

Article

Improvement of Propylene Epoxidation Caused by Silver Plasmon Excitation by UV-LED Irradiation on a Sodium-Modified Silver Catalyst Supported on Strontium Carbonate

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Abstract: The effect that UV-LED irradiation exerted on a sodium-modified silver catalyst supported on strontium carbonate (Ag-Na/SrCO₃) was examined during an epoxidation of propylene to propylene oxide. Based on our previous study, we used Ag(56)-Na(1)/SrCO₃ in this study. The numbers in parentheses refer to the weight percentage of silver and sodium. Although this catalyst system did not contain typical photocatalysts such as titanium oxide or tungsten oxide, UV-LED irradiation of Ag(56)-Na(1)/SrCO₃ resulted in an evident improvement in the selectivity and yield of propylene oxide. Such an advantageous effect of UV-LED irradiation could not be discussed based on the bandgap used in photocatalysts and, therefore, we proposed a mechanism based on the plasmon excitation of silver, which could be accomplished using the irradiation wavelength of UV-LED to produce electrons. Since the lifespan of these electrons is expected to be short, it is difficult to place them into direct contact with the gas phase of oxygen. Once the generated electrons move to SrCO₃, however, the lifespan is improved, which could allow suitable contact with oxygen in the gas phase to form active oxygen. If the oxygen is active for epoxidation as hydrogen peroxide, this could explain the improvement in activity from UV-LED irradiation.

Keywords: epoxidation; propylene; propylene oxide; UV-LED; plasmon excitation; silver catalyst

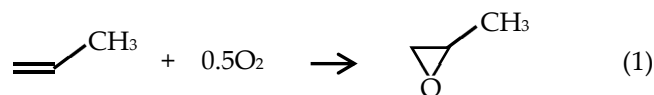
1. Introduction

Since propylene oxide is a raw material for polyurethane that is widely used in automobile parts, food additives, cosmetics, etc., more than 10 million tons are produced annually worldwide by the petrochemical industry [1]. At present, 40% of this production is via the classical production method, the chlorohydrin method, but the construction of new plants has been suppressed due to concerns over environmental pollution [1,2]. The Halcon process has subsequently been developed and has overcome the shortcomings of the chlorohydrin method. However, since the Halcon process is a co-production method, it is greatly affected by the demand for by-products [2,3]. Currently, the cumene method, which overcomes this point, is being developed as a single production method for propylene



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oxide [1–3]. Although not yet industrialized, a method for producing propylene oxide by epoxidation of propylene (Equation (1)) has been widely studied in academia as a simple, economical, and energetically ideal method for producing propylene oxide [4–6]. As shown in our previous paper [7], the activity of catalytic systems tends to be overestimated. Moreover, this epoxidation is classified as a highly difficult oxidation reaction, and in order to improve the production of propylene oxide and the development of catalysts, novel methods and concepts must be introduced into ordinary reaction fields.



Against this background, we examined the catalytic epoxidation of propylene to propylene oxide under UV-LED irradiation conditions, and noted the effect that UV-LED irradiation exerts on epoxidation. Prior to the present study, we investigated the partial oxidation of methane under UV-LED irradiation conditions using a samarium oxide catalyst doped with an anatase type of titanium oxide [8]. Samarium oxide is a suitable catalyst for the oxidative coupling of methane. When titanium oxide was added to samarium oxide, however, partial oxidation of methane to carbon monoxide occurred preferentially under UV-LED irradiation conditions. The effect of active oxygen such as O_2^- generated under UV-LED irradiation conditions was clearly reflected in the catalytic activity. In the present study, therefore, we investigated the effect that UV-LED irradiation exerts on the activity of a sodium-modified silver catalyst supported on strontium carbonate (Ag-Na/SrCO₃). Although the activity of this catalyst was low, we have already found that similar results were obtained when similar methods of this catalyst preparation and activity test were performed in different laboratories, as shown in a previous study [7]. Furthermore, we confirmed that the use of this catalyst could avoid the overestimation of catalytic activity [7]. In a manner similar to the partial oxidation reaction of methane, we attempted to examine the effect of UV-LED irradiation by adding normal photocatalysts such as titanium oxide or tungsten oxide to an Ag-Na/SrCO₃ catalyst. There was no effect from UV-LED when the photocatalyst was added, but there was a clear improvement in the selectivity and yield of propylene oxide when a photocatalyst was not added. Therefore, in the present study, we examined the activity on Ag-Na/SrCO₃ in the absence of a photocatalyst under UV-LED irradiation.

