

Supplementary Information for

Chitosan-based grafted cationic magnetic material to remove emulsified oil in wastewater:

Performance and mechanism

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Materials and methods

- S1. Schematic diagram of particle image velocimetry setup
- S2. DLVO, EDLVO, and MDLVO theory

Results and discussion

- S3. The effect of initial oil concentration.
- S4. The comparison of the reported removal efficiency of different magnetic flocculants for emulsified oily wastewater.
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Materials and methods

S1. Schematic diagram of particle image velocimetry setup

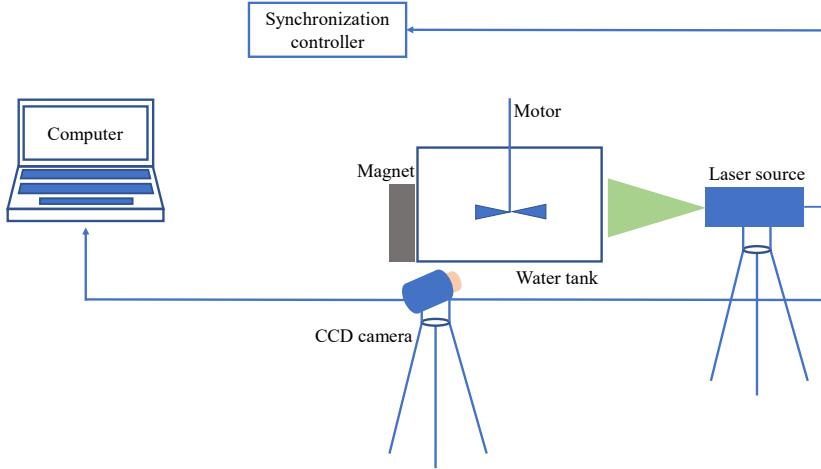


Figure S1 Schematic diagram of Particle Image Velocimetry setup.

S2. DLVO, EDLVO, and MDLVO theory

The magnetic flocculation mechanism of emulsified oil droplets and FS@CTS-P(AM-DMC) was analyzed using the modified DLVO theory. For the classical DLVO model, the total interaction energy (U_{DLVO}) between surfaces is the sum of the van der Waals interaction energy (U_{vdw}) and the electrostatic interaction energy (U_{EL}). In the extended DLVO (EDLVO) theory, the total interaction energy includes the van der Waals interaction energy (U_{vdw}), the electrostatic interaction energy (U_{EL}), and the Lewis acid-base interaction energy (U_{AB}). In the magnetically modified EDLVO theory, the total interaction energy needs to consider the magnetic interaction energy (UM). The total interaction energy between interacting particles can be calculated using the following Equations:

$$U_{DLVO}(h) = U_{vdw}(h) + U_{EL}(h) \quad (S1)$$

$$U_{EDLVO}(h) = U_{DLVO}(h) + U_{AB}(h) \quad (S2)$$

$$U_{MDLVO}(h) = U_{EDLVO}(h) + U_M(h) \quad (S3)$$

The four types of interaction forces can be simulated by Equation S4-S7:

$$U_{vdw}(h) = -\frac{AR_1R_2}{6h(R_1+R_2)} \quad (S4)$$

$$U_{EL}(h) = \frac{\pi\epsilon R_1R_2(\psi_1^2+\psi_2^2)}{(R_1+R_2)} \left[\frac{2\psi_1\psi_2}{\psi_1^2+\psi_2^2} \ln \frac{1+\exp(-kh)}{1-\exp(-kh)} + \ln \{1-\exp(-2kh)\} \right] \quad (S5)$$

$$U_{AB}(h) = 2\pi \frac{R_1R_2}{R_1+R_2} \lambda \Delta G_{h_0}^{AB} [\exp(h_0 - h) / \lambda] \quad (S6)$$

$$U_M(h) = -\frac{8\pi\mu_0 M_S^2 R^3}{9\left(\frac{h}{R}\right)^3} \quad (S7)$$

All the parameters used in the above equations were detailedly summarized in Tables S1-S3:

Table S1 Parameters used in DLVO, EDLVO and MDLVO equations.

R	The radius of FS@CTS-P(AM-DMC) and emulsified oil droplet.
A_{132}	The effective Hamaker constant (J) for particles (1) interacting with particles (2) in the aqueous medium (3).
h_0	The shortest distance between the particles, 0.157 nm [1].
h	The separation distance between the two interacting particles (nm).
κ	The inverse of the Debye length (m^{-1}).
λ	The correlation length of molecules in the liquid medium, 0.6 nm.
ϵ	The dielectric constant of the solution, ($80 \times 8.854 \times 10^{-12} C^2/J/m$ for aqueous).
ψ	The zeta potential of colloidal particles (mV).
N_A	Avogadro's number, $6.02 \times 10^{23} mol^{-1}$.
e	Elementary charge, $1.602 \times 10^{-19} C$.
T	Absolute temperature, 298 K.
K	Boltzmann constant, $1.38 \times 10^{-23} J/K$.
I	Ionic strength
μ_0	The magnetic permeability of vacuum ($\mu_0 = 1.26 \times 10^{-6} Tm \cdot A^{-1}$).
M_s	The magnetization of the particles, $A \cdot m^{-1}$.

