

## Article

# Optimizing an Anaerobic Hybrid Reactor Series for Effective High-Strength Fresh Leachate Treatment and Biogas Generation

Sakulrat Sutthiprapa<sup>1,2</sup>, Sirintornthep Towprayoon<sup>1,2</sup>, Chart Chiemchaisri<sup>3</sup> , Pawinee Chaiprasert<sup>4</sup>   
and Komsilp Wangyao<sup>1,2,\*</sup> 

<sup>1</sup> The Joint Graduate School of Energy and Environment, King Mongkut's University of Technology Thonburi, Bangkok 10140, Thailand; sakulrat.sua@svit.ac.th (S.S.); sirin.jgsee@gmail.com (S.T.)

<sup>2</sup> Center of Excellence on Energy Technology and Environment (CEE), Ministry of Higher Education, Science, Research and Innovation (MHESI), Bangkok 10140, Thailand

<sup>3</sup> Department of Environmental Engineering, Faculty of Engineering, Kasetsart University, Bangkok 10900, Thailand; fengccc@ku.ac.th

<sup>4</sup> Biotechnology Program, School of Bioresources and Technology, King Mongkut's University of Technology Thonburi, Bangkok 10150, Thailand; pawinee.cha@kmutt.ac.th

\* Correspondence: komsilp.wan@kmutt.ac.th; Tel.: +66-2470-8309; Fax: +66-2872-9805

**Abstract:** Treating high-strength fresh leachate is challenging and of great interest due to the inherent variability in its physical and chemical characteristics. This research aims to enhance the efficiency of the anaerobic hybrid reactor (AHR) series in treating high-strength fresh leachate and achieving biogas generation from fresh leachate at ambient temperatures. The AHR series used consists of two serially connected reactors termed the first anaerobic hybrid reactor (AHR-1) and the secondary anaerobic hybrid reactor (AHR-2). AHR-1 treated high-concentration fresh leachate with an organic loading rate (OLR) between 5 and 20 kgCOD/m<sup>3</sup>·d. AHR-2 treated the effluent from the first tank and removed organic matter from the system. The experiment was conducted for 210 days, showing that an OLR of 10 kgCOD/m<sup>3</sup>·d resulted in the most suitable COD removal efficiency, ranging from 82 to 91%. The most suitable OLR for biogas production was 15 kgCOD/m<sup>3</sup>·d. The AHR series proved to be an efficient system for treating high-strength fresh leachate and generating biogas, making it applicable to leachate treatment facilities at waste transfer stations and landfill sites. Treating leachate and utilizing it as a renewable energy source using the AHR series presents a practical and efficient waste management approach. High-strength leachate can be effectively treated with the AHR series; such methods may be integrated into industries treating leachates with high COD values.

**Keywords:** anaerobic digestion efficiency; wastewater-to-energy; sustainable waste management; methane recovery; leachate valorization



**Citation:** Sutthiprapa, S.; Towprayoon, S.; Chiemchaisri, C.; Chaiprasert, P.; Wangyao, K. Optimizing an Anaerobic Hybrid Reactor Series for Effective High-Strength Fresh Leachate Treatment and Biogas Generation. *Sustainability* **2024**, *16*, 3076. <https://doi.org/10.3390/su16073076>

Academic Editors: Mehrab Mehrvar, Edgar Quiñones-Bolaños, Ciro Bustillo-Lecompte and Samira Ghafoori

Received: 20 February 2024

Revised: 27 March 2024

Accepted: 6 April 2024

Published: 7 April 2024



**Copyright:** © 2024 by the authors. Licensee MDPI, Basel, Switzerland. This article is an open access article distributed under the terms and conditions of the Creative Commons Attribution (CC BY) license (<https://creativecommons.org/licenses/by/4.0/>).

## 1. Introduction

The amount of waste being produced worldwide is on the rise as cities grow and populations increase. Waste-to-energy (WTE) technologies like incineration, anaerobic digestion and mechanical biological treatment (MBT) are becoming more popular. These approaches not only help decrease the amount of waste going into landfills but also harness energy from waste, providing a twofold advantage [1–3]. Effective handling of solid waste (MSW) is crucial for promoting sustainable urban development [1]. Challenges in managing waste in developing countries include insufficient waste collection and the practice of open dumping in non-engineered landfills, resulting in pollution and harm to the environment [4]. To tackle these problems, it is essential to adopt waste management strategies that prioritize converting waste into energy and promoting circularity in handling MSW [5].

Fresh leachate is a highly concentrated liquid waste that often contains hazardous components [6]. It is generated during waste collection and landfilling processes and, if

not managed properly, can significantly impact the environment. Leachate treatment is critical to minimize its environmental impact. Organic pollutants and high concentrations of suspended solids and toxins in fresh leachate can inhibit the function of beneficial bacteria in wastewater treatment systems [7]. Untreated leachate discharge can contaminate groundwater, surface water, and the surrounding ecosystems, posing severe environmental and health risks [8,9]. Fresh leachate is characterized by both a high chemical oxygen demand (COD) and a high biochemical oxygen demand (BOD<sub>5</sub>), making its treatment challenging. Traditional wastewater treatment methods are ineffective in reducing this contamination level [10,11]. Furthermore, leachates with high concentrations of ammonia, sulfate, and calcium present significant obstacles to biological treatment methods, reducing the efficiency of leachate treatment and adversely affecting methane (CH<sub>4</sub>) gas production processes [12,13]. Leachate treatment is crucial for sustainable waste management approaches [14,15].

Fresh leachate treatment remains a challenge due to limited studies on the subject. Achieving efficient fresh leachate treatment would address pollution problems and reduce greenhouse gas emissions during leachate management. Effective and swift leachate management can reduce water and air pollution and minimize the prevalence of disease by controlling the spread of pathogens into the environment, thereby reducing health risks to the public. Anaerobic treatment systems are popular solutions for managing high-concentration wastewater [15] and are suitable for treating wastewater with complex compositions. Biogas production is a key advantage of anaerobic leachate treatment [16]. Biogas primarily consists of CH<sub>4</sub> and carbon dioxide (CO<sub>2</sub>), both of which significantly impact the environment [17]. CH<sub>4</sub> production from leachate helps to reduce atmospheric CH<sub>4</sub> emissions, thereby contributing to climate change mitigation. Furthermore, CH<sub>4</sub> produced from fresh leachate can be reused as energy, providing a renewable energy source [18,19]. Biogas is thus a valuable resource for energy production, offsetting energy costs associated with leachate treatment systems.

Developing technologies for renewable energy production from leachate represents a sustainable economic and environmental approach [20] and aligns with circular economy principles and efficient resource use (a closed loop). Transforming waste into valuable resources is a fundamental aspect of sustainable waste management. Leachate is, therefore, increasingly viewed as a resource for energy production and environmental protection [21]. By converting high-strength leachate into biogas, not only does our proposed anaerobic hybrid reactor series contribute to sustainable waste management, but it also unveils significant opportunities for renewable energy production and economic gains, paving the way for a circular economy. This study aims to determine the optimal operating conditions to enhance the efficiency of anaerobic hybrid reactors in treating high-concentration fresh leachate and facilitating biogas production. It then evaluates the rate and quality of biogas and CH<sub>4</sub> production, assessing COD removal efficiency and providing valuable information for effective and sustainable waste management practices.

## 2. Materials and Methods

This research was conducted to enhance the efficiency of the anaerobic hybrid reactor (AHR) series system. The treatment of high-concentration fresh leachate is aimed primarily at biogas production. The experimental procedures and analytical methods used are detailed in the following.