2. Results and Discussion

2.1. Effect of UV-LED Irradiation on Catalytic Behavior

Figure 1 depicts the use of UV-LED irradiation for the epoxidation of propylene to propylene oxide (PO) and shows the effects on Ag(56)-Na(1)/SrCO₃ (0.3 g) at F = 15 mL/min, p(C₃H₆) = p(O₂) = 16.9 kPa and 673 K, which was the starting point for the present study. In the present study, we focused on the behavior of propylene, oxygen and PO. Under the reaction conditions employed in the present study, CO₂, CO, propane, acetaldehyde, propionaldehyde and acrolein were detected in proportional ranges of 81.9–97.6%, 0.0–9.6%, 0.3–8.3%, 0.0–3.4%, 0.0–0.9% and 0.0–1.0%, respectively, in terms of selectivity. As shown in Figure 1, without UV-LED irradiation, the rate of the selectivity and yield of PO at 0.5 h on-stream were 1.2 and 0.04%, respectively, followed by slight enhancements in the PO yield to 0.10% at 1.75 h on-stream. Following irradiation using UV-LED, the selectivity and yield of PO at 0.5 h on-stream were evidently enhanced to 1.7 and 0.07% at 0.75 h on-stream, followed by additional enhancement to 3.4 and 0.42% at 1.75 h on-stream. Almost the same effect of UV-LED irradiation on the selectivity and yield of PO was detected at p(C₃H₆) = 33.8 kPa, p(O₂) = 16.9 kPa and 673 K. Without UV-LED under C₃H₆ rich conditions, the selectivity and yield of PO were 0.4 and 0.02%, respectively, at 1.75 h on-stream. It is noteworthy that, with UV-LED, the selectivity and yield of PO were similarly improved to 2.3 and 0.15%, respectively, at 1.75 h on-stream. It should be noted that the most important effect of UV-LED irradiation is the increase in the selectivity of PO,

followed by the increase in the yield of PO. Although the effect of UV-LED irradiation as an accelerant of the epoxidation of propylene on Ag(56)-Na(1)/SrCO₃ was evident, and it became necessary to examine whether this improvement would continue even if the time-on-stream was extended. Therefore, another test sample of Ag(56)-Na(1)/SrCO₃ was prepared separately and examined for up to 6 h on-stream.

Figure 2 shows the results obtained on Ag(56)-Na(1)/SrCO₃ and Ag(75)-Na(1)/SrCO₃ during 6 h on-stream under the same reaction conditions as those in Figure 1 under UV-LED irradiation conditions.

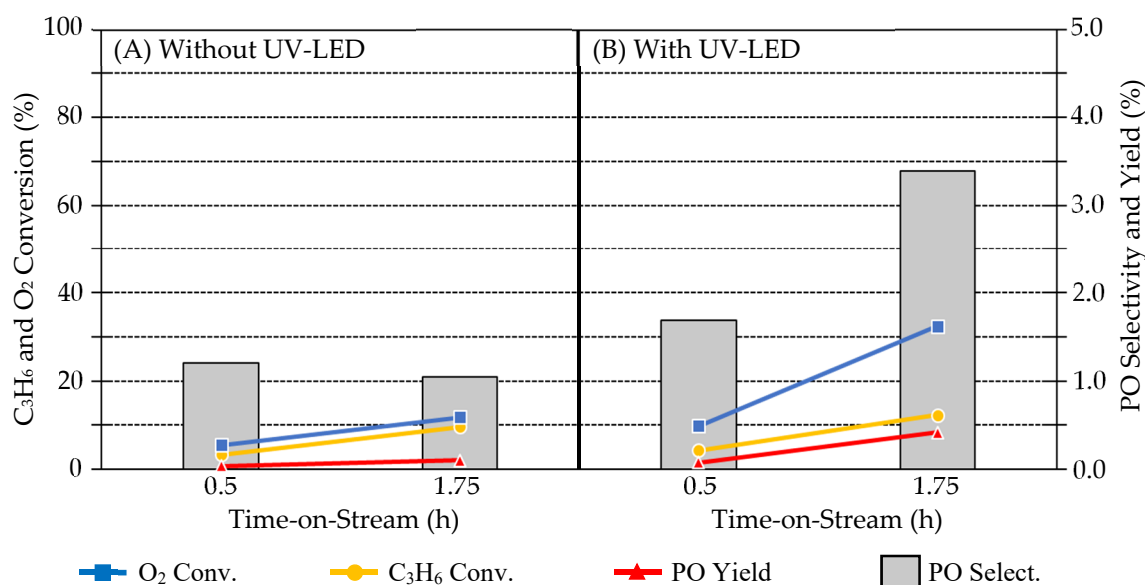


Figure 1. Effect of UV-LED irradiation on catalytic activity on Ag(56)-Na(1)/SrCO₃ (0.30 g) at F = 15 mL/min, p(C₃H₆) = p(O₂) = 16.9 kPa and 673 K.

