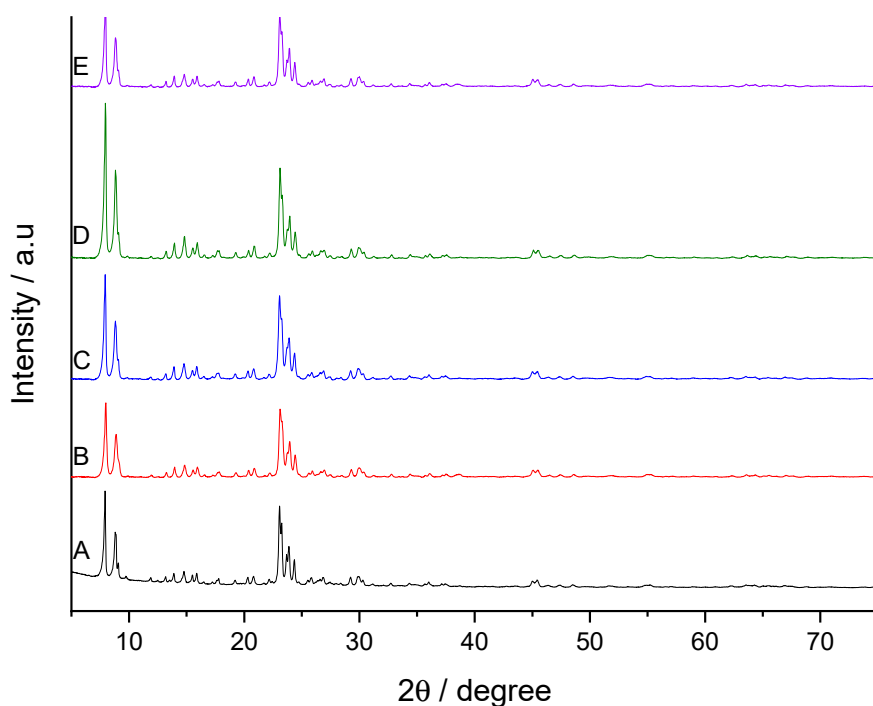


Figure S1. X-ray diffractograms of 1%AuPd_(0.0975)X_(0.025)/ZSM-5 catalysts. **(A)** ZSM-5, **(B)** 1%AuPd_(1.00)/ZSM-5, **(C)** 1%AuPd_(0.0975)Cu_(0.025)/ZSM-5, **(D)** 1%AuPd_(0.0975)Ni_(0.025)/ZSM-5 and **(E)** 1%AuPd_(0.0975)Zn_(0.025)/ZSM-5.

Supplementary text associated with Figure S1.

No significant change in the MFI structure of the ZSM-5 support is observed upon metal impregnation and exposure to a reductive heat treatment (flowing 5% H₂/Ar, 400 °C, 4h, 10°Cmin⁻¹), based on the main reflections associated with ZSM-5 ($\theta = 7.8, 8.8, 14.8, 23.14, 23.91$ and 24.5°).