Table S2 Characteristics of FS@CTS-P(AM-DMC) and emulsified oil droplet.

Characteristics	FS@CTS-P(AM-DMC)	emulsified oil droplet
Particle radius (nm)	10300	1585
Magnetic saturation (kA/m)	53.81	-

Table S3 Surface tension and components of liquid (mJ/m^2).

Liquid	γ_L	$\gamma_L^{LW}(\gamma_L^d)$	$\gamma_L^{AB}(\gamma_L^p)$	γ_L^+	γ_L^-
Water	72.8	21.8	51.0	25.5	25.5
Diiodomethane	58.0	39.0	19.0	2.28	39.6
Formamide	50.8	50.8	0	0	0

The contact angle (θ) of FS@CTS-P(AM-DMC) was measured using a contact angle measurement instrument (OCA20, Dataphysics, Germany). For emulsified oil whose surface tension components were not readily available, the pendant drop method was used to determine the surface tension components [2]. Then, according to the Extended Young's equation (Equation S8), the polar and apolar surface tensions were calculated, as summarized in Table S4 for contact angles and polar surface tension. The Hamaker constant was calculated

based on these surface tension results, as shown in Table S5.

$$\gamma_L(1 + \cos\theta) = 2(\gamma_B^{LW}\gamma_B^{LW})^{1/2} + 2(\gamma_B^+\gamma_B^-)^{1/2} + 2(\gamma_B^-\gamma_B^+)^{1/2} \quad (\text{S8})$$

$$A = -12\pi h_0^2 \Delta G_{adh}^{LW} \quad (\text{S9})$$

$$\Delta G_{adh}^{LW} = -2\gamma_{BL}^{LW} = -2 \times \left(\sqrt{\gamma_B^{LW}} - \sqrt{\gamma_L^{LW}} \right)^2 \quad (\text{S10})$$

Table S4 The contact angles for flocculants and the calculated surface tension energy components.

Surface	Contact angles (°)			Surface tension (mJ/m ²)		
	Water	Formimide	Diiodomethane	γ_i^{LW}	γ_i^+	γ_i^-
FS@CTS-P(AM-DMC)	13.09	17.94	20.09	47.76	0.11	56.34
emulsified oil droplet	-	-	-	35.03	2.34	54.95

Table S5 The Hamaker constants for the interacting emulsified oil droplets and flocculants.

Surface	A ₁₃₁ /A ₁₃₂ (J)	
	FS@CTS-P(AM-DMC)	emulsified oil droplet
FS@CTS-P(AM-DMC)	9.34×10 ⁻²¹	5.21×10 ⁻²¹
emulsified oil droplet	5.21×10 ⁻²¹	2.9×10 ⁻²¹

Results and discussion

S3. The effect of initial oil concentration.

