

# Influence of Low Air Pressure on the Partial Denitrification-Anammox (PD/A) Process

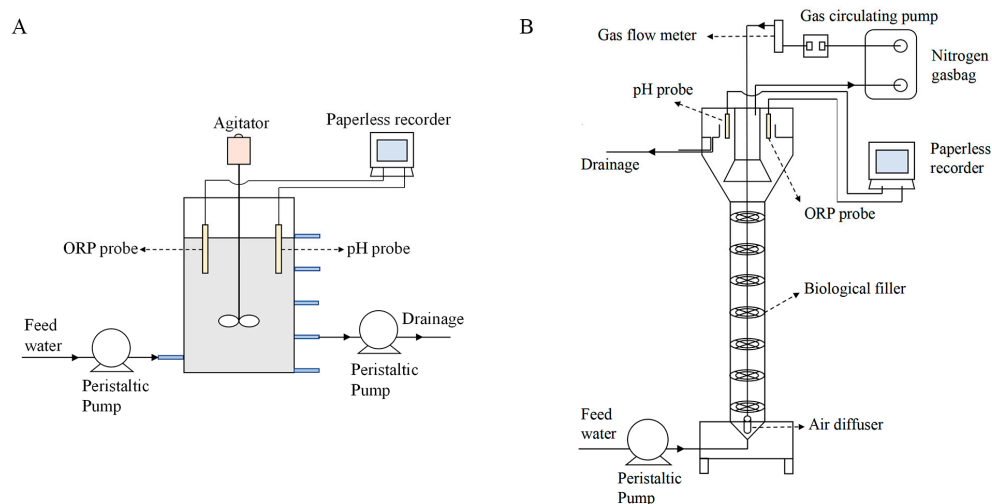
Wen Dai <sup>1</sup>, Zhenpeng Han <sup>1</sup>, Yongze Lu <sup>1</sup>, Shuping Li <sup>2,3</sup>, Gangyin Yan <sup>2,3</sup> and Guangcan Zhu <sup>1,2,\*</sup>

<sup>1</sup> Department of Environmental Science and Engineering, School of Energy and Environment, Southeast University, Nanjing 210096, China

<sup>2</sup> Key Laboratory of Water Pollution Control and Ecological Restoration of Xizang, National Ethnic Affairs Commission, Xizang Minzu University, Xianyang 712082, China

<sup>3</sup> Information Engineer College, Xizang Minzu University, Xianyang 712082, China

\* Correspondence: gc-zhu@seu.edu.cn



**Figure S1.** Schematic diagram of (A)SBR system (B)USR system.

**Table S1.** The composition of synthetic wastewater for (a) SBR-PD (b) SBR-A (c) USR-PD/A.

(a)

Component	Concentration (mg/L)	Component	Concentration (mg/L)
NO <sub>3</sub> <sup>-</sup> -N	50	KI	0.18
COD(CH <sub>3</sub> COONa)	140	H <sub>3</sub> BO <sub>4</sub>	0.15
NH <sub>4</sub> <sup>+</sup> -N	5	CoCl <sub>2</sub> ·6H <sub>2</sub> O	0.15
PO <sub>4</sub> <sup>3-</sup> -P	5	ZnSO <sub>4</sub> ·7H <sub>2</sub> O	0.12
CaCl <sub>2</sub> ·2H <sub>2</sub> O	0.03	MnCl <sub>2</sub> ·4H <sub>2</sub> O	0.12
MgSO <sub>4</sub> ·7H <sub>2</sub> O	0.06	NaMoO <sub>4</sub> ·2H <sub>2</sub> O	0.06
FeCl <sub>3</sub> ·6H <sub>2</sub> O	1.5	CuSO <sub>4</sub> ·5H <sub>2</sub> O	0.06

(b)

Component	Concentration (mg/L)	Component	Concentration (mg/L)
NH <sub>4</sub> <sup>+</sup> -N	50	ZnSO <sub>4</sub> ·7H <sub>2</sub> O	0.43
NO <sub>2</sub> <sup>-</sup> -N	65	CoCl <sub>2</sub> ·6H <sub>2</sub> O	0.24
KHCO <sub>3</sub>	500	MnCl <sub>2</sub> ·4H <sub>2</sub> O	0.99
CaCl <sub>2</sub> ·2H <sub>2</sub> O	180	CuSO <sub>4</sub> ·5H <sub>2</sub> O	0.25

MgSO <sub>4</sub> ·7H <sub>2</sub> O	300	NaMoO <sub>4</sub> ·2H <sub>2</sub> O	0.22
KH <sub>2</sub> PO <sub>4</sub>	30	NiCl <sub>2</sub> ·6H <sub>2</sub> O	0.19
FeSO <sub>4</sub>	5.0	H <sub>3</sub> BO <sub>4</sub>	0.014

(c)