### 2.1. Anaerobic Hybrid Reactor (AHR) Series System

This study involved an experimental trial at the laboratory level. The AHR system used was made from cylindrical acrylic tubes, which are durable and transparent, allowing observation of the operation of the system during experiments. The AHR series had a cylindrical shape, with a diameter of 20 cm and a height of 100 cm, and consisted of a serial connection of AHR-1 and AHR-2 with a total operational volume of 40 L. AHR-1 and AHR-2 were packed with nylon fiber media, which played a crucial role in bacterial adhesion and

increased the surface area available for microbial growth [22]. The integration of suspended and attached growth systems, as exemplified by the Up-flow Anaerobic Sludge Blanket with the Down-flow Hanging Sponge (UASB-DHS) technology discussed in Mazhar et al. [23], represents a significant advancement in the field of wastewater treatment. This study underscores the potential of combining the UASB with the DHS system to achieve high efficiency in pollutant removal, notably BOD, COD, TSS, and VSS, with removal efficiencies reaching up to 93%. Such efficiencies are attributed to the dual-action mechanism where the anaerobic UASB reactor effectively breaks down organic matter, producing biogas, and the DHS system, functioning aerobically, provides additional polishing of the effluent. The characteristics of the media attachment in the reactor before the start of the experiment are shown in Figure 1.



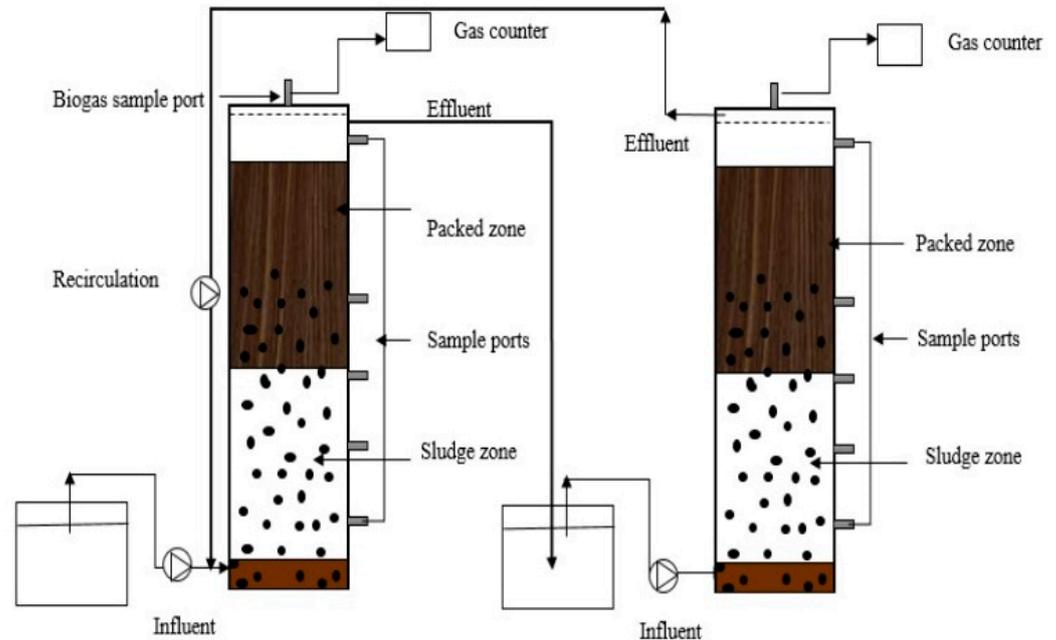
**Figure 1.** Nylon fiber carriers in the AHR series system.

## 2.2. Experimental Procedure

The AHR series system used in this research consisted of two reactors connected in series. AHR-1 received fresh leachate and was set with a specific organic loading rate (OLR). AHR-2 received the effluent from AHR-1. A schematic of the AHR series is shown in Figure 2. This experiment was conducted at room temperature. Before the experiment, sludge, which was collected from an anaerobic leachate treatment system in the Racha Thewa area, Bang Phli, Thailand, was cultured inside the reactors. The experiment started with an OLR of  $1 \text{ kgCOD/m}^3 \cdot \text{d}$  for 60 days, after which the OLR was continuously increased to  $20 \text{ kgCOD/m}^3 \cdot \text{d}$ . The hydraulic retention time (HRT) ranged from 5 to 30 days, whereas the sludge retention time (SRT) was 15 days. The OLR was controlled between 5 and  $20 \text{ kgCOD/m}^3 \cdot \text{d}$ , consistent with Sakulrat et al. [24], who studied a single-tank AHR system. The performance assessment of the AHR series involved the analysis of the quantity of biogas produced. The COD values of both the influent and effluent were determined. The leachate effluent released from AHR-1 provided the influent for AHR-2. The percentage of COD removal within the AHR series was calculated using Equation (1).

$$\% \text{COD Removal of AHR series} = ((C_{i\text{AHR1}} - C_{f\text{AHR2}}) / C_{i\text{AHR1}}) \times 100 \quad (1)$$

where  $C_{i\text{AHR1}}$  is the initial concentration of COD (mg/L) in AHR-1, and  $C_{f\text{AHR2}}$  is the final concentration of COD (mg/L) in AHR-2.



**Figure 2.** AHR series schematic diagram.

### 2.3. Sample Collection and Analysis Methods

The methods for collecting and analyzing the samples used in this study are as follows. Fresh leachate samples from the On-Nut waste transfer station in Bangkok, Thailand, were analyzed for their physical and chemical properties before designing the reactor tanks. The parameters analyzed included pH, COD, BOD, total solids in leachate, total volatile fatty acids, total Kjeldahl nitrogen (TKN), ammonia nitrogen, and heavy metals. The leachate samples were stored at a temperature not exceeding 4 °C prior to analysis. The biochemical methane potential (BMP) of fresh leachate and effluent from the anaerobic reactors was determined to assess the potential for CH<sub>4</sub> production following the method presented by Holliger [25]. Gas samples were collected to analyze the main components of biogas, namely CH<sub>4</sub>, CO<sub>2</sub>, and O<sub>2</sub>, using a Clarus 580 Gas Chromatograph (Shimadzu, Kyoto, Japan). Wastewater was collected daily from the reactors, and the pH of this water was measured using a pH meter. Total solids in leachate were determined by filtering through a glass microfiber filter (GF/C) according to standard methods [26]. The concentration and percentage of CH<sub>4</sub>, CO<sub>2</sub>, and hydrogen sulfide (H<sub>2</sub>S) were measured daily using a Biogas 5000 system (Geotech, Chelmsford, UK). Samples from AHR-1 and AHR-2 were collected for COD analysis once per week. The volatile solids on the nylon fiber media were analyzed at the end of the experiment. Finally, the relationship was analyzed using descriptive statistics to evaluate the enhancement of AHR series efficiency.

## 3. Results and Discussion

### 3.1. COD Removal Efficiency

This study found that the AHR series had an average COD removal efficiency of 91% at an OLR of 10 kgCOD/m<sup>3</sup>·d and maintained a COD removal efficiency of 88% when the OLR increased to 15 kgCOD/m<sup>3</sup>·d, consistent with a previous study by Maleki et al. [27]. Increasing the OLR from 1.36 to 3.18 kgCOD/m<sup>3</sup>·d caused the COD removal efficiency to decrease from 94.1% to 90.2% and the biogas production to decrease from 0.34 to 0.31 L/g.

