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Controlled Synthesis of Heterostructured SnO₂-CuO Composite Hollow Microspheres as Efficient Cu-Based Catalysts for the Rochow Reaction

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Abstract: In this work, we report the design and synthesis of a series of heterostructured SnO_2 -CuO hollow microspherical catalysts (H-SnO₂(*x*)-CuO, *x* is the weight ratio of Sn/Cu) for the Rochow reaction. The microspherical catalysts with nanosheets and nanoparticles as building blocks were prepared by a facile one-pot hydrothermal method coupled with calcination. When tested for the Rochow reaction, the prepared H-SnO₂(0.2)-CuO composite exhibited higher dimethyldichlorosilane selectivity (88.2%) and Si conversion (36.7%) than the solid CuO, hollow CuO and other H-SnO₂(*x*)-CuO microspherical samples, because in the former there is a stronger synergistic interaction between CuO and SnO₂.

Keywords: heterostructure; hollow composite; microsphere; synergistic effect; Rochow reaction

1. Introduction

In material synthesis, how to obtain materials with well-defined structures/shapes is one of the major goals, as each of their application is dependent on their physicochemical attributes and morphologies. Recently, nanostructures with various shapes including nanowires [1], nanotubes [2], nanorods [3] and hollow nanospheres [4] have been reported. Among them, hollow nanostructures are of particular interest owing to their unique structural features such as high surface area and fast diffusion capability, which are of importance to many applications such as catalysis [5,6], sensors [7], pollution treatment [8] and energy conversion [9]. For example, it was reported that CuO and NiO hollow nanospheres showed high catalytic activity and excellent stability for the hydrogenation of 4-nitrophenol [10], while a three-dimensional (3D) graphene network encapsulating SnO₂ hollow spheres exhibited outstanding electrochemical properties as an anode material for lithium-ion batteries [11]. However, most of these reported hollow structures are made up of only single oxide component, limiting their wider application. In principle, hollow heterostructures containing two or more kinds of metal oxide components with specific morphologies will have more abundant structural features such as various synergistic interactions among different components,

thus potentially having more substantial applications [12,13]. However, the controlled synthesis of these multi-component complex systems is still highly more challenging.

One of the applications for multi-Cu component containing system is for the Rochow reaction. This reaction is used to synthesize methylchlorosilanes, which are important intermediates in the organosilane industry [14]. As shown in Scheme 1, this reaction often yields various products, in which $(CH_3)_2SiCl_2$ (M2) is the most needed, as it is widely used for the manufacture of organosilicon products such as silicon rubber and silicon oil. Therefore, to enhance the selectivity and yield of M2, high-performance Cu-based catalysts are always desired. In the past decades, various catalyst systems have been reported [15–17]. In our previous work, many CuO catalysts with specific morphologies and structures have also been prepared and tested for the Rochow reaction. For instance, we observed that the flower-like CuO microspheres displayed a higher M2 selectivity and Si conversion than the commercial CuO catalyst with irregular morphology [18]; the leaf-like CuO nanostructure showed enhanced catalytic properties due to its largely exposed {001} plane that could facilitate formation of more Cu_3Si active phase during the reaction [19]; most recently, we demonstrated that the rambutan-like CeO2-CuO hollow microspheres exhibited superior catalytic performances to their solid counterpart and pure CuO, because of the more intimate contact of CuO with Si powder and the synergistic effect between CeO_2 and CuO in the former [20]. These results indicate that the M2 selectivity and yield could be further improved by rationally controlling the morphology, structure and composition of Cu-based catalysts. Furthermore, it has been recognized that SnO₂ is an outstanding promoter for the Rochow reaction [21,22]. In this sense, SnO₂-CuO micro-nano composites with hollow heterostructures are most likely to be good catalyst candidates too. However, to our knowledge, so far, such a promising catalyst system has not been explored for the Rochow reaction.

$$Si + MeCl \xrightarrow{copper catalyst}_{300-350^{\circ}C} \begin{cases} (CH_3)_3SiCl \\ (CH_3)_2SiCl_2 \\ CH_3SiCl_3 \\ CH_3HSiCl_2 \\ (CH_3)_2HSiCl \\ other low boilers \\ residue \end{cases}$$
(1)

Herein, we report the preparation of heterostructured SnO_2 -CuO composite hollow microspheres with nanosheets and nanoparticles as building blocks and with various Sn/Cu ratios using a facile bottom-up strategy. When employed as catalysts for the Rochow reaction, the SnO_2 -CuO hollow heterostructures showed a higher selectivity of M2 and Si conversion than the solid CuO, hollow CuO and commercial catalyst, particularly at the optimal Sn/Cu ratio. Moreover, the structure-dependent catalytic attributes and the reaction mechanism are also studied.