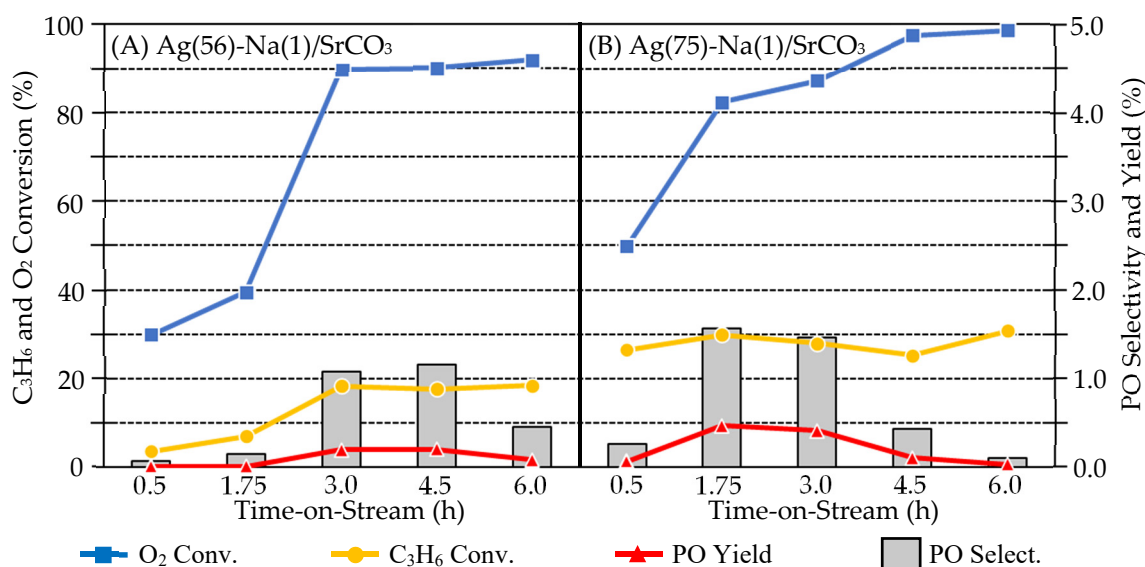


Figure 2. Catalytic activity on Ag(56)-Na(1)/SrCO₃ and Ag(75)-Na(1)/SrCO₃ (both 0.30 g) at F = 15 mL/min, p(C₃H₆) = p(O₂) = 16.9 kPa and 673 K under UV-LED irradiation.

As expected from the previous report [9], since the formation of PO was difficult to confirm on Ag(25)-Na(1)/SrCO₃, we focus on the former two catalysts in the present paper.

The catalytic activity on the newly prepared Ag(56)-Na(1)/SrCO₃ was lower than that in Figure 1, since the catalyst preparation method was greatly affected by slight differences

in the conditions. However, the improvement behavior of the activity by UV-LED with time-on-stream was again observed. As shown in Figure 2, the selectivity and yield of PO on Ag(75)-Na(1)/SrCO₃ was evidently greater than that on Ag(56)-Na(1)/SrCO₃ regardless of time-on-stream, indicating that the contribution of silver to the catalytic activity was evident. Although the PO yield was unavoidably low for the epoxidation of propylene to PO, we focused on the selectivity and yield of PO with time-on-stream on both catalysts. On Ag(56)-Na(1)/SrCO₃, the selectivity and yield of PO increased to 1.2 and 0.20% at 4.5 h on-stream, while the increase was 1.6 and 0.47% at 1.75 h on-stream on Ag(75)-Na(1)/SrCO₃, and both were followed by decreases in both the selectivity and yield of PO. It should be noted that the selectivity and yield on Ag(56)-Na(1)/SrCO₃ was 0.5 and 0.05%, respectively, once UV-LED irradiation was interrupted at 3 h on-stream. Although Ag(56)-Na(1)/SrCO₃ and Ag(75)-Na(1)/SrCO₃ contained no typical photocatalysts such as titanium oxide or tungsten oxide, the improvement in activity from UV-LED irradiation was evident. Therefore, it was necessary to establish whether the influence of this UV-LED irradiation was due to the Ag-Na/SrCO₃ catalyst itself or to the constituent species of this catalyst.