This shows that the anaerobic system suits wastewater with high organic content and offers a viable alternative mechanism for COD removal. The AHR series system is environmentally friendly and provides energy for reuse, as described in research's Genethlio [28]. Figure 3 shows the COD removal efficiency at different OLR levels. Increasing the OLR from 10 to 15 kgCOD/m<sup>3</sup>·d allowed a good COD removal efficiency to be maintained, demonstrating the stability and efficiency of the system when treating wastewater. This flexibility demonstrated the adaptability of the AHR series system, showing that efficient COD removal can be maintained throughout a controlled OLR increase. Rinquest showed that higher OLR values could result in a decrease in COD removal efficiency [29]. Harsha and Maurya found that an increased organic load could affect the ability of microorganisms to grow and efficiently remove COD [30]. As shown in Figure 4a,b, the relationships between the percentage of COD removal CH<sub>4</sub> production and between biogas production and CH<sub>4</sub> production in the AHR series exhibited linear regression with R<sup>2</sup> values of 0.96 and 0.97, respectively.

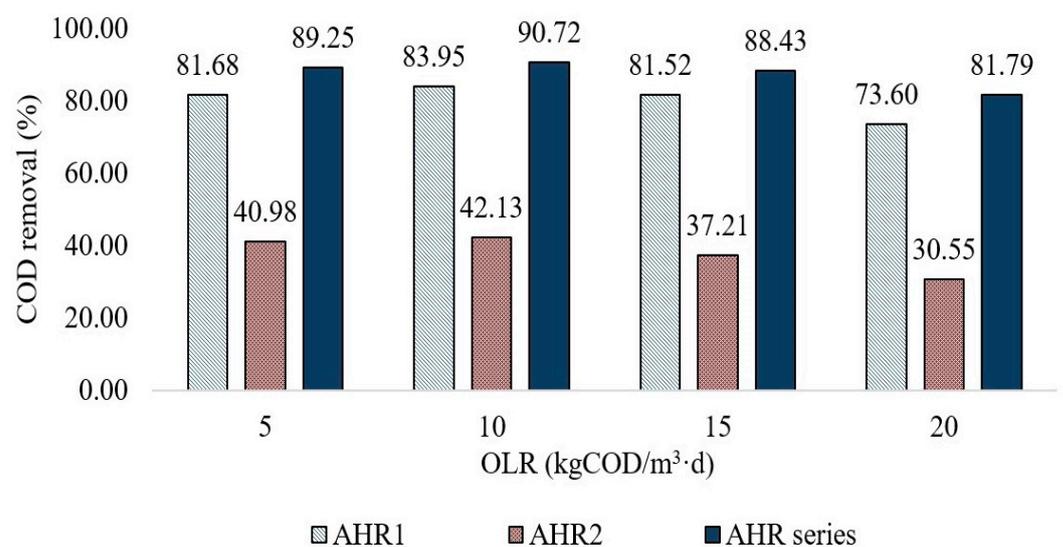


Figure 3. COD removal efficiencies of the AHR series at various OLRs.

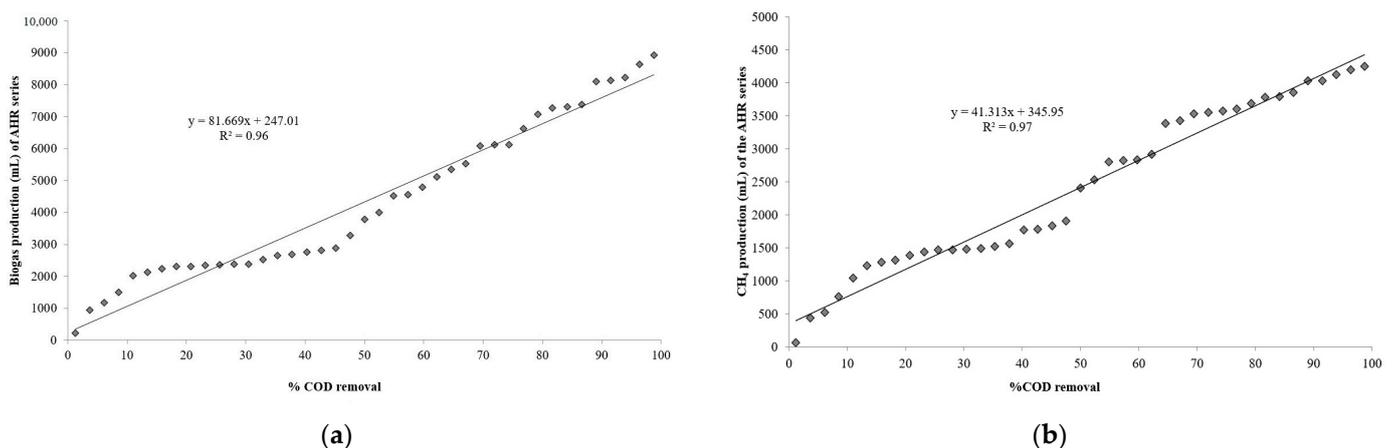


Figure 4. Relationships between (a) %COD removal and biogas production of the AHR series and (b) %COD removal and CH<sub>4</sub> production of the AHR series.

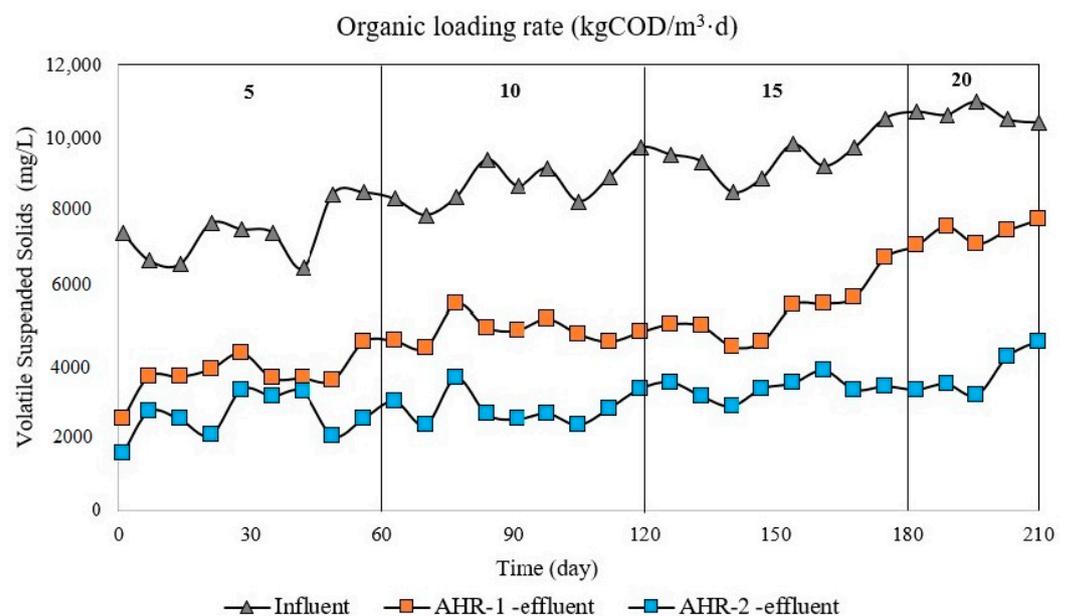
A vital objective of the AHR series system is to enhance COD removal efficiency and biogas production, which were analyzed using a one-way analysis of variance (ANOVA) at a 95% confidence level to assess the relationships between variables. The R<sup>2</sup> value, which explains the relationship between the independent variables affecting COD removal

efficiency and biogas production, suggested that values greater than 0.5 indicate a moderate relationship between parameters [31]. Therefore, the starting OLR directly influences both COD removal efficiency and biogas production. The related factor, a primary variable in this experiment, is OLR, which is correlated with  $\text{CH}_4$  production in the AHR series and has a statistical significance at  $p$ -value  $< 0.05$ .

