

Article

Effect of Mg/Al₂O₃ and Calcination Temperature on the Catalytic Decomposition of HFC-134a

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Abstract: This paper evaluated the effect of calcination temperature and the use of Mg/Al₂O₃ on the decomposition of HFC-134a. Two commercialized catalysts, Al₂O₃ and Mg/Al₂O₃, were calcined at two different temperatures (500 and 650 °C) and their physicochemical characteristics were examined by X-ray diffraction, Brunauer–Emmett–Teller analysis, and the temperature-programmed desorption of ammonia and carbon dioxide analysis. The results show that, in comparison to Al₂O₃, 5% Mg/Al₂O₃ exhibited a larger Brunauer–Emmett–Teller surface area and higher acidity. The relative amount of strong acid sites of the catalysts decreased with increasing calcination temperature. Although a more than 90% decomposition rate of HFC-134a was achieved over all catalysts during the sequential decomposition test of HFC-134a using a vertical plug flow reactor connected directly to a gas chromatography/mass spectrometry system, the lifetime of the catalyst differed according to the catalyst type. Compared to Al₂O₃, Mg/Al₂O₃ revealed a longer lifetime and less coke formation due to the increased Brunauer–Emmett–Teller surface area and weak Lewis acid sites and basic sites arising from Mg impregnation. Higher temperature calcination extended the catalyst lifetime with the formation of less coke due to the smaller number of strong acid sites, which can lead to severe coke formation. A valuable by-product, trifluoroethylene, was formed as a result of the decomposition. Based on the experimental results, a reaction is proposed which reasonably explains the decomposition reaction.

Keywords: catalytic pyrolysis; HFC-134a; Mg/Al₂O₃; calcination temperature

1. Introduction

Rapid global warming and climate change in recent decades and the increased frequency and impact of environmental disasters, such as global warming, sea level rises, heat, drought, and floods, have raised global interest in greenhouse gases [1,2]. Although greenhouse gases, such as CO₂, CH₄, N₂O, and O₃, are produced naturally, their concentrations have increased due to human activity [3]. Among the various kinds of greenhouse gases, fluorinated greenhouse gases are not only synthesized and emitted by human activity but also have a much higher global warming potential (GWP) than other greenhouse gases [4]. Therefore, many studies have focused on minimizing use, recycling,

and direct destruction of these fluorinated greenhouse gases [5]. After the Montreal Protocol, the use of chlorofluorocarbons as refrigerants was banned and hydrofluorocarbons (HFCs) have since been used as substitutes [6]. Among the various kinds of HFCs, 1,1,1,2-tetrafluoroethane (HFC-134a) is the most widely used coolant for air conditioners, but its GWP value is also very high, 1300 times higher than CO₂ [7]. The seriousness of HFC-134a was highlighted in the Kyoto Protocol [8] and a decision was made to reduce its usage in the Kigali Amendment to the Montreal Protocol [9].

Various technologies have been used to minimize HFC-134a emissions, including recycling after purification using polymeric membranes [10] and the direct destruction of waste HFC-134a. Although HFC-134a can be purified using membrane technologies, their technical and economical limitations are difficult to overcome due to the high cost [11] in achieving the target HFC purity required for reuse. Therefore, many studies have considered the direct destruction [12] of HFC-134a instead. The direct destruction of HFC-134a can be achieved by applying thermal conversion technologies, such as incineration, plasma, and pyrolysis. In the case of incineration, combustion in air and ancillary fuels has been introduced, but the additional fuel input cost and equipment corrosion due to excessive HF generation are recognized as problems [13]. Steam plasma is a technology that has high HFC-134a decomposition efficiency [14], but plant enlargement is difficult due to corrosion, probably caused by the high HF concentration in the product gas, and unstable plasma discharge due to the use of steam. The high cost of plasma plant construction and its operation limit its actual commercialization. Pyrolysis can be considered as a favorable process for the decomposition of HFC-134a, but an excessively high temperature (>750 °C) is required because of its high thermal stability [15]. Recently, many researchers have reported the catalytic pyrolysis of HFC-134a because of the lower decomposition temperatures. Ni/Al₂O₃ [16], waste concrete [15], and metal phosphate catalysts [17] have been used. Han et al. [18] compared the HFC-134a decomposition efficiencies of metal oxides, such as CaO and Al₂O₃. They reported the highest decomposition efficiency of HFC-134a over Al₂O₃, but the rapid deactivation of Al₂O₃ by its conversion to AlF₃ limits its use.