2.2. Effect of UV-LED Irradiation on the Components of Ag-Na/SrCO₃ and that on Ag-Na/MgCO₃

The effects that UV-LED irradiation exerted on the catalytic activity of SrCO₃ (A), Ag/SrCO₃ (B), and Na/SrCO₃ (C) together with Ag-Na/MgCO₃ (D) were examined and the results are described in Table 1.

Table 1. Effect of catalytic activity under UV-LED irradiation on SrCO₃ (A), Ag(56)/SrCO₃ (B), Na(1)/SrCO₃ (C), and Ag(56)-Na(1)/MgCO₃ (D) (all at 0.30 g) at F = 15 mL/min, p(C₃H₆) = p(O₂) = 16.9 kPa and 673 K.

Catal.	Time-on-Stream (h)	C ₃ H ₆ Conv. (%)	PO Select. (%)	PO Yield (%)
(A)	0.5	3.5	0.0	0.0
	1.75	6.6	0.0	0.0
	3.0	7.6	0.0	0.0
(B)	0.5	13.8	0.0	0.0
	1.75	15.7	0.0	0.0
	3.0	16.4	0.0	0.0
(C)	0.5	4.6	1.3	0.06
	1.75	5.7	0.0	0.0
	3.0	8.8	0.0	0.0
(D)	0.5	24.1	0.0	0.01
	1.75	33.1	0.0	0.01
	3.0	28.4	0.0	0.01

It was evident that the SrCO₃ support alone (catalyst (A)) showed no activity for the epoxidation of propylene under UV-LED irradiation conditions. With the loading of silver on SrCO₃ (catalyst (B)), the conversion of propylene was evidently enhanced but, again, the effect of UV-LED irradiation was negligible. The loading of sodium onto SrCO₃ resulted in only a slight improvement in activity while the effect of UV-LED irradiation also was negligible. Changing the support from SrCO₃ to MgCO₃ resulted in no effect from UV-LED irradiation and, instead, it prevented the production of PO. Therefore, the effect of UV-LED irradiation on the epoxidation of propylene to PO observed in the present study appeared to be dependent on the interactions of each of the components of the Ag(56)-Na(1)/SrCO₃ catalyst.

2.3. Characterization of the Ag-Na/SrCO₃ Catalyst

The specific surface areas of Ag(56)-Na(1)/SrCO₃ and Ag(75)-Na(1)/SrCO₃ were 2.2 and 1.3 m²/g. As shown in the XRD patterns of Ag(75)-Na(1)/SrCO₃ (Figure 3), only the signals due to metallic silver (PDF 01-087-0597) were detected before and after epoxidation

under UV-LED irradiation. Furthermore, the SEM images of Ag(75)-Na(1)/SrCO₃ (Figure 4) revealed no structural changes such as sintering or transformation to other species either before or after epoxidation, while a covering on the surface by coking was detected.

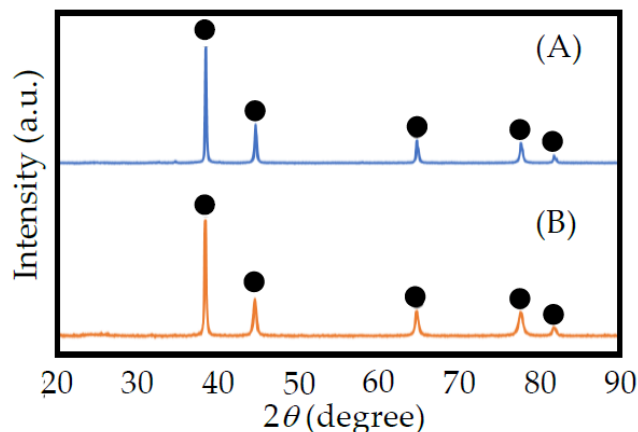


Figure 3. XRD Patterns of Ag(75)-Na(1)/SrCO₃ (A) before and (B) after epoxidation at $F = 15$ mL/min, $p(\text{C}_3\text{H}_6) = p(\text{O}_2) = 16.9$ kPa and 673 K under UV-LED conditions. •: Ag