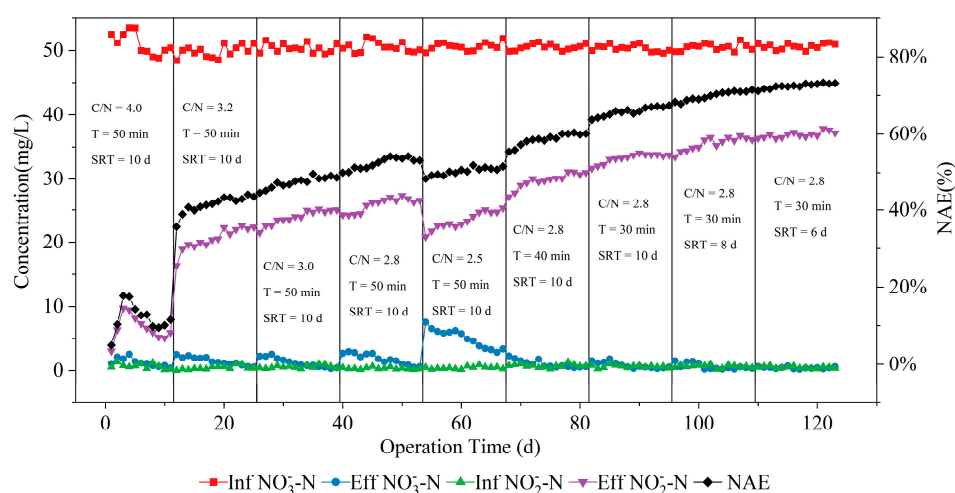
Component	Concentration (mg/L)	Component	Concentration (mg/L)
NH <sub>4</sub> <sup>+</sup> -N	50	ZnSO <sub>4</sub> ·7H <sub>2</sub> O	0.43
NO <sub>3</sub> <sup>-</sup> -N	65	CoCl <sub>2</sub> ·6H <sub>2</sub> O	0.24
COD(CH <sub>3</sub> COONa)	195	MnCl <sub>2</sub> ·4H <sub>2</sub> O	0.99
KHCO <sub>3</sub>	500	CuSO <sub>4</sub> ·5H <sub>2</sub> O	0.25
CaCl <sub>2</sub> ·2H <sub>2</sub> O	180	NaMoO <sub>4</sub> ·2H <sub>2</sub> O	0.22
MgSO <sub>4</sub> ·7H <sub>2</sub> O	300	NiCl <sub>2</sub> ·6H <sub>2</sub> O	0.19
KH <sub>2</sub> PO <sub>4</sub>	30	H <sub>3</sub> BO <sub>4</sub>	0.014
FeSO <sub>4</sub>	5.0		

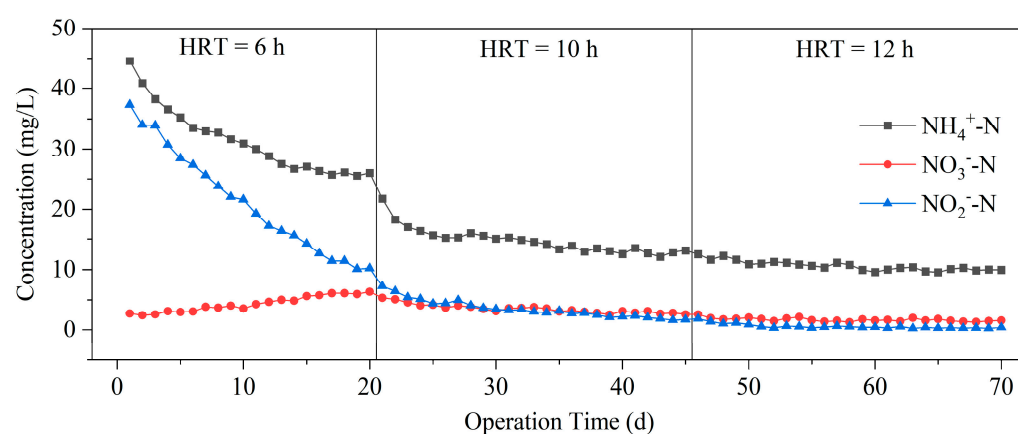
**Table S2.** The operation conditions of reactors.

Reactor	Start-up (96 kPa)	Phase 96 kPa	Phase 72 kPa	Phase 65 kPa
SBR-PD	120 d	1-10 d	11-35 d	36-60 d
SBR-A	35 d	1-35 d	36-70 d	71-105 d
USR-PD/A	50 d	1-10 d	11-40 d	41-70 d

**Table S3.** Microbial community richness and diversity of the PD/A system in end stage of different phases. R.96 kPa: sample at Phase 96 kPa (day 10); R.72 kPa: sample at Phase 72 kPa (day 45); R.65 kPa: sample at Phase 65 kPa (day 70).

Sample description	OTUs	Richness		Diversity	Coverage
		Chao	Ace	Shannon	
R.96 kPa	104	115.50	121.78	3.66	0.994
R.72 kPa	158	240.88	203.99	4.39	0.986
R.65 kPa	131	147.73	151.65	3.87	0.992

**Figure S2.** Nitrogen removal performance of SBR-PD during the start-up period.



**Figure S3.** Nitrogen removal performance of PD/A system during the start-up period.