2. Results and Discussion

2.1. Characterization of H-SnO₂-CuO Precursor Particle

The XRD pattern of the collected precursor before calcination shows that the diffraction peaks match well with those of monoclinic basic cupric carbonate ($Cu_2(OH)_2CO_3$) (JCPDS No. 01-072-0075) (Figure 1a). The formation of $Cu_2(OH)_2CO_3$ should be the result of the chemical reaction between $Cu(CH_3COO)_2 \cdot H_2O$ and Na_2CO_3 solution, which is presented as follows:

 $CO_3^{2-} + H_2O \to HCO_3^- + OH^-$ (2)

$$HCO_3^- + H_2O \rightarrow H_2O + CO_2 + OH^-$$
(3)

The low-magnification FESEM image shows that the $Cu_2(OH)_2CO_3$ precursor is in the shape of microspheres and all particles are uniform with an average size of ca. 5 μ m (Figure 1b). From a

typical crashed microsphere (Inset of Figure 1b), it could be clearly observed that the precursor particle possesses a hollow structure. The high-magnification FESEM image further demonstrates that some disorder nanosheets are stretched out onto the microspherical surface (Figure 1c). The TG curve of this uncalcined sample shows a weight loss of about 27.6% from 200 to 350 °C in air, matching well with 27.9%, the theoretical value for the decomposition process from $Cu_2(OH)_2CO_3$ to CuO (Figure 1d).



Figure 1. (**a**) X-Ray Diffraction (XRD) pattern; (**b**,**c**) Scanning Electron Microscopy (SEM) images; and (**d**) Thermal Gravimetric (TG) curve of the precursor of H-SnO₂-CuO before calcination. The inset of panel (**b**) shows the hollow interior, bar, 2 μm.

2.2. Characterization of H-SnO₂-CuO

Figure 2 exhibits the XRD results of all the obtained products after calcination, including hollow SnO₂-CuO microspheres (denoted as H-SnO₂-CuO), hollow CuO microspheres (denoted as H-CuO) and solid CuO microspheres (denoted as S-CuO). The diffraction peaks observed at 2θ values of 32.5° , 35.5° , 38.7° , 48.7° , 53.4° , 58.3° , 61.5° , 66.2° , 68.1° and 72.4° correspond respectively to (110), (–111), (111), (–202), (020), (202), (–113), (–311), (220) and (311) lattice planes of the monoclinic CuO phase (JCPDS No. 01-005-0611). However, no obvious peak matching with crystalline Sn species could be found, probably due to its small amount or small size. Additionally, no traces of other impurities such as Cu₂O or Cu₂(OH)₂CO₃ can be observed. As we know, particle size often impacts catalytic activity [23]. Hence, the CuO nanocrystal sizes in these materials are calculated from the diffraction peaks at 2θ values of 35.5° using the Scherrer formula, the results are listed in Table 1. It is clearly seen that the average grain size of CuO in H-SnO₂-CuO sample is 22.9 nm, which is smaller than that in H-CuO (42.1 nm), indicating that the CuO particle size could be reduced through introducing Sn. Moreover, the BET surface area and pore volume of various samples is given in Table 1. It can be seen that all H-SnO₂(x)-CuO composites have similar surface areas and the pore volumes but which are much larger than those of S-CuO.

The measured low-magnification FESEM image shows that $H-SnO_2$ -CuO possesses similar morphology to its precursor particle, which is also in the shape of hollow spheres with an average size of ca. 5 μ m (Figure 3a,b). As revealed by the magnified images shown in Figure 3c,d, the CuO shell is constructed by interconnected disordered nanoparticles and nanosheets. The size of the primary nanoparticles is typically about 20 nm. A nearly 91% of morphological yield of this type can be achieved in our work. The SEM-EDS mapping of H-SnO₂-CuO further reveals that the elements of Cu,

O and Sn are homogeneously distributed throughout the entire particle (Figure 3e) and the weight ratio of Sn/Cu is measured to be about 0.19, which is close to the result of ICP-OES and the feeding ratio of the two precursors.