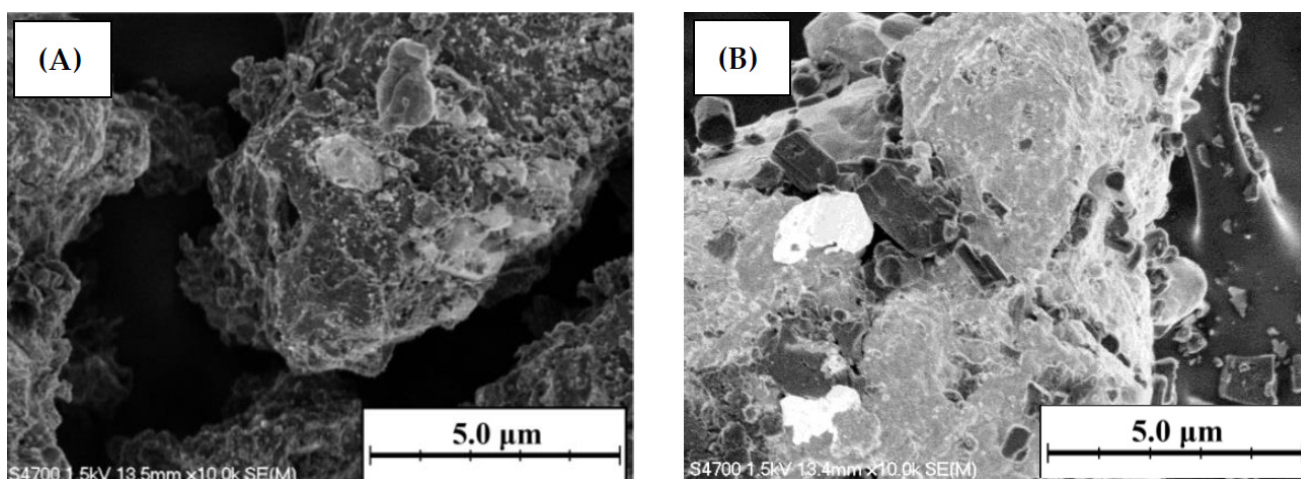


Figure 4. SEM images of Ag(75)-Na(1)/SrCO₃ (A) before and (B) after epoxidation at $F = 15$ mL/min, $p(\text{C}_3\text{H}_6) = p(\text{O}_2) = 16.9$ kPa and 673 K under UV-LED conditions.

The coking was further supported by changes in the acidic and basic properties of the Ag(75)-Na(1)/SrCO₃ catalyst before and after epoxidation. Figures 5 and 6 show the NH₃- and CO₂-TPD of Ag(56)-Na(1)/SrCO₃ and Ag(75)-Na(1)/SrCO₃ before and after epoxidation. Based on Figure 5, the maximum NH₃-TPD peaks of Ag(56)-Na(1)/SrCO₃ and Ag(75)-Na(1)/SrCO₃ before the reaction were detected at 755 and 736 K, respectively, and the amounts of acid were estimated to be 0.023 and 0.013 mmol/g, respectively.