Many studies have applied metal-impregnated Al₂O₃ to increase the overall lifetime of the catalyst for the decomposition of fluorinated hydrocarbons. Han et al. [19] reported that the decomposition tendency for trifluoromethane and the stability of the substrate could be increased by metal impregnation onto Al₂O₃. Song et al. [20] achieved a high level of CF₄ hydrolytic decomposition over metal-supported Al₂O₃ and explained that the catalyst modified by metal impregnation can preserve the Lewis acid sites of the catalyst, which can act as a strong active site for the decomposition of CF₄. Li et al. reported the use of a metal-supported catalyst for the catalytic decomposition of HFC-143a [21]. They explained that metal phosphates can provide a more stable decomposition efficiency of fluorinated hydrocarbons due to the presence of weak acidic sites and dehydrofluorination proceeds via a carbonium-ion mechanism. Previous studies on the use of metal-supported catalysts for the decomposition of other fluorinated hydrocarbons suggested that the catalytic efficiency of Al₂O₃ can be increased and become more stable by metal impregnation, but there has been little systematic research on its use for HFC-134a decomposition.

Therefore, this study examined the catalytic decomposition of HFC-134a over Mg-supported Al₂O₃ (Mg/Al₂O₃). Al₂O₃ (γ-phase) and Mg/Al₂O₃ (γ-phase) were used throughout the experimental investigation. The physicochemical properties (pore size, acidity, and structure) of Al₂O₃ and Mg/Al₂O₃, which was calcined at different temperatures (500 and 650 °C), were analyzed using Brunauer–Emmett–Teller (BET), ammonia–temperature programmed desorption (NH₃-TPD), and carbon dioxide–temperature programmed desorption (CO₂-TPD), and X-ray diffraction (XRD) measurements. The lifetime of each catalyst during the sequential decomposition of HFC-134a was estimated using vertical plug flow reactor–gas chromatography/mass spectrometry (VPFR-GC/MS).

2. Results

Physicochemical Properties of Catalysts

The BET surface areas of the Mg/Al₂O₃ catalysts (246 m²/g for Mg/Al₂O₃-500 and 227 m²/g for Mg/Al₂O₃-650) were larger than those of the Al₂O₃ catalysts (139 m²/g for Al₂O₃-500 and 140 m²/g for Al₂O₃-650). This suggests that the BET surface area of Al₂O₃ increased due to Mg impregnation. Figure 1 and Table 1 show the NH₃-TPD curves and amounts of weak, moderate, and strong acid sites of Al₂O₃ and Mg/Al₂O₃ catalysts, respectively. Mg/Al₂O₃-500 and Mg/Al₂O₃-650 had much higher weak acid amounts than Al₂O₃-500 and Al₂O₃-650, respectively. This suggests that the weak acidity of Al₂O₃ catalysts was increased by Mg impregnation. Jeon et al. [22,23] also reported that the addition of Mg increased weak Lewis acidity. Therefore, it can be concluded that weak Lewis acidity was increased with the addition of Mg to Al₂O₃.

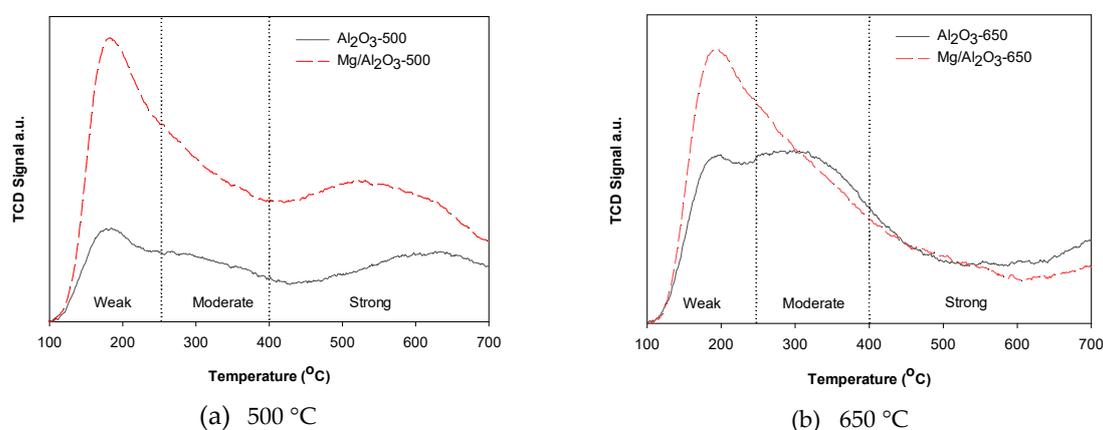


Figure 1. Ammonia-temperature programmed desorption (NH₃-TPD) curves of Al₂O₃ and Mg/Al₂O₃ calcined at different temperatures—500 and 650 °C.

Table 1. Amounts of acidic sites (mmol g⁻¹) of each catalyst obtained from NH₃-TPD analysis.