Figure 2. XRD patterns of all as-obtained samples.



Figure 3. (**a**–**d**) FESEM images of H-SnO₂-CuO; and (**e**) EDS mapping images: Cu (red), O (green) and Sn (yellow). The insert in image e is the corresponding EDS pattern.

Table 1. The physical property of all the samples.

Sample	d _{CuO} ^a (nm)	$S_{BET}^{\ b} (m^2 g^{-1})$	Pore Volume ^c (cm ³ g ^{-1})	Sn/Cu Weight Ratio ($\times 10^{-2}$)	
			fore forume (cm g)	Bulk ^d	Surface ^e
S-CuO	19.4	18.1	0.007	-	-
H-CuO	42.1	26.5	0.15	-	-
-SnO ₂ (0.05)-CuO	34.5	25.9	0.13	0.049	0.05
H-SnO ₂ (0.1)-CuO	30.8	26.8	0.13	0.098	0.18
H-SnO2-CuO	22.4	25.4	0.15	0.199	0.42
H-SnO ₂ (0.4)-CuO	22.9	27.1	0.12	0.398	0.38

^a The crystal size of CuO calculated from the XRD patterns; ^b The BET surface area of the catalysts; ^c Obtained at $P/P_0 = 0.99$; ^d Determined by ICP; ^e Determined by X-ray Photoelectron Spectroscopy (XPS).

The XPS spectra of Cu 2p, Sn 3d and O 1s were shown in Figure 4 and the presence of Cu, Sn, O and C elements are confirmed by XPS analysis of H-SnO₂-CuO (Figure 4a). From the XPS spectra of Cu 2p (Figure 4b), it can be seen that the major peaks at 933.5 and 953.6 eV can be assigned to

Cu $2p_{3/2}$ and Cu $2p_{1/2}$ of CuO, respectively [24], which are accompanied with a satellite peak at ca. 943.8 eV. Comparing with that of H-CuO sample, Cu $2p_{3/2}$ peak has a slight shift and it has decreased by 0.2 eV for H-SnO₂-CuO. Figure 4c shows the Sn 3d XPS spectrum of the H-SnO₂-CuO sample. The binding energies of Sn $3d_{5/2}$ and Sn $3d_{3/2}$ are located at 495.0 and 486.6 eV, respectively, indicating that the Sn species exists in the form of Sn^{4+} [25]. The surface Cu/Sn ratios determined by XPS and the bulk Cu/Sn ratios given by ICP in all the H-SnO₂(x)-CuO samples are both summarized in Table 1. Compared with the bulk counterpart (0.20), the weight ratio of Sn/Cu on the surface (0.42) is larger for H-SnO₂-CuO sample, suggesting that Sn element mainly distributed on crystallite surface. The above results indicate a generation of synergistic interactions between CuO and SnO₂ on the microsphere surface. The O 1s XPS spectra of H-CuO and H-SnO₂-CuO are numerically fitted into two sub-bands, which is shown in Figure 4d. The lower binding energy peak at 529.2–530.0 eV is ascribed to the idiomatical surface lattice oxygen cohere with the metal cations (denoted as O_{latt}) and the higher one at 530.5–531.5 eV is chemisorbed oxygen (denoted as Oads) [26]. The measured binding energies of O 1s for the H-CuO and H-SnO₂-CuO are different. Comparing with that of H-CuO sample, there is an increase of 0.2 eV of in the binding energy of O_{ads} peak for H-SnO₂-CuO, it is indicated that the introducing of Sn species could change the binding energy of O 1s obviously.



Figure 4. XPS spectra of H-CuO and H-SnO₂-CuO: (**a**) the survey spectrum; (**b**) Cu 2p spectrum; (**c**) Sn 3d spectrum; and (**d**) O 1s spectrum.