High-strength fresh leachate can be effectively treated using various methods, as demonstrated in the literature. One study investigated the treatment of fresh leachate from municipal solid waste incineration plants using an expanded granular sludge bed (EGSB) reactor, achieving an average COD removal efficiency of 87% [32]. Another study examined the coagulation–flocculation process followed by biological treatment for landfill leachate, where coagulation treatment achieved a COD removal efficiency of 35%, and the anaerobic filter achieved 20%, with the combined technologies achieving 51.52% [33]. Additionally, the use of organic modified bentonites was effective in the pretreatment of high-strength landfill leachate, with a COD removal efficiency of 67% under optimum conditions [34]. However, our study's AHR series demonstrated a higher COD removal efficiency, achieving an average of 91% at an OLR of  $10 \text{ kgCOD/m}^3 \cdot \text{d}$ , and even maintained an 88% efficiency when the OLR increased to  $15 \text{ kgCOD/m}^3 \cdot \text{d}$ . This not only aligns with but also surpasses the efficiencies reported in previous studies, marking a significant advancement in the treatment of high-strength leachate and showcasing the AHR series as a robust and efficient solution.

### 3.2. Removal of Organics in Solid

The volatile suspended solids (VSS) in the influent and effluent of the system can be used to assess the efficiency of organic matter reduction. A decrease in the VSS of the treatment system indicates the leachate treatment efficiency of the system. As shown in Figure 5, increasing the OLR causes the VSS of the system to increase. At an OLR of  $5 \text{ kgCOD/m}^3 \cdot \text{d}$ , the VSS concentration ranged between 1520 and 4245 mg/L. Increasing the OLR to 10, 15, and 20  $\text{kgCOD/m}^3 \cdot \text{d}$  resulted in a continuous increase in both the VSS and total biomass of the AHR series.



**Figure 5.** Volatile suspended solids in the influent and effluent of AHR reactors.

### 3.3. Quantitative Assessment of Biogas and Methane Production

Quantitative assessments of the volume of biogas and  $\text{CH}_4$  produced in AHR-1, AHR-2, and the AHR series were performed. Biogas and  $\text{CH}_4$  production (both in mL/day) are shown in Table 1.

As shown in Table 1, the AHR series produced the highest biogas and CH<sub>4</sub> at an OLR of 15 kgCOD/m<sup>3</sup>·d, with biogas production at 6476 mL/day and CH<sub>4</sub> production at 3857 mL/day. When the OLR was increased to 20 kgCOD/m<sup>3</sup>·d, the production of biogas and CH<sub>4</sub> decreased. Increasing the OLR provides results consistent with the findings of Maleki et al., who found that biogas production decreased when the OLR was increased from 1.36 to 3.18 kgCOD/m<sup>3</sup>·d. AHR-1 and AHR-2 both showed efficient biogas and CH<sub>4</sub> production and have excellent potential for biogas production [35]. The AHR series is also environmentally friendly, aligning with the concepts of Moujanni et al. [36]. The cumulative biogas and CH<sub>4</sub> volumes are shown in Table 2.

**Table 1.** Quantitative evaluation of biogas and CH<sub>4</sub> production.

| OLR<br>(kgCOD/m <sup>3</sup> ·d) | Biogas Production (mL/Day) |       |            | CH <sub>4</sub> Production (mL/Day) |       |            |
|----------------------------------|----------------------------|-------|------------|-------------------------------------|-------|------------|
|                                  | AHR-1                      | AHR-2 | AHR Series | AHR-1                               | AHR-2 | AHR Series |
| 5                                | 1404                       | 713   | 2117       | 840                                 | 377   | 1217       |
| 10                               | 3102                       | 1435  | 4537       | 1961                                | 810   | 2771       |
| 15                               | 4409                       | 2067  | 6476       | 2676                                | 1181  | 3857       |
| 20                               | 5357                       | 2599  | 7956       | 2628                                | 1160  | 3788       |

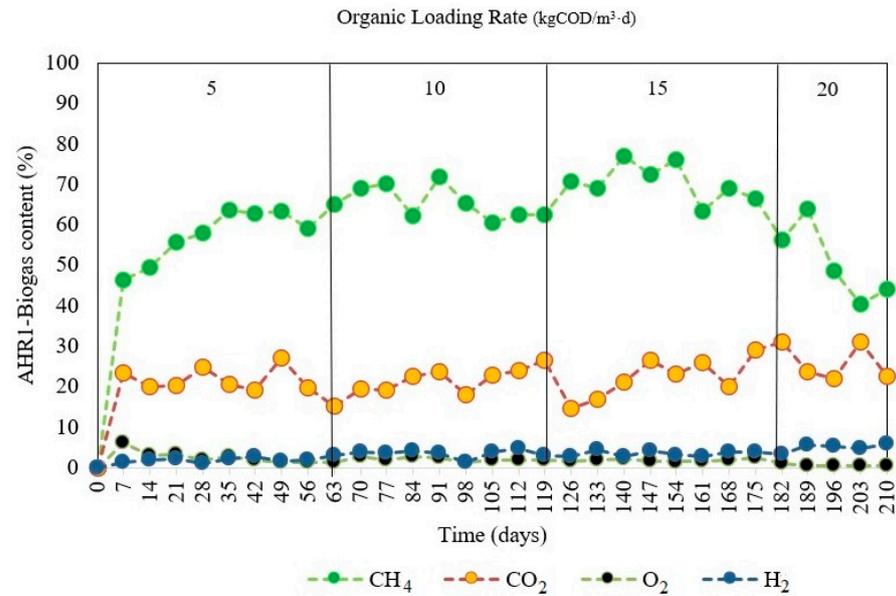
**Table 2.** Cumulative biogas and CH<sub>4</sub> (210 days) using AHR-1, AHR-2 and the AHR series.

| OLR<br>(kgCOD/m <sup>3</sup> ·d) | Cumulative Biogas (mL) |         |            | Cumulative CH <sub>4</sub> (mL) |        |            |
|----------------------------------|------------------------|---------|------------|---------------------------------|--------|------------|
|                                  | AHR-1                  | AHR-2   | AHR Series | AHR-1                           | AHR-2  | AHR Series |
| 5                                | 84,217                 | 42,805  | 127,022    | 50,376                          | 22,618 | 72,994     |
| 10                               | 186,116                | 86,107  | 272,223    | 117,651                         | 48,591 | 166,242    |
| 15                               | 264,537                | 124,012 | 388,549    | 160,577                         | 70,840 | 231,417    |
| 20                               | 160,699                | 77,973  | 238,672    | 78,841                          | 34,803 | 113,644    |

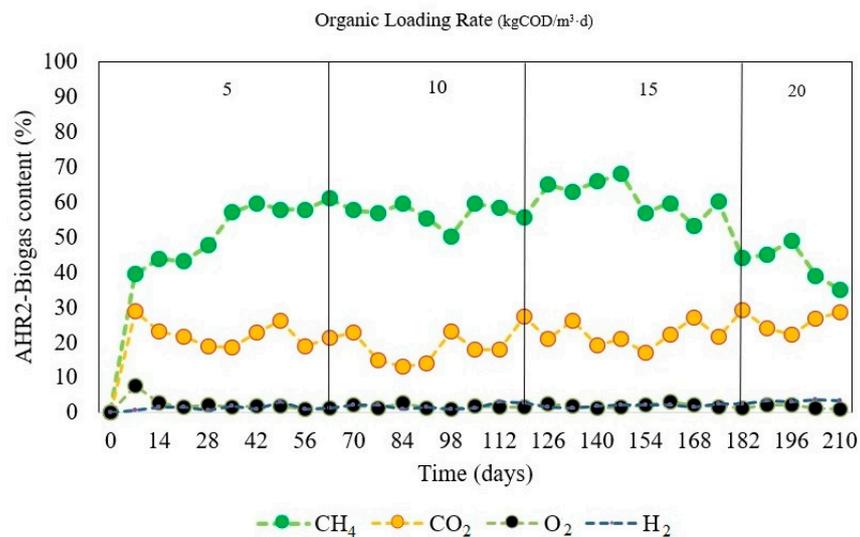
As shown in Table 2, the AHR series produced the highest cumulative biogas and CH<sub>4</sub> at an OLR of 15 kgCOD/m<sup>3</sup>·d, with a cumulative biogas production of 388,549 mL and a cumulative CH<sub>4</sub> production of 231,417 mL. The next highest production occurred at an OLR of 10 kgCOD/m<sup>3</sup>·d. Conversely, increasing the OLR from 15 to 20 kgCOD/m<sup>3</sup>·d caused the production of biogas and CH<sub>4</sub> to decrease.