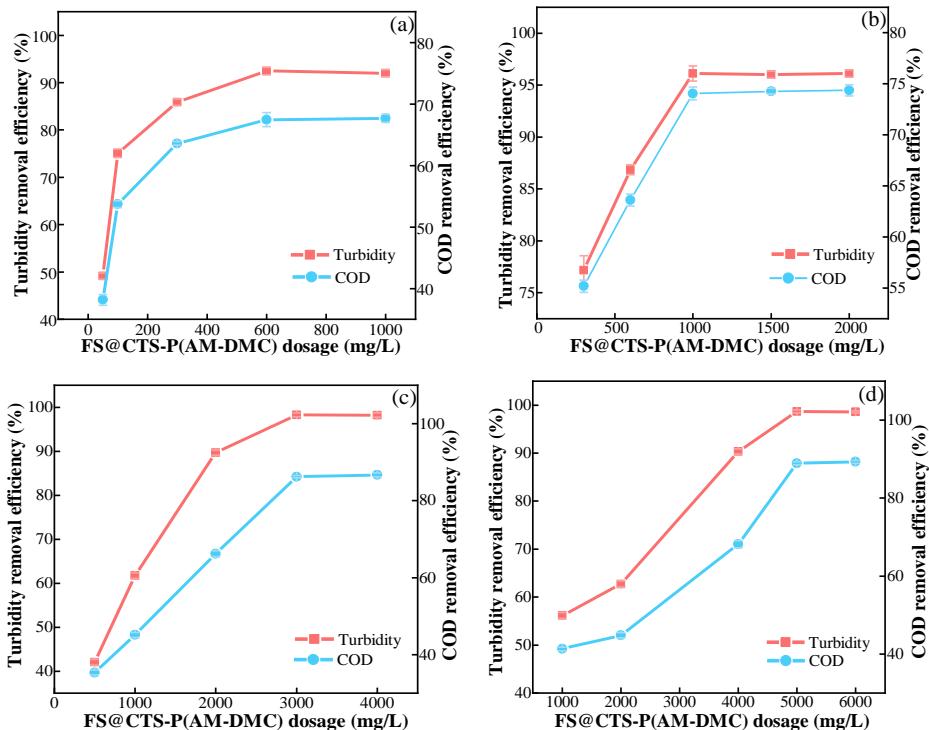


Figure S2 Effect of initial oil concentration on removal efficiency using FS@CTS-P(AM-DMC), (a)200 mg/L, (b)500 mg/L, (c)2000 mg/L, (d)3000 mg/L. Stirring speed = 400 r/min. Stirring time = 10 min. Settling time = 3 min.

S4. The comparison of the reported removal efficiency of different magnetic flocculants for emulsified oily wastewater.

Table S6 Comparison of the reported removal efficiency of different magnetic flocculants for emulsified oily wastewater.

Materials	Water quality parameters of raw water	Removal efficiency	Dosage	Reference
PAM-g-MagCell	Turbidity: 492 NTU COD: 12553 mg/L oil concentration: 0.3 wt%	Turbidity removal: 88.62 % COD removal: 53.23 % demulsification efficiency (ED):97%	1500 mg/L 3 g/L	[3] [4]
Fe ₃ O ₄ @OA	oil concentration: 10.3-14.6 mg/L	Oil removal:95.79 %		
FS-MC	Turbidity: 26.1-37.6 NTU COD: 40.6-90.3 mg/L	Turbidity removal: 87.85 % COD removal: 66.67 %	4-6 ml/L	[5]
FS-MC	oil concentration: 130±20 mg/L	Oil removal:93 %	2 mg/L	[6]
Fe ₃ O ₄ @SiO ₂ @Epoxy	oil concentration: 7.4 g/L	Oil removal:92.3 %	2.5 g/L	[7]
PVP- coated NPs	oil concentration: 150±5 mg/L	Oil removal: 99 %	4.4ppm-70.2ppm	[8]
PVP-coated Fe ₃ O ₄ MNPs	oil concentration: 2700 mg/L	Oil removal: 90-99 %	1-2 g/L	[9]
EP@APTES-Fe ₃ O ₄	oil concentration: 1.0 wt%	ED:95%	500 mg/L	[10]
QC-grafted MNPs	oil concentration: 0.2 wt%	ED:90-100 %	0-1.8 g/L	[11]
Fe ₃ O ₄ @OA	oil concentration: 10 g/L	Oil removal: 98%	30 g/L	[12]
Fe ₃ O ₄ @OA	oil concentration: 3.3 g/L	Oil removal: 97%	100 g/L	[13]
oil concentration: 1000 mg/L				
FS@CTS-P(AM- DMC)	Turbidity: 950 ± 50 NTU COD: 1150 ± 50 mg/L	Turbidity removal: 96.4 % COD removal: 74.5 %	2 g/L	this study

S5. The effect of magnetic field strength.