Catalyst	Weak Acid Amount	Moderate Acid Amount	Strong Acid Amount	Total Acid Amount	Weak Acid Amount/Strong Acid Amount
Al ₂ O ₃ -500	0.26	0.25	0.47	0.98	0.55
Mg/Al ₂ O ₃ -500	0.77	0.66	1.06	2.49	0.73
Al ₂ O ₃ -650	0.23	0.33	0.29	0.86	0.79
Mg/Al ₂ O ₃ -650	0.65	0.59	0.47	1.70	1.38

In addition, both Al₂O₃-650 and Mg/Al₂O₃-650 revealed a smaller number of acid sites than Al₂O₃-500 and Mg/Al₂O₃-500, respectively. In particular, Al₂O₃-650 and Mg/Al₂O₃-650 had fewer strong acid sites than Al₂O₃-500 and Mg/Al₂O₃-500, respectively. This indicates that the calcination of Al₂O₃ and Mg/Al₂O₃ at higher temperatures (650 °C) can lead to a decrease in the number of strong acid sites [24]. The relative ratio of weak acidity/strong acidity was increased with Mg impregnation and the increase of calcination temperature.

The CO₂-TPD curves of Al₂O₃ and Mg/Al₂O₃ catalysts are shown in Figure S1 (Supplementary Information). Mg/Al₂O₃-500 and Mg/Al₂O₃-650 showed higher basicity than Al₂O₃-500 and Al₂O₃-650, suggesting that basicity increased by Mg impregnation. In addition, both Al₂O₃-650 and Mg/Al₂O₃-650 revealed a higher number of weak basic sites and a smaller number of strong basic sites than Al₂O₃-500 and Mg/Al₂O₃-500, respectively. The NH₃- and CO₂-TPD results suggest that calcination of Al₂O₃ and Mg/Al₂O₃ at higher temperatures (650 °C) can lead to an increase in the number of weak acidic and basic sites and a decrease in the number of strong acidic and basic sites. The well-balanced weak Lewis acidity and basicity may affect catalytic decomposition of HFC-134a.

Figure 2 shows XRD patterns of the Al_2O_3 and $\text{Mg}/\text{Al}_2\text{O}_3$ catalysts calcined at different temperatures. The XRD pattern of Al_2O_3 and $\text{Mg}/\text{Al}_2\text{O}_3$ catalysts had the characteristic broad peaks of Al_2O_3 , representing the γ phase, at 46.6° , 67.1° , and 60.9° 2θ (JCPDS 29-63). On the other hand, the peaks could be differentiated by their intensities, as reported elsewhere [25]. The intensity of the line depends on the elemental composition; hence, the impregnation of magnesium onto alumina reduced the intensity of the peaks compared with those of the Al_2O_3 catalysts [26,27]. The typical XRD peaks of Mg particles were barely observed in the XRD pattern of $\text{Mg}/\text{Al}_2\text{O}_3$ catalysts. This suggests that Mg had penetrated into the substitutional sites of the Al lattice. Compared with the XRD peaks of Al_2O_3 catalysts, those of $\text{Mg}/\text{Al}_2\text{O}_3$ catalysts had broader peaks and their 2θ values were shifted to slightly lower values. Wagih [28] reported that the 2θ shift of the Al peak on the XRD pattern of $\text{Mg}/\text{Al}_2\text{O}_3$ occurs due to Mg atomic penetration into the Al matrix. Mg^{2+} ions with a larger ionic radius (86 pm) than Al^{3+} (67.5 pm) are believed to have entered the alumina lattice because the shift was slight and no secondary phases were observed. Other researchers [29] support these observations. An increase in the calcination temperature resulted in an increase in peak height [30], with magnesium-doped alumina calcined at 650°C showing an intense peak compared with its equivalent calcined at 500°C . This was attributed to a slight change in crystallinity that modified the surface morphology. Therefore, the larger BET surface area and higher number of weak acidic sites of $\text{Mg}/\text{Al}_2\text{O}_3$ than those of Al_2O_3 resulted from a structural change of Al_2O_3 caused by the atomic penetration of Mg into the substitutional sites of the Al lattice.