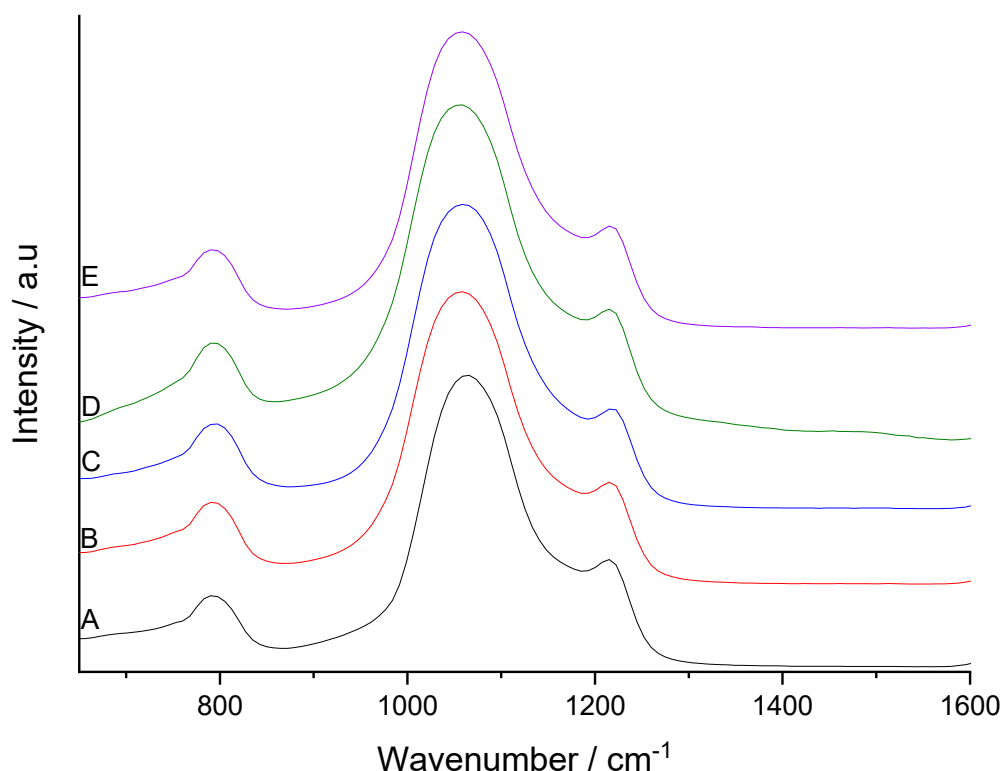


Figure S2. Fourier-transform infrared spectroscopy of 1%AuPd_(0.975)X_(0.025)/ZSM-5 catalysts. **(A)** ZSM-5, **(B)** 1%AuPd_(1.00)/ZSM-5, **(C)** 1%AuPd_(0.975)Cu_(0.025)/ZSM-5, **(D)** 1%AuPd_(0.975)Ni_(0.025)/ZSM-5 and **(E)** 1%AuPd_(0.975)Zn_(0.025)/ZSM-5.

Supplementary text associated with Figure S2.

As with analysis via XRD (Figure S.1), investigation of the 1%AuPd_(0.975)X_(0.025)/ZSM-5 catalysts by FTIR indicates no significant changes in the structure of the ZSM-5 structure is observed after metal impregnation and exposure to a reductive heat treatment (flowing 5% H₂/Ar, 400 °C, 4h, 10°Cmin⁻¹). It is possible to observe three distinct infrared bands in the FTIR spectra of 1%AuPd_(0.975)X_(0.025)/ZSM-5 catalysts at 800, 1060 and 1220 cm⁻¹ characteristic of SiO₄ tetrahedron units. The adsorption band around 1060 cm⁻¹ is attributed to the internal asymmetric stretching vibration of Si-O linkage. While the adsorption band at 1220 cm⁻¹ have been assigned to the 5-membered rings present in the structure of the ZSM-5 zeolite and the band at 800 cm⁻¹ can be assigned the symmetric stretching of the external linkages of the SiO₄ tetrahedron.

Table S2. Summary of porosity and surface area of key 1%AuPd_(0.0975)X_(0.025)/ZSM-5 catalysts and HZSM-5(30).

Catalyst	Surface area / m ² g ⁻¹	V _{Micropore} / cm ³ g ⁻¹
ZSM-5(30)	493	0.185
1%AuPd _(1.00) /ZSM-5	446	0.170
1%AuPd _(0.975) Cu _(0.025) /ZSM-5	440	0.171

Note: ZSM-5 support exposed to calcination prior to metal immobilisation (flowing air, 550 °C, 3 h, 20 °Cmin⁻¹)