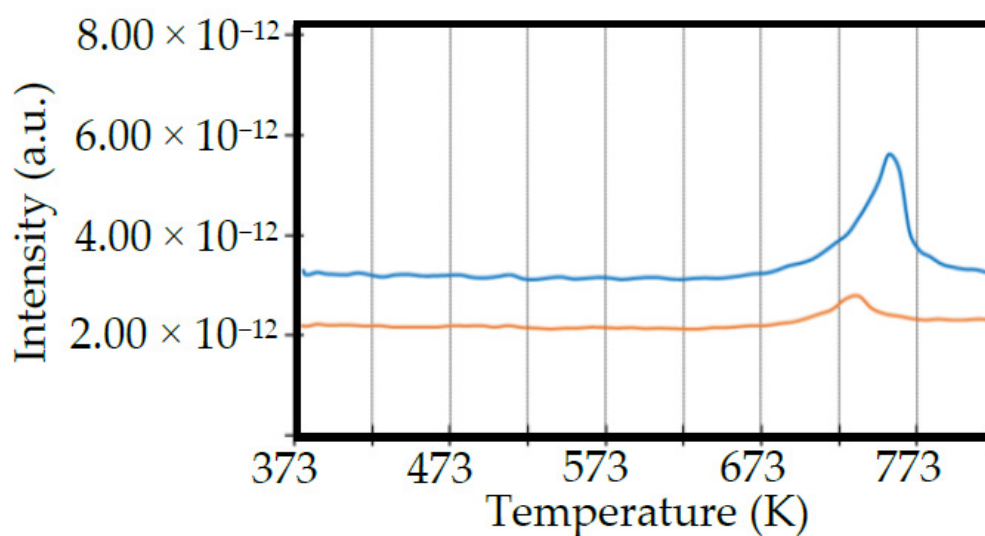


Figure 5. NH_3 -TPD of $\text{Ag}(56)\text{-Na}(1)/\text{SrCO}_3$ (blue line) and $\text{Ag}(75)\text{-Na}(1)/\text{SrCO}_3$ (orange line) before epoxidation at $F = 15 \text{ mL/min}$, $p(\text{C}_3\text{H}_6) = p(\text{O}_2) = 16.9 \text{ kPa}$ and 673 K .

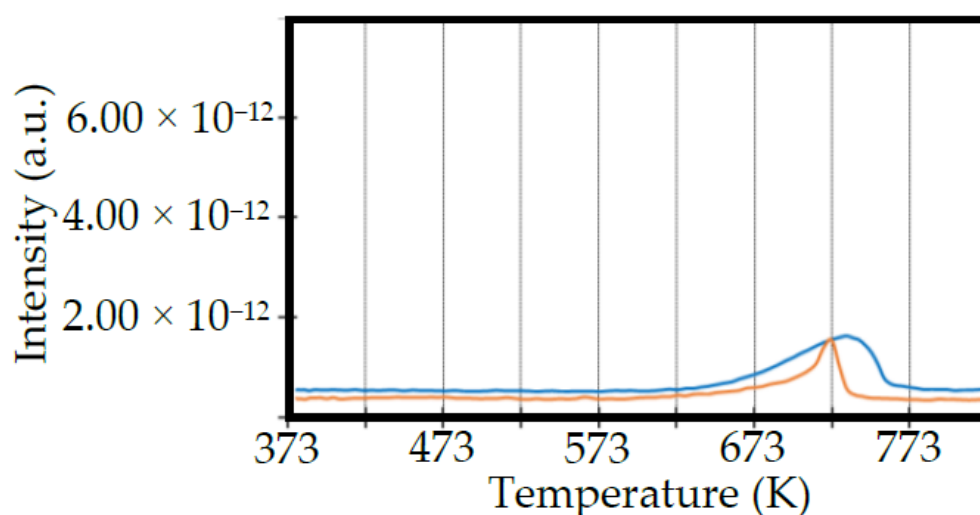


Figure 6. CO_2 -TPD of $\text{Ag}(56)\text{-Na}(1)/\text{SrCO}_3$ (blue line) and $\text{Ag}(75)\text{-Na}(1)/\text{SrCO}_3$ (orange line) before epoxidation at $F = 15 \text{ mL/min}$, $p(\text{C}_3\text{H}_6) = p(\text{O}_2) = 16.9 \text{ kPa}$ and 673 K .

Figure 6 shows the maximum CO_2 -TPD peaks of $\text{Ag}(56)\text{-Na}(1)/\text{SrCO}_3$ and $\text{Ag}(75)\text{-Na}(1)/\text{SrCO}_3$ before the reactions at 733 and 723 K, respectively, and the base amounts were estimated to be 0.048 and 0.009 mmol/g, respectively. However, these NH_3 - and CO_2 -TPD peaks had completely disappeared after the reaction, probably due to the formation of coking.

The characterization results shown above were somewhat of an analogue to the normal catalytic reaction regardless of the employment of the thermal- and photo-reactions when using solid catalysts. These results could not explain the advantageous effect that UV-LED irradiation exerted on Ag-Na/SrCO_3 during the epoxidation of propylene to PO. Therefore, we focused on the silver nano-particles that had formed when using the present catalyst system [7].