### 3.4. Assessment of the Quality of Biogas and CH<sub>4</sub> Production

To enhance the efficiency of biogas production, it is necessary to produce large quantities of high-quality biogas. The quality of CH<sub>4</sub>, expressed as a percentage, is an essential parameter in assessing the use of biogas for energy applications [37,38]. Figure 6 shows the quality of CH<sub>4</sub> at OLR conditions of 5, 10, 15, and 20 kgCOD/m<sup>3</sup>·d. This study found that the operation of AHR-1 and AHR-2 complemented the efficiency of the other. AHR-1 resulted in a CH<sub>4</sub> quality of up to 60.8%, while AHR-2 had a slightly lower CH<sub>4</sub> quality of 57.1%. These results indicate that AHR-1 had more suitable conditions for CH<sub>4</sub> production and was able to consistently maintain higher quantities and quality of CH<sub>4</sub>. Increasing the OLR to 20 kgCOD/m<sup>3</sup>·d caused CH<sub>4</sub> production to decrease, indicating that the efficiency of the system decreases when the OLR is increased above 15 kgCOD/m<sup>3</sup>·d. Higher OLR values influence the function of the CH<sub>4</sub>-producing microbial community due to overloading. The primary objective of the AHR is anaerobic digestion, which involves microbes that produce acids to generate biogas. The results of this study are consistent with the findings of Collivignarelli et al. and Umiejewska et al. [39,40].



(a)

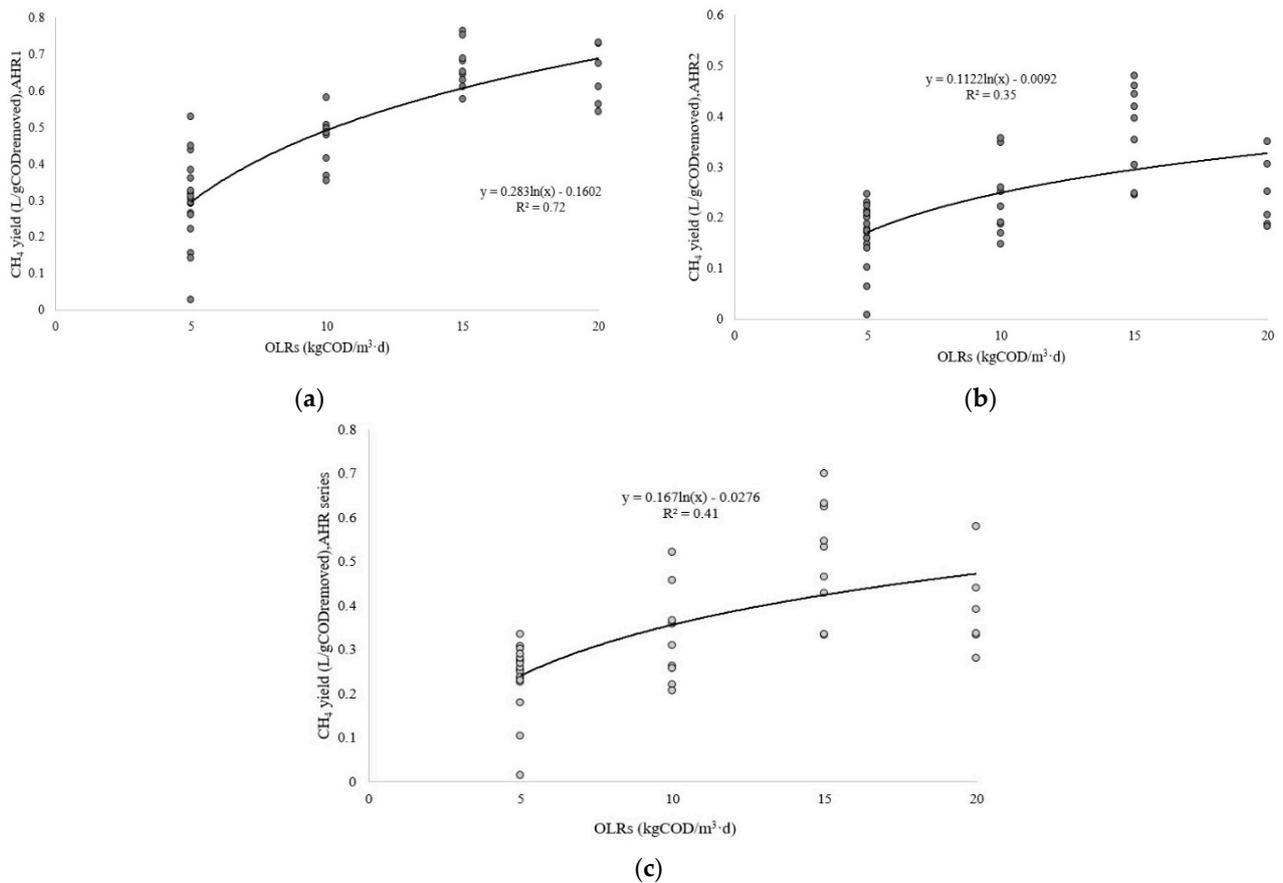


(b)

**Figure 6.** CH<sub>4</sub> contents (%) in (a) AHR-1 and (b) AHR-2.

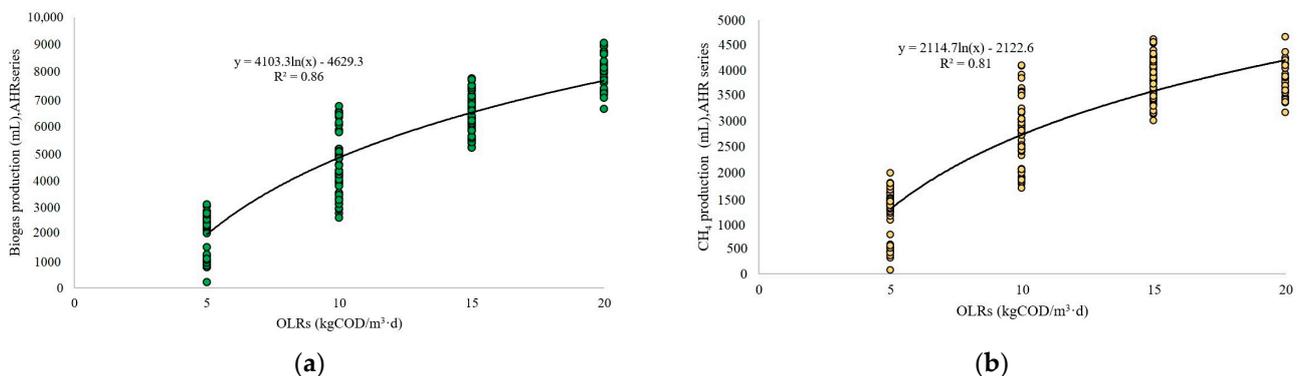
### 3.5. Methane Production Rate

Analysis of the relationship between OLR and CH<sub>4</sub> yield (L/g COD removed) for AHR-1, AHR-2, and the AHR series systems showed that the maximum CH<sub>4</sub> production per COD removal was achieved by setting the OLR of the system to 15 kgCOD/m<sup>3</sup>·d. AHR-1 resulted in an average CH<sub>4</sub> production per COD removal of 0.57–0.76 L/g COD removed, whereas AHR-2 achieved an average of 0.27–0.47 L/g COD removed. The AHR series removed an average of 0.33–0.67 L/g COD. Yodthongdee found that the efficiency of anaerobic wastewater treatment depends on the ability to remove COD and CH<sub>4</sub> formation per COD removal [41]. Analyses of the relationships between OLR and CH<sub>4</sub> yield (L/g COD removed) for AHR-1, AHR-2, and the AHR series systems showed logarithmic curves with coefficient of determination (R<sup>2</sup>) values of 0.72, 0.35, and 0.41, respectively, as shown in Figure 7a–c.