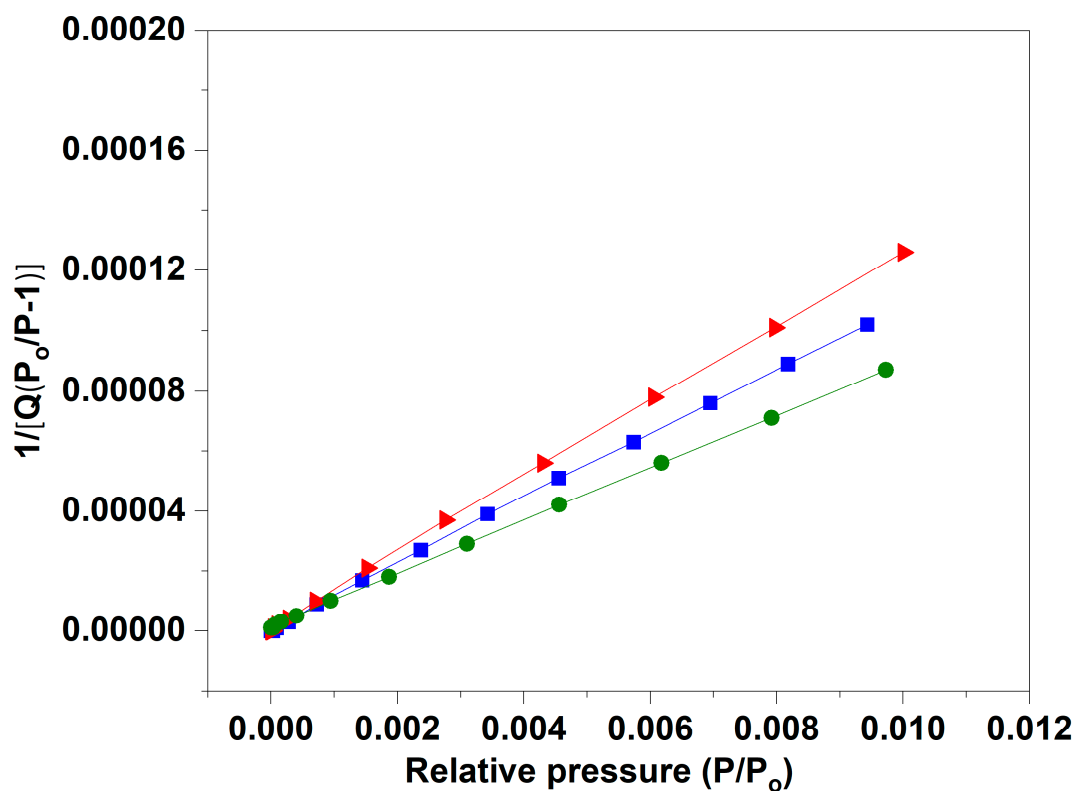


Figure S3. BET analysis plots for key 1%AuPd_(0.0975)X_(0.025)/ZSM-5 catalysts and HZSM-5(30). **Key:** ZSM-5(30) (red triangles), 1%AuPd_(1.00)/ZSM-5 (blue squares), 1%AuPd_(0.975)Cu_(0.025)/ZSM-5 (green circles). **Note:** ZSM-5 support exposed to calcination prior to metal immobilisation (flowing air, 550 °C, 3 h, 20 °Cmin⁻¹)

Table S3. Comparison of initial H₂O₂ synthesis rates over 1%AuPd_(0.0975)X_(0.025)/ZSM-5 (X=Cu, Ni, Zn) catalysts, as a function of Cu loading.

