

# Optimization of Manganese Recovery from a Solution Based on Lithium-Ion Batteries by Solvent Extraction with D2EHPA

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**Table S1.** Conditions of the experimental design and concentrations of metals in the raffinate and in the organic phase after one extraction stage. Contact time of 10 min. Legend: [aq]: concentration of metal in aqueous phase, [org] concentration of meta in organic phase.

Standard Order	Random order	Coded variables			Real variables			Mn		Co		Ni		Li	
		pH	O:A	D2EHPA	pH	O:A	D2EHPA	[aq]	[org]	[aq]	[org]	[aq]	[org]	[aq]	[org]
1	6	-1	-1	-1	2.5	0.5	0.4	6.05	2.97	18.15	0.67	7.96	< 0.01	1.04	0.01
2	11	1	-1	-1	4	0.5	0.4	3.67	7.74	16.35	4.33	7.47	0.98	0.96	0.18
3	10	-1	1	-1	2.5	2	0.4	2.97	2.28	17.82	0.35	7.92	0.02	1.01	0.02
4	4	1	1	-1	4	2	0.4	0.63	3.45	14.34	2.09	7.96	< 0.01	1.04	< 0.01
5	14	-1	-1	1	2.5	0.5	0.6	5.31	4.45	17.75	1.53	7.84	0.25	1.00	0.10
6	5	1	-1	1	4	0.5	0.6	3.22	8.63	16.99	3.05	7.94	0.05	1.02	0.06
7	12	-1	1	1	2.5	2	0.6	1.55	3.00	18.35	0.33	7.96	< 0.01	1.02	0.02
8	13	1	1	1	4	2	0.6	0.24	3.65	10.37	4.07	6.75	0.61	0.94	0.06
9	18	0	0	0	3.25	1.25	0.5	2.09	4.28	17.73	0.44	7.96	< 0.01	1.05	< 0.01
10	8	0	0	0	3.25	1.25	0.5	2.03	4.33	17.50	0.79	7.92	0.04	1.02	0.02
11	7	0	0	0	3.25	1.25	0.5	2.04	4.32	17.52	0.78	7.93	0.02	1.02	0.03
12	9	0	0	0	3.25	1.25	0.5	2.28	4.13	17.69	0.65	7.96	< 0.01	1.02	0.02
13	15	-1	0	0	2.5	1.25	0.5	3.89	2.86	18.40	0.44	7.96	< 0.01	1.05	< 0.01
14	16	1	0	0	4	1.25	0.5	0.93	5.19	13.81	3.70	7.21	0.59	0.93	0.09
15	2	0	-1	0	3.25	0.5	0.5	4.66	5.76	16.85	3.33	7.48	0.97	0.97	0.16
16	1	0	1	0	3.25	2	0.5	0.70	3.42	15.49	1.51	7.37	0.30	0.96	0.04
17	17	0	0	-1	3.25	1.25	0.4	2.75	3.76	17.18	1.04	7.69	0.22	1.02	0.03
18	3	0	0	1	3.25	1.25	0.6	1.45	4.79	17.91	0.47	7.96	< 0.01	1.05	< 0.01

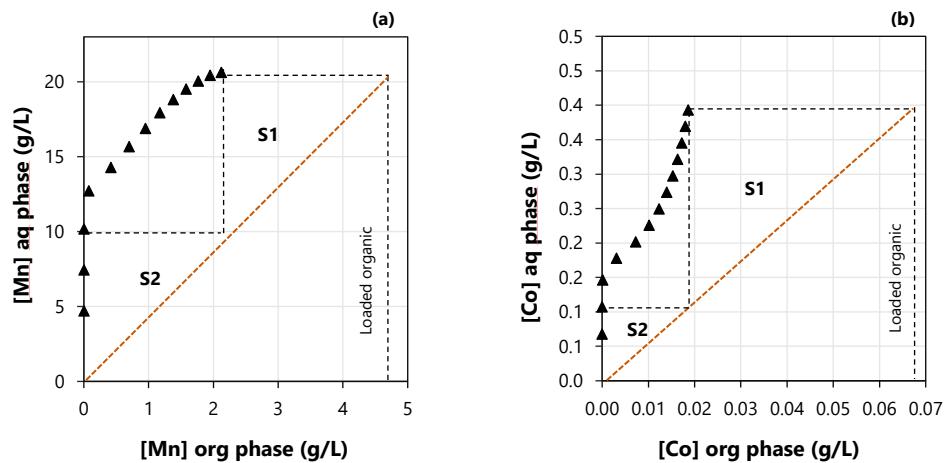
**Table S2.** Conditions of the experimental design, distribution ratios ( $D$ ) and separation factors ( $\beta$ ) after one extraction stage. Contact time of 10 min.

std order	random	Real variables			Distribution ratio ( $D$ )				log $D$				Separation factor ( $\beta$ )		
		pH	O:A	D2EH PA	$D_{\text{Mn}}$	$D_{\text{Co}}$	$D_{\text{Ni}}$	$D_{\text{Li}}$	$\log D_{\text{Mn}}$	$\log D_{\text{Co}}$	$\log D_{\text{Ni}}$	$\log D_{\text{Li}}$	$Mn/C$	$Mn/N$	$Mn/Li$
1	6	2.5	0.5	0.4	0.5	< 0.1	< 0.1	< 0.1	-0.3	-2.3	-3.3	-2.0	104	998	53
2	11	4	0.5	0.4	2.1	0.3	< 0.1	0.2	0.3	-0.6	-0.9	-0.7	8	16	11