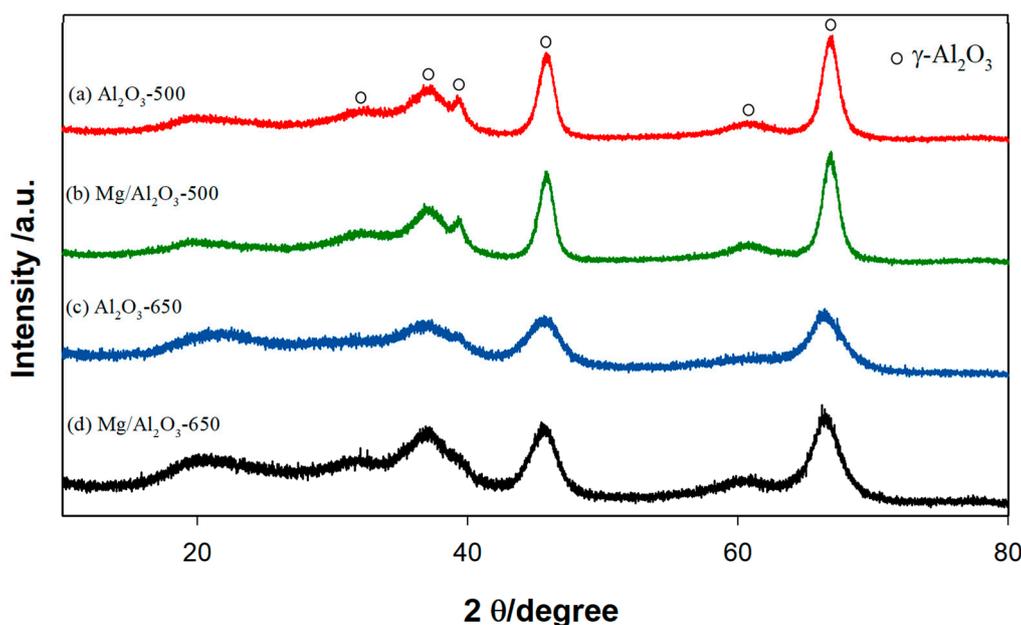


Figure 2. X-ray diffraction (XRD) pattern for Al_2O_3 and $\text{Mg}/\text{Al}_2\text{O}_3$ calcined at different temperatures.

3. Discussion

Catalytic Decomposition of HFC-134a

Figure 3 depicts the conversion rates of HFC-134a obtained from the catalytic decomposition over Al_2O_3 and $\text{Mg}/\text{Al}_2\text{O}_3$ catalysts at 600°C . Although HFC-134a was not decomposed by noncatalytic decomposition, the initial decomposition rates of HFC-134a over both catalysts were higher than 99.0%. Iizuka et al. [15] also indicated that temperatures higher than 750°C , which are required for the noncatalytic decomposition of HFC-134a, could be decreased using an Al_2O_3 catalyst. The high decomposition rates of HFC-134a (>99%) were maintained for more than 6 h over all catalysts used in this study, but they decreased depending on the catalyst.

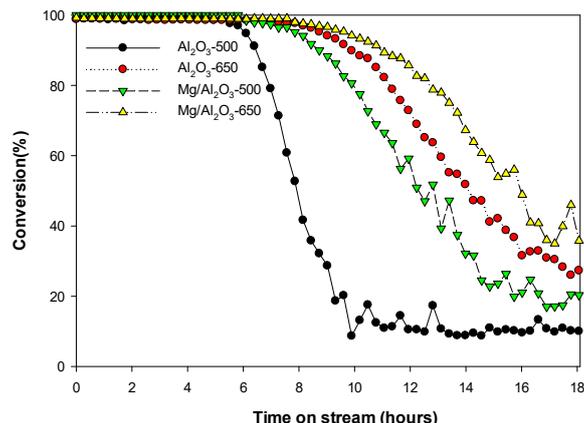


Figure 3. Conversion rate of 1,1,1,2-tetrafluoroethane (HFC-134a) over different catalysts calcined at different temperatures—500 and 650 °C.

Mg/Al₂O₃ decomposed HFC-134a for a longer time than Al₂O₃. This suggests that the Mg impregnated on the surface of Al₂O₃ might play a crucial role in the decomposition reaction of HFC-134a. The larger BET surface area, higher amount of weak Lewis acid sites, and higher amount of weak basicity of Mg/Al₂O₃ catalysts than Al₂O₃ catalysts can also increase the catalyst lifetime for the decomposition of HFC-134a. These findings are in accordance with other studies reporting that a larger surface area allows better mass transfer, which facilitates a better opportunity for the catalyst to contact with the fluorinated gases [31,32].

In addition, the catalysts calcined at 650 °C, Al₂O₃-650 and Mg/Al₂O₃-650, also showed a longer lifetime than Al₂O₃-500 and Mg/Al₂O₃-500 in terms of the catalytic decomposition of HFC-134a. The BET surface areas of Al₂O₃-650 and Mg/Al₂O₃-650 were similar, respectively, to those of Al₂O₃-500 and Mg/Al₂O₃-500. In addition, the total acidity of Al₂O₃ and Mg/Al₂O₃ decreased with the increasing catalyst calcination temperature. The decrease in the number of strong acid sites on the catalysts calcined at 650 °C was the main factor increasing the lifetime of Al₂O₃ and Mg/Al₂O₃. Jia et al. [33] reported that the strong acid sites of Al₂O₃ led to higher coke formation, which can decrease the catalyst lifetime. Especially, the catalytic activities were well correlated with the ratio of weak acidic sites/strong acidic sites (Table 1). The increase of weak basic sites and a decrease of strong basic sites on the catalysts calcined at 650 °C can also be an important factor in increasing the lifetime of Al₂O₃ and Mg/Al₂O₃.