Catalyst	Productivity / mol _{H₂O₂} kg _{cat} ⁻¹ h ⁻¹	H ₂ O ₂ Conc. / wt. %	Initial rate of reaction / mmol _{H₂O₂} mmol _{metal} ⁻¹ min ⁻¹	Degradation / mol _{H₂O₂} kg _{cat} ⁻¹ h ⁻¹
ZSM-5(30)	0	0	0	0
1%AuPd _(1.00) /ZSM-5	69	0.14	37.6	320
1%AuPd _(0.975) Cu _(0.025) /ZSM-5	115	0.23	48.5	529
1%AuPd _(0.975) Ni _(0.025) /ZSM-5	81	0.16	36.4	281
1%AuPd _(0.975) Zn _(0.025) /ZSM-5	77	0.16	39.6	361

H₂O₂ direct synthesis reaction conditions: Catalyst (0.01 g), H₂O (2.9 g), MeOH (5.6 g), 5% H₂/CO₂ (420 psi), 25% O₂/CO₂ (160 psi), 0.5 h, 2° C, 1200 rpm. **Note 1:** Initial reaction rates are determined after a reaction time of 0.083 h and are calculated based on theoretical metal loading. **Note 2:** ZSM-5 support exposed to calcination prior to metal immobilisation (flowing air, 550 °C, 3 h, 20 °Cmin⁻¹)

Table S4. The effect of tertiary metal introduction upon the surface atomic composition of 1%AuPd_(0.975)X_(0.025)/ZSM-5 catalysts (X= Cu, Ni, Zn) , as determined by XPS.

Catalyst	Au: Pd	Pd ²⁺ : Pd ⁰	Productivity / mol _{H₂O₂} kg _{cat} ⁻¹ h ⁻¹
1%AuPd _(1.00) /ZSM-5	0.78	0.30	69
1%AuPd _(0.975) Cu _(0.025) /ZSM-5	0.81	1.06	115
1%AuPd _(0.975) Ni _(0.025) /ZSM-5	0.83	2.13	81
1%AuPd _(0.975) Zn _(0.025) /ZSM-5	0.28	1.13	77

H₂O₂ direct synthesis reaction conditions: Catalyst (0.01 g), H₂O (2.9 g), MeOH (5.6 g), 5% H₂/CO₂ (420 psi), 25% O₂/CO₂ (160 psi), 0.5 h, 2° C, 1200 rpm.

Table S5. Comparison of initial H₂O₂ synthesis rates over 1%AuPdCu/ZSM-5 catalysts, as a function of Cu loading.

Catalyst	Productivity / mol _{H₂O₂} kg _{cat} ⁻¹ h ⁻¹	H ₂ O ₂ Conc. / wt. %	Initial rate of reaction / mmol _{H₂O₂} mmol _{metal} ⁻¹ min ⁻¹
1%AuPd/ZSM-5	69	0.14	37.6
1%AuPd _(0.988) Cu _(0.012) /ZSM-5	111	0.22	45.1
1%AuPd _(0.981) Cu _(0.019) /ZSM-5	116	0.23	45.7
1%AuPd _(0.975) Cu _(0.025) /ZSM-5	115	0.23	48.5
1%AuPd _(0.963) Cu _(0.037) /ZSM-5	75	0.15	29.7

H₂O₂ direct synthesis reaction conditions: Catalyst (0.01 g), H₂O (2.9 g), MeOH (5.6 g), 5% H₂/CO₂ (420 psi), 25% O₂/CO₂ (160 psi), 0.5 h, 2° C, 1200 rpm. **Note:** Initial reaction rates are determined after a reaction time of 0.083 h and are calculated based on theoretical metal loading.