**Figure 7.** Relationships between (a) OLR and CH<sub>4</sub> yield of AHR-1, (b) OLR and CH<sub>4</sub> yield of AHR-2, and (c) OLR and CH<sub>4</sub> yield of the AHR series.

Furthermore, at an OLR of 5–15 kgCOD/m<sup>3</sup>·d, the production of biogas and CH<sub>4</sub> was found to increase. However, when increasing the OLR to 20 kgCOD/m<sup>3</sup>·d, CH<sub>4</sub> tended to decrease due to reduced components within the biogas. Analysis of the relationship between OLR and the production of biogas and CH<sub>4</sub> in the AHR series showed logarithmic curves with R<sup>2</sup> values of 0.86 and 0.81, respectively, as shown in Figure 8a,b.



**Figure 8.** Relationships between (a) OLR and biogas production in the AHR series and (b) OLR and CH<sub>4</sub> production in the AHR series.

### 3.6. Identifying the Optimum OLR

The most suitable OLR to maintain an efficient anaerobic treatment system was identified in this study as 15 kgCOD/m<sup>3</sup>·d; at this value, the CH<sub>4</sub> production and effective COD removal were maximized. Increasing the OLR above 15 kgCOD/m<sup>3</sup>·d causes the

efficiency of the system to decrease. This is consistent with Musa et al. [42], who found that an OLR of 0.52 gCOD/L·d achieved approximately 90% COD removal efficiency, but that the efficiency dropped to below 50% when the loading rate was increased to 15 gCOD/L·d. Similarly, Tritt and Kang reported that a similar reactor achieved a maximum COD removal efficiency of 95% at an OLR of 1 kgCOD/m<sup>3</sup>·d with an HRT of 7.5 days [43]. At an OLR higher than 4.0 kgCOD/m<sup>3</sup>·d, the COD removal efficiency was 75% with an HRT of 2 days. Increasing the OLR causes the volatile solids (VS) in the system to increase, which in turn increases the biomass in the system, as shown by Pereira and Yilmaz [44,45].

### 3.7. Biomass and Microbial Activities

As shown in Table 3, at the beginning of the experiment, the influent leachate to AHR-1 and AHR-2 had equal VSS values of 149 gVSS/reactor. Setting the system to an OLR of 5 kgCOD/m<sup>3</sup>·d for 60 days caused the VSS to decrease. AHR-1 contained a suspended VSS of 73 g and an attached VSS of 5 g. Since AHR-2 received effluent from AHR-1, its VSS was lower, both suspended in the system and attached to the media. The specific methanogenic activity (SMA) is essential for describing microbial activity. This study found that setting the OLR at 5 kgCOD/m<sup>3</sup>·d resulted in an SMA system of 0.39 LCH<sub>4</sub>/gCOD removed in the AHR series. When increasing the OLR to 10, 15, and 20 kgCOD/m<sup>3</sup>·d, the SMA increased to average values of 0.35, 0.52, and 0.44 LCH<sub>4</sub>/gCOD removed, respectively. Increasing the OLR to 20 kgCOD/m<sup>3</sup>·d resulted in the AHR series reaching a high VSS of 303 gVSS, but the SMA decreased by 0.08 LCH<sub>4</sub>/gCOD removed. This indicates that the system is efficient over an OLR range between 10 and 15 kgCOD/m<sup>3</sup>·d, whereas the SMA increased from 0.35 to 0.52 LCH<sub>4</sub>/gCOD removed.

**Table 3.** The specific methanogenic activity (SMA) of biomass inside the AHR series.

| Day of Operation | AHR-1, Biomass (gVSS) |          | AHR-2, Biomass (gVSS) |          | AHR Series, Biomass (gVSS) |          | Total Biomass (gVSS) | SMA of AHR Series (LCH <sub>4</sub> /gCOD Removed) |
|------------------|-----------------------|----------|-----------------------|----------|----------------------------|----------|----------------------|--|
|                  | Suspended             | Attached | Suspended             | Attached | Suspended                  | Attached |                      |  |
| 0                | 149                   | 0        | 149                   | 0        | 298                        | 0        | 298                  | -  |
| 60               | 73                    | 5        | 50                    | 3        | 129                        | 8        | 137                  | 0.27   |
| 120              | 97                    | 11       | 58                    | 9        | 165                        | 20       | 185                  | 0.35   |
| 180              | 106                   | 13       | 68                    | 11       | 204                        | 24       | 228                  | 0.52   |
| 210              | 130                   | 16       | 74                    | 13       | 274                        | 29       | 303                  | 0.44   |

## 4. Future Prospects

The promising outcomes of our investigation into optimizing anaerobic hybrid reactors for the treatment of high-strength fresh leachate and biogas generation set the stage for several future research directions. Foremost, exploring the integration of additional treatment stages or technologies could further enhance effluent quality and biogas yield, potentially incorporating nutrient recovery processes for a more holistic approach to waste management. A detailed environmental impact assessment is an issue that will be studied in the future. This includes analyzing the system's carbon footprint, the impact on greenhouse gas emissions, and the potential impact on the local ecosystems. Moreover, the development and application of system dynamic models could offer deeper insights into the long-term operational efficiencies, economic viability, and environmental impacts of scaled-up systems. This approach would not only refine our understanding of the anaerobic digestion process in varying climatic and waste composition scenarios but also bolster the feasibility of deploying such systems in diverse geographical contexts, particularly in developing countries where waste management challenges are most acute. Ultimately, advancing these research areas could significantly contribute to the global pursuit of sustainable, energy-positive waste management solutions. To promote the widespread adoption of sustainable leachate treatment technologies, policymakers and the waste management industry must collaborate closely, including addressing challenges in high-strength fresh leachate treatment. This entails updating policy frameworks to incentivize sustainability

and foster public–private partnerships, thereby overcoming existing adoption barriers and advancing global waste management practices.

## 5. Conclusions

The main goal of this research was to optimize the operational settings of the AHR series to handle concentrated fresh leachate and boost biogas production effectively. After conducting experiments, the study determined that an OLR of 15 kgCOD/m<sup>3</sup>·d and an HRT of 7 days were optimal for maximizing biogas and CH<sub>4</sub> yields. AHR-1 had an average CH<sub>4</sub> production per COD removal of 0.57–0.76 L/gCOD removed; the corresponding value for AHR-2 was 0.27–0.47 L/gCOD removed. The AHR series had an average of 0.33–0.67 L/gCOD removed. The significance of this study lies in its guidance for leachate management, especially in treating leachate with a high organic load. For example, leachate treatments may be integrated into alternative energy developments using emerging environmental technology. Future research and development should aim to maximize the potential of the AHR series for sustainable waste management practices. As the global waste management challenge persists, the findings of this study can encourage the development of an environmentally friendly, efficient, and more effective waste treatment system suitable for use in scenarios with high organic loads. This technology may help to support a transition to more sustainable wastewater management in the future.