Figure 5 shows the detailed structural features of S-CuO, H-CuO and various H-SnO₂(x)-CuO composites with different ratios. S-CuO also has a uniform spherical shape with a size of ca. 5 µm. However, unlike the above H-SnO₂-CuO, it has a solid structure (Figure 5a). Through adjusting the feeding ratios of Sn/Cu in the synthesis, a series of samples with hollow structures can also be prepared, including H-CuO (Figure 5b), H-SnO₂(0.05)-CuO (Figure 5c), H-SnO₂(0.1)-CuO (Figure 5d) and H-SnO₂(0.4)-CuO (Figure 5e,f). Compared to H-SnO₂-CuO, these samples show no noticeable morphology and size changes. Moreover, the Sn/Cu weight ratios in all samples determined by ICP–OES are summarized in Table 1, which shows that adjustment of the ratio of metal precursors can control the final product composition.

2.3. The Formation Mechanism of H-SnO₂-CuO

To understand the formation mechanism of H-SnO₂-CuO, a series of experiments with various reaction hours were performed. Figure 6a-d illustrate the morphological evolution of the particles along with the reaction processing. In the early stage of the reaction, a fast reaction among the large number of Cu^{2+} ions, the carbonate ions (CO_3^{2-}) and the formed OH⁻ by hydrolysis of CO_3^{2-} occurred, which yields many small nanoparticles of Cu₂(OH)₂CO₃ with size of 20–30 nm (before 30 min, not shown). Meanwhile, Sn⁴⁺ ions are quickly hydrolyzed to produce SnO₂ nanoparticles. After 1 h reaction, these unstable or energetic nanoparticles have spontaneously built up solid microspheres with smooth outside surfaces (Figure 6a). Compared with these small particles in the exterior regions, those in the interior regions of the microsphere have higher surface energies, thus crystallites under the outer surface are preferentially dissolved through the process of inside-out Ostwald ripening. As a result, when the reaction duration is prolonged to 4 h, the solid SnO₂-CuO composites evolve to be a typical hollow yolk/shell structure, as displayed in Figure 6b. Additionally, it is also found that the primary nanoparticles in the outer surfaces become orderly arranged, because they are easier to be crystallized as compared to those in the internal surface. With the reaction up to 8 h, driven by minimization of surface energy, the inner core becomes smaller gradually until its complete disappearance. At the same time, the dissolved internal particles are recrystallized into tiny nanosheets, which finally develop into the "bundles of thorns" stretching out from the surface of these hollow spheres (Figure 6c). Eventually, after the reaction of 12 h, as depicted in Figure 6d, the initial solid structure has been evolved into a typical spherical structure with coarse surface anchoring with thick and large nanosheets. According to the above observations, this unique hollow structure evolution process follows the so-called "growth-cum-assembly" mechanism, which is depicted in Figure 6e. Such a process is very similar to that observed in the synthesis of CeO₂-CuO hollow microsphere [20].



Figure 5. SEM images of as-obtained samples: (**a**) S-CuO; (**b**) H-CuO; (**c**) H-SnO₂(0.05)-CuO; (**d**) H-SnO₂(0.1)-CuO; and (**e**,**f**) H-SnO₂(0.4)-CuO.



Figure 6. FESEM images of products obtained after different hydrothermal reaction time of (**a**) 1 h; (**b**) 4 h; (**c**) 8 h; and (**d**) 12 h; (**e**) Schematic illustration of the formation of the hollow microsphere.