Figure 4 shows the rate of trifluoroethylene (TrFE, C₂HF₃) formation through the catalytic decomposition of HFC-134a over the Al₂O₃ and Mg/Al₂O₃ catalysts calcined at different temperatures. Compared with the Al₂O₃ catalysts, Mg/Al₂O₃ catalysts produced a larger amount of TrFE for a longer duration. In addition, the catalysts calcined at 650 °C produced a larger amount of TrFE than those calcined at 500 °C. This suggests that Mg impregnation and calcination at 650 °C can increase the catalyst lifetime not only for the decomposition of HFC-134a but also for the formation of TrFE. The efficient formation of TrFE is desirable because it is a significant feedstock for the synthesis of fluoroplastics and fluororubbers [16,33]. TrFE can be generated through hydrolysis of trichlorotrifluoroethane, but this is a difficult and an expensive process [34–37]. Therefore, efficient TrFE formation via the catalytic decomposition of HFC-134a over Mg/Al₂O₃ is meaningful because of its cost effectiveness.

Figure 5 shows the oxidative TG and DTG curves of deactivated catalysts collected after the sequential decomposition of HFC-134a. The catalytic decomposition of HFC-134a over Mg/Al₂O₃-650 formed the smallest amount of coke (3.7% ± 1%) followed in order by Mg/Al₂O₃-500 (3.9% ± 1%), Al₂O₃-650 (11.9% ± 1%), and Al₂O₃-500 (16.0% ± 1%), which is in the order of the HFC-134a decomposition efficiency of these catalysts. This suggests that the decomposition efficiency and catalyst lifetime are also strongly related to the amount of coke formed during the catalytic decomposition of

HFC-134a. The Mg/Al₂O₃ catalysts produced a smaller amount of coke and the oxidation temperatures of the coke deposited on the Mg/Al₂O₃ catalysts were also lower than those deposited on Al₂O₃ catalysts. This means that the use of Mg/Al₂O₃ catalysts can provide higher decomposition efficiency for a longer duration than Al₂O₃ catalysts because of the small amount of coke deposition having a lower oxidation temperature.

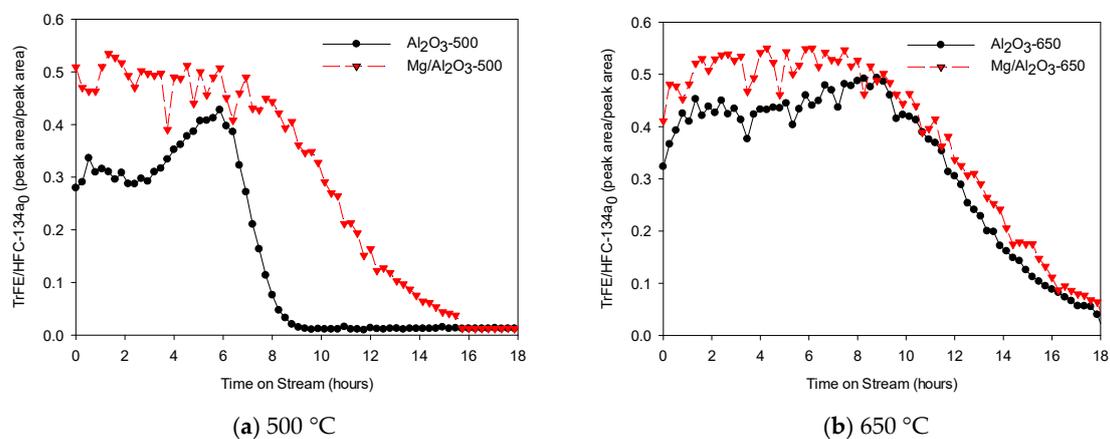


Figure 4. Formation rate of trifluoroethylene (TrFE) on the catalytic decomposition of HFC-134a over different catalysts calcined at different temperatures—500 and 650 °C.

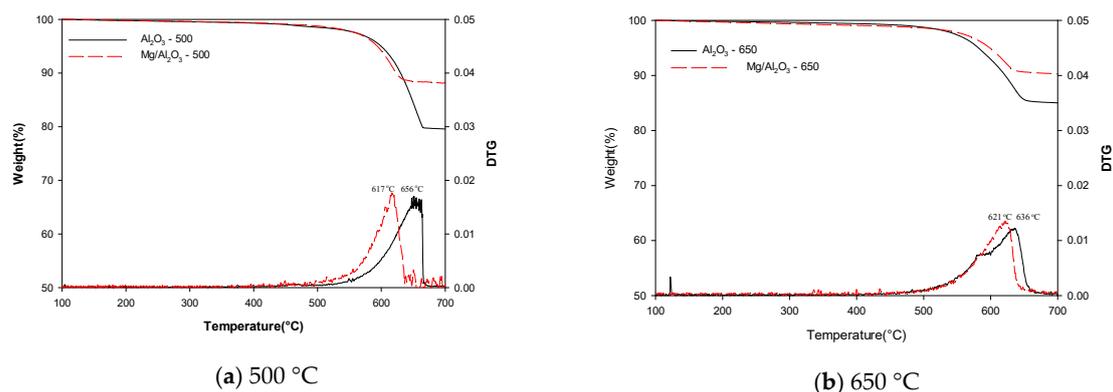
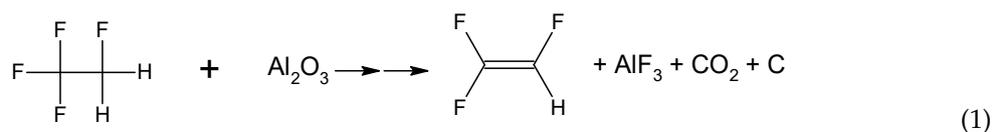


Figure 5. Oxidative Differential Thermogravimetric (DTG) curves of the coke deposited on Al₂O₃ and Mg/Al₂O₃ calcined at different temperatures—500 and 650 °C.