2.4. Contribution of Silver Plasmon Excitation

In our previous paper [7], we reported that nano-particles of silver with a wide distribution of particle sizes had formed on $\text{Ag}(56)\text{-Na}(1)/\text{SrCO}_3$. With such a silver nano-structure, plasmon excitation forms excited electrons, which is thought to contribute to the

catalytic oxidation on some metals [10,11]. In particular, electronic-state calculation of the catalytic oxidation of ethylene on silver nano-particles suggests that the transfer of excited electrons to gaseous oxygen to form active oxygen easily proceeds under silver plasmon excitation conditions [12]. However, since the lifetime of excited electrons is estimated to be very short, it is difficult for the excited electrons to directly transfer to the gas phase of oxygen. Recent studies have shown, however, that once excited electrons are generated on silver nano-particles, they tend to flow onto the support, and are then transferred to the gas phase of oxygen to form active oxygen [13–17]. In the present study, as shown in Table 1, Ag(56)/SrCO₃ and Ag(56)-Na(1)/MgCO₃ showed no advantageous effect of UV-LED irradiation. This indicates that sodium-modified SrCO₃ should be suitable as a support. The present results revealed that the latter suggestion may be supported if plasmonic excitation, which was confirmed on Ag(56)-Na(1)/SrCO₃. Therefore, the steady-state absorption spectra of Ag(56)-Na(1)/SrCO₃ was measured via an absorption spectroscopy. Figure 7 shows the Kubelka–Munk functions (K/S; K: absorption coefficient, S: scattering coefficient) obtained from the absorption spectra of SrCO₃ and Ag(56)-Na(1)/SrCO₃. Although there was no absorption from SrCO₃ at wavelengths longer than 330 nm, as reported [18], plasmon excitation via silver nano-particles was evident from Ag(56)-Na(1)/SrCO₃ between 330 and 500 nm. These are the same absorption regions reported for silver nano-particles [10], which was suitable for the present conditions using UV-LED at a wavelength of 365 nm. The absorptions from SrCO₃ and Ag(56)-Na(1)/SrCO₃ observed at wavelengths shorter than 330 nm could be assigned to the bandgap excitation from SrCO₃ [18,19].

Therefore, we concluded that the selectivity and yield of PO under UV-LED irradiation observed in the present study was improved when electrons derived from plasmon excitation on silver nanoparticles were transferred to the vapor phase of oxygen via the sodium-loaded support (Na/SrCO₃) to generate an active oxygen corresponding to epoxidation.

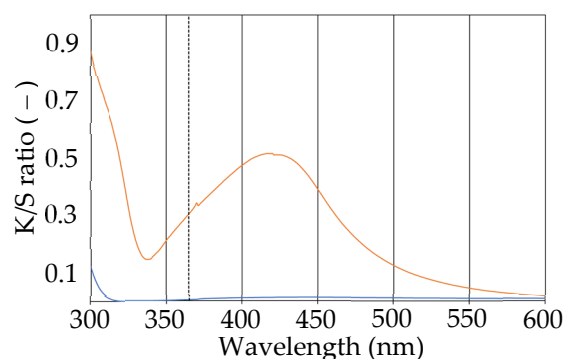


Figure 7. Kubelka–Munk functions of SrCO₃ (blue line) and Ag(56)-Na(1)/SrCO₃ (red line) obtained from the corresponding absorption spectroscopy.

3. Materials and Methods

3.1. Catalyst Preparation

Sodium-modified silver catalyst supported on strontium carbonate was prepared according to a method described in previous papers [7,9]. As a typical example, the preparation method for Ag(56)-Na(1)/SrCO₃ (the numbers in parentheses refer to the weight % loading of silver and sodium) is illustrated as follows. After ethylene diamine (15.0 g, 250 mmol; Kanto Chemical Co., Inc., Tokyo, Japan) was dissolved in distilled water (20.0 g), oxalic acid (10.1 g, 112 mmol; FUJIFILM Wako Pure Chemical Corp., Tokyo, Japan) and Ag₂O (8.90 g, 38.4 mmol) were slowly added to the aqueous solution with magnetic stirring for 1 h. Then, ethanolamine (1.80 g, 29.5 mmol; Kanto Chemical Co., Inc.) and NaCl (0.147 g, 2.51 mmol; FUJIFILM Wako Pure Chemical Corp.) were dissolved in 4 mL distilled water and added to the aqueous solution. After the resultant mixture was stirred for an additional 1 h, we added 6.40 g (43.4 mmol) of SrCO₃ (FUJIFILM Wako Pure

Chemical Corp.) to the mixture to form a slurry. The slurry was stirred for 4 h and dried at 393 K for 2 h, followed by calcination at 633 K for 3 h to afford Ag(56)-Na(1)/SrCO₃.