2.4. Catalytic Performance

Table 2 summarizes the catalytic performances of all the catalysts in Rochow reaction measured at 325 °C for 24 h under atmospheric pressure. S-SnO₂ seems to be inactive. S-CuO also has a poor catalytic activity, with M2 selectivity and Si conversion being 61.2% and 7.9%, respectively. H-CuO shows a slightly better performance (68.6% of M2 selectivity and 13.1% of Si conversion), verifying the advantage of the hollow structure. The obvious improvement in catalytic performance is observed after introduction of SnO_2 into CuO. For H-SnO₂(0.05)-CuO, the M2 selectivity and Si conversion increase to 81.1% and 20.7%, respectively. When the ratio of Sn/Cu increases from 0.05 to 0.2, a drastic enhancement in M2 selectivity (88.2%) and Si conversion (36.7%) are observed for the H-SnO₂-CuO catalyst under the same conditions. This could be attributed to the generated synergetic interaction between CuO and SnO₂ [21]. To confirm it, a mechanically mixed sample of SnO₂ and hollow CuO (SnO₂/CuO) with the same ratio of Sn/Cu as that in H-SnO₂-CuO was prepared, which shows only a similar catalytic result to CuO alone. This fact suggests that the effective interfacial contacts between the CuO and SnO₂ components seems to be very important to improve the catalytic performance, while a simple physical mixing could not create such interface. However, when further increasing the amount of SnO₂, the property of catalyst obviously becomes worse again. In the case of H-SnO₂(0.4)-CuO, the selectivity of M2 and the conversion of Si are reduced to 72.1% and 16.4%, respectively. For all the catalysts investigated, the order of catalytic activity is as follows: H-SnO₂-CuO > H-SnO₂(0.1)-CuO > H-SnO₂(0.4)-CuO > H-CuO > S-CuO > S-SnO₂, suggesting that the excess or inadequate Sn content is adverse for the Rochow reaction. At the same time, to further confirm the superiority of H-SnO₂-CuO, a commercial catalyst Cu-Cu₂O-CuO (C-CAT) was also employed as a comparison. Although C-CAT has a more complex composition, it shows a poorer catalytic activity, with M2 selectivity and Si conversion being 78.0% and 16.0%, respectively, indicating that our H-SnO₂-CuO catalyst possesses much higher activity and selectivity to synthesize M2 than the commercial catalyst. These results demonstrate the importance of both the hollow structure and the SnO₂ promoter to the superior catalytic performance. In addition, byproducts such as M1, M3, M1H, M2H, LBR and HBR are also detected but without any obvious distribution difference over the various prepared catalysts.

Sampla	Product Composition (wt %)							$C_{-}(9/)$
Sample	M1	M2	M3	M1H	M2H	LBR	HBR	C_{Si} (70)
S-SnO ₂	-	-	-	-	-	-	-	-
S-CuO	14.1	61.2	3.7	9.1	1.0	1.9	7.4	7.9
H-CuO	11.7	68.6	1.8	2.5	4.8	2.7	7.9	13.1
H-SnO ₂ (0.05)-CuO	9.4	81.1	1.8	1.6	0.4	2.0	3.7	20.7
H-SnO ₂ (0.1)-CuO	6.9	85.7	1.6	1.2	0.7	1.5	2.4	25.4
H-SnO ₂ -CuO	5.1	88.2	1.0	0.9	1.0	0.9	2.9	36.7
H-SnO ₂ (0.4)-CuO	15.0	72.1	2.2	4.3	0.9	1.6	3.9	16.4
SnO ₂ /CuO ^b	14.0	67.8	2.1	9.3	0.3	1.0	7.5	10.1
C-CAT	12.0	78.0	4.0	0.8	0.6	0.5	3.1	16.0

Table 2. The properties of all the catalysts for the Rochow reaction ^a.

^a Reaction conditions: temperature, 325 °C; time, 24 h; catalyst, 0.5 g; Si, 10 g; gas flow: 25 mL/min. The conversion and selectivity results are obtained by three repeated testsunder the same conditions and the error bars are $\pm 0.1\%$; ^b a mechanical mixture of the as-synthesized SnO₂ and H-CuO at a weight ratio of 0.2:100.

The catalytic stability of our best catalyst H-SnO₂-CuO was measured at 325 °C under atmospheric pressure with a gas flow of 25 mL min⁻¹ for 72 h. Meanwhile, H-CuO and other SnO₂-CuO composites with different Sn/Cu ratios were also tested for comparisons and the results are shown in Figure 7. Among all the measured samples, H-SnO₂-CuO has the most stable catalytic performance. As shown in Figure 7a, after 10 h of induction period, the M2 selectivity only shows a slight decrease from 81.7% to 78.6% over a period of 72 h for H-SnO₂-CuO but for H-CuO, the M2 selectivity reduces from 60.9% to 42.3% after a 60 h reaction, obviously indicating that H-SnO₂-CuO possess a more stable catalytic performance. On the other hand, after 72 h reaction, the M2 yield is still 45.7% and Si conversion still 56.1% for H-SnO₂-CuO shows a much higher M2 yield and Si conversion as compared to those of pure CuO. The above results show that the catalyst stability can be greatly improved by the addition of SnO₂.