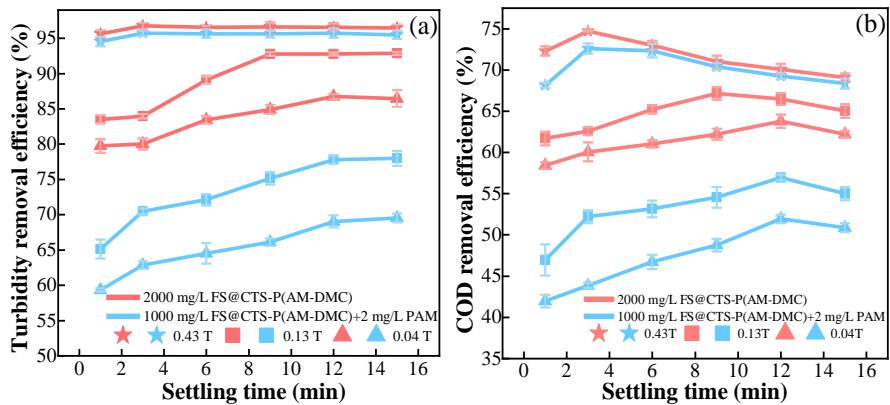


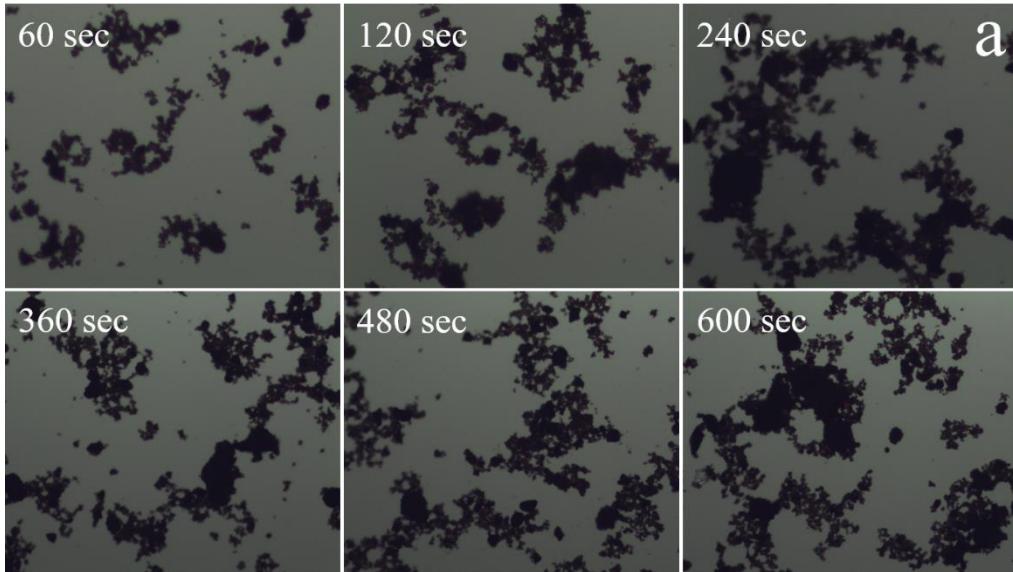
Figure S3 Effect of magnetic field strength on removal (a) turbidity and (b) COD efficiency. Stirring speed = 400 r/min. Stirring time = 10 min.

S6. The evolution of Floc size formed by FS@CTS-P(AM-DMC) under different dosing strategies and pH levels.

Table S7 The properties of flocs under different dosing modes and pH levels.

Dosing mode	pH	Rapid stirring growth rate ($\mu\text{m min}^{-1}$)	Magnetic separation growth rate ($\mu\text{m min}^{-1}$)	Strength factor (%)	Recovery factor (%)
2000 mg/L FS@CTS-P(AM-DMC)	5.0	12.30	14.75	75.10	80.53
	7.0	11.88	14.42	69.27	76.79
	9.0	9.78	14.14	65.08	73.14
1000 mg/L FS@CTS-P(AM-DMC) + PAM 2 mg/L	5.0	15.63	43.14	47.41	57.88
	7.0	14.86	44.64	46.73	51.47
	9.0	14.32	44.86	44.52	52.22

S7. The microscopic images of FS@CTS-P(AM-DMC)-emulsified oil flocs during rapid stirring process.



