

Article

Numerical Analysis for Heat Transfer Augmentation in a Circular Tube Heat Exchanger Using a Triangular Perforated Y-Shaped Insert

Lokesh Pandey¹ and Satyendra Singh^{2,*}¹ Uttarakhand Technical University, Dehradun 248007, Uttarakhand, India; lokesh.pandey21@gmail.com² Department of Mechanical Engineering, B.T. Kumaon Institute of Technology, Dwarahat 263653, Uttarakhand, India

* Correspondence: ssinghiitd@gmail.com

Abstract: The present investigation constitutes CFD analysis of the heat transmission phenomenon in a tube heat exchanger with a Y-shaped insert with triangular perforation. The analysis is accomplished by considering air as a working fluid with a Reynolds number ranging from 3000 to 21,000. The segment considered for analysis consists of a circular tube of 68 mm diameter and 1.5 m length. The geometrical parameter considered is the perforation index (0%, 10%, 20%, and 30%). The constant heat flux is provided at the tube wall and a pressure-based solver is used for the solution. The studies are performed for analyzing the effects of inserts on the heat transfer and friction factor in the circular tube heat exchanger which results in augmented heat transfer at a higher perforation index (PI) and lower friction factor. The investigation results show that the highest heat transfer is 5.84 times over a simple plain tube and the maximum thermal performance factor (TPF) is 3.25 at PI = 30%, Re = 3000.

Keywords: heat exchanger; thermal performance; geometrical parameters; perforation; CFD

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1. Introduction

Nowadays, energy has become an integral part of life for human beings. Researchers are continuously carrying out research to improve the efficiency of devices. The heat exchanger (HE) is a device to exchange heat energy from one source to another and plays an important role in many industries. It has applications in industries such as power plants, refrigeration, air-conditioning, chillers, and many more. Hence, it requires improving the performance of HEs. The heat transfer rate is increased by increasing the surface area and roughness, and by significant change in the boundary conditions. The heat transmission process is executed in three ways: active, passive, and compound. In the active technique, there is a transfer of heat with the assistance of external equipment. In the passive method, the augmentation of heat transfer is completed with the help of the placement of the secondary heating surface—i.e., inserts/turbulators. The employment of both techniques together is carried out in the compound category.

In an experimental investigation, Akcayoglu [1] studied ducts with half delta wings of double row pairs with two different configurations. Double counter-twisted tapes used by Bhuiya et al. [2] in their investigation demonstrated improvements in thermal performance with the increase in the twist ratio of mild steel. Promvong et al. [3] used inclined vortex rings for investigation and found a 1.4 thermal performance factor at their lowest Reynolds number. Kumar et al. [4] found a maximum 1.47-times increment in thermal performance over a plain tube in their investigation of perforation in a circular ring with different perforation indexes. Zong et al. [5] used a hollow cross-disk insert for their numerical studies of the HE; as a results, they found that the flow nature was three-dimensional with turbulent flow. Hameed et al. [6] studied rectangular boxes and obtained that, for maximum outlet temperature, four inserts are to be placed in the fluid domain. Nagarajan

and Sivashanmugam [7] used a right–left helical spacer insert fitted in a circular tube in which they varied the twist ratio of the helix. They achieved improvement in heat transfer by increasing the value of Re and decreasing the value of the twist ratio. The study of an airfoil shaped insert by Gururatana et al. [8] revealed that the maximum TPF found was 1.45 when inserts were placed in 450. Aliabadi et al. [9] investigated a set of arrangements of delta winglets. They arranged 14 vortex-generator inserts with a forward and longitudinal arrangement of the delta winglets. The results showed that two-side-cut delta wings provide better heat transmission enhancement. The literature survey concludes that increasing the effectiveness of circular tube heat exchanger core surface disturbances plays an important role.

Double-sided delta-wing tape inserts have been investigated by Eiamsa-ard and Promvonge [10], in which they concluded that delta wings enhance both the heat transmission and performance of HE. In other studies, Eiamsa-ard and Promvonge [11] analyzed the performance of HE using counter-clockwise and clockwise twisted tape alternatively and used short-length twisted tapes [12] which generated strong swirl flow at the entry and improved the performance. Similarly, considering twin delta-winged twisted tape [13], coupling twisted tape [14], rectangular-cut twisted tapes used by Nakhchi and Esfahani [15], and using jagged twisted tape inserts by Rahimi et al. [16] were studied and achieved a reduction in pressure loss and higher fluid mixing due to higher vortex generation and obtained improved heat transfer characteristics. Singh et al. [17] experimentally investigated solid-hollow circular disks with rectangular winglets and noticed a thermal performance improvement in heat transmission over a simple plain tube (smooth circular tube without any type of insert). Similarly, researchers using circular-ring turbulators [18] and circular rings with twisted tape inserts [19] found enhancement in the heat transfer rate due to the formation of eddies in the former and due to the formation of swirl in addition to eddies in the latter. Gautam et al. [20] investigated using a perforated triple wing vortex generator; they found enhancement in heat transmission and thermal performance over a simple plain tube HE.