Figure 7. Stability of H-CuO and various H-SnO₂-CuO samples: (**a**) M2 selectivity; (**b**) Si conversion; and (**c**) M2 yield. Reaction conditions: temperature, 325 °C; catalyst, 0.5 g; Si, 10 g; gas flow: 25 mL/min.

The measured XRD patterns of the reacted contact masses after a 24 h reaction over S-CuO, H-CuO and H-SnO₂-CuO catalysts are shown in Figure 8a. It is found that, the composition of reacted contact masses are Si and Cu and no any CuO phase is detected, because of the reaction of MeCl with the lattice oxygen from CuO that leads to the formation of Cu in the induction period, which means the time of the transformation of the catalyst into real active phase under reaction conditions [27]. Figure 8b shows the SEM image, elemental mapping images and SEM-EDX spectra of the reacted contact masses by using H-SnO₂-CuO catalyst, which indicates the uniform distribution of the elements Si, Cu and Cl along the interface. For the unreacted regions, the surfaces of Si particles are relatively smooth and flat; while for the reacted region (marked by yellow dotted ellipse), much obvious nick on Si surface indicate that the processing of reaction includes an etching process, which is in accordance with the so-called anisotropic etching reaction mechanics [28,29].



Figure 8. XRD patterns of contact masses after reaction: (**a**) (1) S-CuO, (2) H-CuO and (3) H-SnO₂-CuO); (**b**) SEM image of the contact mass using H-SnO₂-CuO catalysts after a 24 h reaction and the corresponding elemental mapping images.

The previous literature reports have shown that Cu_x Si species produced during the reaction are the necessities of active immediate in the M2 synthesis, therefore the formation of the active Cu_x Si species is the crucial step in Rochow reaction [30–32]. Comparing with S-CuO, H-SnO₂-CuO has smaller primary particles and larger surface areas, thus it can facilitate adsorption of MeCl molecules on its surface more efficiently. These adsorbed MeCl molecules will be dissociated rapidly into electronegative Cl⁻ and electropositive CH₃⁺ [20,33]. As a result, the subsequent next step of forming active immediate Cu_xSi species will be accelerated obviously on H-SnO₂-CuO. In addition, the presence of Sn species on the CuO surface could reduce the activation energy of the reaction due to the synergistic effect [22], thus facilitating formation of more Cu_xSi species. Based on the analysis above, a possible mechanism for the Rochow reaction using H-SnO₂-CuO is proposed. Firstly, the reactant Si is mixed with H-SnO₂-CuO catalyst to form the contact masses. When increasing the reaction temperature, this catalyst first reacts with MeCl to form Cu atoms, then those Cu atoms gradually diffuse into Si matrix and react with the generated Si atom, finally forming the active phase Cu_x Si alloy at the interface. The formative Cu_x Si species there may present modest adsorption and activation energy to MeCl, which subsequently transforms into M2. Finally, more elemental copper is generated with the reaction continues and the catalyst completely deactivates when Cu in the Cu_xSi alloy is consumed.

3. Experimental

3.1. Material Synthesis

All the reagents in this experiment were analytical grade and purchased from Sinopharm Chemical Reagent Co. Ltd., Beijing, China and used as received. The SnO₂-CuO hollow microspheres were synthesized by a hydrothermal method. Typically, 1.2 g of Cu(CH₃COO)₂·H₂O (6 mmol) and a varied amount of SnCl₄·5H₂O were dissolved in 60.0 mL of deionized water with continuous stirring at room temperature, followed by the dropwise addition of 20.0 mL of Na₂CO₃ solution (0.3 M). The mixed solution was then transferred into a 100-mL Teflon-lined stainless steel autoclave, which was kept at 140 °C for 12 h. After cooling, the obtained precipitate was collected by filtration, washed with deionized water and ethanol several times and dried in air at 60 °C overnight. Finally, the obtained intermediate product was calcined in muffle oven at 400 °C for 3 h. The prepared samples are denoted as H-SnO₂(*x*)-CuO (*x* = 0.05, 0.1, 0.2, 0.4), where H refers to "Hollow structure" and *x*

refers to the weight ratios of Sn and Cu. Unless otherwise specified, $H-SnO_2-CuO$ in the text refers to $H-SnO_2(0.2)-CuO$. For comparison, pure H-CuO and $S-SnO_2$ were prepared followed with similar procedures but with only $Cu(CH_3COO)_2 \cdot H_2O$ or $SnCl_4 \cdot 5H_2O$ added, respectively and the samples are denoted as H-CuO and $S-SnO_2$. In addition, the synthesis procedure for S-CuO was the same as that for H-CuO except that the hydrothermal time was 1 h, where S refers to "Solid" structure.