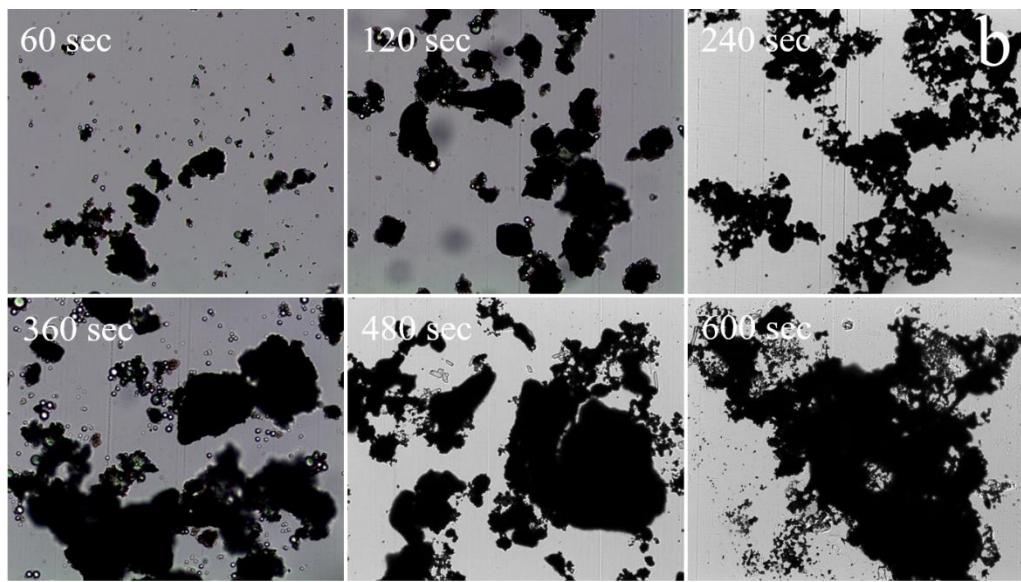
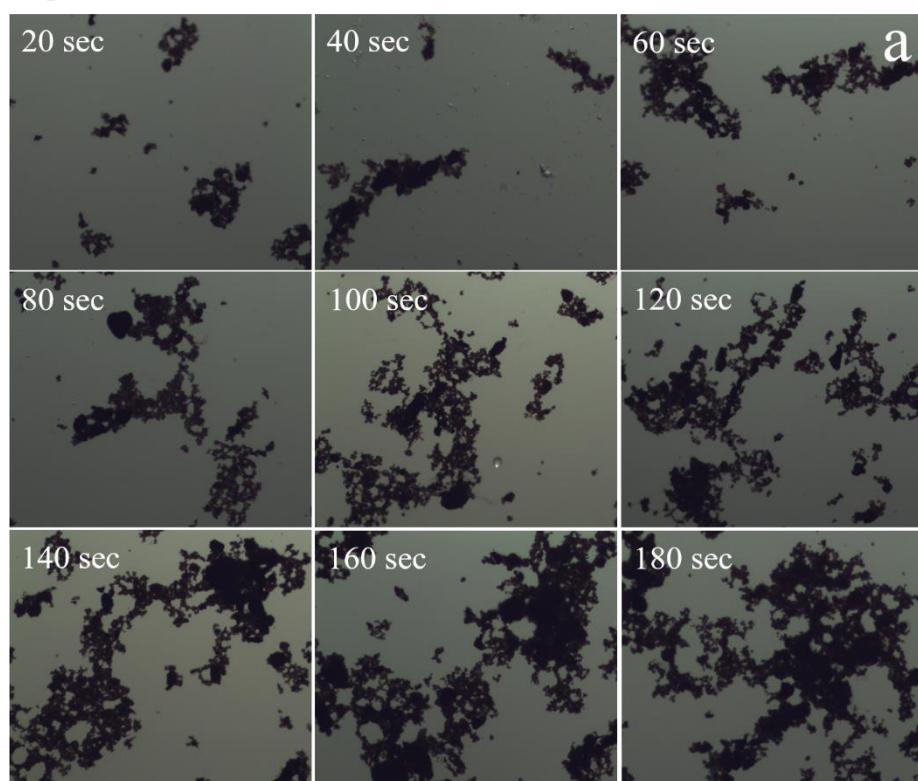


Figure S4 The microscopic images of FS@CTS-P(AM-DMC)-emulsified oil flocs during rapid stirring process for two dosing modes, (a) 2000 mg/L FS@CTS-P(AM-DMC), (b) 1000 mg/L FS@CTS-P(AM-DMC) + 2 mg/L PAM. pH = 7.0. Stirring speed = 400 r/min. Stirring time = 10 min.

S8. The microscopic images of FS@CTS-P(AM-DMC)-emulsified oil flocs during magnetic separation process.