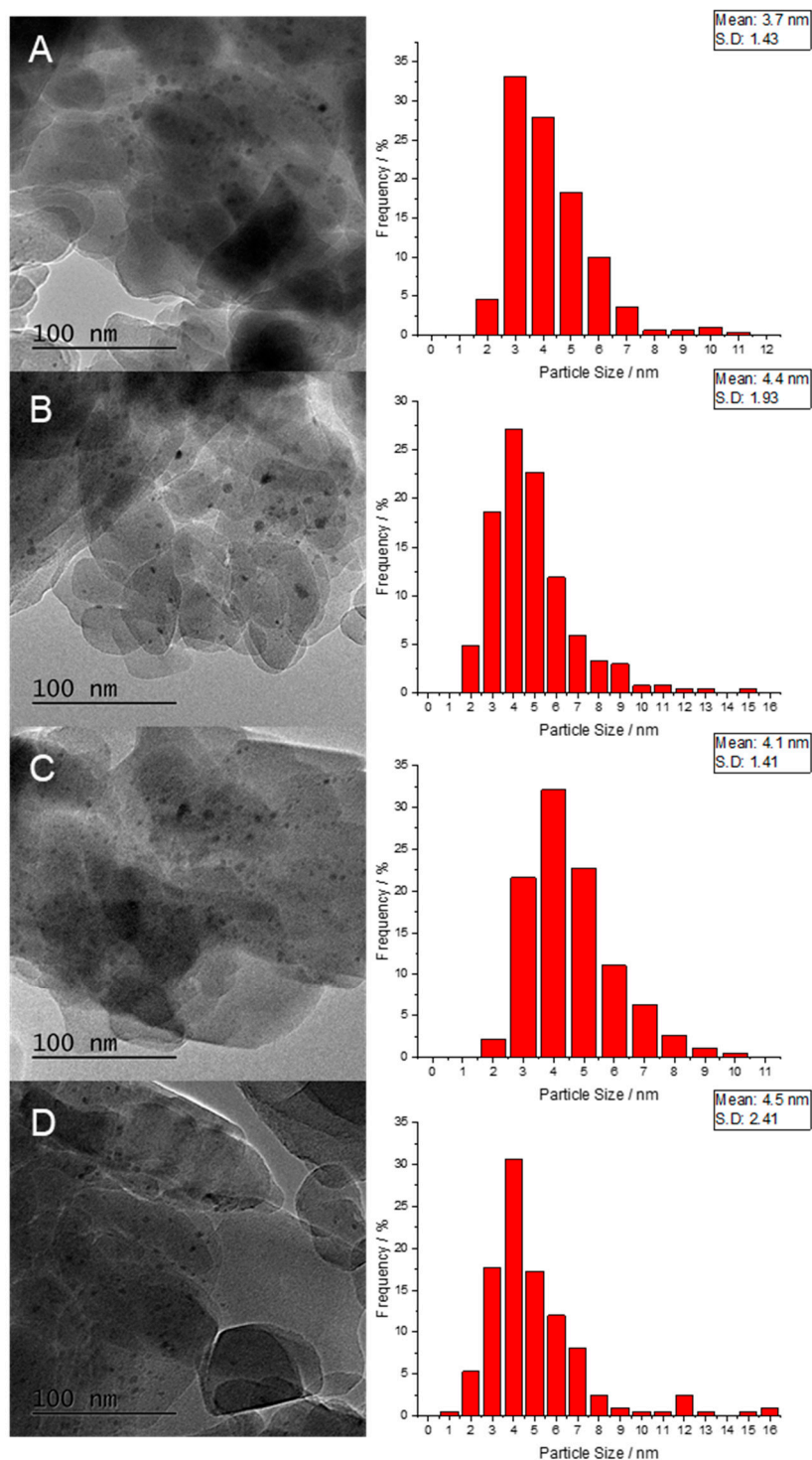


Figure S4. Representative bright field transmission electron micrographs and corresponding particle size histograms of as-prepared (A) 1% $\text{AuPd}_{(1.00)}/\text{ZSM-5}$ and (C) 1% $\text{AuPd}_{(0.975)}\text{Cu}_{(0.025)}/\text{ZSM-5}$ catalysts and analogous (B) 1% $\text{AuPd}_{(1.00)}/\text{ZSM-5}$ and (D) 1% $\text{AuPd}_{(0.975)}\text{Cu}_{(0.025)}/\text{ZSM-5}$ samples after use in the direct synthesis reaction. **H_2O_2 direct synthesis reaction conditions:** Catalyst (0.01 g), H_2O (2.9 g), MeOH (5.6 g), 5% H_2/CO_2 (420 psi), 25% O_2/CO_2 (160 psi), 0.5 h, 2° C, 1200 rpm.