3.2. Material Characterization

X-ray diffraction (XRD) analysis was performed on a PANalytica X'Pert PRO MPD (Almelo, the Netherlands) using the K α radiation of Cu (λ = 1.5418 Å) and the crystallite sizes were calculated using the Debye-Scherrer equation. The dimension and morphology of the samples were characterized by field-emission scanning electron microscopy (FESEM) with energy-dispersive X-ray spectrometer (EDX) (JSM-7001F, JEOL, Tokyo, Japan). X-ray photoelectron spectroscopy (XPS) analysis was carried out on a Model VG ESCALAB 250 spectrometer, Thermo Electron, London, UK, using a non-monochromatized Al–K α X-ray source (1486.6 eV). Thermal gravimetric (TG) analysis was executed on an EXSTAR TG/DTA 6300 (Seiko Instruments, Chiba, Japan). During the measurement, the temperature range was controlled from 30 to 900 °C and the heating rate was kept 2 °C/ min of in air (200 mL/min). The specific surface area was measured using the Brunauer-Emmett-Teller (BET) method and the relative pressure range was from 0.05 to 0.3.

3.3. Catalytic Test

The catalytic performance of the samples was evaluated with a fixed-bed reactor. 10.0 g of Si powder (20-50 mesh, provided by Tangshan Sanyou Group Co., Ltd., Tangshan, China) and 0.5 g of catalysts, together with 0.05 g of zinc (Zn, A.R., Sinopharm Chemical Reagent Co., Ltd., Tangshan, China) as the promoter were mixed homogeneously to form a fresh contact mass. N₂ gas flow (25 mL/min) was used to purge the reactor system for 30 min followed by heating to 325 °C within 1 h. Afterwards, the N₂ gas was turned off and MeCl gas was fed at a flow rate of 25 mL/min to react with Si for a settled time (12–72 h). All the reactions were carried out under atmospheric pressure and at 325 °C. After stopping the reaction, the gas products were cooled into liquid using the circulator bath kept at -5 °C by a programmable thermal circulator (GDH series, Ningbo Xinzhi Biological Technology Co., Ltd., Ningbo, China). Gas chromatograph (GC-7890A, Agilent Technologies, Santa Clara, CA, USA) equipped with a KB-201 capillary column (60 m) and a thermal conductivity detector (TCD) was employed to analyze the composition of liquid products, which were mainly composed of methyltricholorsilane (CH₃SiCl₃, M1), dimethyldichlorosilane ((CH₃)₂SiCl₂, M2), trimethylchlorosilane ((CH₃)₃SiCl, M3), methyldichlorosilane (CH₃SiHCl₂, M1H), dimethylchlorosilane ((CH₃)₂SiHCl, M2H), low boiler (LB) and high boiler (HB). The selectivity of products was determined by calculating the peak area ratio and the conversion of Si was determined by the mass change of Si powder before and after the reaction (Formula (4)).

Si conversion :
$$C_{\rm Si}(\%) = \frac{m_{\rm Si, \ before} - m_{\rm Si, \ after}}{m_{\rm Si, \ before}} \times 100$$
 (4)

4. Conclusions

To summarize, heterostructured SnO₂-CuO hollow microspheres have been synthesized by a simple, template-free hydrothermal method coupled with calcination. In the resultant SnO₂-CuO composite, SnO₂ particles are mainly enriched on the surface of CuO hollow microspheres, which are assembled into by many interconnected CuO nanoparticles in the interior of the microspheres and by the outer layer of CuO nanosheets. Moreover, the obtained hollow SnO₂-CuO composite microspheres exhibit a higher selectivity to synthesize M2 and Si conversion than that of non-hollow structure and individual counterparts for the Rochow reaction, mainly attributed to the advanced structure and the synergistic interaction between CuO and SnO₂. The clear structure-catalytic property relation gained

in this work should be useful to the design of more-efficient multi-component Cu-based catalysts for the Rochow reaction.

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