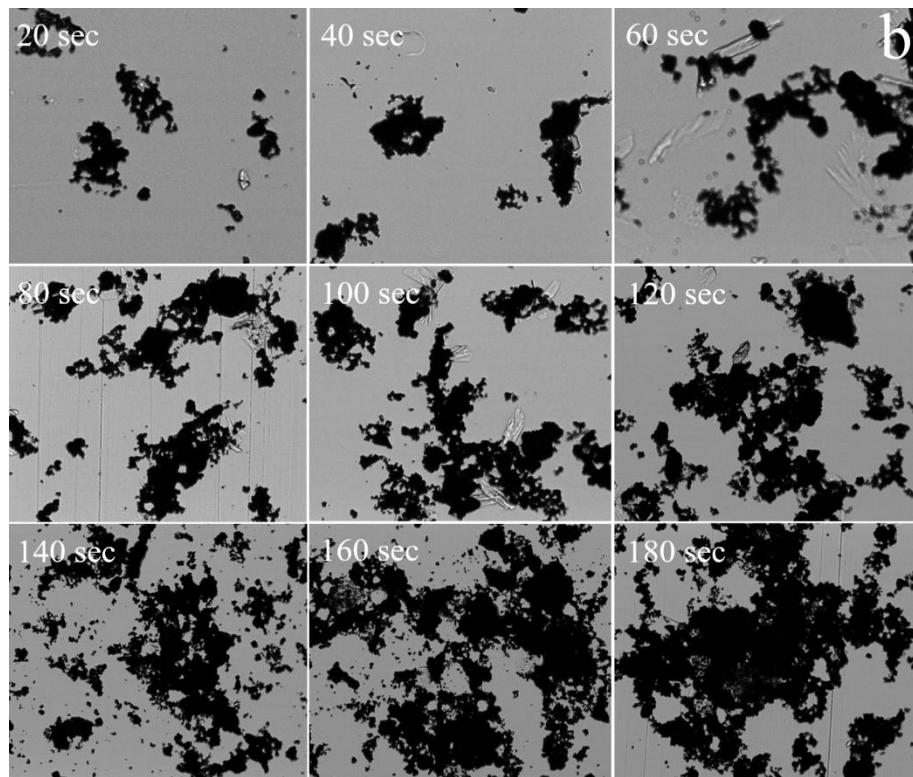
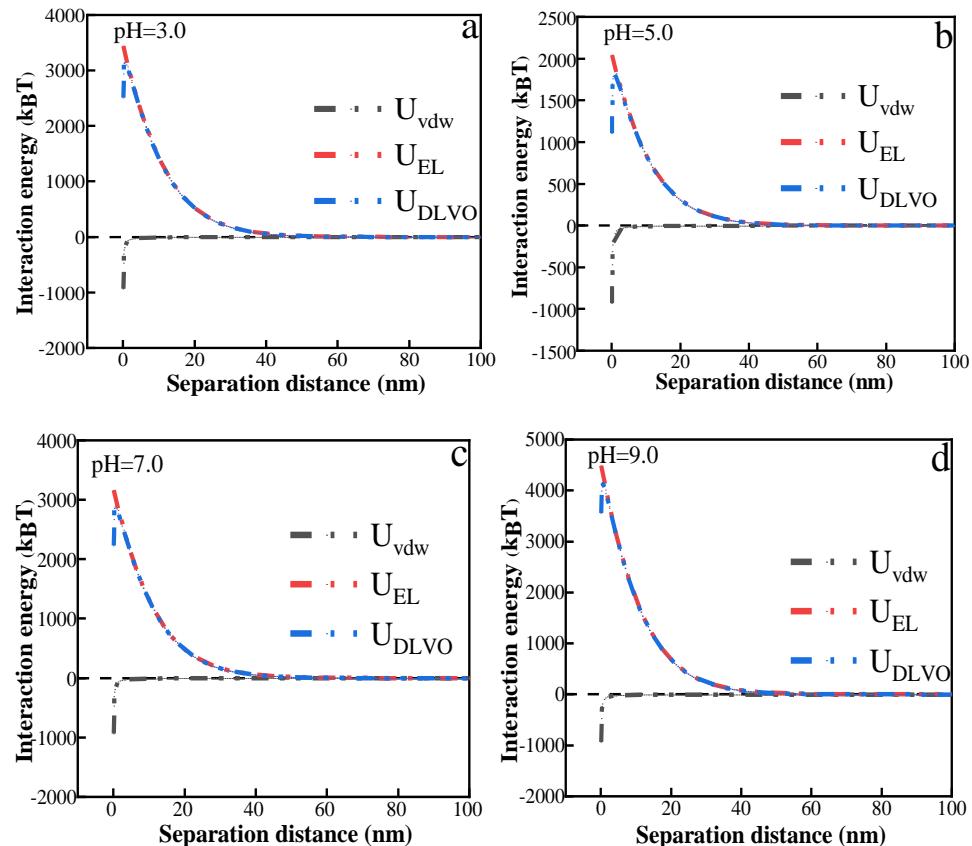


Figure S5 The microscopic images of FS@CTS-P(AM-DMC)-emulsified oil flocs during magnetic separation process for two dosing modes, (a) 2000 mg/L FS@CTS-P(AM-DMC), (b) 1000 mg/L FS@CTS-P(AM-DMC) + 2 mg/L PAM. pH = 7.0. Stirring speed = 400 r/min. Settling time = 3 min.

S9. The DLVO analysis between emulsified oil droplet and emulsified oil droplet.



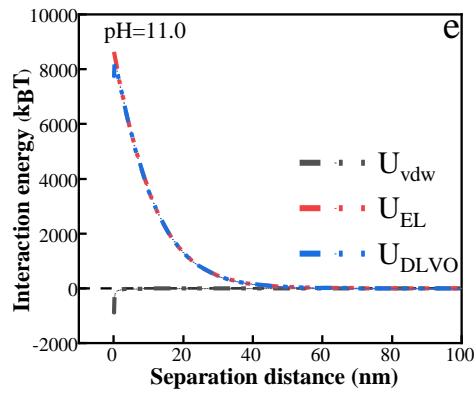


Figure S6 Interaction energy versus interaction distance between different interacting entities: oil droplet and emulsified oil droplet (a-e).

S10. The DLVO analysis between emulsified oil droplet and FS@CTS-P(AM-DMC).