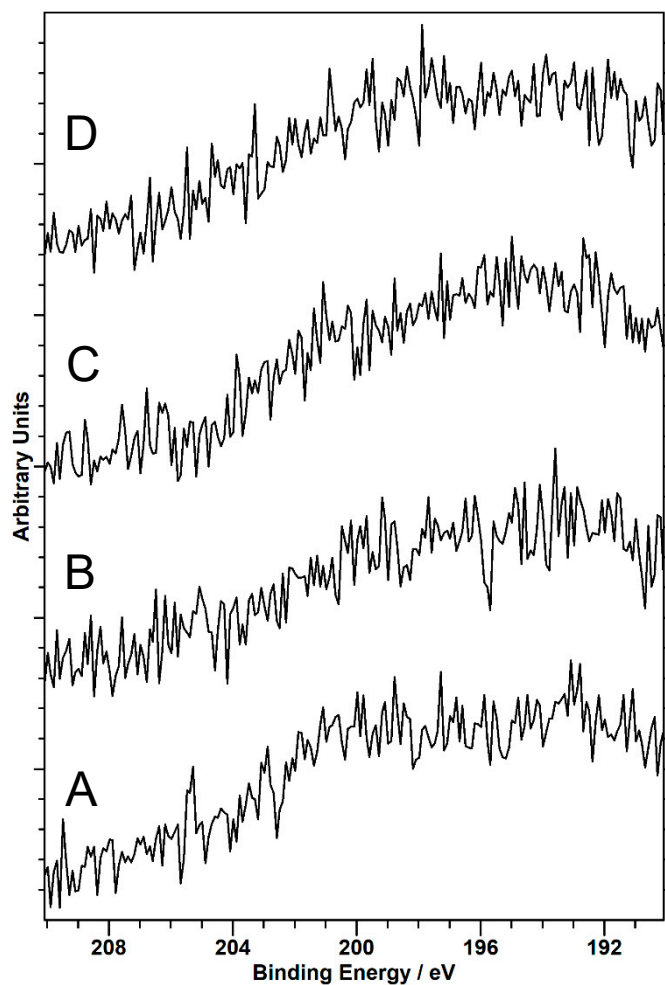


Figure S5. Comparison of surface atomic Cl content of the as-prepared **(A)** and **(B)** used 1% $\text{AuPd}_{(1.00)}$ /ZSM-5 catalyst and the fresh **(C)** and **(D)** used 1% $\text{AuPd}_{(0.975)}\text{Cu}_{(0.025)}$ /ZSM-5 analogue. **Note:** No signal is observed for any catalyst formulation within the expected energy window for Cl(2p) (approx. 200 eV).