It is observed from the literature study that the inserts or turbulators help to reduce the friction factor near the inner wall surface and enhance the heat transfer. A triangular perforated Y-shaped insert in the test section may be one such type of turbulator for the study. The insert divides the fluid flow in three chambers of the Y-shape that reduces the fluid flow in the central core region; each chamber delivers fluid independently and perforation may create swirl that helps to reduce the thermal resistance, ensuring proper mixing of the fluid and enhancing the heat transfer. The numerical analysis of the present model has been carried out in ANSYS Fluent and a turbulence $k-\epsilon$ model has been used. In this computational research, the effect of the perforated Y-shaped insert on Nu , f , and TPF has been presented.

2. Geometry of Insert

Y-shaped inserts with triangular perforations have been used as turbulators. The perforations made are isosceles triangles and possess four different cases of perforation indexes viz. perforation index (PI) = 0%, 10%, 20%, and 30%. The physical model of the test segment consists of a circular channel with a 34-mm internal radius and 1500-mm length, as shown in Figure 1a,b. The Y shape is in three wings and aligned at 120 degrees to each other with a height of 30 mm throughout the length, which is perforated in a triangular shape in each of its wings of three cases of the perforation index (PI)—10%, 20%, and 30%. A non-perforated case has also been studied (PI = 0%). In the present analysis, the air is considered as a working fluid with the temperature as 300 K and a constant wall heat flux density (Q) = 1000 W/m² applied throughout the wall of the test section. The air properties are shown in Table 1. The analysis has been performed for varying the Reynolds number ranging from 3000 to 21,000 for different cases of triangular perforated Y-shaped inserts and the non-perforated case.

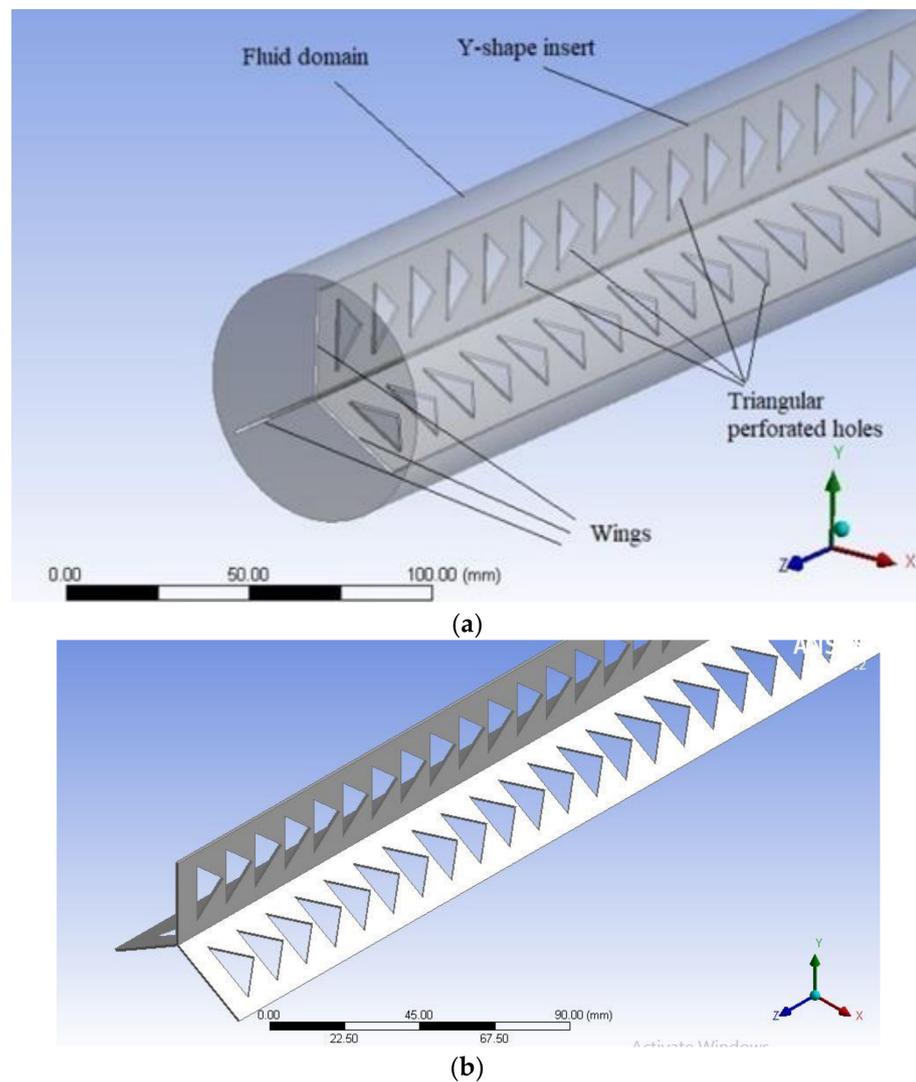


Figure 1. (a): Physical model of triangular perforated Y-shaped insert inside a circular tube; (b) triangular perforated Y-shaped insert for PI = 30%.

Table 1. Boundary condition and physical properties of air.