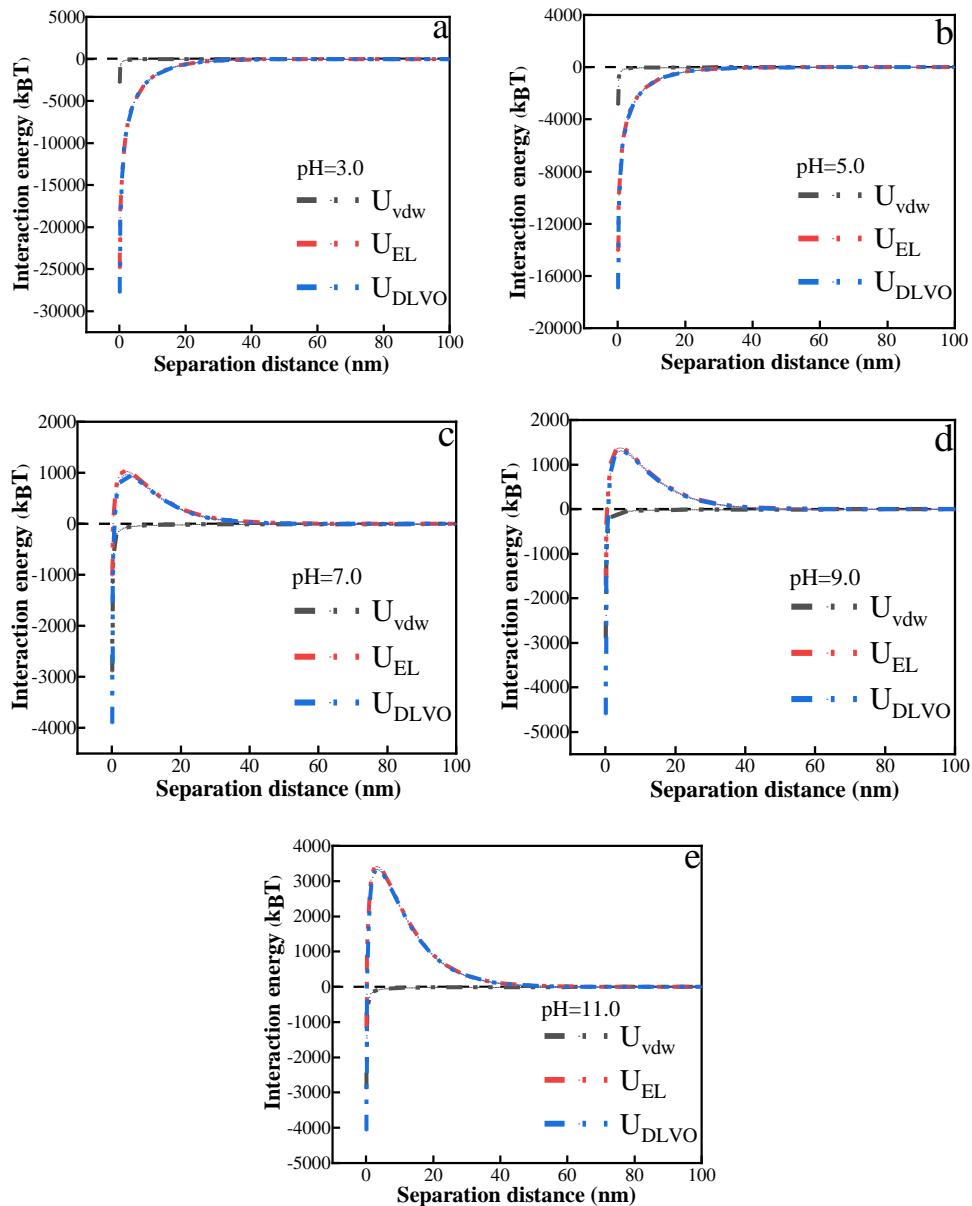


Figure S7 Interaction energy versus interaction distance between different interacting entities: oil droplet

and FS@CTS-P(AM-DMC) (a-e).

S11. The DLVO analysis between FS@CTS-P(AM-DMC) and FS@CTS-P(AM-DMC).