**Author Contributions:** S.S.: methodology, formal analysis, writing-original draft; K.W.: supervision, resources, project administration, review and editing; S.T.: supervision, resources, project administration; C.C.: review and editing, project administration, validation; P.C.: review and editing, project administration, validation. All authors have read and agreed to the published version of the manuscript.

**Funding:** This research was financially supported by the Petchra Pra Jom Klao Scholarship (No. 60300800201), King Mongkut's University of Technology Thonburi.

**Institutional Review Board Statement:** Not applicable.

**Informed Consent Statement:** Not applicable.

**Data Availability Statement:** Data will be made available on request.

**Acknowledgments:** This study was supported by the Joint Graduate School of Energy and Environment (JGSEE), King Mongkut's University of Technology Thonburi, Center of Excellence on Energy Technology and Environment (CEE), Ministry of Higher Education, Science, Research and Innovation (MHESI). We would like to thank Pairojsompong Panitch Co., Ltd., for providing the opportunity to gather information at the study sites.

**Conflicts of Interest:** The authors declare no conflicts of interest.

## References

1. Khan, M.; Mubeen, I.; Yu, C.; Zhu, G.; Khalid, A.; Yan, M. Waste to energy incineration technology: Recent development under climate change scenarios. *Waste Manag. Res.* **2022**, *40*, 1708–1729. [[CrossRef](#)] [[PubMed](#)]
2. Mabalane, P.; Oboirien, B.; Sadiku, E.; Masukume, M. A techno-economic analysis of anaerobic digestion and gasification hybrid system: Energy recovery from municipal solid waste in south Africa. *Waste Biomass Valor.* **2020**, *12*, 1167–1184. [[CrossRef](#)]
3. Tun, M.; Palacky, P.; Juchelková, D.; Sít'ař, V. Renewable waste-to-energy in Southeast Asia: Status, challenges, opportunities, and selection of waste-to-energy technologies. *Appl. Sci.* **2020**, *10*, 7312. [[CrossRef](#)]
4. Devendran, A.A.; Mainali, B.; Khatiwada, D.; Golzar, F.; Mahapatra, K.; Toigo, C.H. Optimization of municipal waste streams in achieving urban circularity in the city of Curitiba, Brazil. *Sustainability* **2023**, *15*, 3252. [[CrossRef](#)]
5. Lara-Topete, G.O.; Yebra-Montes, C.; Orozco-Nunnally, D.A.; Robles-Rodriguez, C.E.; Gradilla-Hernández, M.S. An integrated environmental assessment of MSW management in a large city of a developing country: Taking the first steps towards a circular economy model. *Front. Environ. Sci.* **2022**, *10*, 838542. [[CrossRef](#)]
6. Vaverková, M.D.; Elbl, J.; Koda, E.; Adamcová, D.; Bilgin, A.; Lukas, V.; Podsalek, A.; Kintl, A.; Wdowska, M.; Brtnický, M.; et al. Chemical composition and hazardous effects of leachate from the active municipal solid waste landfill surrounded by farmlands. *Sustainability* **2020**, *12*, 4531. [[CrossRef](#)]
7. Chakri, A.; Ouarghi, H.; Ghalit, M.; Ahari, M. Elimination of orthophosphate from synthetic leachate using adsorption on bentonite clay. *E3S Web Conf.* **2023**, *364*, 02011.

8. Pinpatthanapong, K.; Khetkorn, W.; Honda, R.; Phattarapattamawong, S.; Treesubsuntorn, C.; Panasan, N.; Boonmawat, P.; Tianthong, Y.; Lipiloet, S.; Sorn, S.; et al. Effects of high-strength landfill leachate effluent on stress-induced microalgae lipid production and post-treatment micropollutant degradation. *J. Environ. Manag.* **2022**, *324*, 116367. [[CrossRef](#)]
9. Feng, D.; Song, C.; Mo, W. Environmental, human health, and economic implications of landfill leachate treatment for per-and polyfluoroalkyl substance removal. *J. Environ. Manag.* **2021**, *289*, 112558. [[CrossRef](#)]
10. Reddy, C.; Rao, D.; Kalamdhad, A. Statistical modelling and assessment of landfill leachate emission from fresh municipal solid waste: A laboratory-scale anaerobic landfill simulation reactor study. *Waste Manag. Res.* **2020**, *38*, 1161–1175. [[CrossRef](#)]
11. Abouri, M.; Elmaguiri, A.; Souabi, S.; Aboulhassan, M.A. Valorisation of a wastewater in the treatment of leachate from municipal solid waste in Morocco. *Int. J. Environ. Waste Manag.* **2019**, *23*, 27–39. [[CrossRef](#)]
12. Wang, Z.; Banks, C.J. Treatment of a high-strength sulphate-rich alkaline leachate using an anaerobic filter. *Waste Manag.* **2007**, *27*, 359–366. [[CrossRef](#)]
13. Liu, J.; Luo, J.; Zhou, J.; Liu, Q.; Qian, G.; Xu, Z.P. Inhibitory effect of high-strength ammonia nitrogen on bio-treatment of landfill leachate using EGSB reactor under mesophilic and atmospheric conditions. *Bioresour. Technol.* **2012**, *113*, 239–243. [[CrossRef](#)]
14. Xaypanya, P.; Takemura, J.; Chiemchaisri, C.; Hul, S.; Tanchuling, M. Characterization of landfill leachates and sediments in major cities of Indochina peninsular countries heavy metal partitioning in municipal solid waste leachate. *Environments* **2018**, *5*, 65. [[CrossRef](#)]
15. Zloch, J.; Vaverková, M.D.; Adamcová, D.; Radziemska, M.; Vyhnánek, T.; Trojan, V.; Đorđević, B.; Brtnický, M. Seasonal changes and toxic potency of landfill leachate for white mustard (*Sinapis alba* L.). *Acta Univ. Agric. Silvic. Mendel. Brun.* **2018**, *66*, 235–242. [[CrossRef](#)]
16. Metcalf & Eddy Inc. *Wastewater Engineering: Treatment and Reuse*, 4th ed.; McGraw Hill: New York, NY, USA, 2003.
17. Banerjee, S.; Prasad, N.; Selvaraju, S. Reactor design for biogas production—a short review. *J. Energy Power Technol.* **2022**, *4*, 004. [[CrossRef](#)]
18. Anjum, M.; Anees, M.; Qadeer, S.; Khalid, A.; Kumar, R.; Barakat, M. A recent progress in the leachate pretreatment methods coupled with anaerobic digestion for enhanced biogas production: Feasibility, trends, and techno-economic evaluation. *Int. J. Mol. Sci.* **2023**, *24*, 763. [[CrossRef](#)]
19. Siciliano, A.; Limonti, C.; Curcio, G.; Calabrò, V. Biogas generation through anaerobic digestion of compost leachate in semi-continuous completely stirred tank reactors. *Processes* **2019**, *7*, 635. [[CrossRef](#)]
20. Kheradmand, S.; Karimi-Jashni, A.; Sartaj, M. Treatment of municipal landfill leachate using a combined anaerobic digester and activated sludge system. *Waste Manag.* **2010**, *30*, 1025–1031. [[CrossRef](#)] [[PubMed](#)]
21. Dhamsaniya, M.; Sojitra, D.; Modi, H.; Shabiiimam, M.A.; Kandyia, A. A review of the techniques for treating the landfill leachate. *Mater. Today Proc.* **2023**, *77*, 358–364. [[CrossRef](#)]
22. Bera, S.; Godhaniya, M.; Kothari, C. Emerging and advanced membrane technology for wastewater treatment: A review. *J. Basic Microbiol.* **2021**, *62*, 245–259. [[CrossRef](#)] [[PubMed](#)]
23. Mazhar, M.A.; Khan, N.A.; Khan, A.H.; Ahmed, S.; Siddiqui, A.A.; Husain, A.; Tirth, V.; Islam, S.; Shukla, N.K.; Changani, F.; et al. Upgrading combined anaerobic-aerobic UASB-FPU to UASB-DHS system: Cost comparison and performance perspective for developing countries. *J. Clean. Prod.* **2021**, *284*, 124723. [[CrossRef](#)]
24. Sutthiprapa, S.; Towprayoon, S.; Chiemchaisri, C.; Chaiprasert, P.; Wangyao, K. Performance Comparison between Anaerobic Hybrid Reactor and Anaerobic Continuous Stirred-Tank Reactor for High-Strength Fresh Leachate Treatment. *Pol. J. Environ. Stud.* **2024**, *33*, 2307–2315. [[CrossRef](#)]
25. Holliger, C.; Alves, M.; Andrade, D.; Angelidaki, I.; Astals, S.; Baier, U.; Bougrier, C.; Burrière, P.; Carballa, M.; de Wilde, V.; et al. Towards a standardization of biomethane potential tests. *Water Sci. Technol.* **2016**, *74*, 2515–2522. [[CrossRef](#)]
26. American Public Health Association. *APHA Standard Methods for the Examination of Water and Wastewater*, 23rd ed.; American Public Health Association: Washington, DC, USA, 2017.
27. Maleki, E.; Catalan, L.; Liao, B. Effect of organic loading rate on the performance of a submerged anaerobic membrane bioreactor (SANMBR) for malting wastewater treatment and biogas production. *J. Chem. Technol. Biotechnol.* **2018**, *93*, 1636–1647. [[CrossRef](#)]
28. Genethliou, C.; Tatoulis, T.; Charalampous, N.; Dailianis, S.; Tekerlekopoulou, A.G.; Vayenas, D.V. Treatment of raw sanitary landfill leachate using a hybrid pilot-scale system comprising adsorption, electrocoagulation and biological process. *J. Environ. Manag.* **2023**, *330*, 117129. [[CrossRef](#)]
29. Rinquest, Z.; Basitere, M.; Mewa-Ngongang, M.; Ntwampe, S.K.O.; Njoya, M. Optimization of the COD Removal Efficiency for a Static Granular Bed Reactor Treating Poultry Slaughterhouse Wastewater. *Preprints* **2019**, 2019020036.
30. Harsha, G.; Maurya, N. Liquid state anaerobic co-digestion of cattle manure and wheat straw at various mix ratios for optimal biogas production. *Orient. J. Chem.* **2022**, *38*, 777–784. [[CrossRef](#)]
31. Rumsey, D.J. *Statistics for Dummies*; John Wiley & Sons: Hoboken, NJ, USA, 2015.
32. Reddy, C.V.; Rao, D.S.; Kalamdhad, A.S. Combined treatment of high-strength fresh leachate from municipal solid waste landfill using coagulation-flocculation and fixed bed upflow anaerobic filter. *J. Water Process Eng.* **2022**, *46*, 102554. [[CrossRef](#)]
33. Safari, E.; Valizadeh, R. Analysis of biological clogging potential in a simulated compacted clay liner subjected to high-strength leachate infiltration. *Int. J. Environ. Sci. Technol.* **2018**, *15*, 1029–1038. [[CrossRef](#)]
34. Dang, Y.; Ye, J.; Mu, Y.; Qiu, B.; Sun, D. Effective anaerobic treatment of fresh leachate from MSW incineration plant and dynamic characteristics of microbial community in granular sludge. *Appl. Microbiol. Biotechnol.* **2013**, *97*, 10563–10574. [[CrossRef](#)] [[PubMed](#)]