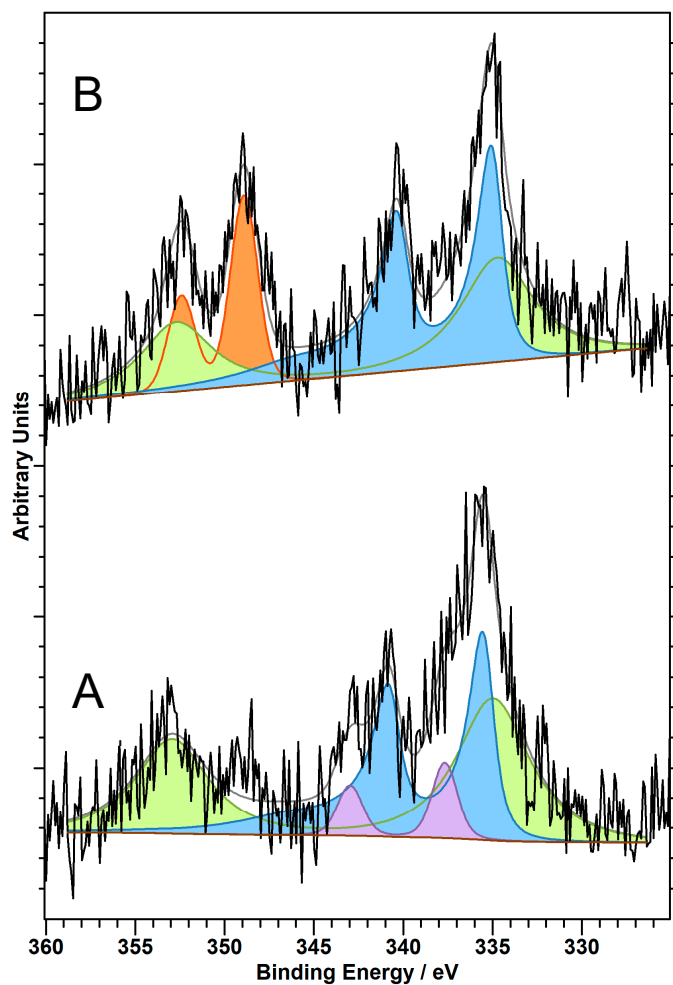


Figure S6. XPS spectra of Pd(3d) regions for the (A) as-prepared and (B) used 1%AuPd_(1.00)/ZSM-5 catalyst, after use in the H₂O₂ direct synthesis reaction. **Key:** Au(4d) (green), Pd⁰(blue), Pd²⁺(purple), Ca²⁺ (orange).

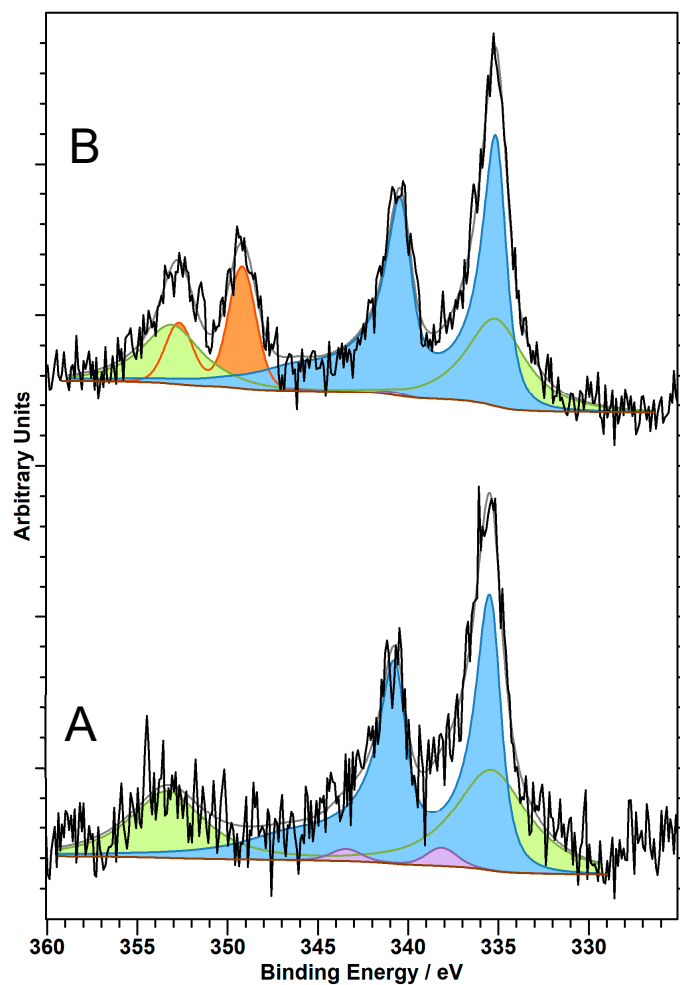


Figure S7. XPS spectra of Pd(3d) regions for the **(A)** as-prepared and **(B)** used 1% $\text{AuPd}_{(0.975)}\text{Cu}_{(0.025)}$ /ZSM-5 catalyst, after use in the H_2O_2 direct synthesis reaction. **Key:** Au(4d) (green), Pd^0 (blue), Pd^{2+} (purple), Ca^{2+} (orange).