Figure 6 shows the XRD pattern of the used Al₂O₃ and Mg/Al₂O₃ catalysts, which were collected from the furnace after the sequential catalytic decomposition of HFC-134a. The typical peak patterns of fresh Al₂O₃ catalysts were not observed in the XRD patterns of the spent catalysts, but the used Al₂O₃ catalysts revealed the typical XRD peak patterns of AlF₃ (at 25°, 42°, 52°, and 58° 2θ [18]). This suggests that the Al₂O₃ catalysts were converted to AlF₃ during the catalytic decomposition of HFC-134a over the Al₂O₃ catalysts. Based on the product distribution and the presence of AlF₃, the decomposition mechanism of HFC-134a can be expressed using Equation (1) as follows:



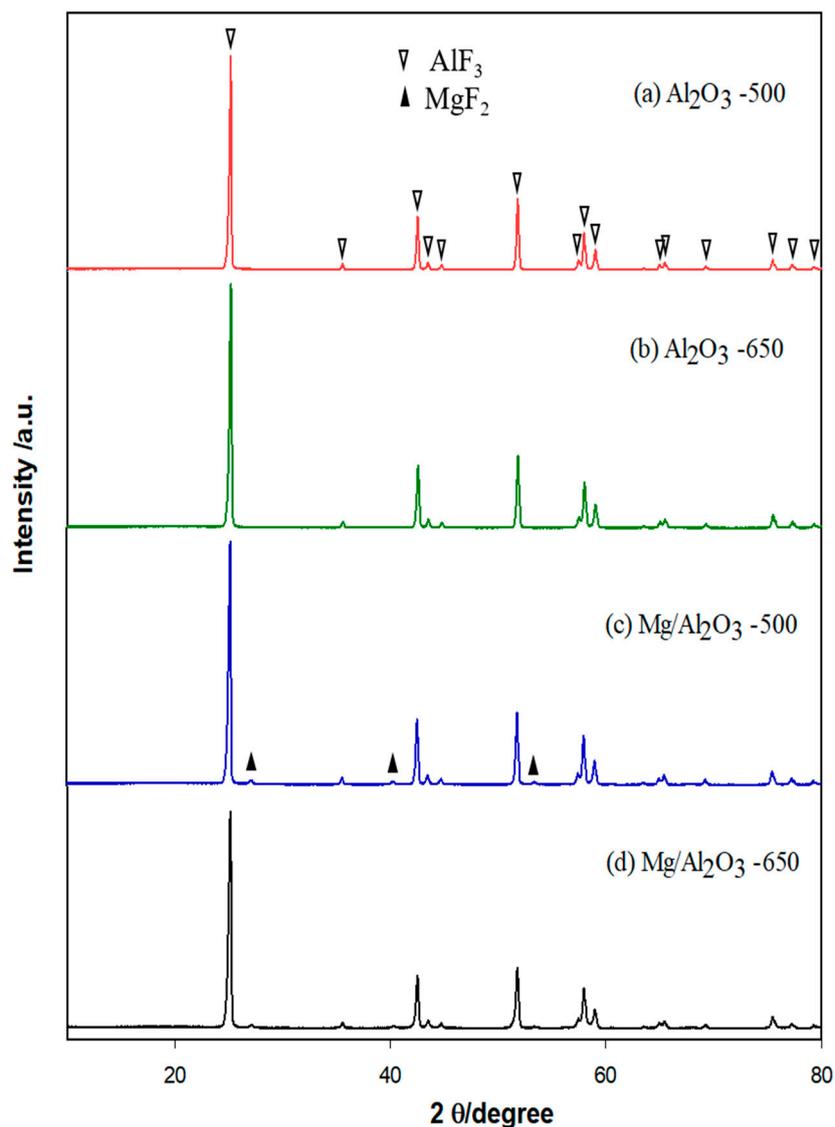


Figure 6. XRD pattern for the used Al_2O_3 and $\text{Mg}/\text{Al}_2\text{O}_3$.