Boundary Condition	Values
Air temperature at inlet (K)	300
Inlet velocity (m/sec)	5.18, 4.44, 3.706, 2.963, 2.22, 1.48, 0.7409
Heat flux (W/m ²)	1000
Ambient Pressure (atm)	1
Density (kg/m ³)	1.225
Specific heat (J/kg ^{-K})	1006.53
Viscosity (kg/m ^{-s})	1.7894 × 10 ⁻⁵
Thermal conductivity (W/m ^{-K})	0.0242

3. Mathematical Calculations

The expressions used in this investigation are given as:

Reynolds number:

$$Re = \rho(vD)/\mu \tag{1}$$

Nusselt number:

$$Nu = \frac{hD}{k} \tag{2}$$

Heat transfer coefficient:

$$h = \frac{Q}{(T_{wm} - T_{fm})A} \tag{3}$$

$$h = \frac{(T_o - T_i)mc_p}{(T_{wm} - T_{fm})A} \tag{4}$$

where

$$T_{wm} = (1/A) \int_0^A (T)dA \tag{5}$$

$$T_{fm} = (T_o - T_i)/2 \tag{6}$$

For calculating the friction factor [16]:

$$f = \frac{\Delta P}{(\frac{\rho v^2}{D}) * (\frac{L}{2})} \tag{7}$$

The effectiveness of HE is measured in the form of the thermal performance factor (TPF) [21]:

$$TPF = \left(\frac{Nu}{Nus} \right) / \left(\frac{f}{f_s} \right)^{\frac{1}{3}} \tag{8}$$

The perforation index (PI) determined as:

$$PI = \frac{\text{Area of Perforated holes on surface}}{\text{Total area of the surface}} \tag{9}$$

4. Modelling and Grid Independence Test

4.1. Mathematical Modelling

The incompressible fluid flow is assumed to be at constant fluid flow properties and heat due to the radiation being assumed to be zero. The equations used for the model are given as follows [15]:

Continuity Equation:

$$\frac{\partial(\rho u_i)}{\partial x_i} = 0 \tag{10}$$

Momentum Equation:

$$\frac{\partial(\rho u_i u_j)}{\partial x_j} = -\frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_i} (\mu \frac{\partial u_i}{\partial x_i} - \overline{\rho u_i' u_j'}) \tag{11}$$

Energy Equation:

$$\frac{\partial(\rho u_i T_{fm})}{\partial x_i} = \frac{\partial}{\partial x_i} (k \frac{\partial T_{fm}}{\partial x_i}) \tag{12}$$

4.2. Numerical Model

A numerical investigation has been carried out to understand the improvement of the heat transmission mechanism in circular HE having triangular perforated Y-shaped inserts using the “Ansys” module in which the k-ε turbulence model has been used for calculation with the finite volume method. For this investigation, a 1.5-m-long section has been used for the testing, in which 1000 W/m² constant heat flux was provided at the tube wall. A pressure-based solver was employed for solving the equations. High Reynolds numbers between 3000 and 21,000 have been taken for this analysis based on the RNG k-ε model.

The boundary conditions and physical properties of air considered in the investigation are shown in Table 1.

4.3. Grid Independence Test (GIT)

The grid independence test has been conducted for determining the number of elements presented in Table 2. The deviation for 15, 24, 877 elements in the Nusselt number was 0.2% and the friction factor was 4.59%, which is satisfactory in terms of accuracy for the simulation. Hence, further computational analysis was performed, taking 15, 24, 877 elements. The meshing of the insert with triangular perforation is shown in Figure 2.

Table 2. Grid independence test.

Grid Number	Nu	$\left \frac{Nu_{i+1} - Nu_i}{Nu_{i+1}} \right $	f	$\left \frac{f_{i+1} - f_i}{f_{i+1}} \right $
50, 258	35.87	-	0.1486	-
98, 547	48.27	0.2569	0.1857	0.2001
3, 54, 782	60.12	0.1971	0.2106	0.1181
8, 84, 704	62.48	0.0378	0.2302	0.0852
15, 24, 877	62.49	0.0002	0.2413	0.0459

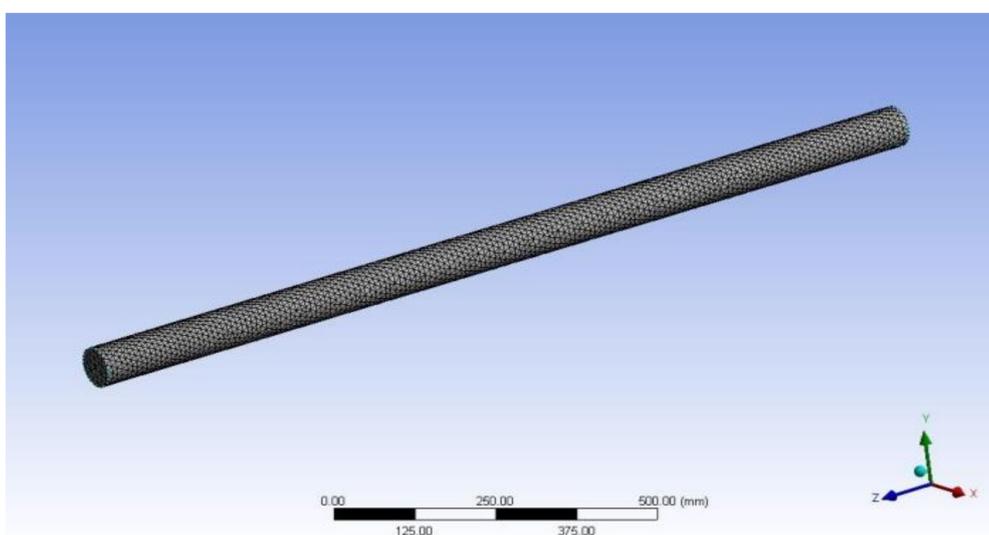


Figure 2. Meshing in Y-shaped insert with triangular perforation.