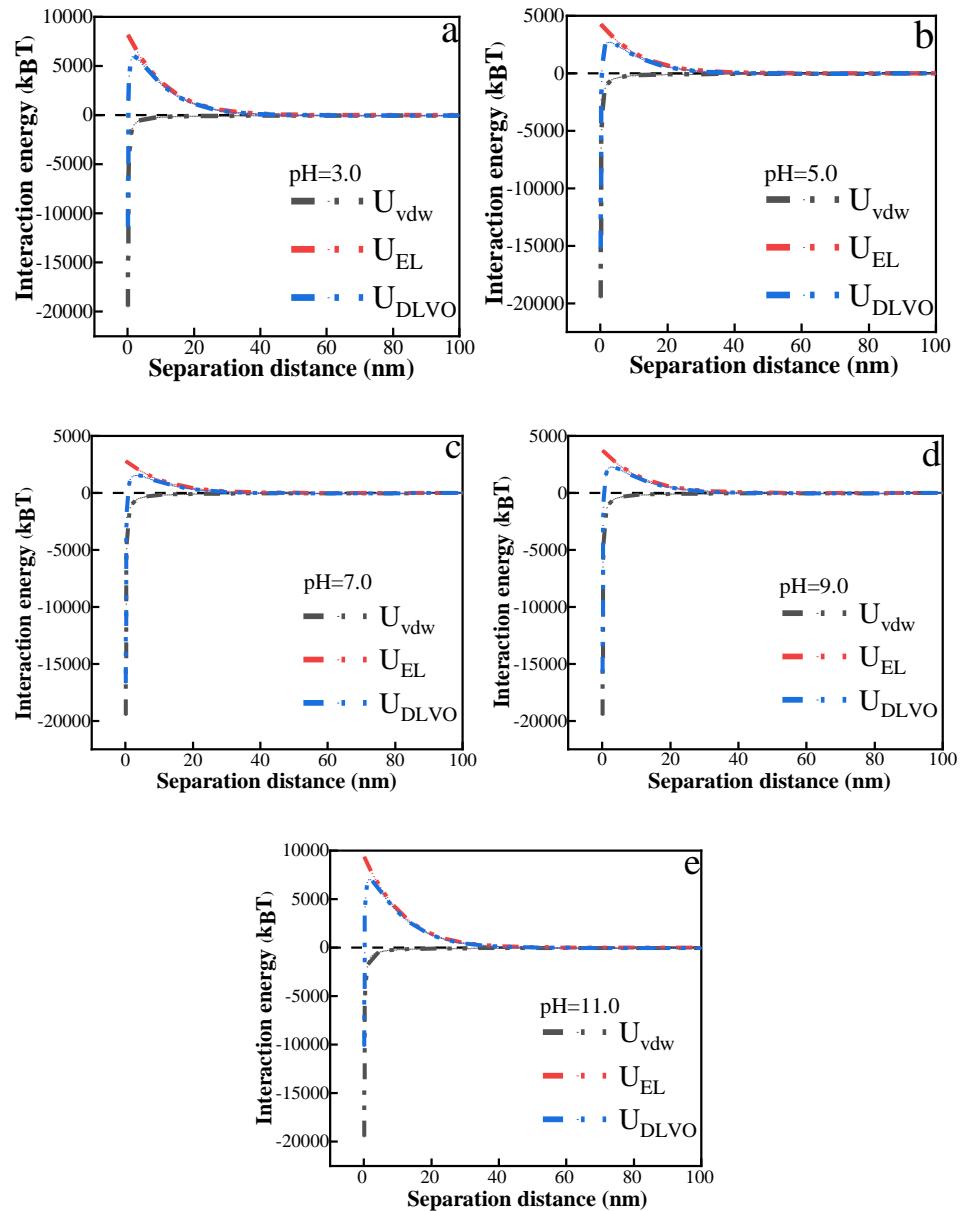


Figure S8 Interaction energy versus interaction distance between different interacting entities: FS@CTS-P(AM-DMC) and FS@CTS-P(AM-DMC) (a-e).

S12. The EDLVO analysis

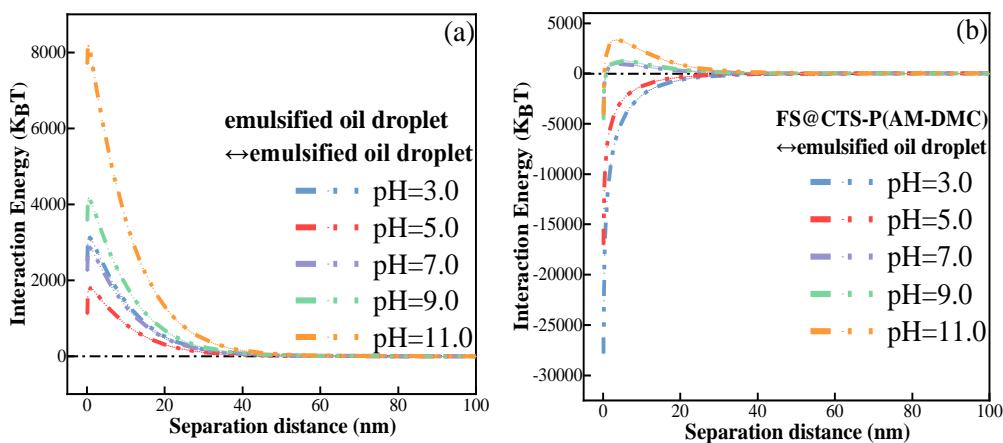


Figure S9 Interaction energy of EDLVO between (a) oil emulsified droplet and oil emulsified droplet, (b) FS@CTS-P(AM-DMC) and oil emulsified droplet.

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