When $\text{Mg}/\text{Al}_2\text{O}_3$ catalysts were used, the typical peaks of MgF_2 were also observed on the XRD pattern of the used $\text{Mg}/\text{Al}_2\text{O}_3$ catalysts (at 24° , 42° , and 52° 2θ [16]), as shown in Figure 7c,d. This suggests that Mg was also directly involved in the defluorination reaction of HFC-134a according to the following reaction:

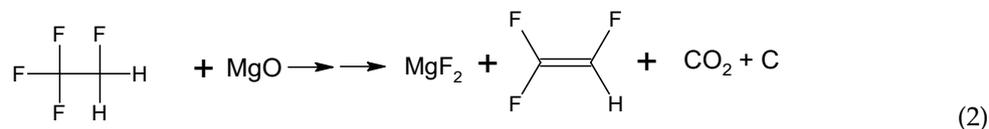


Figure 7 depicts the rate of CO_2 formation during the catalytic decomposition of HFC-134a over Al_2O_3 and $\text{Mg}/\text{Al}_2\text{O}_3$ catalysts. The $\text{Mg}/\text{Al}_2\text{O}_3$ catalysts produced a higher rate of TrFE formation than the Al_2O_3 catalysts and a smaller level of CO_2 production during the reaction. In addition, the $\text{Mg}/\text{Al}_2\text{O}_3$ catalysts produced a smaller amount of coke than the Al_2O_3 catalysts. This can explain the increased number of weak Lewis acidic sites by Mg impregnation to Al_2O_3 catalysts, which can increase the relative ratio (Table 1) of weak acid sites compared to strong acidic sites that result in severe coke formation. The decreased coke formation over $\text{Mg}/\text{Al}_2\text{O}_3$ -650 compared with $\text{Mg}/\text{Al}_2\text{O}_3$ -500

confirmed that the relative number of strong acid sites is strongly related to catalyst deactivation during the catalytic decomposition of HFC-134a.

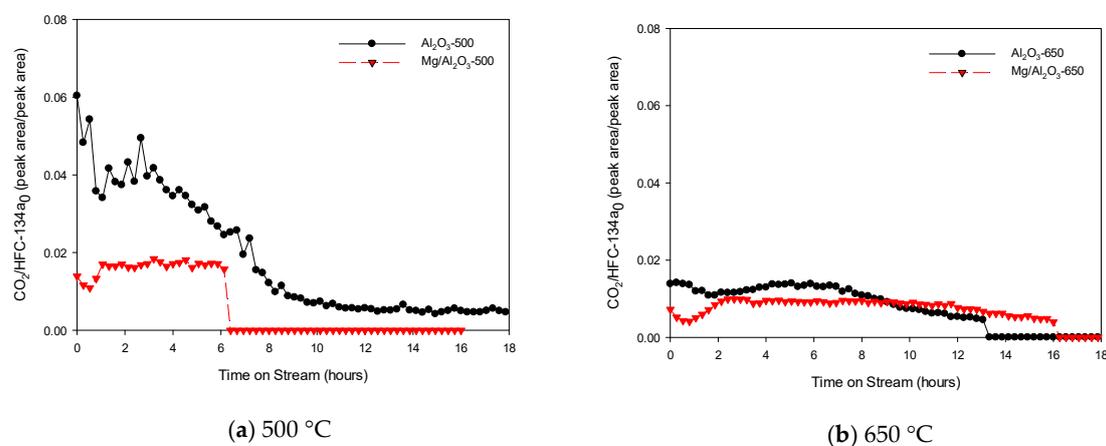


Figure 7. Formation rate of CO₂ on the catalytic decomposition of HFC-134a over different catalysts calcined at different temperatures—500 and 650 °C.

4. Materials and Methods

4.1. HFC-134a and Catalysts

Commercial HFC-134a was procured from RIGAS Co. Ltd., Daejeon, Republic of Korea, a gas manufacturer. Commercial Al₂O₃ and 5 wt % Mg/Al₂O₃ were obtained from Sasol. The catalysts were crushed and sieved to make small particles with a particle size between 1.0 and 1.7 mm. Prior to the catalytic experiments, all catalysts were calcined at different temperatures—500 and 650 °C—for 2 h and categorized as Al₂O₃-500, Al₂O₃-650, Mg/Al₂O₃-500, and Mg/Al₂O₃-650, respectively. The BET surface area and pore volume of each catalyst were measured using a BET analyzer (Micromeritics 3Flex). NH₃-TPD analysis and XRD of the catalysts were performed using the same procedure reported elsewhere [38,39].