4.4. Model Validation

In order to verify the authenticity of the numerical model, the results for the smooth circular tube have been experimentally validated. The values obtained from numerical model of Nusselt number and friction factor are compared with the standard Dittus-Boelter equation and Blasius equation, respectively. The Dittus-Boelter equation and Blasius equation for the Nusselt number and friction factor are given in Equations (13) and (14), respectively.

$$Nu = 0.023 \times [\text{Re}]^{0.8} \times [\text{Pr}]^{0.4} \quad (13)$$

$$f = 0.316 \times [\text{Re}]^{(-0.25)} \quad (14)$$

The obtained results are presented in Figure 3. It can be seen in the figure that the obtained values of the Nusselt number and friction factor have shown good agreement with the experimental results with a deviation of $\pm 4\%$ and $\pm 6\%$, respectively.

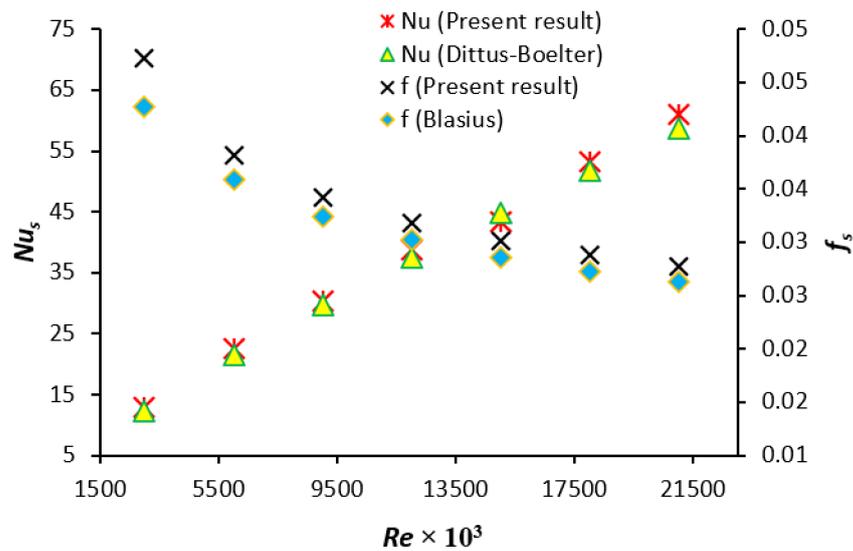


Figure 3. Validation of smooth tube result with standard equations for Nu and f .

5. Results

5.1. Effect on Nu

In Figure 4, variation of Nu with Re shows that as we increase the Reynolds number, the Nusselt number increased gradually. For the 30% perforation index case, the enhancement in the Nusselt number is 5.84 times over a simple plain tube. The increment in Nu is a result of increasing swirl for the higher range of Re , which enhanced fluid mixing inside the round tube. As Re increases, turbulence increases, which results in increment in the value of Nusselt number. The enhancement of Nu (rough tube) with respect to Nu_s (simple plain tube) is shown in Figure 5, which also reflects the similar nature of enhancement of heat transfer for the more perforated insert.

The temperature distribution created at the wall of tube due to Y-shaped triangular perforated insert and variation of temperature at the outlet are shown in Figure 6.

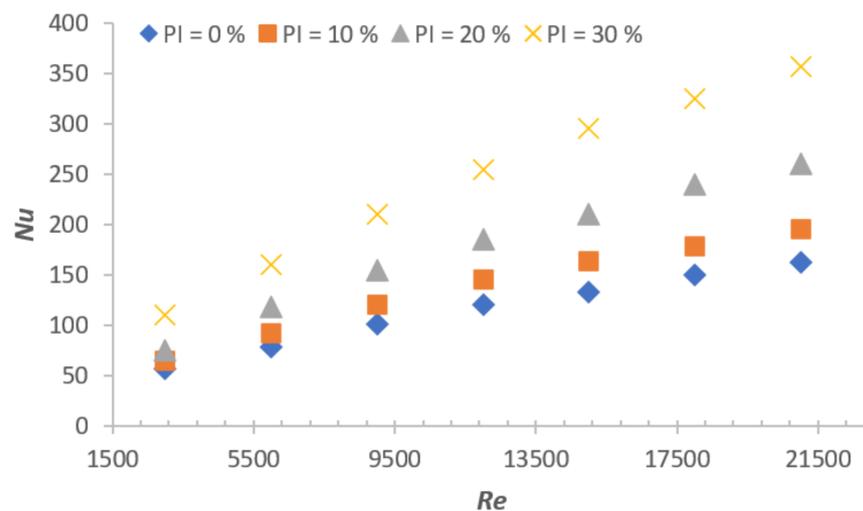


Figure 4. Variation of Nu with Re .