3	10	2.5	2	0.4	0.8	< 0.1	< 0.1	< 0.1	-0.1	-1.7	-2.6	-1.7	39	272	43
4	4	4	2	0.4	5.5	0.1	< 0.1	< 0.1	0.7	-0.8	-3.9	-2.5	38	44750	1629
5	14	2.5	0.5	0.6	0.8	0.1	< 0.1	0.1	-0.1	-1.1	-1.5	-1.0	10	26	9
6	5	4	0.5	0.6	2.7	0.2	< 0.1	0.1	0.4	-0.7	-2.2	-1.2	15	425	46
7	12	2.5	2	0.6	1.9	< 0.1	< 0.1	< 0.1	0.3	-1.7	-3.9	-1.8	101	15798	125
8	13	4	2	0.6	15.4	0.4	0.1	0.1	1.2	-0.4	-1.0	-1.2	39	170	250
9	18	3.25	1.25	0.5	2.1	< 0.1	< 0.1	< 0.1	0.3	-1.6	-3.7	-	78	10646	-
10	8	3.25	1.25	0.5	2.1	< 0.1	< 0.1	< 0.1	0.3	-1.3	-2.3	-1.6	47	465	93
11	7	3.25	1.25	0.5	2.1	< 0.1	< 0.1	< 0.1	0.3	-1.4	-2.5	-1.6	48	733	85
12	9	3.25	1.25	0.5	1.8	< 0.1	< 0.1	< 0.1	0.3	-1.4	-3.7	-1.6	50	9373	77
13	15	2.5	1.25	0.5	0.7	< 0.1	< 0.1	< 0.1	-0.1	-3.4	-3.7	-	1652	3817	-
14	16	4	1.25	0.5	5.6	0.3	0.1	0.1	0.7	-0.6	-1.1	-1.0	21	68	58
15	2	3.25	0.5	0.5	1.2	0.2	0.1	0.2	0.1	-0.7	-0.9	-0.8	6	10	7
16	1	3.25	2	0.5	4.9	0.1	< 0.1	< 0.1	0.7	-1.0	-1.4	-1.3	50	122	110
17	17	3.25	1.25	0.4	1.4	0.1	< 0.1	< 0.1	0.1	-1.2	-1.6	-1.6	22	48	52
18	3	3.25	1.25	0.6	3.3	< 0.1	< 0.1	< 0.1	0.5	-1.6	-3.7	-2.5	125	17140	958

**Table S3.** Conditions of the experimental design and concentrations of metals remaining in the organic phase and in the stripping product. Legend: [aq]: concentration of metal in aqueous phase, [org] concentration of metal in organic phase.

Rand om Order	St. Order	Coded variables				Real variables			Mn		Co		Ni	Li	D ([aq]/[org])
		[H <sub>2</sub> S O <sub>4</sub> ]	O:A	time		[H <sub>2</sub> S O <sub>4</sub> ]	O:A	time	[aq]	[org]	[aq]	[org]	[aq]	[aq]	D Mn D Co
9	1	-1	-1	-1	0.05	1	2		4	0.6	0.06	0.01	n.d.	< 0.01	6.3 5.4
14	2	1	-1	-1	2	1	2		4	0.8	0.05	0.01	n.d.	< 0.01	4.8 3.6
4	3	-1	1	-1	0.05	8	2		11	3.3	0.31	0.03	0.61	< 0.01	3.2 10.8
2	4	1	1	-1	2	8	2		19	2.3	0.26	0.04	0.29	< 0.01	8.1 7.5
15	5	-1	-1	1	0.05	1	25		5	< 0.1	0.08	< 0.01	n.d.	n.d.	- -
11	6	1	-1	1	2	1	25		5	< 0.1	0.07	< 0.01	0.75	n.d.	- -
3	7	-1	1	1	0.05	8	25		10	3.4	0.41	0.02	n.d.	< 0.01	3.1 23.3
8	8	1	1	1	2	8	25		28	1.1	0.42	0.02	0.25	< 0.01	24.6 26.5
16	9	0	0	0	1.025	4.5	13.5		17	0.8	0.26	0.01	n.d.	< 0.01	21.4 25.8
5	10	0	0	0	1.025	4.5	13.5		16	1.1	0.24	0.01	1.61	n.d.	15.5 18.1
7	11	0	0	0	1.025	4.5	13.5		16	1.1	0.24	0.01	n.d.	< 0.01	14.3 17.3
1	12	0	0	0	1.025	4.5	13.5		17	0.8	0.27	0.01	2.63	n.d.	21.4 38.4
18	13	-1	0	0	0.05	4.5	13.5		9	0.4	0.15	0.03	n.d.	n.d.	22.8 4.5
12	14	1	0	0	2	4.5	13.5		17	0.4	0.26	0.01	n.d.	< 0.01	44.1 27.5
10	15	0	-1	0	1.025	1	13.5		5	< 0.1	0.07	< 0.01	1.14	n.d.	- -
6	16	0	1	0	1.025	8	13.5		23	0.4	0.36	0.02	0.41	< 0.01	64.4 15.7
13	17	0	0	-1	1.025	4.5	2		14	0.4	0.21	0.02	0.08	n.d.	35.0 9.6
17	18	0	0	1	1.025	4.5	25		22	< 0.1	0.34	< 0.01	n.d.	n.d.	- -



**Figure S1.** Distribution isotherms of (a) manganese stripping and (b) cobalt stripping obtained using the fitted models. Conditions used as input in the fitted models: stripping time: 13.5 min (coded variable: 0), O:A ratio: 8:1 (coded variable: +1), concentration of H<sub>2</sub>SO<sub>4</sub>: 1 M (coded variable: 0).