4.2. HFC-134a Decomposition Test

The efficiency of the catalysts on the catalytic decomposition of HFC-134a was examined by VPFR-GC/MS, as shown in Figure 8. The VPFR-GC/MS system consisted of a gas supply, reactor, HF trap, and valve-GC/MS. For the catalytic decomposition of HFC-134a, 1.2 g of catalyst was taken in the catalyst bed, and 98 mL/min of N₂ gas and 2 mL/min of HFC-134a gas (2% of HFC-134a/N₂) was supplied to the system. After the stabilization of the system, a temperature of 600 °C was set and the catalytic decomposition began. The gas hourly space velocity (GHSV) and weight hourly space velocity (WHSV) of the system were 1667 h⁻¹ and 5000 mL g_{cat}⁻¹ h⁻¹, respectively. The product gases emitted from the reactor were transferred to a valve GC/MS system (7890A/5975C inert, Agilent, Santa Clara, USA) via an HF trap containing CaO. Table 2 lists the detailed GC/MS conditions used in this study. The peaks on the GC/MS chromatogram were identified by comparing the mass spectrum of each peak on the chromatogram using an MS library (NIST 08th). The MS peak areas for all the components on the chromatogram were integrated to determine their relative amounts. The conversion rate (%) of HFC-134a was calculated using Equation (3):

$$\text{Conversion rate (\%)} = (1 - A_{\text{out}}/A_{\text{in}}) \times 100 \quad (3)$$

where A_{in} is the peak area of HFC-134a in the reactant gas, and A_{out} is the peak area of HFC-134a in the product gas.

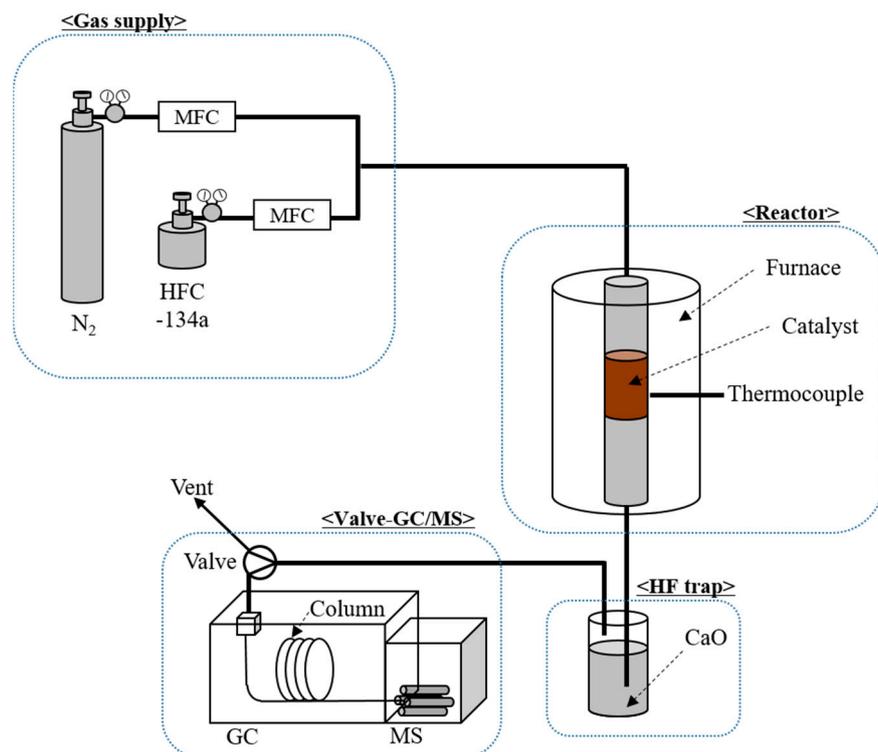


Figure 8. Vertical plug flow reactor–gas chromatography/mass spectrometry (VPFR-GC/MS) system used in this study.

Table 2. GC/MS condition.

	GC	MS
Inlet	260 °C, split ratio 50:1	Ion source 230 °C
Column	GS-GASPRO, 60 m length × 0.32 mm inner diameter	Quadrupole filter 150 °C
Oven	50 °C → 20 °C/min → 260 °C	Scan range m/z 17–600

5. Conclusions

The catalytic decomposition and conversion of HFC-134a was successfully carried out using Al_2O_3 and $\text{Mg}/\text{Al}_2\text{O}_3$ at 600 °C by calcinating the catalysts at 500 and 650 °C. The use of $\text{Mg}/\text{Al}_2\text{O}_3$ and an increase in calcination temperature led to a higher HFC-134a decomposition efficiency. Compared with Al_2O_3 , $\text{Mg}/\text{Al}_2\text{O}_3$ had a larger BET surface area and higher weak Lewis acidity and basicity. The relative number of strong acidic sites in Al_2O_3 and $\text{Mg}/\text{Al}_2\text{O}_3$ also decreased with increasing calcination temperature from 500 to 650 °C, which led to a decrease in the amount of coke formation and increased the lifetime of the catalyst. TrFE, known for being valuable, was obtained as a by-product and its yield was higher over $\text{Mg}/\text{Al}_2\text{O}_3$.

Supplementary Materials: The following are available online at <http://www.mdpi.com/2073-4344/9/3/270/s1>, Figure S1: Carbon dioxide—temperature programmed desorption (CO_2 -TPD) curves of Al_2O_3 and $\text{Mg}/\text{Al}_2\text{O}_3$ calcined at different temperatures—500 and 650 °C.

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