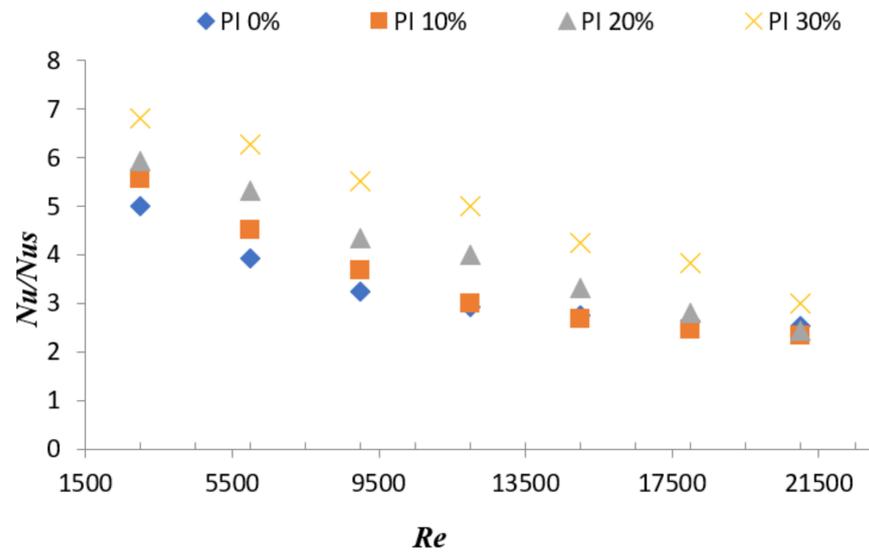


Figure 5. Variation of Nu/Nus with Re .

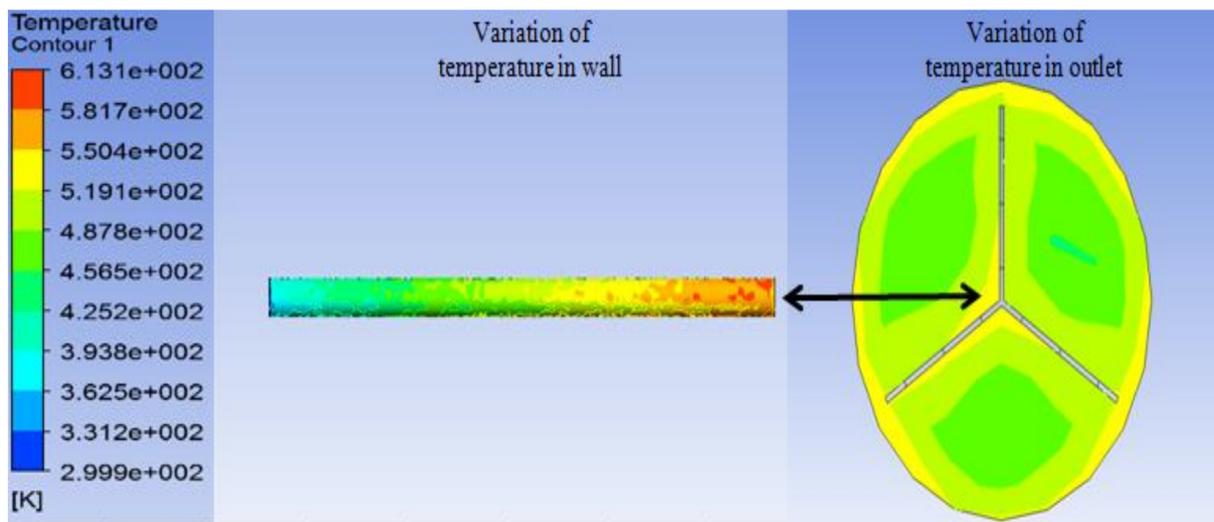


Figure 6. Temperature contours at wall and outlet.

5.2. Effect on f

The friction factor alters the thermal performance of HE. It is expected that the higher the friction factor, the lower the performance of HE. In case of $PI = 20\%$, the friction factor was found higher at the Reynolds number between 3000 and 21,000. This is similar in case of the 10% perforation, the reason being the higher friction factor due to hole variation in the perforation of Y-shaped insert. Variation of f with Re is presented in Figure 7; however, comparison of f (rough tube) with respect to f_s (smooth tube) is shown in Figure 8, in which a similar nature is shown for 20% perforation.

5.3. Effect on TPF

The maximum thermal performance (TPF) was found to be 3.25 in the case of the 30% perforation index at Reynolds number 3000. It can be noticed in Figure 9, that lower Re results in better heat transmission performance. This happens because at higher velocities, the test section undergoes a higher pressure drop; hence, the friction factor increases and thermal performance decreases.