35. Dubber, D.; Gray, N.F. Replacement of chemical oxygen demand (COD) with total organic carbon (TOC) for monitoring wastewater treatment performance to minimize disposal of toxic analytical waste. *J. Environ. Sci. Health A* **2010**, *45*, 1595–1600. [[CrossRef](#)] [[PubMed](#)]
36. Moujanni, A.; Qarraey, I.; Ouattmane, A. Biogas recovery from fresh landfill leachates by using a coupled air stripping-up follow anaerobic sludge blanket (UASB) process. *Environ. Eng. Res.* **2020**, *27*, 200470. [[CrossRef](#)]
37. Liberti, F.; Pistoiesi, V.; Mouftahi, M.; Hidouri, N.; Bartocci, P.; Massoli, S.; Zampilli, M.; Fantozzi, F. An incubation system to enhance biogas and methane production: A case study of an existing biogas plant in Umbria, Italy. *Processes* **2019**, *7*, 925. [[CrossRef](#)]
38. Ahmad, I.; Abdullah, N.; Chelliapan, S.; Yuzir, A.; Koji, I.; Al-Dailami, A.; Arumugham, T. Effectiveness of anaerobic technologies in the treatment of landfill leachate. In *Strategies of Sustainable Solid Waste Management*; IntechOpen: London, UK, 2021.
39. Collivignarelli, M.C.; Abbà, A.; Caccamo, F.; Calatroni, S.; Torretta, V.; Katsoyiannis, I.A.; Miino, M.C.; Rada, E.C. Applications of up-flow anaerobic sludge blanket (UASB) and characteristics of its microbial community: A review of bibliometric trend and recent findings. *Int. J. Environ. Res. Public Health* **2021**, *18*, 10326. [[CrossRef](#)] [[PubMed](#)]
40. Umiejewska, K. Conversion of organic compounds into biogas on a full scale brewery WWTP using IC reactor. *E3S Web Conf.* **2019**, *116*, 00095. [[CrossRef](#)]
41. Yodthongdee, S.; Weerayuttil, P.; Khuanmar, K. Methane production in batch anaerobic digestion of livestock manures with different substrate concentrations. *Int. J. Eng. Technol.* **2018**, *7*, 1380. [[CrossRef](#)]
42. Musa, M.; Idrus, S.; Man, H.; Daud, N. Effect of organic loading rate on anaerobic digestion performance of mesophilic (UASB) reactor using cattle slaughterhouse wastewater as substrate. *Int. J. Environ. Res. Public Health* **2018**, *15*, 2220. [[CrossRef](#)] [[PubMed](#)]
43. Tritt, W.; Kang, H. Slaughterhouse wastewater treatment in a bamboo ring anaerobic fixed-bed reactor. *Environ. Eng. Res.* **2017**, *23*, 70–75. [[CrossRef](#)]
44. Pereira, E.L.; Borges, A.C.; da Silva, G.J. Effect of the progressive increase of organic loading rate in an anaerobic sequencing batch reactor for biodiesel wastewater treatment. *Water* **2022**, *14*, 223. [[CrossRef](#)]
45. Yilmaz, T.; Erdirencelebi, D.; Berkay, A. Effect of COD/SO<sub>4</sub><sup>2-</sup> ratio on anaerobic treatment of landfill leachate during the start-up period. *Environ. Technol.* **2012**, *33*, 313–320. [[CrossRef](#)] [[PubMed](#)]

**Disclaimer/Publisher’s Note:** The statements, opinions and data contained in all publications are solely those of the individual author(s) and contributor(s) and not of MDPI and/or the editor(s). MDPI and/or the editor(s) disclaim responsibility for any injury to people or property resulting from any ideas, methods, instructions or products referred to in the content.