Catalytic cleavage of ether bond in a lignin model compound over carbon-supported noble metal catalysts in supercritical ethanol

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Figure S1. Pressure profiles during the decomposition of BPE over the catalysts at 270 \degree C for 4 h in supercritical ethanol



Entry	Catalyst	Time (h) _	Selectivity(%)				Yield of target
			Phenol	Toluene	2-EP	4-EP	products (%)
1	Ru/C	0	18.26	18.94	0.84	0.86	21.57
2		0.5	27.73	28.56	0.85	0.87	44.71
3		1	27.24	27.27	0.90	1.00	47.66
4		4	24.93	26.51	1.52	1.56	49.94
5	Pd/C	0	30.48	29.43	0.95	0.90	51.32
6		0.5	30.55	32.27	2.26	2.24	59.26
7		1	26.05	32.82	3.57	3.09	54.71
8		4	21.57	33.48	5.23	4.64	52.86
9ª		0	6.91	20.40	n.d. ^b	1.15	12.30
10	Pt/C	0	12.17	15.86	2.17	1.17	14.18
11		0.5	21.00	26.33	3.72	1.51	35.66
12		1	22.95	31.16	4.70	1.94	47.85
13		4	16.99	34.51	8.16	3.55	49.67
14		8	13.93	32.52	8.45	3.80	44.48
15	AC	0	3.43	3.90	n.d.	n.d.	2.98
16		0.5	12.63	9.77	0.78	n.d.	11.72
17		1	16.05	11.76	0.74	0.71	16.03
18		4	26.39	20.86	0.84	0.56	38.63
19	None	0	n.d.	n.d.	n.d.	n.d.	n.d.
20		0.5	2.70	3.99	n.d.	n.d.	2.31
21		1	4.52	8.78	n.d.	n.d.	5.24
22		4	9.03	17.06	0.82	0.39	12.58

Table S1. The selectivity of products and the yield of target products during BPE decomposition over various catalysts at 270 $^{\circ}$ C in supercritical ethanol as a function of reaction time.

^a reacted at 240 °C (non-supercritical condition)

^b not detected