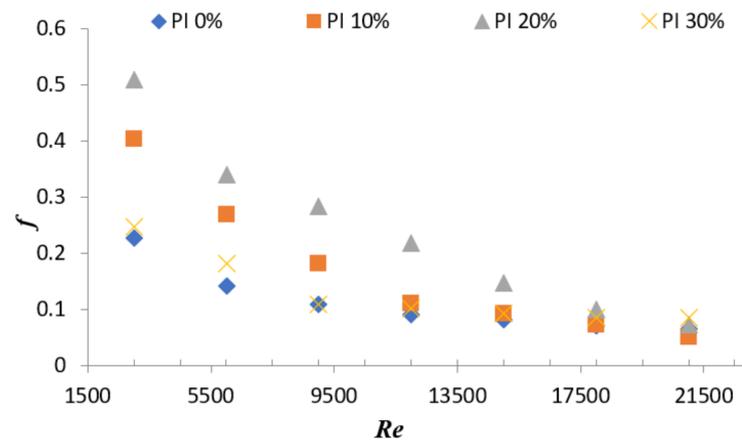


Figure 7. Variation of f with Re .

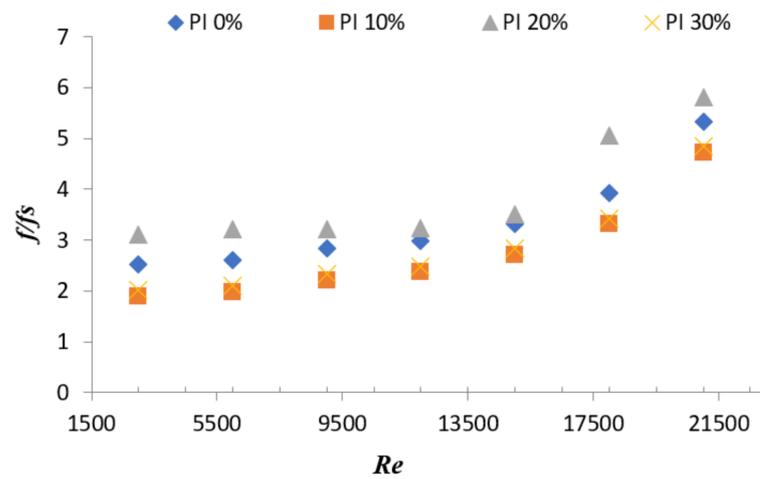


Figure 8. Variation of f/fs with Re .

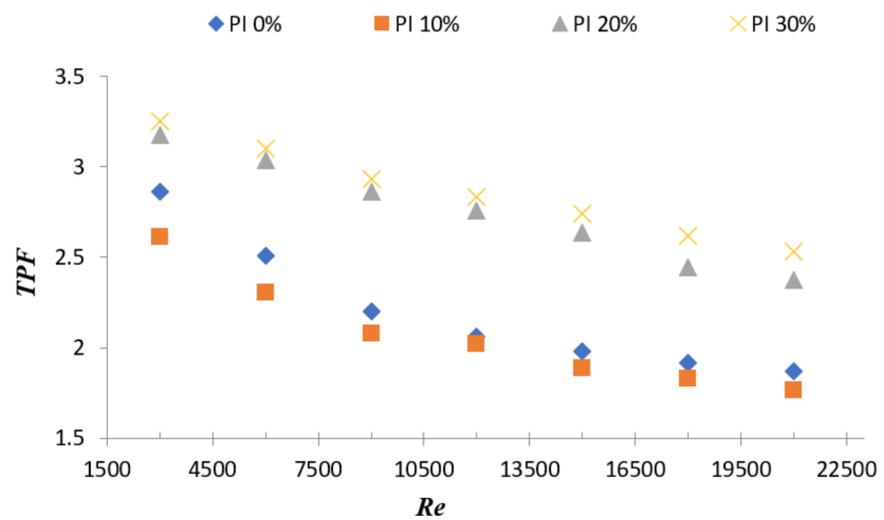


Figure 9. Variation of TPF with Re .

6. Comparison with Previous Work

In Figure 10, comparison of the present study geometry—a Y-shaped insert with triangular perforation—with previously published works has been carried out. The comparison is made in the same range of Reynolds number. The research works considered are: Bhuyia et al. [2], using double counter-twisted tape inserts; Promvong et al. [3], using inclined vortex rings; Kumar et al. [4], using circular rings; Eiamsa-ard et al. [9], using a double-sided delta wing tape insert; Singh et al. [16], using a solid-hollow circular disk with rectangular winglets; and Gautam et al. [19], using a perforated triple-wing vortex generator. It can be seen from Figure 10, that the Y-shaped insert with triangular perforation provides the highest thermal performance factor among all others set of geometries of previous researchers.