3.2. Characterization of the Catalyst

The catalysts were analyzed using nitrogen adsorption–desorption measurement (BELSORPmax12, MicrotracBEL, Osaka, Japan), X-ray diffraction (XRD; SmartLab/RA/INP/DX, Rigaku Co., Tokyo, Japan), NH₃ temperature-programmed desorption (NH₃-TPD; BELCAT II, MicrotracBEL), CO₂ temperature-programmed desorption (CO₂-TPD; BELCAT II, MicrotracBEL), scanning electron microscopy (SEM; JSM-6390, JEOL Ltd., Tokyo, Japan), and/or by using an absorption spectrophotometer (V-670, JASCO Co., Tokyo, Japan). Before the nitrogen adsorption–desorption measurement at 77 K, each catalyst was pretreated at 473 K for 5 h under vacuum. The BET surface area was calculated from the obtained adsorption isotherm. The powder XRD patterns of the catalysts were obtained using monochromatized Cu K α radiation (40 kV, 150 mA). The acidic or basic properties of the catalysts were measured using either NH₃-TPD or CO₂-TPD, both in which the pretreatment temperature was adjusted to 673 K. The desorbed NH₃ or CO₂ from the catalyst was monitored using a BELMass (Microtrac-BEL) quadrupole mass spectrometer with a mass signal of $m/e = 16$ or 44 for NH₃ or CO₂, respectively. It should be noted that when $m/e = 17$, this represented the mass signal of the NH₃ parent peak, which was strongly influenced by H₂O, and, thereafter, $m/e = 16$ was used for the analysis of NH₃. The absorption spectrum of the catalyst was obtained by applying the Kubelka–Munk formula to the diffuse reflection spectrum.

3.3. Evaluation of the Catalytic Performance

The catalytic experiments were performed in a fixed-bed continuous-flow quartz reactor, which was placed in an electric furnace with an optical window, and operated at atmospheric pressure and 898 K [8]. As a light source for UV-LED irradiation, a Light-cure LC-L1V3 (Hamamatsu Photonics K.K., Hamamatsu, Shizuoka) was used. This light source emits UV light at a wavelength of 365 nm for an average maximum irradiation intensity of 14,000 mW/cm² and a maximum output of 450 mW. The temperature of the catalyst (0.30 g) was increased to 673 K under a flow of He. After the reaction temperature was stabilized, the catalyst was treated with a flow of O₂ (15 mL/min) for 1 h. Activity tests were then carried out under 15 mL/min of a reactant gas flow (F) that consisted of C₃H₆ and O₂ diluted with He. In the present study, a partial-pressure ratio of 1.0 was employed for C₃H₆/O₂, and the partial pressures were then adjusted to $p(\text{C}_3\text{H}_6)/p(\text{O}_2) = 16.9 \text{ kPa}/16.9 \text{ kPa}$, unless otherwise stated. Under these conditions, no homogeneous reactions were detected. The reaction was monitored using an on-line TCD gas chromatograph (GC-8APT, Shimadzu Corp., Kyoto, Japan) and an FID capillary gas chromatograph (GC-2010, Shimadzu Corp.). The columns in the TCD-GC consisted of a Molecular Sieve 5A (0.3 m \times Φ 3 mm) for the detection of O₂, CO, and CH₄ at 318 K and a Porapak Q (GL Sciences Inc., Tokyo, Japan, 6 m \times Φ 3 mm) for the detection of CO₂, ethane, ethylene, propane, and propylene at column temperatures that ranged between 318 and 493 K with a heating rate of 10 K/min. Furthermore, the capillary column in the FID-GC consisted of Stabilwax (Shimadzu GLC Ltd., Tokyo, Japan, 60 m \times Φ 0.25 mm \times 0.25 μm) for the detection of acetaldehyde, propylene oxide, propionaldehyde, acetone, acrolein, propane, and propylene at column temperatures of 313 K. The conversion and the selectivity were estimated on a carbon basis.

4. Conclusions

In the present study, excited electrons generated via plasmonic silver on Ag-Na/SrCO₃ under UV-LED irradiation contributed to an improvement in the selectivity and yield of propylene oxide through the catalytic epoxidation of propylene. A plausible explanation is that the electrons generated on the silver were transferred to the SrCO₃ support doped with sodium where they reacted with gaseous O₂ to form active oxygen suitable for epoxidation.

The present study reveals the importance of paying attention to plasmonic excitation in addition to the usual focus on bandgap excitation during photocatalytic reactions on solid catalysts.

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