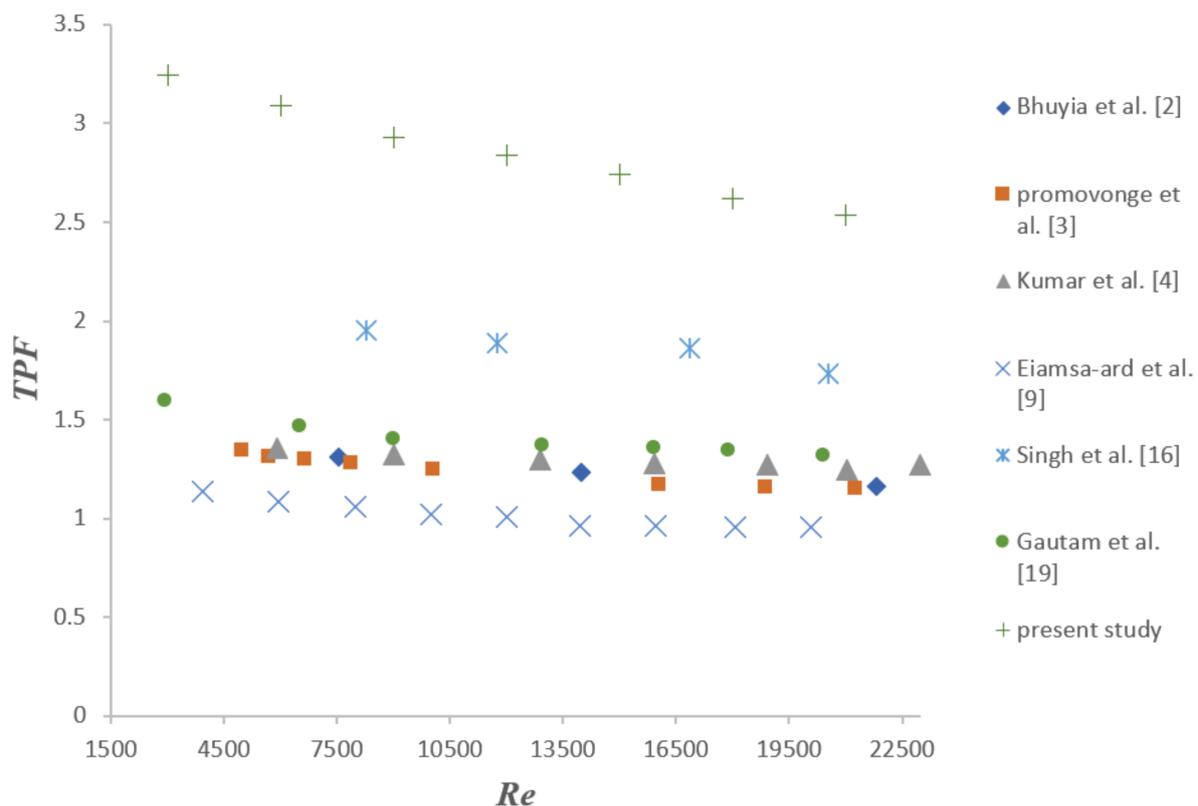


Figure 10. Comparison of triangular perforated Y-shaped insert with previously published works.

7. Conclusions

Under the present work, numerical investigation has been carried out considering the triangular perforated Y-shaped insert in the circular tube HE. Based on the obtained results, it can be said that there are a significant effects of the perforation ratio of triangular perforated Y-shaped inserts on Nu , f , and TPF . The major conclusions drawn from the study are as follows:

- The results show that increasing Re provides better heat transmission characteristics for higher perforated inserts along with decreasing the friction factor. Furthermore, a lower range of Reynolds number gives a higher value of TPF .
- The Nu varies between 60 to 210 with an increase in PI from 0% to 30% under the range of Reynolds number between 3000 and 21,000, whereas the friction factor varies between 0.05 and 0.51 with an increase in PI from 0% to 30% under the range of Reynolds number between 3000 and 21,000.

- The maximum TPF found is 3.25 at perforation index = 30% and $Re = 3000$. The enhancement in heat transmission is found 5.84 times better compared to the simple plain tube.
- It has also been observed from the study that this type of insert may be useful for industrial application because it significantly augments heat transmission by more than of five times and the thermal performance is enhanced by more than three times. The present study showed better heat transmission characteristics as compared to other research in the same range of Reynolds number.

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Nomenclature

A	Area of circular pipe (m^2)
C_p	Specific heat of air ($J/kg^{-1} K^{-1}$)
D	Test segment diameter (m)
f	Friction factor for rough tube
f_s	Friction factor for simple plain tube
h	Average convective heat transfer coefficient ($W m^{-2} K^{-1}$)
k	Thermal conductivity of air ($Wm^{-1} k^{-1}$)
L	Test section length (m)
m	Air flow rate ($kg s^{-1}$)
Nu	Nusselt number
Nu_s	Nusselt number for simple plain tube
P_A	Perforated area of insert (m^2)
Pr	Prandtl number
Q	Heat flux (W)
Q_{air}	Heat carried by air (W)
Q_{conv}	Heat transfer by convection (W)
Re	Reynolds number
T_A	Total area of Y-shaped insert (m^2)
T_{fm}	Fluid mean temperature (K)
T_i	Air temperature at inlet (K)
T_o	Air temperature at outlet (K)
T_{wm}	Wall mean temperature (K)
v	Velocity of air (ms^{-1})
ΔP	Pressure difference (between inlet and outlet of the test segment) (Pa)

Abbreviations

TPF	Thermal performance factor
PI	Perforation index (P_A/T_A)

References

1. Akcayoglu, A. Flow past confined delta-wing type vortex generators. *Exp. Therm. Fluid Sci.* **2011**, *35*, 112–120. [[CrossRef](#)]
2. Bhuiya, M.M.K.; Sayema, A.S.M.; Islam, M.; Chowdhury, M.S.U.; Shahabuddin, M. Performance assessment in a heat exchanger tube fitted with double counter twisted tape inserts. *Int. Commun. Heat Mass Transf.* **2014**, *50*, 25–33. [[CrossRef](#)]
3. Promvong, P.; Koolnapadol, N.; Pimsarn, M.; Thianpong, C. Thermal performance enhancement in a heat exchanger tube fitted with inclined vortex rings. *Appl. Therm. Eng.* **2014**, *62*, 285–292. [[CrossRef](#)]
4. Kumar, A.; Chamoli, S.; Kumar, M. Experimental investigation on thermal performance and fluid flow characteristics in heat exchanger tube with solid hollow circular disk inserts. *Appl. Therm. Eng.* **2016**, *100*, 227–236. [[CrossRef](#)]
5. Zong, Y.; Bai, D.; Zhou, M.; Zhao, L. Numerical studies on heat transfer enhancement by hollow-cross disk for cracking coils. *Chem. Eng. Process. Process Intensif.* **2019**, *135*, 82–92. [[CrossRef](#)]

6. Hameed, V.; Hussein, M. Effect of new type of enhancement on inside and outside surface of the tube side in single pass heat Exchanger. *Appl. Therm. Eng.* **2017**, *122*, 484–491. [[CrossRef](#)]
7. Nagarajan, P.K.; Sivashanmugam, P. Heat Transfer Enhancement Studies in a Circular Tube Fitted with Right-Left Helical Inserts with Spacer, World Academy of Science, Engineering and Technology. *Int. J. Mech. Mechatron. Eng.* **2011**, *5*, 2091–2095.
8. Gururatana, S.; Skullong, S. Experimental investigation of heat transfer in a tube heat exchanger with airfoil-shaped insert. *Case Stud. Therm. Engin.* **2019**, *14*, 100462. [[CrossRef](#)]
9. Khoshvaght-Aliabadi, M.; Sartipzadeh, O.; Alizadeh, A. An experimental study on vortex-generator insert with different arrangements of delta-winglets. *Energy* **2015**, *82*, 629–639. [[CrossRef](#)]
10. Eiamsa-ard, S.; Promvong, P. Influence of Double-sided Delta-wing Tape Insert with Alternate-axes on Flow and Heat Transfer Characteristics in a Heat Exchanger Tube, fluid flow and transport phenomena. *Chin. J. Chem. Eng.* **2011**, *19*, 410–423. [[CrossRef](#)]
11. Eiamsa-ard, S.; Promvong, P. Performance assessment in a heat exchanger tube with alternate clockwise and counter-clockwise twisted-tape inserts. *Int. J. Heat Mass Transf.* **2010**, *53*, 1364–1372. [[CrossRef](#)]
12. Eiamsa-ard, S.; Thianpong, C.; Eiamsa-ard, P.; Promvong, P. Convective heat transfer in a circular tube with short length twisted tape insert. *Int. Commun. Heat Mass Transf.* **2009**, *36*, 365–371. [[CrossRef](#)]
13. Eiamsa-ard, S.; Nuntadusit, C.; Promvong, P. Effect of twin delta-winged twisted-tape on thermal performance of heat exchanger tube. *Heat Transf. Eng.* **2013**, *34*, 1278–1288. [[CrossRef](#)]
14. Eiamsa-ard, S.; Nanan, K.; Thianpong, C.; Eiamsa-ard, P. Thermal performance evaluation of heat exchanger tubes equipped with coupling twisted tapes. *Exp. Heat Transf.* **2013**, *26*, 413–430. [[CrossRef](#)]
15. Nakhchi, M.E.; Esfahani, J.A. Numerical investigation of rectangular-cut twisted tape insert on performance improvement of heat exchangers. *Int. J. Therm. Sci.* **2019**, *138*, 75–83. [[CrossRef](#)]
16. Rahimi, M.; Shabani, S.R.; Alsairafi, A.A. Experimental and CFD studies on heat transfer and friction factor characteristics of a tube equipped with modified twisted tape inserts. *Chem. Eng. Process. Process. Intensif.* **2009**, *48*, 762–770. [[CrossRef](#)]
17. Singh, S.; Negi, J.S.; Bisht, S.; Sah, H. Thermal performance and frictional losses study of solid hollow circular disc with rectangular wings in circular tube. *Heat Mass Transf.* **2019**, *55*, 2975–2986. [[CrossRef](#)]
18. Kongkaitpaiboon, V.; Nanan, K.; Eiamsa-ard, S. Experimental investigation of convective heat transfer and pressure loss in a round tube fitted with circular-ring turbulators. *Int. Comm. Heat Mass Transf.* **2010**, *37*, 568–574. [[CrossRef](#)]
19. Eiamsa-ard, S.; Kongkaitpaiboon, V.; Nanan, K. Thermohydraulics of turbulent flow through heat exchanger tubes fitted with circular-rings and twisted tapes. *Chin. J. Chem. Eng.* **2013**, *21*, 585–593. [[CrossRef](#)]
20. Gautam, A.; Pandey, L.; Singh, S. Influence of perforated triple wing vortex generator on a turbulent flow through a circular tube. *Heat and Mass Transfer.* **2018**, *54*, 2009–2021. [[CrossRef](#)]
21. Webb, R.L. Performance evaluation criteria for use of enhanced heat transfer surfaces in heat exchanger design. *Int. J. Heat Mass Transf.* **1981**, *24*, 715–726. [[CrossRef](#)]